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C-Language Programming for Development of Conventional Water Treatment Plants Decision Support System

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Abstract

Water-Decision Support System (DSS) tools enhance decision-makings towards improved water supply in a given region. The rigours of manual design of the conventional water treatment plants are easily eliminated with the use of softwares as in the case of DSS. Therefore, this paper focuses on the development of a Water-DSS for design of treatment plant in Karkala Town, Udupi District of India. A four-decade population projection was made using the baseline data of 1971 till date. The manual computation for water demand, unit operations and adjoining facilities was carried out and later coded in C-programming language for development of a DSS for easier design and process selection. Data validation was done and results from the two approaches were compared. With the C-programming technique, a decision support tool for design and process selection of drinking water treatment plant using conventional method has been developed and named Water-DSS1. The designed tool is simple, accurate, flexible, efficient and universal, easily adaptable to any similar conventional treatment plant. Water-DSS1 is thus recommended for general use in ultimately alleviating water supply challenges.

Keywords

1. Introduction

In a simple form, Decision Support System, DSS is any system supporting decision-making, including executive
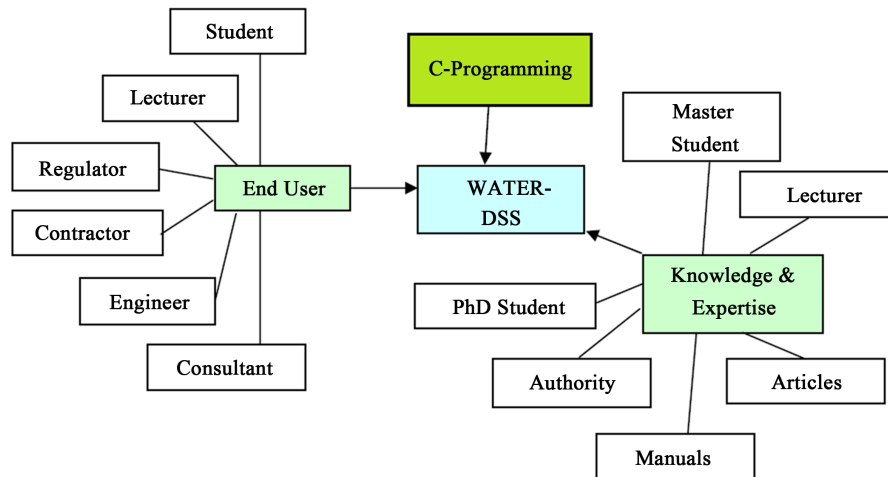
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Figure 2. WATER-DSS development structure.

(c) Conventional Water Treatment Plant Units

The units of a typical conventional treatment plant include aeration, plain sedimentation tank, sedimentation aided with coagulation, flocculation, filters, disinfection etc. **Figure 3** shows the flowchart of conventional water treatment plant.

(d) Manual design of the Water Treatment Plant ([7] [8])

(i) Forecasting population

The Conventional Water Treatment Plant is being designed for the next 3 decades.

Forecasting population of the study area for 3 decades by the Geometric Increase Method:

If the present is *P* and the average percentage growth is I_G the population at the end of *n* decade will be:

$$I_G = P\left[1 + \frac{IG}{100}\right]^n$$

So from **Table 1**, the Expected Population of Karkala by 2043 is 38,396 people.

(ii) Water demand

The water requirement per capita demand of Karkala = 100 LPCD (BIS Code).

Thus, water requirement of Karkala per day = 38,396 × 100 = 3,839,600 = 3.84 MLD.

So, the proposed water treatment plant design is of approximately 3.85 MLD in capacity.

(iii) Aeration process

Assuming number of steps = 5

and that tread width, t = 250 mm

Diameter of the first step, D_1 = 1 m (including the diameter of pipe)

Diameter of the second step, $D_2 = D_1 + 2t = 1 + 2 \times (0.25) = 1.5$ m

Diameter of the third step, $D_3 = D_2 + 2t = 1.5 + 2 \times (0.25) = 2$ m

Diameter of the fourth step, $D_4 = D_3 + 2t = 2 + 2 \times (0.25) = 2.5$ m

Diameter of the fifth step, $D_5 = D_4 + 2t = 2.5 + 2 \times (0.25) = 3$ m

Diameter of aeration tank (collector) = $D_5 + 2(1) = 3 + 2 = 5$ m

Further assuming that:
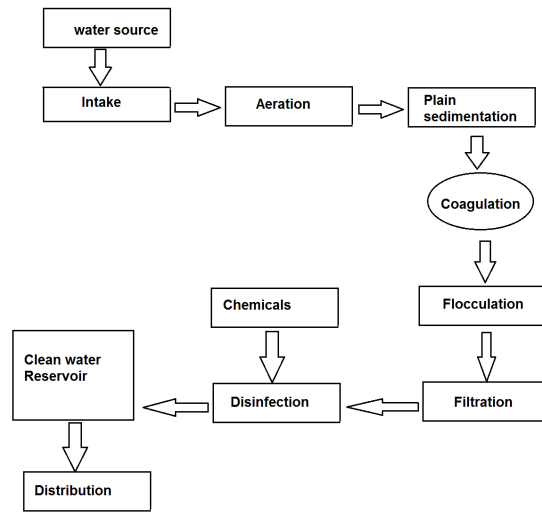
Rise of 1st step = 0.3 m

Rise of 2nd step = 0.4 m

Rise of 3rd step = 0.5 m

Rise of 4th step = 0.6 m

Rise of 5th step = 0.7 m

Overall Dimension of Aeration tank of diameter 5 m and total height of Cascade is 2.5 m.

Figure 3. Flowchart of conventional water treatment plant.

Table 1. Forecasting of population for 3 decades.

Year	Population	Increase in Population	% Increase in population
1971	18,593	-	
1981	20,713	2120	$\dfrac{2120}{18,593}\times100=11.402$
1991	24,109	3396	$\dfrac{3396}{20,713}\times100=16.396$
2001	25,116	1007	$\dfrac{1007}{24,109}\times100=4.177$
Total		6523	31.975 %
Average per decade		2175	10.658 %

Year	Expected Population
2001	$25,116+\dfrac{10.658}{100}\times25,116=27,793$
2011	$27,793+\dfrac{10.658}{100}\times27,793=30,756$
2021	$30,756+\dfrac{10.658}{100}\times30,756=34,007$
2031	$34,007+\dfrac{10.658}{100}\times34,007=37,601$
2043	$37,601+\left(\dfrac{10.568}{100}\times37,601\right)\times0.2=38,396$

(iv) Plain sedimentation tank

Quantity of water to be treated in 24 hours = 3.85×10^6 liters = 3850 m^3.

Quantity of water to be treated by the sedimentation tank during detention period of 6 hours = $\dfrac{3850}{24}\times6$ = 962.5 m^3.

Thus the capacity of the sedimentation tank required = 962.5 m^3.

Assume the velocity of flow = 18 cm per min or 0.003 m/s.

Length of the tank required = Velocity of tank (m/s) × Detention period (s) = 0.003 × (6 × 60 × 60) = 64.8 m.

Cross section of tank required = $\dfrac{\text{capacity of tank required}\left(\text{in m}^3\right)}{\text{Length of tank}\left(\text{in m}\right)}$ = $\dfrac{962.5}{64.8}$ = 14.85 m^2.

Assume the depth of water = 4 m which includes allowable allowance for sludge to be made as 80 cm (or 0.8 m).

Required width of tank = $\dfrac{14.85}{3.2}$ = 4.64 m.

Providing 0.5 m for free board, overall depth of the tank = 4 + 0.5 = 4.5.

Therefore the dimensions of the designed tank are = (64.8 × 4.64 × 4.5) m.

Note that the length of the tank may be provided in one, two, or three parts depending upon the shape of the area available.

(v) Sedimentation tank aided with coagulants

(1) Chemical feeding

Using alum as coagulant, the optimum quantity of dose will be determined actually by jar test in the laboratory.

Let the optimum dose be 5 - 8 mg/liter.

The average quantity of alum required = $\dfrac{962.5 \times 10^3 \times 5}{10^6}$ to $\dfrac{962.5 \times 10^3 \times 8}{10^6}$ = 4.82 to 7.7 kg/day.

The maximum requirement in summer will be 1.5 times more = 7.23 to 11.55 kg/day.

This quantity of alum shall be first mixed with the water to form a solution of 5 strength and then will be added through solution feed device which is given as = 11.55 × 20 liters/day = $\dfrac{11.55 \times 20}{60 \times 24}$ = 0.1604 liters/min.

Minimum dose which will be fed during average demand = $\dfrac{0.1604}{1.5}$ = 0.1609 liters/min.

Quantity of solution to be fed in 8 hours/day = 0.1604 × 60 × 8 = 76.99 liters.

Providing solution tank of capacity = 0.07699 m^3 = 0.077 m^3.

Keeping the depth of solution in the tank as 0.35 m and 0.15 m as free board.

The sides of the square tank = $\sqrt{\dfrac{0.077}{0.35}}$ = 0.4699 m = 0.5 m.

So the designed size of Solution Tank = (0.5 × 0.5 × 0.5) m.

(2) Approach channel

The flow of channel = $\dfrac{962.5}{24 \times 60 \times 60}$ = 0.11 m^3/s.

Providing a velocity of 0.4 m/s, the cross sectional area of approach channel = $\dfrac{0.011}{0.4}$ = 0.0275 m^2.

Provide (0.175 × 0.225) m channel with 175 mm water depth and 50 cm free board.

(3) Mixing tank

Mechanical flash mixers will be used for mixing the coagulant solution with the water.

Assuming the detention period of one minute (60 s).

Capacity of flash mixer = 0.11 × 60 = 0.66 m^3.

Providing depth of 1m, the sides of the square plan mixing tank = $\sqrt{\dfrac{0.66}{1}}$ = 0.8 m.

Therefore provide (1 × 1 × 1) m size of mixing tank with flocculator.

(v) Flocculating Tank

A flocculating tank with mixing slow moving paddles is provided with variable speed electric motors.

Assuming the flocculating time of 30 minutes, the capacity of each flocculating tank = 0.11 × 30 = 19.8 m^3.

So, provide a channel of capacity = 19.8 m^3.

Providing 1.6 m depth of water and 10 m of length of channel its width = $\dfrac{19.8}{1.6 \times 10}$ = 1.2375 m.

Therefore, provide channel of size (10 × 1.4 × 1.6) m with water depth of water 1.4 m and 0.2 m as free board in continuation on flash mixer.

(vi) Settling Tank

Provide a rectangle sedimentation tank with a square tank with surface loading of 2000 litres/hour/m^2 plan of area.

Surface loading of each tank = $\dfrac{0.11 \times 60 \times 60 \times 10^3}{2000}$ = 19.8 m^3.

Assume length = 6 m.

Therefore width becomes = $\dfrac{19.6}{6}$ = 3.3 m.

Therefore weir loading in the settling tank at average flow is given as = $\dfrac{Q}{\text{Perimeter}}$ = $\dfrac{962.5}{6 \times 3.3}$ = 48.61 m^3/m/day.

Providing a detention period of 2.5 hours at a time of maximum flow.

Capacity of tank = $\dfrac{962.5 \times 2.5}{24}$ = 1000.26 m^3.

Now quantity of water to be treated in one hour = $\dfrac{962.5}{24}$ = 40.104 m^3.

Therefore required depth of tank = $\dfrac{40.104}{6 \times 3.3}$ = 2.035 m.

Add 0.5 m for storage and 0.5 m for free board, say overall depth = 3 m.

Provide rectangular settling tank (6 × 3.3 × 3) m. The bottom of the tank is sloped of 1 in 12 pushing the sludge towards the discharging end, with the help of scrappers from where it will be removed by the sludge outlet under hydrostatic pressure of water filled in the tank.

The water will be collected from settling tank over its discharging end along the weir provided all around the water from this channel shall be taken into the rapid gravity filters in covered channels (0.3 × 0.3) m.

(vii) Rapid Gravity Filter

Quantity of water to be treated = 3.85 litres/day.

Assume the rate of filtration of rapid gravity filter—2000 litres/m^2/hour and also assuming that 30 minutes shall be utilized daily in the back-washing of the filter, the total filter area required = $\dfrac{3.85 \times 10^6}{23.5 \times 2000}$ = 81.92 m^2.

Provide 4 units of rapid gravity filters with two numbers of stand-by units.

Surface area of each unit = $\dfrac{81.92}{2}$ = 40.96.

Therefore each unit of size = (6.5 × 6.5) m.

(viii) Chlorination Plant

The dose of the chlorine to be added will vary from 0.5 to 1.0 ppm depending on the quantity of water and the chlorine demand tests.

Therefore quantity of chlorine required = $\dfrac{3.85 \times 10^3 \times 0.5}{24 \times 10^{\wedge}3}$ = 0.08 kg/hour.

Therefore liquid chlorinator having capacity 0.1 to 5 kg/hour will be installed.

(ix) Underground Reservoir Water

Underground clear water reservoir having capacity of about 8 hours will be provided.

Quantity of water to be stored = 3.85 × 10^3 m^3.

Providing 5 m depth, area of clear water reservoir = $\dfrac{3.85 \times 10^{\wedge}3}{5}$ = 770 m^2.

So, the dimensions of the designed underground clear water reservoir = (40 × 19.25 × 5) m.

(x) Design of Pumps (Centrifugal Pumps)

We are adopting two pump stations, one is at source and another is in the middle.

Maximum daily water requirement = 1.5 × 3.85 × 1000 m^3/day = 5.775 × 10^3 m^3/day.

Since Pumping time is 8 hours per day, $Q = \dfrac{5.775 \times 10^{\wedge}3}{8 \times 60 \times 60} = 0.200 \ \text{m}^3/\text{day}$.

Assume: Velocity in pipe, $V = 2$ m/s.

Now, $V = \dfrac{Q}{A} = \dfrac{4Q}{\pi d^2}$,

Therefore $d = \sqrt{\dfrac{4Q}{\pi d^2}} = \sqrt{\dfrac{4 \times 0.200}{\pi \times 2}} = 0.3568$ m.

Say, therefore $d = 0.36$ m.

Calculation of total head loss:

Loss of head due to friction,

Now, $H_f = \dfrac{flv^2}{2gd} = \dfrac{0.03 \times 2000 \times 2^2}{2 \times 9.81 \times 0.36} = 33.978$.

Suction head, $H_s = 2.5$ m.

Delivery head, $H_l = 12.5$ m.

Total head, $H = 33.978 + 2.5 + 12.5 = 48.978 \cong 48.98$ m.

Therefore the power of pump $= \dfrac{QwH}{75\mu} = \dfrac{0.2 \times 1000 \times 48.98}{75 \times 0.8} = 163.27$.

Pump power $\cong 164$ HP.

Provide 41 HP Centrifugal Pumps of six numbers in that two numbers are standby at each pump station.

(e) A portion of Water-DSS1 C-Program for Karkala Treatment Plant Design

The unit processes manually designed above were coded in C-Language and fed into the in Code-Blocks 10.05 software. A portion of the program, for the population forecast, water demand, aeration unit design and underground clear water reservoir, is as shown below:

```
#include <stdio.h>
#include <stdlib.h>
#include <math.h>
int main()
{
float    wr,qty,len,vel,lpcd=100,det,cs,dep,sld,wid,fd,od,dose,alum1,alum2,fd2,dose2,fe,si,de,fl,vi,cs2,wi,den2,
ca,dep2,si2,ft,ca2,dep3,wi2,len2;
float sl,sa,len3,wi3,wl,den3,ca3,dep4,qty2,ss,fb,qty3,fa,sa2,s,ae,dep5,s2,stp,tre,dia2,dia3,ris,ris1, count1=0, max,
tim,qty4;
float dia4,x,y,total=0,Ig,pn,final_population,result,vel1,dis,hf,th,hp,p1;
int i,popu[125],d,j,n,year[125],p;
printf("\nFORECASTING POPULATION OF KARKALA\n");
printf("\nEnter the number of census:\n");
scanf("%d",&n);
for(i=0;i<n;i++)
{
printf("\nEnter the corresponding year:");
scanf("%d",&d);
year[i]=d;
printf("Enter the population in the year %d:",d);
scanf("%d",&popu[i]);
p=popu[i];
}
for(i=1;i<n;i++)
{
printf("\nIncrease in population in decade %d-%d:",year[i-1],year[i]);
printf("%d\n",popu[i]-popu[i-1]);
x=popu[i]-popu[i-1];
```

```c
y=x/popu[i-1]*100;
printf("Percentage increase in population of decade %d-%d:",year[i-1],year[i]);
printf("%0.2f percent\n",y);
total=total+y;
}
printf("\nTotal=%0.2f percent\n",total);
Ig=total/(n-1);
printf("Average per Decade=%0.2f percent\n",Ig);
final_population=p*pow((1+(Ig/100)),n);
printf("\nPopulation at the end of %d decades i.e. by the year 2041 is %0.2f",n-1,final_population);
result=final_population*pow(1+(Ig/100),0.2);
printf("\nTherefore Expected population of Karkala by the year 2043 is %0.2f\n",result);
printf("\nThe WATER DEMAND\n");
wr=(result*lpcd)/1000000;
printf("\nWater required of karkala per day=%f Million litres per day\n",wr);
printf("\nDESIGN OF THE AERATION TANK\n");
printf("\nEnter the number of steps\n");
scanf("%f",&stp);
printf("\nEnter the tread width in millimeters\n");
scanf("%f",&tre);
printf("\nEnter the diameter of the first step in meter\n");
scanf("%f",&dia2);
dia3=dia2;
for(i=1; i<=stp-1;i++)
{
printf("\nDiameter of the %d step =%f meters",i,dia3);
dia3=dia3+(2*(tre/1000));
}
printf("\nDiameter of the %d step =%f meters\n",i,dia3);
printf("\nDiameter of the aeration tank collector =%f meters\n",dia3+2*dia2);
printf("\nEnter the rise of the first step in millimeters\n");
scanf("%f",&ris);
ris1=ris/1000;
for(i=1;i<=stp-1;i++)
{
printf("\nRise of the %d step =%f meters",i,ris1);
count1=count1+ris1;
ris1=((ris1+0.100));
}
count1=count1+ris1;
printf("\nRise of the %d step =%f meters\n",i,ris1);
printf("\nThe overall of aeration tank of diameter %f meters and total height of casacade is %f me-ters",dia3+2*dia2,count1);
printf("\nDESIGN OF UNDERGROUND CLEAR WATER RESERVOIR\n");
printf("\nUnderground clear water reservoir having capacity of about 8 hours will be provided\n");
printf("\nEnter the depth in meters\n");
scanf("%f",&dep5);
ae=(wr*1000)/dep5;
printf("\nArea of the clear water resevoir =%f square meters\n",ae);
printf("\nProviding square clear water resevoir\n ");
s2=sqrt(ae);
printf("\nThe dimension of the clear water resevior is(%f*%f*%f) meters\n",s2,s2,dep5);
return 0;
}
```

3. Results and Discussions

(a) Results: A portion of the direct output values from the C-program is as presented here:
Population forecasting
Enter the corresponding year: 1971
Enter the population in the year 1971: 18593
Enter the corresponding year: 1981
Enter the population in the year 1981: 20713
Enter the corresponding year: 1991
Enter the population in the year 1991: 24109
Enter the corresponding year: 2001
Enter the population in the year 2001: 25116
Increase in population in decade 1971-1981: 2120
Percentage increase in population of decade 1971-1981: 11.40 percent
Increase in population in decade 1981-1991: 3396
Percentage increase in population of decade 1981-1991: 16.40 percent
Increase in population in decade 1991-2001: 1007
Percentage increase in population of decade 1991-2001: 4.18 percent
Total = 31.97 percent
Average per decade = 10.66 percent
Population at the end of 3 decades *i.e.* by the year 2041 is 37660.35
Therefore expected population of Karkala by the year 2043 is 38430.95
Water demand
Water required of Karkala per day=3.843095 million liters per day
Design of the aeration tank
Enter the number of steps 5
Enter the tread width in millimeters 250
Enter the diameter of the first step in meter 1
Diameter of the 1 step = 1.000000 meters
Diameter of the 2 step = 1.500000 meters
Diameter of the 3 step = 2.000000 meters
Diameter of the 4 step = 2.500000 meters
Diameter of the 5 step = 3.000000 meters
Diameter of the aeration tank collector = 5.000000 meters
Enter the rise of the first step in millimeters 300
Rise of the 1 step = 0.300000 meters
Rise of the 2 step = 0.400000 meters
Rise of the 3 step = 0.500000 meters
Rise of the 4 step = 0.600000 meters
Rise of the 5 step = 0.700000 meters
The overall of aeration tank of diameter 5.000000 meters and total height of casacade is 2.500000 meters
Design of underground clear water reservoir
Underground clear water reservoir having capacity of about 8 hours will be provided
Enter the depth in meters 5
Area of the clear water reservoir = 768.618896 square meters
Providing square clear water reservoir
The dimension of the clear water reservoir is (27.723976 × 27.723976 × 5.000000) meters
Process returned 0 (0 × 0) execution time: 318.415 s
Press any key to continue.

(b) Discussions: With the C-programming technique a decision support tool for design and process selection of drinking water treatment plant using conventional method has been developed and named WATER-DSS1. The tool assists in decision making on the process of drinking water treatment plant using conventional treatment methods. The process consists of pre-treatment, coagulation, flocculation, sedimentation, filtration and disinfection. The processes are selected based on the requirement to treat the raw water, chemically, physically

Table 2. Comparison of the manual and C-program output values.

S/N	Unit operation/Design criteria	Manual design values	C-Programming output values
1	Expected population	38430	38430.95
2	The water demand	3.85 MLD	3.843095 MLD
3	Aeration tank	Diameter of 5 m and total height of cascade 2.5 m	-
4	Plain Sedimentation tank	$64.8 \times 4.64 \times 4.5 \text{ m}^3$	$64.800003 \times 4.633360 \times 4.5 \text{ m}^3$
	Sedimentation aided with coagulants		
	i) Chemical feeding (size of solution tank)	$0.5 \times 0.5 \times 0.5 \text{ m}^3$	$0.468621 \times 0.468621 \times 0.5 \text{ m}^3$
5	ii) Approach channel	$0.175 \times 0.225 \text{ m}^2$	$0.166734 \times 0.216734 \text{ m}^2$
	iii) Mixing tank	$1 \times 1 \times 1 \text{ m}^3$	$0.816826 \times 0.816826 \times 1 \text{ m}^3$
	iv) Flocculating tank	$10 \times 1.4 \times 1.6 \text{ m}^3$	$10 \times 1.45100\ 7\times 1.6 \text{ m}^3$
	v) Settling tank (rectangular)	$6 \times 3.3 \times 3 \text{ m}^3$	$6 \times 3.336020 \times 3 \text{ m}^3$
6	Rapid gravity filter	$6.5 \times 6.5 \text{ m}^2$	$6.394058 \times 6.394058 \text{ m}^2$
7	Chlorination plant	Liquid chlorinator having capacity of 0.1 to 5 kg/m	-
8	Underground clear water reservoir	$27.75 \times 27.75 \times 5 \text{ m}^3$	$27.7239 \times 27.7239 \times 5 \text{ m}^3$
9	Horse power of centrifugal pump	41 HP	41.0889 HP

and microbiologically. Each parameters of water has its own treatment procedure but often these can be combined.

In validating the developed program, required data was keyed in and run. At the same time, manual computations are done using the conventional method for the designing the different units of the water treatment plant. The output values of the C-program as compared with those of manual design are presented in **Table 2**. Meanwhile, if the user desires to get the design of any particular unit of the water treatment plant, it is possible to access the desired unit's design using the "*switch case*" statement. This flexibility further confirms the user-friendliness of C-programming Language.

In comparing the C-program output values and the manually designed values only marginal differences were observed, especially in the decimal places. It is so, because in the c-programming "*float*" data type is used which gives the accurate values up to six decimal points whereas in manual design the values are rounded off to two decimal points.

4. Conclusion

In this paper with the C-programming technique, a decision support tool for design and process selection of drinking water treatment plant using conventional method has been developed and named Water-DSS1. The applied C-program is user friendly, saves time and gives more accurate values. The program is much more efficient and reliable than the manual design and can be used repeatedly for different sets of data. It is universal in its approach and easily adaptable to any similar conventional water treatment plant apart from the Karkala one reported in this paper. Water-DSS1 is therefore recommended for general use in alleviating water supply challenges.

References

[1] Power, D.J. (1997) What Is DSS? DSstar. *The Online Executive Journal for Data-Intensive Decision Support*, **2**, 15-20.

[2] Gorry, G.A. and Scott Morton, M.S. (1971) A Framework for Management Information Systems. *Sloan Management Review*, **13**, 55-70.

[3] Kanetkar, Y.P. (2013) Let Us C. 13th Edition, BPB Publications, New Delhi.

[4] Mahaganesha, P.V., Thippeswamy, M.R., Anand, R. and Sharath, B.P. (2014) Design of Conventional Water Treat-

ment PLANT for Karkala Town Using C-Programming. B.E Project Report, Department of Civil Engineering, NMAM Institute of Technology, Nitte.

[5] Ojoawo, S.O. (1997) Performance Evaluation of the Ogbomoso Waterworks. B.Tech Project Report Submitted to the Department of Civil Engineering, Ladoke Akintola University of Technology, Ogbomoso, 3.

[6] Hung, C.K. (2006) Development of a Decision Support System for Drinking Water Treatment Process Design (WATER-DSS). M.E Project Report Submitted to the Faculty of Civil Engineering, Universiti Teknologi Malaysia, 32-35.

[7] Garg, S.K. (2004) Water Supply Engineering. 18th Edition, Khanna Publishers, Delhi.

[8] Crittenden, J., Trussell, R., Hand, D., Howe, K. and Tchobanoglous, G. (2005) Water Treatment: Principles and Design. John Wiley and Sons, New York.

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