



# Maximizing Disinfection Reactor Ct via Integration of Chlorine Demand and Decay

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# **Presentation Summary**

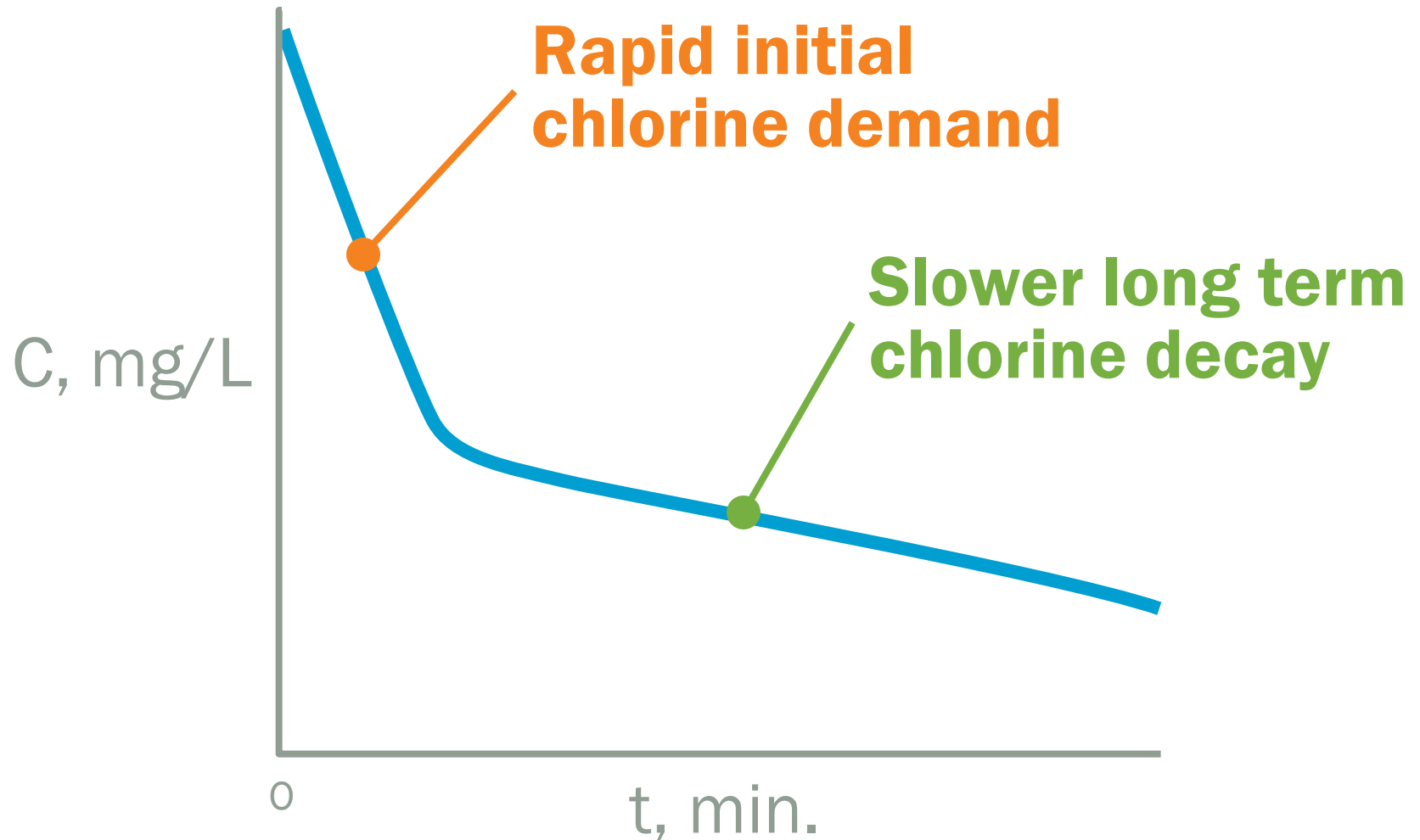
## **Free Chlorine Ct Computations**

- Present Reactor Ct Computations
- Suggested Integration Method for Ct
- Two-stage Algorithm for Predicting CDD
- Integration of CDD Algorithm
- Application of CDD Algorithm Integration

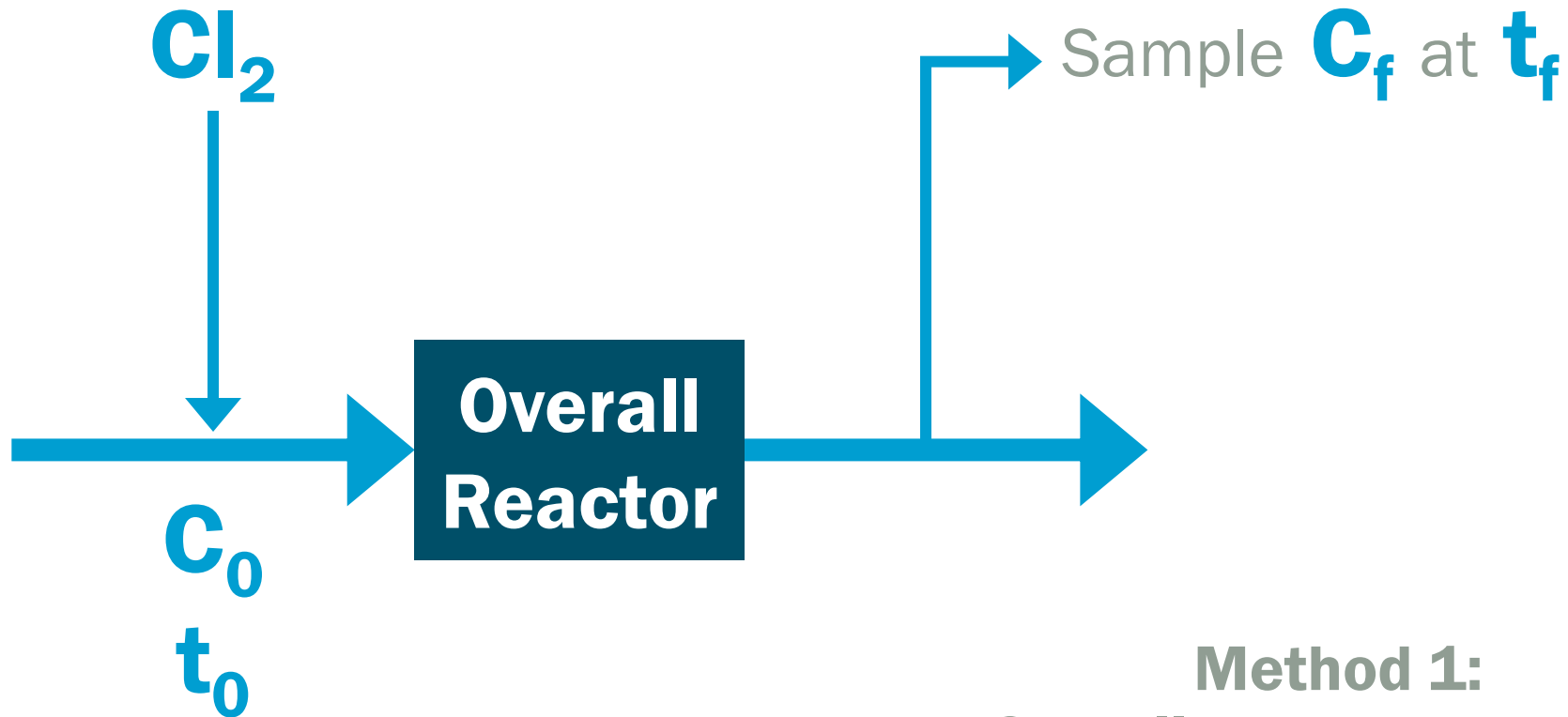
# Importance of Ct Computations

- Protect Water Quality
  - Pathogen inactivation
  - DBP Minimization
- Assure compliance with disinfection regulations
- Meet regular reporting requirements

# Typical CDD Profile

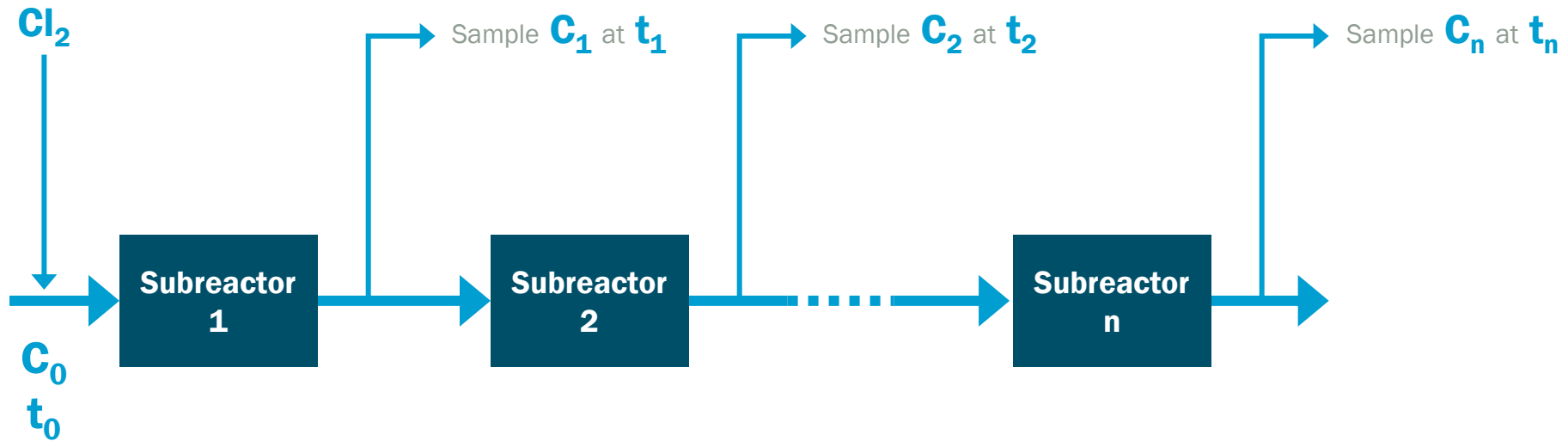


# Two Existing Simple Methods to Compute Ct



**Method 1:**  
Overall reactor sampling  
 $Ct = C_f \times t_f$

# Two Existing Simple Methods to Compute Ct



**Method 2:**  
Intermediate reactor sampling

$$Ct = \sum_{j=1}^{j=n} C_j(t_j - t_{j-1})$$



# Existing methods

- Only accounts for reactor discharge concentration
- Ignores added value of CDD within reactor



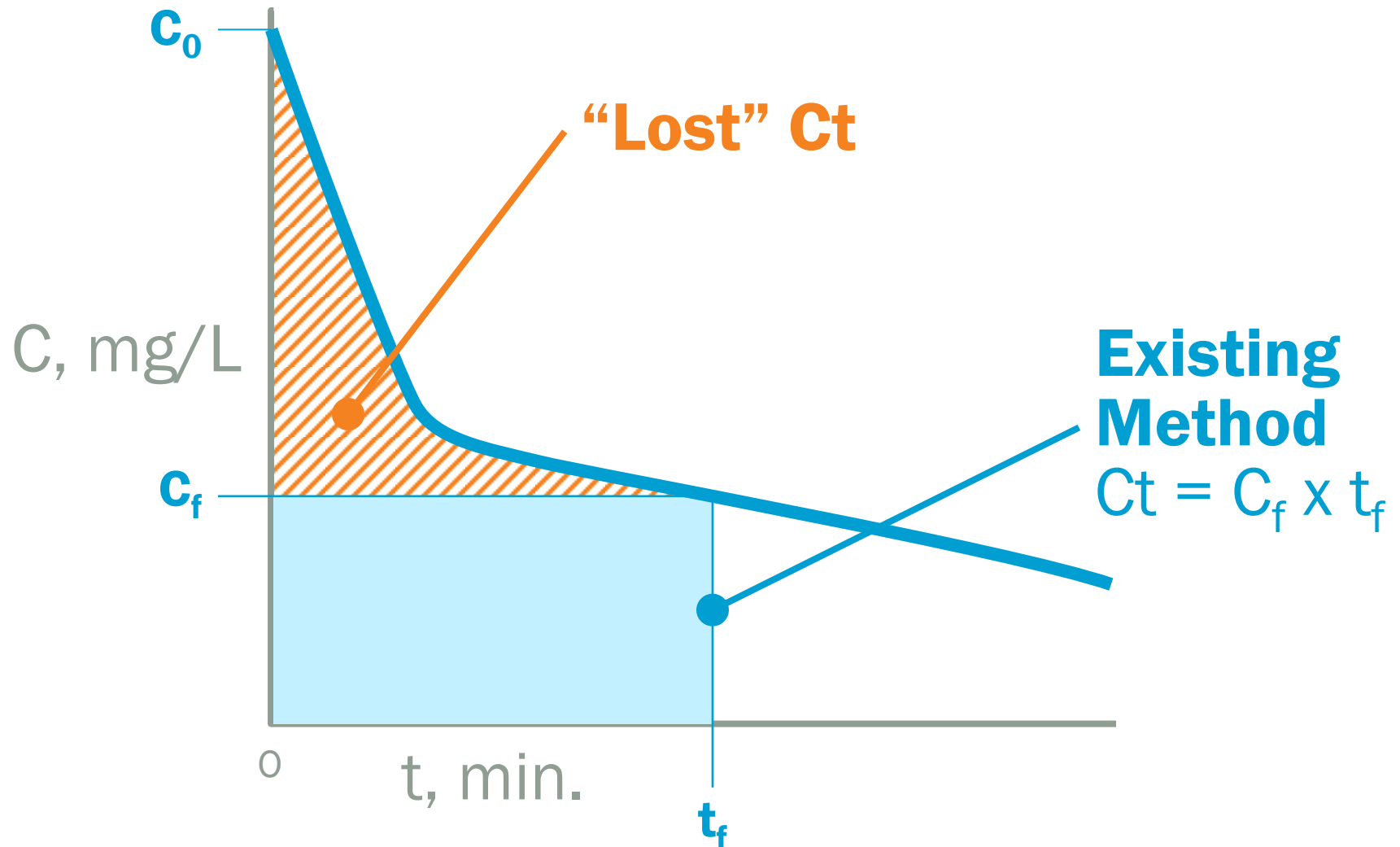
Is there a better way?

**Yes!**

# New Method

- Mathematical model for CDD
- Integrate model
- Account for “lost” Ct value
- Helps when available Ct is “tight” or water is reactive

# Existing Method vs. New



# CDD Algorithms


General form to predict C versus t

$$C = f \left( \begin{array}{l} \text{time, temp, DOC, pH,} \\ \text{oxidizable substances, others} \end{array} \right)$$

# CDD Algorithms

The most basic, simplified form

Where **k** is a rate constant

$$C = C_0 e^{-kt}$$


# CDD Algorithms

A more elaborate and accurate form

**A**


proportionality constant between  
rapid demand and slow decay

**k**

rate coefficient for  
rapid initial demand

**l**

rate coefficient for  
slower long term decay


$$C = C_0 A e^{-k t} + C_0 (1 - A) e^{-l t}$$

For short term applications,  
can set  $A = 1$  and ignore 2nd term

# Yet Another Algorithm Twist

Rate constants vary with temperature!

Higher temperatures increase CDD

- Use Arrhenius Law and van't Hoff equation

$$d(\ln k)/dT = \Delta H^0 / (R_g T^2)$$

$\Delta H^0 = 15,048 \text{ cal/gm-mole}$ ;  $R_g = 1.987 \text{ cal/}^\circ\text{K-gm-mole}$   
Std. State Enthalpy Change

$$k = k_s \text{EXP}[\Delta H^0 / (R_g T_s)] \text{EXP}[- \Delta H^0 / (R_g T)] \quad \text{eq. 2}$$

$$C = C_0 A e^{-k t} + C_0 (1-A) e^{-I t}$$

$$I = I_s \text{EXP}[\Delta H^0 / (R_g T_s)] \text{EXP}[- \Delta H^0 / (R_g T)] \quad \text{eq. 3}$$

The background of the image is a clear, vibrant blue sky filled with numerous small, fluffy white clouds of varying sizes. The clouds are scattered across the frame, with some appearing more prominent than others. The overall mood is bright and positive.

Scare you?

**It's not so bad!**



Combine equations

1, 2, and 3.

It's simple to  
integrate, right?

**Not so fast!**

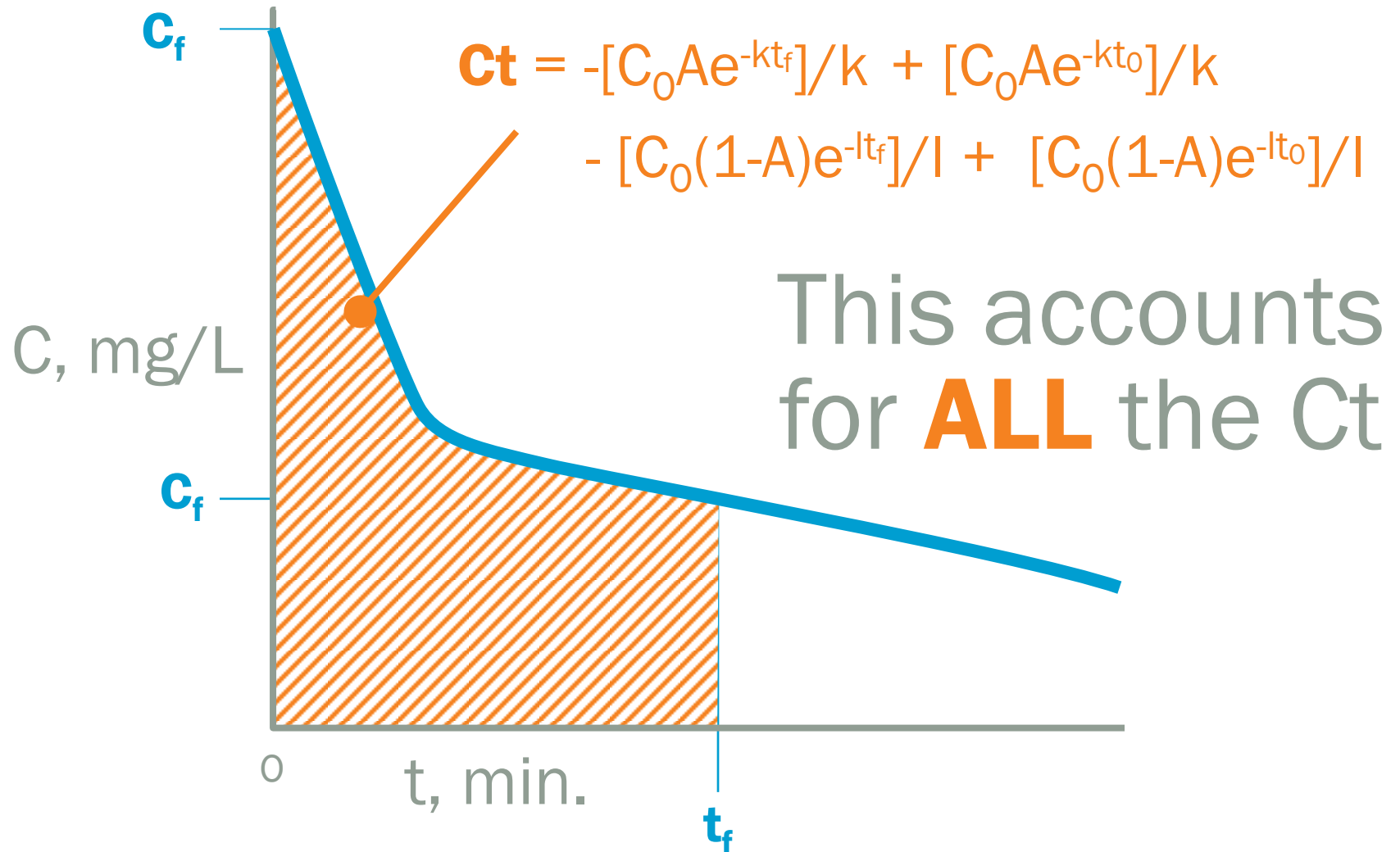
# CDD Integration for Constant Temperature

$$C_t = \int C dt$$

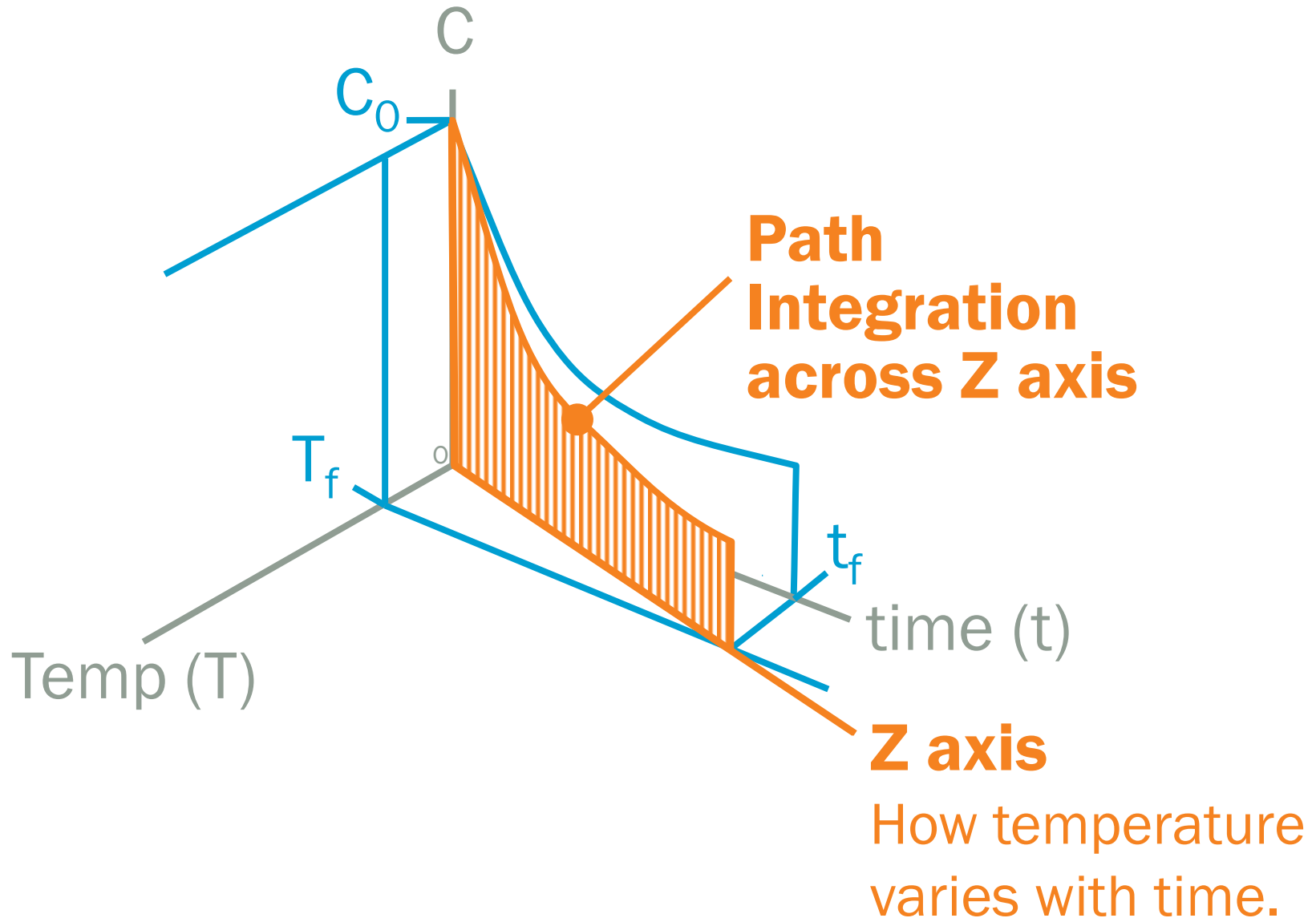
$$C_t = \int_{t=t_0}^{t=t_f} C_0 [Ae^{-kt} + (1-A)e^{-lt}] dt$$

- Analytical integration works at constant temperature
- Not true for varying temperature

# CDD Integration for Constant Temperature

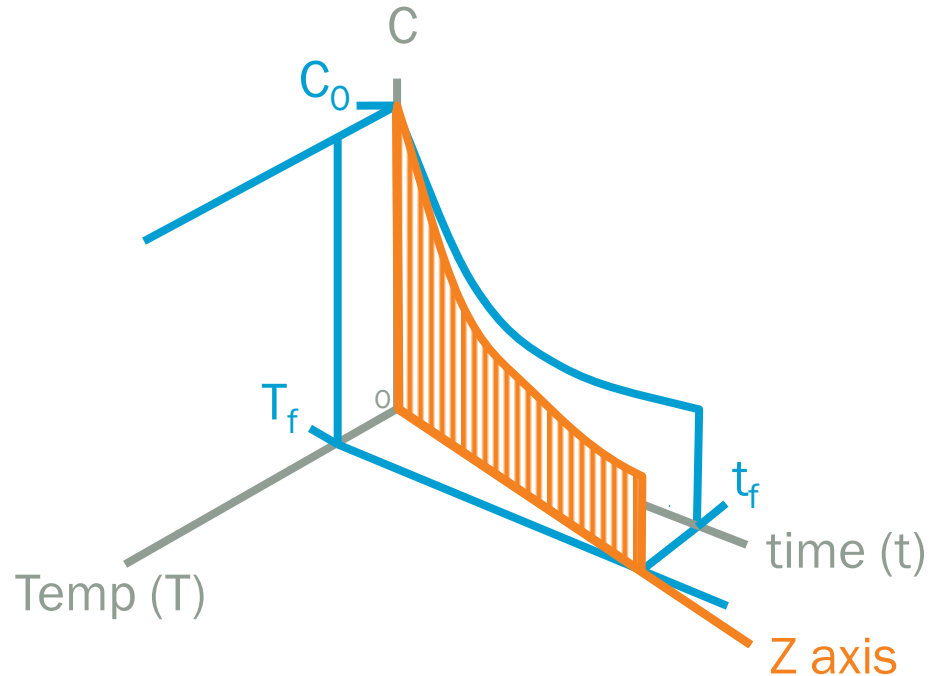


# CDD Varies with Time and Temperature



# Integration for Varying Temperature

- For simplicity, assume  $T = \text{linear } f(t)$
- Re-express  $T$  and  $t$  in equations 1, 2, and 3 in terms of  $Z$
- *Cannot integrate analytically*
- Resort to numerical integration
  - Use Simpson's Rule
  - Slice curve into numerous parabolic segments
  - Add up segment areas under the curve



**Now what?**

# Next Steps

- Perform lab test to measure CDD constants
- Apply math
  - There's a free App for that!
- When to apply this method?
- Will regulators accept this method?

# Example Computations

## NW City “X” WTP

### Existing Method

#### GIVEN:

- 1.0 log inactivation credit via disinfection (direct filtration)
- Clearwell Volume: 325,000 gallons
- $t_{10}/t = 0.51$
- Flow = 8.4 mgd (5,833 gpm)
- pH = 7.8
- Temperature  $T_0 = 19^\circ\text{C}$  (292° K)
- Temperature  $T_f = 20^\circ\text{C}$  (293° K)
- $C_f = 0.8$  mg/L as  $\text{Cl}_2$

### Integration Method

#### GIVEN:

- Same clearwell conditions
- $A = 0.314$
- $k_s = 0.0163 \text{ min}^{-1}$
- $I_s = 0.00017 \text{ min}^{-1}$
- $T_s = 292^\circ\text{K} = 19^\circ\text{C}$

*Empirical values determined from City “X” CDD Study*



# Example Computations

## NW City “X” WTP

### Existing Method

- $t_f = (325,000)(0.51)/5,833$   
= 28.4 minutes
- $C_t (\text{available}) = C_f \times t_f = (0.8)(28.4) =$   
**22.7** mg-min/L
- $C_t (\text{required}) = 24.4$  mg-min/L from  
Ct tables for 1.0 log inactivation
- **Log inactivation achieved =**  
**22.7/24.4 = 0.9**
- Just barely miss the inactivation target
- Causes City “X” to prechlorinate for added  $C_t$
- This practice aggravates DBPs

### Integration Method

- $t_f = (325,000)(0.51)/5,833$   
= 28.4 minutes
- $C_t (\text{available}) =$  **24.4** mg-min/L
- $C_t (\text{required}) = 24.4$  mg-min/L from  
Ct tables for 1.0 log inactivation
- **Log inactivation achieved =**  
**24.4/24.4 = 1.00**
- Improvement in log inactivation  
over traditional method > 7%
- Improvement may be small, but  
important in some circumstances
- In this case...  
**no need to prechlorinate!**

# Summary

- Account for **ALL** reactor Ct, not just discharge value
- Determine CDD reaction variables
- Integrate CDD operating equations
- More useful for reactive waters
- Optimize disinfection reactor performance
  - Use less chlorine
  - Reduce disinfection byproducts

Spend same time  
on the math...

**with better  
results!**



# Questions?

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