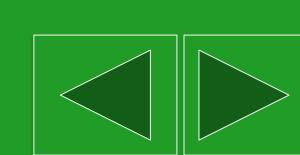
Riyansh Karani - UIC, Akshay Uppal - UIC, & David Amirbekyan - RPI





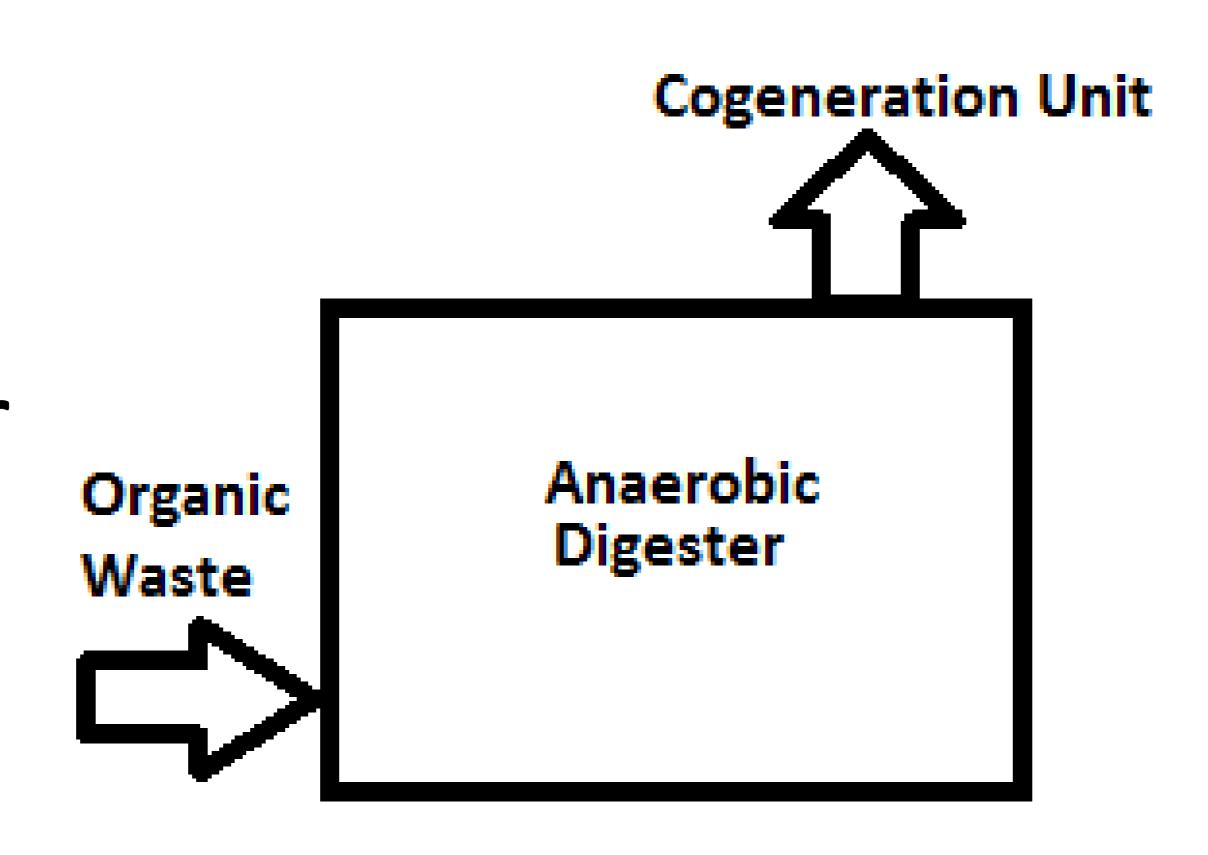


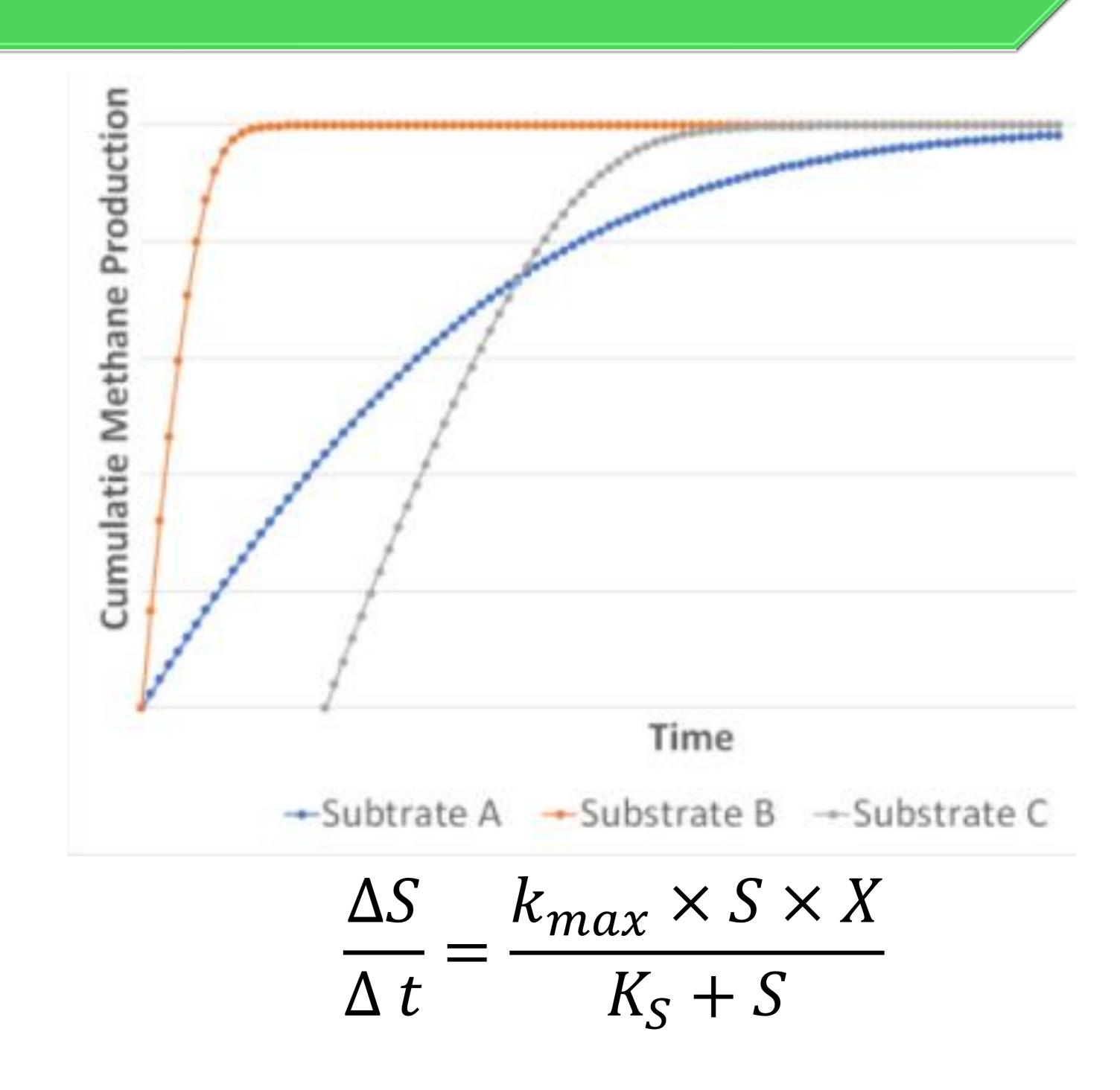
Riyansh Karani – UIC, Akshay Uppal - UIC, & David Amirbekyan - RPI



#### Anaerobic Digestion Introduction

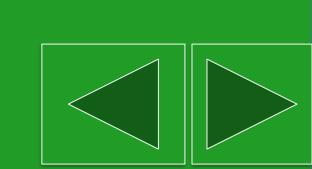
- •Biogas is produced in an anaerobic digester from the fermentation of organic waste
- ·Biogas can be combusted to produce energy
- PurposeEnergy, Inc.
   provided solution to
   a brewery in VT
   saving \$0.7MM / year







Riyansh Karani – UIC, Akshay Uppal - UIC, & David Amirbekyan - RPI

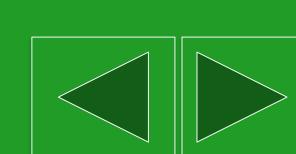


#### Problem statement

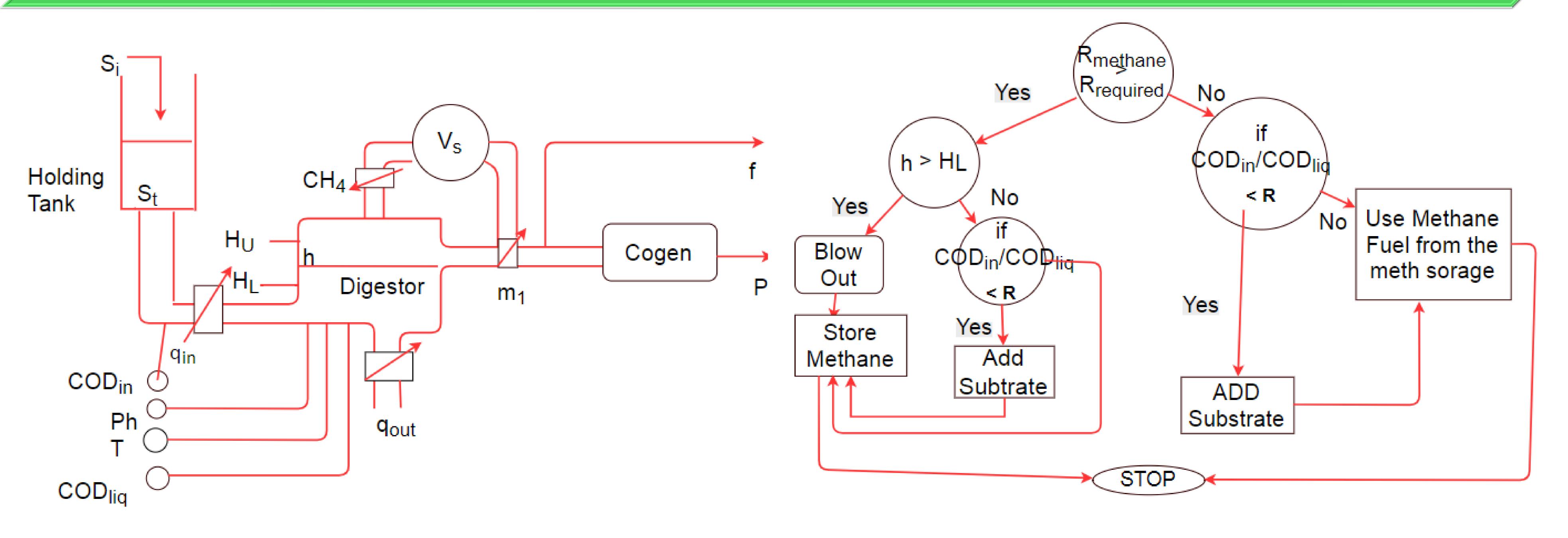
Assuming no prior knowledge of the nature of the imported substrate and using low-cost, commercially available instrumentation, develop a flow control algorithm in pseudocode that controls substrate addition at a rate that "tops off" the CHP power output (i.e. generates just enough biogas to maximize the output of the CHP).



Riyansh Karani – UIC, Akshay Uppal - UIC, & David Amirbekyan - RPI

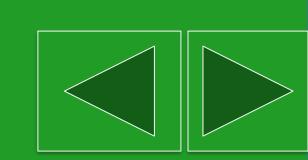


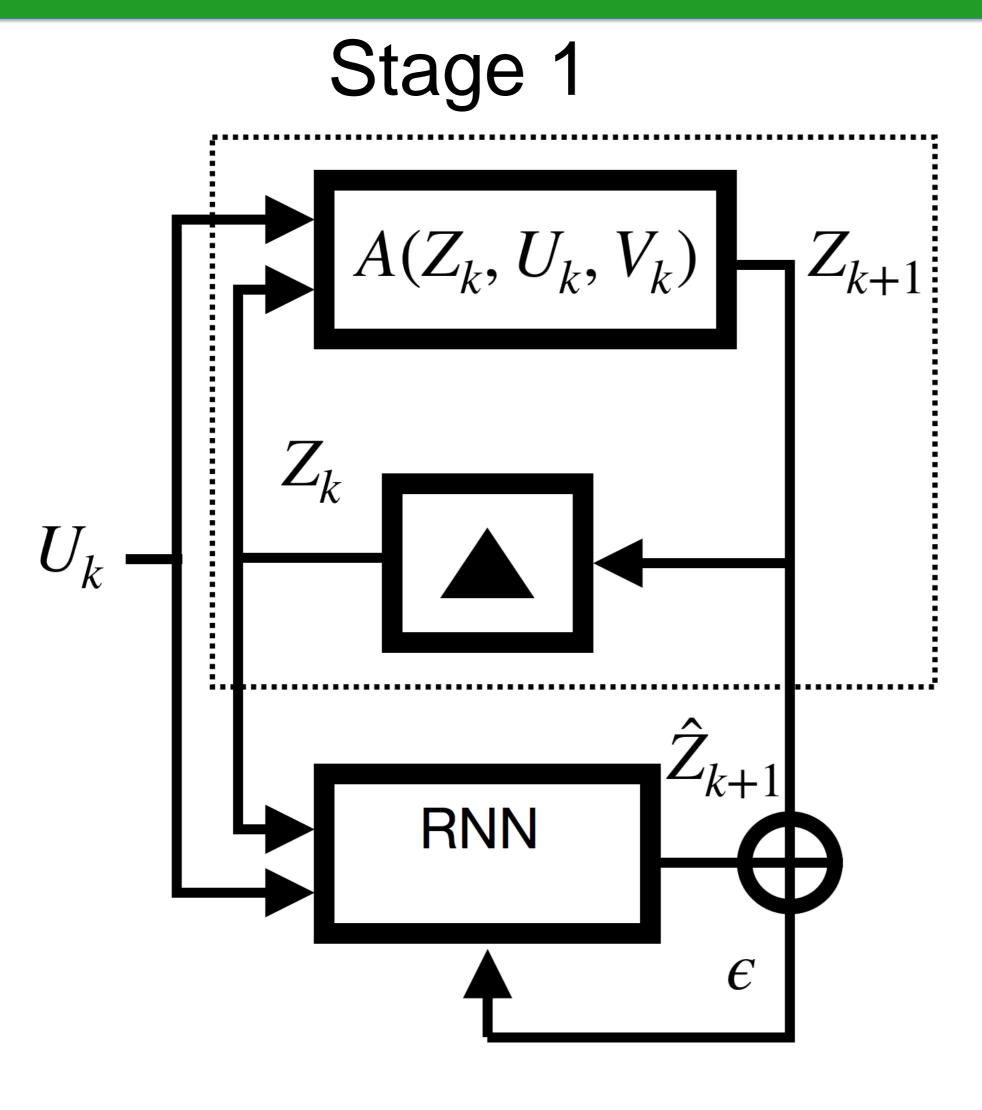
#### Process Flow and Decision Tree





Riyansh Karani – UIC, Akshay Uppal - UIC, & David Amirbekyan - RPI



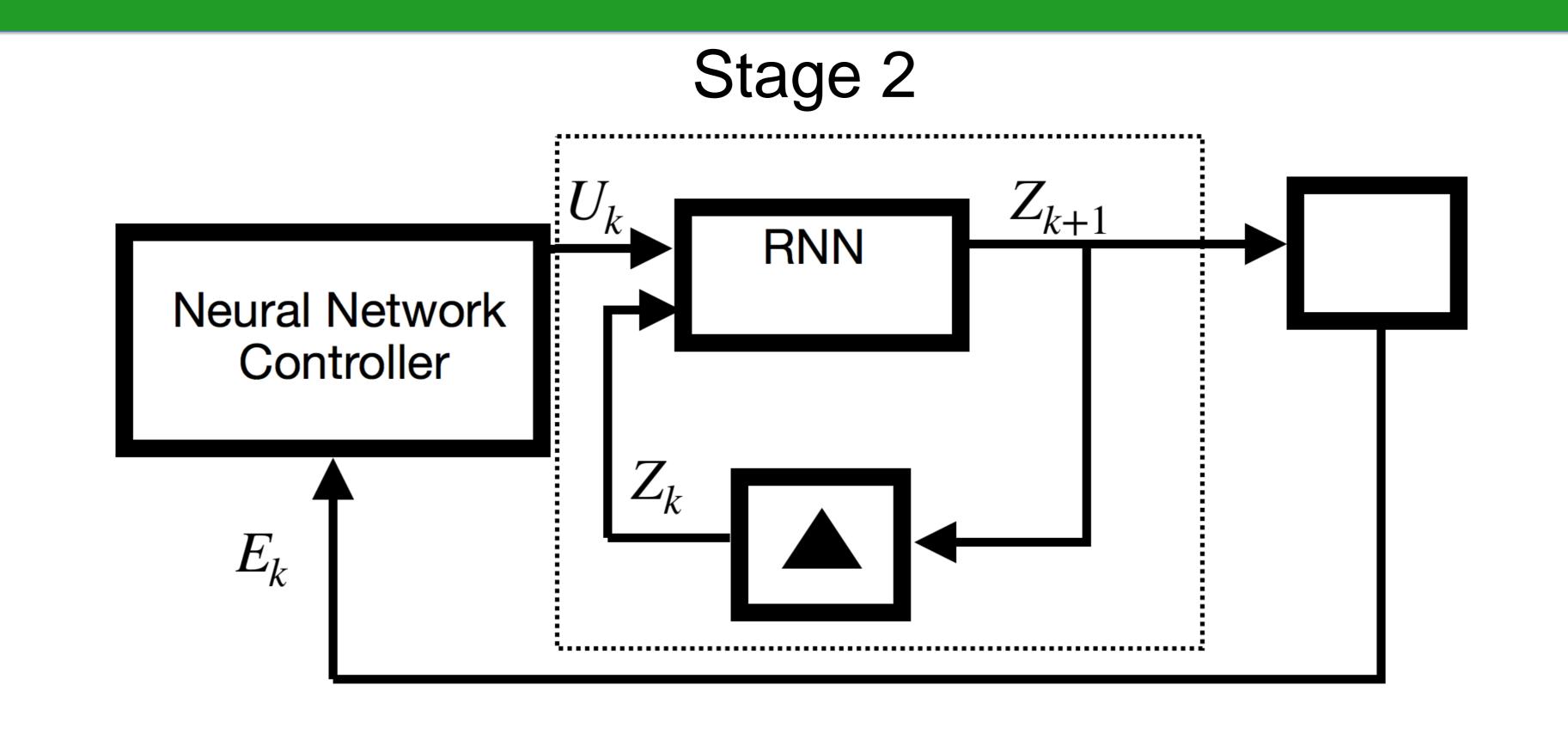


$$U_k = \{Ph_k, T_k, q_{in_k}, q_{out_k}, m_{1_k}\}$$

$$V_k = \{COD_{in_k}, COD_{liq_k}, Meth_k\}$$

$$Z_k = \{P_k, f_k, h_k, V_{s_k}\}$$

$$E = \sum_{k} (z_k - \hat{z}_k)^2 \, \forall z_k \in Z_k$$



$$E_1(h) = \frac{1}{1 + e^{a(h+h_{low})}} + \frac{1}{1 + e^{-a(h-h_{high})}}$$

$$E_2(V_{store}) = e^{b(V_s - V_{smax})}$$

$$E_3(f) = f$$

$$E_4(P) = \frac{1}{1+P}$$

to make sure liquid level in digestion tank is within acceptable limits

to make sure gas tank is not overflown

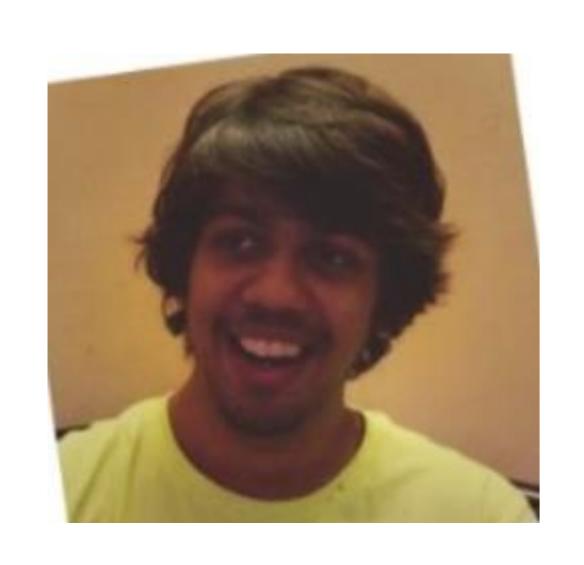
to minimize flaring

to maximize power

$$E = \sum_{k} c1 \cdot E_1(h_k) + c2 \cdot E_2(V_{store_k}) + c3 \cdot E_3(f_k) + c4 \cdot E_4(P_k)$$

#### INAM = It's Not About Me







Computer Science

University of Illinois at Chicago M.S. Computer Science `19



Akshay Uppal

Computer Science

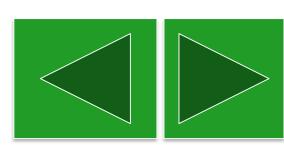
University of Illinois at Chicago M.S. Computer Science `19



David Amirbekyan

Chemical Engineer

Rensselaer Polytechnic Institute`09 Working in water treatment industry with process analyzer experience.



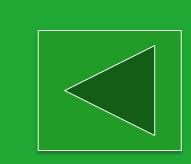
## Appendix

[1] Batstone, D.J.; Keller, J; Angelidaki, I.; Kalyuzhnyi, S.V.; Pavlostathis, S.G.; Rozzi, A.; Sanders, W.T.M.; Siegrist, H.; Vavilin, V.A. 2002. The IWA Anaerobic Digestion Model No 1 (ADM1). Water Science and Technology. 45(10):65-73.

[2] Borja, R.; Martín, A.; Rincón, B.; Raposo, F. 2003. Kinetics for Substrate Utilization and Methane Production during the Mesophilic Anerobic Digestion of Two Phases Olive Pomace (TOPO). Journal of Agriculture and Food Chemistry. 51(11):3390-3395.

[3] Nauman, E.B. 2008. Chemical Reactor Design, Optimization, and Scaleup. 2<sup>nd</sup> Edition. New York: John Wiley & Sons, Inc.



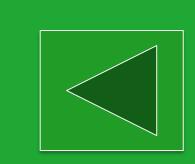


## Appendix

[4] Nguyen, D.H.; Widrow, Bernard. 1990. Neural Networks for Self-Learning Control Systems. IEEE Control Systems Magazine. 10(3):18-23.

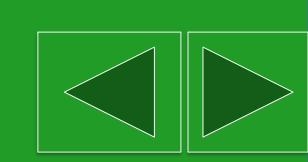
[5] Fitch, E.; Kshetry, H. 2017. Purpose Energy: Robust Anaerobic Digestion. Presented at: 2017 MIT Energy Hackathon; Cambridge, MA.







Riyansh Karani – UIC, Akshay Uppal - UIC, & David Amirbekyan - RPI



#### Online Process Analyzer Examples and Sampling

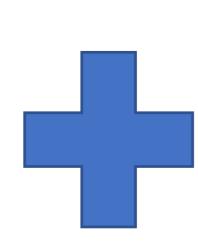


COD Analyzers

LAR Process Analysis AG



CH<sub>4</sub> Analyzer ABB



Proper Sampling and Conditioning System