

# Liquid Cooling of Heat Sink

ME 334- Heat and Mass Transfer

**Group - L**

**Presented by**

Kommanapalli  
Hemanth  
(23110170)

Korada Kusal  
Sai Charan  
(23110171)

Pilla Karthik  
Naidu  
(23110246)

# Problem Statement

- A copper base plate with a rectangular cooling channel receives heat from a square heat source.
- Water enters the channel at a known temperature and different velocities.
- Fins of fixed height are added above the heat source in configurations of 1, 4, 9, and 16 fins (1 cm spacing) to enhance cooling.
- Our Goal is to Predict and simulate how fin count and inlet velocity affect solid temperature and overall heat transfer.

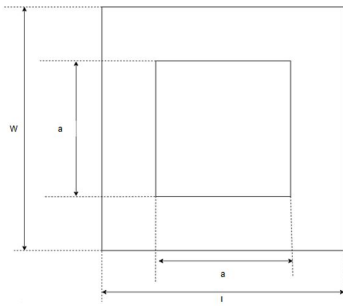
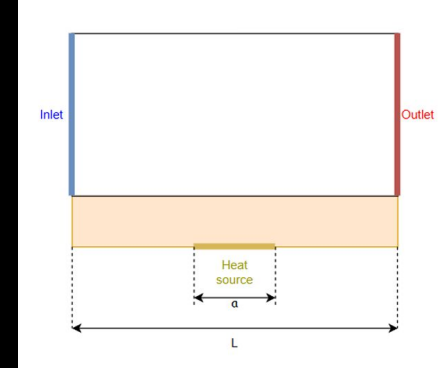


Figure 2

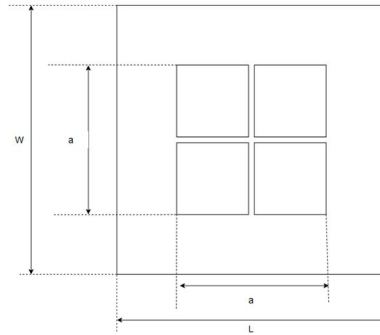


Figure 3

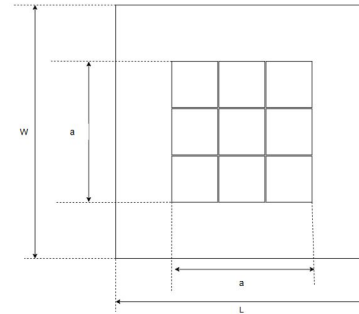


Figure 4

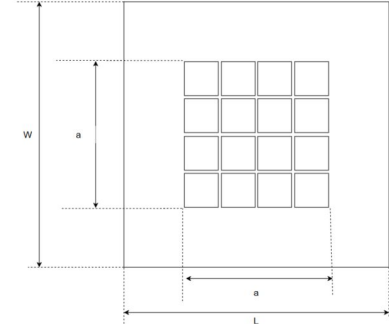


Figure 5

# Formulae Used in Our Analysis

## Assumptions (Same Theory for All Cases)

- Steady-state heat transfer
- One-dimensional conduction along fin length
- Uniform fin cross-section
- Constant material properties ( $k$ ,  $h$ )
- Convection along fin surface **and tip**
- Temperature excess:  $\theta = T - T_\infty$

Governing Fin Equation (Same for All 1,4,9,16 fin cases)

$$\frac{d^2\theta}{dx^2} - m^2\theta = 0$$

$$m^2 = \frac{hP}{kA_c}$$

## Energy Balance on Fin Element

Conduction in = Conduction out + Convection loss

$$\Rightarrow \frac{d^2\theta}{dx^2} - \frac{hP}{kA_c}\theta = 0$$

## Boundary Conditions

- Base:  $\theta(0) = T_b - T_\infty$
- Tip:  $-kA_c \frac{d\theta}{dx} \Big|_{x=L} = hA_c\theta(L)$

# Temperature Profile & Mean Temperature (Using Same Theory for n Fins)

## Temperature Profile

$$\frac{\theta(x)}{\theta_b} = \frac{\cosh[m(L-x)] + \left(\frac{h}{mk}\right) \sinh[m(L-x)]}{\cosh(mL) + \left(\frac{h}{mk}\right) \sinh(mL)}$$

## Mean Fin Temperature

$$\bar{\theta} = \frac{1}{L} \int_0^L \theta(x) dx$$

$$\bar{T} = T_\infty + (T_b - T_\infty) \frac{\sinh(mL) + \left(\frac{h}{mk}\right) (\cosh(mL) - 1)}{mL \left[ \cosh(mL) + \left(\frac{h}{mk}\right) \sinh(mL) \right]}$$

## How Geometry Enters for n Sub-Fins

When one fin is split into  $n$  fins:

$$A_c \rightarrow \frac{A_c}{n}, \quad P \rightarrow \frac{P}{\sqrt{n}}$$

So the fin parameter becomes:

$$m_n^2 = \frac{h(P/\sqrt{n})}{k(A_c/n)} = m^2 \sqrt{n}$$

The formula stays the same, we only substitute the new  $m_n$ .

# No Fin Case:

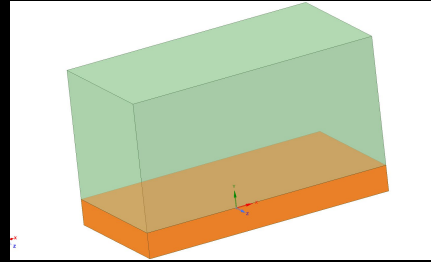
Mandatory Results (i)

Maximum temperature: 777.82 K

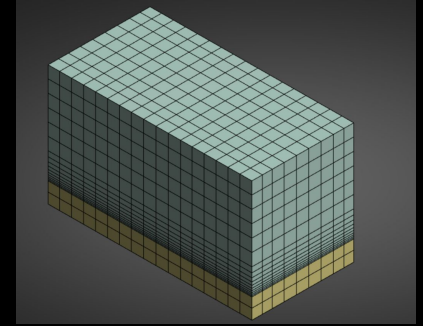
Solid average temperature : 592.36 K

Fluid average temperature: 300.9 K

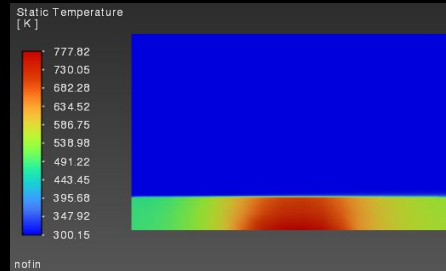
Surface heat transfer coefficient: 314.87992 W/m<sup>2</sup>-K



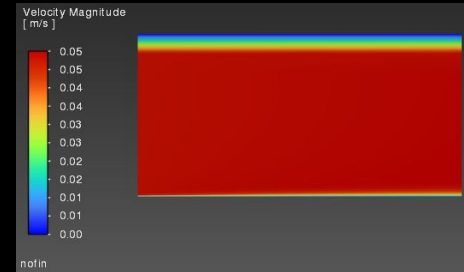
Geometry



Mesh

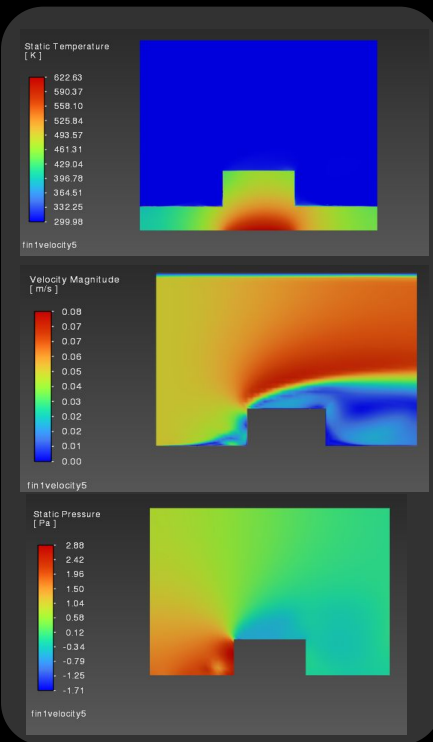


Temperature Distribution



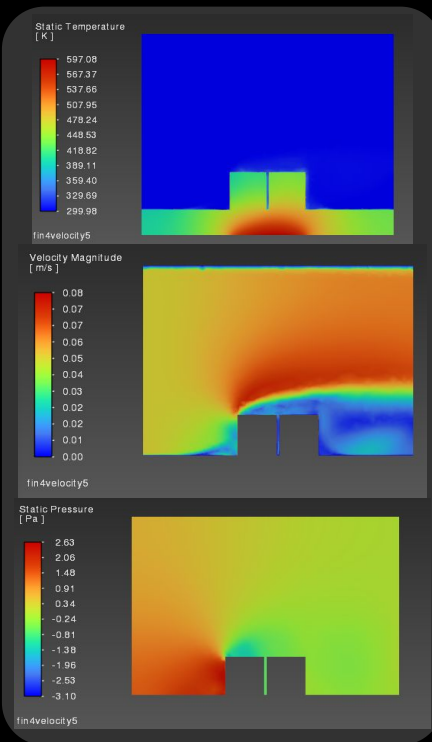
Velocity Distribution

Inlet Velocity : 5 cm/s ,  $T_{inlet} = 300K$



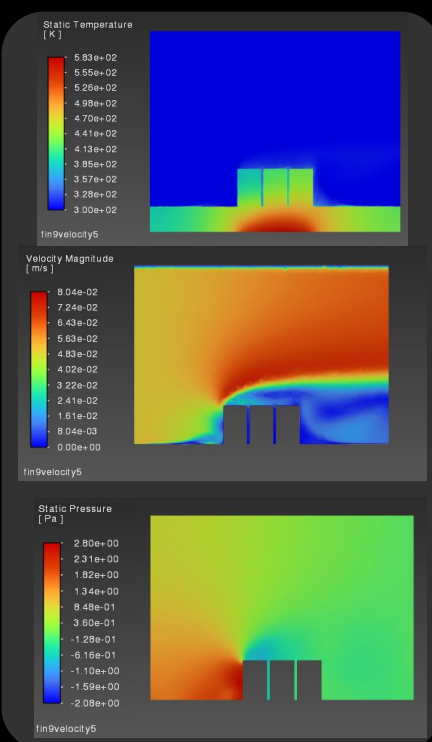
Single Fin

$T_{outlet} = 301.08 K$



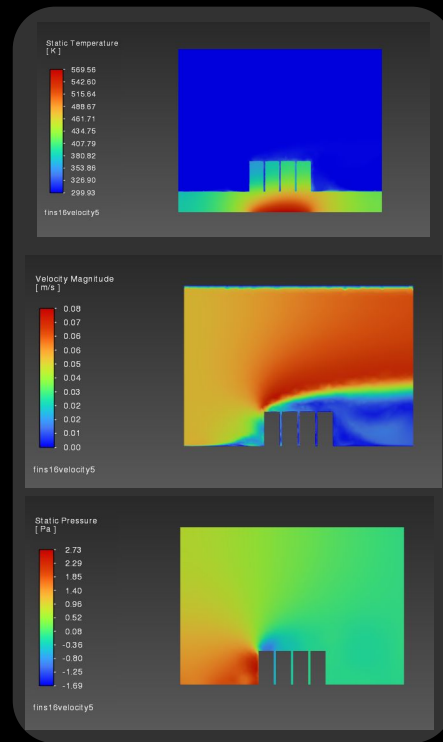
4 Fins

$T_{outlet} = 301.085 K$



9 Fins

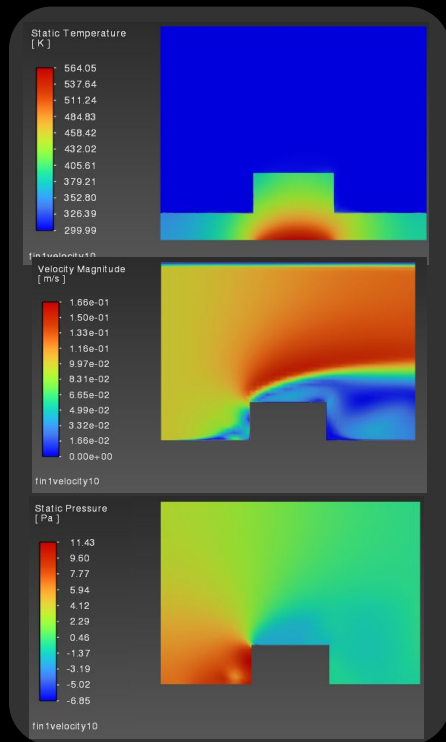
$T_{outlet} = 301.16$



16 Fins

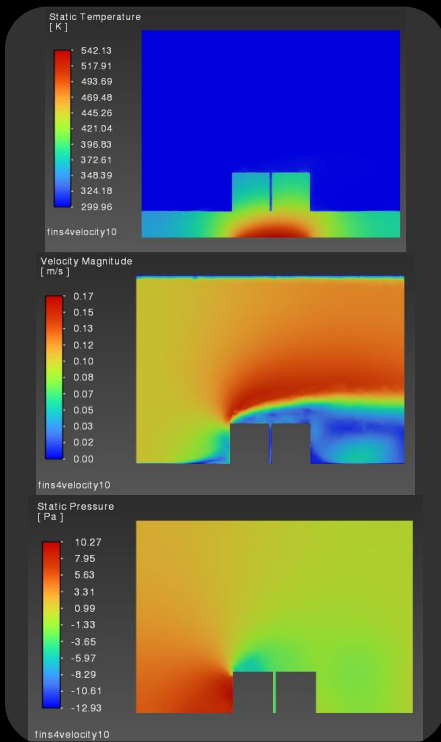
$T_{outlet} = 301.177 K$

Inlet Velocity : 10 cm/s



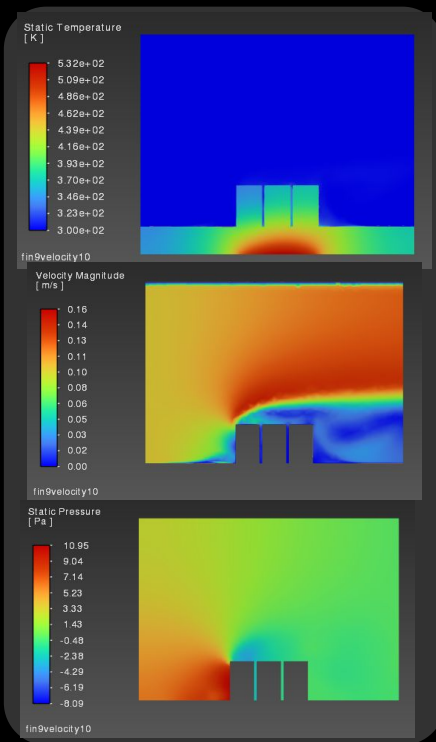
Single Fin

$T_{\text{outlet}} = 300.54 \text{ K}$



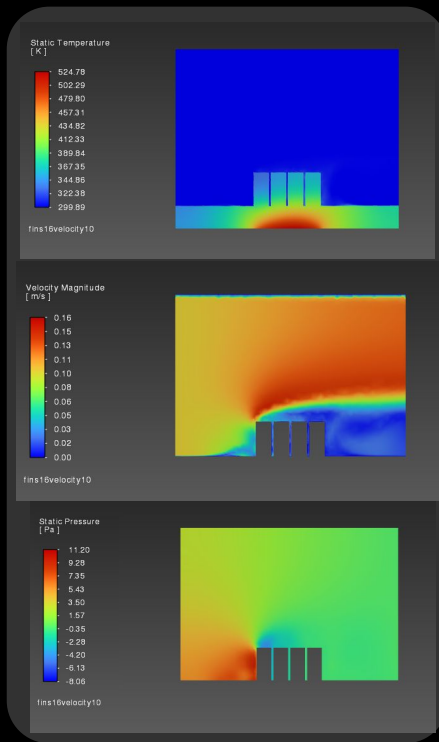
4 Fins

$T_{\text{outlet}} = 300.57 \text{ K}$



9 Fins

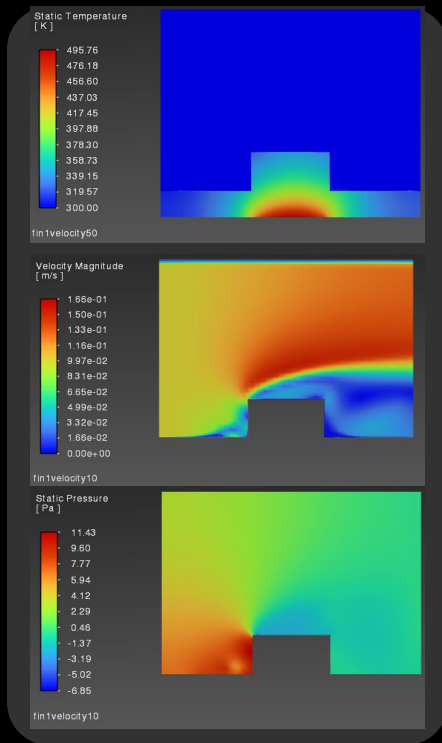
$T_{\text{outlet}} = 300.58 \text{ K}$



16 Fins

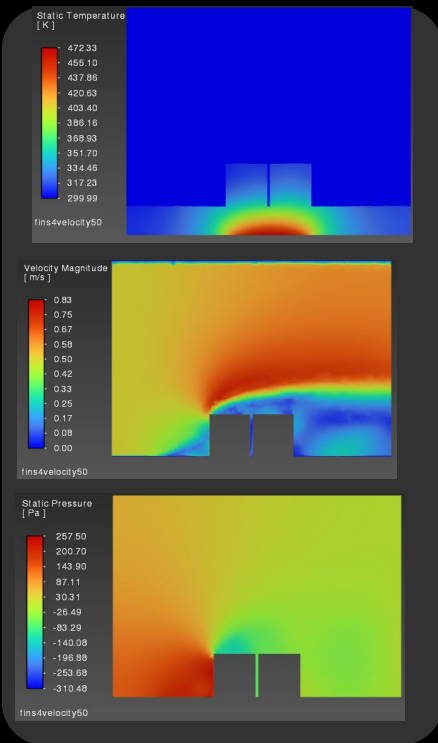
$T_{\text{outlet}} = 300.59 \text{ K}$

Inlet Velocity : 50 cm/s



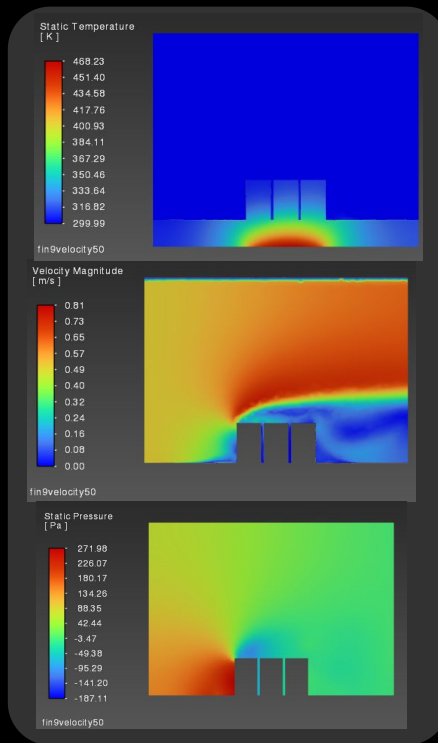
Single Fin

$T_{\text{outlet}} = 300.09 \text{ K}$



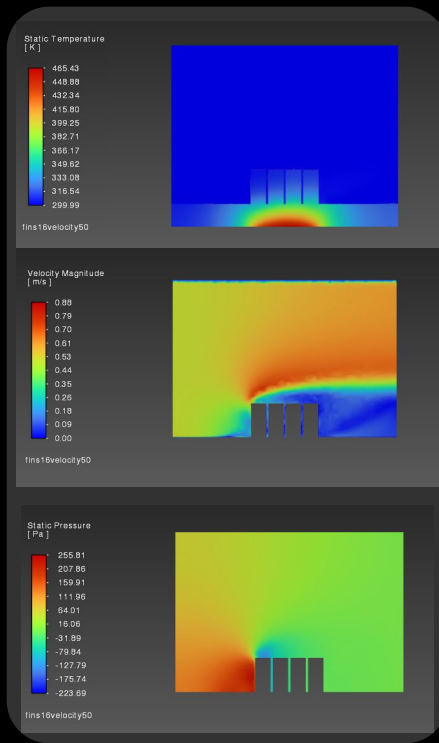
4 Fins

$T_{\text{outlet}} = 300.116 \text{ K}$



9 Fins

$T_{\text{outlet}} = 300.117 \text{ K}$

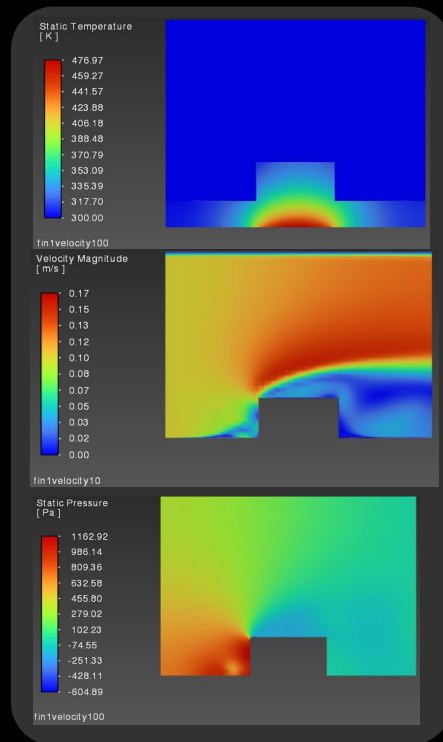


16 Fins

$T_{\text{outlet}} = 300.123 \text{ K}$

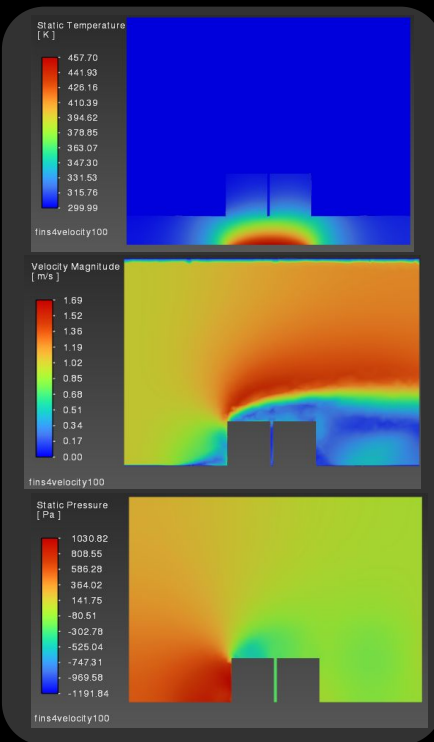


Inlet Velocity : 100 cm/s



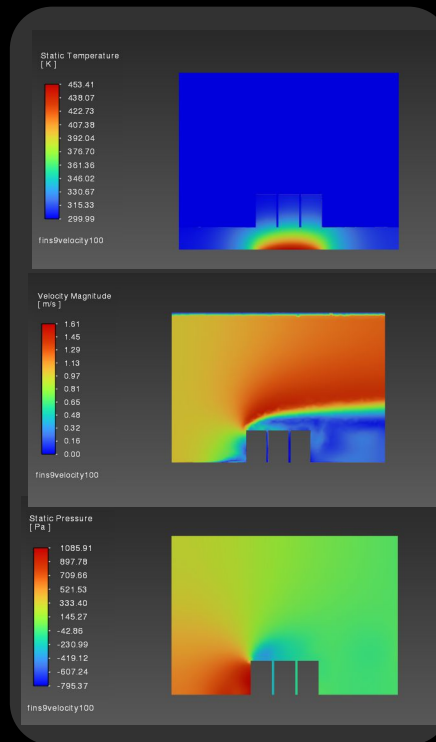
Single Fin

$T_{\text{outlet}} = 300.049 \text{ K}$



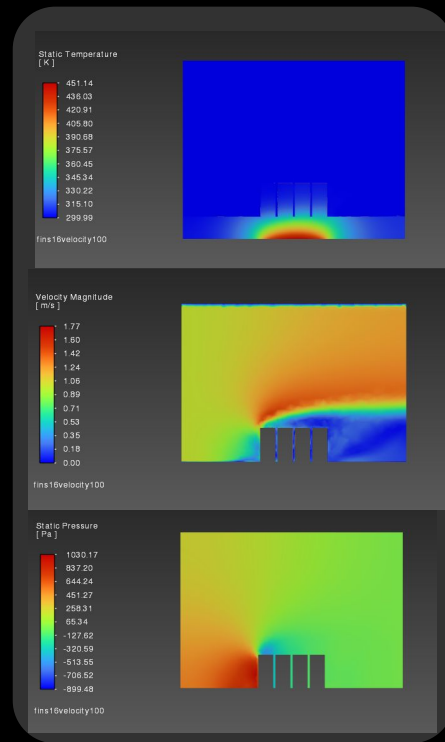
4 Fins

$T_{\text{outlet}} = 300.063 \text{ K}$



9 Fins

$T_{\text{outlet}} = 300.0749 \text{ K}$



16 Fins

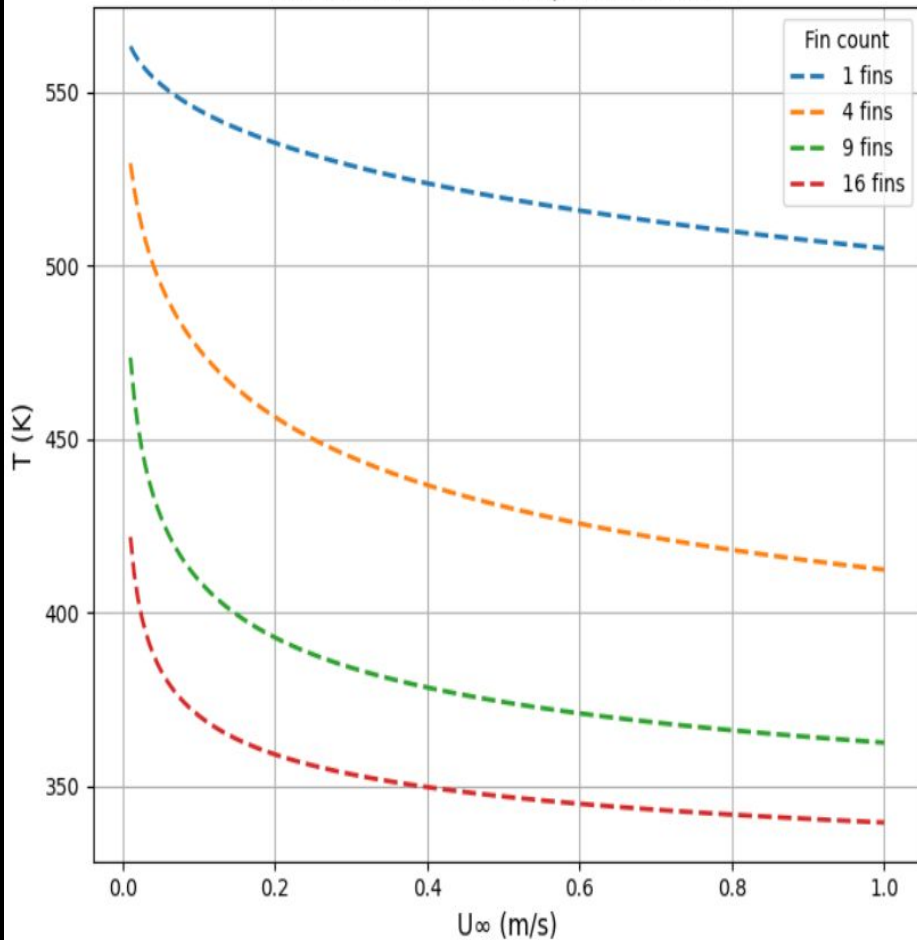
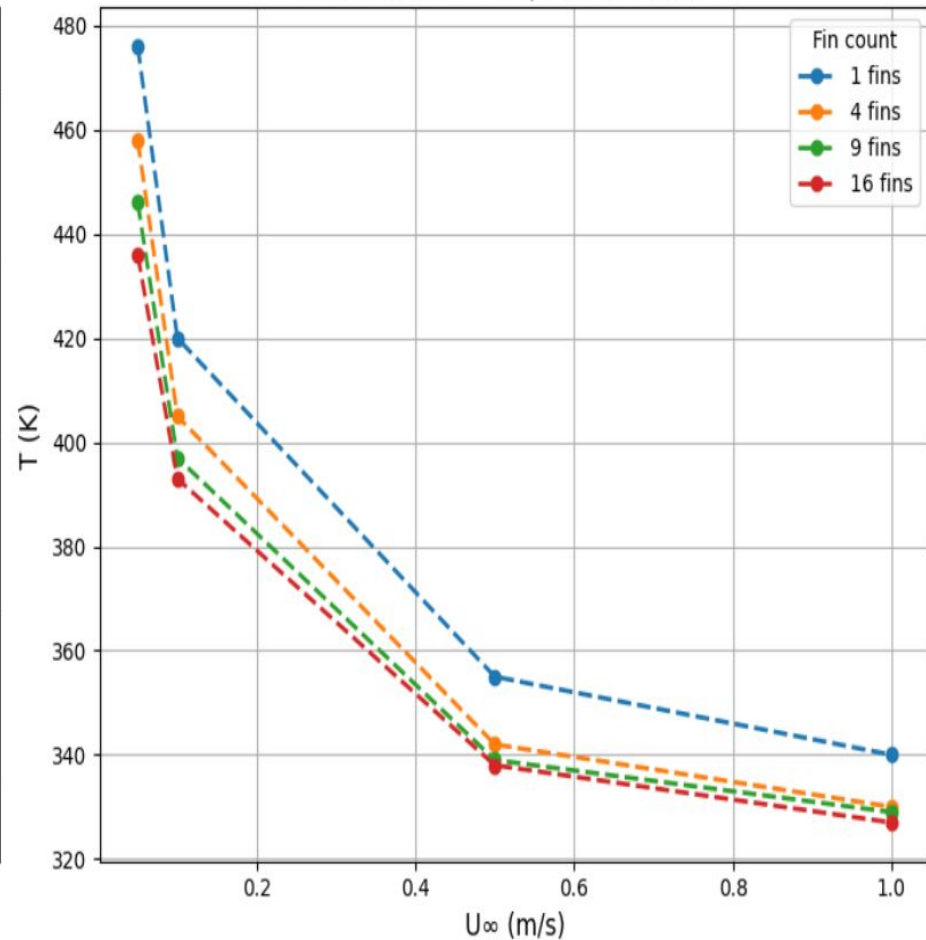
$T_{\text{outlet}} = 300.08 \text{ K}$

ANSYS Data  $T_{\text{mean}}$  (K)

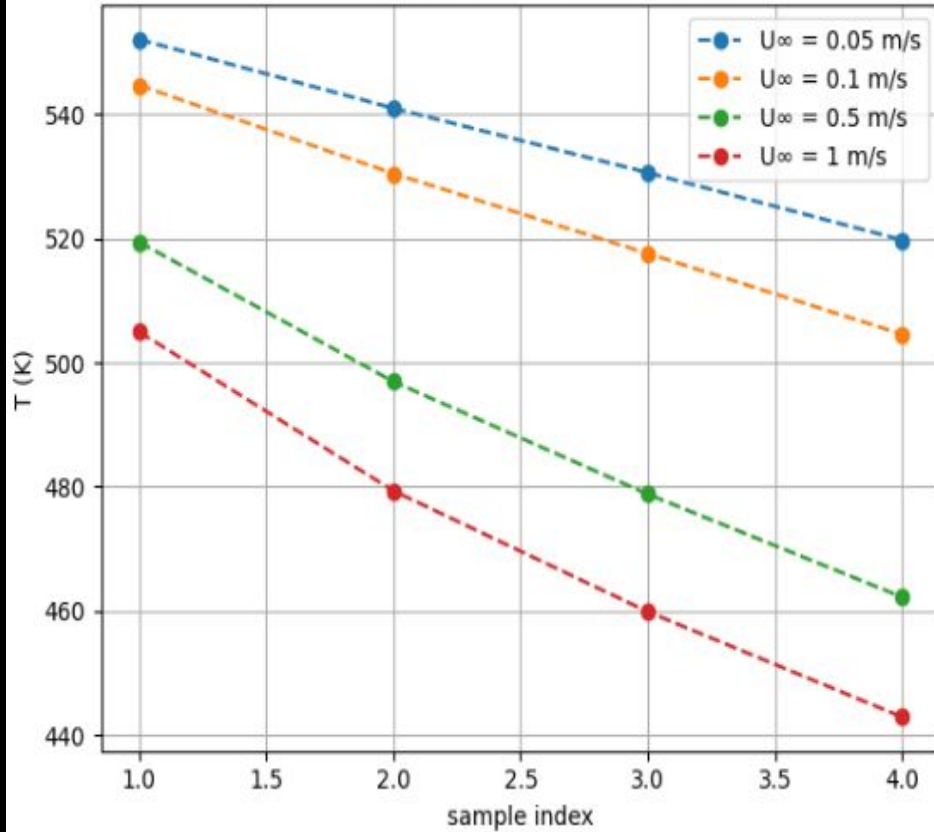
Fins →	1 fin	4 fins	9 fins	16 fins
$U_{\infty} = 0.05 \text{ m/s}$	476	458	446	436
$U_{\infty} = 0.10 \text{ m/s}$	420	405	397	393
$U_{\infty} = 0.50 \text{ m/s}$	355	342	339	338
$U_{\infty} = 1.00 \text{ m/s}$	340	330	329	327

Theoretical Data  $T_{\text{mean}}$  (K)

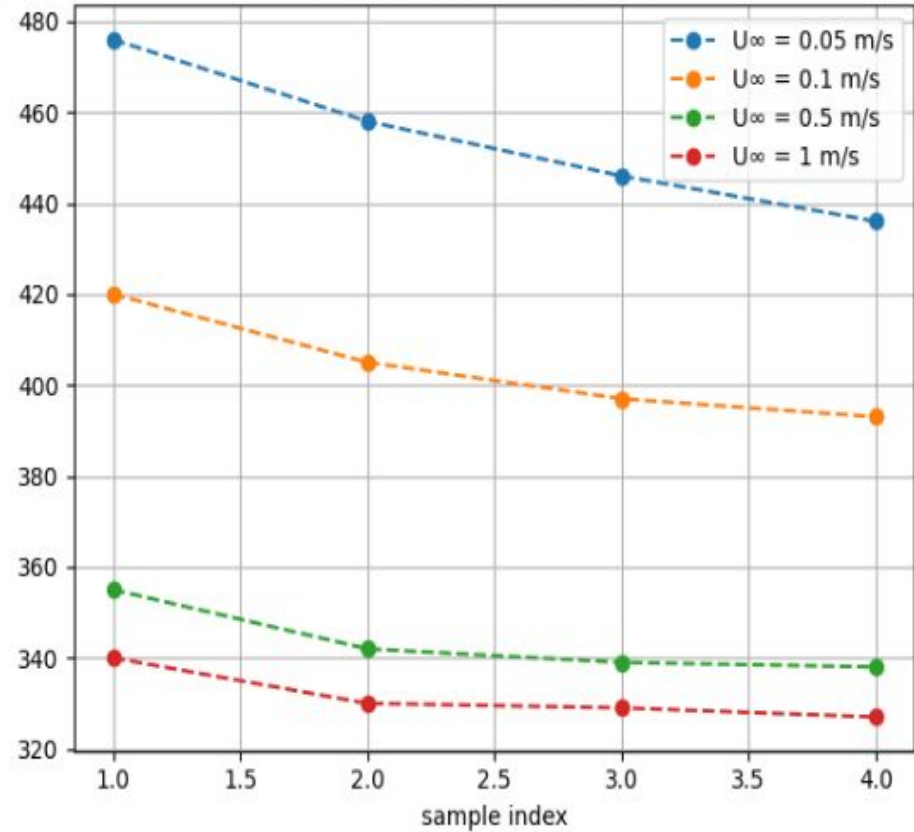
Fins →	1 fin	4 fins	9 fins	16 fins
$U_{\infty} = 0.05 \text{ m/s}$	512	503	494	485
$U_{\infty} = 0.10 \text{ m/s}$	506	494	483	472
$U_{\infty} = 0.50 \text{ m/s}$	485	466	451	437
$U_{\infty} = 1.00 \text{ m/s}$	473	451	435	420

Theoretical Mean Temperature vs  $U_\infty$ ANSYS Mean Temperature vs  $U_\infty$ 

Theoretical Temperature Profiles



ANSYS Temperature Profiles



NOTE :: Sample Index 1, 2, 3, 4 correspond to number fins 1, 4, 9 and 16 respectively