

Liquid Cooling of Heat Sink

ME 334- Heat and Mass Transfer

Group - L

Presented by

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Problem Statement

- A copper base plate with a rectangular cooling channel receives heat from a square heat source.
- Water enters the channel at a known temperature and different velocities.
- Fins of fixed height are added above the heat source in configurations of 1, 4, 9, and 16 fins (1 cm spacing) to enhance cooling.
- Our Goal is to Predict and simulate how fin count and inlet velocity affect solid temperature and overall heat transfer.

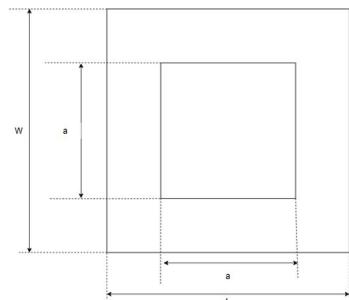
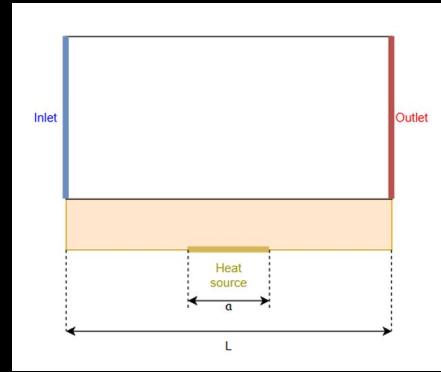


Figure 2

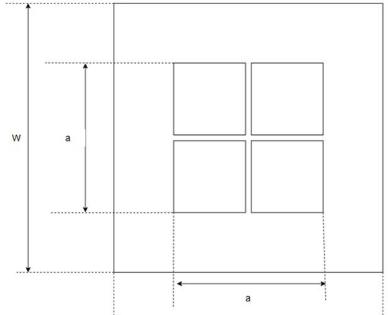


Figure 3

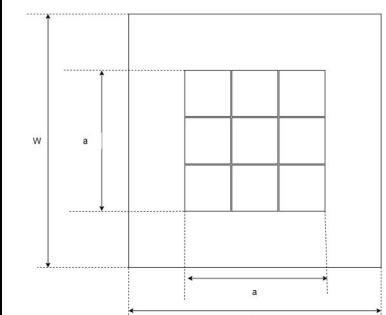


Figure 4

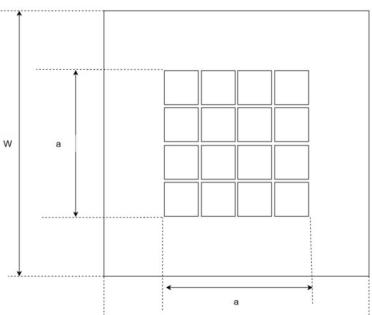


Figure 5

Formulae Used in Our Analysis

Assumptions (Same Theory for All Cases)

- Steady-state heat transfer
- One-dimensional conduction along fin length
- Uniform fin cross-section
- Constant material properties (k, h)
- Convection along fin surface **and tip**
- Temperature excess: $\theta = T - T_\infty$

Governing Fin Equation (Same for All 1,4,9,16 fin cases)

$$\frac{d^2\theta}{dx^2} - m^2\theta = 0$$

$$m^2 = \frac{hP}{kA_c}$$

Energy Balance on Fin Element

Conduction in = Conduction out + Convection loss

$$\Rightarrow \frac{d^2\theta}{dx^2} - \frac{hP}{kA_c}\theta = 0$$

Boundary Conditions

- Base: $\theta(0) = T_b - T_\infty$

- Tip: $-kA_c \frac{d\theta}{dx} \Big|_{x=L} = hA_c\theta(L)$

Temperature Profile & Mean Temperature (Using Same Theory for n Fins)

Temperature Profile

$$\frac{\theta(x)}{\theta_b} = \frac{\cosh[m(L-x)] + \left(\frac{h}{mk}\right) \sinh[m(L-x)]}{\cosh(mL) + \left(\frac{h}{mk}\right) \sinh(mL)}$$

Mean Fin Temperature

$$\bar{\theta} = \frac{1}{L} \int_0^L \theta(x) dx$$

$$\bar{T} = T_\infty + (T_b - T_\infty) \frac{\sinh(mL) + \left(\frac{h}{mk}\right) (\cosh(mL) - 1)}{mL [\cosh(mL) + \left(\frac{h}{mk}\right) \sinh(mL)]}$$

How Geometry Enters for n Sub-Fins

When one fin is split into n fins:

$$A_c \rightarrow \frac{A_c}{n}, \quad P \rightarrow \frac{P}{\sqrt{n}}$$

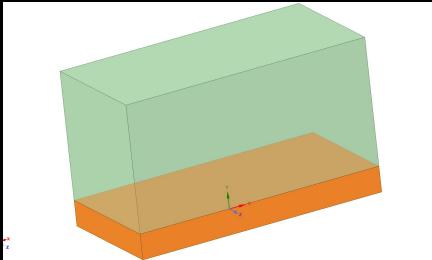
So the fin parameter becomes:

$$m_n^2 = \frac{h (P/\sqrt{n})}{k (A_c/n)} = m^2 \sqrt{n}$$

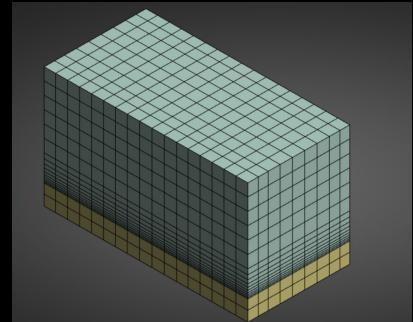
The formula stays the same, we only substitute the new m_n .

No Fin Case:

Mandatory Results (i)



Geometry



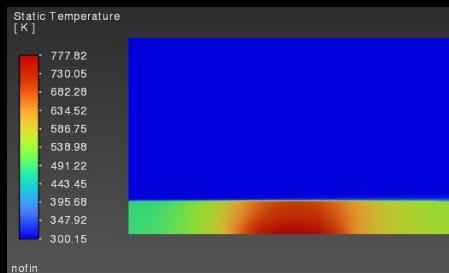
Mesh

Maximum temperature: 777.82 K

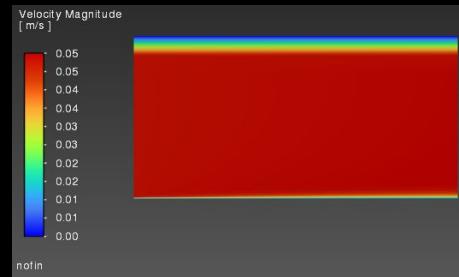
Solid average temperature : 592.36 K

Fluid average temperature: 300.9 K

Surface heat transfer coefficient: $314.87992 \text{ W/m}^2\text{-K}$

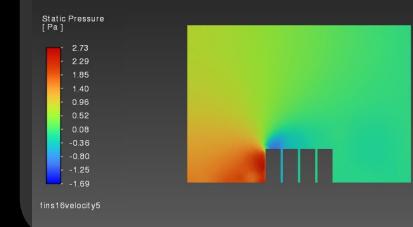
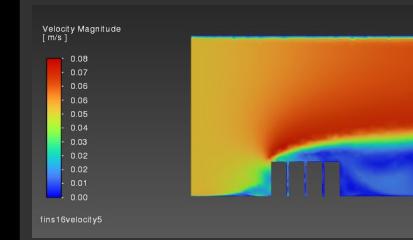
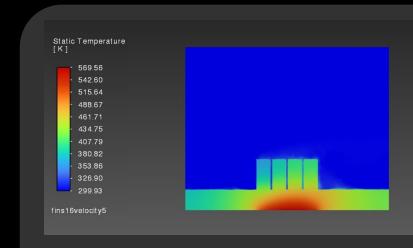
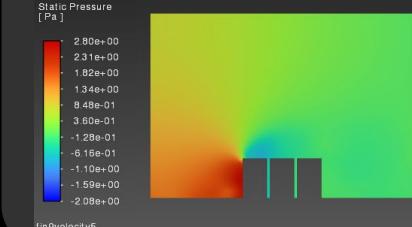
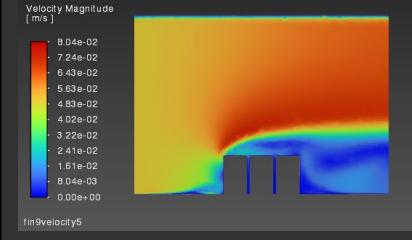
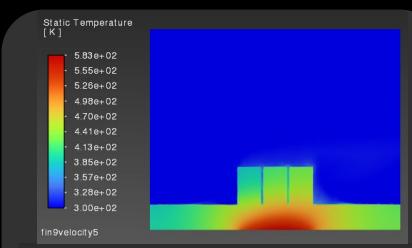
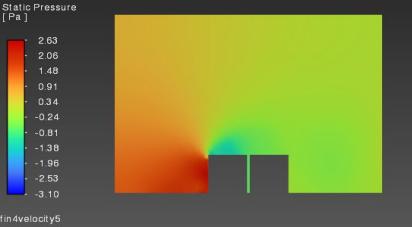
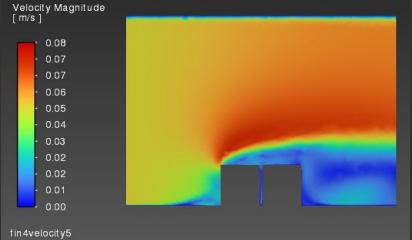
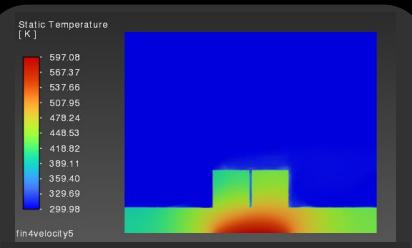
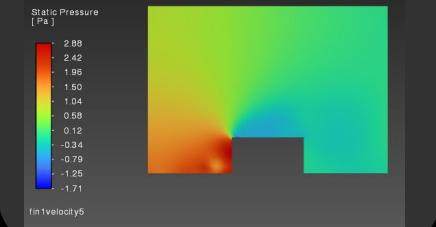
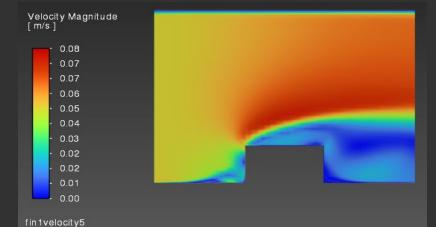
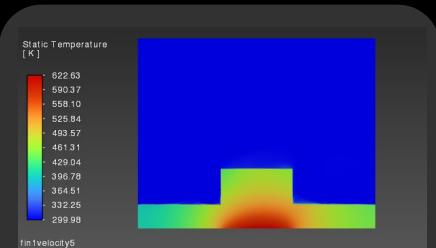


Temperature Distribution



Velocity Distribution

Inlet Velocity : 5 cm/s , T_inlet = 300K



Single Fin

T_outlet = 301.08 K

4 Fins

T_outlet = 301.085 K

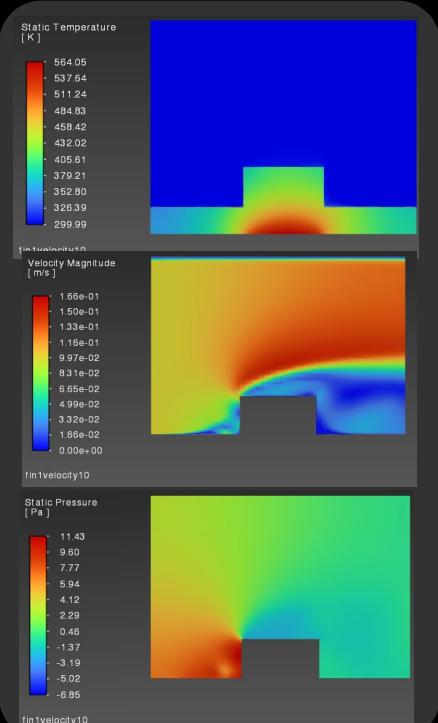
9 Fins

T_outlet = 301.16

16 Fins

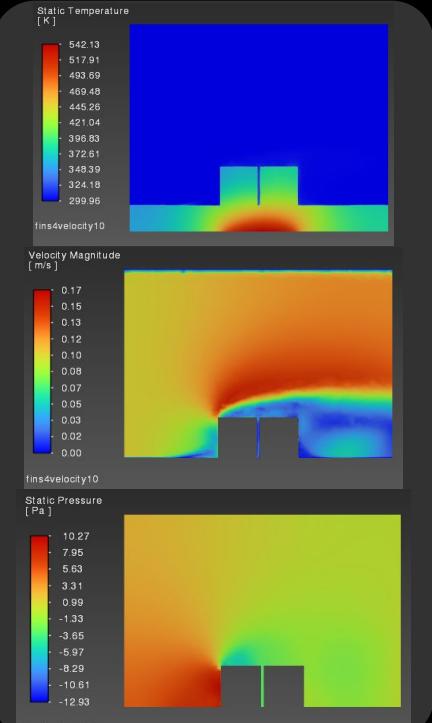
T_outlet = 301.177 K

Inlet Velocity : 10 cm/s



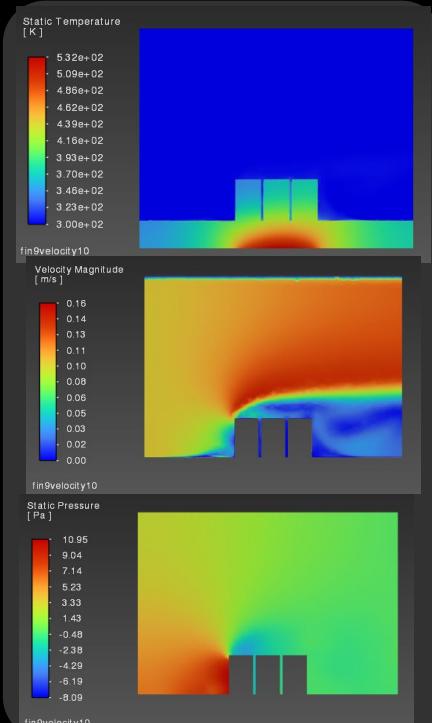
Single Fin

T_outlet = 300.54 K



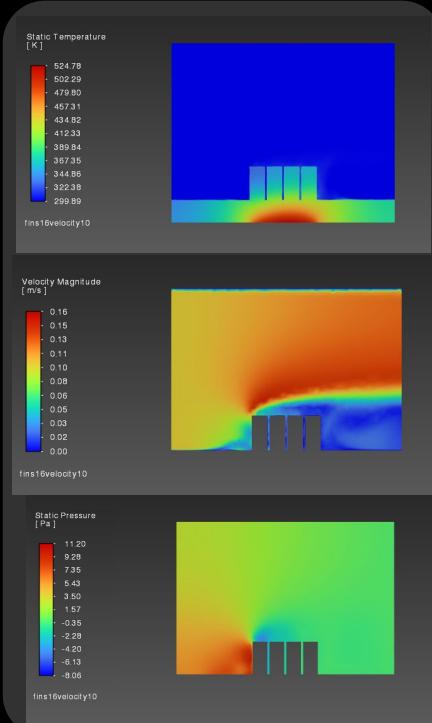
4 Fins

T_outlet = 300.57 K



9 Fins

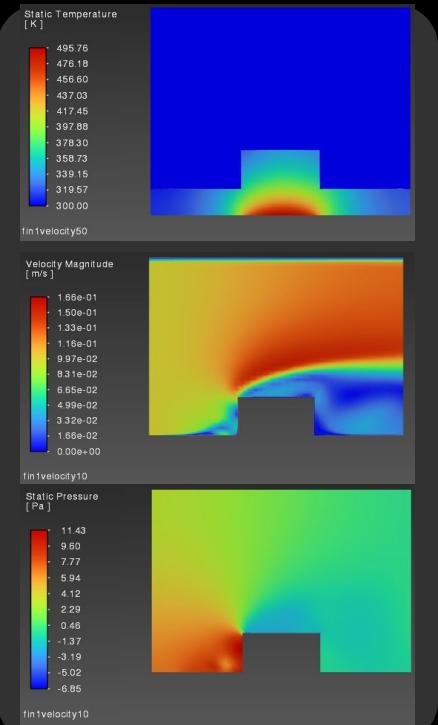
T_outlet = 300.58 K



16 Fins

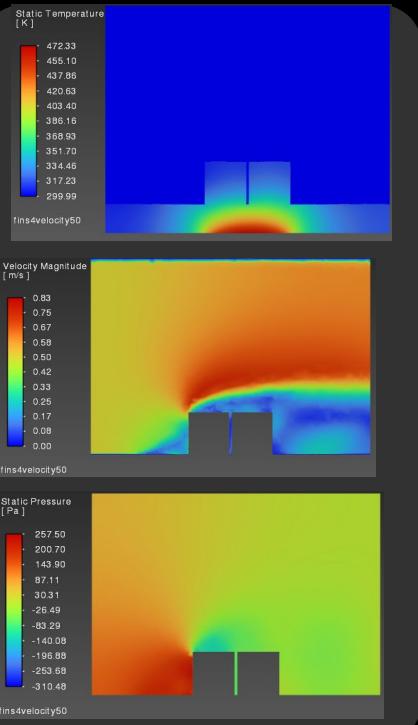
T_outlet = 300.59 K

Inlet Velocity : 50 cm/s



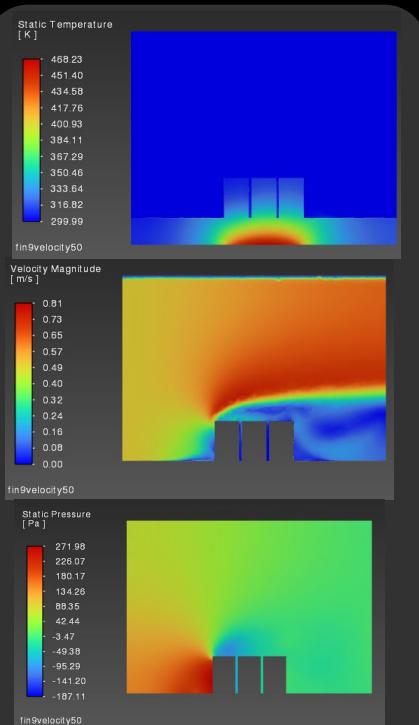
Single Fin

T_outlet = 300.09 K



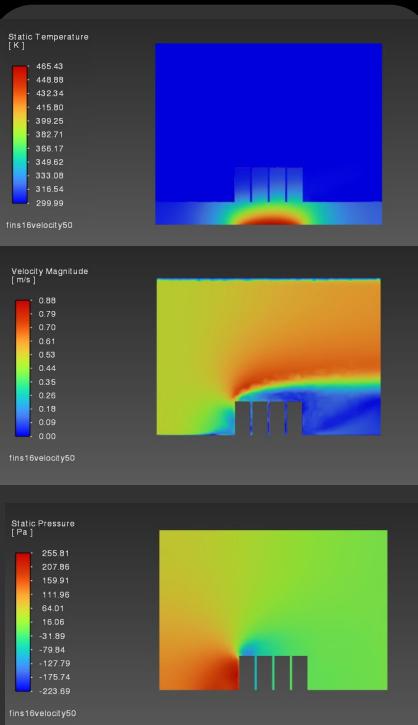
4 Fins

T_outlet = 300.116 K



9 Fins

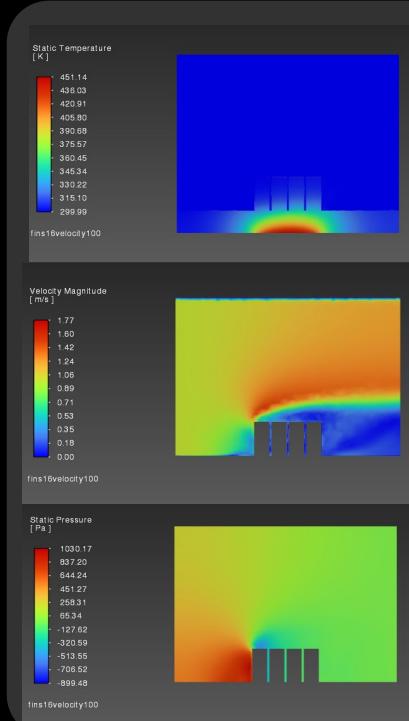
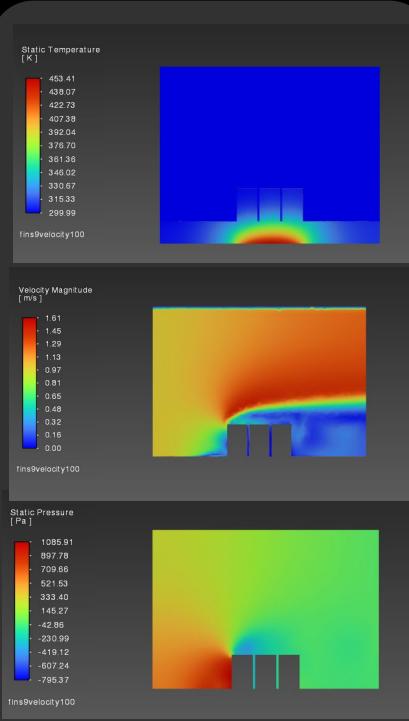
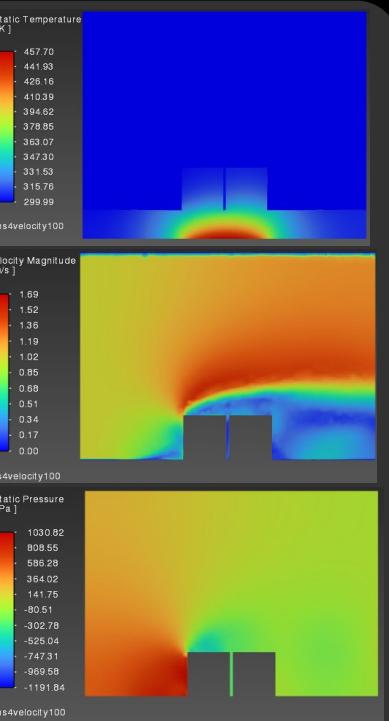
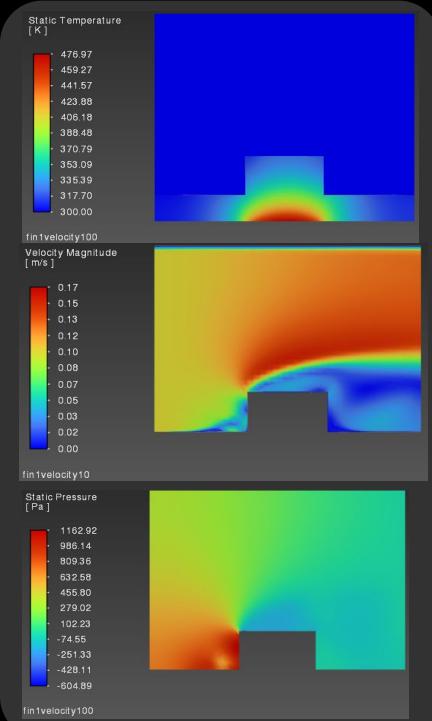
T_outlet = 300.117 K



16 Fins

T_outlet = 300.123 K

Inlet Velocity : 100 cm/s





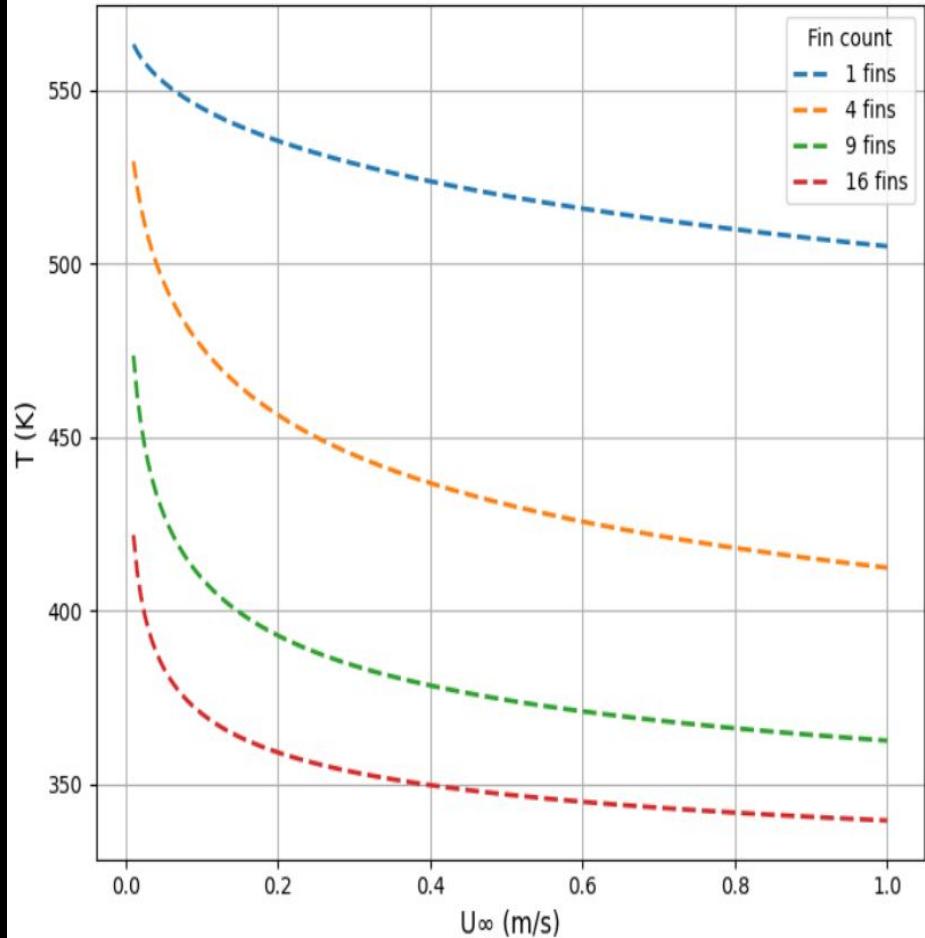
ANSYS Data T_mean (K)

Fins →	1 fin	4 fins	9 fins	16 fins
$U^\infty = 0.05 \text{ m/s}$	476	458	446	436
$U^\infty = 0.10 \text{ m/s}$	420	405	397	393
$U^\infty = 0.50 \text{ m/s}$	355	342	339	338
$U^\infty = 1.00 \text{ m/s}$	340	330	329	327

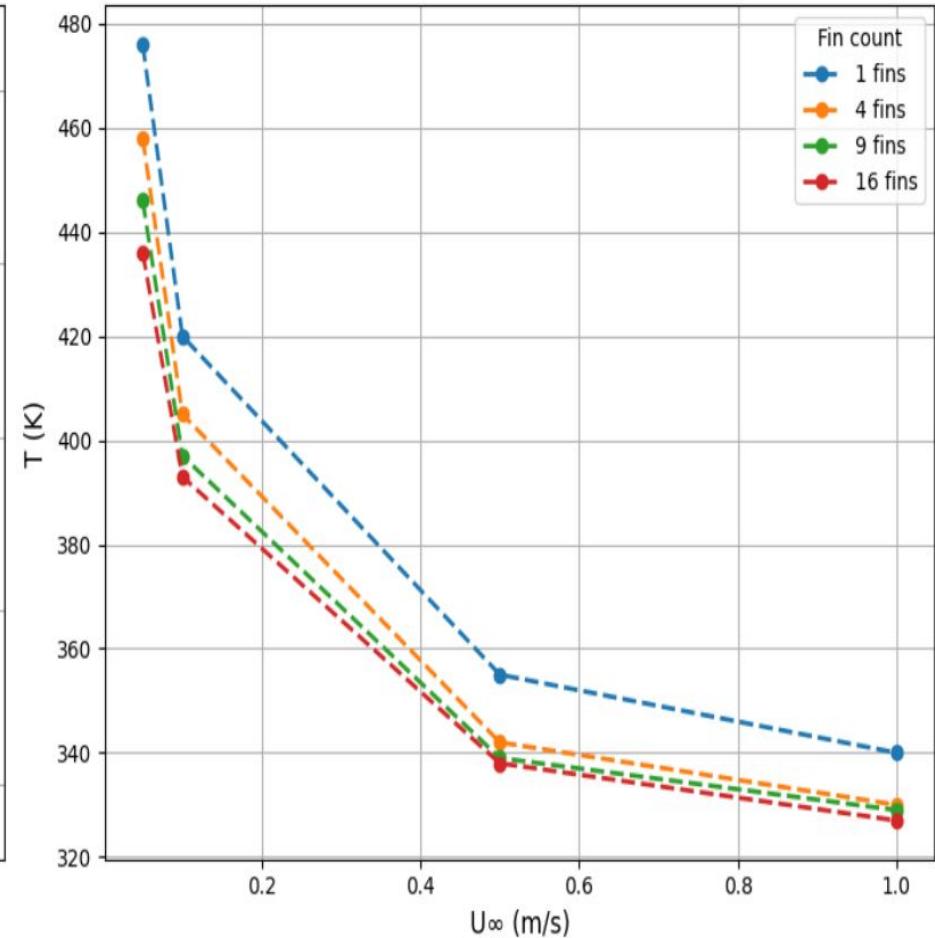
Theoretical Data T_mean (K)

Fins →	1 fin	4 fins	9 fins	16 fins
$U^\infty = 0.05 \text{ m/s}$	512	503	494	485
$U^\infty = 0.10 \text{ m/s}$	506	494	483	472
$U^\infty = 0.50 \text{ m/s}$	485	466	451	437
$U^\infty = 1.00 \text{ m/s}$	473	451	435	420

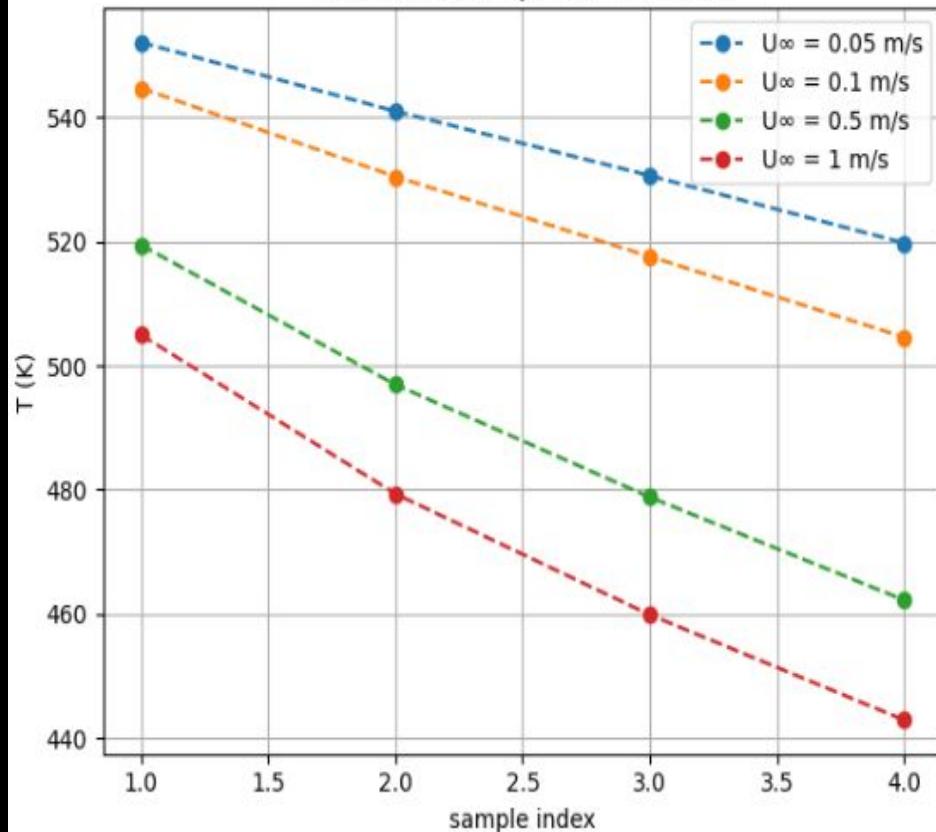
Theoretical Mean Temperature vs U_{∞}



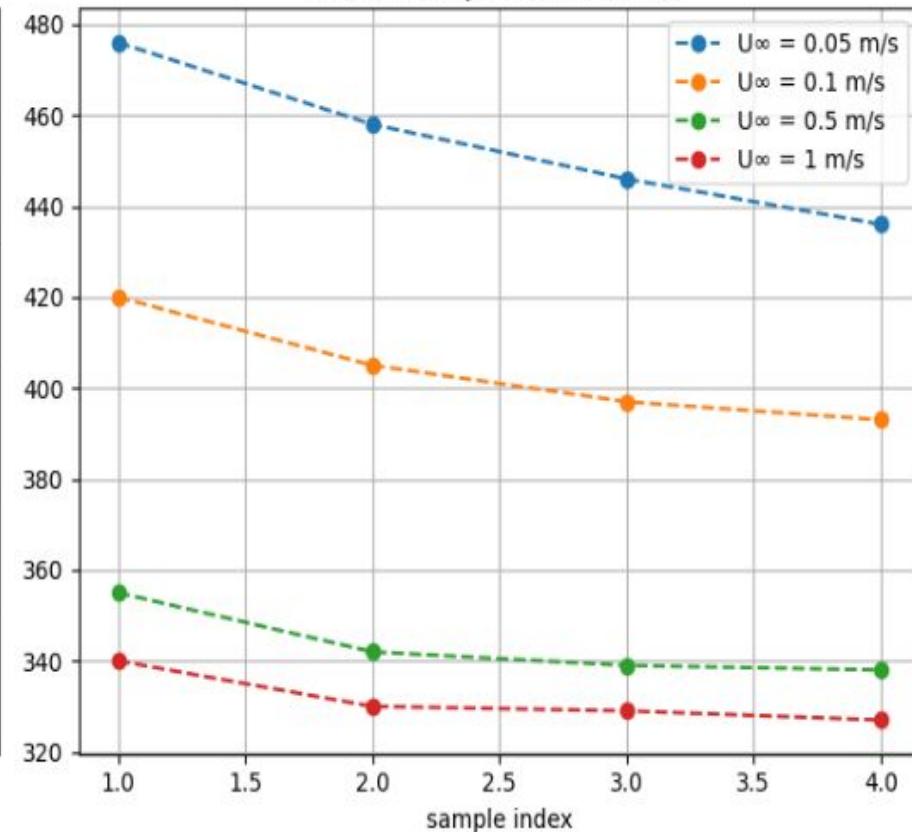
ANSYS Mean Temperature vs U_{∞}



Theoretical Temperature Profiles



ANSYS Temperature Profiles



NOTE :: Sample Index 1, 2, 3, 4 correspond to number fins 1, 4, 9 and 16 respectively