

# EL2450 Hybrid and Embedded Control

## Lecture 4: Computer realization of controllers

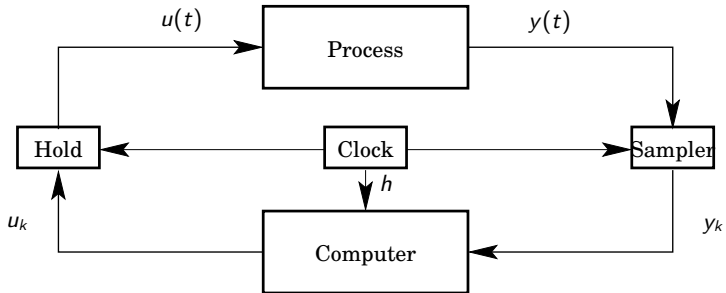
- Approximation of continuous-time designs
- Digital PID structures
- Realization of controllers
- Quantization
- Choice of sampling time

# Today's Goal

You should be able to

- Transform continuous-time controller into discrete time
- Identify and select appropriate controller realizations
- Model and analyze quantization in computations and AD/DA converters
- Decide on reasonable sampling time

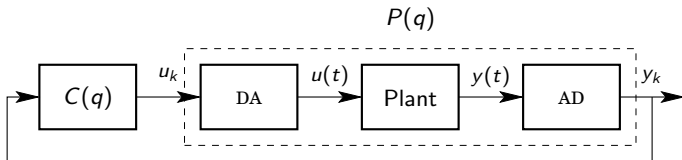
# Time-Triggered Control System



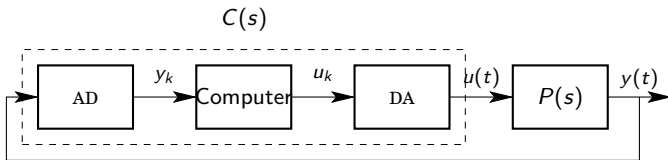
- **Q:** How apply continuous-time design methods to sampled control system?
- **A:** Make cuts at  $u(t)$  and  $y(t)$  (instead of at  $u_k$  and  $y_k$ )

## Designs in Discrete or Continuous Time

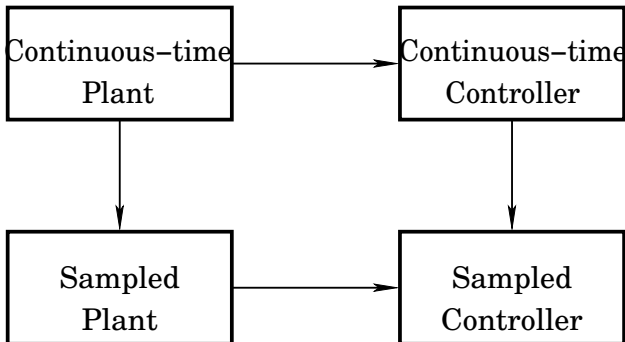
Sample plant, then derive a discrete-time controller:



Derive continuous-time controller, then transform to discrete-time algorithm:



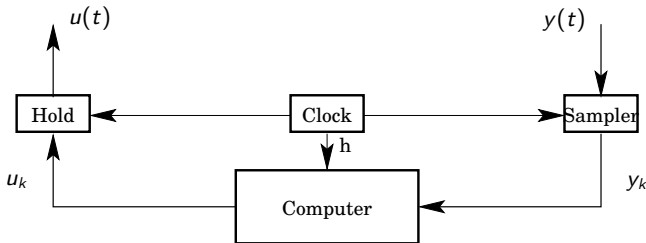
## Designs in Discrete or Continuous Time



## Approximating $C(s)$ by a Computer

**Transform continuous-time design into discrete time:**

Find  $C(z)$  that approximates  $C(s)$



# Approximation of Continuous-Time Derivatives

Forward difference:

$$\frac{dx(t)}{dt} \approx \frac{x(t+h) - x(t)}{h} = \frac{q-1}{h}x(t)$$

Backward difference:

$$\frac{dx(t)}{dt} \approx \frac{x(t) - x(t-h)}{h} = \frac{q-1}{qh}x(t)$$

Tustin's approximation:

$$\frac{dx(t)}{dt} \approx \frac{2}{h} \cdot \frac{q-1}{q+1}x(t)$$

## From $G(s)$ to $H(z)$

Pulse-transfer function  $H(z)$  corresponding to transfer function  $G(s)$  is

$$H(z) = G(s')$$

where

$$s' = \frac{z-1}{h} \quad (\text{Forward difference})$$

$$s' = \frac{z-1}{zh} \quad (\text{Backward difference})$$

$$s' = \frac{2}{h} \cdot \frac{z-1}{z+1} \quad (\text{Tustin's approximation})$$



## Example

Discrete-time approximation of

$$G(s) = \frac{1}{s+1}$$

gives pulse-transfer functions

$$H_1(z) = \frac{h}{z-1+h} \quad (\text{Forward difference})$$

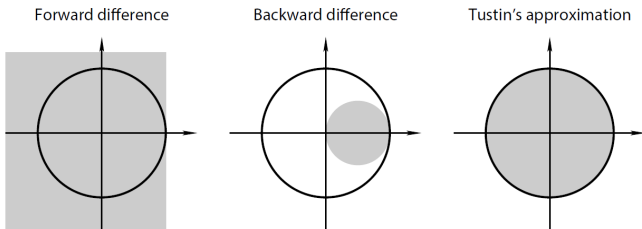
$$H_2(z) = \frac{h(1+h)^{-1}z}{z-(1+h)^{-1}} \quad (\text{Backward difference})$$

$$H_3(z) = \frac{h(2+h)^{-1}(z+1)}{z+(h-2)(h+2)^{-1}} \quad (\text{Tustin's approximation})$$

Note that  $H_1$  is unstable for large  $h$ , but  $H_2$  and  $H_3$  are always stable.

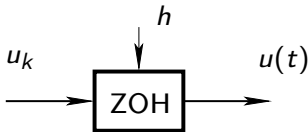
## Stability Regions for $H(z)$

The stability region  $\{s \in \mathbb{C} : \operatorname{Re} s < 0\}$  of continuous-time  $G(s)$  is mapped to the regions below for discrete-time  $H(z) = G(s')$ :



- Forward difference may generate unstable  $H(z)$  even if  $G(s)$  is stable
- Backward difference may yield stable  $H(z)$  even for unstable  $G(s)$
- Tustin maps stable to stable

## Transfer Function of a ZOH Circuit



Impulse response of  $1/s$  is a step. Impulse response of  $e^{-s}/s$  is a delayed step. Hence, a ZOH circuit can be represented as

$$H(s) = \frac{1 - e^{-sh}}{s}$$

since pulses can be represented as a series of impulse responses.

- For small  $h > 0$ :  $H(s) \approx \frac{1 - 1 + sh - s^2 h^2 / 2 + \dots}{s} = h - \frac{sh^2}{2} + \dots$
- Steady-state gain  $H(0) = h$

## Transfer Function of a Sampler

Recall the relationship between the Fourier transforms of the continuous-time and sampled signals:

$$F_s(\omega) = \frac{1}{h} \sum_{k=-\infty}^{\infty} F(\omega + k\omega_s)$$

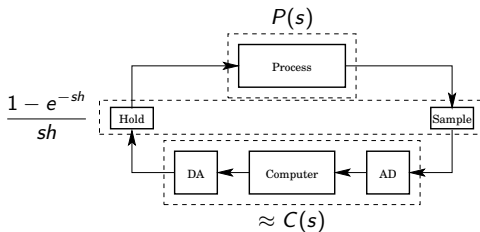
So there is a gain of  $1/h$  between the frequency responses.

ZOH together with sampler hence contribute to the loop with

$$\frac{1 - e^{-sh}}{sh}$$

# Continuous-Time Design of Sampled Controller

1. Design  $C(s)$  based on  $P(s)$  (or on  $P(s)\frac{1 - e^{-sh}}{sh}$  if  $h$  not small)
2. Derive discrete-time approximation of  $C(s)$
3. Implement discrete-time algorithm



# Continuous-time PID Controller

Continuous-time PID controller with  $e = r - y$ :

$$u(t) = K \left[ e(t) + \frac{1}{T_i} \int^t e(t) + T_d \frac{de(t)}{dt} \right]$$

Implementation of pure derivative not desirable since it yields large amplification of measurement noise. Approximation:

$$sT_d \approx \frac{sT_d}{1 + sT_d/N}$$

## Practical continuous-time PID

Continuous-time PID controller:

$$\begin{aligned} U(s) &= K \left[ bR(s) - Y(s) + \frac{1}{sT_i} \left( R(s) - Y(s) \right) - \frac{sT_d}{1 + sT_d/N} Y(s) \right] \\ &= P(s) + I(s) + D(s) \end{aligned}$$

Note the parameter  $b \in [0, 1]$  and that  $r$  is not differentiated in the D-part. Using  $p = \frac{d}{dt}$ :

$$\begin{aligned} u(t) &= K \left[ br(t) - y(t) + \frac{1}{T_i p} \left( r(t) - y(t) \right) - \frac{T_d p}{1 + T_d p/N} y(t) \right] \\ &= P(t) + I(t) + D(t) \end{aligned}$$

## Discretization of P-part

$$P(kh) = K [br(kh) - y(kh)]$$

## Discretization of I-part

$$I(t) = \frac{K}{T_i} \int^t e(s) ds = \frac{K}{T_i p} e(t)$$

Forward approximation gives

$$I(kh + h) = I(kh) + \frac{Kh}{T_i} e(kh)$$



## Discretization of D-part

$$\frac{T_d}{N} \cdot \frac{dD(t)}{dt} + D(t) = -KT_d \frac{dy(t)}{dt}$$

Backward approximation gives

$$\frac{T_d}{Nh} [D(kh) - D(kh - h)] + D(kh) = -\frac{KT_d}{h} [y(kh) - y(kh - h)]$$

so

$$D(kh) = \frac{T_d}{T_d + Nh} D(kh - h) - \frac{KT_d N}{T_d + Nh} [y(kh) - y(kh - h)]$$

# Discretized PID Control

With  $P, I, D$  as given above, then

$$u(kh) = P(kh) + I(kh) + D(kh)$$

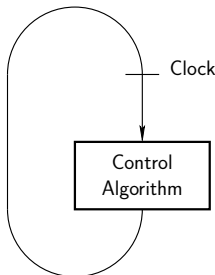
## Note

- The given approximations (backward + forward) enable independent calculations of  $P, I, D$
- Other approximations are possible (e.g., Tustin)
- Sometimes implementation on incremental form with output

$$\Delta u(kh) = u(kh) - u(kh - h)$$

# Computer Code for Sampled-Data Controller

```
nexttime = getCurrentTime();  
while (true) {  
    AD_conversion();  
    calculateOutput();  
    DA_conversion();  
    updateState();  
    nexttime = nexttime + h;  
    sleepUntil(nexttime);  
}
```



- calculateOutput between AD\_conversion and DA\_conversion gives minimum computational time delay in control loop
- Controller states (such as observer state) are updated separately
- sleepUntil supposed to be supported by operating system

## CalculateOutput and UpdateState

For a second-order controller on state space form

$$z(kh + h) = Az(kh) + By(kh)$$

$$u(kh) = Cz(kh) + Dy(kh)$$

calculateOutput() is essentially

$$u = c1*z1 + c2*z2 + d*y;$$

and updateState() is essentially

$$z1 = a11*z1 + a12*z2 + b1*y;$$

$$z2 = a21*z1 + a22*z2 + b2*y;$$

## Java Code for PID Controller

```
public static void main(String[] args) {
    double uc, y, u;
    PID pid = new PID();           // Construct PID controller object
    long time = System.currentTimeMillis(); // Get current time
    while (true) {
        y = readY();
        r = readR();
        u = pid.calculateOutput(r,y);
        writeU(u);
        pid.updateStates;
        time = time + par.pid.h*1000;
        Thread.waitUntil(time);    // Wait until 'time'
    }
}
```

```

public double calculateOutput(double r, double y) {
    signals.r = r;
    signals.y = y;
    double P = par.K*(par.b*r-y);
    states.D = par.ad*states.D-par.bd*(y - states.yold);
    signals.v = P + states.I + states.D;
    if (signals.v < par.ulow) {
        signals.u = par.ulow;
    } else {
        if (signals.v > par.uhigh) {
            signals.u = par.uhigh;
        } else {
            signals.u = signals.v;
        }
    }
    return signals.u;
}

public void updateStates() {
    states.I = states.I + par.bi*(signals.r - signals.y)
        + par.ar*(signals.u - signals.v); // Integral part
    states.yold = signals.y;
}

```

## Comments on PID Computer Code

- Controller state update is separated from controller output calculations
- Controller parameters are pre-calculated (e.g., `par.bi`, `par.ad`)
- A *thread* (e.g., `Thread.waitUntil`) is a real-time task, and supposed to be supported by the operating system

## Well-Conditioned Realizations

Consider controller

$$u(k) = \frac{b_o + b_1 q^{-1} + \dots + b_m q^{-m}}{1 + a_1 q^{-1} + \dots + a_n q^{-n}} y(k)$$

This can be realized in different forms, which influence

- Sensitivity to parameter and state quantization
- Number of storage elements and parameters (memory)
- Parameter range



## Sensitivity Analysis

Consider characteristic polynomial for  $i \in \{1, \dots, n\}$ :

$$A(z, a_i) = z^n + a_1 z^{n-1} + \dots + a_n = (z - p_1) \dots (z - p_n)$$

Suppose perturbation  $a_i + \delta a_i$  gives  $p_k + \delta p_k$ . Then,

$$\begin{aligned} 0 &= A(p_k + \delta p_k, a_i + \delta a_i) \\ &= A(p_k, a_i) + \frac{dA(p_k, a_i)}{dz} \delta p_k + \frac{dA(p_k, a_i)}{da_i} \delta a_i + \dots \end{aligned}$$

For small perturbations,

$$\delta p_k \approx -\frac{dA/da_i}{dA/dz}(p_k, a_i) \delta a_i$$

$$\frac{dA(p_k, a_i)}{da_i} = p_k^{n-i}, \quad \frac{dA(p_k, a_i)}{dz} = \prod_{j \neq k} (p_k - p_j)$$

Hence, if  $p_j \neq p_k$ ,

$$\delta p_k \approx - \frac{p_k^{n-i}}{\prod_{j \neq k} (p_k - p_j)} \delta a_i$$

## Note

- Sensitive to parameter quantization if poles are close and/or close to one
- For  $|p_k| < 1$ , largest perturbation is obtained for  $i = n$ , i.e., sensitivity largest for perturbations in  $a_n$

## Bad Implementation I: Direct Form

$$u(k) = \sum_{i=0}^m b_i y(k-i) - \sum_{i=1}^n a_i u(k-i)$$

- Not minimal form:  $m + n$  variables but only  $n$  states
- Parameters in implementation equal to characteristic polynomial: sensitive to computational errors if  $n$  large and poles close to one or close with each other

## Bad Implementation II: Canonical Form

Canonical forms, such as observable canonical form:

$$x(k+1) = \begin{bmatrix} -a_1 & 1 & 0 & \dots & 0 \\ -a_2 & 0 & 1 & \dots & 0 \\ \vdots & & & \ddots & \vdots \\ -a_{n-1} & 0 & 0 & \dots & 1 \\ -a_n & 0 & 0 & \dots & 0 \end{bmatrix} x(k) + \begin{bmatrix} b_1 \\ b_2 \\ \vdots \\ b_{n-1} \\ b_n \end{bmatrix} y(k)$$
$$u(k) = [1 \quad 0 \quad 0 \quad \dots \quad 0] x(k)$$

- Similar to in direct form: parameters in implementation equal to characteristic polynomial, so sensitive

## Good Implementation

Controller with  $n_r$  distinct poles and  $n_c$  complex pairs:

$$z_i(k+1) = \lambda_i z_i(k) + \beta_i y(k), \quad i = 1, \dots, n_r$$

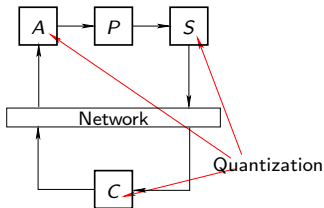
$$v_i(k+1) = \begin{bmatrix} \sigma_i & \omega_i \\ -\omega_i & \sigma_i \end{bmatrix} v_i(k) + \begin{bmatrix} \gamma_{i1} \\ \gamma_{i2} \end{bmatrix} y(k), \quad i = 1, \dots, n_c$$

$$u(k) = \sum_{i=1}^{n_r} \alpha_i z_i(k) + \sum_{i=1}^{n_c} \delta_i^T v_i(k)$$

- Robust to perturbations in parameters and states
- Parallel form implementation, as a cascade of first and second-order filters (see exercise 5.1)

# Quantization

- Quantization in AD converters
- Quantization of controller parameters
- Roundoff, overflow, and underflow in operations (addition etc.)
- Quantization in DA converters



# Quantization in AD and DA Converters

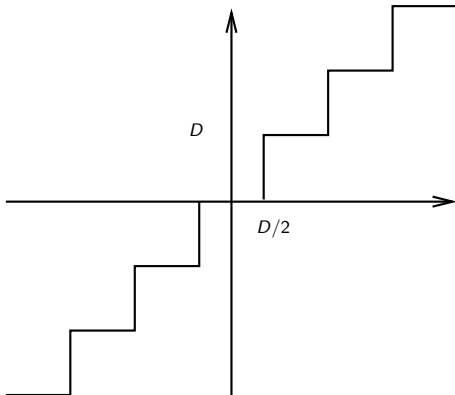
## AD Converter

- Typical accuracy of 8, 10, 12, and 14 bits
- 8 bits correspond to  $1/2^8 \approx 0.4\%$  resolution
- 14 bits correspond to  $1/2^{14} \approx 0.006\%$  resolution

## DA Converter

- Typical accuracy of 10 bits

# Uniform Quantization

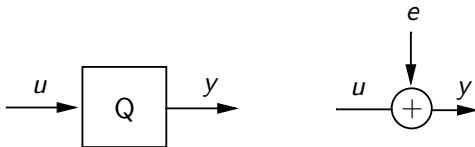




## Linear Model of Quantization

Model quantization error as a uniformly distributed stochastic signal  $e$  independent of  $u$  with

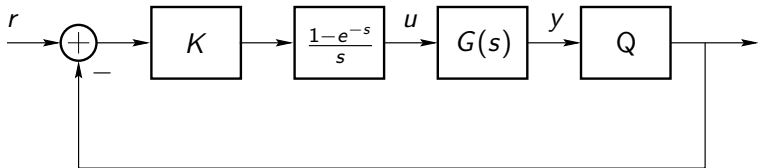
$$\text{Var}(e) = \int_{-\infty}^{\infty} e^2 f_e de = \int_{-D/2}^{D/2} \frac{e^2}{D} de = \frac{D^2}{12}$$

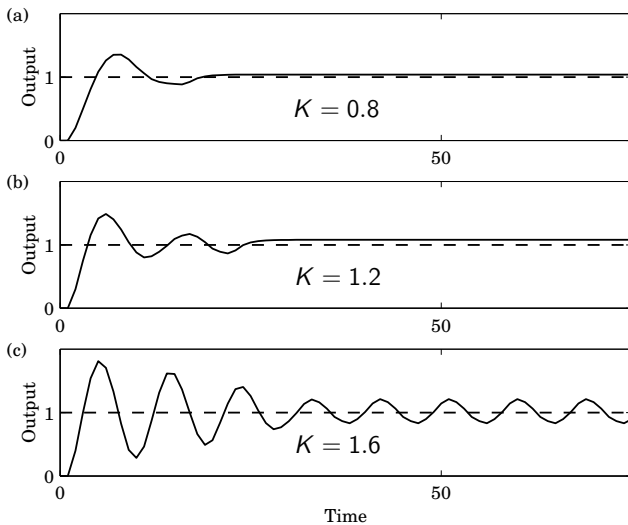


Works if  $D$  is small compared to the variations in  $u$

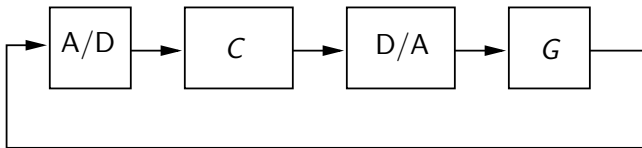
## Example: Sensor Quantization

- Quantization of process output with  $D = 0.2$
- Quantizer generates stable oscillation for  $K = 1.6$
- Can be predicted using nonlinear control methods

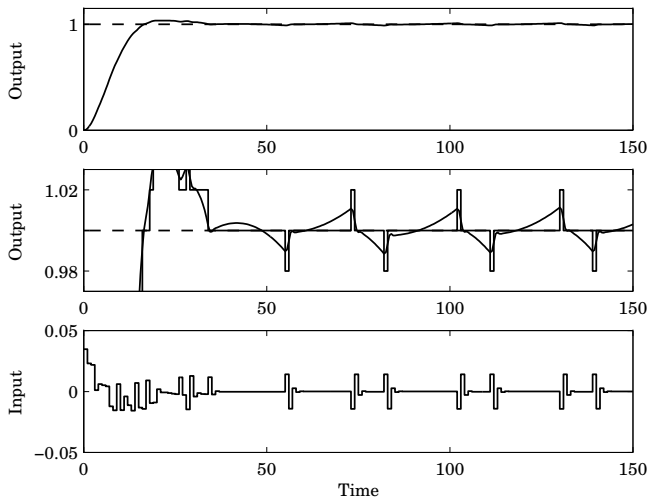




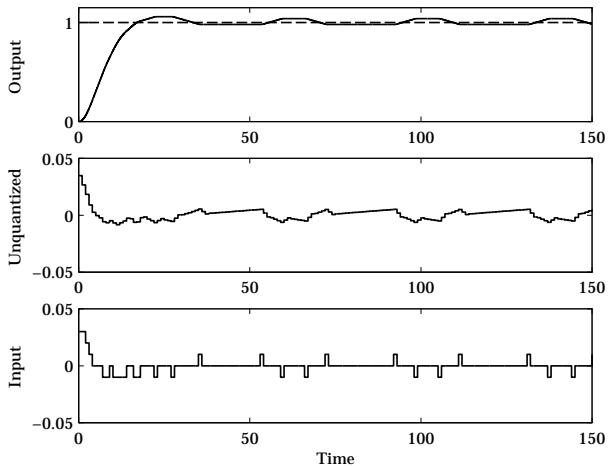
## Example: Quantization in AD or DA



Quantization  $D = 0.02$  in AD converter:



Quantization  $D = 0.01$  in DA converter:



# Choosing Sampling Time

Sampling time  $h > 0$  might be

- Considered as an independent design parameter
- Fixed by the application or implementation platform
- Uncertain due to asynchronous sampling and hold
- Time varying due to communication and computation variations

## Note

- Sampling time might heavily influence closed-loop performance
- Sometimes overlooked in the design
- Lack of systematic methods for choosing sampling time
- Use computer simulations off-line

## Sampling Time Rule of Thumb

- Choose  $h$  such that there will be 4 to 10 samples per rise time

For a second-order system with natural frequency  $\omega_0$  this gives

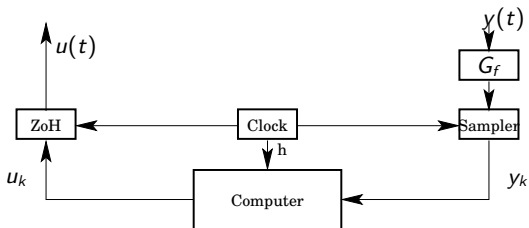
$$0.2 < \omega_0 h < 0.6$$

The sampling frequency  $\omega_s$  should thus fulfill  $10\omega_0 < \omega_s < 30\omega_0$ , so the sampling frequency for control is much higher than the frequency  $2\omega_0$  needed for reconstructing a sampled signal of frequency  $\omega_0$

The rule of the thumb is built on extensive experience, but not much theory



## Another Sampling Time Rule of Thumb



Choose  $h$  such that the zero-order-hold (ZoH) and anti-aliasing filter ( $G_f$ ) give phase margin decrease of 5 to 15 deg

With cross-over frequency  $\omega_c$  for the continuous-time plant, this results (under certain assumptions) in

$$h\omega_c \approx 0.05 \quad \text{to} \quad 0.14$$

## Why Not $h \rightarrow 0$ ?

If a plant

$$\dot{x} = Ax + Bu$$

is sampled fast ( $h \approx 0$ ), then the discrete-time dynamics

$$x(k+1) = \Phi x(k) + \Gamma u(k)$$

looks approximately like integrators to the controller because

$$\Phi = e^{Ah} \approx I + Ah$$

It will then require high numerical accuracy in the controller (computer) to be able to distinguish the difference.

## Next Lecture

- Quantization in state feedback
- Network delays and data drops
- Compensation for delay variations