

EL2520 - Control Theory and Practice - Advanced

Project Lab : The Four Tank Process

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Abstract — This document is a report for the Project Lab conducted under the EL2520 course. This project was divided into 2 distinct sessions. The first one involved deriving a physical model of a four-tank process for minimum phase and non-minimum phase configurations via experimentation and investigating the coupling between the tanks. Emphasis was also given to manually controlling the process to understand the performance limitations due to the non-minimum dynamics. The second instance was dedicated to testing the model-based decentralized PI controller and the robust Glover-McFarlane method.

Thus, the final system of equations turns out to be:

$$\begin{aligned}\frac{dh_1}{dt} &= \frac{-a_1}{A_1} \sqrt{2gh_1} + \frac{a_3}{A_1} \sqrt{2gh_3} + \frac{\gamma_1 k_1}{A_1} u_1 \\ \frac{dh_2}{dt} &= \frac{-a_2}{A_2} \sqrt{2gh_2} + \frac{a_4}{A_2} \sqrt{2gh_4} + \frac{\gamma_2 k_2}{A_2} u_2 \\ \frac{dh_3}{dt} &= \frac{-a_3}{A_3} \sqrt{2gh_3} + \frac{(1-\gamma_2)k_2}{A_3} u_2 \\ \frac{dh_4}{dt} &= \frac{-a_4}{A_4} \sqrt{2gh_4} + \frac{(1-\gamma_1)k_1}{A_4} u_1\end{aligned}\tag{1}$$

I. Modelling

Here, the nonlinear differential equations describing the plant will be derived. Thus, the rate of change of volume in each tank is given as:

$$A \frac{dh}{dt} = q_{in} - q_{out}$$

From Bernoulli's law, we have

$$q_{out} = a \sqrt{2gh} \quad \forall g = 981 \text{ cm/s}^2$$

Now, as there is a pump used, its flowrate is governed as follows:

$$q_L = \gamma k u, \quad q_U = (1 - \gamma) k u \quad \forall \gamma \in [0, 1]$$

$\forall q_L$ denotes the lower tank and q_U denotes the upper tank. From the above equations, we can derive the nonlinear system as follows:

$$\begin{aligned}A_1 \frac{dh_1}{dt} &= -q_{out,1} + q_{out,3} + q_{L,1} \\ A_2 \frac{dh_2}{dt} &= -q_{out,2} + q_{out,4} + q_{L,2} \\ A_3 \frac{dh_3}{dt} &= -q_{out,3} + q_{U,2} \\ A_4 \frac{dh_4}{dt} &= -q_{out,4} + q_{U,1}\end{aligned}$$

A. Equilibrium Equations

For the equilibrium condition, we take the rate of change of height as 0 to get the following set of equations:

$$\begin{aligned}\frac{-a_1}{A_1} \sqrt{2gh_1^0} + \frac{a_3}{A_1} \sqrt{2gh_3^0} + \frac{\gamma_1 k_1}{A_1} u_1^0 &= 0 \\ \frac{-a_2}{A_2} \sqrt{2gh_2^0} + \frac{a_4}{A_2} \sqrt{2gh_4^0} + \frac{\gamma_2 k_2}{A_2} u_2^0 &= 0 \\ \frac{-a_3}{A_3} \sqrt{2gh_3^0} + \frac{(1-\gamma_2)k_2}{A_3} u_2^0 &= 0 \\ \frac{-a_4}{A_4} \sqrt{2gh_4^0} + \frac{(1-\gamma_1)k_1}{A_4} u_1^0 &= 0 \\ y_i^0 &= k_c h_i^0 \quad \forall i = \{1, 2, 3, 4\}\end{aligned}$$

where h_i^0 , u_i^0 , y_i^0 denote the steady state values.

B. Linearization

Let $\Delta u_i = u_i - u_i^0$, $\Delta h_i = h_i - h_i^0$ and $\Delta y_i = y_i - y_i^0$ denote the deviations from the equilibrium and also let

$$u = \begin{bmatrix} \Delta u_1 \\ \Delta u_2 \end{bmatrix}, x = \begin{bmatrix} \Delta h_1 \\ \Delta h_2 \\ \Delta h_3 \\ \Delta h_4 \end{bmatrix}, y = \begin{bmatrix} \Delta y_1 \\ \Delta y_2 \end{bmatrix}$$

For Linearizing the above-derived system of non-linear equation 1 around its equilibrium points, we use the Taylor Series of Expansion (neglecting HOTs) to obtain

the following matrices:

$$A = \left[\begin{array}{cccc} \frac{\partial \Delta h_1}{\partial \Delta h_2} & \frac{\partial \Delta h_1}{\partial \Delta h_2} & \frac{\partial \Delta h_1}{\partial \Delta h_2} & \frac{\partial \Delta h_1}{\partial \Delta h_2} \\ \frac{\partial h_1}{\partial \Delta h_3} & \frac{\partial h_2}{\partial \Delta h_3} & \frac{\partial h_3}{\partial \Delta h_3} & \frac{\partial h_4}{\partial \Delta h_3} \\ \frac{\partial h_1}{\partial \Delta h_4} & \frac{\partial h_2}{\partial \Delta h_4} & \frac{\partial h_3}{\partial \Delta h_4} & \frac{\partial h_4}{\partial \Delta h_4} \\ \frac{\partial h_1}{\partial h_1} & \frac{\partial h_2}{\partial h_2} & \frac{\partial h_3}{\partial h_3} & \frac{\partial h_4}{\partial h_4} \end{array} \right] \Big|_{h_i^0, u_i^0}$$

$$B = \left[\begin{array}{cc} \frac{\partial \Delta h_1}{\partial u_1} & \frac{\partial \Delta h_1}{\partial u_2} \\ \frac{\partial u_1}{\partial \Delta h_3} & \frac{\partial u_2}{\partial \Delta h_3} \\ \frac{\partial u_1}{\partial \Delta h_4} & \frac{\partial u_2}{\partial \Delta h_4} \\ \frac{\partial u_1}{\partial u_1} & \frac{\partial u_2}{\partial u_2} \end{array} \right] \Big|_{h_i^0, u_i^0}$$

$$C = \left[\begin{array}{cccc} \frac{\partial \Delta y_1}{\partial h_1} & \frac{\partial \Delta y_1}{\partial h_2} & \frac{\partial \Delta y_1}{\partial h_3} & \frac{\partial \Delta y_1}{\partial h_4} \\ \frac{\partial h_1}{\partial \Delta y_2} & \frac{\partial h_2}{\partial \Delta y_2} & \frac{\partial h_3}{\partial \Delta y_2} & \frac{\partial h_4}{\partial \Delta y_2} \\ \frac{\partial h_1}{\partial h_1} & \frac{\partial h_2}{\partial h_2} & \frac{\partial h_3}{\partial h_3} & \frac{\partial h_4}{\partial h_4} \end{array} \right] \Big|_{h_i^0, u_i^0}$$

$$D = \left[\begin{array}{cc} \frac{\partial \Delta y_1}{\partial u_1} & \frac{\partial \Delta y_1}{\partial u_2} \\ \frac{\partial u_1}{\partial \Delta y_2} & \frac{\partial u_2}{\partial \Delta y_2} \\ \frac{\partial u_1}{\partial u_1} & \frac{\partial u_2}{\partial u_2} \end{array} \right] \Big|_{h_i^0, u_i^0}$$

After solving the above matrices, we get

$$\dot{x} = Ax + Bu, \quad y = Cx + Du$$

where,

$$A = \left[\begin{array}{cccc} -\frac{1}{T_1} & 0 & \frac{A_3}{A_1 T_3} & 0 \\ 0 & -\frac{1}{T_2} & 0 & \frac{A_4}{A_2 T_4} \\ 0 & 0 & -\frac{1}{T_3} & 0 \\ 0 & 0 & 0 & -\frac{1}{T_4} \end{array} \right]$$

$$B = \left[\begin{array}{cc} \frac{\gamma_1 k_1}{A_1} & 0 \\ 0 & \frac{\gamma_2 k_2}{A_2} \\ 0 & \frac{(1 - \gamma_2) k_2}{A_3} \\ \frac{(1 - \gamma_1) k_1}{A_4} & 0 \end{array} \right]$$

$$C = \left[\begin{array}{cccc} k_c & 0 & 0 & 0 \\ 0 & k_c & 0 & 0 \end{array} \right]$$

and $D = 0$, with $T_i = \frac{A_i}{a_i} \sqrt{\frac{2h_i^0}{g}}$.

C. Transfer Matrix

In order to obtain the Transfer Matrix, we use the following formula -

$$G(s) = C(sI - A)^{-1}B$$

i.e. $G(s) =$

$$\left[\begin{array}{cccc} \frac{T_1}{1+sT_1} & 0 & \frac{\frac{A_3 T_1}{A_1}}{(1+sT_1)(1+sT_3)} & 0 \\ 0 & \frac{T_2}{1+sT_2} & 0 & \frac{\frac{A_4 T_2}{A_2}}{(1+sT_2)(1+sT_4)} \\ 0 & 0 & \frac{T_3}{1+sT_3} & 0 \\ 0 & 0 & 0 & \frac{T_4}{1+sT_4} \end{array} \right] * \left[\begin{array}{cc} \frac{\gamma_1 k_1}{A_1} & 0 \\ 0 & \frac{\gamma_2 k_2}{A_2} \\ 0 & \frac{(1 - \gamma_2) k_2}{A_3} \\ \frac{(1 - \gamma_1) k_1}{A_4} & 0 \end{array} \right] =$$

$$\left[\begin{array}{cc} \frac{\gamma_1 k_1 c_1}{1+sT_1} & \frac{(1 - \gamma_2) k_2 c_1}{(1+sT_3)(1+sT_1)} \\ \frac{(1 - \gamma_1) k_1 c_2}{(1+sT_4)(1+sT_2)} & \frac{\gamma_2 k_2 c_2}{1+sT_2} \end{array} \right]$$

D. Zeros of Transfer Matrix

Zeros of the Transfer matrix $G(s)$ are given by the numerator of the $\det(G(s))$. In other words, zeros of the Transfer matrix can be obtained by solving the equation :

$$\gamma_1 \gamma_2 T_3 T_4 s^2 + \gamma_1 \gamma_2 (T_3 + T_4) s + (\gamma_1 + \gamma_2 - 1) = 0$$

$$\Rightarrow T_3 T_4 s^2 + (T_3 + T_4) s + \frac{\gamma_1 + \gamma_2 - 1}{\gamma_1 \gamma_2} = 0$$

The solution of the above quadratic equation is:

$$s_1 = -\frac{T_3 + T_4}{2T_3 T_4} + \frac{1}{2T_3 T_4} \sqrt{(T_3 + T_4)^2 - 4 \frac{\gamma_1 + \gamma_2 - 1}{\gamma_1 \gamma_2}}$$

$$s_2 = -\frac{T_3 + T_4}{2T_3 T_4} - \frac{1}{2T_3 T_4} \sqrt{(T_3 + T_4)^2 - 4 \frac{\gamma_1 + \gamma_2 - 1}{\gamma_1 \gamma_2}}$$

Here, as s_2 has both terms negative, the zero is on the Left Half of the s -plane. But when it comes to s_1 , if the term $\frac{\gamma_1 + \gamma_2 - 1}{\gamma_1 \gamma_2}$ is positive, value of the square root term will be less than $T_3 + T_4$, which makes the zero negative. Thus, for the **Minimum Phase case**, $(\gamma_1 + \gamma_2 - 1) > 0$ i.e $\gamma_1 + \gamma_2 > 1$ Now as $\gamma_1, \gamma_2 \in [0, 1]$, $\gamma_1 + \gamma_2 \leq 2$

$$\therefore 1 < \gamma_1 + \gamma_2 \leq 2$$

For the **Non-minimum phase case**, one of the zeros is positive which means $(\gamma_1 + \gamma_2 - 1) < 0$. Also, as $\gamma_1, \gamma_2 \in [0, 1]$, $\gamma_1 + \gamma_2 > 0$.

$$\therefore 0 < \gamma_1 + \gamma_2 \leq 1$$

E. RGA Analysis

$RGA(G(0)) = G(0) \cdot G(0)^{-1T}$ Thus,

$$G(0) = \begin{bmatrix} \gamma_1 k_1 c_1 & (1 - \gamma_2) k_2 c_1 \\ (1 - \gamma_1) k_1 c_2 & \gamma_2 k_2 c_2 \end{bmatrix}$$

$$G(0)^{-1T} = \left(\frac{1}{\gamma_1 \gamma_2 k_1 k_2 c_1 c_2 - (1 - \gamma_1)(1 - \gamma_2) k_1 k_2 c_1 c_2} \right) \begin{bmatrix} \gamma_2 k_2 c_2 & -(1 - \gamma_1) k_1 c_2 \\ -(1 - \gamma_2) k_2 c_1 & \gamma_1 k_1 c_1 \end{bmatrix}$$

Hence, the RGA of $G(0)$ is given by

$$RGA(G(0)) = G(0) \cdot G(0)^{-1T} = \begin{bmatrix} \frac{\gamma_1 \gamma_2}{\gamma_1 + \gamma_2 - 1} & \frac{\gamma_1 + \gamma_2 - 1 - \gamma_1 \gamma_2}{\gamma_1 + \gamma_2 - 1} \\ \frac{\gamma_1 + \gamma_2 - 1 - \gamma_1 \gamma_2}{\gamma_1 + \gamma_2 - 1} & \frac{\gamma_1 \gamma_2}{\gamma_1 + \gamma_2 - 1} \end{bmatrix}$$

Now, let $\lambda = \frac{\gamma_1 \gamma_2}{\gamma_1 + \gamma_2 - 1}$. Thus, we get

$$RGA(G(0)) = \begin{bmatrix} \lambda & 1 - \lambda \\ 1 - \lambda & \lambda \end{bmatrix}$$

For **Minimum Phase case** :

$\lambda_1 = 0.625 = \lambda_2$. Thus,

$$RGA(G_{mp}(0)) = \begin{bmatrix} 1.5625 & -0.5625 \\ -0.5625 & 1.5625 \end{bmatrix}$$

For **Non-Minimum Phase case** :

$\lambda_1 = 0.375 = \lambda_2$. Thus,

$$RGA(G_{nmp}(0)) = \begin{bmatrix} -0.5625 & 1.5625 \\ 1.5625 & -0.5625 \end{bmatrix}$$

F. Determination of k_1 and k_2

For determining the values of k_1 and k_2 , we need to measure how fast the pump fills up a tank. Thus, for k_1 , tank 1 was observed and the following experiment was conducted. We stopped the outflow from tank 1 and ensured that only the pump input was allowed into the tank. This helped us obtain the value of k_1 using the following equation:

$$\frac{dh_1}{dt} = -\frac{a_1}{A_1} \sqrt{2gh_1} + \frac{a_3}{A_1} \sqrt{2gh_3} + \frac{\gamma_1 k_1}{A_1} u_1$$

We repeated the same process with the $tank_2$ for obtaining the value of k_2 .

After multiple readings using different voltages, we obtained

$$k_1 = 4.4247 cm^3/sV$$

$$k_2 = 4.1092 cm^3/sV$$

G. Determination of areas of holes

Before proceeding with the procedure, some assumptions used are as follows:

- The cross-sectional areas of the tanks are the same i.e $A = 15.52 \text{ cm}^2$
- The areas a_1 and a_2 remain the same for both Minimum and non-minimum phase cases
- The areas a_3 and a_4 will vary for Minimum and non-minimum phase cases

So, for calculating the areas, we first considered tanks 3 and 4 as they just had a single input and single output making the calculation for a_3 and a_4 simple. We let the upper 2 tanks settle at their equilibrium points h_3^0 and h_4^0 by keeping $u_1^0 = 7.5V$ and $u_2^0 = 7.5V$.

$$\therefore a_3 = \frac{(1 - \gamma_2) k_2}{\sqrt{2gh_3^0}} u_2^0$$

$$\text{and } a_4 = \frac{(1 - \gamma_1) k_1}{\sqrt{2gh_4^0}} u_1^0$$

Now, the entire system was driven to equilibrium and all the steady-state heights (h_i^0) were measured. As we had 2 equations (one each for tank 1 and tank 2) and 2 unknown, the areas of holes 1 and 2 were calculated by solving the 2*2 linear system as follows:

$$a_1 = \frac{a_3}{\sqrt{2gh_1^0}} \sqrt{2gh_3^0} + \frac{\gamma_1 k_1}{\sqrt{2gh_1^0}} u_1^0$$

$$a_2 = \frac{a_4}{\sqrt{2gh_2^0}} \sqrt{2gh_4^0} + \frac{\gamma_2 k_2}{\sqrt{2gh_2^0}} u_2^0$$

For **Minimum Phase Case**

$$a_1 = 0.2250 \text{ cm}^2$$

$$a_2 = 0.2389 \text{ cm}^2$$

$$a_3 = 0.0633 \text{ cm}^2$$

$$a_4 = 0.0888 \text{ cm}^2$$

For **Non-Minimum Phase Case**

$$a_1 = 0.2250 \text{ cm}^2$$

$$a_2 = 0.2389 \text{ cm}^2$$

$$a_3 = 0.115 \text{ cm}^2$$

$$a_4 = 0.213 \text{ cm}^2$$