

Thermal Physics

Yu Lu

April 14, 2023

1 Mathematical tricks

A few important results from multivariate calculus include

- Chain rule: useful for change of variable $U(x, y)$ into $U(u, v)$

$$\left(\frac{\partial U}{\partial x}\right)_y = \left(\frac{\partial U}{\partial u}\right)_v \left(\frac{\partial u}{\partial x}\right)_y + \left(\frac{\partial U}{\partial v}\right)_u \left(\frac{\partial v}{\partial x}\right)_y$$

- Reciprocal rules: useful for changing the subject variable (“dependent variable”)

$$\begin{aligned}\left(\frac{\partial X}{\partial Y}\right)_Z &= \left(\frac{\partial Y}{\partial X}\right)_Z^{-1} \\ \left(\frac{\partial X}{\partial Y}\right)_Z \left(\frac{\partial Y}{\partial Z}\right)_X \left(\frac{\partial Z}{\partial X}\right)_Y &= -1.\end{aligned}$$

The second reciprocal rule is often useful when a thermodynamic potential is held constant: we just turn it to the numerator.

This allows us to easily navigate between differentials of different thermodynamic quantities, yet the question remains: what do we know about the quantities themselves? For example, we might know $p(V, T)$ and correspondingly

$$\left(\frac{\partial F}{\partial V}\right)_T = -p.$$

The best we can do, then, is to integrate the differential with respect to V and hold the T constant:

$$F(V, T) = f(T) + \int \left(\frac{\partial F}{\partial V}\right)_T dV = f(T) + \int -p(V, T) dV,$$

leaving an undetermined function that only depends on T and up to a constant.

A ton of partial differentials can be generated from the algebra above, but often many of them have physical meanings or can be converted. For example, temperature derivatives of entropy can be associated with heat capacities:

$$\boxed{C_V = T \left(\frac{\partial S}{\partial T}\right)_V = \left(\frac{\partial U}{\partial T}\right)_V, \quad C_p = T \left(\frac{\partial S}{\partial T}\right)_p = \left(\frac{\partial H}{\partial T}\right)_p.}$$

Thermodynamic variables are grouped into conjugate groups $\{V, p\}$, $\{S, T\}$, and $\{\mu, N\}$. The partial derivative of one thermodynamic variable with respect to another thermodynamic variable can be converted to another such partial differential using Maxwell’s relations. Often, we want to convert such partial differentials into the conjugate pair $\{V, p\}$ in questions involving gas because the equation of state relates V and p to T . A systematic approach can be used to spot which relation to use: say we start with $\left(\frac{\partial S}{\partial p}\right)_T$, then thermodynamic potential we want to consider will have a total differential

$$dB = \pm SdT \pm xdp,$$

where B is a thermodynamic potential and x is a thermodynamic variable. The potential of interest must then be G with $dG = -SdT + Vdp$, giving the Maxwell relation of interest

$$\left(\frac{\partial S}{\partial p}\right)_T = -\left(\frac{\partial V}{\partial T}\right)_p.$$

The partial differential of a thermodynamic potential with respect to one thermodynamic variable could be identified as another thermodynamic variable. This is only true if the two are natural variables of the potential. For example, because $dG = -SdT + Vdp$, we can identify

$$\left(\frac{\partial G}{\partial T}\right)_p = -S, \quad \left(\frac{\partial G}{\partial p}\right)_T = V.$$

2 The zeroth and the first law

2.1 The zeroth law

An isolated system will eventually display no noticeable change in the macrostate variables, coming to a state called *equilibrium*. The zeroth law states that temperature is a function of macroscopic state only. Specifically, it states that thermal equilibrium is transitive. Consideration of this on three bodies in equilibrium allows us to define temperature $\theta(p, V)$ as a function of state. One possible form is the ideal gas temperature

$$T = \frac{pV}{Nk_B},$$

but to show that this *is* the thermodynamic temperature $\theta(p, V)$ requires the second law.

2.2 The first law

The first law states that energy is a function of state. It can be stated without introducing anything new that the amount of work required to change an isolated system from state 1 to state 2 is path independent, motivating the internal energy

$$dU = \delta q + \delta w,$$

where dU is a state variable, but δq and δw *individually* are not. For a gas in a reversible change,

$$\delta w = -pdV,$$

which is not an exact differential, and thus is path dependent.

3 The second law and entropy

3.1 The statements

Microscopically, everything is reversible due to thermal fluctuation. Macroscopically, things are irreversible if we cannot restore the motion of every microscopic particle (like in a lens). However, assuming that we move the system infinitesimally at a time in the absence of dissipation, macroscopic reversibility is possible (the fluctuation will bring it towards equilibrium).

At its heart, the second law dictates the arrow of time of irreversible changes: what is done cannot be undone, ergo, the second law breaks the time-reversal symmetry. It is often stated in two different ways:

- *À la Kelvin*: No process is possible whose *only* effect is the **complete conversion of heat to work**.
- *À la Clausius*: No process is possible whose *only* effect is to transfer heat **from a colder to a hotter body**.

Reversibility of a process, in the absence of external work, is determined by states of the system only, motivating a state variable characterising reversibility. In other words, reversibility requires

- Quasi-static process: the system comes to equilibrium at every stage of the change such that we can describe every stage of the system by the macroscopic variables (p, V) . (Essentially, a process that can be fully described by a curve on the $p - V$ diagram)
- Absence of dissipation: there is no sources of friction etc.

3.2 Heat engines and the temperature scale

Carnot engine is a cyclic reversible heat engine, comprising of two isotherms connected by two adiabats. In a cycle, it draws heat Q_H from the hot reservoir and expels heat Q_C from the cold reservoir, with the rest $W = Q_H - Q_C$ being converted to work. By relying on the second law and reversibility of a Carnot engine, it can be shown that

- There are no super-Carnot engines in terms of heat efficiency

$$\eta = \frac{W}{Q_H} = 1 - \frac{Q_C}{Q_H}.$$

In other words, a Carnot engine produces the most work for a given Q_H .

- All reversible heat engines are Carnot and have the same efficiency $\eta(T_H, T_C)$.

By combining several Carnot engines together, it can be shown that the efficiency of a Carnot engine must take the form

$$\eta = 1 - \frac{f(\theta_C)}{f(\theta_H)},$$

which, without loss of generality, allows us to define the thermodynamic temperature in terms the Carnot efficiency

$$f(\theta) = \theta \implies \eta = 1 - \frac{\theta_C}{\theta_H}.$$

Consider a Carnot engine driven by ideal gas, then, gives

$$\boxed{\frac{Q_1}{T_1} = \frac{Q_2}{T_2}} \implies T = \theta$$

as promised.

3.3 Clausius' theorem and Entropy

From Carnot's cycle, we can conclude that

$$\frac{Q_1}{T_1} = \frac{Q_2}{T_2}, \implies \oint_{\text{rev}} \frac{\mathrm{d}q}{T} = 0$$

along any reversible path, where $\mathrm{d}q$ is positive for any heat flowing into the system. Since we can always subdivide a Carnot cycle to any arbitrary shape by connecting more isotherms and adiabats around the corner, it is possible to represent any reversible change as a series of Carnot cycles. Therefore, the results above hold for any reversible path in the phase space. It is worth noting that while any path in the pV diagram can represent a reversible change, it is not a sufficient condition for reversibility (essentially, only the quasistatic condition is met). Therefore, it is perfectly fine for the same path in the pV space to represent a reversible change or an irreversible change—the difference lies in dissipation. In this sense, the “path-dependence” in the pV space is not the same as the difference between a reversible and an irreversible change.

The above statement also means that the integral is path-independent in the phase space for a reversible change, motivating us to define the entropy of *the system*

$$\Delta S := \int \frac{\mathrm{d}q_{\text{rev}}}{T}$$

The Carnot's theorem tells us that the irreversible path always ejects more heat into the surrounding, making the integral more negative, thus

$$\boxed{\oint \frac{\mathrm{d}q}{T} \leq 0, \quad \Delta S = \int \frac{\mathrm{d}q_{\text{rev}}}{T} \geq \int \frac{\mathrm{d}q}{T}}$$

for a general change, with the equality achieved for a reversible change. Therefore, a reversible adiabatic change is also isentropic. Extending our notional box to encompass the universe (which is assumed to be isolated) gives that $\Delta S_{\text{universe}} \geq 0$ for any change allowed by the second law.

The entropy S is, as we've seen mathematically, a function of state: a reversible change and an irreversible change following potentially different paths in the pV space lead to the same (likely non-zero) entropy change of *the system*. The reversibility should not matter at this stage, as entropy is *defined* using the heat flow in a reversible change. The difference between a reversible and an irreversible change only lies in the entropy change of the surrounding, which is a function of state of the surrounding. In a reversible change, the entropy change of the surrounding exactly cancels with the entropy change of the system. However, by no means can we find the volume change of the rest of the universe, so this doesn't feel like a state variable to us, as we only have access to state variables of the system. In that regard, it is clear that a reversible change and an irreversible change put the universe into different states.

More specifically, as the irreversible heat is transferred to the surrounding, the only change in its state function is the enthalpy change, equal to the heat received. To calculate the entropy change of the surrounding, we need to regard it as our new system and subject it to the new system, but we should end up with the same enthalpy change, giving $\Delta S = \frac{q}{T_{\text{surr}}}$. As a recipe, the entropy change of the universe in an irreversible process can be calculated as

$$\Delta S_{\text{universe}} = \int \frac{\delta q_{\text{rev}}}{T_{\text{sys}}} + \sum -\frac{q_{\text{irre}}}{T_{\text{surr}}},$$

where q is positive for heat flow into the system and q_{rev} is the heat flow of a devised reversible process with the same start and final state.

3.4 Adiabatic changes

The second law can also be stated as the existence of an adiabatic surface (total differential). The adiabatic curve can be either solved by

$$\delta q = dU - p dV = 0$$

when $U(p, V)$ is known or by

$$dS = 0$$

when the total derivative of $S(p, V)$ is known in analytic thermodynamics.

4 Analytical thermodynamics

In thermodynamics, we distinguish between a system and a surrounding. The surrounding is so large such that its intensive variables (p , T , and μ) are regarded as constants. The boundaries between the system and the surrounding can be different nature

- open system: particle and energy flow dN , δq , and δw allowed
- closed system: only energy flow δq and δw allowed
- isolated system: adiabatic $\delta q = 0$ and $\delta w = 0$, but $dS = 0$ only for reversible changes (think of Joules expansion as a counterexample).

The system is said to be in **thermal equilibrium** once the heat flow is stopped. The system and the surrounding together forms an *isolated* system, so any drop of energy in the system is matched by the same amount of increase in the surrounding. The only exception is the entropy, which stays the same or increases for the whole universe. Every change in the surrounding, therefore, can be expressed with only *system variables*.

Unless specified otherwise, it is assumed that only “ pV -work” is done with fixed particle number, so the master equation is

$$\boxed{dU = T dS - p dV.}$$

4.1 Thermodynamic potentials

The internal energy $U(S, T)$ quantifies energy stored in the system that can be converted to work or heat under certain conditions, but its change is expressed in terms of S and V which are not always convenient. Of course, U can encapsulate other forms of energy, such as CoM kinetic energy and gravitational potential energy, so long as they are state functions. Often, we want to study the heat flow or work done in terms of p and T as well. Moreover, the natural variables of U are S and T , so we only know complete information about the system if $U(S, T)$ is given (the other two quantities can be worked out by differentiation). Often, however, systems are not expressed in S and T , motivating thermodynamic potentials with different natural variables.

Through Legendre transform, *enthalpy*, *Helmholtz free energy*, and *Gibbs free energy* can be defined as (the natural variables are included in the arguments)

$$H(p, S) = U + pV, \quad dH = TdS + Vdp;$$

$$F(V, T) = U - TS, \quad dF = -SdT - pdV;$$

$$G(p, T) = H - TS = F + pV = U + pV - TS, \quad dG = -SdT + Vdp.$$

The $+pV$ terms in Legendre transform can be interpreted as excluding pV -work while the $-TS$ terms can be interpreted as reflecting the maximum work extractable (see section 4.2). Mathematically, thermodynamic variables can be extracted by differentiating these potentials. Moreover, we could arrive at *Maxwell relations* using commuting partial derivatives, such as

$$\frac{\partial^2 U}{\partial S \partial V} = \left(\frac{\partial T}{\partial V} \right)_S = - \left(\frac{\partial p}{\partial S} \right)_V$$

Sometimes we are interested in flow processes, in which gas with (p_1, V_1) are put into some devices and gas with (p_2, V_2) are ejected. In this case, the first law can be expressed in terms of the enthalpy

$$H_1 + Q + W = H_2,$$

and enthalpy is conserved if no heat or work is given to the system.

Since $\dot{d}q = TdS$ for a reversible process, dU and dH quantifies the heat exchange under constant volume and pressure. They are conserved for adiabatic processes ($dS = 0$) under constant volume or constant pressure. The heat capacities are easily measurable, and they are defined as

$$C_x = \left(\frac{\dot{d}q}{dT} \right)_x = T \left(\frac{\partial S}{\partial T} \right)_x,$$

where x is the quantity held constant. Under constant pressure volume or pressure, these can be related to U and H as

$$C_V = \left(\frac{\partial U}{\partial T} \right)_V, \quad C_p = \left(\frac{\partial H}{\partial T} \right)_p.$$

For an isentropic change, $dU = \dot{d}w$, and U truly behaves like an energy. However, since T are not natural coordinates of U and H , these are more useful experimentally.

In situations with varying particle numbers (such as phase transition), the chemical potential

$$\mu = \frac{G}{N}$$

is often useful. It is related to the total differential of G as

$$dG = Vdp - SdT + \mu dN = \mu dN + Nd\mu.$$

Consider a two-phase (or multiple-phase in general) system. At equilibrium, the chemical potential of two phases must be equal ($dG = 0$), which can be used to solve for the pressure distribution of the isothermal atmosphere (or contact potential) after including the gravitational potential energy in U . The same idea is useful in studying phase transition.

4.2 Free energy and availability

By definition, a surrounding is large enough so that its intensive variables p_0 and T_0 does not change in equilibrium. Then the second law requires $T_0 dS \geq dq$, which can be combined with the first law to yield

$$dW_{\text{non-}pV} = dW + p_0 dV \geq dA,$$

where

$$A = U + p_0 V - T_0 S, \quad dA = dU + p_0 dV - T_0 dS,$$

is the availability of the system. Note that this is quite similar to the definition of G , just that T_0 and p_0 are properties of the surrounding, not the system itself. This leads to differences in their differentials.

If we want to extract work from the system, then dw is negative and dA gives the maximum amount of work extractable from the system. Under constant temperature and volume, for example, notionally the maximum work that can be harnessed is the drop in potential energy ΔU (consider a mass dropping from a mountain). If this process has intrinsic entropy change (like in a electrochemical reaction), we could allow heat flow from the surrounding and convert it to work till the point that the entropy change of the universe is zero and the process becomes reversible. The maximum work extractable is then given by the drop in F .

Similarly, if the system is mechanically isolated with $dw_{\text{non-}pV} = 0$, we must have

$$dA \leq 0,$$

Therefore, an isolated system always tries to minimise A . Irreversibility arises during this process, but again this can be harnessed and make the whole process reversible (In a reversible evaporation process (T constant), for example, $\Delta G = 0$, and the maximum work done (including pV work) is $-\Delta F$.) Under different constraints, dA is equivalent to other thermodynamic variables that we try to extremise.

- Isolated with fixed volume ($dU = dV = 0$)

$$dA = -T_0 dS \implies \underline{dS \geq 0};$$

- Fixed volume at constant temperature ($dV = dT = 0$)

$$dA = dF \implies \underline{dF \leq 0};$$

- Constant pressure and temperature ($dp = dT = 0$)

$$dA = dG \implies \underline{dG \leq 0}.$$

Under constant T , $-\Delta F$ gives the maximum work done by the system, including any pV work in a reversible process. If no work is done and V is a constant, then the process is irreversible and

$$dS_{\text{tot}} = -\frac{dF}{T}.$$

Under constant T and p , $-\Delta G$ gives the maximum non- pV work done by the system in a reversible process. If no non- pV work is done, the process is irreversible and

$$dS_{\text{tot}} = -\frac{dG}{T}.$$

Furthermore, if heat flow is allowed in the flow process, then $G_1 = G_2$ when no work is done on the system under constant temperature.

Why do we define $dF = dU - T_0 dS - S dT$ in p.p.178 of Blundell, not the normal $dF = dU - T dS - S dT$?

4.3 Examples

For an ideal gas,

$$S(T, V) = n(C_{V,m} \ln T + R \ln(V/n) + S_0),$$

The isothermal and adiabatic compressibilities are related by

$$\frac{\kappa_T}{\kappa_S} = \frac{\left(\frac{\partial V}{\partial p}\right)_T}{\left(\frac{\partial V}{\partial p}\right)_S} = \frac{C_p}{C_V} = \gamma.$$

The constant pressure and constant volume heat capacities are related by

$$C_p - C_V = T \left(\frac{\partial p}{\partial T}\right)_V \left(\frac{\partial V}{\partial T}\right)_p.$$

The pressure distribution of an isothermal atmosphere is

$$p(h) = p_0 \exp\left(-\frac{m_r g h}{RT}\right),$$

which can be obtained from setting the chemical potential $\mu(h)$ to be uniform.

4.4 Thermodynamics of other systems

The ideas and techniques of thermodynamics can be used to study other systems with a large number of particles, such as rubber molecules, liquid molecules, or magnetic dipoles. In these systems, instead of (only) having the $-pdV$ work, other forms of work

$$dW = X dx,$$

may be of interest, such as $dW = -\mathbf{m} \cdot d\mathbf{B}$ for magnets, $dW = f dL$ for an elastic rod, or $dW = \gamma dA$ for a liquid. We can also introduce the equivalence of free energy or enthalpy to calculate “useful work.”

4.4.1 Elastic rod

For an elastic rod, the first law becomes

$$dU = T dS + f dL.$$

For example, the entropy of the change as length at a constant temperature as

$$\left(\frac{\partial S}{\partial L}\right)_T = A E_T \alpha_f = \left(\frac{\partial f}{\partial L}\right)_T \left(\frac{\partial L}{\partial T}\right)_f.$$

This is positive for metallic bars, as pulling the bar distorts the crystal. Notably, for a rubber band, the expansivity α_f is negative, as pulling actually decreases the entropy by aligning the rubber molecules. This also means that a rubber band heats up in an adiabatic expansion.

4.4.2 Surface tension

For a liquid, the intermolecular attraction is isotropic in the bulk but points towards the inside of liquid near the surface. This gives rise to surface tension, making

$$dW = \gamma dA.$$

At equilibrium, the pressure difference supports the surface tension (the principle of virtual work):

$$dW = p dV = \gamma dA,$$

giving $p - p_{\text{atm}} = 2\gamma/r$ for a droplet. Expansion of the surface area requires injection of heat and would increase the entropy.

4.4.3 Paramagnetism

A magnet consists many magnetic spins, pointing up or down. Magnetic susceptibility of a sample decreases as temperature increases due to Curies' law, giving

$$\left(\frac{\partial\chi}{\partial T}\right)_B < 0$$

and consequently

$$\left(\frac{\partial S}{\partial B}\right)_T < 0, \quad \left(\frac{\partial T}{\partial B}\right)_S > 0.$$

Therefore, isothermal magnetisation emits heat while adiabatic magnetisation heats the magnet up. Microscopically, this is because an external magnetic field aligns the spins, therefore decreasing the entropy. During adiabatic demagnetisation, entropy of the spins increases due to less alignment. However, since the total change of entropy is 0, the entropy of phonon (lattice vibration) must decrease, bringing the temperature down.

The combination of isothermal magnetisation and adiabatic demagnetisation can cool a system down to millikelvins. The system is first magnetised in a heat bath of liquid helium to about 4 Kelvin, after which it is isolated and the magnetic field is brought down.

Magnetisation of sample brings down entropy (the spins line up with B .) Adiabatic demagnetisation works because decreasing field increases entropy due to spins, but adiabatic \Rightarrow entropy of phonons (lattice vibration) decreases, cooling the sample.

5 Phase Transition

5.1 Real gases

Ideality of gas assumes that the gas molecules have no volumes and no intermolecular interactions. In reality, the long-range forces (van de Waals force, for example) drag the molecules together and the finite size of molecules reduces the available space for them to jiggle. We thus want to modify the ideal gas law $p_i V_{mi} = RT$, where the subscript m denotes molar quantity and i denotes ideality. There are different phenomenological models to express p_i and V_{mi} using the measurable p and V_m (note that we assume them to be equal in the ideal gas law).

To account for the finite size of molecule sizes, we simply let $V_i = V - b$, where b is a parameter to be fixed, making the available volume less than the actual volume of the container. The **van de Waals** model of real gas accounts for the intermolecular attraction by $p_i = p + a/V_m^2$, reducing the actual pressure by the long-range attraction. The $1/V_m^2$ form of the pressure reduction can be rationalised by approximating the net interaction potential U as proportional to the number of particles $\propto n$ multiplied by the number of nearest neighbouring paris $\propto n/V$ with the strongest interaction: $U = -an^2/V$ The associated effective pressure ($p_i + p_{\text{eff}} = p$) can be determined by $-p_{\text{eff}}dV = dU$, giving the equation of state

$$\boxed{\left(p + \frac{a}{V_m^2}\right)(V_m - b) = RT.} \quad (1)$$

Eq.(1) cannot be solved explicitly (easily) for V , but it is relatively easy to give an explicit expression for p as

$$p(V, T) = \frac{RT}{V - b} - \frac{a}{V^2}.$$

Often we want to use p as our “subject variable” by performing the relevant math trick. For example,

$$\left(\frac{\partial V}{\partial p}\right)_T = \left(\frac{\partial p}{\partial V}\right)_T^{-1}.$$

Various thermodynamic quantities can be obtained from Eq.(1) from chain rules and the Maxwell relations. For example, the entropy is

$$\begin{aligned} dS &= \left(\frac{\partial S}{\partial T}\right)_V dT + \left(\frac{\partial S}{\partial V}\right)_T dV \\ &= \frac{C_V}{T} dT + \left(\frac{\partial p}{\partial T}\right)_V dV, \end{aligned}$$

where the second line follows from a Maxwell's relation. The equation of state for a van de Waals gas then gives

$$S = C_V \ln T + R \ln(V - b) + \text{const},$$

which is independent of a since entropy only cares about the allowed space for different configurations. We can also evaluate

$$\Delta U = a \left(\frac{1}{V_1} - \frac{1}{V_2} \right),$$

which is independent of b since it only cares about intermolecular interactions.

5.2 Phase transition of gas to liquid

Eq.(1) is in general cubic in V , as shown in Fig.1, so the isotherms might adopt an S-shaped curve with two extrema. This isn't allowed in *equilibrium* thermodynamics, as the isothermal compressibility

$$\kappa_T = -\frac{1}{V} \left(\frac{\partial V}{\partial p} \right)_T$$

should always be positive. This means a positive fluctuation in p expands the gas, making it unstable in a positive feedback loop. At equilibrium, the Gibbs free energy would always be minimised in a constant pressure and temperature experiment, moving along ABC in the $G-p$ plot. The turning point B corresponds is multivalued in the $V-p$ plot and can thus be interpreted as *two phases in equilibrium*: the one on the branch with large volume and large compressibility is gas and the other is liquid. It is worth reiterating that this **phase transition** does not emerge in the ideal gas assumption because intermolecular interaction, which is neglected in gas, cannot be neglected in liquid.

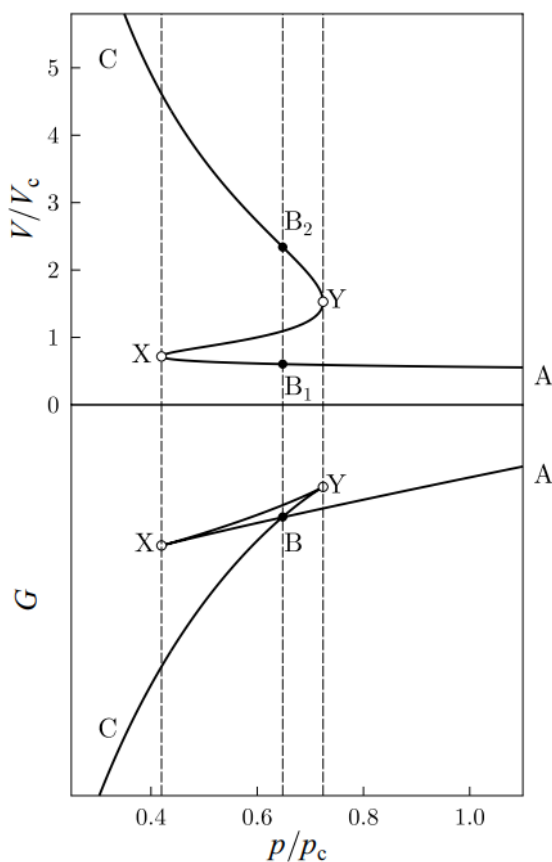


Fig. 26.3 The behaviour of the volume V and Gibbs function G of a van der Waals gas as a function of pressure at $T = 0.9T_c$.

Figure 1: Sub-critical van de Waals isotherm. The kinetically feasible path $AXYC$ is different from the thermodynamically stable path AB_1B_2C (Blundell and Blundell, p.p.301)

At the transition point B , the Gibbs energy has a double well profile (corresponding to the gas and liquid) with equal depth in the phase space, which becomes biased as one deviates from the equilibrium pressure or volume of coexistence. As one contracts the gas, the gas is stuck at the shallower well that is closer to its original gaseous phase going past the equilibrium volume, giving rise to supercooling along CY . The equilibrium is prevented because of an energy barrier between the two phases and the gas is in a **metastable phase**. However, once a perturbation energy is given, the supercooled gas will return to the equilibrium gas phase, corresponding to a vertical line in the phase diagram. Note that only at B can there be two phases coexisting at equilibrium, and supercooling/superheating are just metastable phases with a higher Gibbs free energy.

The critical point for phase transition B can be determined by the single-valuedness of G at this point: $G(B_1) = G(B_2)$. Since G is also state function with $V = (\partial G / \partial p)_T$, the change in G along B_1XYB_2 must also be 0:

$$\int_{B_1}^{B_2} V dp = 0,$$

giving the **Maxwell construction of equal area**.

The coordinates (p , V , T) at the coexistence point B can be used to plot a phase diagram for the gas and liquid. However, the occurrence of a phase transition requires the S -shaped profile of isotherms in the first quadrant, which is only feasible up to a critical T_c , mathematically determined by finding the point of inflexion of the isotherm:

$$\left[\left(\frac{\partial p}{\partial V} \right)_T = 0 \right]_{T=T_c}, \quad \left[\left(\frac{\partial^2 p}{\partial V^2} \right)_T = 0 \right]_{T=T_c}$$

There is no phase transition at a higher temperature and the distinction between phases ceases to exist, giving supercritical liquids.

There are other phenomenological models of the real gas. For example, the Dieterici equation takes the boltzmann distribution into consideration, giving

$$p(V_m - b) = RT \exp \left(-\frac{a}{RTV_m} \right).$$

A useful quantity to test ideality is the compressibility factor

$$Z = \frac{pV_m}{RT},$$

which is unity for the ideal gas. At the critical point, $Z = 3/8$ for van de Waals gas and $Z \approx 0.27$ for Dieterici gas.

Motivated by this factor, we can also model real gas via the virial expansion

$$Z = 1 + \frac{B'}{V_m} + 1 + \frac{C'}{V_m^2} + \dots = 1 + \frac{B(T)}{V_m},$$

where the infinite power series can be terminated at the first term by giving $B(T)$ a temperature dependence. $B = 0$ for an ideal gas, but there is a finite temperature T_B (called the **Boyle temperature**) at which $B = 0$ again (this is a result of the Leonard-Jones potential).

5.3 The law of corresponding states

The empirical parameters a and b in van de Waals equation differ from gas to gas, but the gas's property can be fully specified by the position and depth of the potential well. Therefore, all gases are the same in the reduced phase coordinates V/V_c , p/p_c , and T/T_c (two degrees of freedom for the intermolecular interaction and one more for the sizes of the particles). However, the quantum mechanical effects prominent in hydrogen and helium breaks this law.

5.4 Cooling real gases: Joule-Kelvin expansion

Ideality of the gas assumes that its internal energy U only depends on the temperature T . For an ideal gas, its temperature does not change during a Joule expansion which is adiabatic with no external work,

giving

$$\boxed{\mu_J \equiv \left(\frac{\partial T}{\partial V}\right)_U = -\frac{1}{C_V} \left(\frac{\partial U}{\partial V}\right)_T = -\frac{1}{C_V} \left[T \left(\frac{\partial p}{\partial T}\right)_V - p\right] = 0.}$$

For a van de Waals gas, however, it will cool during expansion with

$$\mu_J = -\frac{a}{C_V V^2}, \implies \Delta T = -\frac{a}{C_V} \left(\frac{1}{V_1} - \frac{1}{V_2}\right) < 0$$

Similarly, an isothermal expansion of van de Waals gas increases its potential energy as

$$\Delta U = a \left(\frac{1}{V_1} - \frac{1}{V_2}\right) > 0.$$

Cooling via Joule expansion is not useful in practice, and we're interested in a constant-enthalpy flow process, thus defining the Joule-Kelvin coefficient

$$\mu_{JK} = \left(\frac{\partial T}{\partial p}\right)_H.$$

From a similar manipulation as that for the Joules coefficient,

$$\mu_{JK} = -\frac{1}{C_p} \left(\frac{\partial H}{\partial p}\right)_T = \frac{1}{C_p} \left[T \left(\frac{\partial V}{\partial T}\right)_p - V\right]$$

which can be either positive or negative, though the entropy change is positive definite. Whether we get a cooling or heating from the Joule-Kelvin expansion depends on the exact p and T , but there is a maximum temperature for cooling to happen, known as the ***inversion temperature***, below which it is feasible to cool the gas by throttling like this.

The inversion temperature T_C is the temperature at which $\mu_{JK} = 0$, determined by

$$T \left(\frac{\partial V}{\partial T}\right)_p - V = 0 \implies -\frac{\left(\frac{\partial p}{\partial T}\right)_V}{\left(\frac{\partial p}{\partial V}\right)_T} = \frac{V}{T}.$$

This is a curve for a real gas with a maximum inversion temperature above which the Joule-Kelvin flow process only heats the gas. But for a van de Waals gas, the inversion temperature is $T_C = 2T_B$, a constant at all pressure, where T_B is the Boyle temperature ($T_B = \frac{a}{bR}$ for a van de Waals gas).

In practice, we can liquefy different gas in a sequence, starting with the species with highest inversion temperature. In the flow process, high-pressure gas is injected while liquid and gas at atmospheric pressure is ejected. The maximum efficiency of liquefaction occurs when

$$\left(\frac{\partial H_{\text{in}}}{\partial p_{\text{in}}}\right)_{T_{\text{in}}} = 0,$$

along the inversion temperature line with $\mu_{JK} = 0$, echoing the line that maximum efficiency is gained only in a reversible process.

5.5 Phase Transition

The continuous change of entropy as temperature increases is characterised by the heat capacity, but often the entropy changes discontinuously at a phase boundary, giving rise to latent heat

$$\boxed{L = T_C \Delta S},$$

where T_C is the temperature of phase transition. The change in entropy from liquid to vapour can be estimated by the change in density of states

$$\frac{\Omega_{\text{vapour}}}{\Omega_{\text{liquid}}} = \frac{\rho_{\text{liquid}}}{\rho_{\text{vapour}}}^{N_A},$$

giving a rough estimate

$$L \approx 10RT_C.$$

In equilibrium under constant p and T , a phase minimises its Gibbs free energy, as discussed in 4.2. Therefore, if two phases are in equilibrium, $dG = 0$ for an infinitesimal change from phase 1 to phase 2, giving $\mu_1 = \mu_2$. This holds for any p and T , giving the **Clausius-Clapeyron equation**

$$d\mu_1 = d\mu_2, \quad \Rightarrow \quad \boxed{\frac{dp}{dT} = \frac{\Delta s}{\Delta v} = \frac{l}{T\Delta v}},$$

where the lowercase letters represent quantities per particle.

5.5.1 Integration of Clausius-Clapeyron equation

The Clausius-Clapeyron equation can be integrated under different assumptions to give phase boundaries of different transitions.

For solid to gas or liquid to gas transitions, we often assume

- $V_{\text{gas}} \gg V_{\text{liquid}} \approx V_{\text{solid}} \Rightarrow \Delta V \approx V_{\text{gas}}$
- $p \ll p_{\text{critical}}$ so that the pressure of gas can be modelled by the ideal gas equation $pv = RT$;
- (weaker) L is constant along the boundary.

These gives

$$\frac{dp}{dT} = \frac{Lp}{RT^2} \Rightarrow \underline{p(T) = p_0 \exp\left(-\frac{L}{RT}\right)}.$$

For solid to liquid transitions, the ideal gas law is no longer applicable. Instead, we just assume that

- ΔV is constant along the boundary, which can be calculated by the difference in densities;
- (weaker) L is constant along the boundary.

The assumption of constant L can be relaxed in the liquid-gas and solid-gas transition, as its temperature dependence can be calculated explicitly by noting

$$\begin{aligned} \frac{d\Delta S(p, T)}{dT} &= \frac{d}{dT} \left(\frac{L}{T} \right) = \frac{1}{T} \frac{dL}{dT} - \frac{L}{T^2}, \\ \Rightarrow \underline{L} &= \underline{L_0 + (C_{pg} - C_{pL})T}. \end{aligned}$$

5.5.2 Phase Diagram

See Blundell and Blundell p.p.327 for an ideal phase diagram. Near the triple point, we should expect

$$L_{sg} = L_{sl} + L_{lg}.$$

The volume change from solid to liquid is usually small, giving the steep boundary between solid and liquid. This slope is usually positive, since liquid is less dense than solid, with the notable exception of water due to hydrogen bonding. The phase boundary between solid and gas and liquid and gas takes the same functional form, with a change in the derivative at the triple point due to the change in L . The pressure of the liquid-gas boundary can be interpreted as the “vapour pressure,” as

The phase change from solid to liquid is inherently discontinuous and involve breakage of symmetry. This does not need to be the case for a liquid to gas transition or other transitions.