

# Thermodynamics of Materials AD19:

## Class Activity 03

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R. Gaskell, D., & E. Laughlin, D. (2018). Introcuction to the Thermodynamics of Materials. (C. Press, Ed.). Taylor & Francis Group.

## Binary Phase Diagrams

In [1]:

```
# PYTHON LIBRARIES
%matplotlib inline

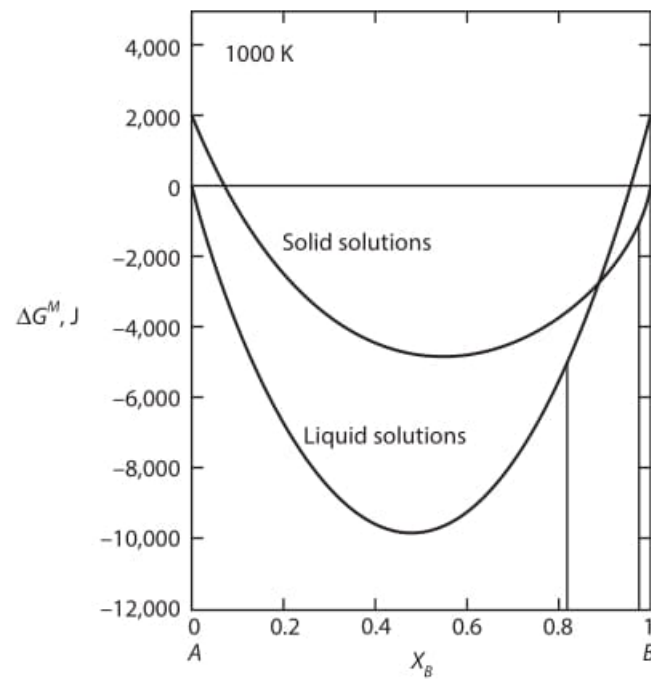
import numpy as np
np.seterr(divide='ignore', invalid='ignore')
import pandas as pd
import matplotlib.pyplot as plt
plt.rc('xtick', labels=15)
plt.rc('ytick', labels=15)

from IPython.display import display, Image
from scipy.optimize import least_squares, fsolve, curve_fit
```

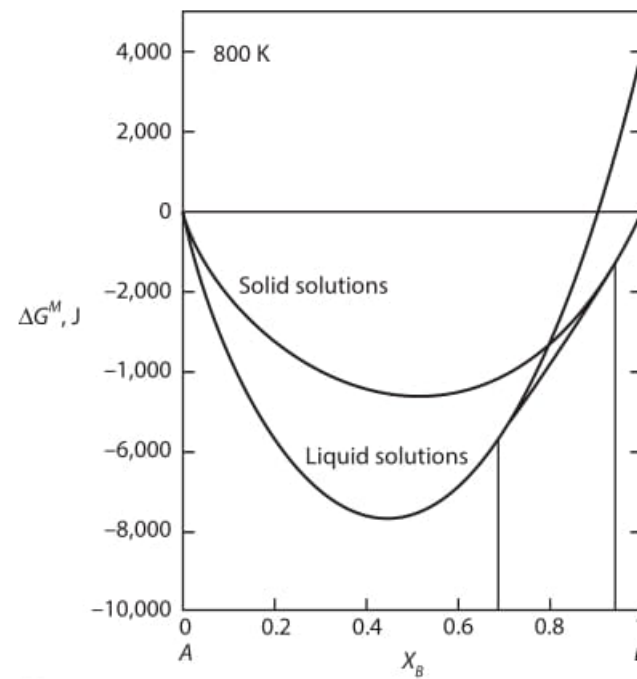
Let's reproduce Gaskell's plots:

In [2]:

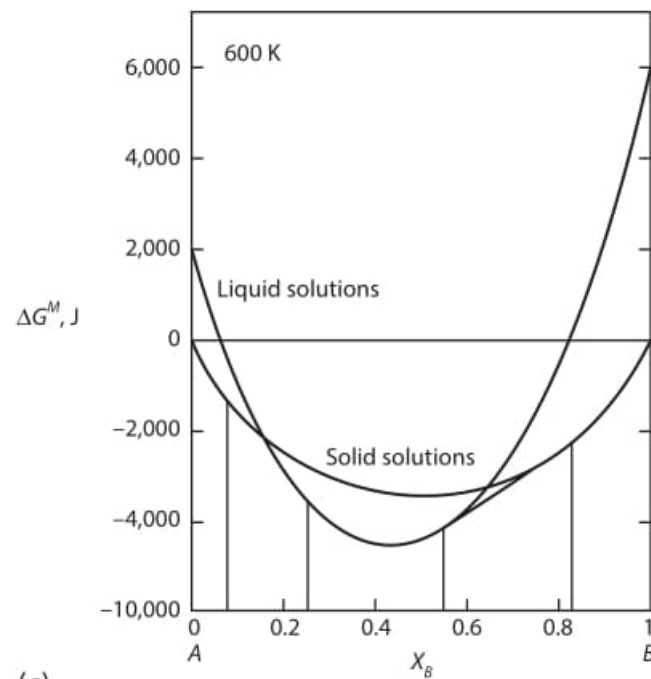
```
display(Image(filename='./img/ITTTOM-378.jpg'))
```



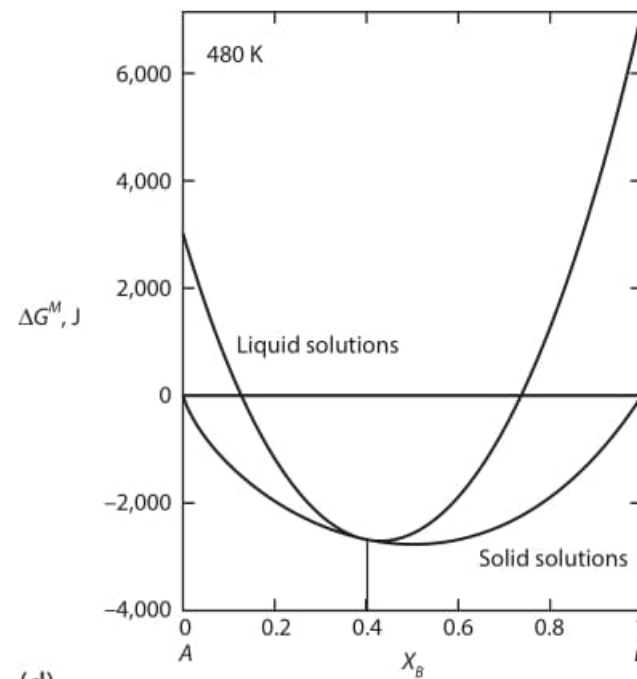
(a)



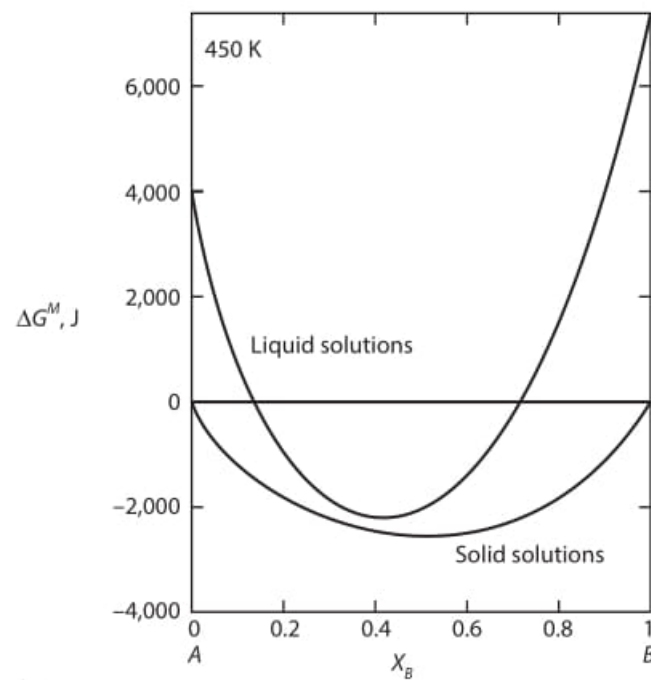
(b)



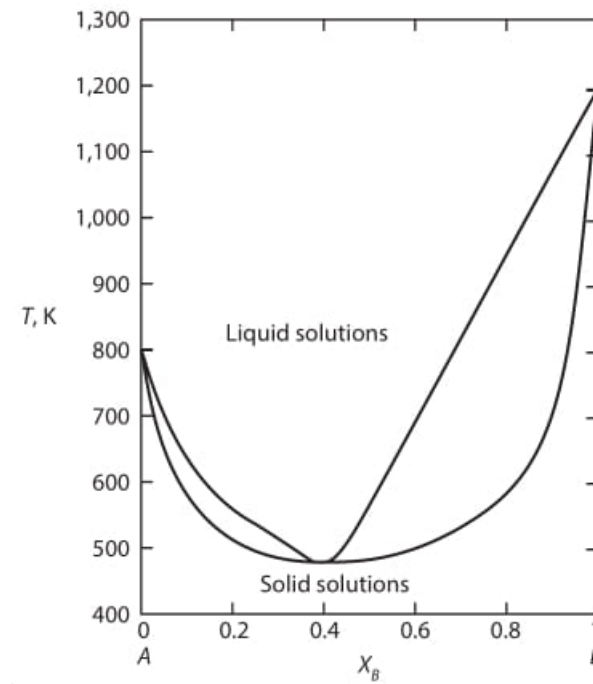
(c)



(d)



(e)



(f)

**Figure 10.24** The molar Gibbs free energy of mixing curves at various temperatures, and the phase diagram for a binary system which forms regular solid solutions in which  $\alpha_s = 0$  and regular liquid solutions in which  $\alpha_l = -20,000$  J.

$$\begin{aligned} \Delta G_{m,A} &= 8000 - 10 T \text{ [J/mol]} & \Delta G_{m,B} &= 12000 - 10 T \text{ [J/mol]} & \Omega_l &= -20000 \text{ [J/mol]} & \Omega_s &= 0 \text{ [J/mol]} \\ \Delta G_s &= -x_A \Delta G_{m,A} + R T (x_A \ln x_A + x_B \ln x_B) + \Omega_s x_A x_B & \Delta G_l &= x_B \Delta G_{m,B} + R T (x_A \ln x_A + x_B \ln x_B) + \Omega_l x_A x_B & G_{B,s} &= 0 & G_{A,l} &= 0 \end{aligned}$$

Substituting numerical values ...

if  $T$  greater than  $T_{m,(A)}$  and lower than  $T_{m,(B)}$  then, the liquid is chosen as the standard state for  $A$ , and the solid is chosen as the standard state for  $B$

$$\begin{aligned} \Delta G_l &= x_B (12000 - 10 T) + R T (x_A \ln x_A + x_B \ln x_B) - 20000 x_A x_B & \frac{d \Delta G_l}{d x_B} &= R T (\ln x_B - \ln x_A) - 10 T - 20000 x_A + 20000 x_B + 12000 \\ \Delta G_s &= -x_A (8000 - 10 T) + R T (x_A \ln x_A + x_B \ln x_B) & \frac{d \Delta G_s}{d x_B} &= R T (\ln x_B - \ln x_A) - 10 T + 8000 \end{aligned}$$

**else if  $T < T_{m,A}$  and  $T < T_{m,B}$  then, solid is chosen as the standard state**  
 $\Delta G_l = x_A (8000 - 10 T) + x_B (12000 - 10 T) + R T (x_A \ln x_A + x_B \ln x_B) - 20000 x_A x_B$   
 $\frac{d \Delta G_l}{d x_B} = R T (\ln x_B - \ln x_A) - 20000 x_A + 20000 x_B + 4000$   
 $\frac{d \Delta G_s}{d x_B} = R T (\ln x_B - \ln x_A)$

**else (if  $T > T_{m,A}$  and  $T > T_{m,B}$  then), liquid is chosen as the standard state**  
 $\Delta G_l = R T (x_A \ln x_A + x_B \ln x_B) - 20000 x_A x_B$   
 $\frac{d \Delta G_l}{d x_B} = R T (\ln x_B - \ln x_A) - 20000 x_A + 20000 x_B$   
 $\Delta G_s = -x_A (8000 - 10 T) - x_B (12000 - 10 T) + R T (x_A \ln x_A + x_B \ln x_B)$   
 $\frac{d \Delta G_s}{d x_B} = R T (\ln x_B - \ln x_A) - 4000$

In [3]:

```
#-----#
### GIBBS FREE ENERGIES OF MIXING for the LIQUID SOLUTIONS ###
#-----#

def DG_l(xb, T):
    R = 8.31446261815324
    xa = 1 - xb
    if (T >= 800 and T <= 1200):
        return xb*(12000 - 10*T) + R*T*(xa*np.log(xa) + xb*np.log(xb)) - 20000*xa*xb ###
    elif (T <= 800 and T <= 1200):
        return (12000 - 10*T)*xb + (8000 - 10*T)*xa + R*T*(xa*np.log(xa) + xb*np.log(xb)) - 20000*xa*xb ###
    else:
        return R*T*(xa*np.log(xa) + xb*np.log(xb)) - 20000*xa*xb ###

def d_DG_l(xb, T):
    R = 8.31446261815324
    xa = 1 - xb
    if (T >= 800 and T <= 1200):
        return 12000 - 10*T - 20000*xa + 20000*xb + R*T*(- np.log(xa) + np.log(xb)) ###
    elif (T <= 800 and T <= 1200):
        return 4000 - 20000*(1-xb) + 20000*xb + R*T*(np.log(xb) - np.log(xa)) ###
    else:
        return R*T*(np.log(xb) - np.log(xa)) - 20000*xa + 20000*xb ###

#-----#
### GIBBS FREE ENERGIES OF MIXING for the SOLID SOLUTIONS ###
#-----#

def DG_s(xb, T):
    R = 8.31446261815324
    xa = 1 - xb
    if (T >= 800 and T <= 1200):
        return - xa*(8000 - 10*T) + R*T*(xa*np.log(xa) + xb*np.log(xb)) ###
    elif (T <= 800 and T <= 1200):
        return R*T*(xa*np.log(xa) + xb*np.log(xb)) ###
    else:
        return -xa*(8000 - 10*T) - xb*(12000 - 10*T) + R*T*(xa*np.log(xa) + xb*np.log(xb)) ###

def d_DG_s(xb, T):
    R = 8.31446261815324
    xa = 1 - xb
    if (T >= 800 and T <= 1200):
        return 8000 - 10*T + R*T*(- np.log(xa) + np.log(xb)) ###
    elif (T <= 800 and T <= 1200):
        return -4000 + R*T*(np.log(xb) - np.log(xa)) ###
    else:
        return -R*T
```

```

elif (T <= 800 and T <= 1200):
    return R*T*(np.log(xb) - np.log(xa)) ###
else:
    return R*T*(np.log(xb) - np.log(xa)) - 4000 ###

```

The tangents are depicted as:

```

y_tan_l = d_DG_l_(x10, T) * (xb - x10) + DG_l_(x10, T)
y_tan_s = d_DG_s_(xs0, T) * (xb - xs0) + DG_s_(xs0, T)

```

function

```

phaseDiagram

```

is to find the common tangent(s),  $y_{\{tan,l\}} = y_{\{tan,s\}}$  at  $x_B = 0$ . So, let's find some  $x_{\{l,0\}}$  and  $x_{\{s,0\}}$  to satisfy that:

```

d_DG_l_(x1, T) - d_DG_s_(x2, T) = 0
d_DG_l_(x1, T)*(x1 - x2) - (DG_l_(x1, T) - DG_s_(x2, T)) = 0

```

Get compositions in equilibrium from a given temperature

In [4]:

```

def phaseDiagram(T):
    #y_tan_l = d_DG_l_(x10, T) * (xb - x10) + DG_l_(x10, T)
    #y_tan_s = d_DG_s_(xs0, T) * (xb - xs0) + DG_s_(xs0, T)

    f1 = lambda x: DG_l_(x, T)
    df1 = lambda x: d_DG_l_(x, T)
    f2 = lambda x: DG_s_(x, T)
    df2 = lambda x: d_DG_s_(x, T)

    def eqns(x):
        x1, x2 = x[0], x[1]
        eq1 = df1(x1) - df2(x2)
        eq2 = df1(x1)*(x1 - x2) - (f1(x1) - f2(x2))
        return [eq1, eq2]

    from scipy.optimize import least_squares
    lowerbound = 0.0000001
    upperbound = 0.9999999
    lb = (lowerbound, lowerbound) # lower bounds on x1, x2
    ub = (upperbound, upperbound) # upper bounds

    x0 = least_squares(eqns, [0.01, 0.01], bounds=(lb, ub)) # liquid xs
    x1 = least_squares(eqns, [0.99, 0.99], bounds=(lb, ub)) # solid xs

    #print(x0.x, x1.x)
    return x0.x[0], x0.x[1], x1.x[0], x1.x[1]

```

# PLOT Gibbs Curves

In [5]:

```
def gibbsCurves(T):
    xb = np.linspace(0.0, 1.0, 1000)
    comp = phaseDiagram(T);

    # PLOT FIG
    scale = 6;
    fig, ax = plt.subplots(figsize=(3*scale, 2*scale));

    # Plot
    #plt.scatter(T, C, s=25, color='red', label='Raw data');
    x = xb
    yl = DG_l_(xb, T)
    plt.plot(x, yl, '-', linewidth=3, label='liquid solutions')

    x = xb
    ys = DG_s_(xb, T)
    plt.plot(x, ys, '-', linewidth=3, label='solid solutions')

    # A, } JXJJHYy * pVeM6
    ax.set(autoscale_on=False)
    ax.set_xticks(ax.get_xticks()[::100]) # remove unnecessary ticks
    ax.ticklabel_format(useOffset=False) # disable scientific notation
    plt.axhline(y=0, linestyle=':', linewidth=1)

    # plot tangents
    lowerbound = 0.0000001
    upperbound = 0.9999999

    if (round(comp[0],3) > lowerbound and round(comp[1],3) < upperbound):
        # plot tangents
        y_tan_l = d_DG_l_(comp[0], T) * (xb - comp[0]) + DG_l_(comp[0], T)
        y_tan_s = d_DG_s_(comp[1], T) * (xb - comp[1]) + DG_s_(comp[1], T)
        if round(y_tan_l[0],2) == round(y_tan_s[0],2):
            plt.plot(x, y_tan_l, '--', linewidth=2)
            #plt.plot(x, y_tan_s, '--', linewidth=2)
            # add values as ticks
            extraticks=[comp[0], comp[1]]
            plt.xticks(list(plt.xticks()[0]) + extraticks)
            plt.axvline(x=comp[0], linestyle=':', linewidth=1)
            plt.axvline(x=comp[1], linestyle=':', linewidth=1)
            # add chemical potentials as legend
            plt.scatter(xb[0], yl[0], s=0, label=r'$\mu_{A,1} = $' + str(round(y_tan_l[0], 2)))
            plt.scatter(xb[0], yl[0], s=0, label=r'$\mu_{B,1} = $' + str(round(y_tan_l[len(y_tan_l)-1], 2)))

    if (round(comp[2],3) > lowerbound and round(comp[3],3) < upperbound):
        # plot tangents
        y_tan_l = d_DG_l_(comp[2], T) * (xb - comp[2]) + DG_l_(comp[2], T)
        y_tan_s = d_DG_s_(comp[3], T) * (xb - comp[3]) + DG_s_(comp[3], T)
        if round(y_tan_l[0],2) == round(y_tan_s[0],2):
            plt.plot(x, y_tan_l, '--', linewidth=2)
            #plt.plot(x, y_tan_s, '--', linewidth=2)
            # add compositions as ticks
            extraticks=[comp[2], comp[3]]
```

```

plt.xticks(list(plt.xticks()[0]) + extraticks)
plt.axvline(x=comp[2], linestyle=':', linewidth=1)
plt.axvline(x=comp[3], linestyle=':', linewidth=1)
# add chemical potentials as legend
plt.scatter(xb[0], yl[0], s=0, label=r'$\mu_{A,2} = $' + str(round(y_tan_l[0], 2)))
plt.scatter(xb[0], yl[0], s=0, label=r'$\mu_{B,2} = $' + str(round(y_tan_l[len(y_tan_l)-1], 2)))

# Print fitting parameters as plot legends
plt.scatter(xb[0], yl[0], s=0, label=r'$T = $' + str(round(T, 2)) + r'$K$')

# Display plots
plt.xlim(0.0, 1.0)
plt.yscale('linear');
plt.xlabel(r'$x_B$', fontsize=24);
plt.ylabel(r'$\Delta G$' + ' ' + r'$[J \cdot mol^{-1}]$', fontsize=24);
#plt.title('Figure 1', size=24);
plt.legend(prop={'size': 18});
display(plt);

#####
T = [1400, 1200, 1000, 800, 600, 480, 450]
for t in T:
    gibbsCurves(t)

```

<module 'matplotlib.pyplot' from 'C:\\Users\\oskat\\Anaconda3\\lib\\site-packages\\matplotlib\\pyplot.py'>

<module 'matplotlib.pyplot' from 'C:\\Users\\oskat\\Anaconda3\\lib\\site-packages\\matplotlib\\pyplot.py'>

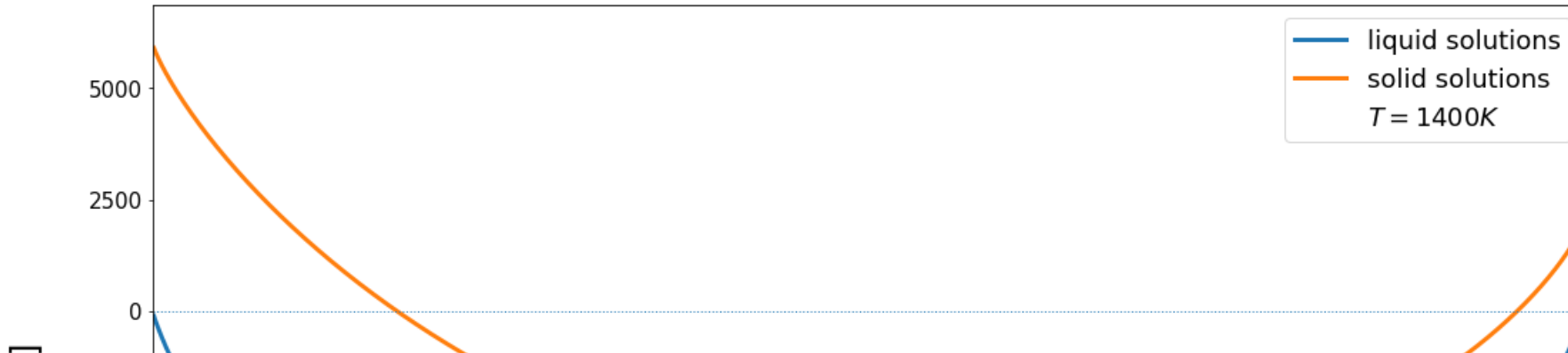
<module 'matplotlib.pyplot' from 'C:\\Users\\oskat\\Anaconda3\\lib\\site-packages\\matplotlib\\pyplot.py'>

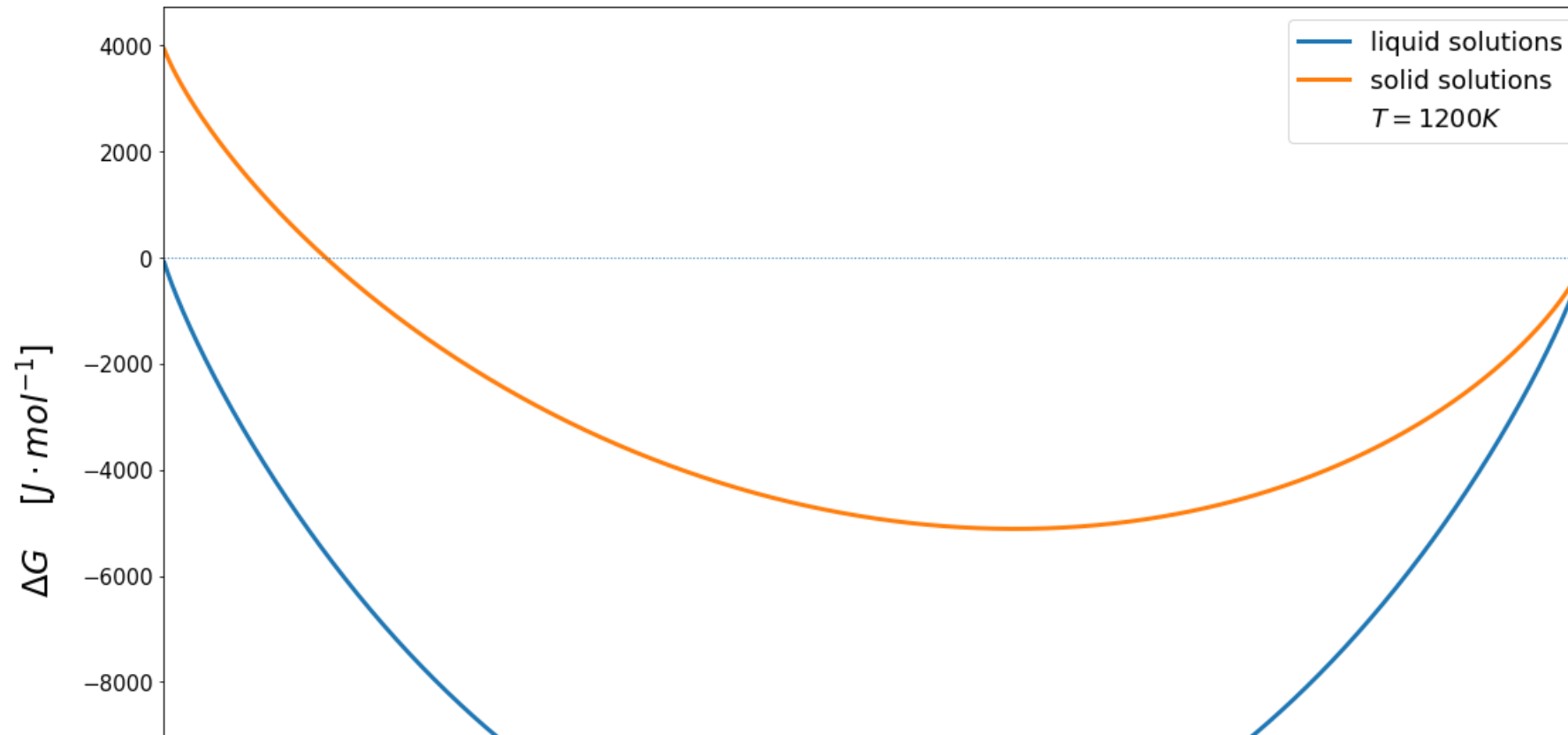
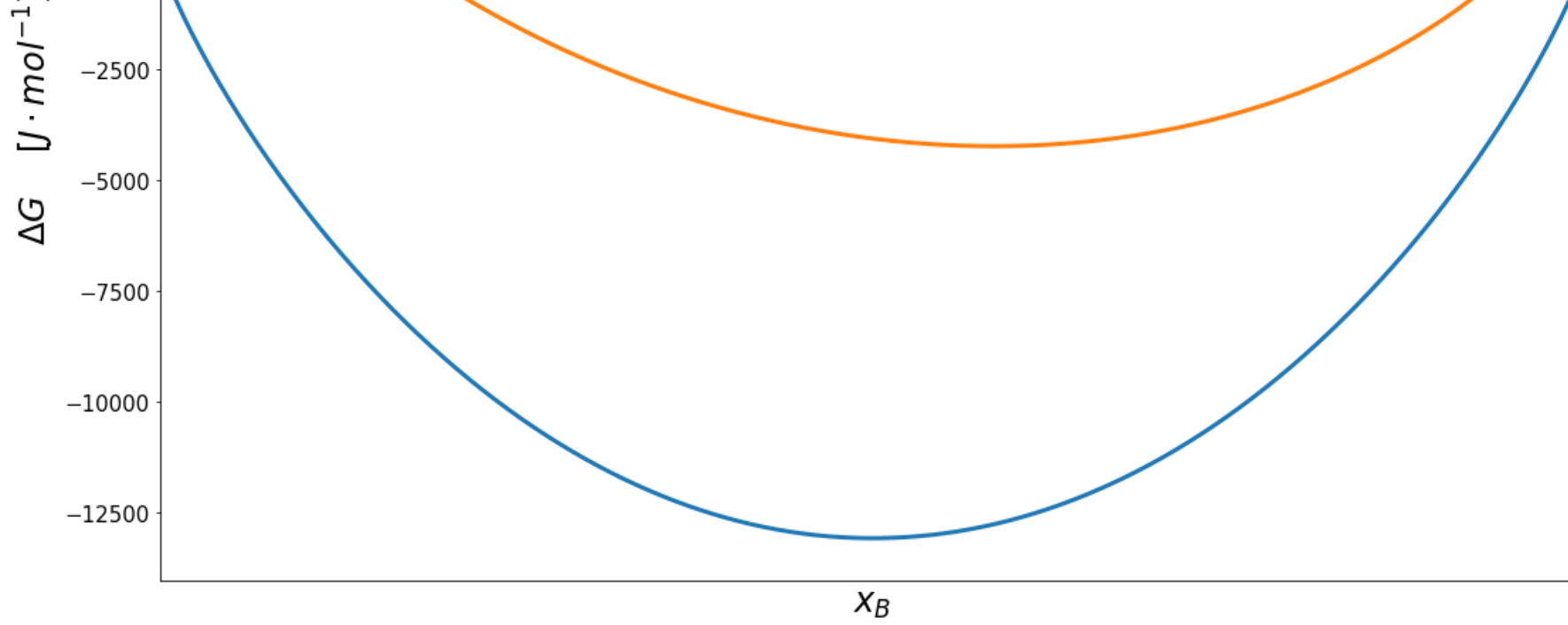
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<module 'matplotlib.pyplot' from 'C:\\Users\\oskat\\Anaconda3\\lib\\site-packages\\matplotlib\\pyplot.py'>

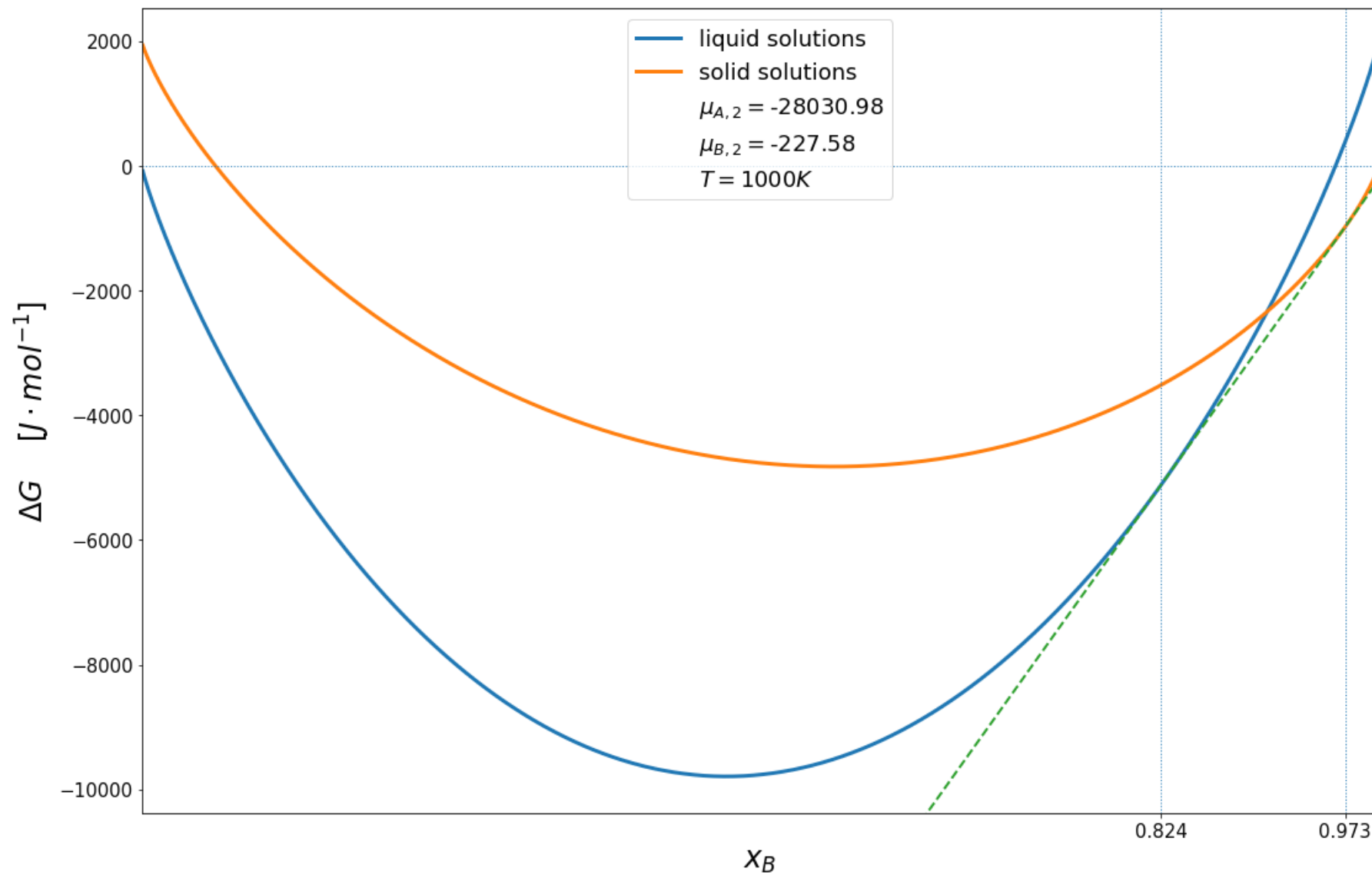
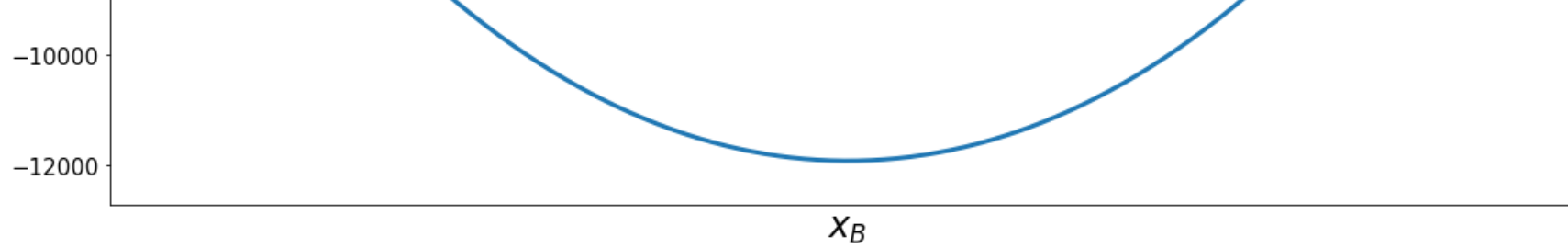
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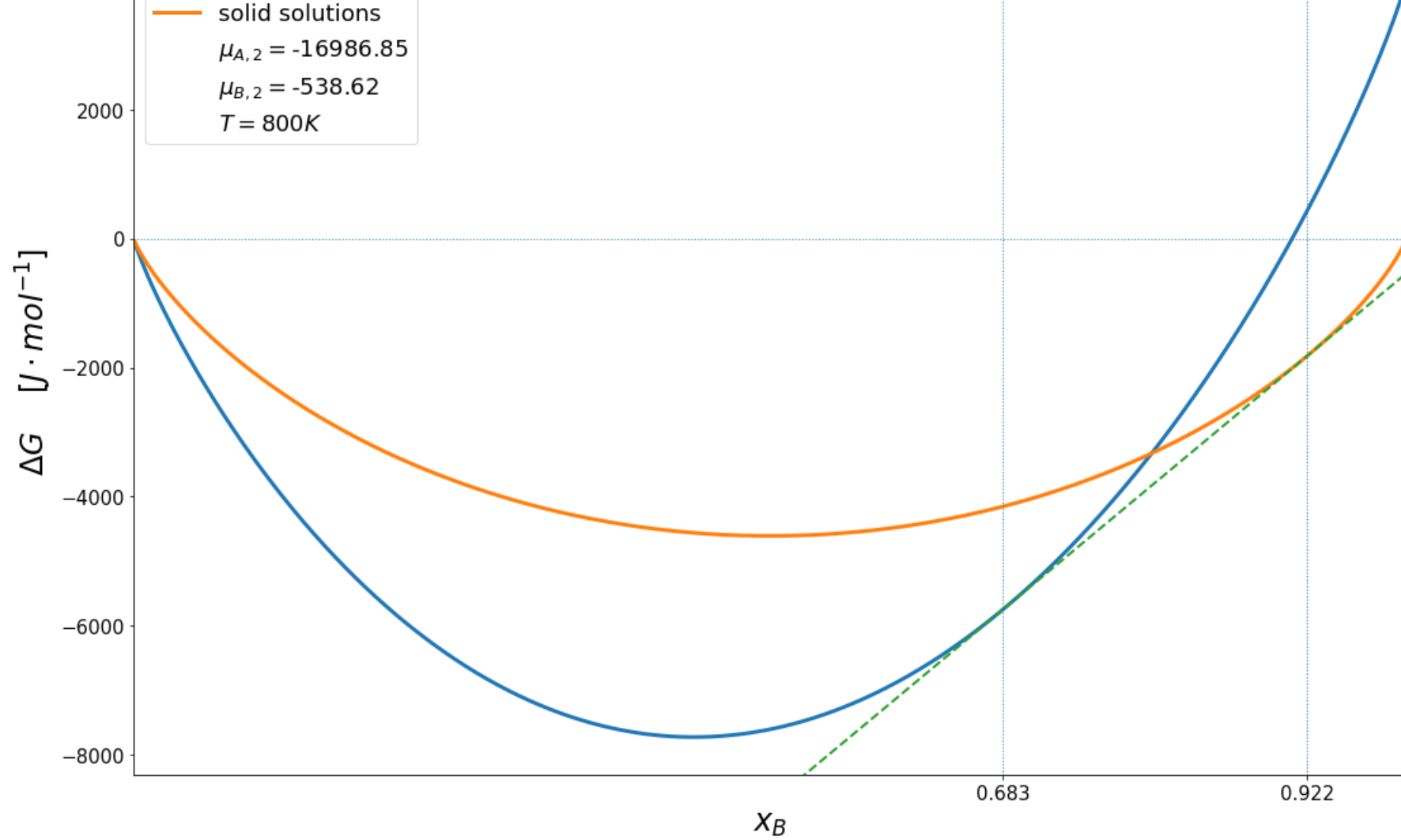
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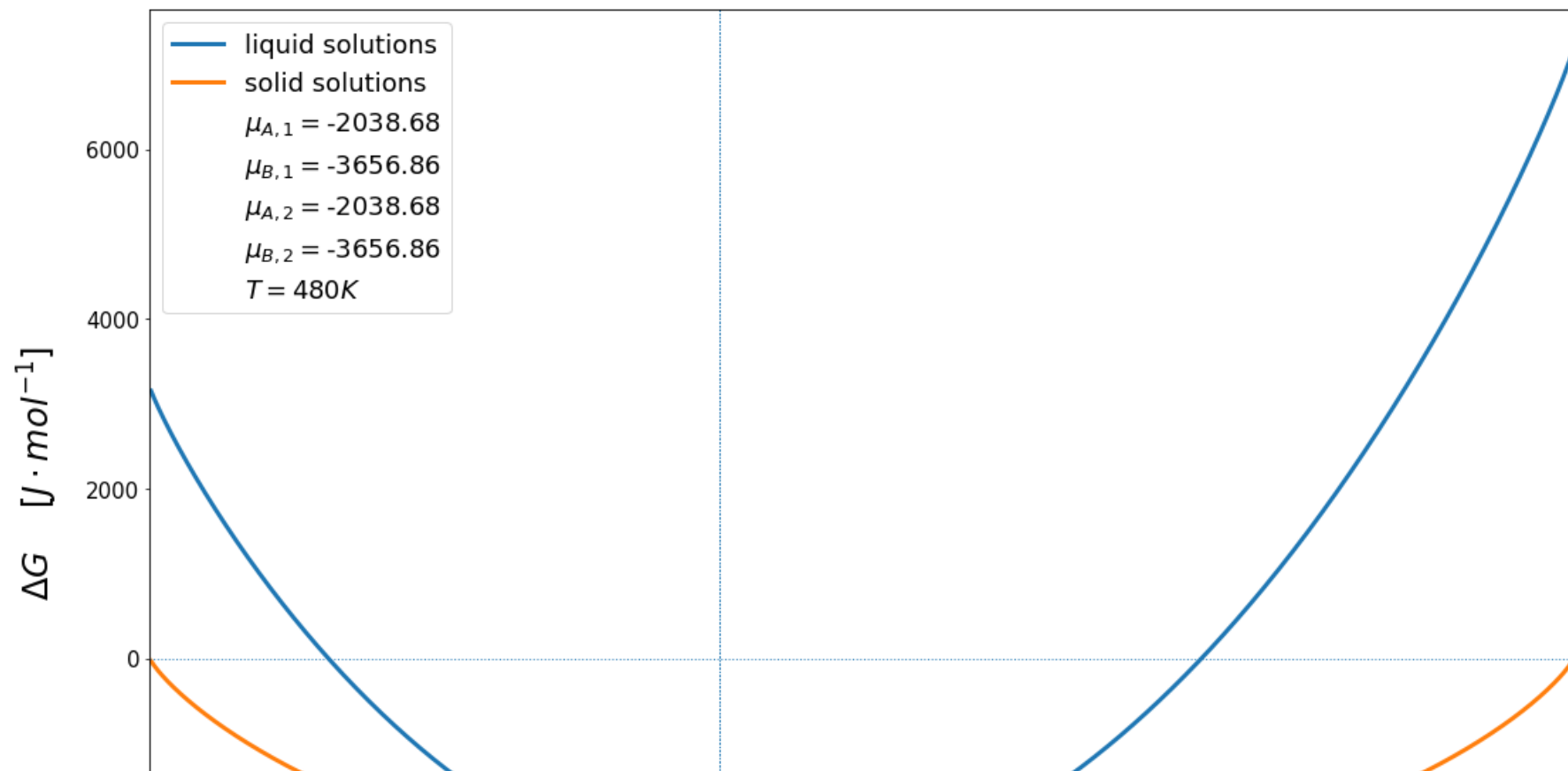
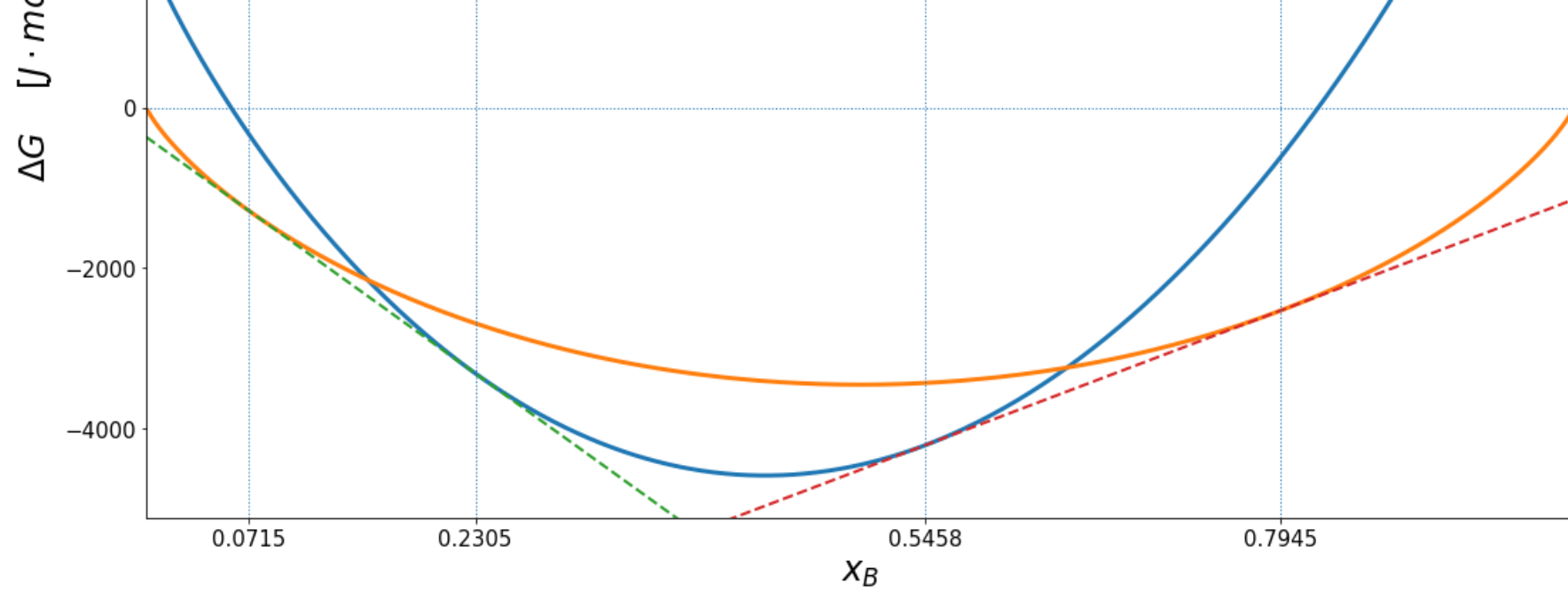


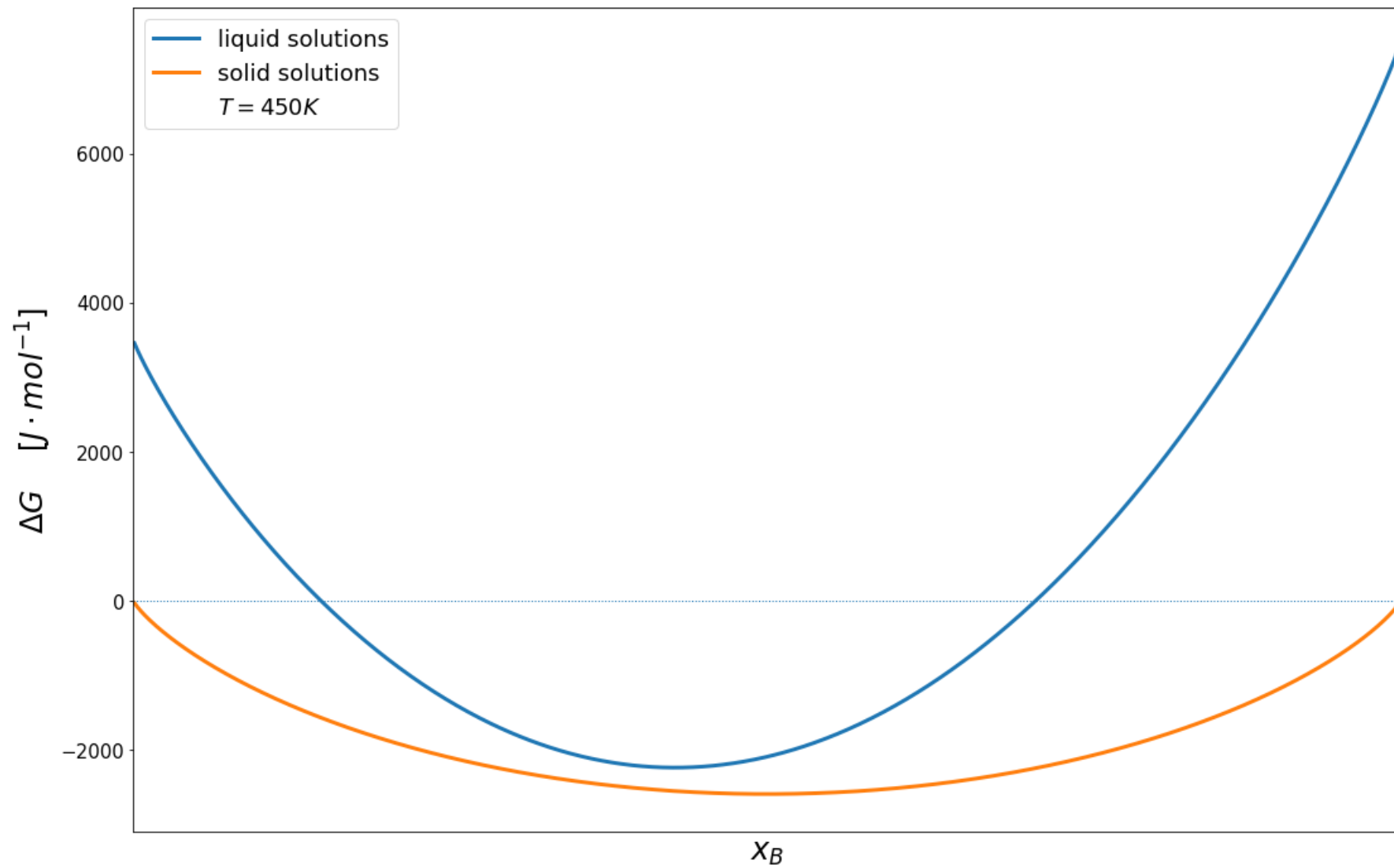
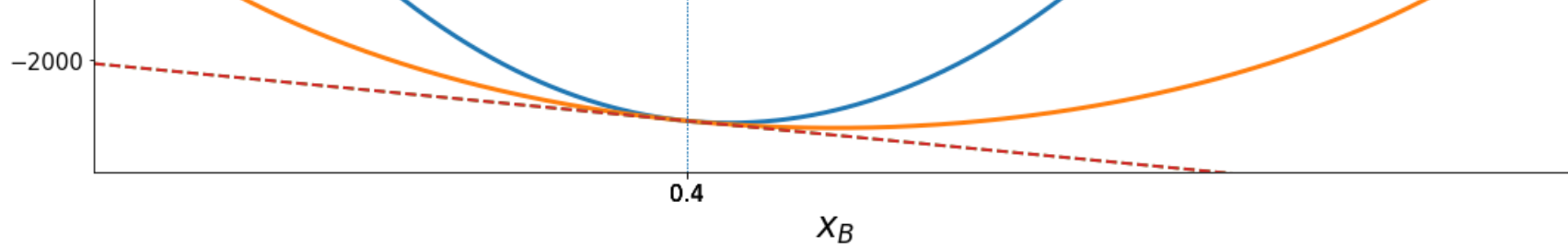












**PLOT Phase Diagram**

In [6]:

```
T = np.linspace(480.0, 1200.0, 100)
xb = np.linspace(0.0, 1.0, 100)

comp0 = []
comp1 = []
comp2 = []
comp3 = []
for t in T:
    comp = phaseDiagram(t);
    comp0.append(comp[0])
    comp1.append(comp[1])
    comp2.append(comp[2])
    comp3.append(comp[3])

# PLOT FIG
scale = 6;
fig, ax = plt.subplots(figsize=(3*scale, 2*scale));

# Plot
#plt.scatter(T, C, s=25, color='red', label='Raw data');
x = comp0
y = T
plt.plot(x, y, '-', linewidth=3, label='liquid solutions')

x = comp1
y = T
plt.plot(x, y, '-', linewidth=3, label='solid solutions')

x = comp2
y = T
plt.plot(x, y, '-', linewidth=3, label='liquid solutions')

x = comp3
y = T
plt.plot(x, y, '-', linewidth=3, label='solid solutions')

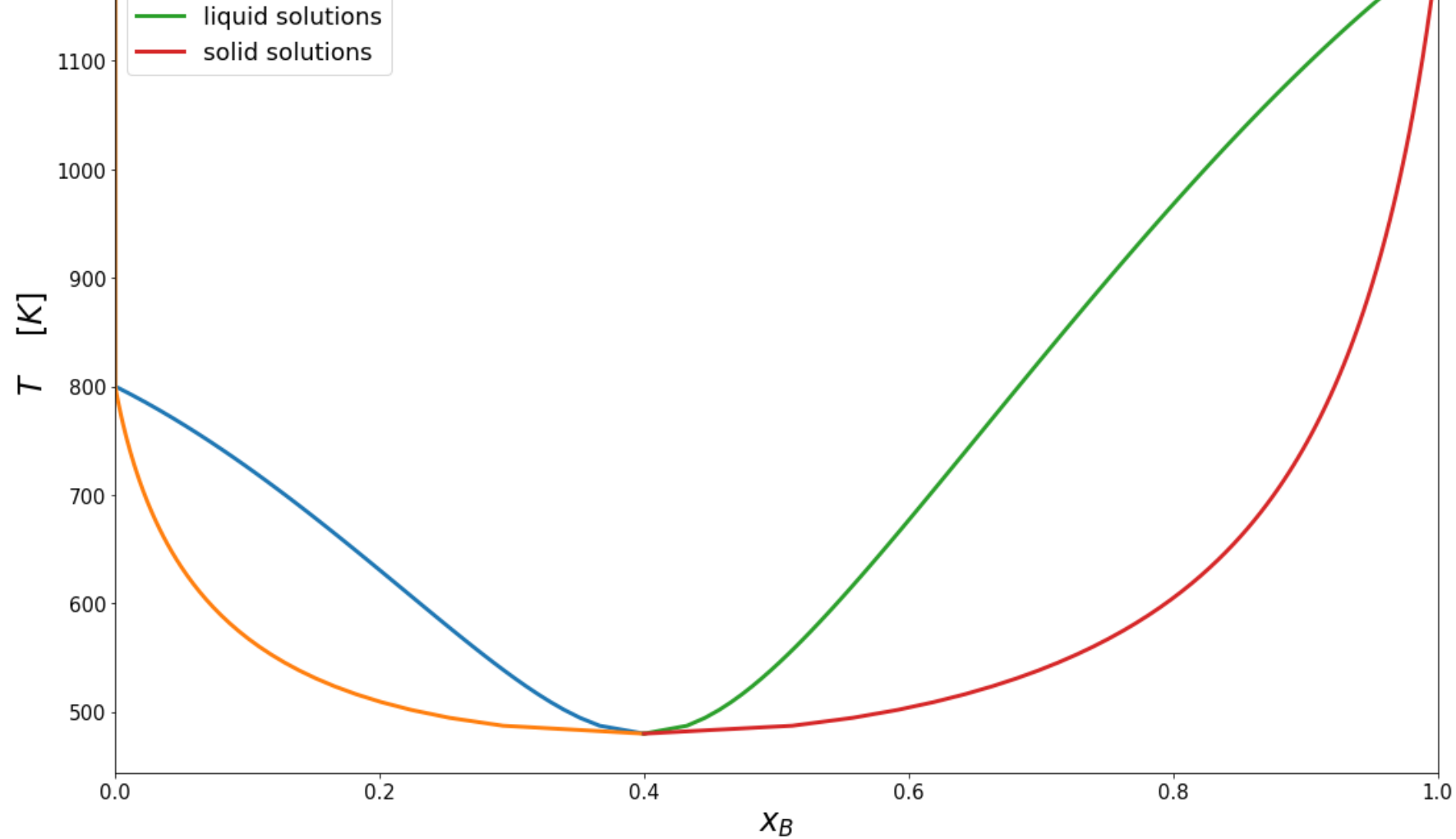
ax.ticklabel_format(useOffset=False) # disable scientific notation

# Display plots
plt.xlim(0.0, 1.0)
plt.yscale('linear');
plt.xlabel(r'$x_B$', fontsize=24);
plt.ylabel(r'$T$' + ' ' + r'$[K]$', fontsize=24);
plt.title('Phase Diagram', size=24);
plt.legend(prop={'size': 18});
display(plt);
```

<module 'matplotlib.pyplot' from 'C:\\Users\\oskat\\Anaconda3\\lib\\site-packages\\matplotlib\\pyplot.py'>

## Phase Diagram





As depicted by the reproductions, the Gibbs curves are identical to the ones in Gaskell's book.

However the blue line in the reproduced phase diagram differs from Gaskell's. (Can't explain why ...)

In [7]:

```
import pdfkit
path_wkhtmltopdf = r'C:\Program Files\wkhtmltopdf\bin\wkhtmltopdf.exe'
config = pdfkit.configuration(wkhtmltopdf=path_wkhtmltopdf)
```

```
options = {
    'page-size': 'A4',
    'margin-top': '0.0in',
    'margin-right': '0.0in',
    'margin-bottom': '0.0in',
    'margin-left': '0.0in',
    'page-label': 'PDF 2'
```

```
'encoding': "UTF-8",
'custom-header' : [
    ('Accept-Encoding', 'gzip')
],
'cookie': [
    ('cookie-name1', 'cookie-value1'),
    ('cookie-name2', 'cookie-value2'),
],
'no-outline': None,
'orientation': 'Landscape'
}

pdfkit.from_file('./BinaryPhaseDiagrams.html', 'BinaryPhaseDiagrams.pdf', configuration=config, options=options)
```

Loading pages (1/6)  
Warning: Failed to load file:///C:/Users/oskat/OneDrive - Instituto Tecnologico y de Estudios Superiores de Monterrey/Documents/MNT\_ITESM\_courses/2.2.ThermodynamicsOfMaterials/classActivity03/custom.css (ignore)  
Counting pages (2/6)  
Resolving links (4/6)  
Loading headers and footers (5/6)  
Printing pages (6/6)  
Done

Out[7]:

True

In [ ]: