# Problem Description/Data/Reference: Final Project (RTA) - SPE 114947 (IIk)

# **Problem Description:**

#### **Elements:**

- This is a production analysis with variable rate + changing flowing bottom hole pressure (FBHP)
- This is a gas well with finite conductivity fracture (bilinear flow).
- Require the use of material balance pseudo time  $(\bar{t_q})$
- Require the use of pseudo-pressure integration

## **Challenges:**

- Need to guess initial gas-in-place (IGIP) and compute average reservoir pressure, pseudo time  $(t_a)$ , and material balance pseudo time  $(\bar{t_a})$ , using SPE 17708.
- Need to plot flowing material balance equation, correct for the transient flow production and iterate for initial gas-inplace (IGIP), using the procedure in SPE 17708.
- Need to use 'De-superposition technique to incorporate finite conductivity element from Lee-Brockenbrough trilinear flow model into Ozkan's fracture well solution. Then use the convolution theorem to convert it to the rate solution to obtain Pratikno's type curve.

## **Results from publication/reference:**

- The time-rate-pressure for the entire history is given
- The preliminary analysis is provided in SPE 84287.
- The permeability and fracture half-length are obtained previously from pressure build up test (PBU)

## **Data Description:**

- There are 5,039 data points  $(t, q, P_{wf})$  with noise.
- Need to manually clean the data and take out some outliers from the shut-in events. The edited data set has only 4,416 data point.

## Reference:

Pratikno, H., Rushing, J. A., and Blasingame, T. A. (2003) Decline Curve Analysis Using Type Curves - Fractured Wells. Society of Petroleum Engineers. doi:10.2118/84287-MS

## Table of Properties

## Fluid Properties:

REF. GAS FVF, MSCF/STB = 0.5483 REF. GAS VISCOSITY, cp = 0.03605 REF. TOTAL COMPRESSIBILITY, 1/psia = 5.0975E-5 TEMPERATURE, deg F = 300

## Reservoir Properties:

RESERVOIR THICKNESS, ft = 170
WELLBORE RADIUS, ft = 0.333
POROSITY, fraction = 0.088
EQUIVALENT POROSITY, fraction = 0.07647 (\*)

(\*) Adjusted to the irreducible water saturation
Swi = 0.131

#### Production Properties:

INITIAL PRESSURE (Pi), psia = 9330 PSEUDO INITIAL PRESSURE (Ppi), psia = 7540.13 INITIAL GAS-IN-PLACE (G), BSCF = 3.23 (\*)

(\*) INTIAL GUESS FROM SPE 17708 METHOD

## Properties to be Solved: (Final Estimates)

(from Python Program)

(Finite-conductivity fracture in a bounded reservoir model)

```
PERMEABILITY (k), md = 0.016

FRACTURE HALF-LENGTH (xf), ft = 112

EQUIVALENT SKIN (S), Dim-Less = -5.12 (*)

FRACTURE COND. (FcD), Dim-less = 27

RESERVOIR RADIUS (re), ft = 491

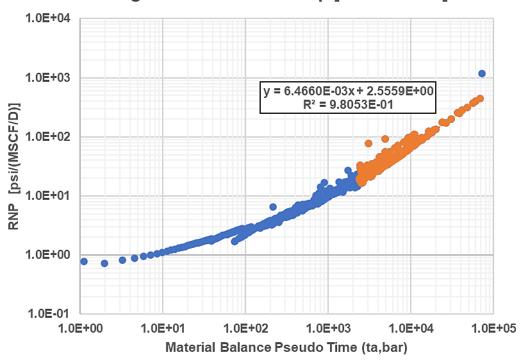
INITIAL GAS-IN-PLACE (G), BSCF = 3.20 (**)
```

- (\*) Calculated from  $S = -\ln(xf/2rw)$
- (\*\*) Use volumetric calculation from reservoir properties and matched reservoir radius (re)

# Material Balance Pseudo Time $(\overline{t_a})$ and Initial Gas-In-Place Iterations (G)

## **Diagnostic Plot [log-log]:**

## Flowing Material Balance Eq. [SPE 114947]



All data

PSS data

..... Linear (PSS data)

# IGIP Iterations (BSCF) G (guess) G (cal) 3.2 3.2085 3.21 3.2185 3.22 3.2220 3.23 3.2293 3.24 3.2387 3.3 3.2734

## **Calculations:**

- 1) Estimate IGIP = 3.23 BSCG
- 2) Estimate productivity index = 1 / 2.5559 = 0.391 psi / (MSCF/D)
- 3) IGIP is sensitive to curve-fitting, depending on how the time to stabilized flow  $(t_{PSS})$  is selected. I will cross-check this IGIP with the one obtained from RTA type curve matching

## Workflow Plot (SPE 17708 - Blasingame):

- 1) Estimate (guess) initial gas-in-place (G)
- 2) Calculate average reservoir pressure, using the material balance equation. For Gp, use the trapezoid rule of qg. Note that z-factor is in a function of reservoir pressure  $\overline{p_r}$

$$\frac{\overline{p_r}}{\overline{z}} = \frac{p_i}{z_i} \left( 1 - \frac{G}{G_p} \right), \qquad G_p = \int_0^t q_g dt$$

3) Calculate pseudo time  $(t_a)$  based on  $\overline{p_r}$ 

$$\mathbf{t}_{\mathbf{a}} = \mu_{gi} c_{ti} \int_{0}^{\tau} \frac{1}{\mu_{g}(\overline{p_{r}}) c_{t}(\overline{p_{r}})} d(\tau)$$

4) Calculate material balance pseudo time  $(\bar{t_a})$  as follows;

$$\overline{t_a} = \frac{1}{q_g} \int_0^{t_a} q_g(\tau_a) d(\tau_a)$$

5) Calculate pseudo-pressure  $(P_{pwf})$  as follows;

$$P_{pwf} = \frac{\mu_{gi} z_{gi}}{P_i} \int_{0}^{t} \frac{P}{\mu_g(\overline{p_r}) z_g(\overline{p_r})} d(P)$$

6) Plot the flowing material balance equation (between ratenormalized pseudo-pressure and material balance pseudo time to obtain initial gas-in-place and the reciprocal of productivity index from slope and intercept, respectively.

$$RNP = \frac{P_{pi} - P_{pwf}}{q_g} = \frac{1}{J} + \frac{\overline{t_a}}{c_{ti}G}$$

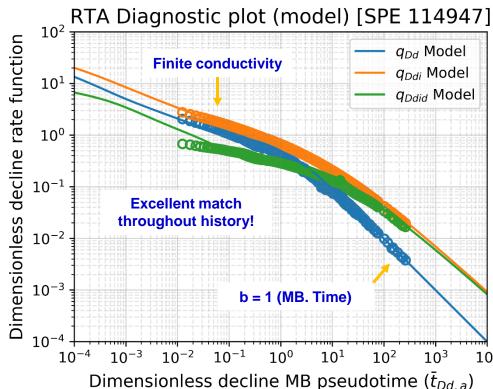
$$J = \frac{kh}{70.6\mu_{gi}B_{gi}\left[ln\left(\frac{4A}{e^{\gamma}C_A r_w^2}\right) + 2S\right]}$$

7) Need to correct extra production from a transient flow

$$q_{trn} = rac{\Delta p_{obs}}{b + m ar{t_a}}, \qquad G_p(trn) = \int\limits_0^{t_{PSS}} q_{trn}( au) d( au) \ G = rac{1}{m c_{ti}} + G_p(t_{PSS}) - G_p(trn)$$

# Analysis Summary Plots (Model)

## "Model" matching: (by Python)



## Type curve matching results:

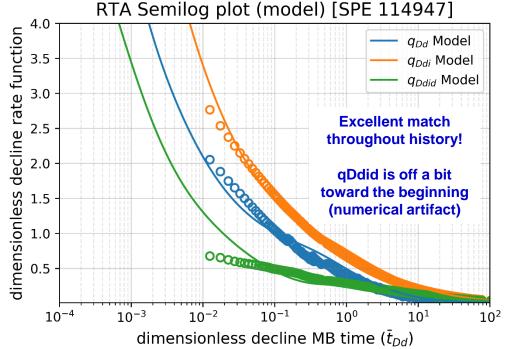
$$k = 0.016 \, md,$$
  $x_f = 112 \, ft$   
 $F_{cD} = 27,$   $r_e = 491 \, ft$ 

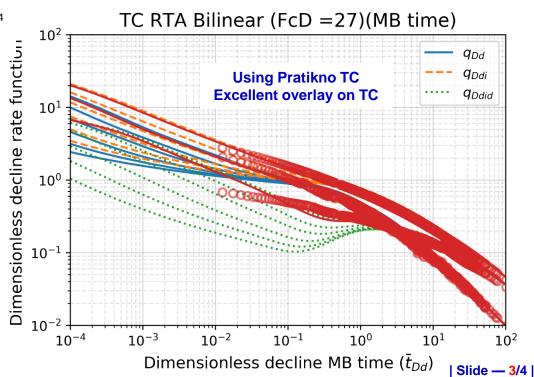
## **Calculation check for IGIP:**

$$G = \frac{\pi r_e^2 h \phi (1 - S_{wi})}{B_{gi} \left[ \frac{rb}{MSCF} \right] \times 5.6146} = \frac{\pi (491^2)(170)(0.088)(1 - 0.131)}{0.5483 \times 5.6146}$$

$$G = 3.198 \times 10^6 MSCF \approx 3.20 BSCF$$

This result agrees well with G obtained from pseudo time calculation, using the method in SPE 17708 (3.23 BSCF)





# Method of Work / Discussion of Results

## Method of Work:

## **Starting Point:**

- Type curve matching requires Stehfest's algorithm.
- Need to follow IGIP and  $\overline{t_q}$  calculation shown in slide 2

## **Governing Equations:**

Blasingame-Poe Desuperposition "Trilinear Pseudo radial"	$ \overline{p}_{TPR,inf}(C_{fD}, s_f)  = \overline{p}_{LBD,inf}(C_{fD}, s_f) - \overline{p}_{LBD,inf}(C_{fD} = \infty, s_f = 0)  + \overline{p}_{ORD,inf}( x_D(C_{fD})  \le 1, y_D = 0) $
Lee-Brockenbrough Trilinear flow equation	$\overline{p}_{LBD,inf}(C_{fD}, s_f) = \frac{\pi}{\mu C_{fD}} \frac{1}{\psi \tanh(\psi)},$ $\psi = \sqrt{\frac{2}{C_{fD}} \frac{\alpha}{1 + \alpha s_f} + \frac{\mu}{\eta_{fD}}}, \alpha = \sqrt{\mu + \sqrt{\mu}}$
Infinite Cond. Fracture soln. (Okzan/Laplace)	$\begin{split} & \overline{p}_{sD}(x_D = 0.732, y_D = 0, \mu) \\ & = \frac{1}{2\mu\sqrt{\mu}} \left[ \int_0^{\sqrt{\mu}(1+x_D)} K_0(z)dz + \int_0^{\sqrt{\mu}(1-x_D)} K_0(z)dz \right] \\ & + \frac{1}{2\mu\sqrt{\mu}} \frac{K_1(\sqrt{\mu}r_{eD})}{I_1(\sqrt{\mu}r_{eD})} \left[ \int_0^{\sqrt{\mu}(1+x_D)} I_0(z)dz + \int_0^{\sqrt{\mu}(1-x_D)} I_0(z)dz \right] \end{split}$
$b_{D,PSS}$ Correlation	$b_{\mathit{D,PSS}} = f(r_{e\mathit{D}}, F_{\mathit{cD}})$ (check SPE 84287 Eq.5)
Dimensionless rate from $q_g$ and $P_{pwf}$	$q_{D} = \frac{141.2\mu_{gi}B_{gi}}{kh} \left(\frac{q_{g}}{P_{pi} - P_{pwf}}\right) = \frac{141.2\mu_{gi}B_{gi}}{kh} (PNR)$
Dimensionless <u>decline</u> function	
Dimensionless <u>decline</u> material balance pseudo time	$\overline{t_{Dd,a}} = 2t_{Df} \left\{ b_{D,PSS} \left[ \left( \frac{r_e}{x_f} \right)^2 - 1 \right] \right\}^{-1}$

## Challenge & Issues:

• [De-superposition] Blasingame and Poe added "Finite-conductivity" element of trilinear solution to Okzan's solution which includes the pseudo radial flow at the late time. Use  $s_f \approx 0$  and  $\eta_{fD} \approx 200 \times C_{fD}$ 

## **Discussion of Results:**

## Diagnostics:

- The bilinear flow at early time is clear. The q<sub>Dd</sub> function in the transient stem has slope of ¼.
- The depletion stem follows the harmonic solution because the material balance pseudo time is used.
- Excellent match on qDd and qDdi
- Some numerical artifact in qDdid toward the beginning

## **Analyses:**

- Permeability from RTA is identical to the one from PTA (k = 0.016 md).
- Fracture half-length from RTA (xf = 112 ft) agrees extremely well with the one from PTA (xf = 119 ft)
- The well is stimulated (negative skin = -5.12)
- According to RTA, fracture is finite fractureconductive (FcD = 27) In PTA, FcD = 4. Bilinear flow regime is more pronounced in PBU.
- Gas in-place estimates from SPE 17708 iteration and type curve match agree within 0.03 BSCF.

## **Assessment:**

 Use L = 0.1-0.15 to smooth the data provides even better-quality rate-integral derivative (qDdid)

## Recommendations/Extra work:

## Technical developments that would help?

- The augmented plot for  $\beta$ -derivative
- Try log-log plot by 'flipping' TC upside down and work with "rate-normalized pressure (RNP)" instead of "pressure-normalized rate (PNR)"
- The  $p_D$  vs  $\sqrt[4]{t_D}$  plot or "Bi-linear flow" specialized plot could yield the straight-line in case of finite-conductivity fracture.