



Stream Function - Vorticity Approach to the Channel Flow

Kumar Saurabh (MA14M004)
Peela V V K S Ganesh (CH13M023)



VORTICITY AND STREAM FUNCTION EQUATIONS

Incompressible Navier-Stokes Equation in 2-D

- X – momentum equation

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

- Y – momentum equation

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

Non-dimensionalization

- X – momentum equation:

$$\tilde{u} = \frac{u}{U_0}, \tilde{v} = \frac{v}{U_0}, \tilde{x} = \frac{x}{H}, \tilde{y} = \frac{y}{H}$$

$$\tilde{t} = \frac{t}{H/U_0}, \tilde{p} = \frac{p}{\rho U_0^2}$$

$$\frac{U_0^2}{H} \left(\frac{\partial \tilde{u}}{\partial \tilde{t}} + \tilde{u} \frac{\partial \tilde{u}}{\partial \tilde{x}} + \tilde{v} \frac{\partial \tilde{u}}{\partial \tilde{y}} \right) = -\frac{U_0^2}{H} \frac{\partial \tilde{p}}{\partial \tilde{x}} + \frac{\nu U_0}{H^2} \left(\frac{\partial^2 \tilde{u}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{u}}{\partial \tilde{y}^2} \right)$$

$$\frac{\partial \tilde{u}}{\partial \tilde{t}} + \tilde{u} \frac{\partial \tilde{u}}{\partial \tilde{x}} + \tilde{v} \frac{\partial \tilde{u}}{\partial \tilde{y}} = -\frac{\partial \tilde{p}}{\partial \tilde{x}} + \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{u}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{u}}{\partial \tilde{y}^2} \right)$$

Non-dimensionalization

- Υ – momentum equation:

$$\frac{\partial \tilde{v}}{\partial \tilde{t}} + \tilde{u} \frac{\partial \tilde{v}}{\partial \tilde{x}} + \tilde{v} \frac{\partial \tilde{v}}{\partial \tilde{y}} = -\frac{\partial \tilde{p}}{\partial \tilde{y}} + \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{v}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{v}}{\partial \tilde{y}^2} \right)$$

The vorticity Equation

- Differentiate X – momentum Equation with respect to y :

$$\frac{\partial}{\partial \tilde{y}} \left[\left(\frac{\partial \tilde{u}}{\partial \tilde{t}} + \tilde{u} \frac{\partial \tilde{u}}{\partial \tilde{x}} + \tilde{v} \frac{\partial \tilde{u}}{\partial \tilde{y}} \right) \right] = -\frac{\partial \tilde{p}}{\partial \tilde{x}} + \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{u}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{u}}{\partial \tilde{y}^2} \right) \quad (1)$$

- Differentiating Y – momentum Equation with respect to x :

$$\frac{\partial}{\partial \tilde{x}} \left[\left(\frac{\partial \tilde{v}}{\partial \tilde{t}} + \tilde{u} \frac{\partial \tilde{v}}{\partial \tilde{x}} + \tilde{v} \frac{\partial \tilde{v}}{\partial \tilde{y}} \right) \right] = -\frac{\partial \tilde{p}}{\partial \tilde{y}} + \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{v}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{v}}{\partial \tilde{y}^2} \right) \quad (2)$$

The vorticity Equation

- Subtracting equation (1) from (2)

$$\frac{\partial \tilde{\omega}}{\partial \tilde{t}} + \tilde{u} \frac{\partial \tilde{\omega}}{\partial \tilde{x}} + \tilde{v} \frac{\partial \tilde{\omega}}{\partial \tilde{y}} = \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{\omega}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\omega}}{\partial \tilde{y}^2} \right)$$

$$\tilde{\omega} = \frac{\partial \tilde{v}}{\partial \tilde{x}} - \frac{\partial \tilde{u}}{\partial \tilde{y}}$$

Stream Function Equation

- Define the stream function:

$$\tilde{u} = \frac{\partial \tilde{\psi}}{\partial \tilde{y}}, \quad \tilde{v} = -\frac{\partial \tilde{\psi}}{\partial \tilde{x}}$$

- Which automatically satisfies the continuity equation for incompressible fluid:

$$\frac{\partial \tilde{u}}{\partial \tilde{x}} + \frac{\partial \tilde{v}}{\partial \tilde{y}} = 0$$

$$\frac{\partial}{\partial \tilde{x}} \frac{\partial \tilde{\psi}}{\partial \tilde{y}} - \frac{\partial}{\partial \tilde{y}} \frac{\partial \tilde{\psi}}{\partial \tilde{x}} = 0$$

Stream Function Equation

- Substituting:

$$\tilde{u} = \frac{\partial \tilde{\psi}}{\partial \tilde{y}}; \quad \tilde{v} = -\frac{\partial \tilde{\psi}}{\partial \tilde{x}}$$

into the definition of vorticity:

$$\tilde{\omega} = \frac{\partial \tilde{v}}{\partial \tilde{x}} - \frac{\partial \tilde{u}}{\partial \tilde{y}}$$

yields

$$\frac{\partial^2 \tilde{\psi}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\psi}}{\partial \tilde{y}^2} = -\omega$$

Navier-Stokes Equation in vorticity - Stream Function form

- Advection/diffusion Equation:

$$\frac{\partial \tilde{\omega}}{\partial \tilde{t}} = -\frac{\partial \tilde{\psi}}{\partial \tilde{y}} \frac{\partial \tilde{\omega}}{\partial \tilde{x}} + \frac{\partial \tilde{\psi}}{\partial \tilde{x}} \frac{\partial \tilde{\omega}}{\partial \tilde{y}} + \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{\omega}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\omega}}{\partial \tilde{y}^2} \right)$$

- Elliptic Equation:

$$\frac{\partial^2 \tilde{\psi}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\psi}}{\partial \tilde{y}^2} = -\omega$$



FINITE DIFFERENCE APPROXIMATION

Finite Difference Approximation

$$\frac{\partial \tilde{\omega}}{\partial \tilde{t}} = -\frac{\partial \tilde{\psi}}{\partial \tilde{y}} \frac{\partial \tilde{\omega}}{\partial \tilde{x}} + \frac{\partial \tilde{\psi}}{\partial \tilde{x}} \frac{\partial \tilde{\omega}}{\partial \tilde{y}} + \frac{1}{\text{Re}} \left(\frac{\partial^2 \tilde{\omega}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\omega}}{\partial \tilde{y}^2} \right)$$

$$\begin{aligned} \frac{\tilde{\omega}_{i,j}^{n+1} - \tilde{\omega}_{i,j}^n}{\Delta \tilde{t}} = & - \left(\frac{\tilde{\psi}_{i,j+1}^n - \tilde{\psi}_{i,j-1}^n}{2\Delta \tilde{y}} \right) \left(\frac{\tilde{\omega}_{i+1,j}^n - \tilde{\omega}_{i-1,j}^n}{2\Delta \tilde{x}} \right) + \left(\frac{\tilde{\psi}_{i+1,j}^n - \tilde{\psi}_{i-1,j}^n}{2\Delta \tilde{x}} \right) \left(\frac{\tilde{\omega}_{i,j+1}^n - \tilde{\omega}_{i,j-1}^n}{2\Delta \tilde{y}} \right) \\ & + \frac{1}{\text{Re}} \left(\frac{\tilde{\omega}_{i+1,j}^n - 2\tilde{\omega}_{i,j}^n + \tilde{\omega}_{i-1,j}^n}{\Delta \tilde{x}^2} + \frac{\tilde{\omega}_{i,j+1}^n - 2\tilde{\omega}_{i,j}^n + \tilde{\omega}_{i,j-1}^n}{\Delta \tilde{y}^2} \right) \end{aligned}$$

Vorticity at new time

$$\omega_{i,j}^{n+1} =$$

$$\omega_{i,j}^n + \Delta t \left[- \left(\frac{\tilde{\psi}_{i,j+1}^n - \tilde{\psi}_{i,j-1}^n}{2\Delta\tilde{y}} \right) \left(\frac{\tilde{\omega}_{i+1,j}^n - \tilde{\omega}_{i-1,j}^n}{2\Delta\tilde{x}} \right) + \left(\frac{\tilde{\psi}_{i+1,j}^n - \tilde{\psi}_{i-1,j}^n}{2\Delta\tilde{x}} \right) \left(\frac{\tilde{\omega}_{i,j+1}^n - \tilde{\omega}_{i,j-1}^n}{2\Delta\tilde{y}} \right) + \frac{1}{\text{Re}} \left(\frac{\tilde{\omega}_{i+1,j}^n - 2\tilde{\omega}_{i,j}^n + \tilde{\omega}_{i-1,j}^n}{\Delta\tilde{x}^2} + \frac{\tilde{\omega}_{i,j+1}^n - 2\tilde{\omega}_{i,j}^n + \tilde{\omega}_{i,j-1}^n}{\Delta\tilde{y}^2} \right) \right]$$

```
for i = 2:nx - 1
    for j = 2:ny - 1
        w(j,i) = vort(j,i) + delta_t*(-((PSI(j+1,i) - PSI(j - 1,i))/(2*dy))*((vort(j,i+1) - vort(j,i - 1))/(2*dx))+...
            +((PSI(j,i+1) - PSI(j,i - 1))/(2*dx))*((vort(j+1,i) - vort(j - 1,i))/(2*dy))+...
            (1/Re)*((vort(j,i+1)-2*vort(j,i)+vort(j,i-1))/(dx^2)) + (vort(j+1,i)-2*vort(j,i)+vort(j - 1,i))/dy^2));
    end
end
```

Stream Function Equation

- $$\frac{\partial^2 \tilde{\psi}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\psi}}{\partial \tilde{y}^2} = -\tilde{\omega}$$

- Solving the elliptic equation:

$$\frac{\tilde{\psi}_{i+1,j}^n - 2\tilde{\psi}_{i,j}^n + \tilde{\psi}_{i-1,j}^n}{\Delta \tilde{x}^2} + \frac{\tilde{\psi}_{i,j+1}^n - 2\tilde{\psi}_{i,j}^n + \tilde{\psi}_{i,j-1}^n}{\Delta \tilde{y}^2} = -\tilde{\omega}_{i,j}^n$$

- This can be solved using Gauss-Seidel Iteration by Successive Over-relaxation (SOR) or Successive Under-relaxation.

Stream Function Equation

```
while (err > 10^(-6))
    tempPSI = PSI;
    for i = 2:nx - 1
        for j = 2:ny - 1
            PSI(j,i) = relax*(1/(2/dX^2+2/dY^2)*((PSI(j,i+1)+PSI(j,i-1))/dX^2+...
                |(PSI(j+1,i)+PSI(j-1,i))/dY^2) + vort(j,i))) + (1 - relax)*PSI(j,i)
        end
    end
    PSI(2:ny,nx) = 2*PSI(2:ny,(nx - 1)) - PSI(2:ny,(nx - 2));
    err = 0;
    for i = 2:nx - 1
        for j = 2:ny - 1
            err = err+ (abs(PSI(j,i) - tempPSI(j,i))/PSI(j,i));
        end
    end

    n = n+1;
end
```


Limitation on Time Step

- Courant – Friedrichs – Lewy condition (CFL):

$$\left(\frac{u\Delta t}{\Delta x} + \frac{v\Delta t}{\Delta y} \right) \leq 1$$

- Grid Fourier Number:

$$\nu\Delta t \left(\frac{1}{\Delta x^2} + \frac{1}{\Delta y^2} \right) \leq \frac{1}{2}$$

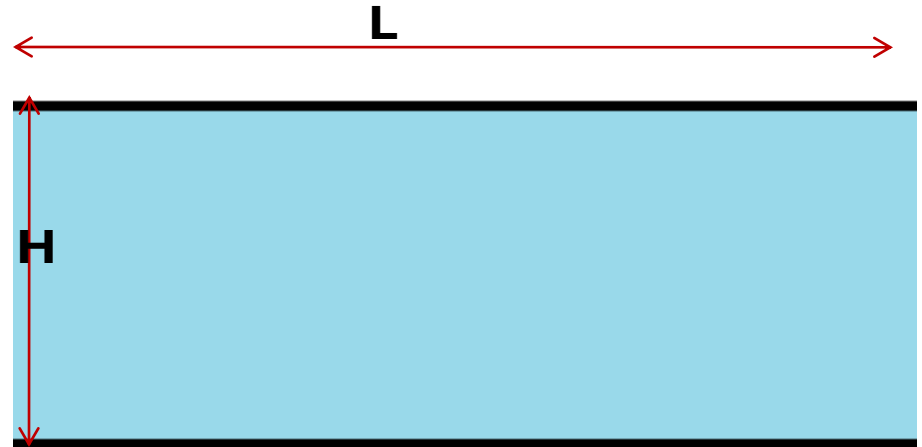
- $\Delta t < \Delta x$



CHANNEL FLOW

Channel flow parameters

- $Re = 100$
- $Pr = 0.7$ (air)
- $H = 1\text{m}$
- $L = ???$



Entrance length


- Hydrodynamic Entrance Length:

$$\frac{L_h}{H} = 0.05 * Re$$

- Thermal Entrance Length:

$$\frac{L_t}{H} = 0.05 * Re * Pr$$

- $L = 14 \text{ m}$



$j = ny$									
$j = ny-1$									
$j = 2$									
$j = 1$									
	$i = 1$	$i = 2$						$i = nx - 1$	$i = nx$

Inlet Boundary Condition

- Assuming uniform velocity:

- $\tilde{u} = 1$

- $\tilde{v} = 0$

- $\tilde{\psi}_{inlet} = \int_0^H \tilde{u}(\tilde{y})_{inlet} d\tilde{y}$

- $\tilde{\psi}_{inlet}(\tilde{y}) = \tilde{y}$

- ```
for j = 1:ny
 PSI(j,1) = (j-1)*dY; % inlet
end
```

- $\tilde{\omega}_{inlet} = 0$



# Outflow Boundary Condition

- $\frac{\partial \tilde{u}}{\partial \tilde{x}} = \frac{\partial \tilde{v}}{\partial \tilde{x}} = 0$
- $\frac{\partial^2 \tilde{\psi}}{\partial \tilde{x}^2} = 0$
- $\tilde{\psi}_{nx,j} = 2 * \tilde{\psi}_{nx-1,j} - \tilde{\psi}_{nx-2,j}$



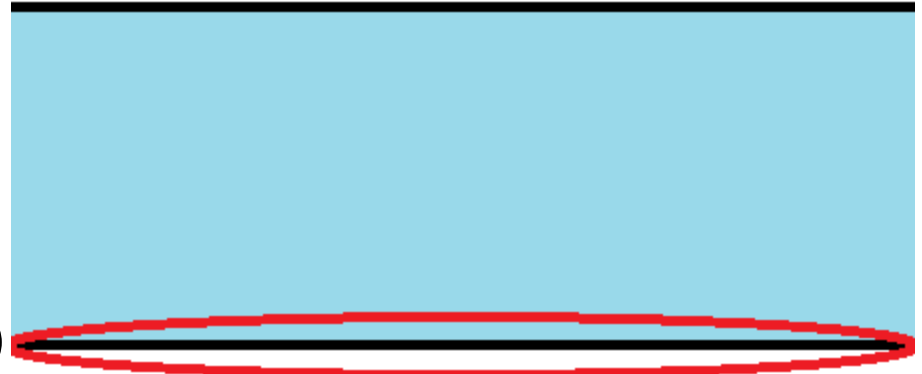
- `PSI(2:ny,nx) = 2*PSI(2:ny,(nx - 1)) - PSI(2:ny,(nx - 2));`

- $\frac{\partial \tilde{\omega}}{\partial \tilde{x}} = 0$
- $\tilde{\omega}_{nx,j} = \tilde{\omega}_{nx-1,j}$

- `vort(2:ny-1,nx) = vort(2:ny-1,nx - 1);`



# Bottom wall : No slip Boundary Condition



- $\tilde{v} = 0 \Rightarrow \frac{\partial \tilde{\psi}}{\partial \tilde{x}} = 0$

- $\tilde{\psi} = \text{constant} = 0$

- $\frac{\partial^2 \tilde{\psi}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\psi}}{\partial \tilde{y}^2} = -\tilde{\omega} \Rightarrow \tilde{\omega}_{\text{wall}} = -\frac{\partial^2 \tilde{\psi}_{i,j=1}}{\partial \tilde{y}^2}$

- $\tilde{\psi}_{i,j=2} = \tilde{\psi}_{i,j=1} + (\Delta \tilde{y}) \frac{\partial \tilde{\psi}_{i,j=1}}{\partial \tilde{y}} + \frac{\Delta \tilde{y}^2}{2} \frac{\partial^2 \tilde{\psi}_{i,j=1}}{\partial \tilde{y}^2} + O(\Delta \tilde{y}^3)$

- $\tilde{\omega}_{\text{wall}} = (\tilde{\psi}_{i,j=1} - \tilde{\psi}_{i,j=2}) \frac{2}{\Delta \tilde{y}^2} + O(\Delta \tilde{y})$

- ```
vort(1,2:nx) = -2.0*(PSI(2,2:nx))/(dy^2); % bottom wall
```

Top wall : No slip Boundary Condition



- $\tilde{v} = 0 \Rightarrow \frac{\partial \tilde{\psi}}{\partial \tilde{x}} = 0$

- $\tilde{\psi} = \text{constant} = 1$

- $\frac{\partial^2 \tilde{\psi}}{\partial \tilde{x}^2} + \frac{\partial^2 \tilde{\psi}}{\partial \tilde{y}^2} = -\tilde{\omega} \Rightarrow \tilde{\omega}_{\text{wall}} = -\frac{\partial^2 \tilde{\psi}_{i,j=ny}}{\partial \tilde{y}^2}$

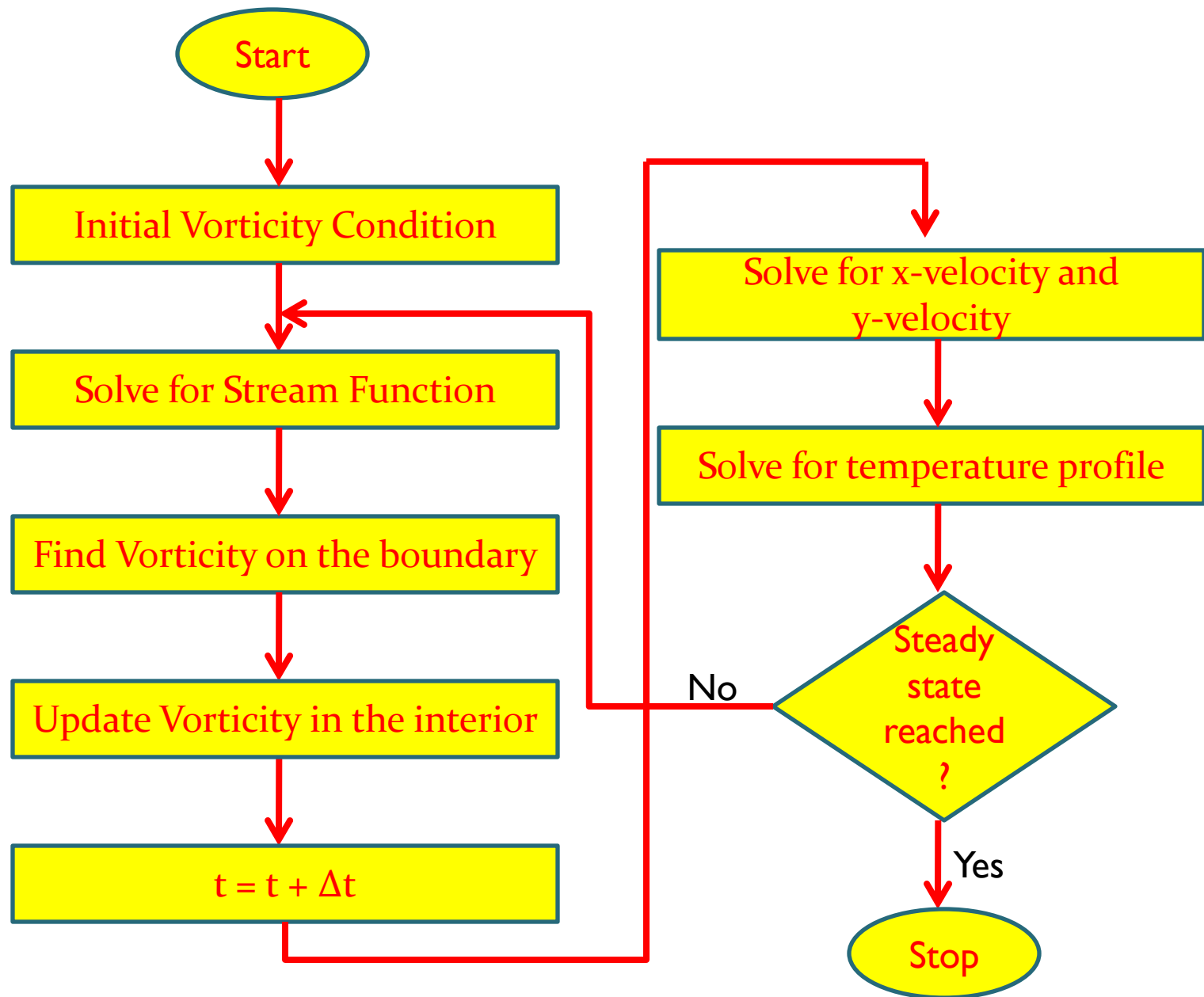
- $\tilde{\psi}_{i,j=ny-1} = \tilde{\psi}_{i,j=ny} - (\Delta \tilde{y}) \frac{\partial \tilde{\psi}_{i,j=ny}}{\partial \tilde{y}} + \frac{\Delta \tilde{y}^2}{2} \frac{\partial^2 \tilde{\psi}_{i,j=ny}}{\partial \tilde{y}^2} + O(\Delta \tilde{y}^3)$

- $\tilde{\omega}_{\text{wall}} = (\tilde{\psi}_{i,j=ny} - \tilde{\psi}_{i,j=ny-1}) \frac{2}{\Delta \tilde{y}^2} + O(\Delta \tilde{y})$

- ```
vort(ny,2:nx) = 2.0*(PSI(ny,2:nx) - PSI(ny - 1,2:nx))/(dy^2); % top wall
```



# FLOW CHART





# ● **VELOCITY PROFILE**

# Velocity profile:

- $\tilde{u} = \frac{\partial \tilde{\psi}}{\partial \tilde{y}}; \quad \tilde{v} = -\frac{\partial \tilde{\psi}}{\partial \tilde{x}}$

- $\tilde{u}_{i,j} = \frac{\tilde{\psi}_{i,j+1} - \tilde{\psi}_{i,j-1}}{2\Delta\tilde{y}}$

- $\tilde{v}_{i,j} = -\frac{\tilde{\psi}_{i+1,j} - \tilde{\psi}_{i-1,j}}{2\Delta\tilde{x}}$

- ```
for j = 2:ny-1
    u(j,:) = (psi(j+1,:)-psi(j-1,:))/(2*dy);
end
for i = 2:nx-1
    v(:,i) = -(psi(:,i+1)-psi(:,i-1))/(2*dx);
end
```

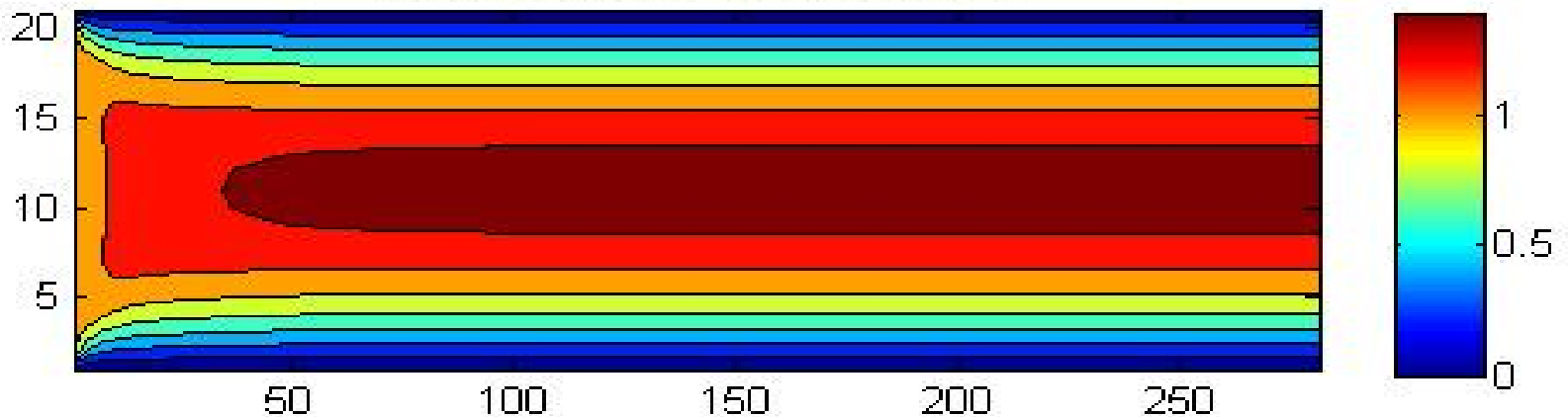
- ## Boundary conditions:

```
u(:,1) = 1;           % inlet
v(:,1) = 0;           % inlet
u(1,:) = 0;           % bottom wall
u(ny,:) = 0;          % top wall
u(2:ny,nx) = u(2:ny,nx - 1); % outflow
```

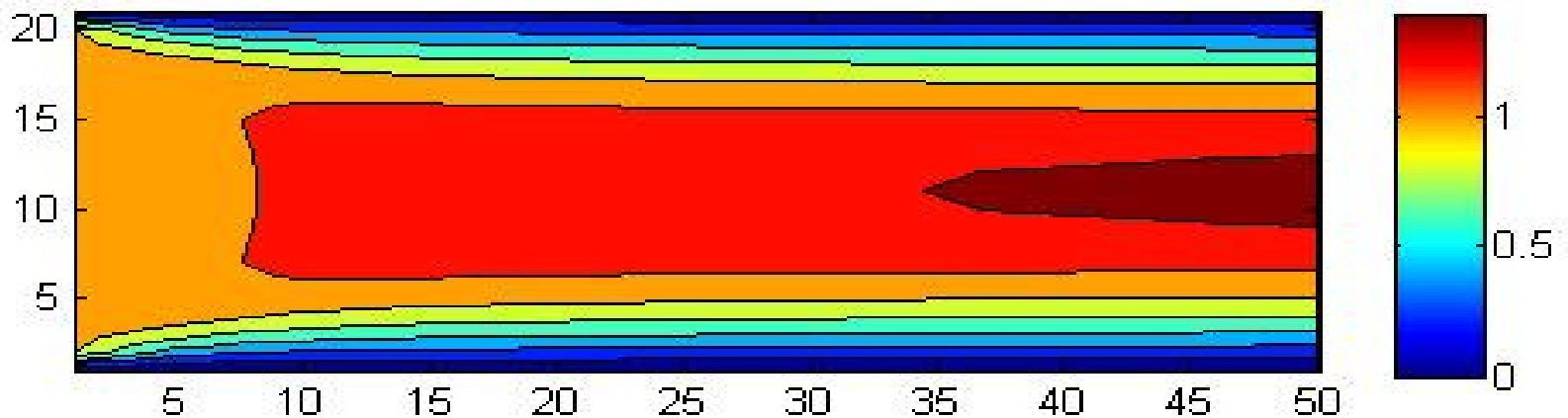
Velocity Contour

Velocity Contours

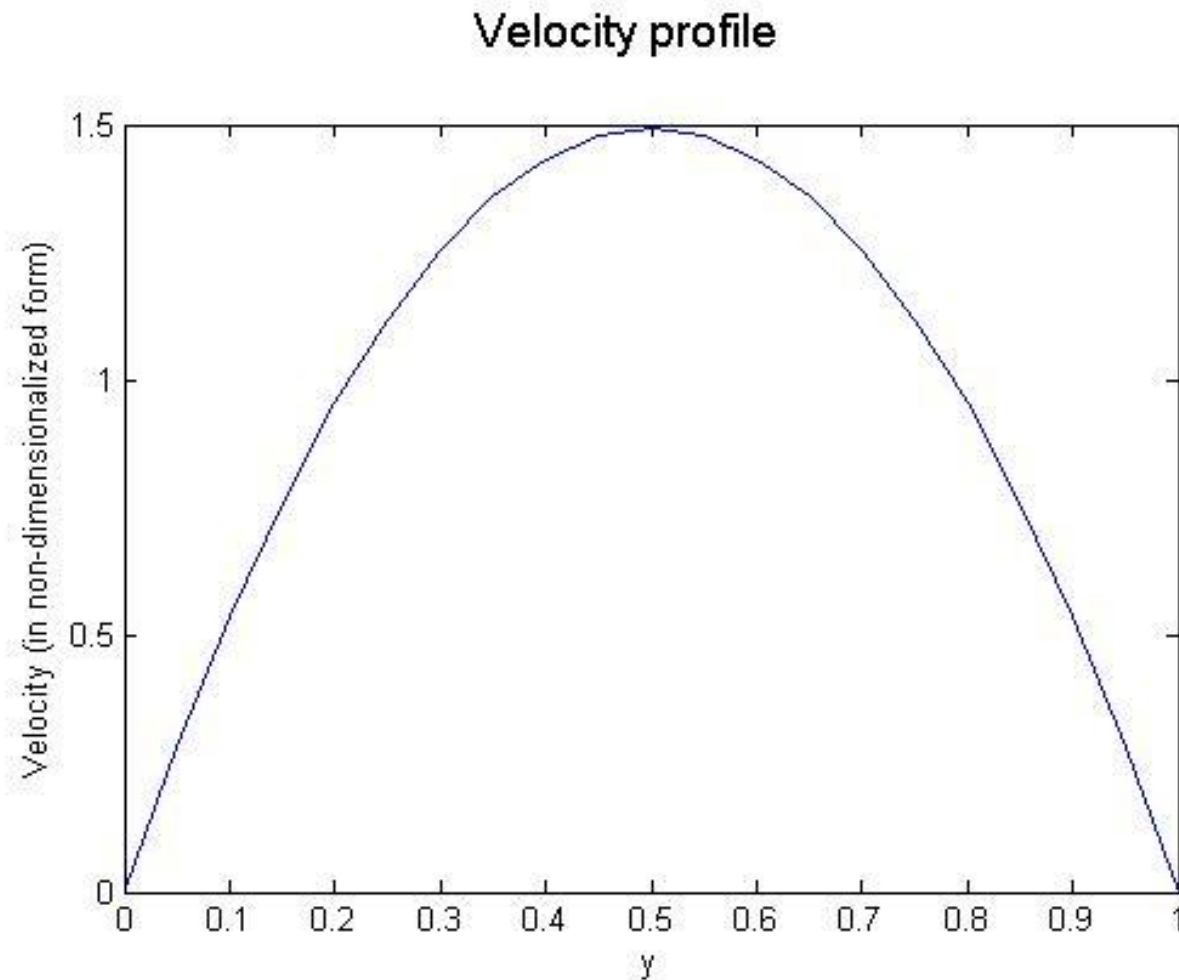
Velocity contours across channel



Velocity contours zoomed at inlet



Velocity Profile near the exit





TEMPERATURE PROFILE

Temperature profile calculation

- $$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$

- Non-dimensionalizing:

- $$\theta = \frac{T - T_{\infty}}{T_w - T_{\infty}}$$

- $$\frac{\partial \theta}{\partial \tilde{t}} + \tilde{u} \frac{\partial \theta}{\partial \tilde{x}} + \tilde{v} \frac{\partial \theta}{\partial \tilde{y}} = \frac{1}{\text{Re}^* \text{Pr}} \left(\frac{\partial^2 \theta}{\partial \tilde{x}^2} + \frac{\partial^2 \theta}{\partial \tilde{y}^2} \right)$$

Finite Difference Approximation

- $$\frac{\partial \theta}{\partial \tilde{t}} + \tilde{u} \frac{\partial \theta}{\partial \tilde{x}} + \tilde{v} \frac{\partial \theta}{\partial \tilde{y}} = \frac{1}{\text{Re}^* \text{Pr}} \left(\frac{\partial^2 \theta}{\partial \tilde{x}^2} + \frac{\partial^2 \theta}{\partial \tilde{y}^2} \right)$$

- $$\frac{\theta_{i,j}^{n+1} - \theta_{i,j}^n}{\Delta \tilde{t}} = - \left(\tilde{u}_{i,j}^n \frac{\theta_{i+1,j}^n - \theta_{i-1,j}^n}{2\Delta \tilde{x}} + \tilde{v}_{i,j}^n \frac{\theta_{i,j+1}^n - \theta_{i,j-1}^n}{2\Delta \tilde{y}} \right)$$

$$+ \frac{1}{\text{Re}^* \text{Pr}} \left(\frac{\theta_{i+1,j}^n - 2\theta_{i,j}^n + \theta_{i-1,j}^n}{\Delta \tilde{x}^2} + \frac{\theta_{i,j+1}^n - 2\theta_{i,j}^n + \theta_{i,j-1}^n}{\Delta \tilde{y}^2} \right)$$

Temperature at new time

$$\theta_{i,j}^{n+1} = \theta_{i,j}^n + \Delta \tilde{t} \left[- \left(\tilde{u}_{i,j}^n \frac{\theta_{i+1,j}^n - \theta_{i-1,j}^n}{2\Delta \tilde{x}} + \tilde{v}_{i,j}^n \frac{\theta_{i,j+1}^n - \theta_{i,j-1}^n}{2\Delta \tilde{y}} \right) + \frac{1}{\text{Re} * \text{Pr}} \left(\frac{\theta_{i+1,j}^n - 2\theta_{i,j}^n + \theta_{i-1,j}^n}{\Delta \tilde{x}^2} + \frac{\theta_{i,j+1}^n - 2\theta_{i,j}^n + \theta_{i,j-1}^n}{\Delta \tilde{y}^2} \right) \right]$$

```
for i = 2:nx - 1
    for j = 2:ny - 1
        Conv1 = -u(j,i)*(thetha_prime(j,i+1) - thetha_prime(j,i - 1))/(2*dx);
        Conv2 = -v(j,i)*(thetha_prime(j+1,i) - thetha_prime(j-1,i))/(2*dy);
        diff1 = (1/(Re*Pr))*(thetha_prime(j,i-1) + thetha_prime(j,i+1) - 2*thetha_prime(j,i))/dx^2;
        diff2 = (1/(Re*Pr))*(thetha_prime(j+1,i) + thetha_prime(j-1,i) - 2*thetha_prime(j,i))/dy^2;
        thetha(j,i) = thetha_prime(j,i) + delta_t*(Conv1 + Conv2 + diff1 + diff2);
    end
end
```

Boundary Conditions:

- Inlet:

$$\theta = 0$$

- Outflow:

$$\frac{\partial \theta}{\partial \tilde{x}} = 0$$

- Top Wall and Bottom Wall:

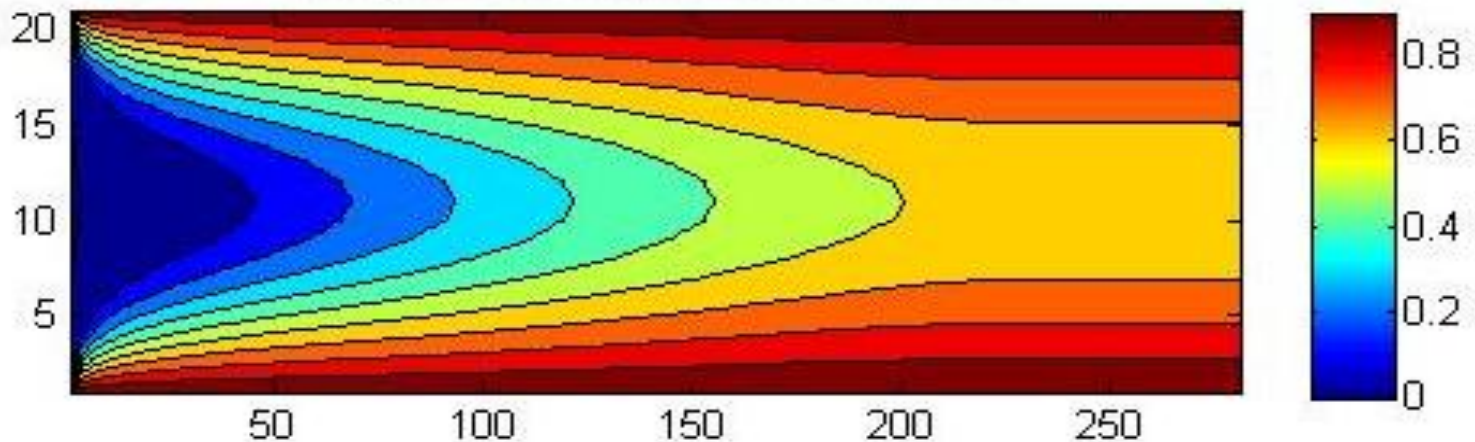
$$\theta = 1$$

```
thetha(1,:) = 1;  
thetha(ny,:) = 1;  
thetha(2:ny - 1,1) = 0;  
thetha(2:ny - 1,nx) = thetha(2:ny - 1,nx - 1);
```

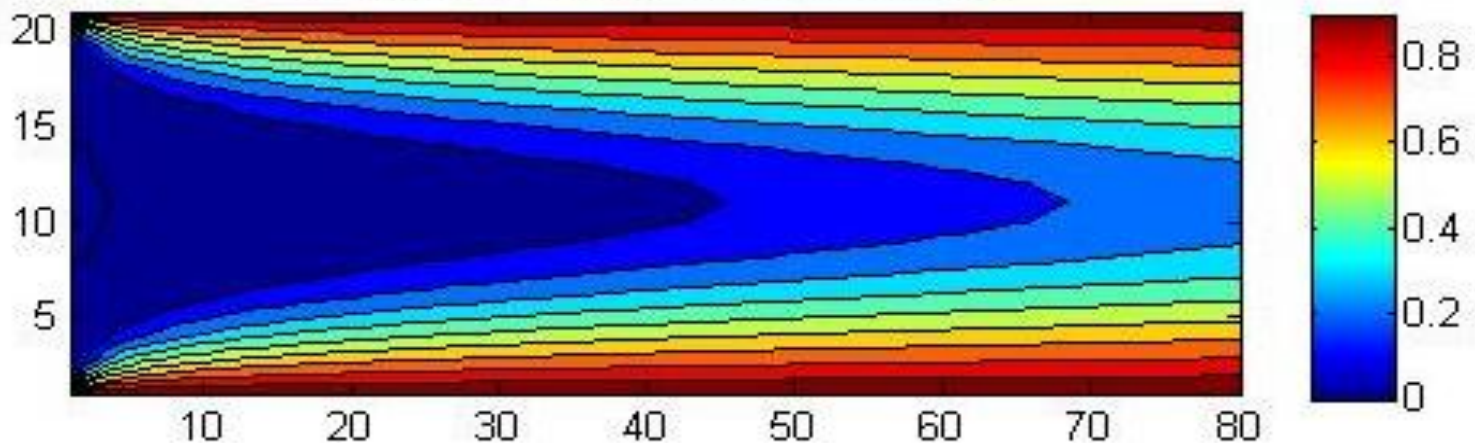

Temperature contours

Temperature Contours

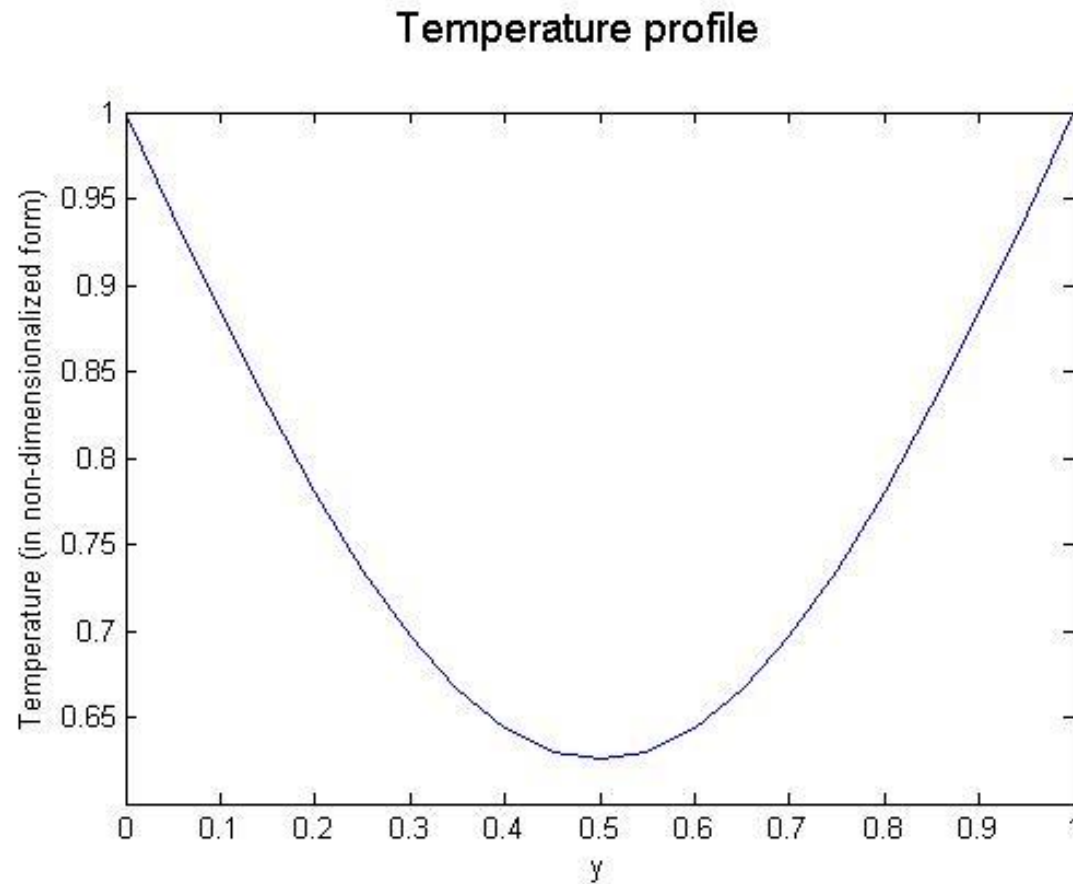
Temperature contours across channel



Temperature contours zoomed at inlet



Temperature profile



Nusselt Number

- From Fourier's law of conduction and Newton's law of cooling:

$$-k \frac{\partial T}{\partial y} = h(T - T_{\infty})$$

$$\Rightarrow -k \frac{(T_w - T_{\infty}) \partial \theta}{H \partial \tilde{y}} = h \theta (T_w - T_{\infty})$$

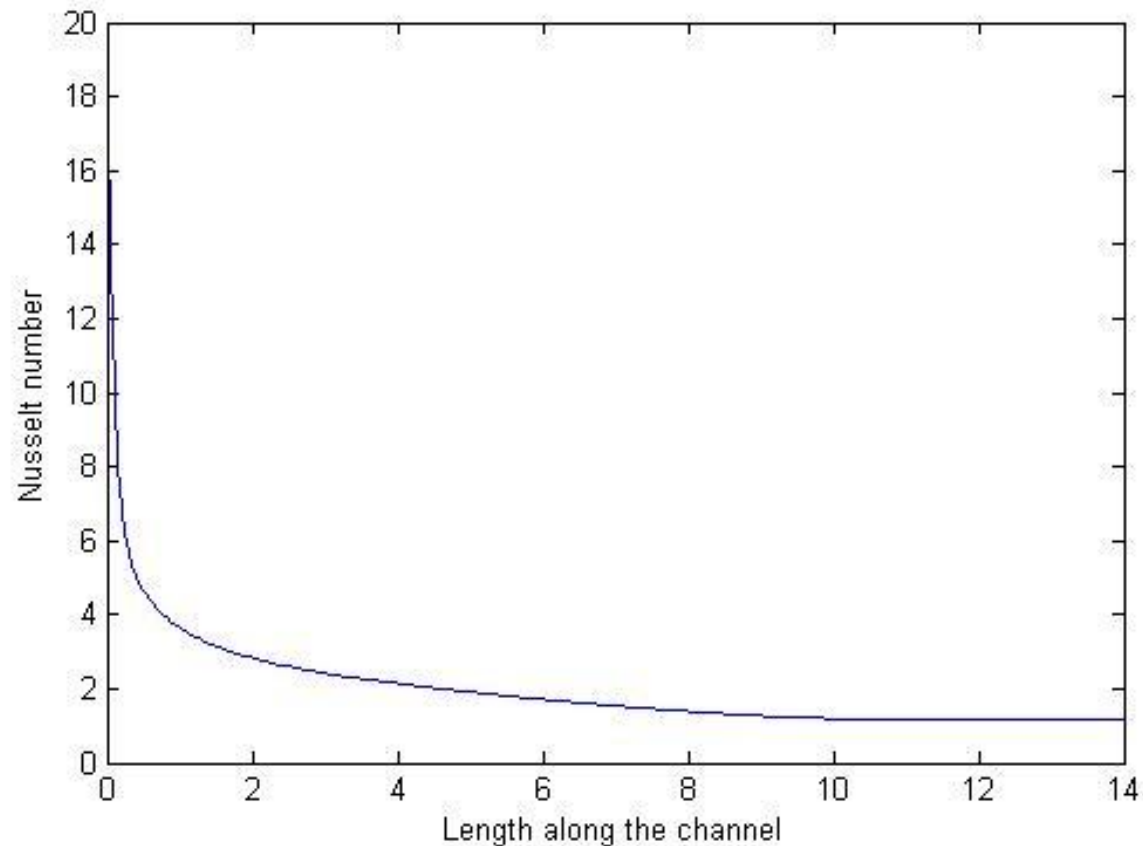
$$\Rightarrow \frac{hH}{k} = Nu = -\frac{1}{\theta} \frac{\partial \theta}{\partial \tilde{y}}$$

$$Nu_{wall} = -\frac{1}{\theta_{wall}} \left(\frac{\partial \theta}{\partial \tilde{y}} \right)$$

$$\Rightarrow Nu_{wall} = -\frac{\partial \theta}{\partial \tilde{y}}$$

Variation of Nusselt Number near the wall

Variation of Nusselt Number along the length of channel



Local Nusselt Number

Steady state reached

Local Nusselt Number near the walls = 2.042



References:

- nptel.ac.in/courses/112104030/pdf/lecture25.pdf
- Fully Developed Pipe and Channel Flows: Indo – German Winter Academy, 2006