

Turbulence phenomenology

The Gioia[‡] way.

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Velocity component at s scale

$$u_s^2 = \int_0^s E(\sigma) \sigma^{-2} d\sigma = \int_{1/s}^{\infty} E(k) dk.$$

with $E(\sigma) \sim \varepsilon^{2/3} \sigma^{5/3} \mathbf{c}_d(\eta/\sigma) \mathbf{c}_e(R/\sigma)$ and $E(k) \sim \varepsilon^{2/3} k^{-5/3} \mathbf{c}_d(\eta k) \mathbf{c}_e(Rk)$ ¹.

$$\begin{cases} \mathbf{c}_d(x) = \exp(-\beta_d x) \\ \mathbf{c}_e(x) = (1 + \beta_e x^{-2})^{-17/6} \end{cases}.$$

\mathbf{c}_d 形式来自 Gioia 等(2006), \mathbf{c}_e 取自 von Kármán. 在惯性区 $\eta \ll s \ll R$, 两个修正项均为 1².

¹Note: Gioia 等(2006) 中使用 $\mathbf{c}_e(\sigma/R)$ 形式, 注意到 $R/\sigma = Rk$, 为了 \mathbf{c}_e 的统一形式将其定义为 $\mathbf{c}_e(R/\sigma)$.

²为什么调整耗散区和含能区系数无法推导常见的 -1 标度律? 参考(Nikora, 1999)。



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The uniform form of velocity u_s

Let $\xi = sk = s/\sigma$, rewrite u_s in a uniform form:

$$u_s \sim (\varepsilon s)^{1/3} \left[\int_1^\infty \xi^{-5/3} \mathbf{c}_d \left(\frac{\eta}{s} \xi \right) \mathbf{c}_e \left(\frac{R}{s} \xi \right) d\xi \right]^{1/2} \triangleq (\varepsilon s)^{1/3} \sqrt{\mathcal{I}}.$$

Takeaway msg

- $u_s \sim (\varepsilon s)^{1/3}$ in inertial range ($\eta \ll s \ll R$).
- 提取涡体 (尺度为 s) 特征速度 u_s 的问题转化为修正函数 \mathcal{I} 的讨论,
 $\mathcal{I}(\eta/s, R/s) \triangleq \int_1^\infty \xi^{-5/3} \mathbf{c}_d \left(\frac{\eta}{s} \xi \right) \mathbf{c}_e \left(\frac{R}{s} \xi \right) d\xi.$



The phenomenology big picture

- Energy cascade

$$u_s^3/s \sim u_R^3/R.$$

- With $\varepsilon \sim u_R^3/R$, $\eta = (\nu^3/\varepsilon)^{1/4} \sim R \cdot Re^{-3/4}$.
- With $\varepsilon \sim u_\tau^3/\kappa y$ and $v_n \sim (\varepsilon s)^{1/3}$, for inertial range eddies (especially the log layer, i.e. the outer layer $s \sim y$) $v_n \sim u_\tau (s/y)^{1/3} \sim u_\tau^3$.

³因此，在忽略黏性底层的外区，掺混动量的涡体天然具有 u_τ 的特征速度。



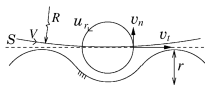
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The Gioia way: Local shear stress model

Eddies (u_s, s) that straddle wetted surface $W_y \Rightarrow$ shear stress τ ,

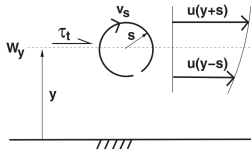
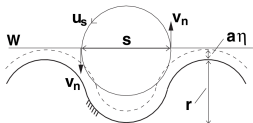
- v_n 代表涡体传递动量的速率，取决于涡体的特征速度 ($\sim u_s$)
- v_t 代表涡体能够传递的动量大小，取决于湿面积两侧的动量差 ($\propto \frac{\partial u}{\partial y} \cdot s$)

$$\tau \sim \rho v_t v_n.$$



- Local wall shear stress model (Gioia 等, 2006): $v_t \sim V, v_n \sim u_{r+a\eta}$
- Local water column shear stress model (Gioia 等, 2010):

$$v_t \sim u(y+s) - u(y-s) \approx 2su'(y) \sim 2y \cdot u'(y), v_n \sim u_y$$



Unify the local shear stress model

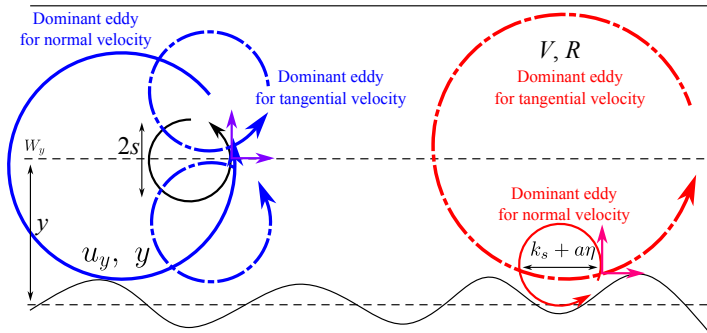


图 1: The unified picture of the Gioia model.



Unify the local shear stress model

- 搬运工 v_n : 近床面位置, 特征涡体由粗糙高度 k_s 和黏性底层 $a\eta$ 共同控制 $s = k_s + a\eta$ [‡]; 外区部分的特征涡体完全由床面高度 $s \sim y$ 控制⁴
- 货物 v_t [‡]: 提供 v_n 分量的涡体起到动量搬运工的作用, 而其空间尺度决定⁵了其所能搬运的动量 v_t
 - 一旦涡体尺度 s 确定, v_n 和 v_t 同时确定? 那么大涡叠加小涡的模型不再必要, 仅需引入搬运工涡体, 与附着涡模型类似。
 - 外区速度梯度引起的能够搬运的动量差

$$v_t \sim 2su'(y) \sim 2y \cdot u'(y).$$

- 壁面附近的动量差^{‡6}

$$\lim_{y \rightarrow 0} v_t \sim (k_s + a\eta) \lim_{y \rightarrow 0} u'(y) = \frac{(k_s + a\eta)u_\tau^2}{\nu} \sim (k_s + a\eta) \frac{(k_s/R)^{\frac{1}{3}} V^2}{\nu}.$$

⁴Townsend 附着涡模型存在类似的特征尺度正比于床面距离的一系列自相似涡体。或许可视为仅考虑外区涡体的特例, 这导致附着涡模型仅适用于对数区(Marusic 等, 2019)。

⁵因为给定涡体空间尺度 s , 此距离覆盖的速度梯度是关于 s 的函数。

⁶Strickler-type for transitional rough $\tau_0 \propto (k_s/R)^{\frac{1}{3}} \rho V^2$.



The Gioia eddy model vs Attached eddy model



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The Gioia eddy model vs Eddy viscosity model






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The vision

- The local shear stress model \Rightarrow sub-grid stress model
- New sub-grid stress model \Rightarrow Mesh optimizer




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