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AIM - The first objective is to estimate the parameters of Antoine equation using regression. While several functional forms are proposed to predict vapor pressure (p_{vap}) as a function of temperature, the Antoine equation is often preferred. The form of the equation is:

$$\ln(p^{vap}) = A - \frac{B}{T}$$

where A and B are parameters that vary with compounds, and T is temperature. The data of p_{vap} for different temperature is given for CH₃OH and H₂O.

1. Determine A and B for CH₃OH and H₂O using linear regression on the training dataset.
2. Report the training and test dataset's root mean squared error.
3. Make plots for CH₃OH and H₂O to show the predicted $\ln(p_{vap})$ and the actual $\ln(p_{vap})$ as a function of temperature (T).

The second objective is to compute the molar volume of CO₂ and H₂ in mol/m³ at 78 bar and 210 °C using ideal gas, Redlich-Kwong (RK), and Peng-Robinson (PR) equations of state. RK and PR belong to a class of cubic equation of state. The generic form of the equation can be stated as follows:

$$V = \frac{RT}{P} + b - \frac{a(T)}{P} \frac{V - b}{(V + \epsilon b)(V + \sigma b)}$$

METHOD -

1. Load the data for both components given in the Excel sheet using the readmatrix function.
2. Use the fitlm function with the training dataset to estimate A and B for CH₃OH and H₂O.
3. Using the computed parameters, estimate p_{vap} for the testing set and compute the root mean squared error.

The above equation is nonlinear in V and may be solved using the fsolve function. It is often convenient to define the following dimensionless quantities:

$$\beta = \frac{bP}{RT}, q = \frac{a(T)}{bRT}, \Omega = \frac{\beta T_r}{P_r}, \Psi = \frac{q\Omega T_r}{a(T_r, \omega)}, T_r = \frac{T}{T_c}, P_r = \frac{P}{P_c}$$

Table 1. Parameters for equations of state.

Eq. of state	$\alpha(T_r)$	σ	ϵ	Ω	Ψ
RK	$T_r^{-0.5}$	1	0	0.08664	0.42748
PR	$[1 + (0.37464 + 1.54226\omega - 0.26992\omega^2)(1 - T_r^{0.5})]^2$	$1+\sqrt{2}$	$1-\sqrt{2}$	0.0778	0.45724

Table 2. Parameters for CO₂ and H₂.

Substance	P_c (bar)	T_c (K)	ω
CO ₂	7.38	304.15	0.225
H ₂	12.93	33.18	-0.22

RESULT -

- $A_{\text{CH}_3\text{OH}} = 24.850034739689832$
- $A_{\text{H}_2\text{O}} = 24.695726929983188$
- $B_{\text{CH}_3\text{OH}} = 4.510372064085043\text{e}+03$
- $B_{\text{H}_2\text{O}} = 4.940460460481752\text{e}+03$
- $\text{rms_test_CH}_3\text{OH} = 0.073576299704207$
- $\text{rms_train_CH}_3\text{OH} = 0.073996352008509$
- $\text{rms_test_H}_2\text{O} = 0.075949087194976$
- $\text{rms_train_H}_2\text{O} = 0.078482677132507$
- $V_{\text{CO}_2\text{_PR}} = 5.845814056333681\text{e}-04$
- $V_{\text{CO}_2\text{_RK}} = 5.881422791853185\text{e}-04$
- $V_{\text{H}_2\text{_PR}} = 5.128264014540197\text{e}-04$
- $V_{\text{H}_2\text{_RK}} = 5.184023916415067\text{e}-04$

