

HAMT - Tool for simulation of Heat And Mass Transfer

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1 Numerics

According to [1] the Gauss divergence theorem can be rewritten as

$$\int_V \nabla \vec{F} \, d^n V = \oint_S \vec{F} \cdot \vec{n} \, d^{n-1} S \quad (1.1)$$

Using ∇f for \vec{F} Eqn. (1.1) can be rewritten as

$$\int_V \nabla^2 f \, d^n V = \oint_S (\nabla f) \cdot \vec{n} \, d^{n-1} S \quad (1.2)$$

For the numerical solution a cell wise discretization is made. Assuming that $\nabla^2 f$ is constants over a cell the equation above reduces to

$$V_C \cdot \nabla^2 f = \sum_i^N (\nabla f) \cdot \vec{n}_i \cdot A_i. \quad (1.3)$$

1.1 2D Application for triangular mesh

For a triangular mesh assuming one can write

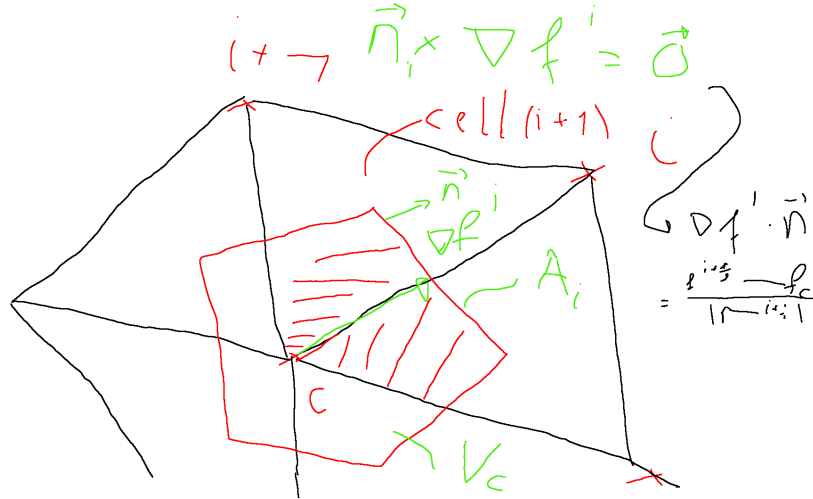


Figure 1.1: Test

$$\nabla f \cdot \vec{n}_i = \frac{f_i - f_C}{|\vec{r}_i|} \quad (1.4)$$

for a 2d geometry $A_{C,i}$ becomes a line segment

$$A_i = |\vec{b}_{i+1} - \vec{b}_i| = L_i \quad (1.5)$$

where \vec{b}_i is the barycentre of the last cell containing the point i . In this context V_C becomes the volume of created new cell A_C which is defined as

$$A_C = \frac{1}{2} \cdot \sum_i^N \vec{b}_{i+1} \times \vec{b}_i \quad (1.6)$$

This leads to

$$\nabla^2 f = \frac{1}{A_C} \cdot \sum_i^N \frac{f_i - f_C}{|\vec{r}_i|} \cdot |\vec{b}_{i+1} - \vec{b}_i|. \quad (1.7)$$

2 Heat Transfer

The base equation for the heat transfer is the balance equation of the form

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \vec{j} = f(\vec{r}, t) \quad (2.1)$$

where ρ is the density of the quantity in question, \vec{j} is the flux, \vec{r} is the position vector and t is time. For heat transfer problem we define ρ as the volumetric heat density q which is defined as

$$q = \frac{Q}{V} = c \rho T \quad (2.2)$$

\vec{j} is equivalent to the heat flux \vec{q}

$$\vec{q} = -\lambda \nabla T \quad (2.3)$$

and the source $f(\vec{r}, t)$ is the volumetric heat source $\dot{q}_v(\vec{r}, t)$. Inserting 2.2 and 2.3 in 2.1 leads to the heat transfer equation

$$\frac{\partial(c \rho T)}{\partial t} + \nabla \cdot (-\lambda \nabla T) = \dot{q}_v(\vec{r}, t) \quad (2.4)$$

where the quantities are defined as seen in table 2.1.

Table 2.1: Heat Transfer - parameters

Quantity	Description	Unit
c	Specific heat capacity	$\text{J kg}^{-1} \text{K}^{-1}$
ρ	Density	kg m^{-3}
T	Temperature	K
λ	Thermal conductivity	$\text{W m}^{-1} \text{K}^{-1}$
\dot{q}_v	Volumetric heat source	W m^{-3}

2.1 Homogeneous Heat Transfer Equation

Assuming no time dependence $\frac{\partial(c \rho T)}{\partial t} = 0$ and no heat source $\dot{q}_v(\vec{r}, t) = 0$ Eqn. (2.4) reduces to

$$\nabla \cdot (\lambda \nabla T) = 0 \quad (2.5)$$

where $\lambda = \text{fn}(\vec{r})$. According to the product rules for vector calculus Eqn. (2.5) evaluates to

$$\nabla \cdot (\lambda \nabla T) = \nabla T \cdot (\nabla \lambda) + \lambda (\nabla \cdot \nabla T) \quad (2.6)$$

$$\nabla \cdot (\lambda \nabla T) = \nabla \lambda \cdot \nabla T + \lambda \cdot \nabla^2 T \quad (2.7)$$

which leads to

$$\nabla \lambda \cdot \nabla T + \lambda \cdot \nabla^2 T = 0. \quad (2.8)$$

2.1.1 2D Cartesian Formulation

Evaluating Eq. (2.5) for two variables in cartesian form leads to

$$\nabla(\lambda \nabla T) = \frac{\partial}{\partial x} \left(\lambda \frac{\partial T}{\partial x} \right) + \frac{\partial}{\partial y} \left(\lambda \frac{\partial T}{\partial y} \right) \quad (2.9)$$

$$= \frac{\partial \lambda}{\partial x} \frac{\partial T}{\partial x} + \lambda \frac{\partial^2 T}{\partial x^2} + \frac{\partial \lambda}{\partial y} \frac{\partial T}{\partial y} + \lambda \frac{\partial^2 T}{\partial y^2} \quad (2.10)$$

$$= \frac{\partial \lambda}{\partial x} \frac{\partial T}{\partial x} + \frac{\partial \lambda}{\partial y} \frac{\partial T}{\partial y} + \lambda \frac{\partial^2 T}{\partial x^2} + \lambda \frac{\partial^2 T}{\partial y^2} \quad (2.11)$$

$$= \nabla \lambda \cdot \nabla T + \lambda \cdot \nabla^2 T \quad (2.12)$$

2.1.2 2D Cylindrical Formulation

Evaluating Eq. (2.5) for two variables in cartesian form leads to

$$\nabla(\lambda \nabla T) = \frac{\partial}{\partial r} \left(\lambda \frac{\partial T}{\partial r} \right) + \frac{1}{r} \frac{\partial}{\partial \phi} \left(\lambda \frac{1}{r} \frac{\partial T}{\partial \phi} \right) \quad (2.13)$$

$$= \frac{\partial \lambda}{\partial r} \frac{\partial T}{\partial r} + \lambda \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \left[\frac{\partial \lambda}{\partial \phi} \frac{1}{r} \frac{\partial T}{\partial \phi} + \lambda \frac{1}{r} \frac{\partial^2 T}{\partial \phi^2} \right] \quad (2.14)$$

$$= \frac{\partial \lambda}{\partial r} \frac{\partial T}{\partial r} + \frac{1}{r} \frac{\partial \lambda}{\partial \phi} \frac{1}{r} \frac{\partial T}{\partial \phi} + \lambda \left[\frac{\partial^2 T}{\partial r^2} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} \right] \quad (2.15)$$

$$= \nabla \lambda \cdot \nabla T + \lambda \left[\frac{\partial^2 T}{\partial r^2} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} \right] \quad (2.16)$$

2.2 Finite-Difference Scheme - Triangular Unordered 2D Grid

Using a second order Taylor series expansion around a arbitray point in space for two variables on can write

$$T f(x; a) = f(a) + \sum_{j=1}^2 \frac{\partial f(a)}{\partial x_j} + \frac{1}{2} \sum_{j=1}^2 \sum_{k=1}^2 \frac{\partial^2 f(a)}{\partial x_j \partial x_k} (x_k - a_k) + O(\Delta^3) \quad (2.17)$$

2.3 Finite-Difference Scheme - Homogeneous Equidistant 2D Grid

2.3.1 Boundary Conditions

For all boundary condition is present the dirichlet boundary condtions always orride other boudnary conditions on contact nodes. If two cells with different dirichlet boundary condtions touch, a arichmetical mean is taken.

Corner Boundary Conditions

Examples buttom left corner

$$T_{i+1,j} - T_{i,j} = \Delta x_1 c_1 \quad (2.18)$$

$$T_{i,j+1} - T_{i,j} = \Delta x_2 c_2 \quad (2.19)$$

By adding the two functions one gets

$$T_{i+1,j} + T_{i,j+1} - 2T_{i,j} = \Delta x_1 c_1 + \Delta x_2 c_2. \quad (2.20)$$

Radiation Boundary Conditions

$$\vec{q}_r = \epsilon \sigma T^4 \vec{n} \quad (2.21)$$

Using the Taylor series

$$T f(x; a) = \sum_{n=0}^{\infty} \frac{f^{(n)}(a)}{n!} (x - a)^n \quad (2.22)$$

we get the linearized equation for the heat flux due to radiation

$$T \dot{q}_r(T; T_0) = (4 \epsilon \sigma T_0^3) T - 3 \epsilon \sigma T_0^4. \quad (2.23)$$

Using equation (2.3)

$$-\lambda \frac{\partial T}{\partial x} = T \dot{q}_r(T; T_0) \quad (2.24)$$

leads to the discretized, linear equation

$$(1 + 4 k T_0^3) T_i - T_{i-1} = 3 k T_0^4 \quad (2.25)$$

where

$$k = \frac{\epsilon \sigma \Delta x}{\lambda} \quad (2.26)$$

Table 2.2: Radiation Boundary Condition - parameters

Quantity	Description	Unit
ϵ	Emissivity factor	—
σ	Stefan-Boltzmann constant	$\text{W m}^{-2} \text{K}^{-4}$
Δx	Spatial step	m

2.3.2 Cartesian Coordinates

The homogeneous heat equation in cartesian coordinates is expressed as

$$\lambda \frac{\partial^2 T}{\partial x^2} + \lambda \frac{\partial^2 T}{\partial y^2} + \lambda \frac{\partial^2 T}{\partial z^2} = 0 \quad (2.27)$$

By assuming only the x and y directions equation (2.27) reduces to

$$\lambda \frac{\partial^2 T}{\partial x^2} + \lambda \frac{\partial^2 T}{\partial y^2} = 0. \quad (2.28)$$

Using equation (??) equation (2.28) can be discretized as

$$\lambda_{i+1,j} T_{i+1,j} + \lambda_{i,j+1} T_{i,j+1} - \lambda_{tot} T_{i,j} + \lambda_{i-1,j} T_{i-1,j} + \lambda_{i,j-1} T_{i,j-1} = 0 \quad (2.29)$$

where

$$\lambda_{tot} = \lambda_{i+1,j} + \lambda_{i-1,j} + \lambda_{i,j+1} + \lambda_{i,j-1}. \quad (2.30)$$

In case any of the λ parameters is to be taken on a boundary between two segments, a mean between the two is to be taken. The correctness of this assumption can be proven by setting up 4 equations around a center node using Fourier's law. For $\lambda = \text{const}$ the equation reduces to

$$T_{i+1,j} + T_{i,j+1} - 4 T_{i,j} + T_{i-1,j} + T_{i,j-1} = 0 \quad (2.31)$$

2.3.3 Cylinder Coordinates

while in cylinder coordinates as

$$\lambda \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \lambda \frac{1}{r^2} \frac{\partial^2 T}{\partial \phi^2} + \lambda \frac{\partial^2 T}{\partial z^2} = 0. \quad (2.32)$$

2.3.4 Verification

Heat conductivity through a layered wall

$$\dot{q} = \left(\sum_{i=1}^N \frac{\Delta x_i}{\lambda_i} \right)^{-1} \Delta T \quad (2.33)$$

Bibliography

- [1] G Erlebacher. “Finite difference operators on unstructured triangular meshes”. In: *The Free-Lagrange Method*. Springer, 1985, pp. 22–53.