

## Project

In recent years, carbon capture and sequestration (CCS) presented itself as the ultimate solution to mitigate climate change. No wonder, it gained tremendous support from the scientific community [1]. Scientists around the world ought to model efficient adsorption technologies and develop new materials for CO<sub>2</sub> capture. Depending on the CO<sub>2</sub> source, some technologies do better than others. In general, Pressure Swing Adsorption/Vacuum Swing Adsorption (PSA/VSA) is considered one of the promising options [2]. In this project, the PSA/VSA process will be implemented to capture CO<sub>2</sub> from post-combustion power plant flue gas. A preliminary process flow diagram is shown in Figure 1. The flue gas coming in at atmospheric pressure is cooled down to 25°C prior to adsorption. Once the adsorbent is saturated with CO<sub>2</sub>, the pressure is dropped to 0.2 bar, keeping the same temperature, and CO<sub>2</sub> is desorbed. Finally, the CO<sub>2</sub> rich stream is compressed to 100-150 bars to be stored in geological formations.

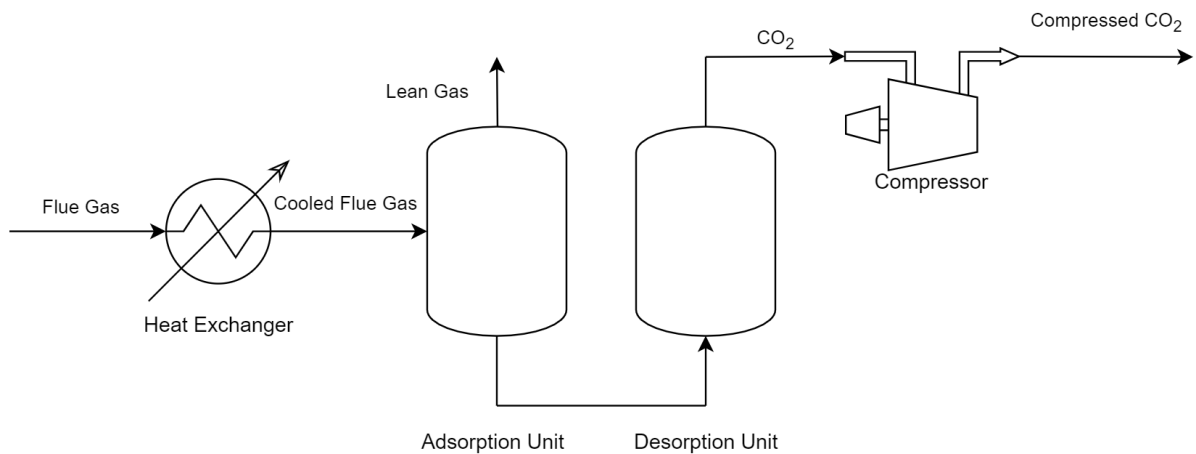


Figure 1: Flow diagram of the PSA/VSA process

Metal Organic Frameworks (MOFs) are crystalline nanoporous materials that have emerged as good sorbents for post-combustion CO<sub>2</sub> capture due to their high CO<sub>2</sub> capacity and CO<sub>2</sub>/N<sub>2</sub> selectivity [3]. Assuming that the flue gas contains only CO<sub>2</sub> (~15%) and N<sub>2</sub> (~85%), you need to rank a given group of materials based on some basic properties:

1. Compute the density (g.cm<sup>-3</sup>), accessible surface area - ASA (A<sup>2</sup>), accessible probe-occupiable volume - POAV (A<sup>3</sup>) and porosity of the different structures by running pore analysis. Use a probe radius of 1.525 Å (4 each structure)
2. Compute the henry coefficients for CO<sub>2</sub> and N<sub>2</sub> at 25°C (2 each structure). Rank the structures based on their affinity for CO<sub>2</sub> (5)
3. Compute CO<sub>2</sub> and N<sub>2</sub> pure component isotherms at 25°C for the given structures (3 each structure). Plot the pure isotherms per molecule (3)
4. Calculate the CO<sub>2</sub> working capacity (WC) for the different structures (4 each structure)
5. Calculate the CO<sub>2</sub>/N<sub>2</sub> selectivity (S) for the different structures (2 each structure)
6. Rank the structures using a WC vs. S plot (10)
7. Is the screening model conclusive as to which material performs best in a PSA/VSA process for post-combustion CO<sub>2</sub> capture ? Discuss the level at which the screening was performed and come up with more complex key performance indicators (10)
8. Organization of the report (6)

## Hints

1. For the material structures, please refer to the Moodle page. These structures were already optimized and their charges were calculated. Use the following simulation parameters:
  - Zeo++ volpo samples: 10,000
  - Number of samples for block calculation: 100
  - Number of Widom cycles: 50,000
  - Number of GCMC initialization cycles: 500
  - Number of GCMC production cycles: 5,000
  - Maximum distance between pressure points: 0.6
  - Pressure range: 0.2 to 10.2 bars
2. The working capacity measures how much CO<sub>2</sub> can be theoretically recovered, i.e. the maximum recoverable amount of CO<sub>2</sub> given the process conditions:

$$WC = q_{adsorption} - q_{desorption}$$

Where  $q$  is the binary loading of CO<sub>2</sub> in mmol.g<sup>-1</sup> obtained from IAST calculations.

3. The ideal selectivity gives an indication on the competitiveness of adsorption between the different components of a gas mixture:

$$S_{CO_2/N_2} = \frac{q_{CO_2} y_{N_2}}{q_{N_2} y_{CO_2}}$$

Where  $q$  is the binary loading, obtained from IAST calculations, at the adsorption conditions in mmol.g<sup>-1</sup>, and  $y$  is the molar fraction of the component in the flue gas.

## References

- [1] M. Bui *et al.*, “Carbon capture and storage (CCS): The way forward,” *Energy Environ. Sci.*, vol. 11, no. 5, pp. 1062–1176, 2018.
- [2] M. T. Ho, G. W. Allinson, and D. E. Wiley, “Reducing the cost of CO<sub>2</sub> capture from flue gases using pressure swing adsorption,” *Ind. Eng. Chem. Res.*, vol. 47, no. 14, pp. 4883–4890, 2008.
- [3] T. D. Burns *et al.*, “Prediction of MOF Performance in Vacuum Swing Adsorption Systems for Postcombustion CO<sub>2</sub> Capture Based on Integrated Molecular Simulations, Process Optimizations, and Machine Learning Models,” *Environ. Sci. Technol.*, vol. 54, no. 7, pp. 4536–4544, 2020.
- [4] A. Ajenifuja, L. Joss, and M. Jobson, “A New Equilibrium Shortcut Temperature Swing Adsorption Model for Fast Adsorbent Screening,” 2020.