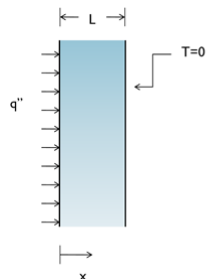


# ICE for PDE

## Problem 1.



$$\rho c_p \frac{\partial T}{\partial t} = k \frac{\partial^2 T}{\partial x^2}$$

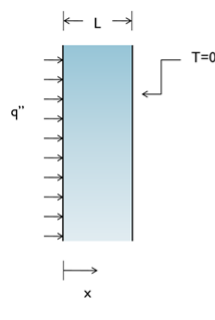
$$T(x, 0) = 0$$

$$-k \left. \frac{\partial T}{\partial x} \right|_{x=0} = q''$$

$$T(L, t) = 0$$

$L=0.1\text{m}$ ,  $k=200 \text{ W}/(\text{m.K})$ ,  $\rho = 10000 \text{ kg}/\text{m}^3$ ,  $c_p = 500 \text{ J}/(\text{kg.K})$ ,  $q'' = 1 \times 10^6 \text{ W}/\text{m}^2$ .

## Problem 2



$$\rho c_p \frac{\partial T}{\partial t} = k \frac{\partial^2 T}{\partial x^2}$$

$$T(x, 0) = 0$$

$$-k \left. \frac{\partial T}{\partial x} \right|_{x=0} = q''$$

$$-k \left. \frac{dT}{dx} \right|_{x=L} = h(T - T_{bulk})$$

$T_{bulk} = 20^\circ\text{C}$ ,  $h = 1 \times 10^4 \text{ W}/\text{m}^2\text{K}$ .

## Problem 3

The advection-diffusion equation is used to compute the distribution of concentration along the length of a rectangular chemical reactor.

$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2} - U \frac{\partial c}{\partial x} - kc$$

where  $c$ =concentration ( $\text{mg}/\text{m}^3$ ),  $t$ =time(min),  $D$ = a diffusion

coefficient ( $\text{m}^2/\text{min}$ ),  $x$ =distance along the tank's longitudinal axis (m) where  $x=0$  at the tank's inlet,  $U$ =velocity in the  $x$  direction ( $\text{m}/\text{min}$ ), and  $k$ =a reaction rate ( $\text{min}^{-1}$ ) whereby the chemical decays to another form. Develop an explicit scheme to solve this equation numerically. Test it for  $k=0.15$ ,  $D=100$ , and  $U=1$  for a tank of length 10 m. Use a  $\Delta x = 1\text{m}$ , and a step size  $\Delta t = 0.005$ . Assume that the inflow concentration is 100 and that the initial concentration in the tank is zero. Perform the simulation from  $t=0$  to 100 and plot the final resulting concentration versus  $x$ .