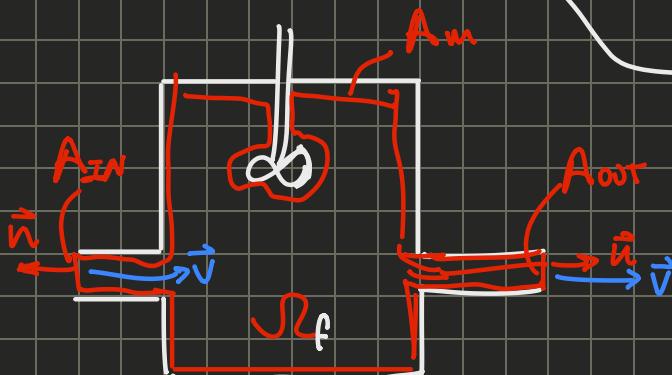


## Lesson 5 -

What we did yesterday and will do today should be reviewed as quick as possible.

Mass in the control volume can either accumulate or change through a differential in the mass entering and exiting at the two ports.

### Energy Balance



(Balance of Power really since

$dM/dt = 0$  Mass of the fluid body

$$\frac{dM}{dt} = 0 \text{ where } M = \int \rho dV$$

linear momentum

$$S(t)$$

Newton's law

$$\vec{\Pi} = \int_{S(t)} \rho \vec{v} dV \rightarrow \frac{d\vec{\Pi}}{dt} = \vec{F}$$

$$\vec{F} = \int_{S(t)} \rho \vec{f} dV + \int_{S(t)} \vec{\sigma} dA$$

summation of all the forces

These laws are for bodies in control volumes.

volume forces field Surface forces such as pressure and friction.

$\vec{\sigma} = -\vec{P}_n + \vec{\tau}$

It's dependent on the speed of deformation of the fluid body (seen in MF)  
strain-rate

14:46

$$\text{In general } \vec{\tau} \propto \frac{\partial v_i}{\partial x_j} \cdot \mu$$

Our equations are instantaneous, we don't need the history, we can take the fluid body as the one which at  $t=\infty$  fills the control volume.

At  $t = \tau \rightarrow \mathcal{V}(\tau) = \mathcal{V}_f \Rightarrow$  For RTT we can.

calculate the  $L_o$  and  $\dot{Q}$   
in the CV without issue.

$$\downarrow = \int_{\mathcal{V}(\tau)} \rho \vec{f} dV + \int_{\partial \mathcal{V}(\tau)} \vec{\sigma} dA$$

$$= \int_{\mathcal{V}_f} \rho \vec{f} dV + \int_{\partial \mathcal{V}_f} \vec{\sigma} dA \quad 14:49$$

since we taking snapshot

$$\vec{\Gamma} = \int_{\mathcal{V}(\tau)} \vec{r} \times \rho \vec{v} dV$$

Angular momentum

$$\frac{d \vec{\Gamma}}{dt} = \vec{M}$$

$\rightarrow$  Moment/Torque of the forces

$$\vec{M} = \int_{\mathcal{V}(t)} \vec{r} \times \rho \vec{v} dV + \int_{\partial \mathcal{V}(t)} \vec{r} \times \vec{\sigma} dA$$

$$\text{For the same reasons} \rightarrow = \int_{\mathcal{V}_f} \vec{r} \times \rho \vec{v} dV + \int_{\partial \mathcal{V}_f} \vec{r} \times \vec{\sigma} dA$$

We will not be developing linear/angular momentum momentum balances since they are not too useful (except for one case)

We can only calculate the rate of change of energy, not the energy exchange. So we calculate power.

We will be using the instantaneous exchange of work and heat.

$\rightarrow$  Instantaneous power that can be exchanged by mechanical or thermal power.

$$\frac{dE}{dt} = \dot{L}_o + \dot{Q}$$

overall

There are other methods of exchanging power but the ones most useful for us.

We need to find  $E$ ,  $L_o$  and  $\dot{Q}$ .  
 $\rightarrow$  why this overall

We focus mainly on  $E$  and  $\dot{L}$ .

$\boxed{E}$

$$E_k = \frac{1}{2} \rho V^2 M \rightarrow \boxed{E_k = \int_{V_2(t)}^{V_1(t)} \frac{1}{2} \rho V^2 dV}$$

speed  
volm

$$E_p = g z M \rightarrow \boxed{E_p = \int_{V_2(t)}^{V_1(t)} \rho g z dV}$$

$$\boxed{U = \int_{V_2(t)}^{V_1(t)} \rho u dV}$$

$$\frac{d}{dt} \int_{V_2(t)}^{V_1(t)} \rho \left( u + \frac{V^2}{2} + gz \right) dV = \dot{L}_o + \dot{Q}$$

$$\frac{dE}{dt}$$

we can say more about  
this

like volume forces

If we only consider only conservative forces, the mechanical power can be seen as a change in potential energy.

Since cannot count it twice, we will not count it as a change in work, therefore the potential energy change is considered as just the change in the potential energy, and only count it here, in  $\frac{dE}{dt}$ .

$$\dot{L}_o = \int_{\partial V(t)} \vec{\sigma} \cdot \vec{v} dA = \int_{\partial V(t)} \vec{\sigma} \cdot \vec{v} dA = \int_{A_m} \vec{\sigma} \cdot \vec{v} dA + \int_{A_{in+out}} \vec{\sigma} \cdot \vec{v} dA$$

$t = \tau$

$$\vec{\sigma} = -P \hat{n} + \vec{\tau}$$

these are not  
dependent on  
how we  
design our  
machine

$$= \dot{L}_o + \int_{A_{in+out}} -P \hat{n} \cdot \vec{v} dA$$

$$\int_{A_{IN+A_{OUT}}} \vec{\sigma} \cdot \vec{v} dA = \int_{A_{IN+A_{OUT}}} -P\vec{n} \cdot \vec{v} dA + \int_{A_{IN+A_{OUT}}} \vec{\tau} \cdot \vec{v} dA$$

Pulse power

Non è 0 perché ci sono punti come allo superficie della turbina dove la velocità non è 0.

If we take the  $A_{IN}$  and  $A_{OUT}$  we can find places in which the velocity is practically uniform and therefore the  $\vec{\tau}$  will be minimal. The power on the circumferential surface is negligible for the calculation since we take the area advantageously.

$$\frac{d}{dt} \int_{V_C(t)} \rho \left( u + \frac{V^2}{2} + g_z \right) dV = \dot{L}_o + \dot{Q}$$

Derived from the RTT

$$= \frac{d}{dt} \int_{V_C} \rho \left( u + \frac{V^2}{2} + g_z \right) dV + \int_{A_{IN+A_{OUT}}} \rho \left( u + \frac{V^2}{2} + g_z \right) \vec{v} \cdot \vec{n} dA =$$

$\frac{d\phi}{dt} = \frac{d\phi_{CV}}{dt} + \int_{\partial V_C} \vec{v} \cdot \vec{n} dA$

(⇒ Flux of material that enters/exits the CV)

$$= \dot{L} + \int_{A_{IN+A_{OUT}}} -\rho(V P) \vec{v} \cdot \vec{n} dA + \dot{Q}$$

multiply and divided by density and  $\frac{1}{\rho} = v$ , does so too keep the same form.

$$\Rightarrow \frac{d}{dt} \int_{V_C} \rho \left( u + \frac{V^2}{2} + g_z \right) dV + \int_{A_{IN+A_{OUT}}} \rho \left( u + P_v + \frac{V^2}{2} + g_z \right) \vec{v} \cdot \vec{n} dA = \dot{L} + \dot{Q}$$

$h \rightarrow$  enthalpy

By calculating the enthalpy we don't need to calculate  $u$ ,  $P$  or  $v$ .

$h$  is the sum of the flux of energy ( $u$ ) and the flux of mechanical power  $P_v$ .

In full: Power balance for control volume

$$\frac{d}{dt} \int_{V_C} \rho \left( u + \frac{V^2}{2} + g_z \right) dV + \int_{A_{OUT}} \rho \left( h + \frac{V^2}{2} + g_z \right) v_{u,out} dA$$

This is not the

$$-\int_{A_{IN}} \rho \left( h + \frac{V^2}{2} + g z \right) v_{m, in} dA = \dot{L} + \dot{Q}$$

from the general form by

flux of the first  
since we use  $h$   
not  $u$ , and  
 $h$  considers the  
pulse power term.

We want to simplify it using the assumptions.

$$\frac{d}{dt} \int_{V_F} \rho \left( h + \frac{V^2}{2} + g z \right) dV + \int_{A_{OUT}} \rho \left( h + \frac{V^2}{2} + g z \right) v_{m, OUT} dA$$

$\rightarrow 0, \text{ steady flow}$

$$-\int_{A_{IN}} \rho \left( h + \frac{V^2}{2} + g z \right) v_{m, in} dA = \dot{L} + \dot{Q}$$

we no longer care  
about what's happening  
inside, we infer it from  
what happens at the  
two ends.

If we apply the lumped parameter approach:

$$\Rightarrow \underbrace{\left( h + \frac{V^2}{2} + g z \right)_{OUT}}_{\text{Average value}} \cdot \int_{A_{OUT}} \rho v_{m, OUT} dA - \underbrace{\left( h + \frac{V^2}{2} + g z \right)_{IN}}_{\dot{m}_{IN}} \cdot \dot{m}_{IN} = \dot{L} + \dot{Q}$$

$\underbrace{\dot{m}_{OUT}}_{\text{mass flow}}$

Due to the assumptions the mass balance is also valid

$$\begin{cases} \dot{m}_{IN} = \dot{m}_{OUT} = \dot{m} \\ \left( h + \frac{V^2}{2} + g z \right) \cancel{\dot{m}} - \left( h + \frac{V^2}{2} + g z \right) \cancel{\dot{m}} = \frac{\dot{L} + \dot{Q}}{\dot{m}} = \ell + q \end{cases}$$

The assumptions are not strong enough to cause issues in the balances.

$$\ell + q = h_{OUT} - h_{IN} + \frac{V_{OUT}^2 - V_{IN}^2}{2} + g(z_{OUT} - z_{IN})$$

→ Energy  
Balance

While this equation is useful since it includes everything,  
sometimes we would just the mechanical terms or just the heat terms,  
this is since it allows us to find the efficiency, writing equations

based on mechanical or heat terms unless the wasted products count.

$$\text{Clausius: } q = \int_{IN}^{OUT} T ds - \cancel{h_w}$$

Since  $\cancel{h_w} = T \Delta S_{IRR}$

$$h_{OUT} - h_{IN} = \int_{IN}^{OUT} T ds + \int_{IN}^{OUT} v dP$$

16:19 → Why surprising

$$\ell + \int_{IN}^{OUT} T ds - \cancel{h_w} = \int_{IN}^{OUT} T ds + \int_{IN}^{OUT} v dP + \frac{\Delta V^2}{2} + g \Delta z$$

$$\ell - \cancel{h_w} = \int_{IN}^{OUT} v dP + \frac{\Delta V^2}{2} + g \Delta z$$

no Mechanical Energy Balance

→ It shows that mechanical energy is not conserved there is a sink which is the  $\cancel{h_w}$ , this is because we are only considering mechanical energy and don't look at the thermal energy.

$$q + \cancel{h_w} = \int_{IN}^{OUT} T ds$$

→ Thermal Energy Balance

PUMP



Compressor



$$\ell > 0$$

$$\cancel{h_w} > 0$$

$$\ell > \ell - \cancel{h_w} = \\ = \ell > \int v dP + \frac{\Delta V^2}{2} + g \Delta z$$

↳ What is paid will always be greater than what we effectively transfer to the fluid.

Turbine  $\textcircled{T}$   $\ell < 0$   $\ell - \ell_w = -|\ell| - \ell_w \rightarrow$  Trick to make the sign appear  
 Thermal Turbine  $\boxed{\textcircled{T}}$   $\ell_w > 0$   $-|\ell| - \ell_w = - \left| \int_{\text{IN}}^{\text{OUT}} v dP + \frac{\Delta v^2}{2} + g \Delta z \right|$   
 shows that mechanical energy reduces.

$$\Rightarrow |\ell| = \left| \int_{\text{IN}}^{\text{OUT}} v dP + \frac{\Delta v^2}{2} + g \Delta z \right| - \ell_w$$

Turbine efficiency is how much of the mechanical energy of the fluid which we have that we can extract

$g \Delta z$  is typically very small, the change in velocity can also be small.

$$\ell - \ell_w = \int_{\text{IN}}^{\text{OUT}} v dP \xrightarrow{\substack{\text{Ideal} \\ \text{liquid}}} \ell - \ell_w = \frac{\Delta P}{\rho} + \frac{\Delta v^2}{2} + g \Delta z =$$

Normally this term dominates.

Technical work

$$= \Delta \left( \frac{\rho}{\rho} + \frac{v^2}{2} + g z \right) = \Delta T$$

$\textcircled{T}$   $\rightarrow$  Bernoulli  
Theorem

$$= \int_{\text{IN}}^{\text{OUT}} v dP \xrightarrow{\substack{\text{IDEAL} \\ \text{GAS}}} \int_{\text{IN}}^{\text{OUT}} R T \frac{dP}{P} \rightarrow$$

we cannot say anything about the relationship between  $T$  and  $P$ , it depends on the transformation,

in ideal liquid we didn't have such an issue since we can only have isentropic transformations.

$\Rightarrow$  we have to define the transformations to calculate the change in energy.

Not all thermodynamic cycles can be realized (e.g. isothermal), that's why many transformations are not used.

Compressors have fans that spin fast this heat the fluid, so if we wanted an isothermal compressors, we can cool the fluid down and have something that is kind of like that transformation.