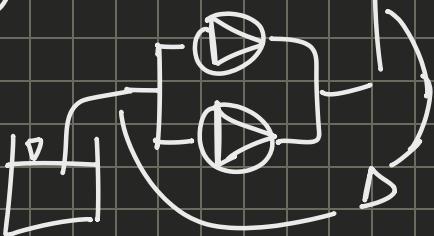


desireuse 1S - (Training)

Exercise 6

a) D_2



$$n = 1500$$

Pump in series \Rightarrow same flow rate
 \hookrightarrow sum head

$$\Delta z = 4 \text{ m}$$

$$\left\{ \begin{array}{l} H_p = -100Q^2 - 20Q + 12.5 \\ \eta_p = -0.2Q^2 - Q + 1 \end{array} \right.$$

$$D = 0.4 \text{ m}$$

$$\dot{Q} = ?$$

$$H = ?$$

$$L = ?$$

CIRCUIT

$$H = \Delta z + \frac{\Delta p}{\rho g} + 3Q^2$$

$$y = 25 \frac{V^2}{2} = 25 \left(\frac{Q}{\pi D^2 / h} \right)^2 = \frac{1}{2} \frac{25,41}{2\pi D^2} Q^2$$

$$H_c = 80,77 Q^2 + 4$$

Pumps

$$Q = Q_{p1} + Q_{p2} = 2Q_p$$

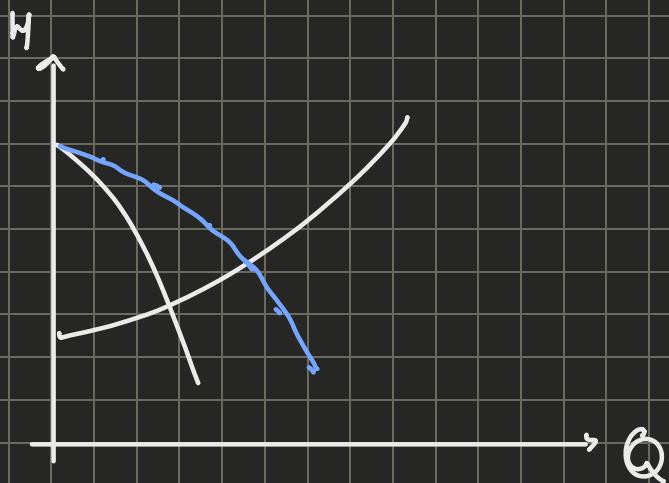
$$H = H_1 = H_2$$

The pressure after both pumps has to be the same since there will be a backflow going into one branch if the pressure is not identical therefore

$Q_{p1} = Q_{p2} = Q_p$, since pumps are identical the $Q_p = \frac{1}{2}Q$. and the pumps

$$\Rightarrow H_{p_1} = H_{p_2} = 100 \left(\frac{Q}{\alpha} \right)^2 - 70 \left(\frac{Q}{\alpha} \right) + 12,5$$

$$\begin{cases} H = -25 Q^2 - 10Q + 12,5 \\ H_c = 80,77 Q^2 + 4 \\ \Rightarrow \begin{cases} Q = 0,24 \frac{m^3}{s} \rightarrow Q_{p_1} = Q_{p_2} = 0,12 \frac{m^3}{s} \\ H = 8,66 \text{ m} = H_{p_1} = H_{p_2} \end{cases} \end{cases}$$



$\text{---} = \text{system of two parallel pumps}$

Systems of pumps will allow us to increase the flow rate without buying a specialised heavy flow machine.

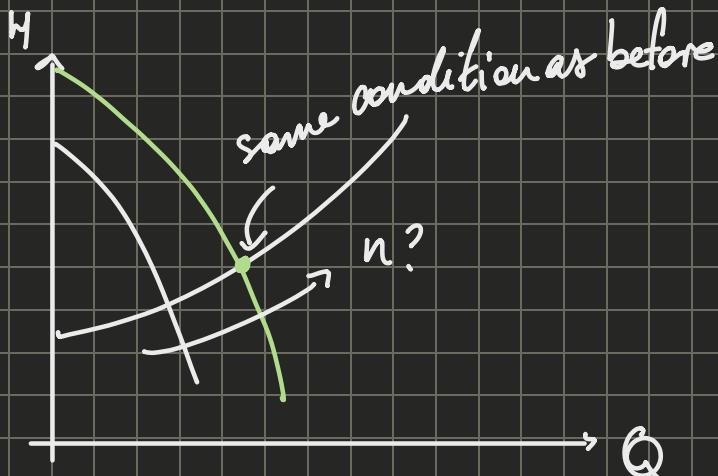
$$\dot{L} = \dot{L}_{p_1} + \dot{L}_{p_2}$$

$$= \rho Q_{p_1} \frac{g H_{p_1}}{\eta_{p_1}} + \rho Q_{p_2} \frac{g H_{p_2}}{\eta_{p_2}} = 23,3 \text{ kW}$$

$$\eta_{p_1} = -0,2(0,12)^2 - 0,12 + 1 = 0,88 = \eta_{p_2}$$

If we break but we want to maintain the same operating condition, how much will the n be to operate

at this condition?



We cannot search for it through similarity, but we can use the similarity concept to find it.

$$H = -100 Q^2 - 20Q + 12,5$$

$$\eta = 0,2 Q^2 - Q + 1$$

$$H(n) = -100 Q^2 - \frac{n}{1500} \cdot 20 Q + \left(\frac{n}{1500}\right)^2 \cdot 12,5$$

$$H_c = 80,77 Q^2 + 4$$

$$\Rightarrow H(n) - H_c \Rightarrow -100 Q^2 - 20 \frac{n}{1500} Q + \left(\frac{n}{1500}\right)^2 12,5 = \\ = 80,77 Q^2 + 4$$

$$Q \text{ is the same as before} \rightarrow Q = 0,24 \frac{m^3}{s}$$

$$\Rightarrow n = 1925 \text{ rpm}$$

$$\eta(n) = -0,2 \left(\frac{1500}{n}\right)^2 Q^2 - \left(\frac{1500}{n}\right) Q + 1$$

The efficiency can only close or open with n

$$\eta(1925) = 0,806$$

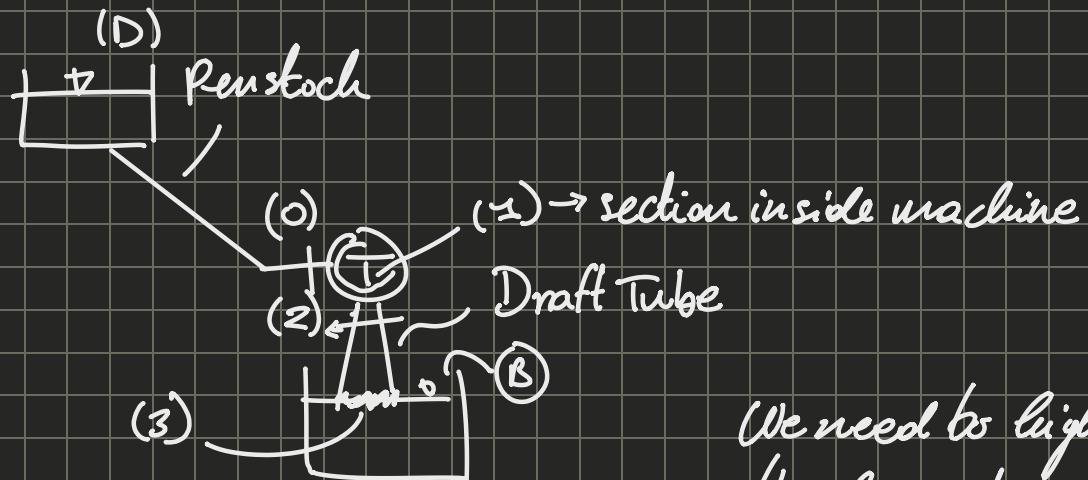
$$L = \rho Q g \frac{H}{\eta} = 25,3 \text{ kW}$$

Q, M are the same since
the operation condition is the
same, but γ is lower since
we only have one pump, so L
has to be higher

Start of Theory

Hydraulic Turbines

Hydro-Electricity Systems



BME ($D \rightarrow B$) Penstock

We need to highlight
the losses at 3 since not
accounting for them will can
reduce of the efficiency by 10%.

$$+ |l| + l_w + y_p + y_{DT} = (\bar{T}_B - \bar{T}_D) = -g(z_B - z_D)$$

since $|l|$ \rightarrow Draft Tube

$$|l| = g(z_D - z_B) - y_p - y_{DT} - l_w$$

(*) $g H_m = T_0 - T_2$

\downarrow
motorhead

Draft Tube

$$\text{BME } 0 \rightarrow B \quad l - l_w - y_{DT} = \bar{T}_B - \bar{T}_0$$

Technically $P_{ATM,B} \neq P_{ATM,D}$,
but we are not making
money from this so we
consider them to be
equal.

$$\Rightarrow -|\ell| - \ell_w - y_{DT} = T_B - T_0$$

$$|\ell| + \ell_w = T_0 - T_B - y_{DT}$$

BME 0 → 2

$$\ell - \ell_w = T_2 - T_0 \Rightarrow T_0 - T_2 = g H_m = |\ell| + \ell_w$$

Ranshach losses

For a turbine:

$$\eta_T = \frac{|\ell|}{g H_m} = \frac{|\ell|}{|\ell| + \ell_w} = \frac{g(z_0 - z_B) - y_p - y_{DT} - \ell_w}{g(z_D - z_B) - y_p - y_{DT}}$$

$$= 1 - \frac{\ell_w}{g H_m}$$

The manufacturer gives us the machine and the draft tube, the draft tube is a part of the machine, but also considering the draft tube losses is not very useful so we use another explanation.

$$(※※) g H_m = T_0 - T_B + T_D - T_0 = (T_D - T_B) - (T_0 - T_D)$$

$$= g(z_D - z_B) - \underbrace{(T_0 - T_D)}_{y_p}$$

$$= g(z_D - z_B) - y_p$$

Definition of efficiency

$$\eta = \frac{|f|}{g H_m} = \frac{g(z_0 - z_3) - y_p - \ell_w - y_{DT}}{g(z_0 - z_B) - y_p} = 1 - \frac{\ell_w}{g H_m} - \frac{y_{DT}}{g H_m}$$

By playing with the definition of H_m , we managed to include y_{DT} in the definition of the efficiency, which is useful since the manufacturer will also sell us the draft tube.

$$y_{DT} = y_{m_D} + y_{m_C} = \xi \frac{V_3^2}{2} + \frac{V_3^2}{2} = (\xi_{DT} + 1) \frac{V_3^2}{2}$$

↳ Concentric
Com coefficient
at exit

$$= 1 - \frac{\ell_w}{g H_m} - \xi_{DT} \frac{V_3^2}{2 g H_m} - \frac{V_3^2}{2 g H_m}$$

The draft tube will be a divergent since we want to reduce V_3 as much as possible to reduce the losses.

Advantage of increasing cross section

Mass Balance

2 → 3

$$\frac{\frac{V_2}{4} \pi D_2^2}{\frac{V_3}{4} \pi D_3^2} = \frac{V_2 \pi D_2^2}{V_3 \pi D_3^2} \Rightarrow V_3^2 = V_2^2 \left(\frac{D_2}{D_3} \right)^4$$

↳ $V_2 = V_{2m} \rightarrow$ machine with draft tube
we try to make sure V_2 is purely
meridional, so we don't have
swirls which have low pressure

in the middle, possibly causing cavitation.

The fact that the draft tube releases in a basin at P_{ATM} , and the fact that the P increases along the tube, it imposes P_z to be lower than P_{ATM} .