

Esercitazione 3 - Hydraulic Similarity + Cavitation

Exercise 5

Centrifugal Pump,
design

$$n_d = 1400 \text{ rpm}$$

$$Q_d = 0,153 \frac{\text{m}^3}{\text{s}}$$

$$D_d = 300 \text{ mm}$$

$$H_d = 39 \text{ m}$$

$$W_d = 68 \text{ kW}$$

$$\eta_d = \eta_{\max} \rightarrow \text{BEP}$$

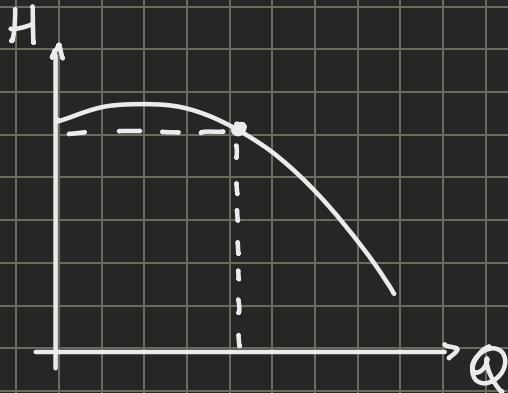
We need to keep η the same, so we need to maintain similarity.

a) $n_a = 1200 \text{ rpm}$

$$D_a = D_d$$

$$Q_a = ?$$

$$H_a = ?$$



$$gH = \underbrace{\ell - \ell_w}_{\propto U^2} \rightarrow f(D, n)$$

To non-dimensionalize, we divide by $n^2 D^2$

$$\underbrace{\frac{gH}{n^2 D^2}}_{\psi} = \underbrace{\frac{\ell}{n^2 D^2}}_{\lambda} - \underbrace{\frac{\ell_w}{n^2 D^2}}_{\zeta} \rightarrow \psi = \psi(\varphi, Re, \text{SHAPE})$$

dynamic problem

Head
Coefficient

Work
Coefficient

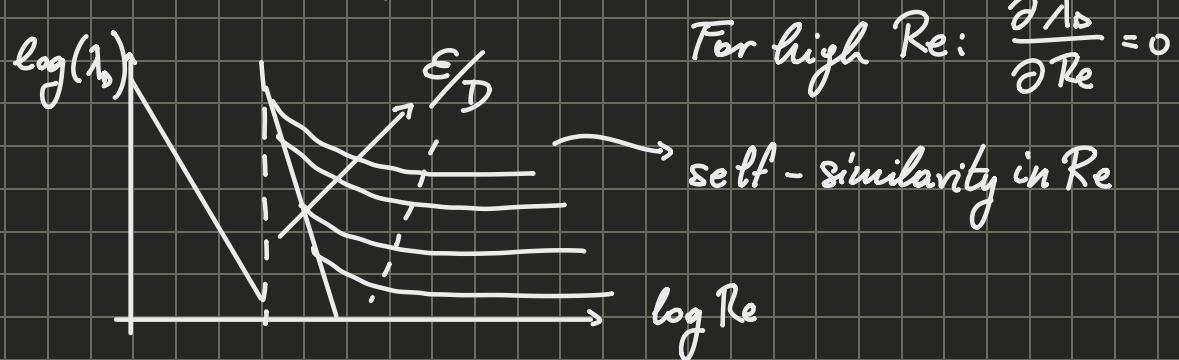
Flow Coefficient

$$\lambda = \lambda \left(\varphi, \frac{D_2}{b_1}, \frac{D_2}{b_2}, \alpha_1, \beta_2 \right) = \lambda \left(\varphi, \text{SHAPE} \right)$$

$\frac{Q}{n D^3}$ Shape parameters

ξ is like $\gamma_{\text{loss, friction}} = \xi_D \frac{V^2}{2}$ ↳ includes Variation and other factors.

$$\xi_D = \xi_D(R_e, \text{SHAPE}) = \lambda_D(R_e, \frac{\epsilon}{D}) \cdot \frac{L}{D}$$



* With high R_e , we have self-similarity of R_e :

$$\Rightarrow \psi = \psi(\varphi, \text{SHAPE}) \rightarrow \text{kinematic problem.}$$

From where we can get efficiency:

$$\eta = \eta(\varphi, \text{SHAPE})$$

$$\eta = \frac{g H}{\ell} \rightarrow \eta = \frac{\psi}{\lambda} = \frac{\psi(\varphi, \text{SHAPE})}{\lambda(\varphi, \text{SHAPE})}$$

Fixing φ , ψ will be the same

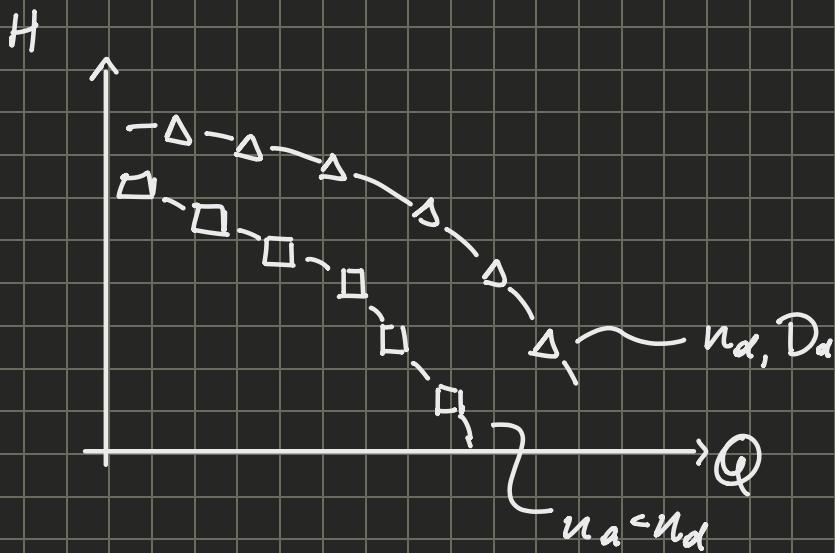
Return to exercise:

$$\begin{aligned} \varphi_0 &= \varphi_a \\ \downarrow & \\ \frac{Q_d}{n_d D_d^3} &= \frac{Q_a}{n_a D_a^3} \rightarrow Q_a = \frac{n_a}{n_d} Q_d = 0,127 \frac{m^3}{s} \end{aligned}$$

We respect the similarity by fixing the φ and SHAPE

$$\rightarrow \psi_a = \psi_a \rightarrow \frac{g H_a}{n_a^2 D_a^2} = \frac{g H_d}{n_d^2 D_d^2} \rightarrow H_a = \left(\frac{n_a}{n_d} \right)^2 H_d = 26,7 \text{ m}$$

$\eta_a = \eta_d = \eta_{\min}$ → Since we want to keep similarity.



$$b) n_b = n_a$$

$$D_b = 200 \text{ mm} (< D_a)$$

Q_b and H_b ? such the $\eta = \text{const} \Rightarrow$ similarity

$$\varphi_b = \varphi_a$$

$$\frac{Q_b}{\eta_b D_b^3} = \frac{Q_a}{\eta_a D_a^3} \rightarrow Q_b = \left(\frac{D_b}{D_a} \right)^3 Q_a = 1,453 \frac{\text{m}^3}{\text{s}}$$

$$\Psi_b = \Psi_a \rightarrow \frac{g H_b}{\eta_b D_b^2} = \frac{g H_a}{\eta_a D_a^2} \rightarrow H_b = \left(\frac{D_b}{D_a} \right)^2 H_a = 17,5 \text{ m}$$

When we adhere to a similarity condition, we are able to calculate everything

Exercise 3

Hydraulic Turbine

$$H_d = 1200 \text{ m} \quad \xrightarrow{\text{chosen from Balje chart}}$$

$$Q_d = 4 \frac{\text{m}^3}{\text{s}} \quad \xrightarrow{\text{Pelton Turbine}} \quad (\text{is most efficient turbine})$$

$$\omega_s = 0,093 \rightarrow \text{specific speed} \rightarrow \eta = 0,88$$

$$D_s = 16 \rightarrow " \text{ diameter}$$

$$Q_L = ?$$

$$H_L = 200 \text{ m}$$

$$W_L = 15 \text{ hLW}$$

$$\omega_L, \omega_d = ?$$

$$D_L, D_d = ?$$

\hookrightarrow D_L \rightarrow real

$$\left. \begin{aligned} \varphi &= \frac{Q}{nD^3} \\ \psi &= \frac{gH}{n^2 D^2} \end{aligned} \right\}$$

don't use ω_s or D_s ,
so we need more
different dimensionless
parameters.



\rightarrow no correlation, since dependant
on shape and size!

Machines at their BEP

$$\psi = \frac{gH}{n^2 D^2} \rightarrow D = \frac{(gH)^{1/2}}{n \sqrt{\psi}} \rightarrow n = \dots$$

$$\varphi = \frac{Q}{nD^3} \rightarrow \varphi = \frac{Q n^{3/2} \psi^{3/2}}{n (gH)^{3/4}}$$

$$\sqrt{\frac{\varphi}{\psi^{3/2}}} = \frac{\sqrt{Qn}}{(gH)^{3/4}} = n_s$$

if n rather than n_s , it would be ω_s

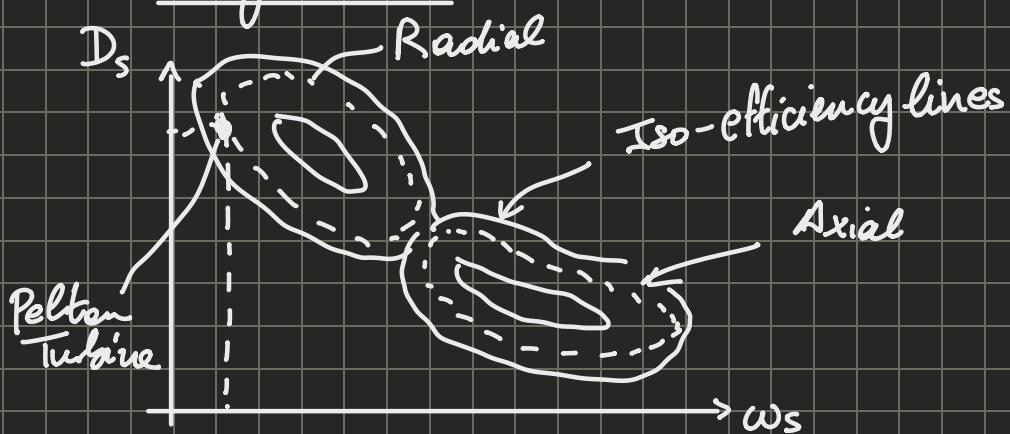
$$D_s = \frac{D \sqrt{gH}}{\sqrt{Q}}$$

\rightarrow we are able to isolate the
effect of shape



We have form the definition of D_s and ω_s

Baile Chart



$$\omega_a = \frac{\omega_s (g H_d)^{3/4}}{\sqrt{Q_d}} = 52,5 \frac{\text{rad}}{\text{s}} = 500 \text{ rpm}$$

$$D_a = \frac{D_s \sqrt{Q_d}}{(g H_d)^{3/4}} = 3,1 \text{ m}$$

$$Q_L = \frac{\omega_L}{\rho g H_L \eta} = 0,0087 \frac{\text{m}^3}{\text{s}}$$

$$W_L = \rho Q_L \cdot l = \rho Q_L \eta g H_L$$

$\eta = \frac{l}{g H_L}$ ↗ inverse of the pump, since l in turbine is the useful output.

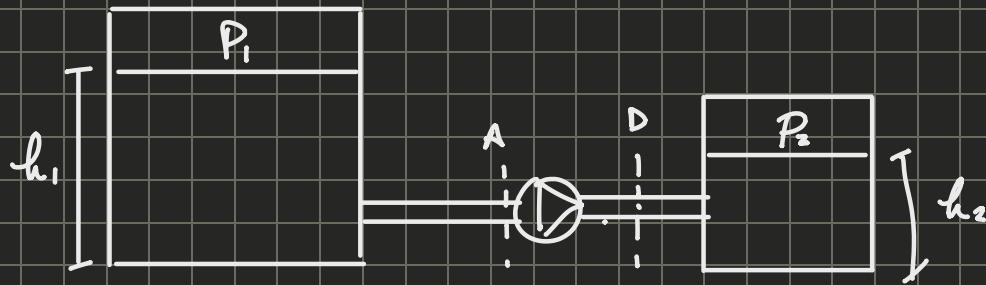
$$l = (g H_L) \eta$$

$$\Rightarrow \omega_L = \frac{\omega_s (g H_L)^{3/4}}{\sqrt{Q_L}} = 293,7 \frac{\text{rad}}{\text{s}} = 2800 \text{ rpm}$$

$$D_L = \frac{D_s \sqrt{Q_L}}{(g H_L)^{3/4}} = 0,224 \text{ m}$$

Cavitation

Exercise 2



$$P_1 = 0,3 \text{ bar}$$

$$P_2 = 2,3 \text{ bar}$$

$$z_1 = 10 \text{ m}$$

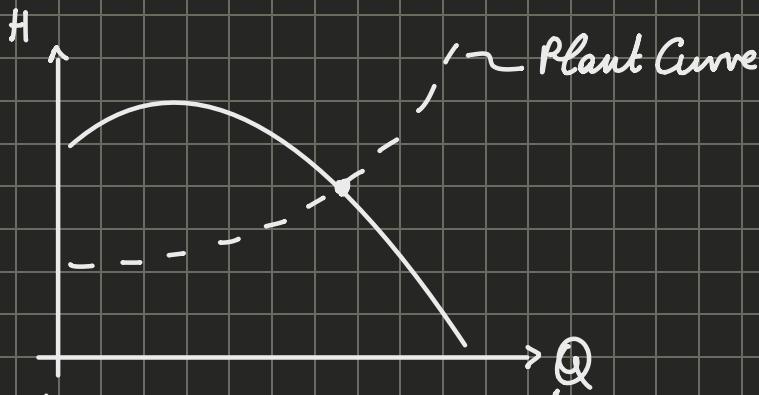
$$z_2 = 5 \text{ m}$$

$$D_1 = 350 \text{ mm}$$

$$D_2 = 350 \text{ mm}$$

$$\xi_{ASP} = 5$$

$$\xi_{total} = 15$$



a) $H = ?$ $Q = ?$ Operating Point \rightarrow intersection of two curves.

BME ($1 \rightarrow 2$)

$$g H_c - Y_{asp} - Y_{aer} = \frac{P_2 - P_1}{\rho} - \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1)$$

$\cancel{\frac{V^2}{2}}$

$\underbrace{g H_c}_{= l - l_w}$

$$Y_{asp} = \xi_{asp} \frac{V_{asp}^2}{2}$$

$$Y_{aer} = \xi_{aer} \frac{V_{aer}^2}{2}$$

$$Q_{del} = Q_{asp}$$

$$V_{del} \frac{\pi D_{del}^2}{4} = V_{asp} \frac{\pi D_1^2}{4} \rightarrow \underbrace{V_{del}}_{\text{same pipe}} = V_{asp} = V$$

$$H_c = \frac{P_2 - P_1}{\rho g} + (z_2 - z_1) + (\xi_{asp} + \xi_{add}) \frac{V^2}{2g}$$

$$\begin{aligned} Q &= \frac{\pi D^2}{4} V \rightarrow V = \frac{4Q}{\pi D^2} \\ &= \frac{P_2 - P_1}{\rho g} + (z_2 - z_1) + (\xi_{asp} + \xi_{add}) \frac{8Q^2}{\pi^2 D^4 g} \end{aligned}$$

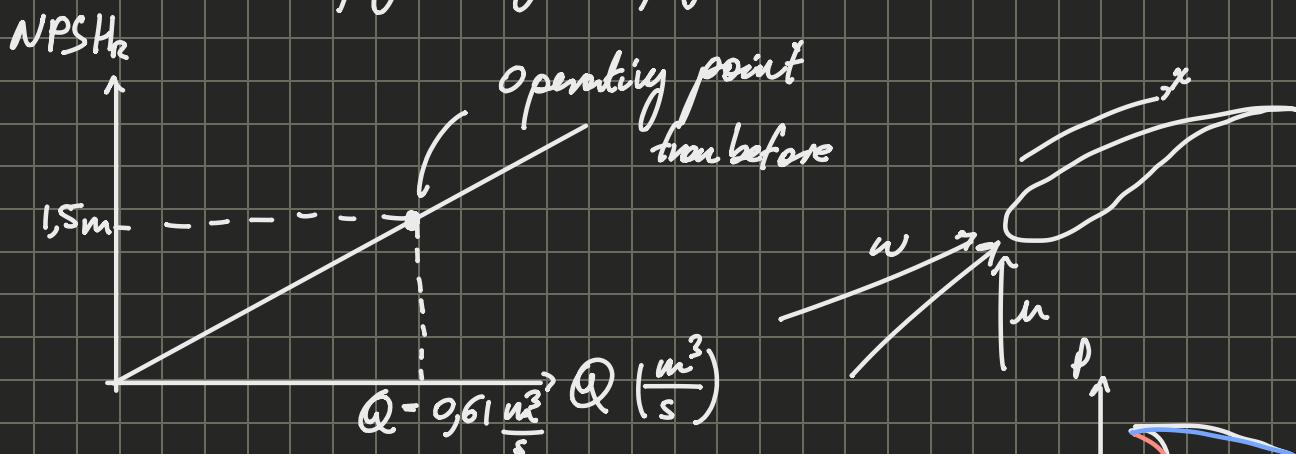
We now have $H_c = H_c(Q) \rightarrow$ plant resistance curve.

$$H_c = 17,68 + 110,24 Q^2$$

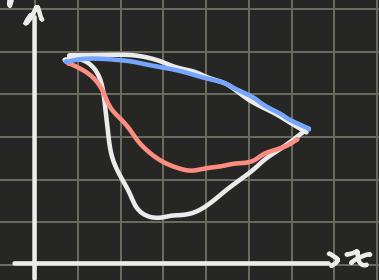
We are able to then find the intersection point with the pump curve, where $H = 58 \text{ m}$, $Q = 0,61 \frac{\text{m}^3}{\text{s}}$.

b) Maximum height of installation, to avoid cavitation

$$NPSH_R = \frac{P_{in}}{\rho g} + \frac{V_{in}^2}{2g} - \frac{P_{min}}{\rho g}$$



A change in Q , changes w , which deviates the flow from the optimum, changing P .



We need to find z_A such that $NPSH_A > NPSH_R$

$$NPSH_A = \frac{P_A}{\rho g} + \frac{V_A^2}{2g} - \frac{P_{sat}}{\rho g}$$

Available
Inlet

$\frac{P_{sat}}{\rho g} = 1,5 \text{ m} \rightarrow$ Be careful, sometimes they give P_{sat} in meters, which already takes into account ρg .

$$BME (1 \rightarrow A) \rightarrow - \frac{Y_{asp}}{g} = \left(\frac{P_A}{\rho g} + \frac{V_A^2}{2g} + z_A \right) - \left(\frac{P_1}{\rho g} + \frac{V_1^2}{2g} + z_1 \right)$$

$$Y_{asp} = \sum_{asp} \frac{V_{asp}^2}{2} = \sum_{asp} \frac{8Q}{\pi^2 D_{asp}^4}$$

$$NPSH_A = \frac{P_1}{\rho g} + (z_1 - z_A) - \sum_{asp} \frac{8Q^2}{\pi^2 D_g^4 g} - \frac{P_{sat}}{\rho g}$$

$NPSH_A > NPSH_R \rightarrow$ find z_A such that this is true

$$\Rightarrow z_A < \frac{P_1}{\rho g} + z_1 - \sum_{asp} \frac{8Q^2}{\pi^2 D_g^4 g} - \frac{P_{sat}}{\rho g} - NPSH_R$$

$$z_A < 0,15 \text{ m}$$