

Tutorial 3

Q1. $\eta = 1 - \frac{T_L}{T_H}$

$$\eta = 1 - \frac{303}{973} = 0.6886 //$$

Q2. $\frac{Q_L}{Q_H} = \frac{T_L}{T_H}$

$$\frac{200}{300} = \frac{303}{T} \\ T = 454.5 \text{ K} //$$

Q3.

$$\text{COP}_{\text{REF}} = \frac{1}{\frac{Q_H}{Q_L} - 1}$$

$$\dot{Q}_H = 3 \times \frac{1800}{3600} = 1.5 \text{ kW}$$

$$\dot{Q}_L = 3 \times \frac{1800}{3600} = 1.5 \text{ kW}$$

$$\dot{Q}_L = \dot{Q}_H - \dot{W}_{\text{in}}$$

$$\dot{Q}_L = 1.0 \text{ kW}$$

$$\text{COP}_{\text{REF}} = \frac{1}{\frac{1.5}{1.0} - 1}$$

$$\text{COP}_{\text{REF}} = \frac{\dot{Q}_L}{\dot{W}_{\text{in}}} = \frac{1.0}{0.5}$$

$$\text{COP}_{\text{REF}} = 2 //$$

Q4. Let the time taken be t , seconds.

$$\therefore \dot{Q}_L = \frac{m c \Delta \theta}{t} = \left(\frac{840}{t} \right) \text{ kW}$$

$$\text{COP}_{\text{REF}} = \frac{\dot{Q}_L}{\dot{W}_{\text{in}}}$$

$$2.5 = \frac{(840) \times 1000}{t}$$

$$t = \frac{840000}{2.5} = 336000 \text{ s}$$

$$t = 840 \text{ s} //$$

Q5. $W_{out} = \frac{55 \times 10^3}{3600} \times 27 \times \frac{20}{100}$
 $82.5 \text{ MW} //$

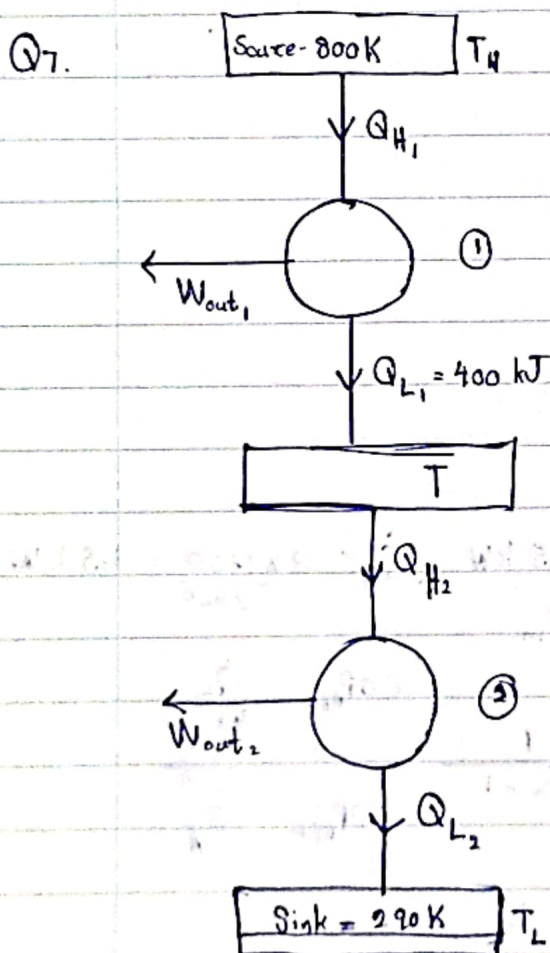
Q6. $COP_{REF, rev} = \frac{1}{\frac{T_H}{T_L} - 1}$
 $= \frac{1}{\frac{303}{253} - 1} = 5.06$

$\therefore COP_{REF} = 5.06 \times \frac{1}{4}$
 $= 1.265$

$COP_{REF} = \frac{Q_L}{W_{in}}$

$1.265 = \frac{30 \times 10^3 \times 211}{60 W_{in}}$

$W_{in} = 83.4 \text{ MW} //$



(i) $\eta_1 = 1 - \frac{Q_L}{Q_H} = 1 - \frac{T}{800}$

$\eta_2 = 1 - \frac{290}{T}$

$\eta_1 = \eta_2$

$1 - \frac{T}{800} = 1 - \frac{290}{T}$

$T = 481.66 \text{ K} //$

(ii) $\frac{Q_H}{Q_L} = \frac{481.66}{800}$

$Q_{H1} = 664.37 \text{ kJ} //$

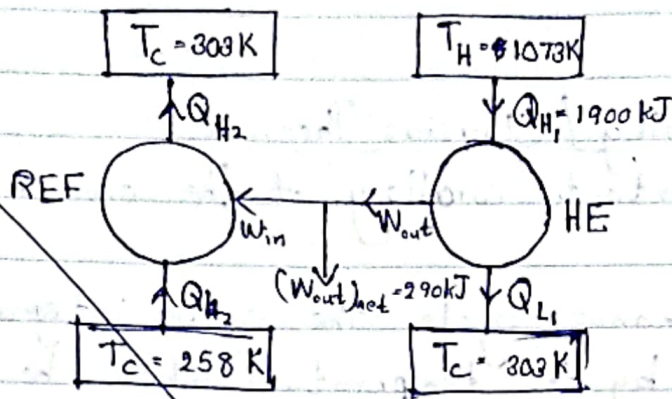
(iii) $W_{out1} = Q_{H1} - Q_{L1} = 264.37 \text{ kJ} //$

$\eta_1 = \eta_2 = 0.398$

$W_{out2} = \eta_2 Q_{H2}$

$W_{out2} = 159.166 \text{ kJ} //$

Q8.



$$\frac{Q_{H1}}{Q_{L1}} = \frac{T_H}{T_L}$$

$$\frac{1900}{Q_{L1}} = \frac{1073}{303}$$

$$Q_{L1} = 536.533 \text{ kJ}$$

$$W_{out} = 1363.467 \text{ kJ}$$

$$W_{in} = 1073.467 \text{ kJ}$$

$$Q_{H2} = W_{in} + Q_{L2} \quad \text{--- (1)}$$

$$\frac{Q_{H2}}{Q_{L2}} = \frac{303}{258} \quad \text{--- (2)}$$

from (1), (2)

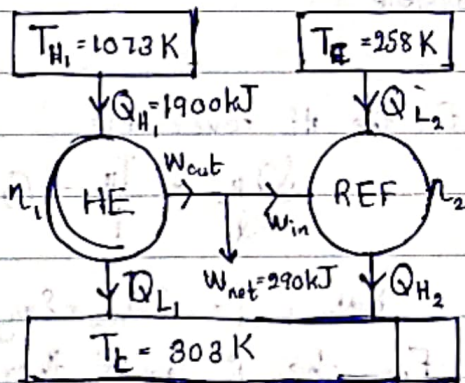
$$\frac{303}{258} Q_{L2} = 1073.467 + Q_{L2}$$

$$Q_{L2} = 6154.544 \text{ kJ}$$

$$Q_{H2} = 7228.011 \text{ kJ}$$

P2

Q8.



$$Q_{L1} = 536.533 \text{ kJ}$$

$$\eta_{HE} = \eta_{REF} \quad \text{--- (1)}$$

$$\eta_{HE} = \eta_{REF}$$

$$\eta_{HE} = 1 - \frac{303}{1073} = 0.7176$$

$$W_{out} = \eta_{HE} Q_{H1}$$

$$W_{out} = 1363.467 \text{ kJ}$$

$$W_{in} = W_{out} - W_{net}$$

$$W_{in} = 1073.467 \text{ kJ}$$

$$(COP)_{REF} = \frac{1}{\frac{303}{258} - 1} = 5.7333$$

Heat transfer to the refrigerant, Q_{L2}

$$Q_{L2} = 6154.544 \text{ kJ}$$

Total heat transfer to 30°C thermal reservoir, $Q_{H2} = W_{in} + Q_{L2} = 7228.011 \text{ kJ}$

$$Q_{total} = Q_{L1} + Q_{L2} = 7764.544 \text{ kJ}$$