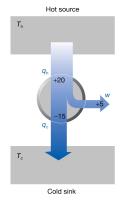
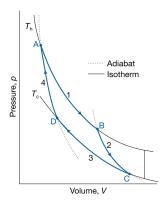
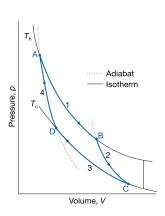
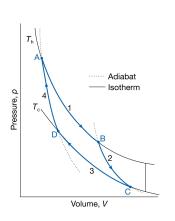
Example of a Carnot engine



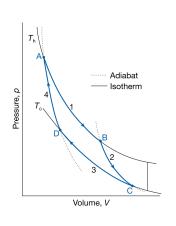


 $q_h = nRT_h \ln rac{V_B}{V_A}; \quad q_c = nRT_c \ln rac{V_D}{V_C}$





 $q_h = nRT_h \ln \frac{V_B}{V_A};$ $q_c = nRT_c \ln \frac{V_D}{V_C}$ adiabats: $V_A T_h^c = V_D T_c^c$ (exponent $c = \frac{C_V}{nR}$) and $V_C T_c^c = V_B T_h^c$

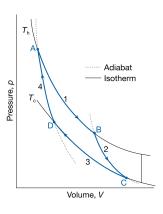


$$\begin{split} q_h &= nRT_h \ln \frac{V_B}{V_A}; \quad q_c = nRT_c \ln \frac{V_D}{V_C} \\ \text{adiabats: } V_A T_h^c &= V_D T_c^c \text{ (exponent } c = \frac{C_V}{nR} \text{)} \\ \text{and} \qquad V_C T_c^c &= V_B T_h^c \\ \text{obtain: } V_A V_C T_h^c T_c^c &= V_D V_B T_h^c T_c^c \end{split}$$

and
$$\therefore \frac{V_A}{V_B} = \frac{V_D}{V_C} \Longrightarrow q_C = -nRT_C \ln \frac{V_B}{V_A}$$

 $\cdot q_b = -T_b$

$$\therefore \frac{q_h}{q_c} = -\frac{T_h}{T_c}$$



$$q_h = nRT_h \ln rac{V_B}{V_A}; \quad q_c = nRT_c \ln rac{V_D}{V_C}$$

and $V_C T_c^c = V_B T_h^c$

obtain :
$$V_A V_C T_h^c T_C^c = V_D V_B T_h^c T_c^c$$

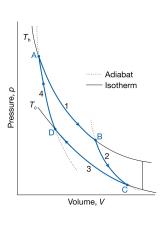
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adiabats: $V_A T_h^c = V_D T_c^c$ (exponent $c = \frac{C_V}{nR}$)

$$\therefore \frac{q_h}{q_c} = -\frac{T_h}{T_c}$$
work performed

efficiency,
$$\eta = \frac{\text{work performed}}{\text{heat absorbed}} = \frac{|w|}{q_h}$$

$$= \frac{q_h + q_c}{q_h} = 1 + \frac{q_c}{q_h} = 1 - \frac{T_c}{T_h}$$



 $q_h = nRT_h \ln rac{V_B}{V_A}; \quad q_c = nRT_c \ln rac{V_D}{V_C}$

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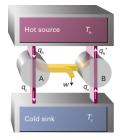
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$$\Delta S = \frac{q_h}{T_h} + 0 + \frac{q_c}{T_c} + 0 = 0$$

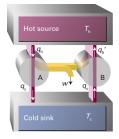


▶ Equivalent to Kelvin-Planck statement : Proof by contradiction



Let $\eta_A > \eta_B$ engine A takes heat q_h from hot source and dumps q_c in cold reservoir

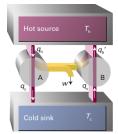
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Reverse engine B

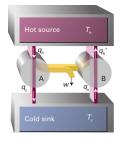
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Reverse engine B engine B acquires energy heat q_c from cold reservoir and releases $q_h' < q_h$ to the hot end

▶ Equivalent to Kelvin-Planck statement : Proof by contradiction



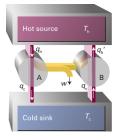
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Form composite engine C: A+B



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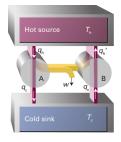
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C takes heat $q_h - q'_h$ from hot source and converts it completely into work

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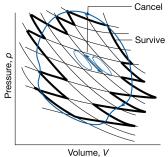


C takes heat $q_h - q_h'$ from hot source and converts it completely into work

⇒ violation of Kelvin-Planck statement of second law

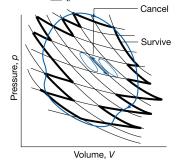
any reversible cycle \approx collection of Carnot cycles \oint (arbitrary path)

$$=\sum \oint$$
 (each cycle)



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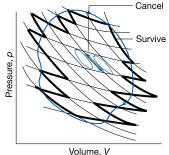
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 ΔS along an individual path inside is cancelled by ΔS along the path it shares with neighbouring cycle

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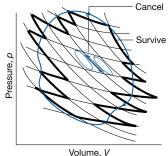


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The approxmn. becomes exact as individual cycles become infinitesimal $\phi(\text{arbitrary path}) = \sum \phi \text{ (each cycle)} = 0$

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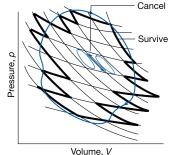
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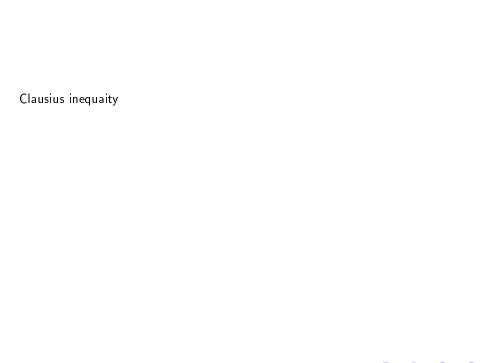
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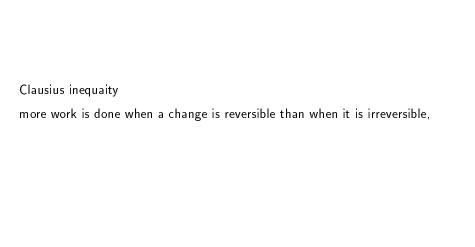
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In the limit of infinitesimal cycles, the non-cancelling edges of Camot cycles match the overall cycle exactly, and the sum becomes an integral

 \implies dS is exact differential and S is state function





Clausius	inequaity	

i.e.,, $|dw_{rev}| \ge |dw|$

more work is done when a change is reversible than when it is irreversible,

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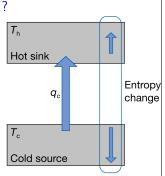
$$dU = dq + dw = dq_{\text{rev}} + dw_{\text{rev}}$$

 $dq_{\text{rev}} \ge dq, :: \Delta S = \int \frac{dq_{\text{rev}}}{T} \ge \int \frac{dq}{T}$

Consider the reverse of an engine : transfer of energy as heat from one system - hot source-at T_h to another system - the cold sink- at T_c

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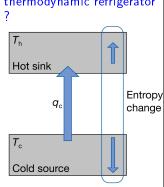
thermodynamic refrigerator



energy removed from cool source at temp. $T_c = \frac{|q_c|}{|q_c|}$

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thermodynamic refrigerator

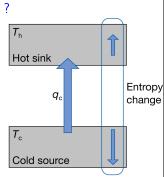


energy removed from cool source at temp. T_c

and deposited in warmer sink at temp. T_h

Consider the reverse of an engine : transfer of energy as heat from one system - hot source-at \mathcal{T}_h to another system - the cold sink- at \mathcal{T}_c

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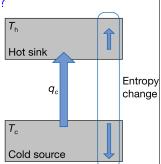
energy removed from cool source at temp. $T_c = \frac{|q_c|}{T_c}$

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$$\Delta S = -\frac{|q_e|}{T_e} + \frac{|q_e|}{T_h} < 0 \implies$$
 not spontaneous

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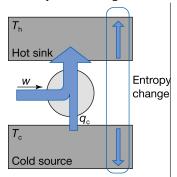


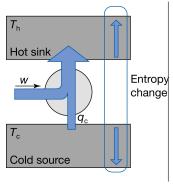
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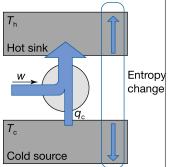
$$\Delta S = -\frac{|q_e|}{T_e} + \frac{|q_e|}{T_b} < 0 \implies$$
 not spontaneous

to generate more entropy, energy must be added to the stream that enters the warm sink. task: find minimum energy to be supplied



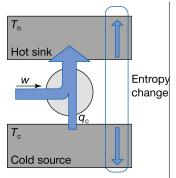


coefficient of peformance, $c = \frac{\text{energy transferred as heat}}{\text{energy transferred as work}} = \frac{|q_c|}{|w|}$

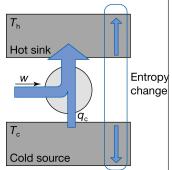


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The less the work required to achieve a given transfer, greater is \boldsymbol{c}

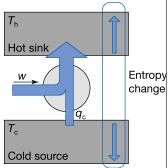


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$$\frac{1}{c} = \frac{|q_h| - |q_c|}{|q_c|} = \frac{|q_h|}{|q_c|} - 1$$

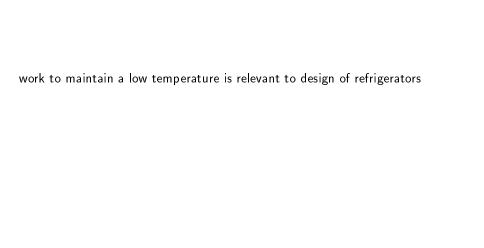
Thermodynamic refrigerator



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The less the work required to achieve a given transfer, greater is c and more efficient the refrigerator.

using $\frac{q_h}{q_c} = -\frac{T_h}{T_c}$, we get, $c = \frac{T_c}{T_h - T_c}$

 $\frac{1}{c} = \frac{|q_{h}| - |q_{c}|}{|q_{c}|} = \frac{|q_{h}|}{|q_{c}|} - 1$



work to maintain a low temperature is relevant to design of refrigerators
No thermal insulation is perfect there is always a flow of energy as heat into the sample at a rate $\propto \Delta T$

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by heating surroundings
$$P \propto rac{1}{c}.A(T_h - T_c) = rac{A(T_h - T_c)^2}{T_c}$$

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by heating surroundings $A(T_k - T_c)^2 = D \cdot (A T_c)^2$

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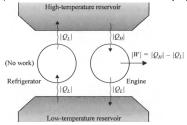
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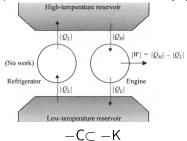
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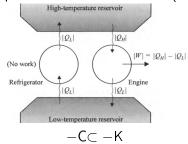
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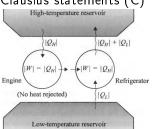
power increases as $(\Delta T)^2$

: air-conditioners more expensive to run on hot days than on mild days





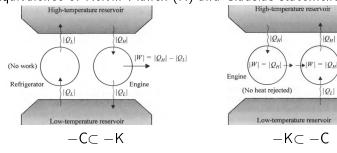


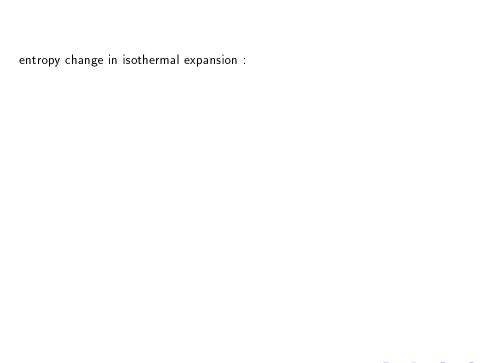


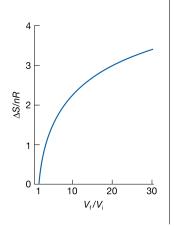
 $|Q_H| + |Q_L|$

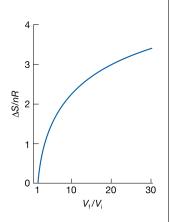
 $|Q_L|$

Refrigerator

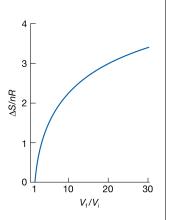




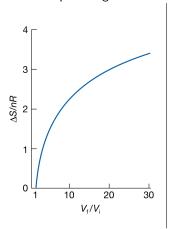




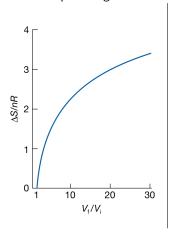
Reversible : $\Delta U = 0$;



Reversible : $\Delta U = 0$; q = -w;

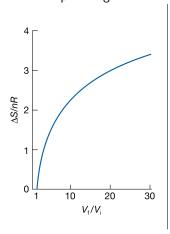


Reversible : $\Delta U = 0$; q = -w; $\Delta S_{\text{sys}} = nR \ln \frac{V_f}{V_i}$



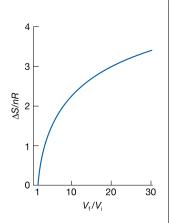
 $S_{\text{surr (rev)}} = -\Delta S_{\text{sys}}$

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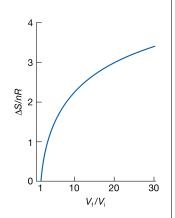


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Irreversible : $\Delta U = 0$

... If isothermal expansion occurs freely, and irreversibly, then $q = -w = p_{ex}(V_f - V_i)$



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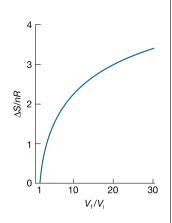
$$\Delta S_{\text{surr (rev)}} = -\Delta S_{\text{sys}}$$

Irreversible : $\Delta U = 0$

$$\therefore$$
 If isothermal expansion occurs freely, and irreversibly, then $q = -w = p_{ex}(V_f - V_i)$

$$\therefore \Delta S_{\mathsf{surr (irrev)}} = - \tfrac{p_{\mathsf{ex}}(V_f - V_i)}{T} = - \tfrac{nR(V_f - V_i)}{V_f}$$

 $\Delta S_{
m svs}$ remains the same as before (calculated using reversible path)



Reversible : $\Delta U = 0$; q = -w; $\Delta S_{sys} = nR \ln \frac{v_f}{V_i}$

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$$\therefore \Delta S_{\mathsf{surr (irrev)}} = - \tfrac{p_{\mathsf{ex}}(V_f - V_i)}{T} = - \tfrac{nR(V_f - V_i)}{V_f}$$

 $\Delta S_{
m svs}$ remains the same as before (calculated using reversible path)

$$\Delta S_{\text{total(rev)}} = 0 \text{ rev}$$

Phase transition : $\Delta_{\mathsf{trs}} \mathcal{S} = \frac{\Delta_{\mathsf{trs}} \mathcal{H}}{T_{\mathsf{trs}}}$

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wide range of liquids have approx. same $\Delta_{\text{vap}} S$ ($\approx 85 \text{ J K}^{-1} \text{ mol}^{-1}$)

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- boils at 59.2°C, $\Delta_{\rm vap}H^{\odot}=T_b\times 85\rm J~mol^{-1}$ = 332.4 \times 85 = 28kJ mol $^{-1}$

experimental value : 29.45 kJ mol⁻¹

entropy change as a function of temperature (varying heat capacity) :

$$S(T_f) = S(T_i) + \int_{T_i}^{T_f} \frac{dq_{rev}}{T}$$

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$$\mathrm{const.} \ p(\mathsf{V}) : S(T_f) = S(T_i) + \int_{T_1}^{T_f} \frac{C_{p(\mathsf{V})}dT}{T}$$

$$= S(T_i) + C_{p(\mathsf{V})} \ln \frac{T_f}{T_i}$$
 | label : heat capacity

solved problem : Calculate ΔS when 0.500 dm³ of Ar at 25°C and 1.00 bar expands to 1.000 dm³ and is simultaneously heated to 100°C

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S is a state function

... choose a convenient path from initial state

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$$\Delta S = \Delta S_{\mathsf{I}} + \Delta S_{\mathsf{II}} = nR \left(\ln \frac{V_f}{V_i} + \frac{3}{2} \ln \frac{T_f}{T_i} \right) = \frac{p_i V_i}{T_i} \ln \left(\frac{V_f}{V_i} \left[\frac{T_f}{T_i} \right]^{\frac{3}{2}} \right)$$
$$= \frac{10^5 \, \mathsf{Pa} \times 0.5 \times 10^{-3} \, \mathsf{m}^3}{298} \ln \left(\frac{1}{0.5} \left[\frac{373}{298} \right]^{\frac{3}{2}} \right)$$

$$= \frac{10^{5} \, \text{Pa} \times 0.5 \times 10^{-3} \, \text{m}^{3}}{298} \, \text{ln} \left(\frac{1}{0.5} \left[\frac{373}{298} \right]^{\frac{3}{2}} \right) = 0.173 \, \, \text{JK}^{-1}$$

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0.5 dm³ Ar; 25°C $\xrightarrow[\text{isothermal}]{\text{erev. expansion}}$ 0.05dm³ Ar; 25°C $\xrightarrow[\text{const. V}]{\text{const. V}}$ 0.05dm³ Ar; -25°C

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0.5 dm³ Ar; 25°C
$$\xrightarrow{\text{rev. expansion}}_{\text{isothermal}} 0.05 \text{dm}^3$$
 Ar; 25°C $\xrightarrow{\text{cool}}_{\text{const. V}} 0.05 \text{dm}^3$ Ar; -25°C $\xrightarrow{\text{cool}}_{\text{const. V}} 0.05 \text{dm}^3$ Ar; -25°C $\xrightarrow{\text{cool}}_{\text{const. V}} 0.05 \text{dm}^3$ Ar; -25°C $\xrightarrow{\text{cool}}_{\text{const. V}} 0.05 \text{dm}^3$ Ar; -25°C

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$$\Delta S$$
 when 0.5 dm³ of Ar at 25°C and 1.00 bar is compressed to 0.05 dm³ and is simultaneously cooled to -25° C

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C

0.5 dm³ Ar: 25°C rev. expansion 0.05 dm³ Ar: 25°C $\xrightarrow{\text{cool}}$ 0.05 dm³ Ar: -25° C

0.5 dm³ Ar; 25°C
$$\xrightarrow{\text{rev. expansion}}_{\text{isothermal}}$$
 0.05dm³ Ar; 25°C $\xrightarrow{\text{cool}}_{\text{const. V}}$ 0.05dm³ Ar; -25°C $\Delta S_{\text{II}} = nR \ln \frac{V_f}{V_i} = \frac{p_i V_i}{T_i} \ln \frac{V_f}{V_i}$; $\Delta S_{\text{II}} = C_V \ln \frac{T_f}{T_i}$

0.5 dm³ Ar; 25°C
$$\xrightarrow[\text{isothermal}]{\text{evaluation}}$$
 0.05dm³ Ar; 25°C $\xrightarrow[\text{const. V}]{\text{const. V}}$ 0.05dm³ Ar; -25°C $\Delta S_{\text{I}} = nR \ln \frac{V_f}{V_i} = \frac{p_i V_i}{T_i} \ln \frac{V_f}{V_i}$; $\Delta S_{\text{II}} = C_V \ln \frac{T_f}{T_i}$

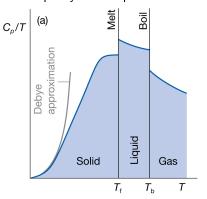
 $\Delta S = \Delta S_{\mathsf{I}} + \Delta S_{\mathsf{II}} = nR \left(\ln \frac{V_f}{V_i} + \frac{3}{2} \ln \frac{T_f}{T_i} \right) = \frac{p_i V_i}{T_i} \ln \left(\frac{V_f}{V_i} \left\lceil \frac{T_f}{T_i} \right\rceil^{\frac{3}{2}} \right)$

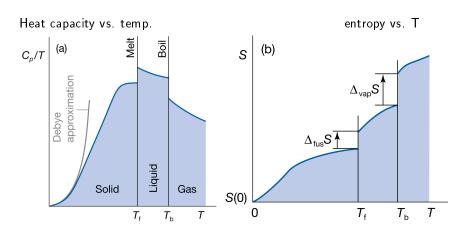
 $=\frac{10^5 \text{Pa} \times 0.5 \times 10^{-3} \text{m}^3}{298} \ln \left(\frac{0.05}{0.5} \left[\frac{248}{298} \right]^{\frac{3}{2}} \right) =$

 $= -0.44 = -0.44 \text{ IK}^{-1}$

Heat capacity vs. temp.

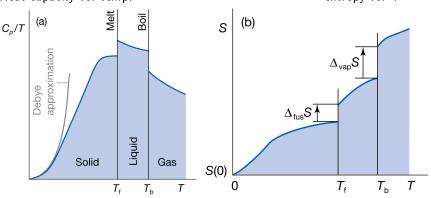




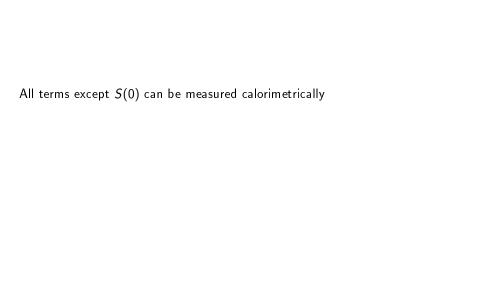


Heat capacity vs. temp.

entropy vs. T



$$S(T) = S(0) + \int_{0}^{T_f} \frac{C_{p}(s)dT}{T} + \frac{\Delta_{\text{fus}}H}{T_{\text{fus}}} + \int_{T_1}^{T_b} \frac{C_{p}(l)dT}{T} + \frac{\Delta_{\text{vap}}H}{T_{\text{vap}}} + \int_{T_1}^{T} \frac{C_{p}(g)dT}{T}$$

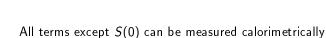


ana	a meegrating analytically	

integrals can be evaluated either graphically or by fitting a polynomial to the data

All terms except S(0) can be measured calorimetrically

and integrating analytically



 $\therefore \frac{dT}{T} = d \ln T$, one can evaluate area under a plot of C_p against $\ln T$

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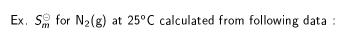
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 $\therefore \frac{dT}{T} = d \ln T$, one can evaluate area under a plot of C_p against $\ln T$. Debye extrapolation : $\mathcal{L}t_0C_p \longrightarrow aT^3$



Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data : $|S_m^{\odot}/J \ K^{-1} mol^{-1}|$

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

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Debye extrapolation	1.92

Ex. S_m^{\odot} for $N_2(g)$ at 25°C calculated from following data :

	$S_m^{\odot}/J\;K^{-1}$ mol $^{-1}$
Debye extrapolation	1.92
35.61	25.25

Ex. S_m^{\odot} for N ₂ (g) at 25°C calculated from following data :

$S_m^{\odot}/J\;K^{-1}mol^{-1}$
1.92
25.25
6.43

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

=x: 0m ::: 12(8) at 10 0 cardarate ::: 11 11 11 11 11 11 11 11 11 11 11 11		
$S_m^{\odot}/J\;K^{-1}mol^{-1}$		
1.92		
25.25		
6.43		
23.38		

Ex. S_m^{\odot} for N₂(g) at 25°C calculated from following data :

111 = (0)	O
	$ S_m^{\odot}/J K^{-1}mol^{-1}$
Debye extrapolation	1.92
35.61	25.25
Phase transition : 35.61K	6.43
63.14	23.38
Fusion: 63.14K	11.42

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77.32	11.41

Ex. S_m^{\odot} for $N_2(g)$ at 25°C calculated from following data :

	$\mid S_m^{\odot} / J \; K^{-1} mol^{-1}$
Debye extrapolation	1.92
35.61	25.25
Phase transition: 35.61K	6.43
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Fusion: 63.14K	11.42
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Vaporization: 77.32K	72.13
	1

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72.13
39.20

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298.15	39.20
Correction for gas imperfection	0.92

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Total	192.06

Ex. S_m^{\odot} for $N_2(g)$ at 25°C calculated from following data : $S_m^{\odot}/J \text{ K}^{-1} \text{mol}^{-1}$ Debye extrapolation 1.92 35.61 25 25

J 10	23.23
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63.14	23.38
Fusion: 63.14K	11.42
77.32	11.41
Vaporization: 77.32K	72.13
298.15	39.20
	0.00

0.92 Correction for gas imperfection Total 192.06

 $S_m(298.15 \,\mathrm{K}) = S_m(0) + 192.06 \,\mathrm{J} \,\mathrm{K}^{-1} \mathrm{mol}^{-1}$

Nernst heat theorem : $\mathop{\mathcal{L}t}_{T o 0}\Delta S\longrightarrow 0$ for any transformation provided all

substances involved are perfectly crystalline

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The entropy of all perfect crystalline substances is zero at T=0

3rd law (?) :

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 $\Omega=\#$ ways the molecules can be arranged in a crystalline form

Boltzmann formula : $S = k_B \ln \Omega$

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In most cases, $\underset{T\to 0}{\mathcal{L}t}\Omega=1,$ $\therefore \underset{T\to 0}{\mathcal{L}t}S=0$

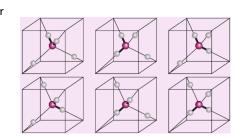
when $\Omega \neq 0$, then S = S(0), residual entropy

each H atom can lie either close to or far from its 'parent' O atom total # of arrangements in sample of N H_2O molecules with 2N H atoms $= 2^{2N}$

lce-l_h:

each H atom can lie either close to or far from its 'parent' O atom total # of arrangements in sample of N H_2O molecules with 2N H atoms = 2^{2N} consider a single central O atom. total number of arrangements of

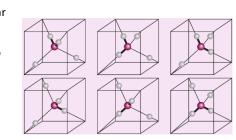
locations of H atoms around central O atom of one H_2O molecule is $2^4 = 16$



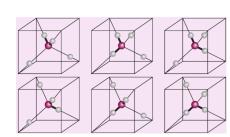
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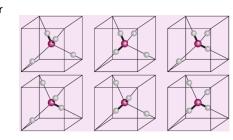
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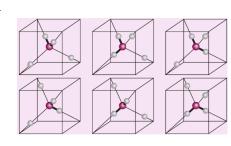
 $(3/8)^N$ of all arrangements are possible



∴ for N water molecules
of possible configurations $= 2^{2N} (3/8)^N = \left(\frac{3}{2}\right)^N$

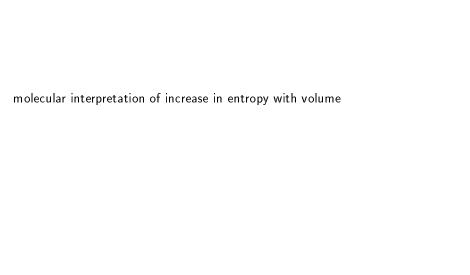
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... for N water molecules # of possible configurations = $2^{2N}(3/8)^N = \left(\frac{3}{2}\right)^N$

$$S(0) = Nk_B \ln \left(\frac{3}{2}\right) = 3.37 \text{ J mol}^{-1} \text{K}^{-1}$$



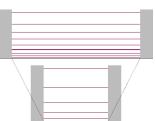
molecular interpretation of increase in entropy with volume

As the system size increases energy levels move closer together and more become accessible to the molecules

molecular interpretation of increase in entropy with volume

As the system size increases energy levels move closer together and more become accessible to the molecules

ways of achieving same energy (Ω) increases



Maxwell's demon: a thought experiment

Open the tab and gas in first chamber expands to fill both chambers

A gas initially in one chamber, connected via a closed tap to a second chamber

containing only vacuum

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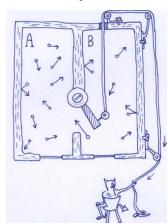
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Maxwell imagined that the tap was operated by a microscopic intelligent creature. If it sees a molecule heading from the second chamber back into the first, it opens the tap and then shuts it, just letting the molecule through. If it sees a molecule heading from the first chamber back into the second chamber, it keeps the tap closed



Maxwell's demon: a thought experiment

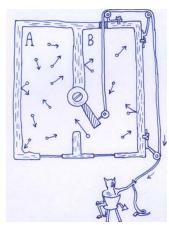
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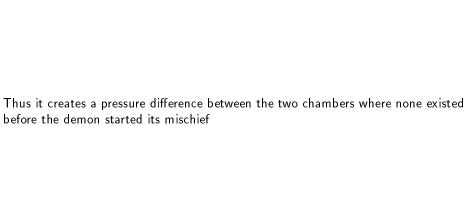
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Demon does no work and yet it makes molecules in second chamber all go back into the first chamber



Thus it	creates	a pressure	difference	between	the two	chambers	where none	existed

as if the demon could therefore cause entropy to decrease in a system with no

before the demon started its mischief

consequent increase in entropy anywhere else

► Conventional explanation : All observations and measurements require energy consumption and the demon is no exception

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- Modern explanation: demon needs to have a memory to operate, this act of storing information (actually it is erasing information) is associated with an increase of entropy, and this increase cancels out any decrease in entropy that

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 It is possible to design a computational process that proceeds entirely

reversibly, and therefore has no increase in entropy associated with it

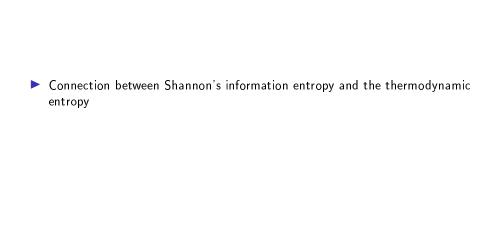
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- Modern explanation : demon needs to have a memory to operate, this act of storing information (actually it is erasing information) is associated with an increase of entropy, and this increase cancels out any decrease in entropy that
- the demon might be able to effect in the system
- ▶ The demon is a computational device that processes and stores information
- It is possible to design a computational process that proceeds entirely reversibly, and therefore has no increase in entropy associated with it
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 Maxwell's demon can operate reversibly therefore, but only if it has a large enough hard disc that it doesn't ever need to clear space to continue operation



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 generally, S = k_BH, where H = information entropy

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▶ Erasure of one bit of information requires a minimum energy cost equal to $k_B T \ln 2 \approx 0.018$ eV, where T is the temperature of a thermal reservoir used in the process.

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- is transmitted by physical devices exploiting electrical or optical signals.
 ∴ it must obey the laws of physics and, first and foremost, the laws of thermodynamics.

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non-information-bearing degrees of freedom of the information-processing system

(1) any logically irreversible process must result in an entropy increase in the non-information-bearing degrees of freedom of the information-processing system or its environment

(2) any logically reversible process can be implemented thermodynamically reversibly.

• an amount of energy equal to $k_BT \ln 2$ (k_BT = thermal noise per unit bandwidth) is needed to transmit a bit of information, and more if quantized channels are used with photon energies $h\nu > kT$