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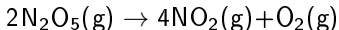


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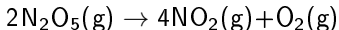
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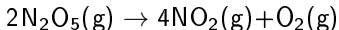
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at time t , degree of dissociation = α

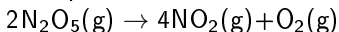
	N_2O_5	NO_2	O_2	total
amount	$n(1 - \alpha)$	$2\alpha n$	$\frac{1}{2}\alpha n$	$n(1 + \frac{3}{2}\alpha)$

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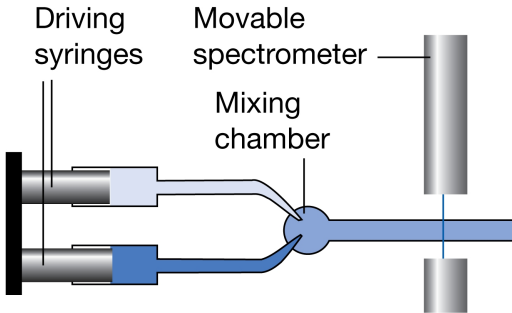
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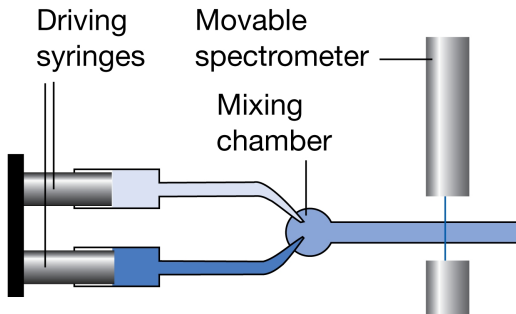
When $\alpha = 0$, $p = p_0$ \therefore at time t , $p(t) = (1 + \frac{3}{2}\alpha) p_0$

real-time-analysis: flow technique



location of the spectrometer corresponds to different times after initiation

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e.g., progress of the reaction $\text{H}_2(\text{g}) + \text{Br}_2(\text{g}) \rightarrow 2\text{HBr}(\text{g})$

can be followed by measuring amount of visible light absorbed by $\text{Br}_2(\text{g})$

Similarly, changes in conductivity and pH can be used as means of monitoring the progress of a reaction

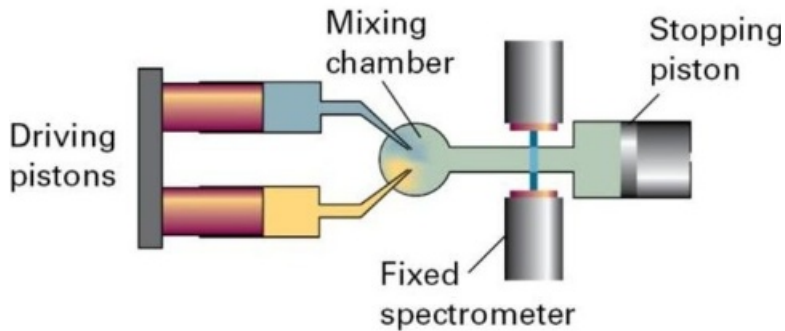
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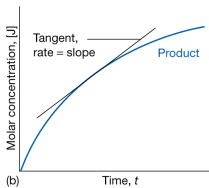
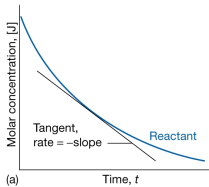
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can be monitored by measuring either conductivity or pH

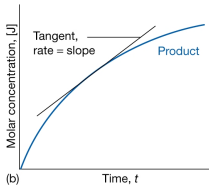
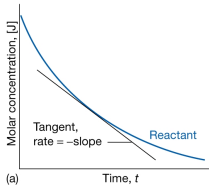
stopped-flow technique



instantaneous rate



instantaneous rate



$$\text{extent of reaction } \xi = \frac{n_J - n_{J,0}}{\nu_J}$$

J refers to species in a reaction mixture

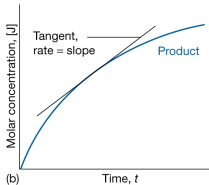
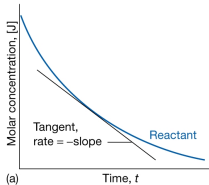
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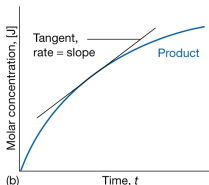
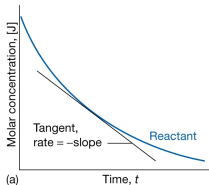
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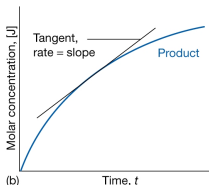
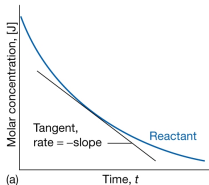
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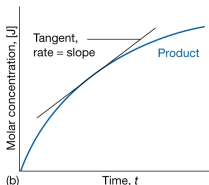
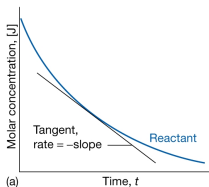
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for gas phase, (molecules.cm⁻³s⁻¹)

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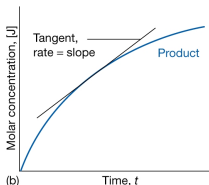
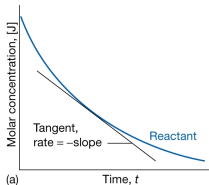
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Typical rate expression, $v = k [A]^m [B]^n$; k = rate constant

order w.r.t. A = $m \in \mathbb{R}$; order w.r.t. B = $n \in \mathbb{R}$; overall order = $m + n \in \mathbb{R}$

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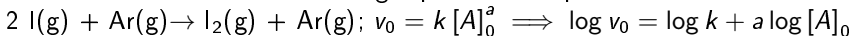
example : unimolecular, $\text{N}_2\text{O}_4 \rightarrow 2\text{NO}_2$

bimolecular, $\text{O} + \text{H}_2 \rightarrow \text{OH} + \text{H}$

Method of initial rates:

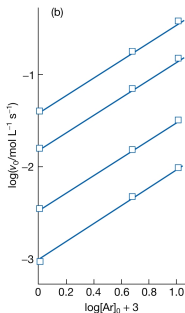
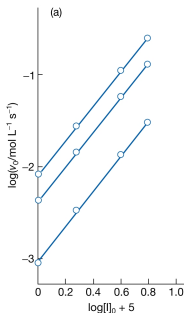
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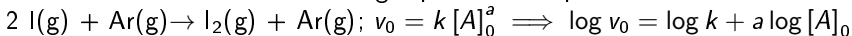
$[\text{I}]_0 / (10^{-5} \text{ mol dm}^{-3})$	1.0	2.0	4.0	6.0
$v_0 / (\text{mol dm}^{-3} \text{ s}^{-1})$	(a) 8.70×10^{-4}	3.48×10^{-3}	1.39×10^{-2}	3.13×10^{-2}
	(b) 4.35×10^{-3}	1.74×10^{-2}	6.96×10^{-2}	1.57×10^{-1}
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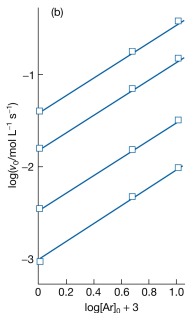
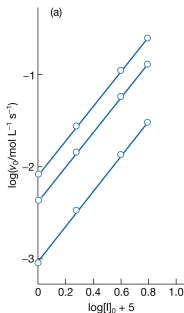
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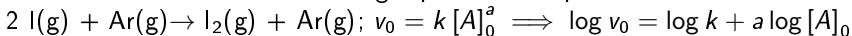
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intercept, $k = 9 \times 10^9 \text{ mol}^{-2} \text{ dm}^6 \text{ s}^{-1}$

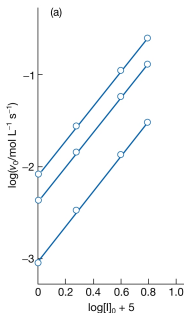
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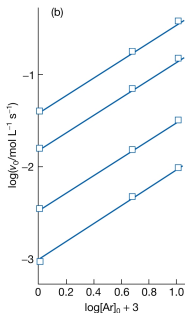


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- ▶ e.g., products participate in the synthesis of HBr, $\text{H}_2 + \text{Br}_2 \rightarrow \text{HBr}$
 - ▶ full rate law depends on $[\text{HBr}]$

half-life

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1st order reaction: $t_{\frac{1}{2}} = \frac{\ln 2}{k}$

time constant, $\tau = \frac{1}{k}$

integrated rate law: Zero- order rxn

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$$\frac{d[A]}{dt} = -k[A]^0 = -k$$

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$$[A] = [A]_0 - kt$$

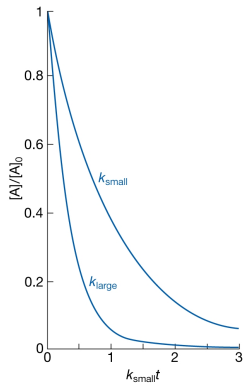
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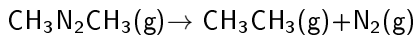
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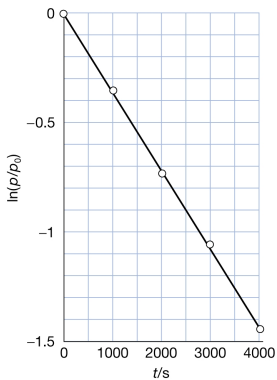
1st order rxn

$$\frac{d[A]}{dt} = -k[A]$$
$$[A] = [A]_0 e^{-kt}$$





t/s	0	1000	2000	3000	4000
p/Pa	10.9	7.63	5.32	3.71	2.59



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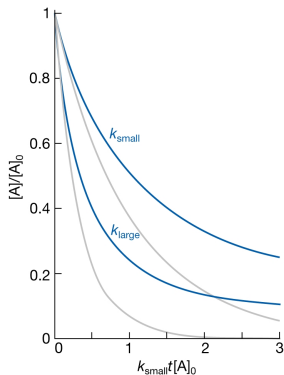
$$\frac{1}{[A]} - \frac{1}{[A]_0} = kt$$

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$$\frac{d[A]}{dt} = -k[A]^2$$

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$$[A] = \frac{[A]_0}{1 + kt[A]_0}$$



$k_{\text{large}} = 3k_{\text{small}}$
(grey lines for first order)

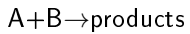
half life for second order reaction: $t_{\frac{1}{2}} = \frac{1}{k[A]_0}$

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In general, for n -th order reaction: $t_{\frac{1}{2}} = \frac{1}{k[A]_0^{n-1}}$

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A+B→products

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$$\ln \left(\frac{\frac{[B]}{[B]_0}}{\frac{[A]}{[A]_0}} \right) = ([B]_0 - [A]_0) kt$$

Order	Reaction	Rate law*	$t_{1/2}$
0	$A \rightarrow P$	$v = k_t$ $k_t t = x$ for $0 \leq x \leq [A]_0$	$[A]_0/2k_t$
1	$A \rightarrow P$	$v = k_t[A]$ $k_t t = \ln \frac{[A]_0}{[A]_0 - x}$	$(\ln 2)/k_t$
2	$A \rightarrow P$	$v = k_t[A]^2$ $k_t t = \frac{x}{[A]_0([A]_0 - x)}$	$1/k_t[A]_0$
	$A + B \rightarrow P$	$v = k_t[A][B]$ $k_t t = \frac{1}{[B]_0 - [A]_0} \ln \frac{[A]_0([B]_0 - x)}{([A]_0 - x)[B]_0}$	
	$A + 2 B \rightarrow P$	$v = k_t[A][B]$ $k_t t = \frac{1}{[B]_0 - 2[A]_0} \ln \frac{[A]_0([B]_0 - 2x)}{([A]_0 - x)[B]_0}$	
	$A \rightarrow P$ with autocatalysis	$v = k_t[A][P]$ $k_t t = \frac{1}{[A]_0 + [P]_0} \ln \frac{[A]_0([P]_0 + x)}{([A]_0 - x)[P]_0}$	
3	$A + 2 B \rightarrow P$	$v = k_t[A][B]^2$ $k_t t = \frac{2x}{(2[A]_0 - [B]_0)([B]_0 - 2x)[B]_0} + \frac{1}{(2[A]_0 - [B]_0)^2} \ln \frac{[A]_0([B]_0 - 2x)}{([A]_0 - x)[B]_0}$	
$n \geq 2$	$A \rightarrow P$	$v = k_t[A]^n$ $k_t t = \frac{1}{n-1} \left\{ \frac{1}{([A]_0 - x)^{n-1}} - \frac{1}{[A]_0^{n-1}} \right\}$	$\frac{2^{n-1} - 1}{(n-1)k_t[A]_0^{n-1}}$

* $x = [P]$ and $v = dx/dt$

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This is a differential-difference equation (also called a master equation) with the

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$$[\text{using } \sum_0^m p \binom{m}{p} a^p b^{m-p} =$$

$$m a \sum_{p=1}^{m-1} \frac{(m-1)!}{(p-1)! \{(m-1)-(p-1)\}!} a^{p-1} b^{\{(m-1)-(p-1)\}} = m a (a + b)^{m-1} \text{ and } a + b = 1]$$

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2. We could have obtained the final result above by starting from first order decay, such that the probability of a molecule remaining unreacted after time t is e^{-kt} and not reacting is $1 - e^{-kt}$

\implies the probability of n molecules remaining unreacted after time t is $(e^{-kt})^n$ and not reacting is $(1 - e^{-kt})^{n_0-n}$

3. The variance $= n_0 e^{-kt} (1 - e^{-kt})$

[using $\sum_{p=0}^m p^2 \binom{m}{p} a^p b^{m-p} \stackrel{a+b=1}{=} m(m-1)a^2 + ma$

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i.e., the larger the number of molecules, the relative deviation from the mean will be smaller. This is why the phenomenological results work - at the macroscopic level, the deviation is negligible.

4. The assumption that the transition is occurring in a single step from n to $n - 1$ and not to $n - 2$ is tantamount to Markovian statistics.