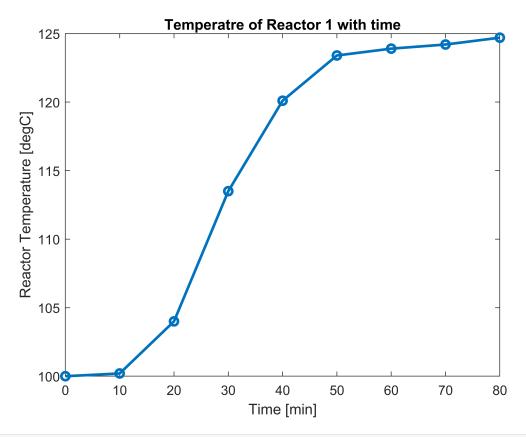
```
clear
clc
% defining general variables
V_ac = 210; %in ml, acetic acid
V_but = 340; %in ml, butanol
rho ac = 1.05; %in g/ml
rho_but = 0.81; %in g/ml
M ac = 60; % Molar mass
M but = 74;
n_ac = (V_ac*rho_ac)/M_ac; % no. of moles
n but = (V_but*rho_but)/M_but;
t = (0:10:80);
%For reactor 1:
T_r1 = [100, 100.2, 104, 113.5, 120.1, 123.4, 123.9, 124.2, 124.7];
V_{naoh_r1} = [9.1, 8, 7.4, 6.3, 5.0, 4.3, 2.2, 1.2, 0.5]; %in ml
n_acid_r1 = 1*V_naoh_r1/1000; %mol of acid in sample neutralised by 1N NaOH
V_sample = 2; %volume of sample in ml
conc acid r1 = n acid r1*1000/V sample;
cum_sample = (2:2:18);
water_lost = [0,16.5,15,16,11.5,9.5,5,2.0,1.3];%
cum_water_rem_r1 = zeros(1,length(water_lost));
for i=2:9
    cum water rem r1(i) = water lost(i)+cum water rem r1(i-1);
end
vol_in_r1 = 550-cum_sample-cum_water_rem_r1;
n acid reacted r1 = (vol in r1.*conc acid r1)/1000;
X1 = (n_ac-n_acid_reacted_r1)/(n_ac)
X1 = 1 \times 9
   0.3215
            0.4237
                     0.4840
                             0.5761
                                      0.6728
                                               0.7253
                                                        0.8616
                                                                0.9251 ...
V_{\text{M}} naoh = [0,9,7.1,6.1,5.1,4.1,4.4,2.4,1.5];
V W = 5 \% m1
V W = 5
acid_lost = (((1.*V_W_naoh)/V_W).*water_lost) % in millimoles
acid lost = 1 \times 9
                                                                 0.9600 ...
           29.7000
                    21.3000
                                               7.7900
                                                        4.4000
                            19.5200
                                     11.7300
total_acid_lost=sum(acid_lost)
total acid lost = 95.7900
%For reactor 2:
T_r2 = [98.7, 97.4, 97, 96.9, 96.4, 96.5, 96.5, 96.6, 96.5];
V_{\text{naoh}_r2} = [9.5, 8.5, 7.2, 6.2, 5.5, 5, 4.6, 4.4, 4.6];
n acid r2 = 1*V naoh r2/1000;
conc_acid_r2 = n_acid_r2*1000/V_sample;
V_{in_r2} = 550-cum_sample;
```

```
n_acid_reacted_r2 = (V_in_r2.*conc_acid_r2)/1000;
X2 = (n_ac-n_acid_reacted_r2)/n_ac;

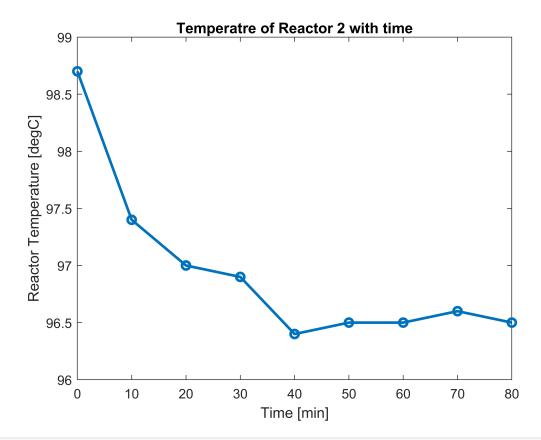
%Enhancement factor:
E = (X1-X2)./X2;

% error analysis

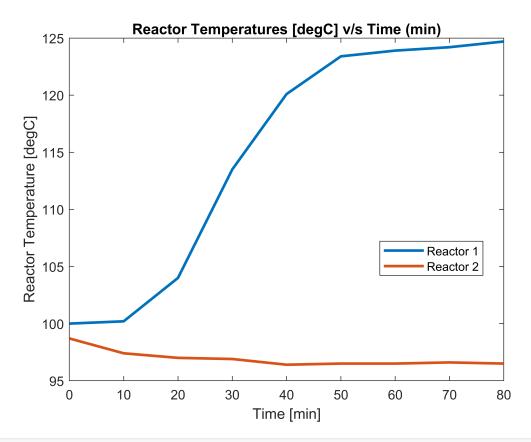
%Plots
plot(t, T_r1,'-o', 'LineWidth', 2)
title('Temperatre of Reactor 1 with time')
ylabel('Reactor Temperature [degC]')
xlabel('Time [min]')
```



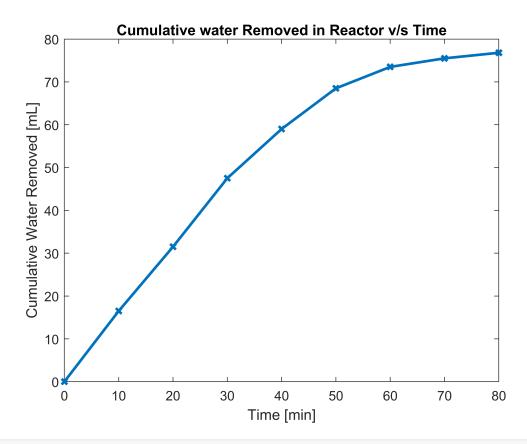
```
plot(t, T_r2, '-o', 'LineWidth', 2)
title('Temperatre of Reactor 2 with time')
ylabel('Reactor Temperature [degC]')
xlabel('Time [min]')
```



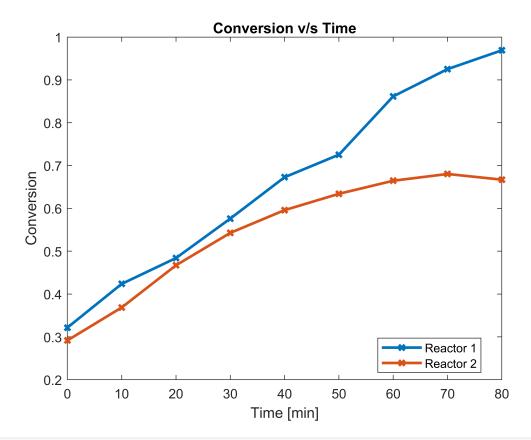
```
plot(t, T_r1, 'LineWidth', 2)
hold on
plot(t, T_r2, 'LineWidth', 2)
title('Reactor Temperatures [degC] v/s Time (min)')
ylabel('Reactor Temperature [degC]')
xlabel('Time [min]')
legend('Reactor 1', 'Reactor 2', 'Location', 'best')
hold off
```



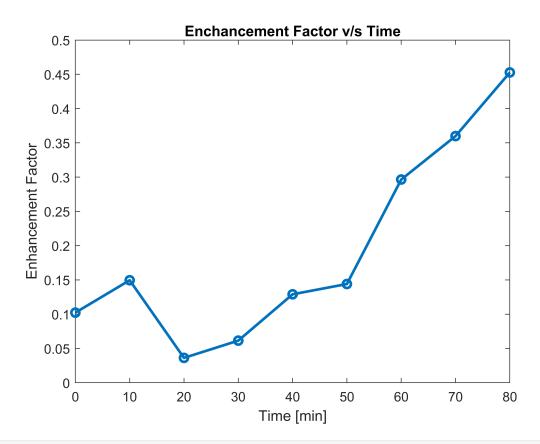
```
plot(t, cum_water_rem_r1, '-x','LineWidth',2)
xlabel('Time [min]')
ylabel('Cumulative Water Removed [mL]')
title('Cumulative water Removed in Reactor v/s Time')
```



```
plot(t,X1,'-x','LineWidth',2)
hold on
plot(t,X2,'-x','LineWidth',2)
xlabel('Time [min]')
ylabel('Conversion')
title('Conversion v/s Time')
legend('Reactor 1', 'Reactor 2', 'Location','best')
%ylim([0 1])
hold off
```



```
plot(t, E,'-o','LineWidth',2)
hold on
xlabel('Time [min]')
ylabel('Enhancement Factor')
title('Enchancement Factor v/s Time')
hold off
```



```
% for Reactor 1
```

Writing to Excel

```
filename='MT_302.xlsx';
T=table(t',T_r1',water_lost',V_naoh_r1',vol_in_r1',X1');
T.Properties.VariableNames = {'Time','Temperature','Water Lost','NaOH required','Volume remain:
```

 $T = 9 \times 6 \text{ table}$

Time Water Lost Temperature NaOH required Volume remaining 0 100 0 9.1000 548 2 10 100.2000 16.5000 8 529.5000 3 20 104 15 7.4000 512.5000 4 30 113.5000 6.3000 494.5000 16 5 40 120.1000 11.5000 5 481 6 50 123.4000 9.5000 4.3000 469.5000 7 60 123.9000 5 2.2000 462.5000 8 70 124.2000 2 1.2000 458.5000

	Time	Temperature	Water Lost	NaOH required	Volume remaining
9	80	124.7000	1.3000	0.5000	455.2000

```
writetable(T,filename,'Sheet','reactor 1')

T1=table(t',T_r2',V_naoh_r2',X2');
T1.Properties.VariableNames = {'Time','Temperature','NaOH required','Conversion (X2)'}
```

 $T1 = 9 \times 4 \text{ table}$

	Time	Temperature	NaOH required	Conversion (X2)	
1	0	98.7000	9.5000	0.2917	
2	10	97.4000	8.5000	0.3686	
3	20	97	7.2000	0.4671	
4	30	96.9000	6.2000	0.5428	
5	40	96.4000	5.5000	0.5959	
6	50	96.5000	5	0.6340	
7	60	96.5000	4.6000	0.6645	
8	70	96.6000	4.4000	0.6803	
9	80	96.5000	4.6000	0.6670	

```
writetable(T1,filename,'Sheet','reactor 2')

results = table(t',X1',X2',E');
results.Properties.VariableNames={'Time','Conversion (X1)', 'Conversion (X2)', 'Enhancement Face)
```

results = 9×4 table

	Time	Conversion (X1)	Conversion (X2)	Enhancement Factor
1	0	0.3215	0.2917	0.1022
2	10	0.4237	0.3686	0.1495
3	20	0.4840	0.4671	0.0362
4	30	0.5761	0.5428	0.0614
5	40	0.6728	0.5959	0.1290
6	50	0.7253	0.6340	0.1440
7	60	0.8616	0.6645	0.2965
8	70	0.9251	0.6803	0.3599
9	80	0.9690	0.6670	0.4527

```
writetable(results,filename,'sheet','Results')
```