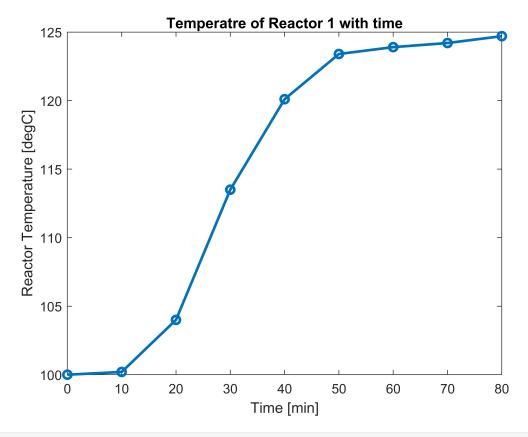
```
clear
clc
% defining general variables
V_ac = 210; %in ml, acetic acid
V_but = 340; %in ml, butanol
rho ac = 1.05; %in g/ml
rho_but = 0.81; %in g/ml
M ac = 60; % Molar mass
M but = 74;
n_ac = (V_ac*rho_ac)/M_ac; % no. of moles
n but = (V but*rho but)/M but;
t = (0:10:80);
%For reactor 1:
T_r1 = [100, 100.2, 104, 113.5, 120.1, 123.4, 123.9, 124.2, 124.7];
V_{naoh_r1} = [9.1, 8, 7.4, 6.3, 5.0, 4.3, 2.2, 1.2, 0.5]; %in ml
n_acid_r1 = 1*V_naoh_r1/1000; %mol of acid in sample neutralised by 1N NaOH
V_sample = 2; %volume of sample in ml
conc acid r1 = n acid r1*1000/V sample;
cum_sample = (2:2:18);
water_lost = [0,16.5,15,16,11.5,9.5,5,2.0,1.3];%
cum_water_rem_r1 = zeros(1,length(water_lost));
for i=2:9
    cum water rem r1(i) = water lost(i)+cum water rem r1(i-1);
end
vol_in_r1 = 550-cum_sample-cum_water_rem_r1
vol_in_r1 = 1 \times 9
 548.0000 529.5000 512.5000 494.5000 481.0000 469.5000 462.5000 458.5000 ...
n acid reacted r1 = (vol in r1.*conc acid r1)/1000;
X1 = (n_ac-n_acid_reacted_r1)/(n_ac);
V W naoh = [0,9,7.1,6.1,5.1,4.1,4.4,2.4,1.5];
V W = 5; \% m1
acid_lost = ((1.*V_W_naoh)/V_W).*water_lost % in millimoles
acid lost = 1 \times 9
                                                                0.9600 ...
           29.7000
                   21.3000
                           19.5200
                                    11.7300
                                              7.7900
                                                       4.4000
total_acid_lost=sum(acid_lost)
total_acid_lost = 95.7900
%For reactor 2:
T_r2 = [98.7, 97.4, 97, 96.9, 96.4, 96.5, 96.5, 96.6, 96.5];
V_{\text{naoh}_r2} = [9.5, 8.5, 7.2, 6.2, 5.5, 5, 4.6, 4.4, 4.6];
n acid r2 = 1*V naoh r2/1000;
conc acid r2 = n acid r2*1000/V sample;
V_{in_r2} = 550-cum_sample;
n_acid_reacted_r2 = (V_in_r2.*conc_acid_r2)/1000;
```

X2 = (n_ac-n_acid_reacted_r2)/n_ac;

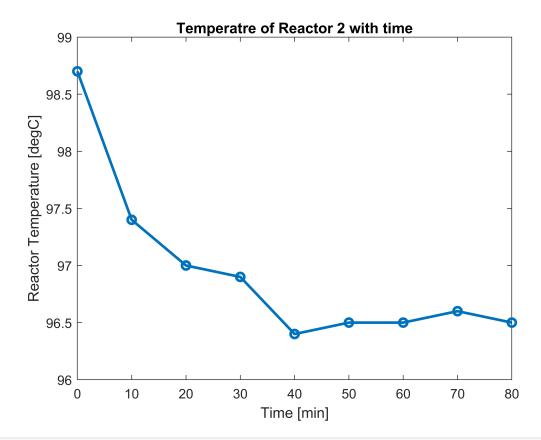
```
%Enhancement factor:
E = (X1-X2)./X2;

% error analysis

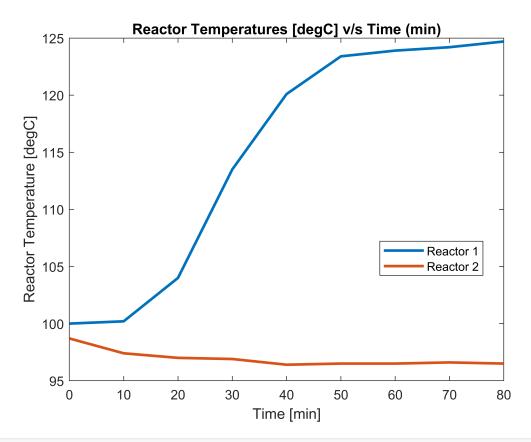
%Plots
plot(t, T_r1,'-o', 'LineWidth', 2)
title('Temperatre of Reactor 1 with time')
ylabel('Reactor Temperature [degC]')
xlabel('Time [min]')
```



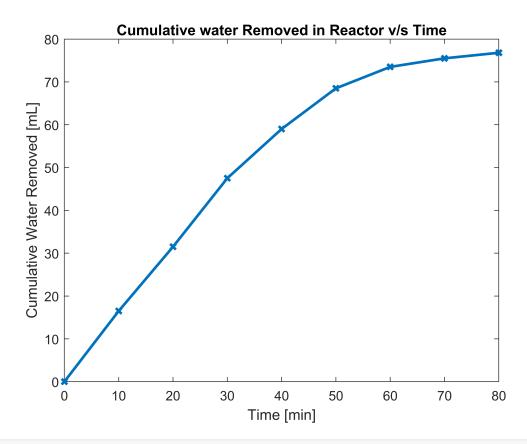
```
plot(t, T_r2, '-o', 'LineWidth', 2)
title('Temperatre of Reactor 2 with time')
ylabel('Reactor Temperature [degC]')
xlabel('Time [min]')
```



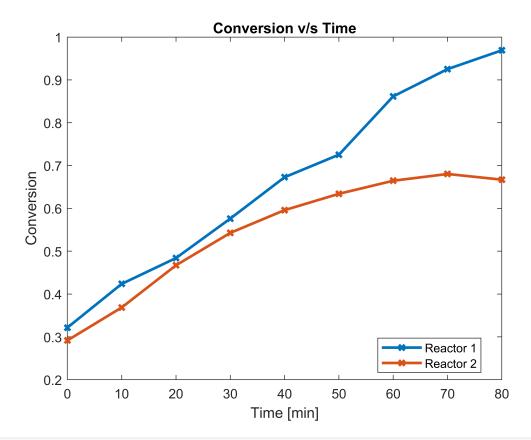
```
plot(t, T_r1, 'LineWidth', 2)
hold on
plot(t, T_r2, 'LineWidth', 2)
title('Reactor Temperatures [degC] v/s Time (min)')
ylabel('Reactor Temperature [degC]')
xlabel('Time [min]')
legend('Reactor 1', 'Reactor 2', 'Location', 'best')
hold off
```



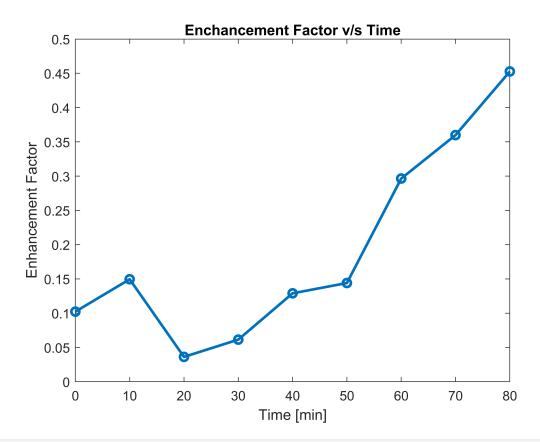
```
plot(t, cum_water_rem_r1, '-x','LineWidth',2)
xlabel('Time [min]')
ylabel('Cumulative Water Removed [mL]')
title('Cumulative water Removed in Reactor v/s Time')
```



```
plot(t,X1,'-x','LineWidth',2)
hold on
plot(t,X2,'-x','LineWidth',2)
xlabel('Time [min]')
ylabel('Conversion')
title('Conversion v/s Time')
legend('Reactor 1', 'Reactor 2', 'Location','best')
%ylim([0 1])
hold off
```



```
plot(t, E,'-o','LineWidth',2)
hold on
xlabel('Time [min]')
ylabel('Enhancement Factor')
title('Enchancement Factor v/s Time')
hold off
```



```
% for Reactor 1
```

Writing to Excel

```
filename='MT_302.xlsx';
T=table(t',T_r1',water_lost',acid_lost',V_naoh_r1',vol_in_r1',X1');
T.Properties.VariableNames = {'Time','Temperature','Water Lost','Acid Lost','NaOH required','Vol_in_r1', Temperature', Temperatur
```

 $T = 9 \times 7 \text{ table}$

Acid Lost Time Water Lost Temperature NaOH required 0 100 0 0 9.1000 2 10 100.2000 16.5000 29.7000 8 3 20 104 15 21.3000 7.4000 4 30 113.5000 19.5200 6.3000 16 5 40 120.1000 11.5000 11.7300 5 6 50 123.4000 9.5000 7.7900 4.3000 7 60 123.9000 5 4.4000 2.2000 8 70 124.2000 2 0.9600 1.2000

| | Time | Temperature | Water Lost | Acid Lost | NaOH required |
|---|------|-------------|------------|-----------|---------------|
| 9 | 80 | 124.7000 | 1.3000 | 0.3900 | 0.5000 |

```
writetable(T,filename,'Sheet','reactor 1')

T1=table(t',T_r2',V_naoh_r2',X2');
T1.Properties.VariableNames = {'Time','Temperature','NaOH required','Conversion (X2)'}
```

 $T1 = 9 \times 4 \text{ table}$

| | Time | Temperature | NaOH required | Conversion (X2) |
|---|------|-------------|---------------|-----------------|
| 1 | 0 | 98.7000 | 9.5000 | 0.2917 |
| 2 | 10 | 97.4000 | 8.5000 | 0.3686 |
| 3 | 20 | 97 | 7.2000 | 0.4671 |
| 4 | 30 | 96.9000 | 6.2000 | 0.5428 |
| 5 | 40 | 96.4000 | 5.5000 | 0.5959 |
| 6 | 50 | 96.5000 | 5 | 0.6340 |
| 7 | 60 | 96.5000 | 4.6000 | 0.6645 |
| 8 | 70 | 96.6000 | 4.4000 | 0.6803 |
| 9 | 80 | 96.5000 | 4.6000 | 0.6670 |

```
writetable(T1,filename,'Sheet','reactor 2')

results = table(t',X1',X2',E');
results.Properties.VariableNames={'Time','Conversion (X1)', 'Conversion (X2)', 'Enhancement Face)
```

results = 9×4 table

| | Time | Conversion (X1) | Conversion (X2) | Enhancement Factor |
|---|------|-----------------|-----------------|--------------------|
| 1 | 0 | 0.3215 | 0.2917 | 0.1022 |
| 2 | 10 | 0.4237 | 0.3686 | 0.1495 |
| 3 | 20 | 0.4840 | 0.4671 | 0.0362 |
| 4 | 30 | 0.5761 | 0.5428 | 0.0614 |
| 5 | 40 | 0.6728 | 0.5959 | 0.1290 |
| 6 | 50 | 0.7253 | 0.6340 | 0.1440 |
| 7 | 60 | 0.8616 | 0.6645 | 0.2965 |
| 8 | 70 | 0.9251 | 0.6803 | 0.3599 |
| 9 | 80 | 0.9690 | 0.6670 | 0.4527 |

```
writetable(results,filename,'sheet','Results')
```