# Stretching colloidal suspensions: from flow to fracture

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## Concentrated colloidal suspensions

Concentrated suspensions of particles (CS) are common every day fluids

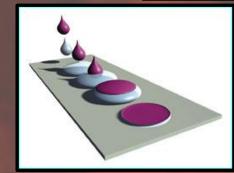




CS can exhibit pronounced increases in viscosity with strain rate (shear thickening)



Under certain conditions fluids may even jam solid





## Model Hard Sphere Colloids

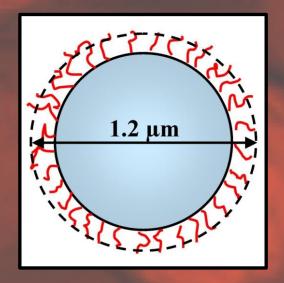
Hard spheres are commonly used as a model system.

This simplifies the interactions present:

- Geometry rather than energetics
- Hydrodynamic interactions

Insights gained from hard spheres, provide insight into more complicated systems (e.g emulsions)





### **Our Colloids**

Poly-methyl methacrylate particles (D  $\sim$  1.2  $\mu$ m )

Sterically stabilised with 10nm Poly-12- hydroxystearic acid chains

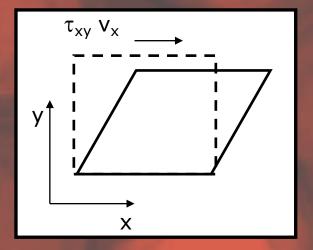
### Shear and extensional flows

Concentrated suspensions are generally studied in shear flows

Very little research has examined extensional geometries.

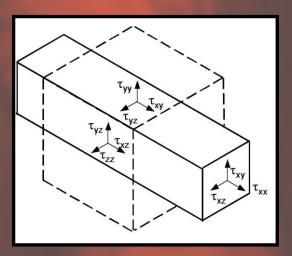
However, many practical flows are extensional or mixed.
e.g nozzle flows

#### **Shear flow:**



$$\eta = \frac{\tau_{xy}}{\dot{\gamma}_{xy}}$$

### **Extensional flow:**



$$\eta_e = \frac{\tau_{xx} - \tau_{yy}}{\dot{\epsilon}_{xx}}$$

### **Extensional Rheometer**

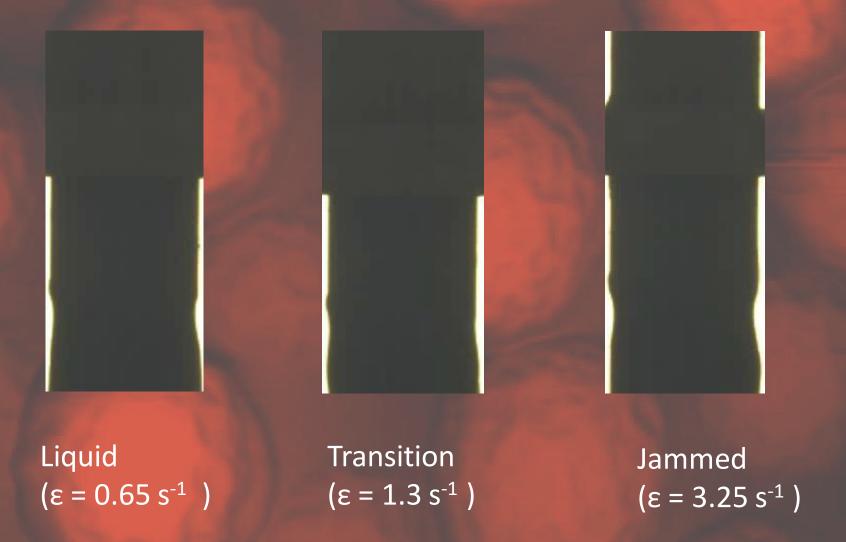


Sample placed between two cylindrical plates (example using Glycerol)

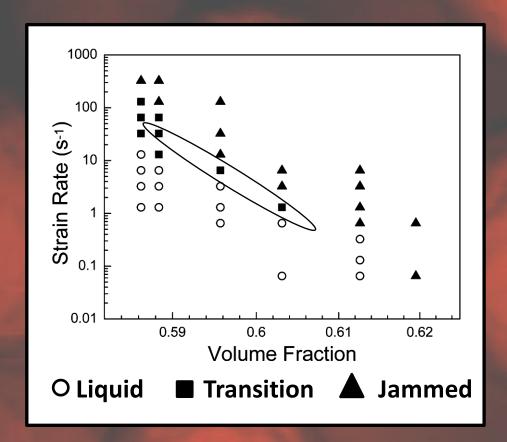
Top plate is moved upwards at a constant velocity

The dynamics of the liquid are imaged using a high speed camera

## Strain-rate dependent behaviour of Concentrated Suspensions of Colloids (φ~0.603)

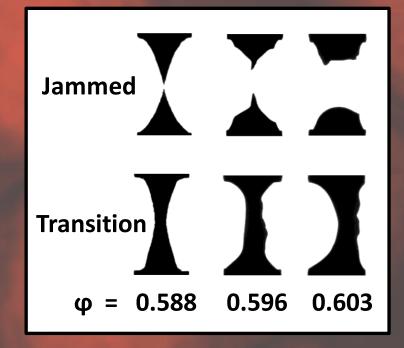


### Volume Fraction Dependence



With increasing volume fraction we see increasing asymmetry and larger granules

A 2% change in volume fraction alters critical strain rate by ~2 orders of magnitude



## Understanding the jamming mechanism

## Relationship to Shear Rheology

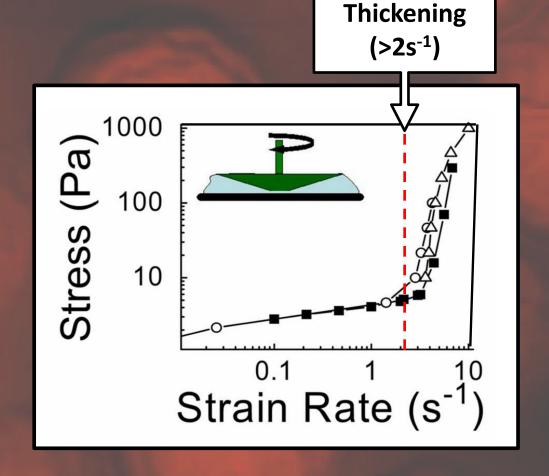
For  $\phi \sim 0.603$  we observe strong shear thickening...

...but **not** jamming

Timescale for the onset of shear thickening closely matches the 'transition'

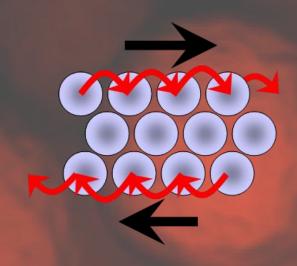
In extension the plate separation initially results in a mixed flow of shear and extension

So what causes the dramatic jamming and granulation in the extensional geometry?



**Shear** 

## Dilatancy

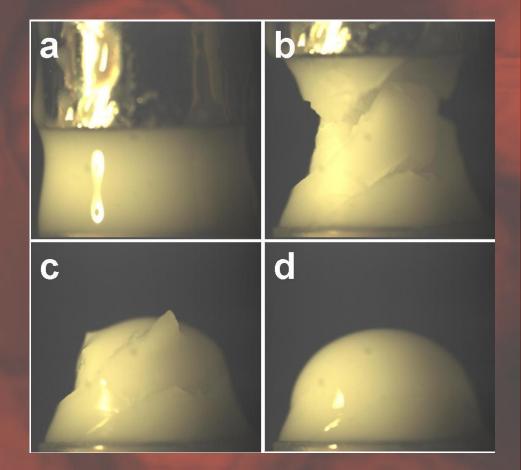


Particles poke through the liquid surface resulting in scattering

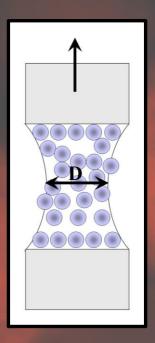
→ Surface appears dry and matt

Dilatancy appears to correlate with the onset of granulation

In order for a packed bed of particles to flow the volume must increase.



### **Jamming**



As volume filled by the particles expands, particles will poke through the air-liquid interface .

Dilatancy would be enhanced by Shear Thickening due to cluster formation

Capillary forces generated between exposed particles confine and arrest flow of suspension.

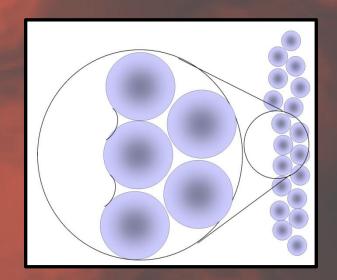
→ jamming and granulation

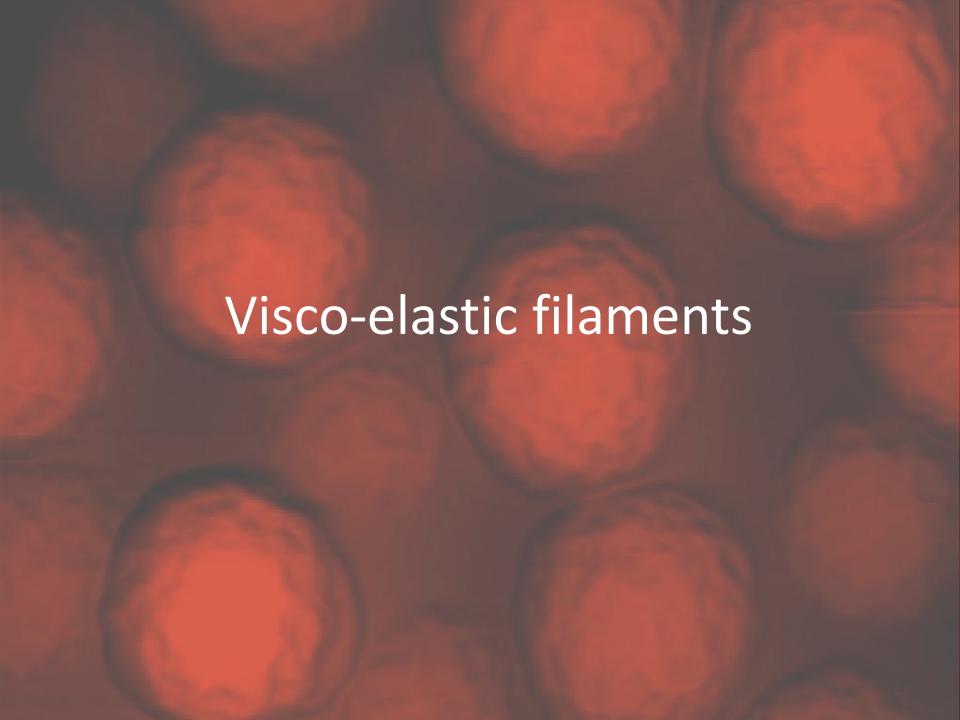
### Simple estimate:

$$P_{\text{osmotic}} = \dot{\eta \epsilon}/(1-(\phi/\phi_0))^2 \sim P_{\text{LaPlace}} = \gamma/D$$

$$\rightarrow \dot{\epsilon}_{Critical} \sim 10s^{-1}$$
 for  $\phi \sim 0.6$ 

Compares well with experimental value of ~ 4s<sup>-1</sup>





### Viscoelastic filament

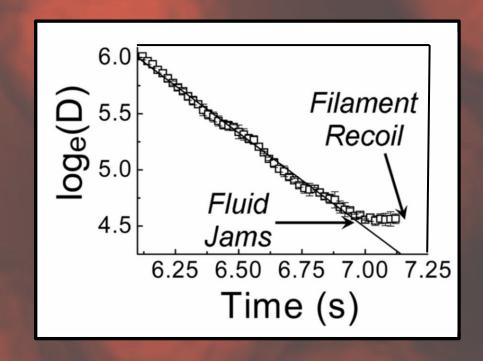
We observe visco-elastic recoil of filaments

#### Two stages:

- 1) Rapid elastic recoil after filament ruptures
- 2) Slow viscous movement on timescale of fluid relaxation.

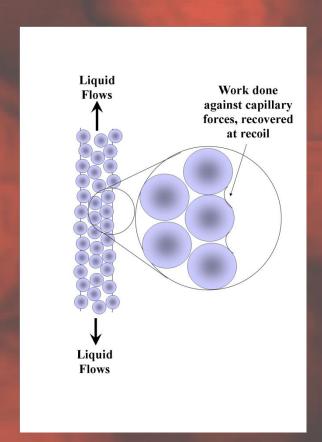
Diameter of filament narrows exponentially with time

Prior to recoil, filament diameter stops thinning → Jamming



### Viscoelastic filament

- Jamming may be due to self-filtration
  - filament ~100x particle diameter
  - $-u^{(\sigma/D^2)ka^2/\eta} \rightarrow \text{few } \% \text{ change in volume}$  fraction
- Upon jamming the rheometer continues to stretch the filament
- This performs work against capillary forces which is recoverable upon rupture (ie elastic)



### Conclusions

 Above a critical strain rate hard sphere colloidal suspensions undergo dilatancy induced jamming and granulation.

Colloidal filaments can display visco-elastic recoil.

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