

**The University of Melbourne**  
**School of Engineering**

**Semester 1 Assessment 2012**

**ENGR30001 – Fluid Mechanics & Thermodynamics**

Exam Duration: 3 hours

This paper has FIFTEEN (15) pages consisting of EIGHT (8) questions.

*Authorized material:*

Electronic calculators approved by the School of Engineering may be used.  
Three tables, one chart and a table of formulae are attached.

*Instructions to Invigilators:*

Script books to be provided.

*Instructions to Students:*

All questions are to be attempted.  
Full marks will be awarded for obtaining 100 marks of a potential 110 marks

**THIS PAPER MUST NOT BE REMOVED FROM THE EXAMINATION ROOM**

*This paper is to be held by the Baillieu Library*

**Question 1**

- i) Sketch a  $T - v$  diagram for  $H_2O$  showing the liquid, saturation and superheated regions and at least one isobar passing through each of these regions. Also indicate the critical point on the diagram. **(3 marks)**
- ii) An open container of water, initially at sea-level, is transported up Mt Jackson, Colorado, where the atmospheric pressure is 70.11kPa. Has the  $H_2O$  boiling point temperature increased, decreased or remained the same during transport? **(1 mark)**
- iii) Determine the saturation temperature for  $H_2O$  on Mt Jackson. **(1 mark)**
- iv) A worker at an observatory on Mt Jackson needs to produce superheated steam. Using steam tables, calculate the heat energy (in Joules) required to raise the temperature of 0.5kg of dry saturated  $H_2O$  by  $10^\circ\text{C}$  above the saturation temperature. **(4 marks)**
- v) What is the specific volume of  $H_2O$  at  $T = 250^\circ\text{C}$  and  $p = 132.15 \text{ kPa}$ ? **(2 marks)**

**(Total for Question 1 = 11 marks)**

**Question 2**

- i) Consider the compression of a hot gas by a piston in a leakproof cylinder. Is this system definitely open, closed or isolated? **(1 mark)**
- ii) State the first law of thermodynamics and the non-flow energy equation **(2 marks)**
- iii) Calculate the specific volume of air at a gauge pressure of 500 kPa and temperature of  $25^\circ\text{C}$ .  $\bar{R} = 287 \text{ J/(kg K)}$  for air. Assume  $p_{atm} = 101.3 \text{ kPa}$ . **(2 marks)**

*(Question 2 continues on next page)*

**Question 2 (continued)**

- iv) Consider the flow of H<sub>2</sub>O through a turbine. The process is adiabatic (no heat is transferred). The turbine inlet pressure is  $p_1 = 4$  MPa, with  $T_1 = 400^\circ\text{C}$ . The inlet velocity is  $V_1 = 30$  m/s. The exit pressure,  $p_2 = 0.1$  MPa with  $T_2 = 90^\circ\text{C}$  and exit velocity of  $V_2 = 20$  m/s. Using the steady flow energy equation, determine the specific work done by the turbine. **(5 marks)**
- v) Determine the mass flow rate required for the turbine to produce 1 MW of power. **(1 mark)**
- vi) In one or two sentences, explain why this turbine could not work in practice. **(1 mark)**

**(Total for Question 2 = 12 marks)**

**Question 3**

- i) Sketch a  $p - v$  property diagram illustrating the Joule-Brayton Cycle. **(2 marks)**
- ii) Sketch a  $T - s$  diagram for the Joule-Brayton Cycle. You may need to make use of the equation to relate entropy to temperature and pressure:

$$s_2 - s_1 = C_p \ln\left(\frac{T_2}{T_1}\right) - \bar{R} \ln\left(\frac{p_2}{p_1}\right)$$

(Note: only a sketch is required – the equation above is only provided to help you qualitatively estimate the shape of the  $T-s$  curves for the processes in the cycle)

**(2 marks)**

*(Question 3 continues on next page)*

**Question 3 (continued)**

- iii) Show that the thermal efficiency of a Gas Turbine engine (using the Joule-Brayton cycle) is given by:

$$\eta = 1 - r_p^{\frac{1-\gamma}{\gamma}}$$

Note that for adiabatic compression or expansion:

$$\frac{T_2}{T_1} = \left( \frac{p_2}{p_1} \right)^{\frac{\gamma-1}{\gamma}}$$

**(4 marks)**

- iv) What are the two main purposes of the turbine stage of a gas turbine engine in a helicopter (i.e., what does the turbine drive). **(2 marks)**
- v) Consider two engines, a Gas Turbine (Joule-Brayton Cycle) and a Spark Ignition Internal Combustion engine (Otto cycle). If air can be supplied to these engines at  $p = 101.3\text{kPa}$  and  $T = 25^\circ\text{C}$  (representing min. pressure and temperature), and after combustion  $T = 800^\circ\text{C}$  and  $p = 3\text{ MPa}$  (max. temperature and pressure), determine which engine has the higher efficiency.  $\bar{R} = 287\text{ J/(kg K)}$  and  $\gamma = 1.4$  for air.

The efficiency of the Otto cycle is given by:

$$\eta = 1 - \frac{1}{r_v^{\gamma-1}},$$

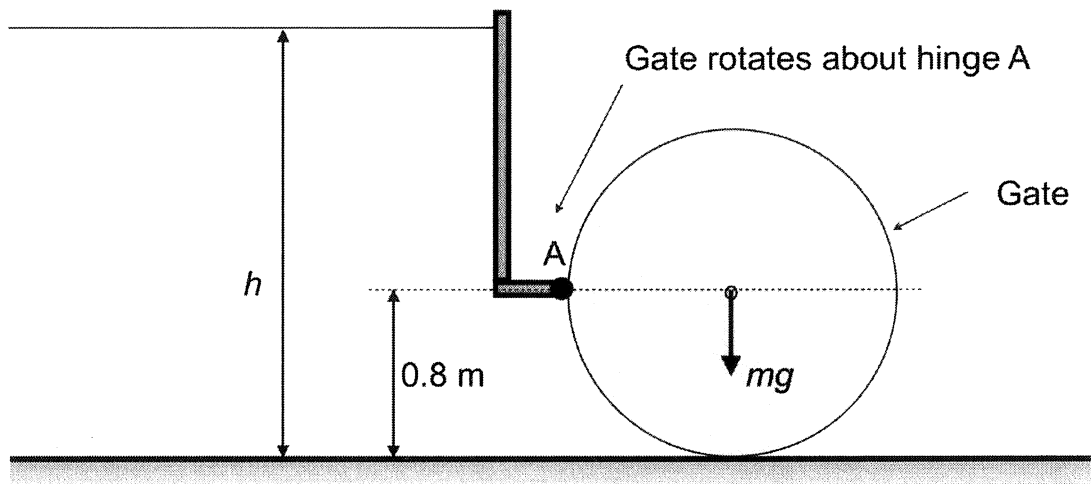
where  $r_v$  is the ratio between the maximum and minimum volumes during the cycle.

**(2 marks)**

**(Total for Question 3 = 12 marks)**

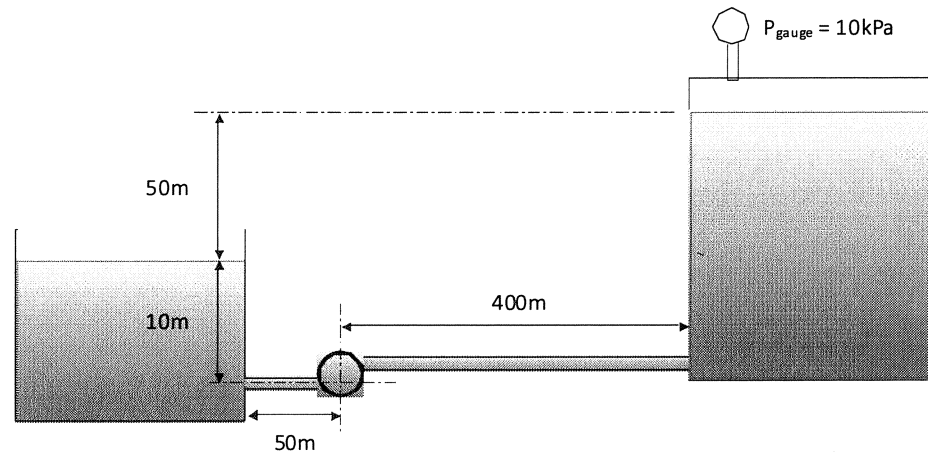
**Question 4**

A 1.0 m long solid cylinder hinged at point A is used as an automatic gate, as shown in the figure. When the water (of density  $1000 \text{ kg/m}^3$ ) reaches the level of 5 m ( $h = 5 \text{ m}$ ), the gate opens by turning about the hinge at point A.



- (a) Determine the net horizontal and vertical forces acting on the gate when the gate is just about to open. (Hint: you do *not* need to integrate along the curved surface to resolve these forces.) **(7 marks)**
- (b) From this, determine the total hydrostatic force acting on the gate and its line of action when the gate is just about to open. **(3 marks)**
- (c) Calculate the mass of the gate. (You may assume that the resultant hydrostatic force acts along a line that passes through the center of the circle.) **(5 marks)**

**(Total for Question 4 = 15 marks)**

**Question 5**

Water of density  $1000 \text{ kg/m}^3$  is pumped between two large reservoirs through a pipe that has an internal diameter of 300 mm and a roughness length of 1.2 mm. The inlet tank is open to atmosphere (where  $P_{\text{atm}} = 101 \text{ kPa}$ ), while the discharge tank is sealed and is maintained at a pressure of 10kPa above atmospheric pressure. Loss coefficients for minor losses are as follows:

Minor Loss	Loss coefficient
Inlet loss	0.5
Exit loss	1.0

- (a) Given that the pipe flow is in the fully rough regime, write an expression for the system head purely as a function of the volume flow rate  $Q$ . **(8 Marks)**
- (b) The manufacturer of the pump provides details of the performance of the pump, where the pump head (in m) as a function of volume flow rate (in  $\text{m}^3/\text{s}$ ) is given by

$$h_p = 150 - 25Q^2$$

Determine the volume flow rate at the operating point of the system. **(4 Marks)**

*(Question 5 continues on next page)*

**Question 5 (continued)**

- (c) The required Net Positive Suction Head ( $NPSH_R$ ) supplied by the pump manufacturer is 3 m. Determine whether the pump is within the permissible operating range at the operating point. The vapour pressure of water at the operating conditions is 2000 Pa. **(5 Marks)**
- (d) If the mechanical efficiency of the pump is  $\eta = 0.65$ , determine the mechanical brake power supplied to the pump at the operating condition. **(3 Marks)**

**(Total for Question 5 = 20 marks)**

**Question 6**

The mechanical energy equation for horizontal, isothermal, ideal gas flow in a pipe of uniform cross-section is

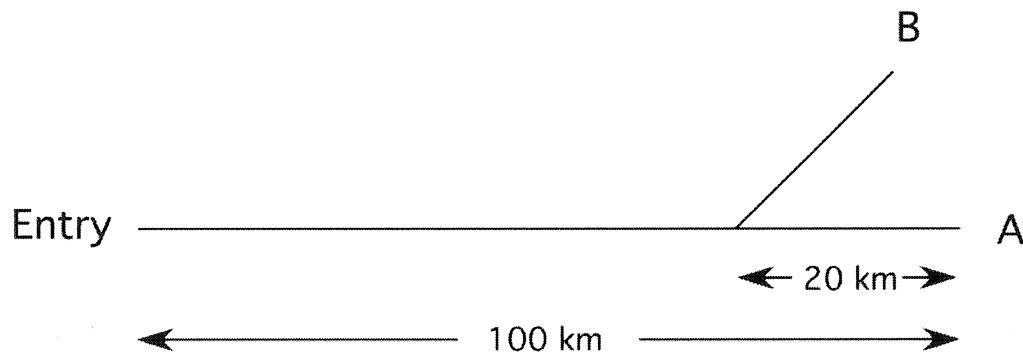
$$\frac{P_2^2 - P_1^2}{2(RT/M)} + \left(\frac{G}{A}\right)^2 \ln\left(\frac{P_1}{P_2}\right) + \frac{2fL}{D} \left(\frac{G}{A}\right)^2 = 0$$

where all symbols have their usual meaning. You may ignore the kinetic energy term when using this equation to calculate pressure. Otherwise, you should retain the kinetic energy term.

*(Question 6 continues on next page)*

**Question 6 (continued)**

Natural gas flows through a pipeline 100 km long and 25 cm in diameter to a receiving station A. At a point 20 km before A, a branch leads off from the main pipeline and runs to a receiving station B. The pressure at the beginning of the pipeline is 1000 kPa, the pressure at station A is 400 kPa, and the mass flow rate entering station A is 0.75 kg/s. The Fanning friction factor for all pipes is  $f = 0.005$ . Assume that the flow is isothermal at 30°C. Ignore energy losses at the branch point.



Gram molecular weight of natural gas

16

Gas constant R

 $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ 

- a) Calculate the velocity of the gas entering station A (5 marks)
- b) Calculate the pressure where the pipe branches (5 marks)
- c) Calculate the mass flow rate of gas entering the main pipeline (4 marks)
- d) Calculate the mass flow rate of gas entering station B (2 marks)

**(Total for Question 6 = 16 marks)**



**Question 7**

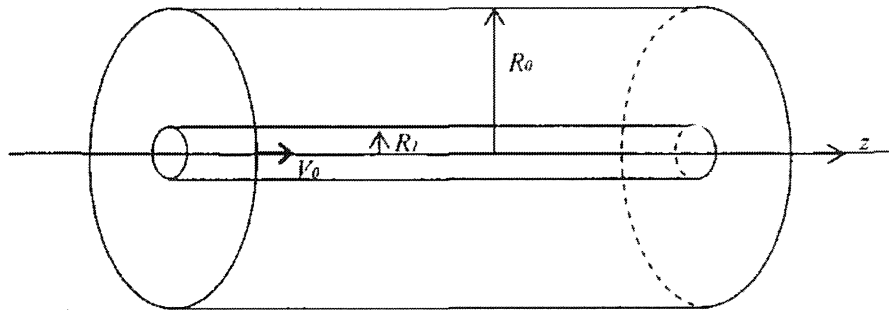
- (a) Define the modified Froude number for stirred tanks, stating the meaning of each symbol used. **(2 marks)**
- (b) The Froude number can be interpreted as the ratio of which two forces? **(1 mark)**
- (c) Under what conditions is the modified Froude number important in stirred tanks? **(1 mark)**
- (d) Describe the type of flow produced in a stirred tank by using (i) a flat blade turbine and (ii) a propeller. Draw a sketch for each case to illustrate the flow pattern. **(4 marks)**

**(Total for Question 7 = 8 marks)**

*QUESTION 8 IS ON THE NEXT PAGE*

**Question 8**

An incompressible Newtonian fluid flows steadily between two infinitely long, concentric cylinders having radii  $R_0$  and  $R_1$  as shown in the diagram. The outer cylinder is fixed, but the inner cylinder moves with an axial velocity  $V_0$ . The fluid is also being driven in the  $z$ -direction due to a constant applied pressure gradient  $\frac{\partial p}{\partial z} = -B$ . The flow is steady and axially symmetric, with flow directed only in the  $z$ -direction.



- a) Show that the axial velocity  $v_z$  is only a function of the radius  $r$

(2 marks)

- b) Find an expression for the velocity profile of the liquid in the annular region.

(6 marks)

- c) Hence find an expression for the volumetric flow rate when  $B = 0$ .

(8 marks)

(Total for Question 8 = 16 marks)

(Total for paper = 110 marks)

Table 2, Temperature Saturation

**Saturated Water & Steam**

Temperatures from 1 to 120 °C

°C	kN/m <sup>2</sup>	m <sup>3</sup> /kg	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg	kJ/kg	kJ/kg	kJ/kg K	kJ/kg K	kJ/kg K	°C
<i>T</i>	<i>p</i>	<i>v<sub>f</sub></i>	<i>v<sub>g</sub></i>	<i>u<sub>f</sub></i>	<i>u<sub>g</sub></i>	<i>h<sub>f</sub></i>	<i>h<sub>fg</sub></i>	<i>h<sub>g</sub></i>	<i>s<sub>f</sub></i>	<i>s<sub>fg</sub></i>	<i>s<sub>g</sub></i>	<i>T</i>
1	0.657	0.001000	192.6	4.174	2376.9	4.174	2499.2	2503.4	0.0153	9.116	9.131	1
2	0.705	0.001000	179.9	8.386	2378.3	8.387	2496.8	2505.2	0.0306	9.074	9.105	2
4	0.813	0.001000	157.3	16.80	2381.1	16.80	2492.1	2508.9	0.0611	8.992	9.053	4
6	0.935	0.001000	137.8	25.21	2383.8	25.21	2487.4	2512.6	0.0913	8.910	9.001	6
8	1.072	0.001000	121.0	33.60	2386.6	33.60	2482.6	2516.2	0.1213	8.830	8.951	8
10	1.227	0.001000	106.4	41.99	2389.3	41.99	2477.9	2519.9	0.1510	8.751	8.902	10
12	1.401	0.001000	93.84	50.38	2392.1	50.38	2473.2	2523.6	0.1805	8.673	8.854	12
14	1.597	0.001001	82.90	58.75	2394.8	58.75	2468.5	2527.2	0.2098	8.596	8.806	14
16	1.817	0.001001	73.38	67.12	2397.6	67.13	2463.8	2530.9	0.2388	8.521	8.759	16
18	2.062	0.001001	65.09	75.49	2400.3	75.50	2459.0	2534.5	0.2677	8.446	8.713	18
20	2.337	0.001002	57.84	83.86	2403.0	83.86	2454.3	2538.2	0.2963	8.372	8.668	20
22	2.642	0.001002	51.49	92.22	2405.8	92.23	2449.6	2541.8	0.3247	8.299	8.624	22
24	2.982	0.001003	45.93	100.6	2408.5	100.6	2444.9	2545.5	0.3530	8.228	8.581	24
26	3.360	0.001003	41.03	108.9	2411.2	108.9	2440.2	2549.1	0.3810	8.157	8.538	26
28	3.778	0.001004	36.73	117.3	2414.0	117.3	2435.4	2552.7	0.4088	8.087	8.496	28
30	4.241	0.001004	32.93	125.7	2416.7	125.7	2430.7	2556.4	0.4365	8.018	8.455	30
32	4.753	0.001005	29.57	134.0	2419.4	134.0	2425.9	2560.0	0.4640	7.950	8.414	32
34	5.318	0.001006	26.60	142.4	2422.1	142.4	2421.2	2563.6	0.4913	7.883	8.374	34
36	5.940	0.001006	23.97	150.7	2424.8	150.7	2416.4	2567.2	0.5184	7.816	8.335	36
38	6.624	0.001007	21.63	159.1	2427.5	159.1	2411.7	2570.8	0.5453	7.751	8.296	38
40	7.375	0.001008	19.55	167.4	2430.2	167.5	2406.9	2574.4	0.5721	7.686	8.258	40
42	8.198	0.001009	17.69	175.8	2432.9	175.8	2402.1	2577.9	0.5987	7.622	8.221	42
44	9.100	0.001009	16.04	184.2	2435.6	184.2	2397.3	2581.5	0.6252	7.559	8.184	44
46	10.09	0.001010	14.56	192.5	2438.3	192.5	2392.5	2585.1	0.6514	7.497	8.148	46
48	11.16	0.001011	13.23	200.9	2440.9	200.9	2387.7	2588.6	0.6776	7.435	8.113	48
50	12.34	0.001012	12.05	209.2	2443.6	209.3	2382.9	2592.2	0.7035	7.374	8.078	50
52	13.61	0.001013	10.98	217.6	2446.2	217.6	2378.1	2595.7	0.7293	7.314	8.043	52
54	15.00	0.001014	10.02	226.0	2448.9	226.0	2373.2	2599.2	0.7550	7.254	8.009	54
56	16.51	0.001015	9.159	234.3	2451.5	234.4	2368.4	2602.7	0.7804	7.195	7.976	56
58	18.15	0.001016	8.381	242.7	2454.1	242.7	2363.5	2606.2	0.8058	7.137	7.943	58
60	19.92	0.001017	7.679	251.1	2456.8	251.1	2358.6	2609.7	0.8310	7.080	7.911	60
62	21.84	0.001018	7.044	259.4	2459.4	259.5	2353.7	2613.2	0.8560	7.023	7.879	62
64	23.91	0.001019	6.469	267.8	2462.0	267.8	2348.8	2616.6	0.8809	6.967	7.848	64
66	26.15	0.001020	5.948	276.2	2464.5	276.2	2343.9	2620.1	0.9057	6.911	7.817	66
68	28.56	0.001022	5.476	284.6	2467.1	284.6	2338.9	2623.5	0.9303	6.856	7.786	68
70	31.16	0.001023	5.046	292.9	2469.7	293.0	2334.0	2626.9	0.9548	6.802	7.756	70
72	33.96	0.001024	4.656	301.3	2472.2	301.4	2329.0	2630.3	0.9792	6.748	7.727	72
74	36.96	0.001025	4.300	309.7	2474.8	309.7	2324.0	2633.7	1.003	6.695	7.698	74
76	40.19	0.001027	3.976	318.1	2477.3	318.1	2318.9	2637.1	1.027	6.642	7.669	76
78	43.65	0.001028	3.680	326.5	2479.8	326.5	2313.9	2640.4	1.051	6.590	7.641	78
80	47.36	0.001029	3.409	334.9	2482.3	334.9	2308.8	2643.8	1.075	6.538	7.613	80
82	51.33	0.001031	3.162	343.3	2484.8	343.3	2303.8	2647.1	1.099	6.487	7.586	82
84	55.57	0.001032	2.935	351.7	2487.3	351.7	2298.6	2650.4	1.123	6.436	7.559	84
86	60.11	0.001033	2.727	360.1	2489.7	360.1	2293.5	2653.6	1.146	6.386	7.532	86
88	64.95	0.001035	2.536	368.5	2492.2	368.5	2288.4	2656.9	1.169	6.336	7.506	88
90	70.11	0.001036	2.361	376.9	2494.6	376.9	2283.2	2660.1	1.193	6.287	7.480	90
92	75.61	0.001038	2.200	385.3	2497.0	385.4	2278.0	2663.4	1.216	6.239	7.454	92
94	81.46	0.001039	2.052	393.7	2499.4	393.8	2272.8	2666.6	1.239	6.190	7.429	94
96	87.69	0.001041	1.915	402.1	2501.8	402.2	2267.5	2669.7	1.261	6.143	7.404	96
98	94.30	0.001042	1.789	410.5	2504.1	410.6	2262.2	2672.9	1.284	6.095	7.380	98
100	101.3	0.001044	1.673	419.0	2506.5	419.1	2256.9	2676.0	1.307	6.049	7.355	100
105	120.8	0.001048	1.419	440.0	2512.3	440.2	2243.6	2683.7	1.363	5.933	7.296	105
110	143.3	0.001052	1.210	461.2	2518.0	461.3	2230.0	2691.3	1.418	5.820	7.239	110
115	169.1	0.001056	1.036	482.3	2523.5	482.5	2216.2	2698.7	1.473	5.710	7.183	115
120	198.5	0.001061	0.892	503.5	2529.0	503.7	2202.2	2706.0	1.528	5.602	7.129	120

		MN/m <sup>2</sup>																								
		<i>p</i>	0.001	0.01	0.02	0.05	0.1	0.5	1	2	4	6	8	10	15	20	25	30	35	40	45	50	60	80	100	<i>p</i>
°C	<i>T</i>																									<i>T</i>
0	999.8	999.8	999.8	999.8	999.8	999.8	1000	1000	1001	1002	1003	1004	1005	1007	1010	1012	1014	1017	1019	1022	1024	1028	1037	1046	0	
5	999.9	999.8	999.8	999.8	999.8	999.8	1000	1000	1001	1002	1003	1004	1005	1007	1009	1012	1014	1016	1019	1021	1023	1028	1036	1044	5	
10	0.00766	999.8	999.8	999.8	999.8	999.8	1000	1000	1001	1002	1003	1004	1004	1007	1009	1011	1014	1016	1018	1020	1022	1027	1035	1043	10	
20	0.00739	998.3	998.3	998.3	998.3	998.5	998.7	999.2	1000	1001	1002	1003	1005	1007	1009	1012	1014	1016	1018	1020	1024	1032	1040	20		
25	0.00727	997.0	997.0	997.0	997.0	997.2	997.4	997.9	998.8	999.7	1001	1001	1004	1006	1008	1010	1012	1014	1016	1018	1022	1030	1038	25		
30	0.00715	995.7	995.7	995.7	995.8	995.9	996.2	996.6	997.5	998.4	999.2	1000	1002	1004	1007	1009	1011	1013	1015	1017	1021	1029	1036	30		
40	0.00692	992.3	992.3	992.3	992.3	992.5	992.7	993.1	994.0	994.9	995.7	996.6	998.7	1001	1003	1005	1007	1009	1011	1013	1017	1025	1032	40		
50	0.00671	0.0673	988.0	988.0	988.1	988.2	988.5	988.9	989.8	990.6	991.5	992.4	994.5	996.6	998.7	1001	1003	1005	1007	1009	1013	1020	1027	50		
60	0.00651	0.0652	981.9	983.2	983.2	983.4	983.6	984.0	984.9	985.8	986.6	987.5	989.6	991.8	993.8	995.9	997.9	999.9	1002	1004	1008	1015	1023	60		
70	0.00632	0.0633	0.1269	977.7	977.7	977.9	978.1	978.5	979.4	980.3	981.2	982.1	984.2	986.4	988.5	990.6	992.6	994.7	996.7	998.6	1003	1010	1017	70		
80	0.00614	0.0615	0.1232	971.6	971.7	971.8	972.1	972.5	973.4	974.3	975.2	976.1	978.3	980.5	982.7	984.8	986.9	988.9	990.9	993.0	996.9	1005	1012	80		
90	0.00597	0.0598	0.1197	0.301	965.1	965.3	965.5	966.0	966.9	967.9	968.8	969.7	972.0	974.2	976.4	978.5	980.7	982.8	984.8	986.9	990.9	998.7	1006	90		
100	0.00581	0.0582	0.1165	0.293	0.590	958.3	958.6	959.0	960.0	960.9	961.9	962.8	965.1	967.4	969.7	971.9	974.1	976.2	978.3	980.4	984.5	992.5	1000	100		
125	0.00544	0.0545	0.1091	0.274	0.550	938.8	939.1	939.6	940.6	941.7	942.7	943.7	946.2	948.7	951.1	953.5	955.9	958.2	960.4	962.7	967.0	975.5	983.5	125		
150	0.00512	0.0512	0.1026	0.257	0.516	916.8	917.1	917.7	918.8	920.0	921.1	922.2	925.0	927.7	930.4	933.0	935.6	938.1	940.5	943.0	947.7	956.7	965.3	150		
175	0.00484	0.0484	0.0968	0.243	0.487	2.504	892.1	892.8	894.1	895.4	896.7	898.0	901.1	904.2	907.2	910.1	912.9	915.7	918.4	921.1	926.3	936.2	945.5	175		
200	0.00458	0.0458	0.0917	0.230	0.460	2.353	4.856	865.0	866.6	868.1	869.6	871.1	874.7	878.2	881.6	884.9	888.1	891.3	894.3	897.3	903.1	914.0	924.1	200		
225	0.00435	0.0435	0.0871	0.218	0.437	2.223	4.554	9.643	835.1	837.0	838.8	840.6	844.9	849.0	853.0	856.9	860.6	864.3	867.8	871.2	877.7	889.9	901.1	225		
250	0.00414	0.0414	0.0829	0.207	0.416	2.108	4.296	8.973	799.2	801.5	803.8	806.1	811.4	816.5	821.3	826.0	830.4	834.7	838.8	842.7	850.3	864.1	876.6	250		
275	0.00395	0.0395	0.0791	0.198	0.396	2.006	4.073	8.429	18.34	759.3	762.2	765.2	772.3	778.9	785.1	790.9	796.4	801.6	806.6	811.3	820.2	836.2	850.4	275		
300	0.00378	0.0378	0.0756	0.189	0.379	1.914	3.876	7.968	17.00	27.67	41.21	715.4	725.7	735.0	743.3	751.0	758.1	764.7	770.9	776.7	787.5	806.4	822.7	300		
325	0.00362	0.0362	0.0725	0.181	0.363	1.830	3.700	7.569	15.94	25.42	36.54	50.40	663.6	679.0	691.8	703.0	712.9	721.8	729.9	737.5	751.0	773.9	792.9	325		
350	0.00348	0.0348	0.0696	0.174	0.348	1.754	3.541	7.217	15.05	23.68	33.39	44.60	87.24	600.1	625.0	643.5	658.6	671.4	682.6	692.6	710.0	738.1	760.6	350		
375	0.00334	0.0334	0.0669	0.167	0.335	1.685	3.396	6.902	14.29	22.29	31.04	40.76	72.04	132.0	488.7	555.4	586.5	608.5	625.9	640.4	664.2	699.7	726.5	375		
400	0.00322	0.0322	0.0644	0.161	0.322	1.620	3.263	6.617	13.63	21.11	29.15	37.87	63.85	100.5	166.3	353.3	473.8	523.8	555.1	578.3	612.6	658.8	691.4	400		
425	0.00310	0.0310	0.0621	0.155	0.311	1.561	3.141	6.357	13.04	20.09	27.57	35.55	58.37	87.21	127.0	189.3	292.3	390.6	455.0	497.2	551.1	613.6	653.9	425		
450	0.00300	0.0300	0.0599	0.150	0.300	1.506	3.028	6.119	12.51	19.19	26.22	33.62	54.20	78.70	109.0	148.5	201.8	272.1	343.2	401.3	479.9	564.3	613.9	450		
475	0.00290	0.0290	0.0579	0.145	0.290	1.455	2.923	5.900	12.02	18.39	25.03	31.97	50.87	72.54	97.92	128.3	165.4	210.5	262.9	315.9	403.9	510.8	571.2	475		
500	0.00280	0.0280	0.0561	0.140	0.280	1.407	2.825	5.696	11.58	17.67	23.98	30.53	48.09	67.70	89.86	115.2	144.4	178.1	216.2	257.6	338.8	457.0	528.2	500		
550	0.00263	0.0263	0.0527	0.132	0.263	1.320	2.649	5.331	10.80	16.41	22.17	28.09	43.65	60.43	78.61	98.37	119.9	143.2	168.5	195.6	253.3	361.8	445.3	550		
600	0.00248	0.0248	0.0496	0.124	0.248	1.244	2.494	5.012	10.13	15.34	20.66	26.10	40.19	55.06	70.79	87.44	105.0	123.6	143.2	163.6	206.8	295.9	374.8	600		
650	0.00235	0.0235	0.0469	0.117	0.235	1.176	2.356	4.731	9.537	14.42	19.38	24.41	37.36	50.83	64.87	79.48	94.68	110.5	126.8	143.7	178.7	251.6	322.0	650		
700	0.00223	0.0223	0.0445	0.111	0.223	1.115	2.233	4.481	9.017	13.61	18.26	22.96	34.98	47.37	60.13	73.28	86.80	100.7	115.0	129.5	159.5	221.3	282.8	700		
750	0.00212	0.0212	0.0424	0.106	0.212	1.060	2.123	4.256	8.555	12.89	17.28	21.70	32.94	44.45	56.21	68.24	80.52	93.04	105.8	118.8	145.2	199.3	253.0	750		
800	0.00202	0.0202	0.0404	0.101	0.202	1.011	2.023	4.054	8.140	12.26	16.41	20.58	31.17	41.94	52.89	64.03	75.33	86.80	98.42	110.2	134.0	182.5	230.4	800		
<i>T<sub>sat</sub></i>	6.98	45.83	60.09	81.35	99.63	151.8	179.9	212.4	250.3	275.5	295.0	311.0	342.1	365.7												
<i>ρ<sub>f</sub></i>	999.9	989.9	983.1	970.8	958.4	915.0	887.0	849.9	798.7	758.3	722.4	688.4	603.2	490.9												
<i>ρ<sub>g</sub></i>	0.00774	0.0681	0.1307	0.309	0.590	2.669	5.147	10.05	20.10	30.83	42.51	55.43	96.71	170.2												

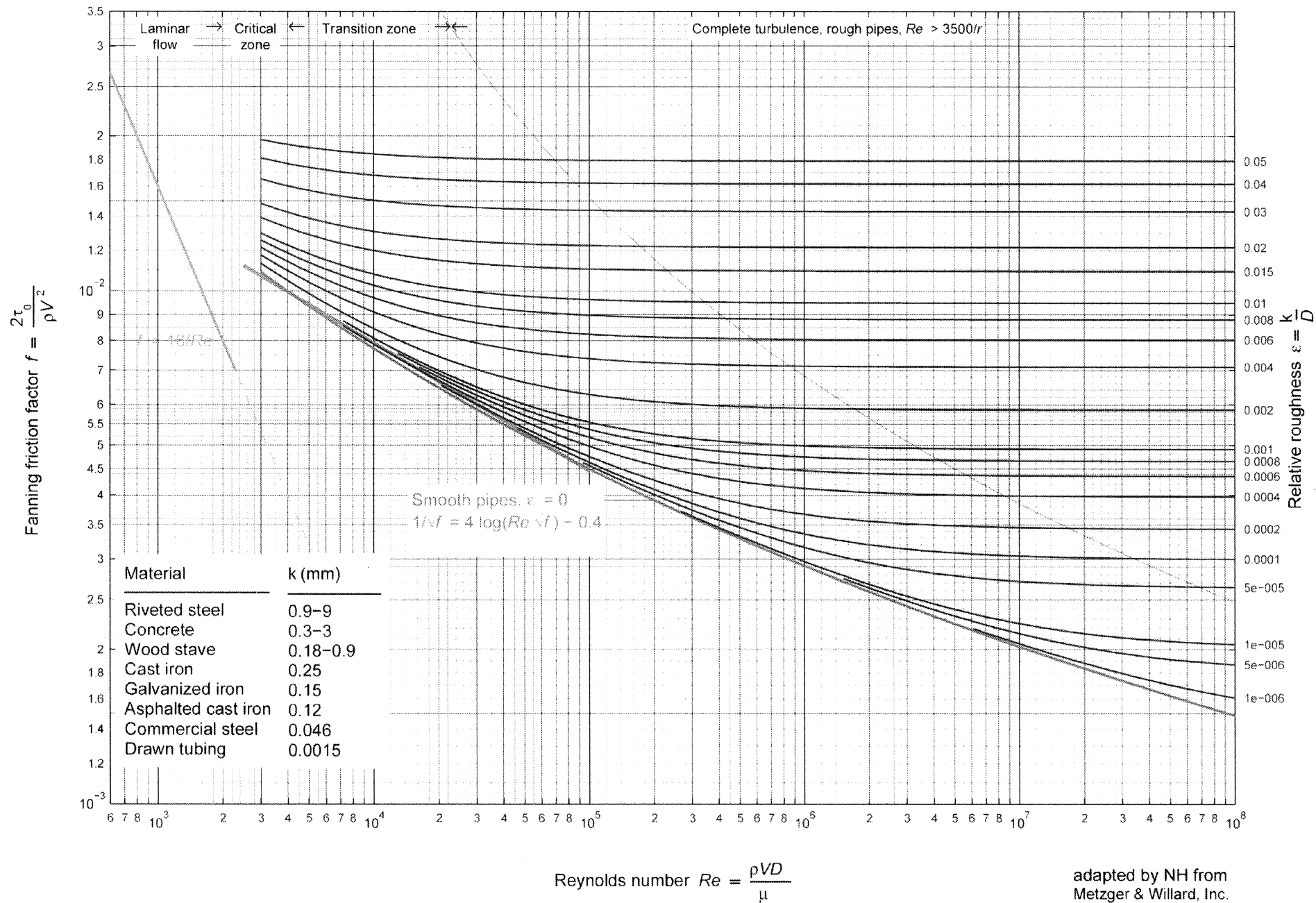
*Table 6. Density*

		MN/m <sup>2</sup>																								
		p	0.001	0.01	0.02	0.05	0.1	0.5	1	2	4	6	8	10	15	20	25	30	35	40	45	50	60	80	100	p
°C	T																								T	
0	0	0.042	0.042	0.043	0.043	0.044	0.054	0.065	0.088	0.131	0.173	0.213	0.250	0.336	0.409	0.469	0.517	0.553	0.577	0.590	0.592	0.571	0.454	0.324	0	
5	5	21.02	21.02	21.02	21.02	21.02	21.02	21.02	21.02	21.01	21.01	21.01	21.00	20.98	20.95	20.91	20.86	20.81	20.74	20.67	20.58	20.40	19.96	19.50	5	
10	10	2389	41.99	41.99	41.99	41.99	41.98	41.97	41.95	41.90	41.85	41.80	41.75	41.62	41.49	41.35	41.21	41.06	40.90	40.74	40.57	40.22	39.47	38.68	10	
20	20	2403	83.86	83.86	83.86	83.85	83.83	83.80	83.74	83.62	83.50	83.38	83.26	82.96	82.66	82.36	82.06	81.77	81.47	81.17	80.87	80.27	79.05	77.83	20	
25	25	2410	104.8	104.8	104.8	104.8	104.7	104.7	104.6	104.5	104.3	104.2	104.0	103.6	103.3	102.9	102.5	102.2	101.8	101.4	101.1	100.4	98.96	97.56	25	
30	30	2417	125.7	125.7	125.7	125.7	125.6	125.6	125.5	125.3	125.1	124.9	124.7	124.3	123.9	123.4	123.0	122.6	122.1	121.7	121.3	120.5	118.9	117.3	30	
40	40	2431	167.4	167.4	167.4	167.4	167.3	167.2	167.0	166.7	166.5	166.2	165.7	165.1	164.5	164.0	163.4	162.9	162.3	161.8	160.8	158.8	156.9	156.9	40	
50	50	2445	2444	209.2	209.2	209.2	209.2	209.1	208.9	208.6	208.3	208.1	207.8	207.0	206.3	205.7	205.0	204.3	203.7	203.0	202.4	201.1	198.8	196.5	50	
60	60	2460	2458	251.1	251.1	251.1	251.0	250.9	250.7	250.4	250.0	249.7	249.3	248.5	247.6	246.8	246.0	245.2	244.5	243.7	243.0	241.5	238.8	236.2	60	
70	70	2474	2473	2471	292.9	292.9	292.8	292.7	292.5	292.1	291.7	291.3	290.9	289.9	289.0	288.0	287.1	286.2	285.3	284.5	283.6	282.0	278.8	275.9	70	
80	80	2488	2487	2486	334.9	334.9	334.8	334.6	334.4	333.9	333.5	333.0	332.6	331.5	330.4	329.3	328.3	327.2	326.2	325.3	324.3	322.4	318.9	315.6	80	
90	90	2502	2501	2500	2497	376.9	376.8	376.6	376.4	375.8	375.3	374.8	374.3	373.1	371.8	370.6	369.5	368.3	367.2	366.1	365.0	362.9	359.0	355.3	90	
100	100	2516	2516	2515	2512	2507	418.8	418.7	418.4	417.8	417.2	416.7	416.1	414.7	413.4	412.1	410.8	409.5	408.2	407.0	405.8	403.5	399.1	395.1	100	
125	125	2552	2552	2551	2549	2545	524.7	524.5	524.1	523.4	522.6	521.9	521.2	519.4	517.7	516.0	514.4	512.8	511.2	509.6	508.1	505.2	499.7	494.6	125	
150	150	2588	2588	2587	2586	2583	631.6	631.4	630.9	630.0	629.1	628.2	627.3	625.0	622.9	620.8	618.7	616.8	614.8	612.9	611.0	607.4	600.7	594.4	150	
175	175	2625	2625	2624	2623	2620	740.1	739.5	738.3	737.1	736.0	734.9	732.1	729.4	726.8	724.3	721.8	719.4	717.1	714.8	710.4	702.2	694.6	694.6	175	
200	200	2662	2661	2661	2660	2658	850.2	848.8	847.3	845.9	844.4	841.0	837.7	834.4	831.3	828.3	825.3	822.5	819.7	814.3	804.4	795.3	795.3	200		
225	225	2699	2699	2698	2697	2696	962.5	960.6	958.8	957.0	952.6	948.4	944.3	940.4	936.6	933.0	929.5	926.1	919.5	907.5	896.7	896.7	225			
250	250	2736	2736	2736	2735	2734	1081	1078	1076	1073	1068	1062	1057	1052	1047	1043	1038	1034	1026	1012	998.9	998.9	250			
275	275	2774	2774	2774	2773	2772	1203	1200	1196	1188	1181	1174	1168	1162	1156	1150	1145	1135	1118	1102	1102	275				
300	300	2812	2812	2812	2811	2811	1329	1318	1307	1298	1289	1281	1273	1266	1259	1247	1225	1207	1207	300						
325	325	2851	2851	2851	2850	2849	1464	1464	1447	1432	1419	1407	1397	1387	1378	1362	1335	1313	1313	325						
350	350	2890	2890	2890	2889	2889	1585	1563	1545	1530	1516	1504	1483	1447	1419	1419	350									
375	375	2929	2929	2929	2929	2928	1652	1652	1642	1614	1585	1563	1545	1530	1516	1504	1483	1447	1419	1419	375					
400	400	2969	2969	2969	2969	2968	1814	1739	1703	1677	1656	1639	1610	1567	1534	400										
425	425	3009	3009	3009	3009	3008	1900	1822	1771	1771	425															
450	450	3050	3050	3050	3049	3045	2006	2006	450																	
475	475	3091	3091	3091	3091	3090	2127	2127	475																	
500	500	3132	3132	3132	3132	3132	2369	2369	500																	
550	550	3217	3217	3217	3216	3216	2591	2591	550																	
600	600	3303	3303	3303	3302	3302	2811	2811	600																	
650	650	3390	3390	3390	3390	3390	3027	3027	650																	
700	700	3480	3480	3480	3479	3477	3280	3280	700																	
750	750	3571	3571	3571	3571	3570	3567	3567	750																	
800	800	3663	3663	3663	3663	3663	3662	3662	800																	
T <sub>sat</sub>		6.98	45.83	60.09	81.35	99.63	151.8	179.9	212.4	250.3	275.5	295.0	311.0	342.1	365.7											
u <sub>f</sub>		29.33	191.8	251.4	340.5	417.4	639.6	761.5	906.2	1082	1206	1306	1394	1586	1786											
u <sub>g</sub>		2385	2438	2457	2484	2506	2560	2582	2598	2601	2590	2572	2547	2460	2301											

Specific Internal Energy of Water &amp; Steam kJ/kg

Table 7, Internal Energy

# Moody Diagram



Continuity and Navier-Stokes equations for incompressible homogeneous fluids in Cartesian, cylindrical, and spherical coordinates

Cartesian	Cylindrical	Spherical
Continuity equation		
$\frac{\partial v_x}{\partial x} + \frac{\partial v_y}{\partial y} + \frac{\partial v_z}{\partial z} = 0$	$\frac{1}{r} \frac{\partial(rv_r)}{\partial r} + \frac{1}{r} \left( \frac{\partial v_\theta}{\partial \theta} \right) + \frac{\partial v_z}{\partial z} = 0$	$\frac{1}{r^2} \frac{\partial(r^2 v_r)}{\partial r} + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (v_\theta \sin \theta) + \frac{1}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} = 0$
Navier-Stokes equation		
$\rho \left( \frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right)$ $= -\frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right)$	$\rho \left( \frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta^2}{r} + v_z \frac{\partial v_r}{\partial z} \right)$ $= -\frac{\partial p}{\partial r} + \mu \left[ \frac{\partial}{\partial r} \left( \frac{1}{r} \frac{\partial}{\partial r} (rv_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} + \frac{\partial^2 v_r}{\partial z^2} \right]$	$\rho \left( \frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_r}{\partial \phi} - \frac{v_\theta^2 + v_\phi^2}{r} \right)$ $= -\frac{\partial p}{\partial r} + \mu \left[ \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial v_r}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial v_r}{\partial \theta} \right) \right.$ $\left. + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 v_r}{\partial \phi^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} - \frac{2}{r^2} \frac{\partial v_\phi}{\partial \phi} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \phi} \right]$
$\rho \left( \frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right)$ $= -\frac{\partial p}{\partial y} + \mu \left( \frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right)$	$\rho \left( \frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_z}{r} \frac{\partial v_\theta}{\partial z} + v_r \frac{\partial v_\theta}{\partial r} \right)$ $= -\frac{1}{r} \frac{\partial p}{\partial \theta} + \mu \left[ \frac{\partial}{\partial r} \left( \frac{1}{r} \frac{\partial}{\partial r} (rv_\theta) \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} + \frac{\partial^2 v_\theta}{\partial z^2} \right]$	$\rho \left( \frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_\theta}{\partial \phi} + \frac{v_r v_\phi}{r} + \frac{v_\theta^2 \cot \theta}{r} \right)$ $= -\frac{1}{r \sin \theta} \frac{\partial p}{\partial \theta} + \mu \left[ \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial v_\theta}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial v_\theta}{\partial \theta} \right) \right.$ $\left. + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 v_\theta}{\partial \phi^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} - \frac{v_\theta}{r^2 \sin^2 \theta} - \frac{2 \cos \theta}{r^2 \sin^2 \theta} \frac{\partial v_\phi}{\partial \phi} \right]$
$\rho \left( \frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right)$ $= -\frac{\partial p}{\partial z} + \mu \left( \frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right)$	$\rho \left( \frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right)$ $= -\frac{\partial p}{\partial z} + \mu \left[ \frac{1}{r} \frac{\partial}{\partial r} \left( \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right]$	$\rho \left( \frac{\partial v_\phi}{\partial t} + v_r \frac{\partial v_\phi}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\phi}{\partial \theta} + \frac{v_\phi}{r \sin \theta} \frac{\partial v_\phi}{\partial \phi} + \frac{v_r v_\phi}{r} + \frac{v_\theta v_\phi \cot \theta}{r} \right)$ $= -\frac{1}{r \sin \theta} \frac{\partial p}{\partial \phi} + \mu \left[ \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial v_\phi}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left( \sin \theta \frac{\partial v_\phi}{\partial \theta} \right) \right.$ $\left. + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 v_\phi}{\partial \phi^2} - \frac{v_\phi}{r^2 \sin^2 \theta} + \frac{2}{r^2 \sin \theta} \frac{\partial v_r}{\partial \phi} + \frac{2 \cos \theta}{r^2 \sin^2 \theta} \frac{\partial v_\theta}{\partial \phi} \right]$



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