1) Momentum equation

$$F = P \omega A_2 V_2^2$$

$$70 = 1000 \times \Pi \times 0.03^2 \times V_2^2$$

$$V_2 = 9.95 \text{ m/s}$$

continuity
$$A_1V_1 = A_2V_2$$

$$A|XO \cdot 1^{2} \times V_{1} = A|XO \cdot 0^{3} \times 9.95$$

$$V_{1} = 0.03^{2} \times 9.95$$

$$= 0.896 \text{m/s}$$

MEB between 1 and 2

$$\frac{\Delta P}{P} + 902 + \Delta V^{2} + Ws + F = 0$$

$$\frac{\Delta P}{P} = \frac{1}{2}(V_{1}^{2} - V_{2}^{2})$$

$$P_{2} - P_{1} = \frac{1}{2}(0.896^{2} - 995^{2}) \times 1000$$

$$P_{1} = 101325 + 49100$$

$$= 150.425 KPa$$

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2) height of spill way.

assume factionless bump

$$\frac{Q^{2}}{29b^{2}(4)^{2}} + 4 = \frac{Q^{2}}{29b^{2}(0.6)^{2}} + 0.6$$

$$\frac{9^2}{2\times9.81\times16} + 4 = \frac{9^2}{2\times9.8\times0.36} + 0.6$$

$$0.139 \ 9^{2} = 3.4$$

$$9^{2} = 3.4$$

$$0.139$$

$$9 = \sqrt{\frac{3.4}{0.139}}$$

$$hcnt = \left(\frac{q^2}{9.8}\right)^{1/3}$$

$$h bump = 4 - 1.36$$

= 2.64 m

$$= \frac{200}{1000} \times 1$$
 m³/s

$$hf_1 = hf_2 = hf_3$$
.

$$\frac{2xf_{F}x_{2}xV_{1}^{2}}{p_{1}} = \frac{2xf_{F}x_{2}xV_{2}^{2}}{p_{2}} = 2xf_{F}x_{2}xV_{3}^{2}$$

D1=b3 same, thus ff and Valso same. assume ff constant for all pipes.

$$\frac{2 \times \{F \times 2 \times Q_1^2 = 2 \times \frac{F \times 2 \times Q_2^2}{p_2^5 \Pi^2}}{(p_1)^5 \Pi^2} = \frac{2 \times \frac{F \times 2 \times Q_2^2}{p_2^5 \Pi^2}}{(24)^5}$$

$$\frac{Q_1^2}{(18)^6} = \frac{Q_2^2}{(24)^6}$$

$$Q_1 = \left(\frac{18}{24}\right)^{5/2} Q_2$$

$$Q_1 + Q_2 + Q_3 = Q$$
 total

$$\left(2 \times \left(\frac{18}{24}\right)^{5/2} + 1\right) Q_2 = 0 \cot 1$$

$$Q_2 = 1.69 \text{ m}^3/\text{s}.$$

$$= 101.3 \text{ L/min}$$

$$Q_1 = Q_3 = \left(\frac{10}{24}\right)^{5/2} \times 101.3$$

= 49.35 L/M/N/A

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4) (1)
$$\int_{x \in I} \int_{x=h}^{\infty} \int_{x=h}^{\infty} b \cdot C$$

$$\frac{dV_z}{dx} = 0 \quad \text{(b)}$$

Vz(x=0) = Wbelt.

using equation of motion in the z-component.

$$\frac{\partial^2 V_z}{\partial x^2} = \frac{\partial^2 V_z}{\partial x^2}$$

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using B.C (1), $C_1 = -\rho g_2 h$

$$\frac{\partial Vz}{\partial x} = \frac{\rho g_z}{\nu} (x-h).$$

$$Vz(x) = \frac{\rho g_z(x^2 - hx) + c_2}{\nu}$$

at z=0, Vz=Wbelt

$$V_z(x) = \frac{\rho g_z}{N} \left(\frac{x^2}{2} - hx \right) + \text{Wbelt}$$

no ner flow

$$\int_{0}^{h} V_{z}(x) dx = 0$$

$$\int_{0}^{h} P_{z}(x^{2}/2 - hx) dx + \int_{0}^{h} Wbelt dx = 0.$$

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$$V_2(x) = \frac{\rho g_2}{\nu} \left(\frac{x^2}{2} - hx + \frac{h^2}{3} \right)$$

- 6 (a) diagphragm pump avoid cornsion of the pump by liquid
 - (b) penstalhopump -> biological isolation.
 - (c) Cavitanon = bubbles form inside pump and cause physical damage

(d).
$$\Delta z = -WS/9$$

= hp
= ISM.

heads is mofwater

- (e) (1) 0010, 0011, 0012, 0013,0014
 - (ii) 0013
 - (iii) 31.5 L/min
 - (iv) use throttling valve that A system head and will & as Frichan term increases.

Find By

$$\frac{P_{J^{2}} - (\Omega 0 \times 10^{3})^{2}}{2 \times 8 \cdot 3 \cdot 4 \times 298} + 2 \times \frac{2 \times 500 \times 0.005}{0.15} \times \left(\frac{1.5}{11 \times 0.15^{2}}\right)^{2} = 0$$

$$P_{J} = 432856 Pa$$

Find 62

$$\frac{432826^{2} - (480 \times 10^{3})^{2}}{2 \times 8314 \times 298} + 6^{2} \times 2 \times 300 \times 0.005} = 0$$

$$\frac{19 \times 10^{-3}}{6^{2}} = 0.906 \text{ kg}^{2}/\text{s}^{2}$$

Find PR

$$\frac{10 \times 10^{-3}}{5 \times 9 \cdot 314 \times 500} + 5 \cdot 42 \times 5 \times 100 \times 0.002 = 0$$

$$P_R = \frac{P_R}{RT/M} = \frac{345120}{8314 \times 298} = 2.65 \text{ kg/m}^3$$

$$\frac{G}{P_R A} = V_R$$

$$V_{R} = \frac{2.45}{9.000} = 52.4 \frac{1}{1}$$