

# Distributionally Robust Co-Optimization of Energy and Reserve Dispatch of Integrated Electricity and Heat System - Online Appendix

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## NOMENCLATURE

### A. Indexes and Sets

$n$	Index of nodes
$l$	Index of thermal loads
$s$	Index of heat stations
$p$	Index of pipes
$\Lambda^N$	Set of nodes
$\Lambda^P$	Set of pipes
$\Lambda^{N-}$	Set of nodes with a single pipe ending
$\Lambda^{N+}$	Set of nodes with a single pipe starting
$\Theta_n^{HS}$	Set of heat sources (HS) at node $n$
$\Theta_n^{CHP}$	Set of CHPs at node $n$ , $\Theta_n^{CHP} \in \Theta_n^{HS}$
$\Theta_n^{HP}$	Set of heat pumps at node $n$ , $\Theta_n^{HP} \in \Theta_n^{HS}$
$\Theta_n^{HL}$	Set of heat demands at node $n$
$\Theta_n^{P,OUT}$	Set of indices of pipes starting at node $n$
$\Theta_n^{P,IN}$	Set of indices of pipes ending at node $n$

### B. Parameters

$\underline{P}^G, \bar{P}^G$	Vector of the minimum and maximum real power output of generators [MW]
$\underline{P}^{CHP}, \bar{P}^{CHP}$	Vector of the minimum and maximum power supply from CHP unit [MW]
$\bar{R}^G$	Vector of the generators reserve limits [MW]
$\bar{R}^{CHP}$	Vector of the CHP reserve limits [MW]
$P_W^f$	Wind power forecast vector [MW]
$P^D$	Electric demand vector [MW]
$P^l$	Line transmission capacity vector [MW]
$\underline{H}_s^{HS}, \bar{H}_s^{HS}$	Minimum and maximum heat supply from HS unit [MW]
$H_l^L$	Heat demand [MW]
$c_2, c_1, c_0$	Cost coefficients of generators [\$/MWh]
$c_e, c_h$	Cost coefficients for CHP [\$/MWh]
$\bar{c}_G, \underline{c}_G$	Cost coefficients of generators for providing reserves [\$/MWh]
$\bar{c}_c, \underline{c}_c$	Cost coefficients of CHP for providing reserves [\$/MWh]

$\rho_s^H, \rho_s^E$

Heat/Electricity-to-fuel ratio of the extraction CHP

$\rho_s$

Heat-to-Electricity output ratio of the extraction CHP

$\eta^{WP}$

Water pump efficiency

$COP_s$

Coefficient of performance of the heat pump

$\bar{F}_s$

Maximum fuel consumption of CHP unit [MW]

$\underline{P}_s^{WP}, \bar{P}_s^{WP}$

Technical limits of the water pump at the heat station

$\underline{m}_p^S, \bar{m}_p^S$

Lower and upper limits of mass flow rate of the pipeline  $p$  in supply network [kg/s]

$\underline{m}_p^R, \bar{m}_p^R$

Lower and upper limit of mass flow rate of the pipeline  $p$  in return network [kg/s]

$\underline{m}_s^{HS}, \bar{m}_s^{HS}$

Lower and upper limit of mass flow rate of the HS  $s$  [kg/s]

$\underline{m}_l^{HL}, \bar{m}_l^{HL}$

Lower and upper limit of mass flow rate of the heat load  $l$  [kg/s]

$\underline{T}_n^S, \bar{T}_n^S$

Minimum/maximum temperature at node  $n$  in the supply network [°C]

$\underline{T}_n^R, \bar{T}_n^R$

Minimum/maximum temperature at node  $n$  in the return network [°C]

$\underline{T}_p^S, \bar{T}_p^S$

Minimum/maximum temperature at pipe  $p$  in the supply network [°C]

$\underline{T}_p^R, \bar{T}_p^R$

Minimum/maximum temperature at pipe  $p$  in the return network [°C]

$\underline{pr}_n^S, \bar{pr}_n^S$

Minimum/maximum pressure at node  $n$  in the supply network [kPa]

$\underline{pr}_n^R, \bar{pr}_n^R$

Minimum/maximum pressure at node  $n$  in the return network [kPa]

$\underline{pr}_l^{HL}$

Minimum pressure difference at the heat load [kPa]

$C_p$

Specific water capacity [J/kg°C]

$\lambda$

Heat transfer coefficient per unit length [W/m°C] [MW]

$K_p$

Pipe resistance coefficient [ $m^{-1}kg^{-1}$ ]

$L_p$

Length of pipe  $p$  [m]

$D_p$	Diameter of a pipe $p$ [m]
$\nu_p$	Absolute roughness of a pipe $p$ [m]

### C. Decision Variables

$m_p^S, m_p^R$	Mass flow rate of pipeline $p$ [kg/s]
$m_s^{HS}$	Mass flow rate of HS $s$ [kg/s]
$m_l^{HL}$	Mass flow rate of heat load $l$ [kg/s]
$T_p^{S,start}$	Temperature at the start node of pipe $p$ in the supply network [°C]
$T_p^{S,end}$	Temperature at the end node of pipe $p$ in the supply network [°C]
$T_p^{R,start}$	Temperature at the start node of pipe $p$ in the return network [°C]
$T_p^{R,end}$	Temperature at the end node of pipe $p$ in the return network [°C]
$T_n^S$	Temperature of node $n$ in the supply network [°C]
$T_n^R$	Temperature of node $n$ in the return network [°C]
$H_s^{HS}$	Heat supply from HS unit $s$
$P^{CHP}$	Day-ahead power dispatch from CHP unit [MW]
$P^G$	Day-ahead power dispatch of generators [MW]
$P_s^{HP}$	Power consumption of heat pump [MW]
$P_s^{WP}$	Power consumption of circulation pump [MW]
$R^{up/dn}$	Upward/Downward reserves for the generators [MW]
$R^{uc/dc}$	Upward/Downward reserve for the CHPs [MW]
$Y$	Generation participation factor

**Notation:** Index denotes an element of the vector with the corresponding dimension.

### DISTRIBUTIONALLY ROBUST REFORMULATION

Stochastic constraints that involve random variable could be written as one-side chance-constraints

$$\mathbb{P}(A[C(P+R) + C_W(P^f + \Delta W) - C_D P^D - C_p P^{WP} - C_{HP} P^{HP}] \geq -P^l) \geq 1 - \epsilon$$

$$\mathbb{P}(A[C(P+R) + C_W(P^f + \Delta W) - C_D P^D - C_p P^{WP} - C_{HP} P^{HP}] \leq P^l) \geq 1 - \epsilon$$

$$\mathbb{P}(P + R \geq \underline{P}) \geq 1 - \epsilon$$

$$\mathbb{P}(P + R \leq \overline{P}) \geq 1 - \epsilon$$

$$\mathbb{P}(R \leq RT^{up}) \geq 1 - \epsilon$$

$$\mathbb{P}(R \geq -RT^{dn}) \geq 1 - \epsilon$$

where  $\epsilon$  - is the violation probability. By substituting  $R = -Y \sum_w \Delta W_w$  and the summation into  $\sum_w = \mathbf{1}_{1 \times N_W}^T$  we can fraction out the uncertain part. Then the inner part of the above mentioned constraints can be reformulated as

$$(A_i^x)^T \xi \leq b_i^x, \forall i = 1, \dots, m$$

where random variable  $\xi$  is wind forecast error  $\Delta W$ ,  $m$  - is a number of chance-constraints, matrices  $A_i^x$  and  $b_i^x$  - deterministic parts of the constraints which depend only on the

decision variables. The DR variants of the chance-constraints are formulated as follows

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}((A_i^x)^T \xi \leq b_i^x) \geq 1 - \epsilon_i, \forall i = 1 \dots m$$

In our case:

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}(A(CY \mathbf{1}_{1 \times N_W}^T - C_W) \Delta W \leq A(CP + C_W P^f - C_D P^D - C_p P^{WP} - C_{HP} P^{HP}) + P_l) \geq 1 - \epsilon$$

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}(A(-CY \mathbf{1}_{1 \times N_W}^T + C_W) \Delta W \leq A(-CP - C_W P^f + C_D P^D + C_p P^{WP} + C_{HP} P^{HP}) + P_l) \geq 1 - \epsilon$$

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}((Y \mathbf{1}_{1 \times N_W}^T) \Delta W \leq P - \underline{P}) \geq 1 - \epsilon$$

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}((-Y \mathbf{1}_{1 \times N_W}^T) \Delta W \leq -P + \overline{P}) \geq 1 - \epsilon$$

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}((-Y \mathbf{1}_{1 \times N_W}^T) \Delta W \leq RT^{up}) \geq 1 - \epsilon$$

$$\inf_{\xi \in \mathcal{D}_\xi} \mathbb{P}(Y \mathbf{1}_{1 \times N_W}^T \Delta W \leq RT^{dn}) \geq 1 - \epsilon$$

After calculating from the data samples  $\{\xi^l\}_{l=1}^N$  the empirical mean vector  $\mu_{N_W \times 1} = \frac{1}{N} \sum_{l=1}^N \xi^l$  and covariance matrix  $\Sigma_{N_W \times N_W} = \frac{1}{N} \sum_{l=1}^N (\xi^l - \mu)(\xi^l - \mu)^T$  we can build moment-based ambiguity set  $\mathcal{D}_\xi$

$$\mathcal{D}_\xi := \{\mathbb{P}_\xi \in \mathcal{P}' : \mathbb{E}_{\mathbb{P}_\xi}[\xi] = \mu, \mathbb{E}_{\mathbb{P}_\xi}[(\xi - \mu)(\xi - \mu)^T] = \Sigma\}$$

which requires that the true mean and covariance matrix of  $\xi$ , given by any distribution in set  $\mathcal{D}_\xi$ , be exactly the empirical mean  $\mu$  and covariance  $\Sigma$ . General DR chance-constraints can be reformulated as follows

$$\sqrt{\left(\frac{1-\epsilon}{\epsilon}\right)} (A_i^x)^T (\Sigma) A_i^x \leq b_i^x - (A_i^x)^T \mu, \forall i = 1 \dots m$$

which is a second-order cone constraint:

$$K_\epsilon \|(\Sigma)^{\frac{1}{2}} A_i^x\|_2 \leq b_i^x - (A_i^x)^T \mu, \forall i = 1 \dots m \quad (1)$$

where  $K_\epsilon = \sqrt{\left(\frac{1-\epsilon}{\epsilon}\right)}$ .

### CASE STUDY DATA

Electrical demand is 200 MW and 100 MW at buses 4 and 5. We assume that reserves from generator are more expensive than CHP reserves  $\overline{c_G} = \underline{c_G} = 1.2c_1$ ,  $\overline{c_c} = \underline{c_c} = 1.1c_e$ . In this study water density is  $\rho = 1000 \text{ kg/m}^3$  and kinematic viscosity of water is  $\mu = 0.4736 \times 10^{-6} \text{ m}^2/\text{s}$ . Darcy friction factor  $f_D = 0.0118$  that is computed as in [1]. The characteristics of the generation units, transmission lines parameters and DHN parameters are presented in Table I,II,III and IV.

### REFERENCES

- [1] D. Clamond, "Efficient resolution of the colebrook equation," *Industrial & Engineering Chemistry Research*, vol. 48, no. 7, pp. 3665–3671, 2009.

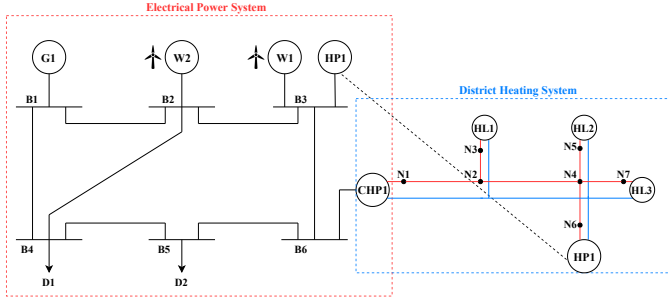


Fig. 1. Configuration of the six-bus and seven-node integrated system.

TABLE I  
GENERATION UNITS

		$G_1$	$CHP_1$	$HP_1$
$\bar{P}$	MW	230	208.3	-
$\underline{P}$	MW	10	15	-
$\bar{R}$	MW	92	41.66	-
$\underline{R}$	MW	0	0	-
$\underline{H}$	MW	-	0	5
$\bar{H}$	MW	-	250	100
$\bar{m}_s^{HS}$	kg/s	-	300	300
$\bar{m}_s^{HS}$	kg/s	-	700	700
$\bar{F}$	MW	-	500	-
COP	-	-	-	2.5
$r$	-	-	0.5	-
$\rho^E$	-	-	2.4	-
$\rho^H$	-	-	0.25	-
$\eta$	-	-	0.9	0.9
$\bar{P}_{WP}$	MW	-	20	20
$\underline{P}_{WP}$	MW	-	0	0
$c_2$	\$/ MWh <sup>2</sup>	0.00125	-	-
$c_1$	\$/ MWh	40.622	-	-
$c_0$	\$	0	-	-
$c_e$	\$/ MWh	-	3.6	-
$c_h$	\$/ MWh	-	0.06	-

TABLE II  
ELECTRICAL TRANSMISSION LINES

		$l_{12}$	$l_{14}$	$l_{23}$	$l_{24}$	$l_{36}$	$l_{45}$	$l_{56}$
$\bar{P}_l$	MW	200	250	250	200	250	250	250
$X$	p.u.	0.17	0.0586	0.1	0.072	0.0625	0.16	0.085

TABLE III  
DISTRICT HEATING PIPES

		$p_{12,24,46}$	$p_{23}$	$p_{45,47}$
$L_p$	m	800	600	500
$D_p$	m	0.8	0.8	0.8
$\lambda$	W/m°C	0.2	0.2	0.2
$\nu_p$	$m \times 10^{-3}$	0.045	0.045	0.045
$K_p$	$1/[m \times kg]$	0.0233	0.0175	0.0146
$\bar{m}_p^S, \bar{m}_p^R$	kg/s	300	300	300
$\bar{m}_p^S, \bar{m}_p^R$	kg/s	700	700	700
$\bar{T}_p^R$	°C	45	45	45
$\bar{T}_p^R$	°C	25	25	25
$\bar{T}_p^S$	°C	65	65	65
$\bar{T}_p^S$	°C	50	50	50

TABLE IV  
DISTRICT HEATING NETWORK PARAMETERS

		$N_{1,2,4,6}$	$N_3(L)$	$N_5(L)$	$N_7(L)$
$\bar{m}_l^{HL}$	kg/s	-	300	300	300
$\bar{m}_l^{HL}$	kg/s	-	700	700	700
$H_l^L$	MW	-	45	40	50
$\bar{T}_n^S$	°C	50	50	50	50
$\bar{T}_n^S$	°C	65	65	65	65
$\bar{T}_n^R$	°C	25	25	25	25
$\bar{T}_n^R$	°C	45	45	45	45
$\bar{pr}_n^S, \bar{pr}_n^R$	kPa	0	0	0	0
$\bar{pr}_n^S, \bar{pr}_n^R$	kPa	30000	30000	30000	30000
$\bar{pr}_l^{HL}$	kPa	-	50	50	50