# **Real Gas Effect in Reacting Flow**

This code repository is used to evaluate the advantages of the proposed real gas equation of state (EoS)

### 1. Code Environment

```
# Cantera used in /opt/cantera_libs/cantera, one can modified code in `src` and build & install by
conda activate cantera
python3 /usr/bin/scons build
python3 /usr/bin/scons install

# The code in this repo can be run by
source /usr/local/bin/setup_cantera
python3 src/xxx.py
```

### 2. Basic Theory

#### 1.0 Generalized EoS

Helmholtz Free Energy:  $F \equiv U - TS = A(T, v, n)$ , where U is the internal energy of the system, T is the absolute temperature, S is the entropy of the system.

- 1st law of thermodynamics:  $dU = \delta Q + \delta W$
- 2nd law of thermodynamics:  $\delta Q = TdS$
- pressure work:  $\delta W = -pdV$

Thus we have:

- dU = TdS pdV
- $\Rightarrow dU = d(TS) SdT pdV$
- $\Rightarrow d(U TS) = -SdT pdV$
- $\Rightarrow dF = -SdT pdV$

Therefore,

$$\begin{split} S &= -\left(\frac{\partial F}{\partial T}\right)_{V} \\ p &= -\left(\frac{\partial F}{\partial V}\right)_{T} \\ U &= F + TS = F - T\left(\frac{\partial F}{\partial T}\right)_{V} \\ H &= U + pV = F - T\left(\frac{\partial F}{\partial T}\right)_{V} - V\left(\frac{\partial F}{\partial V}\right)_{T} \\ C_{p} &= \left(\frac{\partial H}{\partial T}\right)_{p} = T\left[\left(\frac{\partial^{2} F}{\partial V \partial T}\right)_{V,T}^{2} / \left(\frac{\partial^{2} F}{\partial V^{2}}\right)_{T} - \left(\frac{\partial^{2} F}{\partial T^{2}}\right)_{V}\right] \\ C_{V} &= \left(\frac{\partial U}{\partial T}\right)_{V} = -T\left(\frac{\partial^{2} F}{\partial T^{2}}\right)_{V} \end{split}$$

#### 1.1 Ideal Gas

$$p = \frac{nRT}{V_m}$$

where  $V_m$  is the molar volume of the gas .

### 1.2 Van der Waals (vdW) real gas equation 1783

$$p = \frac{RT}{V_m - b} - \frac{a}{V_m^2}$$

where b is the volume that is occupied by one mole of the molecules. vdW is a cubic type EoS.

## 1.4 Redlich-Kwong (RK) real gas equation 1948

$$p = rac{RT}{V_m - b} - rac{a}{\sqrt{T}V_m(V_m + b)}$$

where a is a constant that corrects for attractive potential of molecules and b is a constant that corrects for volume. The constants are different depending on which gas is being analyzed and can be calculated from the critical point data of corresponding gas:

$$a = rac{1}{9(\sqrt[3]{2}-1)}rac{R^2T_c^{2.5}}{P_c} \ b = rac{\sqrt[3]{2}-1}{3}rac{RT_c}{P_c}$$

Where  $T_c$  is the temperature at the critical point and  $P_c$  is the pressure at the critical point. Noted that a and b are solved analytically from the thermodynamic criteria for the critical point:

$$\left(\frac{\partial P}{\partial V}\right)_T = 0, \left(\frac{\partial^2 P}{\partial V^2}\right)_T = 0.$$

For more details, please refer to original paper or wikipedia of Redlich Kwong equation of state.

### 1.5 Soave modified Redlich-Kwong (SRK) real gas equation 1972

In 1966, Barner noted that the acentric factor  $\omega$  can be used to improve RK EoS. SRK is proposed by Soave as:

$$p = \frac{RT}{V_m - b} - \frac{a\alpha}{V_m(V_m + b)}$$

where

$$lpha = \left[1 + (0.480 + 1.574\omega - 0.176\omega^2)(1 - \sqrt{T_r})\right]^2$$
 $a = \frac{1}{9(\sqrt[3]{2} - 1)} \frac{R^2 T_c^2}{P_c}$ 
 $b = \frac{\sqrt[3]{2} - 1}{3} \frac{R T_c}{P_c}$ 

where  $T_r = T/T_c$  is the reduced temperature of the compound. Noted that  $\frac{1}{\sqrt{T}}$  term in RK is vanished and its effect is put into a in SRK.

## 1.6 Peng-Robinson (PR) real gas equation 1976

The Peng-Robinson EoS further modified the RK EoS by modifying the attractive term, giving

$$p = \frac{RT}{V_m - b} - \frac{a\alpha}{V_m(V_m + b) + b(V_m - b)}$$

where

$$lpha = \left[1 + (0.37464 + 1.54226\omega - 0.26992\omega^2)(1 - \sqrt{T_r})\right]^2$$
  $a = 0.457235 \frac{R^2 T_c^2}{P_c}$   $b = 0.077796 \frac{RT_c}{P_c}$ 

### 1.7 PR-RK real gas equation 2005

The limited accuracy of the two-parameter cubic EoS is caused by the inconsistency in the density dependence of its equation rather than the empirical nature of model constants a and b. Many researchers proposed three parameters EoS. In 2005, Cismondi and Mollerup have proposed a three-parameter cubic EoS (hereafter RK-PR EoS) by introducing an additional parameter,  $\delta_1$ .

$$p = rac{RT}{V_m - b} - rac{alpha}{(V_m + \delta_1 b)(V_m + \delta_2 b)}$$

where  $\delta_2$  is not independent and  $\delta_2=(1-\delta_1)(1+\delta_1)$ . And it will degenerate to SRK when  $\delta_1=1,\delta_2=0$ ; and degenerate to PR when  $\delta_1 = 1 + \sqrt{2}, \delta_2 = 1 - \sqrt{2}$ .

## 1.7 Mixture properties

When handling mixture, to obtain the aggregate parameters  $a_m$ ,  $b_m$  of the cubic EoS, mixing rules from the van der Waals one-fluid theory is applied:

$$a_m = \sum_i^{N_s} \sum_j^{N_s} X_i X_j a_{ij} \ b_m = \sum_i^{N_s} X_i b_i$$

where  $X_i$  is the mole fraction of the  $i^{th}$  components of the mixture,  $X_j$  is the mole fraction of the  $j^{th}$  components of the mixture. Besides,  $a_{ij}$  is the attractive term between a molecule of species i and species j, which is usually calculated by  $a_{ij} = (a_i a_j)^{1/2}$  or  $a_{ij}=(a_ia_j)^{1/2}(1-\delta_{ij}).$   $\delta_{ij}$  is an empirically determined binary interaction coefficient characterizing the binary formed by component i and component j.

The mixture properties  $(a\alpha)_m$  is similarly:

$$(alpha)_m = \sum_{i=1}^N \sum_{j=1}^N X_i X_j (a_{ij}lpha_{ij})$$

$$(a_{ij}lpha_{ij})=\sqrt{a_ia_jlpha_ilpha_j}$$

### 2. The calibration model of alpha

The  $\alpha$  is previously calculated by Sovae-type functions like

- In SRK:  $\alpha=\left[1+(0.480+1.574\omega-0.176\omega^2)(1-\sqrt{T_r})\right]^2$  In PR:  $\alpha=\left[1+(0.37464+1.54226\omega-0.26992\omega^2)(1-\sqrt{T_r})\right]^2$

But those are empirical approximations and would lead to notable effects in particular thermodynamically sensitive simulations. Here a Gaussian Process (GP) based semi-parametric method is used to utilize the information of experimental data as most as possible.

### 2.1 The GP model

Here we're trying to fit a function that can map the inputs including  $T_r$  to the output  $\alpha$ . Using the concept of Gaussian Process (GP) model, given the observations (X, y), when applying GP to predict the target  $y_*$  at new input  $X_*$ , one have

$$egin{aligned} \mu(y_*) &= oldsymbol{K}_*^T (oldsymbol{K} + \sigma_n^2 oldsymbol{I})^{-1} y \ \sigma^2(y_*) &= oldsymbol{K}_{**} - oldsymbol{K}_*^T (oldsymbol{K} + \sigma_n^2 oldsymbol{I})^{-1} oldsymbol{K}_* \end{aligned}$$

where  $\sigma_n^2$  is the covariance of estimated Gaussian noise from observed data  $(\boldsymbol{X},y)$ ,  $\boldsymbol{K}$  related terms are the covariance matrices as

$$egin{aligned} oldsymbol{K} &= cov(oldsymbol{X}, oldsymbol{X}) \ oldsymbol{K}_* &= cov(oldsymbol{X}_*, oldsymbol{X}_*) \ oldsymbol{K}_{**} &= cov(oldsymbol{X}_*, oldsymbol{X}_*) \end{aligned}$$

#### 2.2 Kernel functions

The covariance are usually obtained via kernel functions, which are very important for GP's data training. The most famous ones are:

• Squared exponential (or say Radial Basis Function, RBF):

$$cov(x_i, x_j) = \sigma_F^2 \exp \left( -rac{d(x_i, x_j)^2}{2\gamma^2} 
ight)$$

where  $d(x_i, x_j)$  is the Euclidean distance of  $x_i$  and  $x_j$ , l is the length scale of kernel size.

• Matern:

$$k(x_i,x_j) = rac{1}{\Gamma(
u)2^{
u-1}}igg(rac{\sqrt{2
u}}{l}d(x_i,x_j)igg)^
u K_
uigg(rac{\sqrt{2
u}}{l}d(x_i,x_j)igg),$$

where  $\Gamma$  is the Gamma function,  $K_{\nu}$  is the modified Bessel function of order  $\nu$ .

#### 2.3 Basis functions

The basis function provides an important ability to model the mean of y to zero.

$$y(\boldsymbol{x}) = f(\boldsymbol{x}; \boldsymbol{\theta}) + b_{\boldsymbol{\theta}}(\boldsymbol{x}) + \epsilon$$

where  $\epsilon$  is the (Gaussian) stochastic error in the database,  $f(x; \theta)$  is a basis function that can model y(x) as much as possible, and  $b_{\theta}(x)$  is the bias term that can compensate the error between  $f(x; \theta)$  and y(x).

To solve this optimization problem, let  $f(x; \theta) = \theta_3 x_2 + \theta_2 x_1 + \theta_1$  as a linear combination of the input variables x, where the input variable are  $x = [x_1, x_2]$ ,  $x_1$  and  $x_2$  are the input from each dimension; and  $\theta = [\theta_1, \theta_2, \theta_3]$  are corresponding parameters in the linear combination function f.

The corresponding kernel function then be formed as:

$$k(x_i, x_i) = k0(x_i, x_i) - h_{\theta}(x_i)^T \boldsymbol{H}_{\theta} h_{\theta}(x_i)$$

where  $h_{\theta}(x)$  is the 1st order global sensitivity obtained from:

$$h_{ heta}(x) = \int_{oldsymbol{X}} 
abla_{ heta} f(\xi) k_0(x,\xi) d\xi$$

the 2nd order global sensitivity, i.e., Hessian matrix is

$$oldsymbol{H}_{ heta} = \int_{oldsymbol{X}} \int_{oldsymbol{X}} (
abla_{ heta} f(\xi)) (
abla_{ heta} f(\zeta))^T k_0(\xi,\zeta) d\xi d\zeta$$

The parameter gradient of f shows

$$abla_{ heta}f(oldsymbol{x}) = rac{\partial}{\partialoldsymbol{ heta}}f(oldsymbol{x};oldsymbol{ heta}) = egin{bmatrix} 1 \ x_1 \ x_2 \end{bmatrix}$$

The matrix constructed by gradients' outer product of randomly samples  $\xi, \zeta$ 

$$(
abla_{ heta}f(oldsymbol{\xi}))(
abla_{ heta}f(oldsymbol{\zeta}))^T = egin{bmatrix} 1 \ \xi_1 \ \xi_2 \end{bmatrix} [1 \quad \zeta_1 \quad \zeta_2] = egin{bmatrix} 1 & \zeta_1 & \zeta_2 \ \xi_1 & \xi_1\zeta_1 & \xi_1\zeta_2 \ \xi_2 & \xi_2\zeta_1 & \xi_2\zeta_2 \end{bmatrix}$$

The kernel function  $k_0$  is:

$$k_0(\xi,\zeta) = \sigma_F^2 \exp\left(-\sum_i rac{(\xi_i-\zeta_i)^2}{2\gamma_i^2}
ight) = \sigma_F^2 \exp\left(-rac{(\xi_1-\zeta_1)^2}{2\gamma_1^2}
ight) \exp\left(-rac{(\xi_2-\zeta_2)^2}{2\gamma_2^2}
ight)$$

where  $\gamma_1, \gamma_2$  are the parameters of kernel function in dimension  $x_1$  and  $x_2$ .

The corresponding distribution of the evaluated output  $y_*$  at new  $x_*$  should be:

$$egin{aligned} \mu(y_*) &= f(x_*; heta) + oldsymbol{K}_*^T igg( oldsymbol{K} + rac{\sigma_n^2}{
u} oldsymbol{I} igg)^{-1} \left[ y - f(oldsymbol{X}; heta) 
ight] \ \sigma(y_*) &= 
u + oldsymbol{K}_{**} - 
u oldsymbol{K}_*^T igg( oldsymbol{K} + rac{\sigma_n^2}{
u} oldsymbol{I} igg)^{-1} oldsymbol{K}_* \end{aligned}$$

where  $\nu$  is a measurement of possible noises, its maximum likelihood estimation (MLE)  $\hat{\nu}$  is

$$\hat{
u} = rac{1}{N}[y - f(oldsymbol{X}; heta)]^T (oldsymbol{K} + goldsymbol{I})^{-1}[y - f(oldsymbol{X}; heta)]$$

where g is the original possible noise level, which still should be estimated by optimization program.

# 2.4 Thermodynamic Properties

By setting at least two thermo states like  $p, T, \rho$ , one can calculate all the related thermodynamic properties of given mixture. Where pressure p and temperature T can be obtained explicitly from the equation of state (EoS). Density can be obtained by first getting  $V_m$  via solving the cubic function:

$$p = \frac{RT}{V - b} - \frac{a\alpha}{V^2 + 2Vb - b^2}$$

Other related thermodynamic properties can be calculated via:

$$egin{aligned} C_v &= \left(rac{\partial H}{\partial T}
ight)_V - V\left(rac{\partial p}{\partial T}
ight) \ C_p &= C_v - Tigg(rac{\partial p}{\partial T}igg)^2 / rac{\partial p}{\partial V} \ s(T,p) &= e(T,p) &= h(T,p) &= \end{aligned}$$

where the corresponding partial derivatives are:

$$\begin{split} \left(\frac{\partial H}{\partial T}\right)_{V} &= C_{p,0} + V \frac{\partial p}{\partial T} - R + \frac{1}{2\sqrt{2}b} \log\left(\frac{V+b}{V-b}\right) T \frac{\partial^{2}(a\alpha)_{m}}{\partial T^{2}} \\ \frac{\partial p}{\partial T} &= \frac{R}{V-b} - \frac{\partial(a\alpha)_{m}}{\partial T} \frac{1}{V^{2} + 2Vb - b^{2}} \\ \frac{\partial p}{\partial V} &= -\frac{RT}{(V-b)^{2}} + 2\frac{(a\alpha)_{m}(V+b)}{V^{2} + 2Vb - b^{2}} \end{split}$$

The alpha related properties are:

$$egin{aligned} rac{\partial (alpha)_m}{\partial T} &= \sum_{i=1}^N \sum_{j=1}^N X_i X_j rac{\partial (a_{ij}lpha_{ij})}{\partial T} \ rac{\partial^2 (alpha)_m}{\partial T^2} &= \sum_{i=1}^N \sum_{j=1}^N X_i X_j rac{\partial^2 (a_{ij}lpha_{ij})}{\partial T^2} \end{aligned}$$

where the derivatives of  $(a_{ij}\alpha_{ij})$  are:

$$\begin{split} \frac{\partial(a_{ij}\alpha_{ij})}{\partial T} &= \sqrt{a_ia_j}\frac{\partial\sqrt{\alpha_i\alpha_j}}{\partial T} = \frac{1}{2}\sqrt{a_ia_j\alpha_i\alpha_j}\left(\frac{1}{\alpha_i}\frac{\partial\alpha_i}{\partial T} + \frac{1}{\alpha_j}\frac{\partial\alpha_j}{\partial T}\right) \\ \frac{\partial^2(a_{ij}\alpha_{ij})}{\partial T^2} &= \frac{1}{2}\sqrt{a_ia_j\alpha_i\alpha_j}\left[\frac{1}{\alpha_i}\frac{\partial^2\alpha_i}{\partial T} + \frac{1}{\alpha_j}\frac{\partial^2\alpha_j}{\partial T} + \frac{2}{\alpha_i\alpha_j}\frac{\partial\alpha_i}{\partial T}\frac{\partial\alpha_j}{\partial T} - \frac{1}{2}\left(\frac{1}{\alpha_i}\frac{\partial\alpha_i}{\partial T} + \frac{1}{\alpha_j}\frac{\partial\alpha_j}{\partial T}\right)^2\right] \end{split}$$

Finally, we only need to get  $\frac{\partial \alpha}{\partial T}$  and  $\frac{\partial^2 \alpha}{\partial T^2}$ .

• For the original Peng-Robinson EoS framwork,

$$lpha = \left[1 + \kappa \left(1 - \sqrt{T/T_c}
ight)
ight]^2$$

Therefore.

$$egin{aligned} rac{\partial lpha}{\partial T} &= rac{\kappa^2}{T_c} - (\kappa^2 + \kappa) rac{1}{\sqrt{Tc}} T^{-1/2} \ rac{\partial^2 lpha}{\partial T^2} &= rac{1}{2} (\kappa^2 + \kappa) rac{1}{\sqrt{T_c}} T^{-3/2} \end{aligned}$$

• For the Gaussian Process's framework without basis function, we have

$$lpha(x_*) = \mu(lpha_*) = oldsymbol{K}_*^T (oldsymbol{K} + \sigma_n^2 oldsymbol{I})^{-1} lpha_{obs}$$

where  $\alpha_{obs}$  is the given observed data of  $\alpha$  from NIST or experimental data at specific temperatures and pressures. The right hand side (RHS) term  $(\mathbf{K} + \sigma_n^2 \mathbf{I})^{-1} \alpha_{obs}$  is known during the prediction of  $\alpha(x_*)$ , hence is denoted as  $\mathbf{m}$  here. For a single new evaluation point  $x_* = (T_{r,*}, P_{r,*})$ , the  $\mathbf{K}_*$  is matrix of dimension  $N \times 1$ , so:

$$lpha = \sum_{i=1}^N k_{*,i} m_i$$

where

$$k_{*,i} = \sigma_F^2 \exp \left( -rac{(T_{r,*} - T_{r,i})^2}{2\gamma_T^2} - rac{(P_{r,*} - P_{r,i})^2}{\gamma_T^2} 
ight)$$

Thus,

$$\begin{split} \frac{\partial \alpha}{\partial T} &= \sum_{i=1}^N m_i \frac{\partial k_{*,i}}{\partial T} = \sum_{i=1}^N m_i \left( -\frac{1}{T_c} \frac{T_{r,*} - T_{r,i}}{\gamma_T^2} \right) k_{*,i} \\ \frac{\partial^2 \alpha}{\partial T^2} &= \sum_{i=1}^N m_i \frac{\partial^2 k_{*,i}}{\partial T^2} = \sum_{i=1}^N m_i \left( \frac{1}{T_c^2} \frac{(T_{r,*} - T_{r,i})^2}{\gamma_T^4} - \frac{1}{T_c^2} \frac{1}{\gamma_T^2} \right) k_{*,i} \end{split}$$

• For the Gaussian Process's framework with basis function, we have

$$egin{aligned} lpha(x_*) = \mu(lpha_*) = f(x_*; heta) + oldsymbol{K}_*^T igg(oldsymbol{K} + rac{\sigma_n^2}{
u} oldsymbol{I}igg)^{-1} \left[y - f(oldsymbol{X}; heta)
ight] \end{aligned}$$

Similarly, one can define the known RHS terms as  $m{m} = \left(m{K} + rac{\sigma_n^2}{
u} m{I} \right)^{-1} [y - f(m{X}; heta)]$ , and  $m{\alpha} = f(x_*; heta) + \sum_{i=1}^N k_{*,i} m_i$ , with

$$k_{*,i} = k0(x_*,x_i) - h_{ heta}(x_*)^T oldsymbol{H}_{ heta} h_{ heta}(x_i)$$

where

$$egin{aligned} h_{ heta}(x_*) &= \int_{oldsymbol{X}} 
abla_{ heta} f(\xi) k_0(x_*, \xi) d\xi \ h_{ heta}(x_i) &= \int_{oldsymbol{X}} 
abla_{ heta} f(\xi) k_0(x_i, \xi) d\xi \end{aligned}$$

so  $m{H}_{ heta}h_{ heta}(x_i)$  is a known term and is hereby denoted as  $g_{ heta}(x_i)=[g_{i,1},g_{i,2},g_{i,3}]$  . Therefore,

$$k_{*,i} = k0(x_*, x_i) - h_{\theta}(x_*)^T g_{\theta}(x_i) = k0(x_*, x_i) - g_{i,1} \sum_{j=1}^N k0(x_*, x_j) - g_{i,2} \sum_{j=1}^N x_{j,1} k0(x_*, x_j) - g_{i,3} \sum_{j=1}^N x_{j,2} k0(x_*, x_j)$$

$$\frac{\partial k_{*,i}}{\partial T} = \frac{\partial k0(x_*, x_i)}{\partial T} - g_{i,1} \sum_{j=1}^N \frac{\partial k0(x_*, x_j)}{\partial T} - g_{i,2} \sum_{j=1}^N \left[ x_{j,1} \frac{\partial k0(x_*, x_j)}{\partial T} + \frac{\partial x_{j,1}}{\partial T} k0(x_*, x_j) \right] - g_{i,3} \sum_{j=1}^N x_{j,2} \frac{\partial k0(x_*, x_j)}{\partial T}$$

$$\frac{\partial^2 k_{*,i}}{\partial T^2} = \frac{\partial^2 k0(x_*, x_i)}{\partial T^2} - g_{i,1} \sum_{j=1}^N \frac{\partial^2 k0(x_*, x_j)}{\partial T^2} - g_{i,2} \sum_{j=1}^N \left[ x_{j,1} \frac{\partial^2 k0(x_*, x_j)}{\partial T^2} + 2 \frac{\partial x_{j,1}}{\partial T} \frac{\partial k0(x_*, x_j)}{\partial T} \right] - g_{i,3} \sum_{j=1}^N x_{j,2} \frac{\partial^2 k0(x_*, x_j)}{\partial T^2}$$

And finally:

$$egin{aligned} rac{\partial lpha}{\partial T} &= rac{\partial f}{\partial T} + \sum_{i=1}^N m_i rac{\partial k_{*,i}}{\partial T} \ rac{\partial^2 lpha}{\partial T^2} &= rac{\partial^2 f}{\partial T^2} + \sum_{i=1}^N m_i rac{\partial^2 k_{*,i}}{\partial T^2} \end{aligned}$$

## 2.5 Implementation

#### 2.6 Validation

## 3. Appendix

Using the chain rule from Table 5, Page 4 of Partial derivatives of thermodynamic state properties for dynamic simulation,

$$C_p = \left(rac{\partial H}{\partial T}
ight)_p = \left(rac{\partial H}{\partial T}
ight)_V - \left(rac{\partial H}{\partial V}
ight)_T \left(rac{\partial p}{\partial T}
ight)_V \left(rac{\partial p}{\partial V}
ight)_T^{-1}$$

where

$$\begin{split} \left(\frac{\partial H}{\partial T}\right)_{V} &= \left(\frac{\partial F}{\partial T}\right)_{V} - \left(\frac{\partial F}{\partial T}\right)_{V} - T\left(\frac{\partial^{2} F}{\partial T^{2}}\right)_{V} - V\left(\frac{\partial^{2} F}{\partial V \partial T}\right)_{T,V} \\ &= -T\left(\frac{\partial^{2} F}{\partial T^{2}}\right)_{V} - V\left(\frac{\partial^{2} F}{\partial V \partial T}\right)_{T,V} \\ \left(\frac{\partial H}{\partial V}\right)_{T} &= \left(\frac{\partial F}{\partial V}\right)_{T} - T\left(\frac{\partial^{2} F}{\partial T \partial V}\right)_{V,T} - \left(\frac{\partial F}{\partial V}\right)_{T} - V\left(\frac{\partial^{2} F}{\partial V^{2}}\right)_{T} \\ &= -T\left(\frac{\partial^{2} F}{\partial T \partial V}\right)_{V,T} - V\left(\frac{\partial^{2} F}{\partial V^{2}}\right)_{T} \\ \left(\frac{\partial p}{\partial T}\right)_{V} &= -\left(\frac{\partial^{2} F}{\partial V \partial T}\right)_{T,V} \\ \left(\frac{\partial p}{\partial V}\right)_{T} &= -\left(\frac{\partial^{2} F}{\partial V^{2}}\right)_{T} \end{split}$$

therefore,

$$\begin{split} C_p &= \left(\frac{\partial H}{\partial T}\right)_V - \left(\frac{\partial H}{\partial V}\right)_T \left(\frac{\partial p}{\partial T}\right)_V \left(\frac{\partial p}{\partial V}\right)_T^{-1} \\ &= -T \left(\frac{\partial^2 F}{\partial T^2}\right)_V - V \left(\frac{\partial^2 F}{\partial V \partial T}\right)_{T,V} + \left[T \left(\frac{\partial^2 F}{\partial T \partial V}\right)_{V,T} + V \left(\frac{\partial^2 F}{\partial V^2}\right)_T\right] \left(\frac{\partial^2 F}{\partial V \partial T}\right)_{T,V} / \left(\frac{\partial^2 F}{\partial V^2}\right)_T \\ &= -T \left(\frac{\partial^2 F}{\partial T^2}\right)_V + T \left(\frac{\partial^2 F}{\partial T \partial V}\right)_{V,T} \left(\frac{\partial^2 F}{\partial V \partial T}\right)_{T,V} / \left(\frac{\partial^2 F}{\partial V^2}\right)_T \\ &= T \left[\left(\frac{\partial^2 F}{\partial V \partial T}\right)_{V,T}^2 / \left(\frac{\partial^2 F}{\partial V^2}\right)_T - \left(\frac{\partial^2 F}{\partial T^2}\right)_V\right] \end{split}$$