

A MGRPO-TD3 Strategy for Optimizing Multi-Area HPT Networks

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This supplementary document compiles the key modelling assumptions, component efficiencies, cost coefficients, and baseline travel-time coefficient inputs, used to parameterize the technical analyses reported in the paper.

1) PEM Electrolyzer Parameters

Table I lists the electrochemical and cost coefficients that define the PEM electrolyzer model adopted in this study [1].

TABLE I ELECTROCHEMICAL AND COST PARAMETERS OF THE PEM ELECTROLYZER						
\mathfrak{I}_1	\mathfrak{I}_2	\mathfrak{I}_3	\mathfrak{I}_4	\mathfrak{I}_5	\mathfrak{I}_6	\mathfrak{I}_7
99.5%	-9.5788 (m^2/A)	-0.0555 ($m^2/A \times ^\circ C$)	0	1502.7083 (m^4/A)	-70.8005 ($m^4/A \times ^\circ C$)	0
		F	z_{mk}	μ^{PEM}		
		96485.34 (C/mol)	0.002016 (kg/mol)	36 (\$/kg) per year		

2) Compressor, Hydrogen Tank, and Electrical Storage Parameters

Table II consolidates the thermodynamic constants and operating-cost coefficients used to model the hydrogen compressor, hydrogen tank, and on-site electrical storage systems, as sourced from [2]-[4].

TABLE II THERMODYNAMIC AND OPERATIONAL PARAMETERS FOR COMPRESSOR, HYDROGEN TANK, AND ELECTRICAL STORAGE UNITS				
Compressor				
ζ	R^{gc}	μ^{comp}	ρ^{ih}	ρ^{ie}
1.41	4.124 kJ/(kg·K)	1 (\$/kg) per year	14.31 (kJ/kg.K)	0.8
Hydrogen tank				
μ^{tank}	SoC_{max}^T	SoC_{min}^T	η_{ch}^T	η_{dc}^T
32 (\$/kg) per year	0.9	0.05	0.9	0.9
Electrical storage				
SoC_{min}^{ES}	SoC_{max}^{ES}	η_{ch}^{ES}	η_{dc}^{ES}	μ^{ES}
0.1	0.9	0.95	0.95	0.0005 (\$/kWh)

3) Hydrogen-Pricing Equation Coefficients

Table III summarizes the key coefficients appearing in the dynamic hydrogen-pricing formulation with values taken from [5], [6].

TABLE III
COEFFICIENTS USED IN THE HYDROGEN-PRICING MODEL

ω_t^{ren}	C_t^{ren}	δ^{SP}	η_t^{PEM}
0.6	0.03	1	45
	(\$/kWh)	(\$/kg)	(kWh/kg)

4) *Penalty Coefficients*

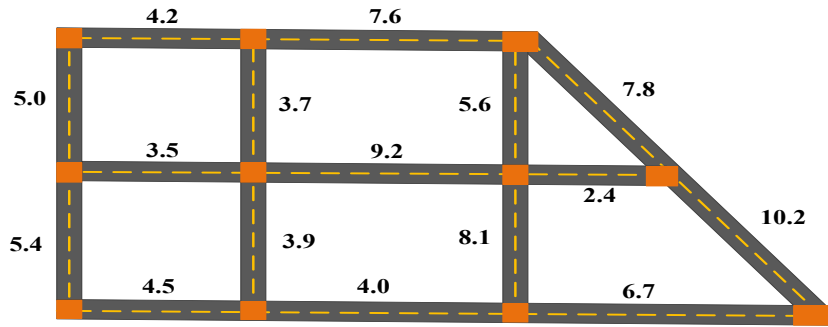
TABLE IV
PENALTY COEFFICIENTS

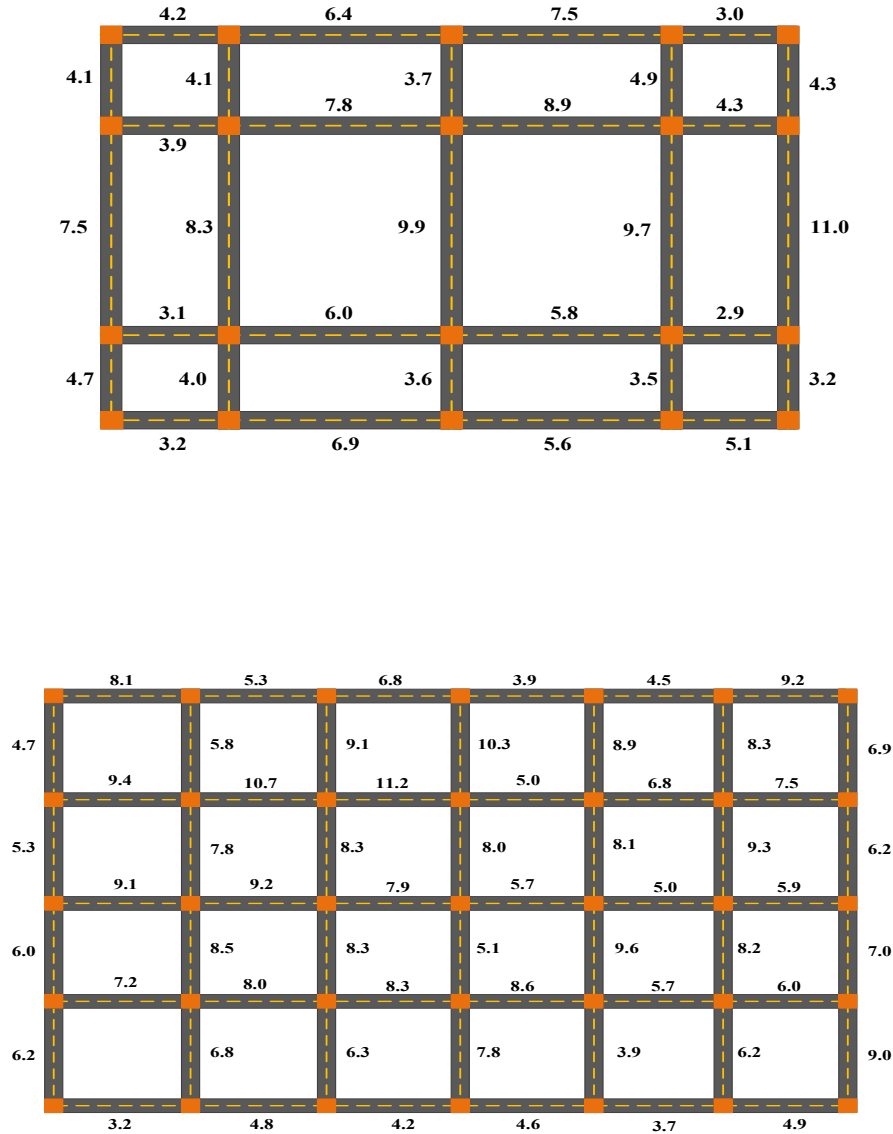
μ^{HU}	C^{tr}	$q_{\alpha,\zeta}$ & c^{HP} (Soft constraints penalty coefficient)
130	40	100-1000
(\$/kg)	(\$/h)	(\$ per unit)

5) *Non-Congested Travel Time Coefficients*

Table V presents the non-congested travel time coefficients for streets, used as baseline inputs in the OD-equilibrium model for the Calgary network. The inter-area coefficients are 62.5 between Areas #1 & #2, 83.7 between Areas #1 & #3, and 106.7 between Areas #2 & #3.

TABLE V
ASSUMED NON-CONGESTED TRAVEL TIME COEFFICIENTS FOR STREETS AND INTER-AREA ROUTES





References:

- [1] F. Scheepers, M. Stähler, A. Stähler, E. Rauls, M. Müller, M. Carmo, and W. Lehnert, "Temperature optimization for improving polymer electrolyte membrane–water electrolysis system efficiency," *Applied Energy*, vol. 283, Art. no. 116270, 2021.
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- [3] M.-R. Tahan, "Recent advances in hydrogen compressors for use in large-scale renewable energy integration," *Int. J. Hydrogen Energy*, vol. 47, no. 83, pp. 35275–35292, Sep. 2022.
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- [5] H. E. Dillon, C. A. Antonopoulos, A. E. Solana, and B. J. Russo, *Renewable Energy Requirements for Future Building Codes: Options for Compliance*, Tech. Rep. PNNL-20727, Pacific Northwest National Laboratory, Richland, WA, USA, Sep. 2011.
- [6] Technical Targets for Proton Exchange Membrane Electrolysis [Online]. Accessed: Oct. 20, 2024. Available: [U.S. Department of Energy](https://www.energy.gov/eere/energy-efficiency/technical-targets-for-proton-exchange-membrane-electrolysis).