

# A MGRPO-TD3 Strategy for Optimizing Multi-Area HPT Networks

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This supplementary document compiles the key modelling assumptions, component efficiencies, cost coefficients, and baseline travel-time coefficient inputs, used to parameterize the technical analyses reported in the paper.

## 1) PEM Electrolyzer Parameters

Table I lists the electrochemical and cost coefficients that define the PEM electrolyzer model adopted in this study [1].

$\mathfrak{I}_1$	$\mathfrak{I}_2$	$\mathfrak{I}_3$	$\mathfrak{I}_4$	$\mathfrak{I}_5$	$\mathfrak{I}_6$	$\mathfrak{I}_7$
99.5%	-9.5788 ( $m^2/A$ )	-0.0555 ( $m^2/A \times ^\circ C$ )	0	1502.7083 ( $m^4/A$ )	-70.8005 ( $m^4/A \times ^\circ C$ )	0
		$F$	$z_{mk}$	$\mu^{PEM}$		
		96485.34 (C/mol)	0.002016 (kg/mol)	36 (\$/kg) per year		

## 2) Compressor, Hydrogen Tank, and Electrical Storage Parameters

Table II consolidates the thermodynamic constants and operating-cost coefficients used to model the hydrogen compressor, hydrogen tank, and on-site electrical storage systems, as sourced from [2]-[4].

<b>Compressor</b>				
$\zeta$	$R^{gc}$	$\mu^{comp}$	$\rho^{ih}$	$\rho^{ie}$
1.41	4.124 kJ/(kg·K)	1 (\$/kg) per year	14.31 (kJ/kg.K)	0.8
<b>Hydrogen tank</b>				
$\mu^{tank}$	$SoC_{max}^T$	$SoC_{min}^T$	$\eta_{ch}^T$	$\eta_{dc}^T$
32 (\$/kg) per year	0.9	0.05	0.9	0.9
<b>Electrical storage</b>				
$SoC_{min}^{ES}$	$SoC_{max}^{ES}$	$\eta_{ch}^{ES}$	$\eta_{dc}^{ES}$	$\mu^{ES}$
0.1	0.9	0.95	0.95	0.0005 (\$/kWh)

## 3) Hydrogen-Pricing Equation Coefficients

Table III summarizes the key coefficients appearing in the dynamic hydrogen-pricing formulation with values taken from [5], [6].

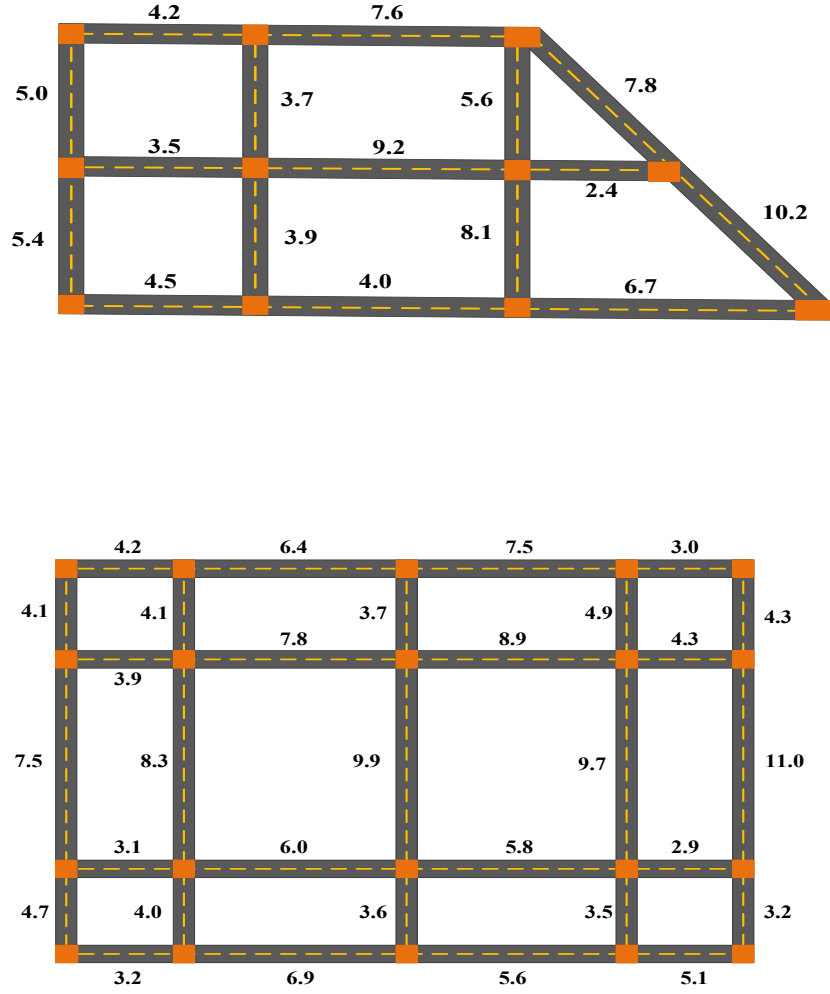
TABLE III  
COEFFICIENTS USED IN THE HYDROGEN-PRICING MODEL

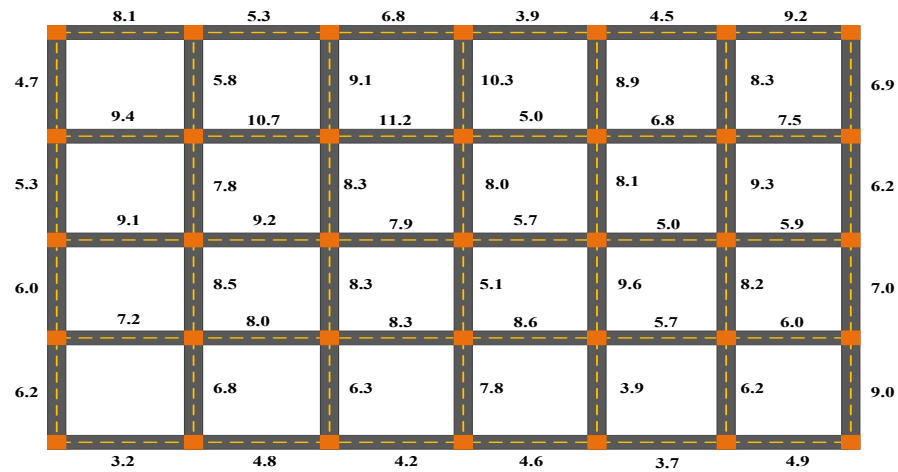
$\omega_t^{ren}$	$C_t^{ren}$	$\delta^{SP}$	$\eta_t^{PEM}$
0.6	0.03	1	45
	(\$/kWh)	(\$/kg)	(kWh/kg)

4) *Non-Congested Travel Time Coefficients*

Table IV lists the non-congested travel time coefficients used as baseline inputs in the OD-equilibrium model for the Calgary network. The inter-area coefficients are 62.5 between Areas #1 & #2, 83.7 between Areas #1 & #3, and 106.7 between Areas #2 & #3.

TABLE IV  
ASSUMED NON-CONGESTED TRAVEL TIME COEFFICIENTS BETWEEN TRAFFIC AREAS





References:

[1] F. Scheepers, M. Stähler, A. Stähler, E. Rauls, M. Müller, M. Carmo, and W. Lehnert, “Temperature optimization for improving polymer electrolyte membrane–water electrolysis system efficiency,” *Applied Energy*, vol. 283, Art. no. 116270, 2021.

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[3] M.-R. Tahan, “Recent advances in hydrogen compressors for use in large-scale renewable energy integration,” *Int. J. Hydrogen Energy*, vol. 47, no. 83, pp. 35275–35292, Sep. 2022.

[4] M. Jadidbonab, H. Abdeltawab, and Y.A.R.I. Mohamed, “A Hybrid Traffic Flow Forecasting and Risk-Averse Decision Strategy for Hydrogen-Based Integrated Traffic and Power Networks,” *IEEE Syst. J.*, pp. 1-13, July 2024.

[5] H. E. Dillon, C. A. Antonopoulos, A. E. Solana, and B. J. Russo, *Renewable Energy Requirements for Future Building Codes: Options for Compliance*, Tech. Rep. PNNL-20727, *Pacific Northwest National Laboratory, Richland, WA, USA*, Sep. 2011.

[6] Technical Targets for Proton Exchange Membrane Electrolysis [Online]. Accessed: Oct. 20, 2024. Available: [U.S. Department of Energy](#).