

## Tutorial 3 – SOLUTIONS

### Tutorial 3: First Law of Thermodynamics (closed & open system) including specific heats

**Note:** numerical solution are based on one approach to solving the tutorial questions. Other approaches can also be correct and could lead to slightly different numerical answers.

#### Conceptual Questions:

1. For the classical sign convention of the first law (i.e.  $\Delta E_{sys} = Q_{net} - W_{net}$ ), what is regarded as **positive** work and **positive** heat?

Solution: According to  $\Delta E_{sys} = Q_{net} - W_{net}$ ,  $Q_{net} = Q_{in} - Q_{out}$  and  $W_{net} = W_{out} - W_{in}$ . Thus, heat transfer INTO a system and work done BY (out of) a system are positive; heat transfer FROM (out of) a system and work done ON (into) a system are negative.

2. Briefly explain the three modes of heat transfer.

- Conduction: exchange of energy between molecules of a substance with no bulk motion.
- Convection: exchange of energy between a surface and the adjacent liquid or gas that is in motion.
- Radiation: exchange of energy from the surface of one body to the surface of another due to electromagnetic radiation.

3. Using the definition of enthalpy ( $h = u + Pv$ ) and the definitions  $du = C_v dT$  and  $dh = C_p dT$ , show that  $C_p = C_v + R$  for an ideal gas.

Solution:

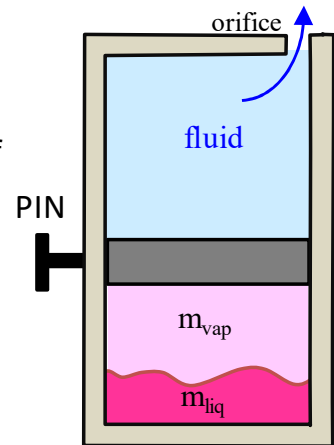
- $h = u + Pv$ ;  $Pv = RT$
- $dh = du + d(RT)$
- $dh = C_p dT$  &  $du = C_v dT \rightarrow C_p dT = C_v dT + d(RT) \rightarrow C_p = C_v + R$

4. What is the definition of the specific heat ratio ( $k$ )?

Solution:  $k = C_p / C_v$

#### Problem Solving Questions:

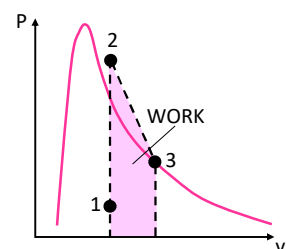
5. A piston cylinder device is comprised of two compartments. The bottom compartment is closed and contains refrigerant R-134a. The top compartment is open with a small orifice and contains an unknown fluid. The closed compartment contains 2.5 kg of refrigerant R134a at  $-20^{\circ}\text{C}$ . Initially 25% of the refrigerant exists as a vapor, while the remaining exists as a liquid. A pin is used to secure the piston in place.
- (a) Heat is transferred to the cylinder via an electric heater, while the pin is still locked. The refrigerant temperature rises to  $30^{\circ}\text{C}$ . Determine the heat transferred (in kJ).
- (b) The electric heater is turned off and the pin is removed. The piston moves upward and fluid exits the top compartment such that the pressure in the closed compartment decreases linearly with increasing volume. The cylinder expands until the refrigerant is a saturated vapor at 400 kPa. Determine the final temperature, boundary work, and any heat transfer to the surroundings.



### Solution:

- There are several processes occurring, so we will first define them
  - Process 1-2: Refrigerant, initially at a saturated mixture at  $T_1 = -20^{\circ}\text{C}$  is heated at constant volume until the refrigerant temperature is  $30^{\circ}\text{C}$ .
  - Process 2-3: Heat addition from the electric heater ceases. Cylinder expands upon pin removal and refrigerant expands as pressure decreases linearly until the refrigerant reaches a saturated vapor (i.e.  $x_3 = 1$ ) at  $P_3 = 400$  kPa. There might be heat transfer to the surroundings during this process.
- Define the system: refrigerant in the cylinder
- Process 1-2: Apply the first law of thermodynamics
  - $\Delta U + \Delta KE + PE = Q_{21} - W_{21} + \Delta E_{mass,21}$
  - System is closed, stationary and fixed volume, thus:  $m(u_2 - u_1) = Q_{21}$
  - Determine relevant variables for state 1:
    - $x_1 = 0.25, T_1 = -20^{\circ}\text{C}$
    - $v_1 = v_{f@-20^{\circ}\text{C}} + x_1 v_{fg@-20^{\circ}\text{C}} = 0.000738 \frac{\text{m}^3}{\text{kg}} + 0.25 \left( 0.14576 \frac{\text{m}^3}{\text{kg}} \right) = 0.03718 \frac{\text{m}^3}{\text{kg}}$
    - $u_1 = u_{f@-20^{\circ}\text{C}} + x_1 u_{fg@-20^{\circ}\text{C}} = 173.65 \frac{\text{kJ}}{\text{kg}} + 0.25 \left( 192.85 \frac{\text{kJ}}{\text{kg}} \right) = 221.9 \frac{\text{kJ}}{\text{kg}}$
  - Determine relevant variables for state 2 ( $T_2 = 30^{\circ}\text{C}$ )
    - Fixed volume & mass:  $v_1 = v_2 = 0.03718 \frac{\text{m}^3}{\text{kg}}$
    - $V_1 = V_2 = v_1 m = 0.03718 \frac{\text{m}^3}{\text{kg}} * 2.5 \text{ kg} = 0.0929 \text{ m}^3$
    - $v_2 > v_{g@30^{\circ}\text{C}} \rightarrow \text{state is superheated vapor}$
    - Need to interpolate in steam tables to find  $u_2$  and  $P_2$

- $\frac{u_2 - u_{500kPa,30C}}{v_2 - v_{500kPa,30C}} = \frac{u_{600kPa,30C} - u_{500kPa,30C}}{v_{600kPa,30C} - v_{500kPa,30C}}$
- $u_2 = u_{500kPa,30C} + \frac{v_2 - v_{500kPa,30C}}{v_{600kPa,30C} - v_{500kPa,30C}} (u_{600kPa,30C} - u_{500kPa,30C})$
- $u_2 = 398.99 \frac{kJ}{kg} + \frac{0.03718 - 0.04446}{0.03609 - 0.04446} (397.44 - 398.99) \frac{kJ}{kg} = 397.6 \frac{kJ}{kg}$
- $\frac{P_2 - P_{500kPa}}{v_2 - v_{500kPa,30C}} = \frac{P_{600kPa} - P_{500kPa}}{v_{600kPa,30C} - v_{500kPa,30C}}$
- $P_2 = P_{500kPa} + \frac{v_2 - v_{500kPa,30C}}{v_{600kPa,30C} - v_{500kPa,30C}} (P_{600kPa} - P_{500kPa})$
- $P_2 = 500kPa + \frac{0.03718 - 0.04446}{0.03609 - 0.04446} (600 - 500)kPa = 587kPa$
- Determine heat addition for Process 1-2
  - $Q_{21} = m(u_2 - u_1) = 2.5kg(397.6 - 221.9) \frac{kJ}{kg} = 439.25kJ$
- Process 2-3: Apply First Law of Thermodynamics
  - $\Delta U + \Delta KE + \Delta PE = Q_{32} - W_{32} + \Delta E_{mass,32}$
  - System is closed and stationary, but has moving boundaries
    - $m(u_3 - u_2) = Q_{32} - W_{32}$
  - Determine relevant variables for state 3
    - Saturated vapor at  $P_3 = 400 \text{ kPa}$
    - $T_3 = T_{sat@400kPa}$ . This can be seen as the saturated entry in the superheated R134a tables at 400kPa.  $T_3 = 8.84^\circ\text{C}$
    - $u_3 = 383.02 \frac{kJ}{kg}$ ;  $v_3 = 0.05136 \frac{m^3}{kg}$
    - Find Volume:  $V_3 = mv_3 = 2.5kg * 0.05136 \frac{m^3}{kg} = 0.1284m^3$
  - Determine the boundary work
    - There is a linear relationship between pressure and volume for process 2-3.
    - Plot process 2-3 on the P-V diagram
    - Pressure will decrease linearly, while volume will increase linearly
    - From lecture (and book):  $W_b = \frac{1}{2}(P_3 + P_2)(V_3 - V_2)$
    - $W_{b,32} = \frac{1}{2}(400 + 587)kPa(0.1284 - 0.0929)m^3 = 17.5kJ$
    - This value is also equal to the area under the P-V curve
    - Since the system is expanding, the work is out of the system, so  $W_{net}$  is positive
  - Determine the heat transfer in process 2-3
    - From the 1<sup>st</sup> law of thermodynamics:  $m(u_3 - u_2) = Q_{32} - W_{32}$



- $Q_{32} = m(u_3 - u_2) + W_{b,32} = 2.5 \text{ kg} (383.02 - 397.6) \frac{\text{kJ}}{\text{kg}} + 17.5 \text{ kJ} = -18.95 \text{ kJ}$
- Thus heat is leaving the system towards the surroundings

6. Complete the table below (for substances that can be assumed to be ideal gases, where these are properties at 300K,  $R_u = 8.314 \text{ kJ/(kmolK)}$ ).

Substance	Molar mass kg/kmol	R kJ/(kgK)	$C_p$ kJ/(kgK)	$C_v$ kJ/(kgK)	k
Air	28.97	0.287	1.005	0.718	1.400
Carbon Dioxide	44.01	0.189	0.846	0.657	1.289
Hydrogen	2.016	4.124	14.31	10.18	1.405
Nitrogen	28.01	0.297	1.039	0.743	1.400
Oxygen	32.00	0.260	0.918	0.658	1.395

**Solution:**

Air

- $R = R_u / M \rightarrow M = R_u / R = 8.314 / 0.287 = 28.97 \text{ kg/kmol}$
- $C_v = R / (k-1) = 0.287 / (1.400 - 1) = 0.718 \text{ kJ/(kgK)}$
- $C_p = C_v + R = 0.718 + 0.287 = 1.005 \text{ kJ/(kgK)}$

Carbon dioxide

- $k = C_p / C_v = 0.846 / 0.657 = 1.288$
- $C_p = C_v + R \rightarrow R = C_p - C_v = 0.846 - 0.657 = 0.189 \text{ kJ/(kgK)}$
- $R = R_u / M \rightarrow M = R_u / R = 8.314 / 0.189 = 43.99 \text{ kg/kmol}$

Hydrogen

- $R = R_u / M = 8.314 / 2.016 = 4.124 \text{ kJ/(kgK)}$
- $C_p = C_v + R = 10.18 + 4.124 = 14.30 \text{ kJ/(kgK)}$
- $k = C_p / C_v = 14.30 / 10.18 = 1.405$

Nitrogen

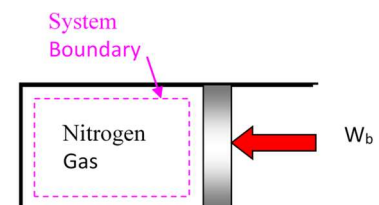
- $R = R_u / M = 8.314 / 28.01 = 0.297 \text{ kJ/(kgK)}$
- $C_p = C_v + R \rightarrow C_v = C_p - R = 1.039 - 0.297 = 0.742 \text{ kJ/(kgK)}$
- $k = C_p / C_v = 1.039 / 0.742 = 1.400$

Oxygen

- $k = C_p / C_v \rightarrow C_v = C_p / k = 0.918 / 1.395 = 0.658 \text{ kJ/(kgK)}$
- $C_p = C_v + R \rightarrow R = C_p - C_v = 0.918 - 0.658 = 0.260 \text{ kJ/(kgK)}$
- $R = R_u / M \rightarrow M = R_u / R = 8.314 / 0.260 = 31.98 \text{ kg/kmol}$

7. Three kilograms of nitrogen gas at 27°C, 0.15 MPa are compressed isothermally to 0.3 MPa in a piston-cylinder device. For nitrogen:  $R = 0.2968 \text{ kJ/(kgK)}$  and the critical temperatures and pressures are  $T_{cr} = 126.2 \text{ K}$ ,  $P_{cr} = 3.39 \text{ MPa}$ .

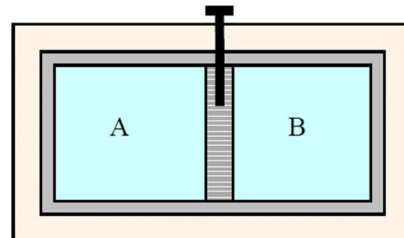
- Show that nitrogen can be expected to behave as an ideal gas during this process.
- Determine the minimum work of compression, in kJ.
- Determine the heat transfer involved in this process?



**Solution:**

- a. Ideal gas is satisfied if  $T > 2xT_{cr}$  OR  $P/P_{cr} \ll 1$ .
- Is temperature greater than  $2 \times T_{cr}$ ?  $T = (27+273.15) \rightarrow 300.15K > 2T_{cr}$ , behaves as ideal gas
  - Is  $P / P_{cr} \ll 1$ ?  $0.15 / 3.39 = 0.0442$ . Yes, behaves as ideal gas
- b. Determine the boundary work
- System: Nitrogen in piston cylinder
  - Boundary work: constant pressure, ideal gas:  $W_b = \int_1^2 P dV = \int_1^2 \frac{mRT}{V} dV$ 
    - $W_b = mRT \ln(V_2/V_1)$
    - $m_1 = m_2 \rightarrow P_1 V_1 / RT_1 = P_2 V_2 / RT_2 \rightarrow P_1 V_1 = P_2 V_2 \rightarrow V_2/V_1 = P_1/P_2$
    - $W_b = mRT \ln(P_1/P_2) = 3kg * 0.2968 \text{ kJ/kgK} * 300.15K * \ln(0.15/0.30)$
    - **$W_b = -184.5 \text{ kJ}$ ; work is into the system**
- c. Determine the heat transfer
- 1<sup>st</sup> Law:  $\Delta U + \Delta KE + \Delta PE = Q_{21} - W_{21} + \Delta E_{mass,21}$
  - Closed, stationary system  $\rightarrow \Delta U = Q_{21} - W_{21}$
  - Ideal gas:  $\Delta U = mC_p(T_2 - T_1)$ ; temperature is constant so  $\Delta U = 0$
  - **$Q_{21} = W_{21} = -184.5 \text{ kJ}$ ; work is into the system, while heat transfer is out of the system**

8. An insulated cylinder is divided into two sections of  $0.5 \text{ m}^3$  each by a piston which is locked by a pin. Side A has air at 300 kPa, 360 K, while side B has air at 1.2 MPa, 1000K. The piston is now unlocked so that it is free to move and it conducts heat so that the air comes to a uniform temperature  $T_A = T_B$ . The piston reaches an equilibrium position. Assume ideal gas with variable specific heats (i.e. use ideal gas AIR TABLES in the BACK of the BOOK (A.7 Borgnakke/Sonntag, or Table A-17 Cengel & Boles) and  $R = 0.287 \text{ kJ/kgK}$ .



- (a) Find the mass in section A and B.
- (b) Determine the work done of the entire system.
- (c) Find the final temperature and pressure
- (d) Determine the piston movement in meters if the cross sectional area of the piston is  $A = 0.25 \text{ m}^2$ .

**Solution:**

- (a)  $P_{1A} = 300 \text{ kPa}$ ,  $T_{1A} = 360 \text{ K}$ ,  $V_{1A} = 0.5 \text{ m}^3$ ;  $P_{1B} = 1200 \text{ kPa}$ ,  $T_{1B} = 1000 \text{ K}$ ;  $V_{1B} = 0.5 \text{ m}^3$
- $PV = mRT$

- $m_A = P_{1A}V_{1A}/(RT_{1A}) = 300 \text{ kPa} * 0.5\text{m}^3 / (0.287 \text{ kJ/kgK} * 360\text{K}) = \underline{1.45 \text{ kg}}$
- $m_B = P_{1B}V_{1B}/(RT_{1B}) = 1200 \text{ kPa} * 0.5\text{m}^3 / (0.287 \text{ kJ/kgK} * 1000\text{K}) = \underline{2.09 \text{ kg}}$

(b) Take the entire system to be section A + B. There is no movement of any of the boundaries with the surroundings. Boundary work = 0. No other forms of work.  
**Work = 0 kJ**

(c) 1st law of thermodynamics:  $\Delta U + \Delta KE + \Delta PE = Q_{21} - W_{21} + \Delta E_{mass,21}$

- System is closed, stationary, and no work. If we also take the system to be A + B, then no heat is transferred to the surroundings (i.e. insulated cylinder). Thus  $\Delta U = 0$ .
- $\Delta U = 0 = \Delta U_A + \Delta U_B = m_A(u_{2A} - u_{1A}) + m_B(u_{2B} - u_{1B}) = 0$
- Further if  $T_{2A} = T_{2B}$ , then  $u_{2A} = u_{2B} = u_2$  because for an ideal gas, internal energy depends on temperature only.
  - $m_A(u_2 - u_{1A}) = m_B(u_{1B} - u_2)$
  - Solving for  $u_2$ :  $u_2 = m_B/(m_A + m_B) u_{1B} + m_A/(m_A + m_B) u_{1A}$
- From tables:
  - State 1A: 360K  $\rightarrow u_{1A} = 257.53 \text{ kJ/kg}$
  - State 1B: 1000K  $\rightarrow u_{1B} = 759.19 \text{ kJ/kg}$
- $u_2 = 2.09 \text{ kg}/(1.45+2.09)\text{kg} * 759.19\text{kJ/kg} + 1.45\text{kg}/(1.45+2.09)\text{kg} * 257.53\text{kJ/kg}$
- $u_2 = 553.59 \text{ kJ/kg}$
- Use the tables to interpolate  $T_2$ .
  - $\frac{T_2 - T_{740K}}{u_2 - u_{740K}} = \frac{T_{760K} - T_{740K}}{u_{760K} - u_{740K}}$ ;  $T_2 = T_{740K} + \frac{u_2 - u_{740K}}{u_{760K} - u_{740K}} (T_{760K} - T_{740K})$
  - $T_2 = 740K + \frac{553.59 - 544.33}{560.32 - 544.33} (760 - 740)K$ ;  **$T_2 = 751.6K$**
- Pressure at state 2
  - If the piston reaches an equilibrium position, then  $P_{2A} = P_{2B}$ . If this was not the case, then the piston would still be moving and not be in equilibrium.
  - Because we do not know the individual volumes, take the entire system at state 2 and solve for  $P_2$ 
    - $P_2 V_{2,A+B} = (m_A + m_B)RT_2$ ;  $P_2 = (m_A + m_B)RT_2 / (V_{1A} + V_{1B})$
    - $P_2 = (1.45 + 2.09)\text{kg} * 0.287\text{kJ/kgK} * 751.6K / 1\text{m}^3$ ;  **$P_2 = 764.1 \text{ kPa}$**

(d) Find volume displaced in section A or B

- $V_{2A} = m_A RT_2 / P_2$ ;  $V_{2A} = 1.45\text{kg} * 0.287\text{kJ/kgK} * 751.6K / 764.1 \text{ kPa} = 0.4098 \text{ m}^3$
- Volume displaced =  $V_{1A} - V_{2A} = 0.5 - 0.4098 = 0.0902\text{m}^3$
- Piston displaced =  $\Delta V_A / A_{\text{piston}} = 0.0902\text{m}^3 / 0.25\text{m}^2$ ; **Distance = 0.36 m**