

MARKS

Solution:

State 1: given: $P_1 = 2000 \text{ kPa}$, $T_1 = 300^\circ\text{C}$, $V_1 = 0.1 \text{ m}^3$

Superheated Steam: $v_1 = 0.12547 \text{ m}^3/\text{kg}$, $u_1 = 2772.56 \text{ kJ/kg}$

Mass: $m = V_1 / v_1 = 0.1 \text{ m}^3 / 0.12547 \text{ m}^3/\text{kg} = 0.797 \text{ kg}$

Process 1-2: heat is removed at constant volume until the piston is at the onset of movement.

State 2: $P_2 = 500 \text{ kPa}$ because piston is at onset of movement (given). Thus, pressure is equal to that of the air supply (i.e. same as the force on the piston)

$V_2 = V_1$ (piston has not yet moved) & $v_2 = v_1$ because the mass has not changed;

$v_2 = v_1 = 0.12547 \text{ m}^3/\text{kg}$

(a) At 500 kPa $v_{f@500\text{kPa}} < v_2 < v_{g@500\text{kPa}}$.

- Thus **state 2 is a saturated liquid vapor mixture** (4 pts)
- Find quality at state 2 and the internal energy at state 2.
 - $x_2 = (v_2 - v_{f@500\text{kPa}}) / v_{fg@500\text{kPa}} = (0.12547 - 0.001093) / 0.3738 \rightarrow x_2 = 0.333$
 - $u_2 = u_{f@500\text{kPa}} + x_2 * u_{fg@500\text{kPa}} = 639.66 + 0.333 * 1921.57 \rightarrow u_2 = 1279.54 \text{ kJ/kg}$
 - $T_2 = T_{\text{sat}@500\text{kPa}} = 151.86^\circ\text{C}$

Process 2-3: Piston is moving and force acting on piston is equivalent to $P_{\text{air}} * A_{\text{piston}}$. Area of piston is constant, so the force is constant for process 2-3

(b) **$P_3 = 500 \text{ kPa}$** (4 pts)

(c) To find boundary work, we need to find the variables at state 3

- State 3: $T_3 = 100^\circ\text{C}$, $P_3 = 500 \text{ kPa} \rightarrow$ compressed liquid
- $v_3 = 0.001043 \text{ m}^3/\text{kg}$; $u_3 = 418.80 \text{ kJ/kg}$
- Final volume: $V_3 = v_3 * m = 0.001043 \text{ m}^3/\text{kg} * 0.797 \text{ kg}$; $V_3 = 0.000831 \text{ m}^3$
- $W_{\text{boundary}} = \int P dV \rightarrow$ constant $P \rightarrow W_{\text{boundary}} = P(V_3 - V_2)$ (2 pts)
- $W_{\text{boundary}} = 500 \text{ kPa} * (0.000831 - 0.1) \text{ m}^3$; **$W_{\text{boundary}} = -49.6 \text{ kJ} = W_{32}$** (2 pts)
- Work is into the system. $W_{\text{IN}} = 49.6 \text{ kJ}$

(d) Apply first law of thermodynamics to find the total heat transfer

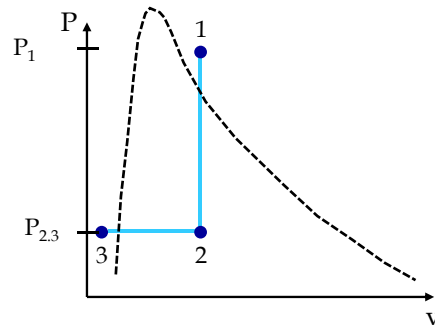
- **Process 1-2:** $m(u_2 - u_1) = Q_{21}$; $Q_{21} = 0.797 \text{ kg}(1279.54 - 2772.56) \frac{\text{kJ}}{\text{kg}} = -1189.94 \text{ kJ}$
- $Q_{21} = -1189.94 \text{ kJ}$ or 1189.94 kJ out of the system (1-2pts)
- **Process 2-3:** $m(u_3 - u_2) = Q_{32} - W_{32}$; ($W_{32} = W_{\text{boundary}}$)
- $Q_{32} = m(u_3 - u_2) + W_{32} = 0.797 \text{ kg}(418.8 - 1279.54) \frac{\text{kJ}}{\text{kg}} + (-49.6 \text{ kJ}) = -735.6 \text{ kJ}$
- $Q_{32} = -735.6 \text{ kJ}$ or 735.6 kJ out of the system (1-2pts)
- **$Q_{\text{total}} = Q_{21} + Q_{32} = (-1189.94 + -735.6 \text{ kJ}) = -1925.55 \text{ kJ}$** (1pts)

(e) State 1 \rightarrow superheated vapor, State 2 \rightarrow saturated mixture ($x_2 = 0.333$), State 3 \rightarrow compressed liquid

Process 1-2: decrease in pressure at constant volume

Process 2-3: decrease in volume at constant pressure

(2 pts for states, 2 points for processes (i.e. correct paths))



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