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A UNIFIED FORMULATION OF THE SEGREGATED CLASS OF ALGORITHMS FOR MULTIFLUID FLOW AT ALL SPEEDS

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The class of segregated pressure-based, single-fluid, all-speed flow algorithms is extended to multifluid flow simulations using a unified, compact, and easy-to-understand notation. Depending on the constraint equation used to derive the pressure-correction equation, the extended multifluid flow algorithms are shown to fall under two categories, denoted in this work as mass conservation-based algorithms (MCBA) and geometric conservation-based algorithms (GCBA). This article deals with the formulation of both types of algorithms and presents several techniques developed to promote and accelerate their convergence. Moreover, the differences and similarities between the two categories are explained and the mass conservation-based formulation is shown to represent a subset of the geometric-based formulation.

INTRODUCTION

Over the past two decades important advances have taken place in computational fluid dynamics (CFD) centered around increasing numerical accuracy through the development of high-resolution schemes [1–14] and improving efficiency through devising better solution algorithms [15–21], better solvers [22, 23], and increasing use of multigrid techniques [24–27]. While high-resolution schemes, solvers, and multigrid techniques can be applied indiscriminately to the simulation of single-fluid or multifluid flows, nearly all developments in solution algorithms have been directed toward the simulation of incompressible, compressible, and more recently all-speed single-fluid flows [28–32]. In this article, a solution algorithm denotes the procedure used to solve the coupling among the velocity, pressure, mass fraction, and density (for compressible flow) fields.

For the solution of single-fluid flow, a number of segregated solution algorithms have been developed [15, 16–18, 20, 33, 34]. Additionally, several techniques

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NOMENCLATURE

$A_p^{(k)}$	coefficients in the discretized equation for $\phi^{(k)}$	t	time
$B_p^{(k)}$	source term in the discretized equation for $\phi^{(k)}$	$T^{(k)}$	temperature of fluid/phase k
$\mathbf{B}^{(k)}$	body force per unit volume of fluid/phase k	$U_f^{(k)}$	interface flux velocity ($\mathbf{v}_f^{(k)} \cdot \mathbf{S}_f$) of fluid/phase k
$C_p^{(k)}$	coefficient equal to $1/R^{(k)}T^{(k)}$	$\mathbf{u}^{(k)}$	velocity vector of fluid/phase k
$\hat{\mathbf{d}}_f$	covariant unit vector (i.e., in the direction of \mathbf{d}_f)	$u^{(k)}, v^{(k)}, \dots$	velocity components of fluid/phase k
$D_p^{(k)}[\phi^{(k)}]$	the D operator	x, y, z	Cartesian coordinates
$\tilde{D}_p^{(k)}[\phi^{(k)}]$	the modified D operator	$\ a, b\ $	the maximum of a and b
$\mathbf{D}_p^{(k)}[\phi^{(k)}]$	the vector form of the D operator	$\beta^{(k)}$	thermal expansion coefficient for phase/fluid k
$\tilde{\mathbf{D}}_p^{(k)}[\phi^{(k)}]$	the vector form of the modified D operator	γ	scaling factor
$g^{(km)}$	drag function [(Eq. (4))]	$\Gamma^{(k)}$	diffusion coefficient of fluid/phase k
$G^{(k)}$	turbulence production rate of fluid/phase k	δt	time step
$H_p[\phi^{(k)}]$	the H operator	$\Delta_p[\phi^{(k)}]$	the Δ operator
$HI_p[\phi^{(k)}]$	the HI operator working on $\phi^{(k)}$ ($\phi^{(k)} = u^{(k)}, v^{(k)}$, or $w^{(k)}$)	ε	turbulence dissipation rate of fluid/phase k
$HP_p[\phi^{(k)}]$	the HP operator working on $\phi^{(k)}$ ($\phi^{(k)} = u^{(k)}, v^{(k)}$, or $w^{(k)}$)	κ_f	space vector equal to $(\hat{\mathbf{n}}_f - \gamma \hat{\mathbf{d}}_f) \mathbf{S}_f$
$HP\tilde{p}[\phi^{(k)}]$	the modified HP operator working on $\phi^{(k)}$ ($\phi^{(k)} = u^{(k)}, v^{(k)}$, or $w^{(k)}$)	$\mu^{(k)}, \mu_t^{(k)}$	laminar and turbulent viscosity of fluid/phase k
$\mathbf{HP}_p[\mathbf{u}^{(k)}]$	the vector form of the HP operator	$\rho^{(k)}$	density of fluid/phase k
$\tilde{\mathbf{HP}}_p[\mathbf{u}^{(k)}]$	the vector form of the modified HP operator	$\phi^{(k)}$	general scalar quantity associated with fluid/phase k
$\mathbf{HI}_p[\mathbf{u}^{(k)}]$	the vector form of the HI operator	$\Phi^{(k)}$	dissipation term in energy equation of fluid/phase k
$\mathbf{I}^{(k)}$	interphase transfer term	Ω	cell volume
$\mathbf{J}_f^{(k)D}$	diffusion flux of $\phi^{(k)}$ across cell face f	Subscripts	
$\mathbf{J}_f^{(k)C}$	convection flux of $\phi^{(k)}$ across cell face f	e, w, ...	refers to the east, west, ... , face of a control volume
$k^{(k)}$	turbulence kinetic energy of fluid/phase k	E, W, ...	refers to the East, West, ... , neighbors of the main grid point
$\dot{M}^{(k)}$	mass source per unit volume	f	refers to control volume face f
\tilde{n}_f	contravariant unit vector (i.e., in the direction of \mathbf{S}_f)	P	refers to the P grid point
P	pressure	Superscripts	
$\text{Pr}^{(k)}, \text{Pr}_t^{(k)}$	laminar and turbulent Prandtl number for fluid/phase k	C	refers to convection contribution
$\dot{q}^{(k)}$	heat generated per unit volume of fluid/phase k	D	refers to diffusion contribution
$Q^{(k)}$	general source term of fluid/phase k	(k)	refers to fluid/phase k
$r^{(k)}$	volume fraction of fluid/phase k	$(k)^*, (k)^{**}, \dots$	refers to first, second, ... , updated value at the current iteration
$R^{(k)}$	gas constant for fluid/phase k	$(k)^o$	refers to values of fluid/phase k from the previous iteration
\mathbf{S}_f	surface vector	$(k)'$	refers to correction field of phase/fluid k
		m	refers to fluid/phase m
		old	refers to values from the previous time step
		SX	refers to SIMPLEX

to improve the performance, facilitate the implementation, and extend the capability of these algorithms have been advertised. The use of the momentum-weighted interpolation method (MWIM) [35–39] and the pressure-weighted interpolation method (PWIM) [40–44] that have enabled the implementation of these algorithms with a collocated variable arrangement is an example of such techniques. Another example is the extension of the segregated pressure-based algorithms to simulating flows at all speeds [31, 32, 45–48].

On the other hand, developments in multifluid solution algorithms have lagged behind that of single-fluid algorithms, partly because of the higher computational cost involved, and partly due to the numerical difficulties that had to be first addressed in the simulation of single-fluid flow. While the main difficulty in simulating single-fluid flow stems from the coupling between the momentum and continuity equations, in multifluid flow this problem is further complicated by the fact that there are as many sets of continuity and momentum equations as there are fluids, that they are all coupled together in various ways (interchange momentum, etc.), and that the fluids share space.

Despite these complexities, successful segregated pressure-based solution algorithms have been devised. These algorithms can be divided into two groups based on the constraint equation used in deriving the pressure equation. Among these algorithms are the inter-phase slip algorithm (IPSA) and its variants devised by the Spalding Group at Imperial College [49–52] and the implicit multi-field algorithms (IMF) developed by the Los Alamos Scientific Laboratory (LASL) group [53–62]. However, in contrast with the widespread information available on single-fluid solution algorithms, much less information is available on multifluid solution algorithms, a fact that has confined their implementation to a small community, slowed their development, and isolated them from the newer developments in single-fluid flow algorithms (PWIM, all speed flows, etc.).

From the above, it is obvious that the segregated class of algorithms and the many techniques developed for single-fluid flow have neither been fully extended nor applied to the simulation of multifluid flow. The main objective of this work is to extend the applicability of segregated single-fluid algorithms to multifluid flow simulations, and to derive these algorithms using a unified, compact, and easy-to-understand notation that can be expanded systematically to yield the coefficients of the pressure-correction equation, thus facilitating the implementation of these algorithms to a wider audience within the CFD community. To this effect, it is shown that all multifluid algorithms can be implemented using a two-step procedure, whereby in the first step a multifluid pressure equation is derived based on either volume conservation [49, 63–65] or mass conservation [50, 63–70]. Then, in the second step, the different segregated single-fluid algorithms are applied to the constraint equation, yielding a multifluid correction equation that drives the global iterations toward convergence in a manner similar to the pressure-correction equation in single-fluid flows.

In what follows, the governing equations for multifluid flows are presented and their discretization outlined so as to lay the ground for the derivation of the pressure or pressure-correction equation. Then, using the unified notation, the different multifluid algorithms are described and the framework for implementing them explained. For compactness, either the mass conservation or the geometric conserva-

tion form of an algorithm will be presented. For the same reason, only the generic forms of the interfacial mass, momentum, and energy transfers are given. Moreover, it should be stressed that the intention of the article is not to compare the relative performance of the different multifluid algorithms—this would be a work in progress; rather, the aim is to unify their formulation.

THE GOVERNING EQUATIONS

In multifluid flow the various components coexist with different concentrations at different locations in the flow domain and move with unequal velocities. Thus, the equations governing multifluid flows are the conservation laws of mass, momentum, and energy for each individual fluid in addition to a set of auxiliary relations. Moreover, for turbulent flows, additional equations to compute the turbulent viscosity or Reynolds stresses are needed. The number of these equations depends on the turbulence model used.

Conservation of Mass

The volume fraction $r^{(k)}$, which is the proportion of volumetric space occupied by the k th fluid ($\Omega^{(k)}/\Omega$) along with the k th fluid density, $\rho^{(k)}$, and velocity, $\mathbf{u}^{(k)}$, in order to satisfy the mass conservation principle, have to obey the differential equation

$$\frac{\partial(r^{(k)}\rho^{(k)})}{\partial t} + \nabla \cdot (r^{(k)}\rho^{(k)}\mathbf{u}^{(k)}) = r^{(k)}\dot{M}^{(k)} \quad (1)$$

Mass sources are often nonzero, as when one fluid is transformed to another fluid. However, summation over all fluids leads to the following “overall mass conservation” equation:

$$\sum_k \left[\frac{\partial(r^{(k)}\rho^{(k)})}{\partial t} + \nabla \cdot (r^{(k)}\rho^{(k)}\mathbf{u}^{(k)}) \right] = 0 \quad (2)$$

The zero on the right-hand side signifies that the sum of mass sources (generation and loss) is zero.

Conservation of Momentum

Denoting the velocity of the k th phase by $\mathbf{u}^{(k)}$, then the momentum equation for the k th phase can be written as

$$\begin{aligned} & \frac{\partial(r^{(k)}\rho^{(k)}\mathbf{u}^{(k)})}{\partial t} + \nabla \cdot (r^{(k)}\rho^{(k)}\mathbf{u}^{(k)}\mathbf{u}^{(k)}) \\ &= \nabla \cdot [r^{(k)}(\mu^{(k)} + \mu_t^{(k)})\nabla\mathbf{u}^{(k)}] + \frac{1}{3}\nabla[(\mu^{(k)} + \mu_t^{(k)})\nabla \cdot \mathbf{u}^{(k)}] + r^{(k)}(-\nabla P + \mathbf{B}^{(k)}) + \mathbf{I}_M^{(k)} \end{aligned} \quad (3)$$

Here P stands for the pressure, which is regarded as being shared by the fluids, $\mathbf{B}^{(k)}$ includes the cross-derivative terms and body forces per unit volume of phase (k) , and $\mathbf{I}_M^{(k)}$ is the momentum transfer to phase (k) resulting from interaction with other phases and can be written in the following form:

$$\mathbf{I}_M^{(k)} = \sum_{m \neq k} g^{(km)} (\mathbf{u}^{(m)} - \mathbf{u}^{(k)}) \quad (4)$$

Conservation of Energy

Let $T^{(k)}$ be the temperature of the k th phase; the energy equation for the k th phase is then given by

$$\begin{aligned} & \frac{\partial (r^{(k)} \rho^{(k)} T^{(k)})}{\partial t} + \nabla \cdot (r^{(k)} \rho^{(k)} \mathbf{u}^{(k)} T^{(k)}) \\ &= \nabla \cdot \left[r^{(k)} \left(\frac{\mu^{(k)}}{\text{Pr}^{(k)}} + \frac{\mu_t^{(k)}}{\text{Pr}_t^{(k)}} \right) \nabla T^{(k)} \right] \\ &+ \frac{r^{(k)}}{c_p^{(k)}} \left\{ \beta^{(k)} T^{(k)} \left[\frac{\partial P}{\partial t} + \nabla \cdot (\mathbf{P} \mathbf{u}^{(k)}) - P \nabla \cdot (\mathbf{u}^{(k)}) \right] + \Phi^{(k)} + \dot{q}^{(k)} \right\} + \frac{\mathbf{I}_t^{(k)}}{c_p^{(k)}} \end{aligned} \quad (5)$$

where $\Phi^{(k)}$ is the viscous dissipation function of the k th phase, $\beta^{(k)}$ is the thermal expansion coefficient of the k th phase which is equal to $1/T^{(k)}$ for an ideal gas, and $\mathbf{I}_t^{(k)}$ is the interfacial energy transfer to phase (k) .

Turbulence Modeling

The effect of turbulence on interfacial mass, momentum, and energy transfer is a difficult modeling task and is an active area of research. Similar to single-fluid flow, researchers have used several models to describe turbulence. These models depend on the flow type and vary in complexity from simple algebraic [71] models to state-of-the-art Reynolds-stress [72] models. However, the widely used multiphase turbulence model, presented next, is the two-equation k - ε model [73] that is based on its single-phase counterpart. Without going into details, the conservation equations governing the turbulence kinetic energy (k) and turbulence dissipation rate (ε) are given by

$$\begin{aligned} & \frac{\partial (r^{(k)} \rho^{(k)} k^{(k)})}{\partial t} + \nabla \cdot (r^{(k)} \rho^{(k)} \mathbf{u}^{(k)} k^{(k)}) \\ &= \nabla \cdot \left(r^{(k)} \frac{\mu_t^{(k)}}{\sigma_k^{(k)}} \nabla k^{(k)} \right) + r^{(k)} (G^{(k)} - \rho^{(k)} \varepsilon^{(k)}) + \mathbf{I}_k^{(k)} \end{aligned} \quad (6)$$

$$\begin{aligned} & \frac{\partial (r^{(k)} \rho^{(k)} \varepsilon^{(k)})}{\partial t} + \nabla \cdot (r^{(k)} \rho^{(k)} \mathbf{u}^{(k)} \varepsilon^{(k)}) \\ &= \nabla \cdot \left(r^{(k)} \frac{\mu_t^{(k)}}{\sigma_\varepsilon^{(k)}} \nabla \varepsilon^{(k)} \right) + r^{(k)} \frac{\varepsilon^{(k)}}{k^{(k)}} (c_{1\varepsilon} G^{(k)} - c_{2\varepsilon} \rho^{(k)} \varepsilon^{(k)}) + \mathbf{I}_\varepsilon^{(k)} \end{aligned} \quad (7)$$

where $\mathbf{I}_k^{(k)}$ and $\mathbf{I}_\varepsilon^{(k)}$ represent the interfacial turbulence terms. The turbulent viscosity is calculated as

$$\mu_t^{(k)} = C_\mu \rho^{(k)} \frac{(k^{(k)})^2}{\varepsilon^{(k)}} \quad (8)$$

The General Multifluid Scalar Equation

A review of the above differential equations reveals that they are similar in structure. If a typical representative variable associated with phase (k) is denoted by $\phi^{(k)}$, the general differential equation may be written as

$$\frac{\partial(r^{(k)} \rho^{(k)} \phi^{(k)})}{\partial t} + \nabla \cdot (r^{(k)} \rho^{(k)} \mathbf{u}^{(k)} \phi^{(k)}) = \nabla \cdot (r^{(k)} \Gamma^{(k)} \nabla \phi^{(k)}) + r^{(k)} Q^{(k)} \quad (9)$$

where the expressions for $\Gamma^{(k)}$ and $Q^{(k)}$ can be deduced from the parent equations.

Auxiliary Relations

The above set of differential equations has to be solved in conjunction with observance of constraints on the values of the variables represented by algebraic relations. These auxiliary relations include the equations of state, the geometric conservation equation, and the interfacial mass, momentum, energy, and turbulence energy transfers.

Physically, the geometric conservation equation is a statement indicating that the sum of volumes occupied by the different fluids within a cell is equal to the volume of the cell containing the fluids:

$$\sum_k r^{(k)} = 1 \quad (10)$$

For a compressible multifluid flow, auxiliary equations of state relating density to pressure and temperature are needed. For the k th phase, such an equation can be written as

$$\rho^{(k)} = \rho^{(k)}(P, T^{(k)}) \quad (11)$$

Several models have been developed for computing the interfacial mass, momentum, energy, and turbulence energy transfers terms [73–76]. For compactness, details regarding these terms are not included here; for more information, the reader is referred to the mentioned references and to many other publications dealing with the subject.

In order to present a complete mathematical problem, thermodynamic relations may be needed and initial and boundary conditions should supplement the above equations.

DISCRETIZATION PROCEDURE

In the previous sections the differential equations governing multifluid flow phenomena were outlined as well as the associated auxiliary relations. The task now is to present the finite-volume-based numerical solution algorithm for solving these equations.

Discretization of the General Conservation Equation

The general conservation Eq. (9) is integrated over a finite volume (Figure 1) to yield the following expression:

$$\begin{aligned} \int_{\Omega} \int \frac{\partial(r^{(k)} \rho^{(k)} \phi^{(k)})}{\partial t} d\Omega + \int_{\Omega} \int \nabla \cdot (r^{(k)} \rho^{(k)} \mathbf{u}^{(k)} \phi^{(k)}) d\Omega \\ = \int_{\Omega} \int \nabla \cdot (r^{(k)} \Gamma^{(k)} \nabla \phi^{(k)}) d\Omega + \int_{\Omega} \int r^{(k)} Q^{(k)} d\Omega \end{aligned} \quad (12)$$

where Ω is the volume of the control cell. Using the divergence theorem to transform the volume integral into a surface integral and then replacing the surface integral by a summation of the fluxes over the sides of the control volume, Eq. (12) is transformed to

$$\frac{\partial(r^{(k)} \rho^{(k)} \phi^{(k)})}{\partial t} \Omega + \sum_{nb=e,w,n,s,t,b} (\mathbf{J}_{nb}^{(k)D} + \mathbf{J}_{nb}^{(k)C}) = r^{(k)} Q^{(k)} \Omega \quad (13)$$

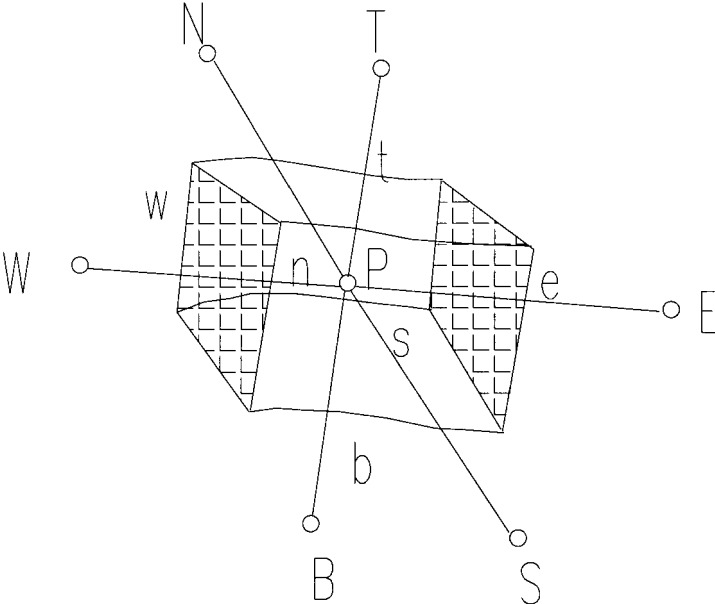


Figure 1. Control volume.

where $\mathbf{J}_{\text{nb}}^{(k)D}$ and $\mathbf{J}_{\text{nb}}^{(k)C}$ are the diffusive and convective fluxes, respectively. The discretized form of the diffusive flux along an east face is given by

$$\mathbf{J}_e^{(k)D} = -r_e^{(k)} \Gamma_e^{(k)} \left[(\phi_E^{(k)} - \phi_P^{(k)}) \frac{\mathbf{S}_e \cdot \mathbf{S}_e}{\mathbf{S}_e \cdot \mathbf{d}_e} + (\overline{\nabla \phi^{(k)}})_e \cdot \kappa_e \right] \quad (14)$$

where the overbar denotes a value obtained by interpolation, κ_e is a space vector defined as

$$\kappa_e = (\hat{\mathbf{n}}_e - (\gamma \hat{\mathbf{d}})_e) \mathbf{S}_e = \kappa_e^x \mathbf{i} + \kappa_e^y \mathbf{j} + \kappa_e^z \mathbf{k} \quad (15)$$

and γ is a scaling factor given by [70],

$$\gamma_e = \frac{1}{\hat{\mathbf{n}}_e \cdot \hat{\mathbf{d}}_e} = \frac{\mathbf{S}_e \cdot \mathbf{d}_e}{\mathbf{S}_e \cdot \mathbf{d}_e} \quad (16)$$

and $\hat{\mathbf{n}}_f$ and $\hat{\mathbf{d}}_f$ are the contravariant and covariant unit vectors, respectively. The discretized convective flux along an east side is given by

$$\mathbf{J}_e^{(k)C} = (r^{(k)} \rho^{(k)} \mathbf{u}^{(k)} \cdot \mathbf{S})_e \phi_e^{(k)} = (r^{(k)} \rho^{(k)} U^{(k)})_e \phi_e^{(k)} = C_e^{(k)} \phi_e^{(k)} \quad (17)$$

where \mathbf{S}_e and C_e are the surface vector and convection flux coefficient at cell face e , respectively. After substituting the face values by their functional relationship relating to the node values of ϕ , Eq. (13) is transformed after some algebraic manipulations into the following discretized equation:

$$A_P^{(k)} \phi_P^{(k)} = \sum_{\text{NB}} A_{\text{NB}}^{(k)} \phi_{\text{NB}}^{(k)} + B_P^{(k)} \quad (18)$$

where the coefficients $A_P^{(k)}$ and $\phi_{\text{NB}}^{(k)}$ depend on the selected scheme and $B_P^{(k)}$ is the source term of the discretized equation. In compact form, the above equation can be written as

$$\phi_P^{(k)} = H_P[\phi^{(k)}] = \frac{\sum_{\text{NB}} A_{\text{NB}}^{(k)} \phi_{\text{NB}}^{(k)} + B_P^{(k)}}{A_P^{(k)}} \quad (19)$$

Discretization of the Momentum Equation

The discretization procedure for the momentum equation yields an algebraic equation of the form

$$\mathbf{A}_P^{(k)} \mathbf{u}_P^{(k)} = \sum_{\text{NB}(P)} \mathbf{A}_{\text{NB}}^{(k)} \mathbf{u}_{\text{NB}}^{(k)} + \mathbf{B}_P^{(k)} - r_P^{(k)} \Omega_P \nabla_P(P) + \Omega_P \sum_{m \neq k} g^{(km)} (\mathbf{u}_P^{(m)} - \mathbf{u}_P^{(k)}) \quad (20)$$

In the above equation, the interphase term is written out explicitly to show the strong coupling among the momentum equations of the different fluids. This is in contrast

with the *spatial* coupling that exists among the neighboring velocities of the same fluid. One way to improve the overall convergence and robustness of the algorithm is to rewrite the discretized momentum equations for the various phases such that

$$\mathbf{A}_p^{(k)} \mathbf{u}_p^{(k)} = \sum_{\text{NB}} \mathbf{A}_{\text{NB}}^{(k)} \mathbf{u}_{\text{NB}}^{(k)} + \mathbf{B}_p^{(k)} - r_p^{(k)} \Omega_p \nabla_p(P) + \Omega_p \sum_{m \neq k} g^{(km)} \mathbf{u}_p^{(m)} \quad (21)$$

where now

$$\mathbf{A}_p^{(k)} = \mathbf{A}_p^{(k)} + \Omega_p \sum_{m \neq k} (g_p^{(km)}) \quad (22)$$

For later reference, the value of $\mathbf{A}_p^{(k)}$ before the addition of the interphase terms will be denoted by $\tilde{\mathbf{A}}_p^{(k)}$. To this end, the discretized form of the momentum equation can be rewritten as

$$\mathbf{u}_p^{(k)} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)}] - r^{(k)} \mathbf{D}_p^{(k)} \nabla_p(P) \quad (23)$$

where the body force and interphase terms are absorbed in the $\mathbf{B}_p^{(k)}$ source term within the $\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)}]$ term, or as

$$\mathbf{u}_p^{(k)} = \mathbf{H}\mathbf{I}_p[\mathbf{u}^{(k)}] + \mathbf{D}_p^{(k)} \sum_{m \neq k} (g^{(km)} \mathbf{u}_p^{(m)}) \quad (24)$$

where the body force and pressure gradient terms are absorbed in the $\mathbf{B}_p^{(k)}$ source term within the $\mathbf{H}\mathbf{I}_p[\mathbf{u}^{(k)}]$ term. For later use, modified forms of the $\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)}]$ and $\mathbf{D}_p^{(k)}$ operators are defined as

$$\widetilde{\mathbf{H}\mathbf{P}}_p[\mathbf{u}^{(k)}] = \frac{\sum_{\text{NB}} \mathbf{A}_{\text{NB}}^{(k),u} \mathbf{u}_{\text{NB}}^{(k)}}{\mathbf{A}_p^{(k),u}} \quad \tilde{\mathbf{D}}_p^{(k)} = \frac{\mathbf{D}_p^{(k)}[\mathbf{u}]}{1 - \widetilde{\mathbf{H}\mathbf{P}}_p[1]} \quad (25)$$

Discretization of the Continuity Equation

The mass conservation principle (Eq. (1)) can be viewed as a volume-fraction equation for the k th phase, in which case it can be discretized and written in the form

$$r_p^{(k)} = H_p[r^{(k)}] \quad (26)$$

or as a continuity equation for the k th phase to be used in deriving the pressure-correction equation, in which case it is discretized in the following form:

$$\frac{(r_p^{(k)} \rho_p^{(k)}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega - \Delta_p[r^{(k)} \mathbf{u}^{(k)} \cdot \mathbf{S}] = r^{(k)} \dot{M}^{(k)} \quad (27)$$

where the Δ operator represents the operation

$$\Delta_p[\Theta] = \sum_{f=\text{NB}(P)} \Theta_f \quad (28)$$

Discretization of the Energy Equation

The discretization of the energy equation follows that of the general multifluid scalar equation. The only difference is the one pertaining to the discretization of the additional source terms. Since a control-volume approach is followed, the integral of these sources over the control volume appears in the discretized equation. By using the divergence theorem, the volume integral is transformed into a surface integral and the resultant discretized expressions are evaluated explicitly.

MULTIFLUID SOLUTION ALGORITHMS

Before detailing the multifluid segregated solution algorithms, it will be shown that these algorithms may be grouped in two categories, denoted in this work as the *geometric conservation-based algorithms* and the *mass conservation-based algorithms*. To justify this classification, attention is focused on the equations and variables involved in a multifluid flow situation with n fluids. In such a case, there will be n momentum equations, n volume fraction (or mass conservation) equations, a geometric conservation equation, and, for the case of a compressible flow, an additional n auxiliary pressure–density relations. Moreover, the variables involved are the n velocity vectors, the n volume fractions, the pressure field, and for a compressible flow an additional n unknown density fields. It is clear that the n velocity fields are associated with the n momentum equations; i.e., the momentum equations can be used directly to calculate the velocity fields. The volume fractions could arguably be calculated from the volume-fraction equations, which means that the remaining equation, i.e., the geometric conservation equation (the volume fractions sum to 1), has to be used in deriving the pressure equation or, equivalently, the pressure-correction equation. This results in what is called here the *geometric conservation-based algorithm (GCBA)*.

The equations can be arranged differently, with the n momentum equations used to calculate the n velocity fields, $n - 1$ volume-fraction (mass conservation) equations used to calculate $n - 1$ volume-fraction fields, and the last volume-fraction field calculated using the geometric conservation equation

$$r^{(n)} = 1 - \sum_{k \neq n} r^{(k)} \quad (29)$$

The remaining volume-fraction equation can be used to calculate the pressure field. However, instead of using this last volume-fraction equation, the global conservation equation can be employed, i.e., the sum of the individual mass conservation equations, to derive a pressure-correction equation. The resulting algorithm is denoted in this case as the *mass conservation-based algorithm (MCBA)*.

With this classification, attention will now be directed toward presenting the various MCBA and GCBA in addition to several techniques that were introduced to enhance the performance and accelerate the convergence of these algorithms.

PART I: MASS CONSERVATION-BASED ALGORITHMS

The sequence of events in the mass conservation-based algorithm is as follows:

1. Solve the momentum equations for velocities.
2. Solve the pressure-correction equation based on global mass conservation.

3. Correct velocities, densities, and pressure.
4. Solve the individual mass conservation equations for volume fractions.
5. Solve the energy equations.
6. Return to the first step and repeat until convergence.

The above steps, along with some of the techniques that were developed to improve on them, are detailed next.

Solving for Velocities

In this first step, the following systems of momentum equations are solved to find $\mathbf{u}_p^{(k)*}$ based on guessed or previously calculated volume-fraction and pressure fields:

$$\mathbf{u}_p^{(k)} = \mathbf{H}_p[\mathbf{u}^{(k)}] + \mathbf{D}_p^{(k)} \sum_{m \neq k} g^{(km)} \mathbf{u}_p^{(m)} \quad (30)$$

From Eq. (30) it is clear that the $\mathbf{H}_p[\mathbf{u}^{(k)}]$ term couples $\mathbf{u}_p^{(k)}$ to the neighboring phase (k) velocities (*geometric or spatial coupling*), while the $\mathbf{D}_p^{(k)} \sum_{m \neq k} g^{(km)} \mathbf{u}_p^{(m)}$ term couples $\mathbf{u}_p^{(k)}$ to the velocity of all other phases at grid point P (*interphase coupling*). Therefore, the rate of convergence of the iterative solution procedure used to solve the above system will depend greatly on its ability to resolve both types of coupling. The spatial coupling presents no problem to the well-established iterative techniques, since it couples velocities of the same phase. The interphase coupling is problematic, however, since it relates velocities of different phases. An explicit evaluation of this term slows the convergence rate considerably, especially when the interfluid momentum transfer terms, represented by $g^{(mm)}$, are large. To accelerate convergence, the partial elimination algorithm (PEA) [68] and the simultaneous solution of nonlinearly coupled equations (SINCE) [67] technique were developed.

Improvement 1: The partial elimination algorithm and the SINCE. The central idea in the partial elimination algorithm, applicable to two-fluid flow, is to render the discretized momentum equations more implicit by decoupling the two sets of equations. This is achieved in a straightforward manner and results in a modification to the values of $\mathbf{A}_p^{(k)}$ and $\mathbf{B}_p^{(k)}$.

For the case of two-fluid flow, the momentum equations are given by

$$\mathbf{u}_p^{(1)} = \mathbf{H}_p[\mathbf{u}^{(1)}] + \mathbf{D}_p^{(1)} g^{(12)} \mathbf{u}_p^{(2)} \quad \mathbf{u}_p^{(2)} = \mathbf{H}_p[\mathbf{u}^{(2)}] + \mathbf{D}_p^{(2)} g^{(21)} \mathbf{u}_p^{(1)} \quad (31)$$

It is clear that each of the Eqs. (31) contains both variables $\mathbf{u}_p^{(1)}$ and $\mathbf{u}_p^{(2)}$ simultaneously. In order to eliminate the velocity of one of the phases from the other phase momentum equation, and vice versa, these equations may be rewritten using the PEA as

$$\mathbf{u}_p^{(1)} = \frac{\mathbf{H}_p[\mathbf{u}^{(1)}] + \mathbf{D}_p^{(1)} g^{(12)} \mathbf{H}_p[\mathbf{u}^{(2)}]}{1 - \mathbf{D}_p^{(1)} g^{(12)} \mathbf{D}_p^{(2)} g^{(21)}} \quad \mathbf{u}_p^{(2)} = \frac{\mathbf{H}_p[\mathbf{u}^{(2)}] + \mathbf{D}_p^{(2)} g^{(21)} \mathbf{H}_p[\mathbf{u}^{(1)}]}{1 - \mathbf{D}_p^{(1)} g^{(12)} \mathbf{D}_p^{(2)} g^{(21)}} \quad (32)$$

This treatment renders the equations more implicit ($\mathbf{u}_p^{(2)}$ is absent from the $\mathbf{u}_p^{(1)}$ equation and vice versa) and enhances the rate of convergence, which otherwise would have been slowed down by the lagging interlinkage of the two equations.

The use of the PEA technique with more than two fluids can become cumbersome. The simultaneous solution of nonlinearly coupled equations (SINCE) method [67] is a technique similar to the PEA in its aim, applicable to three or more phases. It is different from the PEA, however, in that the equations' spatial coupling and interphase coupling are accounted for in two distinct steps. In the first step, the interphase coupling is resolved by solving the momentum equations on each grid point without accounting for the spatial coupling, i.e., by moving the $\mathbf{H}\mathbf{I}_p[\mathbf{u}^{(k)}]$ terms to the right-hand side and treating them as source terms. The system of equations for a k -fluid flow can be rearranged and written in the following form:

$$\begin{aligned}\check{\mathbf{u}}_p^{(1)} &= \mathbf{D}_p^{(1)} \sum_{m \neq 1} g^{(1m)} \check{\mathbf{u}}_p^{(m)} + \mathbf{H}\mathbf{I}_p[\check{\mathbf{u}}^{(1)}] & \check{\mathbf{u}}_p^{(2)} &= \mathbf{D}_p^{(2)} \sum_{m \neq 2} g^{(2m)} \check{\mathbf{u}}_p^{(m)} + \mathbf{H}\mathbf{I}_p[\mathbf{u}^{(2)}] \\ \check{\mathbf{u}}_p^{(k)} &= \mathbf{D}_p^{(k)} \sum_{m \neq k} g^{(km)} \check{\mathbf{u}}_p^{(m)} + \mathbf{H}\mathbf{I}_p[\mathbf{u}^{(k)}]\end{aligned}\quad (33)$$

These equations are solved in a first step for the respective control volumes, and the solution used as a first estimate of the velocity fields ($\check{\mathbf{u}}_p^{(k)}$) in calculating the interphase terms. In the second step, the interphase friction terms are absorbed into the standard source terms of Eq. (18) and the full-field solution of the momentum equations is accomplished in a sequential manner using the normal calculation method via the following system of equations:

$$\mathbf{u}_p^{(k)*} = \mathbf{H}\mathbf{I}_p[\mathbf{u}^{(k)*}] + \mathbf{D}_p^{(k)} \sum_{m \neq k} g^{(km)} \check{\mathbf{u}}_p^{(m)} \quad (34)$$

Solving for Pressure Correction

Before convergence, the velocities calculated from the momentum equations do not satisfy the mass conservation equations. In the segregated approach, the burden of restoring balance rests on the pressure-correction equation, which in this case is derived from the overall mass conservation equation. The segregated MCBA can be viewed as extensions to the SIMPLE algorithm and its variants, in which, the pressure-correction equation derivation follows the same pattern as in SIMPLE (or any of its variants), and the corrections are applied only to the velocity, pressure, and density fields. No correction is applied to the volume fractions; rather, they are obtained by solving the individual continuity and geometric constraint equations.

To derive the pressure-correction equation, the mass conservation equations of the various phases are added to yield the overall mass conservation equation given by

$$\sum_k \left\{ \frac{(r_p^{(k)} \rho_p^{(k)}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p (r^{(k)} \rho_p^{(k)} \mathbf{u}^{(k)} \cdot \mathbf{S}) \right\} = \sum_k r^{(k)} \dot{M}^{(k)} = 0 \quad (35)$$

In the predictor stage a guessed or estimated pressure field from the previous iteration, denoted by P^o , is substituted into the momentum equations. The resulting

velocity fields, denoted by $\mathbf{u}^{(k)*}$, which now satisfy the momentum equations, will not, in general, satisfy the mass conservation equations. Thus, corrections are needed in order to yield velocity and pressure fields that satisfy both equations. Denoting the corrections for pressure, velocity, and density by P' , $\mathbf{u}^{(k)'}$, and $\rho^{(k)'}$, respectively, the corrected fields are written as

$$P = P^o + P' \quad \mathbf{u}^{(k)} = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'} \quad \rho^{(k)} = \rho^{(k)o} + \rho^{(k)'} \quad (36)$$

Thus, before the pressure field is known, the velocities obtained from the momentum equations are actually $\mathbf{u}^{(k)*}$ rather than $\mathbf{u}^{(k)}$. Hence the equations solved in the predictor stage are

$$\mathbf{u}_p^{(k)*} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)*}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (37)$$

while the final solutions satisfy

$$\mathbf{u}_p^{(k)} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P \quad (38)$$

Subtracting the two sets of Eqs. (38) and (37) from each other yields the following equation involving the correction terms:

$$\mathbf{u}_p^{(k)'} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \quad (39)$$

The velocity and density fields are corrected to satisfy mass conservation. Therefore, the new density and velocity fields, $\rho^{(k)}$ and $\mathbf{u}^{(k)}$, will satisfy the overall mass conservation equation if

$$\sum_k \left\{ \frac{(r_p^{(k)o} \rho_p^{(k)}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)} \mathbf{u}^{(k)} \cdot \mathbf{S}] \right\} = 0 \quad (40)$$

Linearizing the $(\rho^{(k)} \mathbf{u}^{(k)})$ term, one gets

$$(\rho^{(k)*} + \rho^{(k)'}) (\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}) = \rho^{(k)*} \mathbf{u}^{(k)*} + \rho^{(k)*} \mathbf{u}^{(k)'} + \rho^{(k)'} \mathbf{u}^{(k)*} + \rho^{(k)'} \mathbf{u}^{(k)'} \quad (41)$$

Substituting Eqs. (41) and (39) into Eq. (40), rearranging, and replacing density correction by pressure correction, the final form of the pressure-correction equation is written as

$$\begin{aligned} & \sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P'_p + \Delta_p [r^{(k)o} \mathbf{U}^{(k)*} C_p^{(k)} P'] - \Delta_p [r^{(k)o} \rho^{(k)*} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\} \\ & = - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)*} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)*} \mathbf{U}^{(k)*}] \right. \\ & \quad \left. + \Delta_p [r^{(k)o} \rho^{(k)*} (\mathbf{H}\mathbf{P}[\mathbf{u}^{(k)'}]) \cdot \mathbf{S}] + \Delta_p [r^{(k)o} \rho^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \right\} \quad (42) \end{aligned}$$

The second-order correction term $\rho^{(k)'} \mathbf{u}^{(k)'}$ is usually neglected. Moreover, if the $\mathbf{HP}[\mathbf{u}^{(k)'}]$ term in the above equation is retained, there will result a pressure-correction equation relating the pressure-correction value at a point to all values in the domain. To facilitate implementation and reduce cost, simplifying assumptions related to this term have been introduced. Depending on these assumptions, different algorithms are obtained. These algorithms were originally developed for incompressible single-fluid flow and most of them have not yet been extended to compressible multifluid flow. It is an objective of this work to perform this extension.

Extending the segregated class of single-fluid flow algorithms to multi-fluid flow situations. Moukalled and Darwish [21] have recently unified the formulation of the segregated class of algorithms for single-fluid flow and detailed the philosophies behind them. Therefore, it is sufficient here to present the symbolic form of the multifluid version of these algorithms. For additional discussion related to their development, the reader is referred to [21].

In the derivations to follow, the superscripts “old” and “o” denote values from the previous time step and previous iteration, respectively. Moreover, the superscripts *, **, ***, and **** represent the first, second, third, and fourth updated values at the current iteration, respectively.

The MCBA following SIMPLE (MCBA-SIMPLE): Symbolic form.

Predictor:

$$\mathbf{u}_p^{(k)*} = \mathbf{HP}_p[\mathbf{u}^{(k)*}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (43)$$

Corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}) (\mathbf{u}^{(k)**} = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}, P^* = P^o + P', \rho^{(k)*} = \rho^{(k)o} + \rho^{(k)'}) \quad (44)$$

$$\mathbf{u}_p^{(k)**} = \mathbf{HP}_p[\mathbf{u}^{(k)**}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P^* = \mathbf{HP}_p[\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p (P^o + P') \quad (45)$$

$$\therefore \begin{cases} \mathbf{u}_p^{(k)'} = \mathbf{HP}_p[\mathbf{u}^{(k)'}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_p^{(k)} P' \end{cases} \quad (46)$$

Condition:

$$\begin{aligned} & \sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P'_p + \Delta_p [r^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p [r^{(k)o} \rho^{(k)o} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\} \\ & = - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)o} U^{(k)*}] \right. \\ & \quad \left. + \Delta_p [r^{(k)o} \rho^{(k)o} \mathbf{HP}[\mathbf{u}^{(k)'}] \cdot \mathbf{S}] + \Delta_p [r^{(k)o} \rho^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \right\} \quad (47) \end{aligned}$$

Approximation:

Neglect:

$$\mathbf{HP}[\mathbf{u}^{(k)'}], \quad \Delta_p[r^{(k)o} \rho^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \Rightarrow \mathbf{u}_p^{(k)'} = -r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \quad (48)$$

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P_p' + \Delta_p[r^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p[r^{(k)o} \rho^{(k)o} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\} \\ &= - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p[r^{(k)o} \rho^{(k)o} U^{(k)*}] \right\} \quad (49) \end{aligned}$$

A global MCBA-SIMPLE iteration

1. Solve implicitly for $\mathbf{u}^{(k)}$, using the old pressure and density fields.
2. Calculate the $\mathbf{D}^{(k)}$ -fields.
3. Solve the pressure-correction equation and correct $\mathbf{u}^{(k)}$, P , and $\rho^{(k)}$.
4. Solve implicitly for $r^{(k)}$.
5. Solve implicitly the energy equations and update the density fields.
6. Return to the first step and iterate until convergence.

The MCBA following SIMPLEST (MCBA-SIMPLEST): Symbolic form.

Predictor:

$$\mathbf{u}_p^{(k)*} = \mathbf{HP}_p^D[\mathbf{u}^{(k)*}] + \mathbf{HP}_p^C[\mathbf{u}^{(k)o}] - r^{(k)o} \mathbf{D}_p^{(k)*} \nabla_p P^o \quad (50)$$

Corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}) (\mathbf{u}^{(k)**} = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}, P^* = P^o + P', \rho^{(k)*} = \rho^{(k)o} + \rho^{(k)'}) \quad (51)$$

$$\begin{aligned} \therefore \mathbf{u}_p^{(k)**} &= \mathbf{HP}_p^D[\mathbf{u}^{(k)*}] + \mathbf{HP}_p^D[\mathbf{u}^{(k)'}] + \mathbf{HP}_p^C[\mathbf{u}^{(k)*}] + \mathbf{HP}_p^C[\mathbf{u}^{(k)'}] \\ &\quad - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P^o - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \quad (52) \end{aligned}$$

$$\therefore \begin{cases} \mathbf{u}_p^{(k)'} = \mathbf{HP}_p[\mathbf{u}^{(k)'}] + \mathbf{HP}_p^C[\mathbf{u}^{(k)*} - \mathbf{u}^{(k)o}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_p^{(k)} P' \end{cases} \quad (53)$$

Condition:

$$\sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P'_p + \Delta_p [r^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p [r^{(k)o} \rho^{(k)o} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\}$$

$$= - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)o} U^{(k)*}] \right. \\ \left. + \Delta_p [r^{(k)o} \rho^{(k)o} (\mathbf{H} \mathbf{P}^C [\mathbf{u}^{(k)*} - \mathbf{u}^{(k)o}] + \mathbf{H} \mathbf{P} [\mathbf{u}^{(k)'}]) \cdot \mathbf{S}] \right. \\ \left. + \Delta_p [r^{(k)o} \rho^{(k)o} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \right\} \quad (54)$$

Approximation:

Neglect:

$$\mathbf{H} \mathbf{P}^C [\mathbf{u}^{(k)*} - \mathbf{u}^{(k)o}], \mathbf{H} \mathbf{P} [\mathbf{u}^{(k)'}], \Delta_p [r^{(k)o} \rho^{(k)o} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \Rightarrow \mathbf{u}_p^{(k)'} = -r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \quad (55)$$

Approximate equation:

$$\sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P'_p + \Delta_p [r^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p [r^{(k)o} \rho^{(k)o} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\}$$

$$= - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)o} U^{(k)*}] \right\} \quad (56)$$

A global MCBA-SIMPLEST iteration

1. Solve for $\mathbf{u}^{(k)}$, treating $\mathbf{H} \mathbf{P}^D [\mathbf{u}^{(k)}]$ implicitly and $\mathbf{H} \mathbf{P}^C [\mathbf{u}^{(k)}]$ explicitly.
2. Calculate the $\mathbf{D}^{(k)}$ fields.
3. Solve the pressure-correction equation and correct $\mathbf{u}^{(k)}$, P , and $\rho^{(k)}$.
4. Solve implicitly for $r^{(k)}$.
5. Solve implicitly the energy equations and update the density fields.
6. Return to the first step and iterate until convergence.

The MCBA following PISO (MCBA-PISO): Symbolic form.

First predictor:

$$\mathbf{u}_p^{(k)*} = \mathbf{H} \mathbf{P}_p [\mathbf{u}^{(k)*}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (57)$$

First corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}) (\mathbf{u}^{(k)**}) = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}, P^* = P^o + P', \rho^{(k)*} = \rho^{(k)o} + \rho^{(k)'} \quad (58)$$

$$\therefore \mathbf{u}_p^{(k)**} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)**}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P^* = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p (P^o + P')$$
(59)

$$\therefore \begin{cases} \mathbf{u}_p^{(k)'} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'}] - r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_p^{(k)} P' \end{cases}$$
(60)

Condition:

$$\begin{aligned} & \sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P_p + \Delta_p [r^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p [r^{(k)o} \rho^{(k)o} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\} \\ &= - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)o} U^{(k)*}] \right. \\ & \quad \left. + \Delta_p [r^{(k)o} \rho^{(k)o} (\mathbf{H}\mathbf{P}[\mathbf{u}^{(k)'}]) \cdot \mathbf{S}] + \Delta_p [r^{(k)o} \rho^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \right\} \end{aligned}$$
(61)

Approximation:

Neglect:

$$\mathbf{H}\mathbf{P}[\mathbf{u}^{(k)'}], \Delta_p [r^{(k)o} \rho^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \Rightarrow \mathbf{u}_p^{(k)'} = -r^{(k)o} \mathbf{D}_p^{(k)} \nabla_p \mathbf{P}'$$
(62)

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P'_p + \Delta_p [r^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p [r^{(k)o} \rho^{(k)o} (r^{(k)o} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\} \\ &= - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)o} \rho^{(k)o} U^{(k)*}] \right\} \end{aligned}$$
(63)

Second corrector:

$$(\mathbf{u}^{(k)''}, \mathbf{P}'', \rho^{(k)''}) (\mathbf{u}^{(k)****} = \mathbf{u}^{(k)***} + \mathbf{u}^{(k)''}, \mathbf{P}^{**} = \mathbf{P}^* + \mathbf{P}'', \rho^{(k)**} = \rho^{(k)*} + \rho^{(k)'}) \quad (64)$$

$$\therefore \mathbf{u}_p^{(k)****} = \mathbf{H}\mathbf{P}_p^{**}[\mathbf{u}^{(k)****}] - r^{(k)o} \mathbf{D}_p^{(k)**} \nabla_p (\mathbf{P}^* + \mathbf{P}'') \quad (65)$$

$$\mathbf{u}_p^{(k)***} = \mathbf{H}\mathbf{P}_p^{**}[\mathbf{u}^{(k)**}] - r^{(k)o} \mathbf{D}_p^{(k)**} \nabla_p \mathbf{P}^* \quad (66)$$

$$\therefore \begin{cases} \mathbf{u}_p^{(k)''} = \mathbf{H}\mathbf{P}_p^{**}[\mathbf{u}^{(k)***} - \mathbf{u}^{(k)**} + \mathbf{u}^{(k)''}] - r^{(k)o} \mathbf{D}_p^{(k)**} \nabla_p \mathbf{P}'' \\ \rho^{(k)''} = C_p^{(k)} \mathbf{P}'' \end{cases} \quad (67)$$

Condition:

$$\sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)^\circ} C_p^{(k)} P_p'' + \Delta_p [r^{(k)^\circ} C_p^{(k)} U^{(k)***} P'' - \Delta_p [r^{(k)^\circ} \rho^{(k)*} (r^{(k)^\circ} \mathbf{D}^{(k)**} \nabla P'') \cdot \mathbf{S}]] \right\} \\ = - \sum_k \left\{ \frac{r_p^{(k)^\circ} \rho_p^{(k)*} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)^\circ} \rho^{(k)*} U^{(k)***}] \right. \\ \left. + \Delta_p [r^{(k)^\circ} \rho^{(k)*} (\mathbf{HP}^{**} [\mathbf{u}^{(k)***} - \mathbf{u}^{(k)**} + \mathbf{u}^{(k)''}] \cdot \mathbf{S}) + \Delta_p [r^{(k)^\circ} \rho^{(k)*} \mathbf{u}^{(k)''} \cdot \mathbf{S}] \right\} \quad (68)$$

Approximation:

Neglect:

$$\mathbf{HP}^{**} [\mathbf{u}^{(k)***} - \mathbf{u}^{(k)**} + \mathbf{u}^{(k)''}], \Delta_p [r^{(k)^\circ} \rho^{(k)*} \mathbf{u}^{(k)''} \cdot \mathbf{S}] \Rightarrow \mathbf{u}_p^{(k)''} = -r^{(k)^\circ} \mathbf{D}_p^{(k)**} \nabla_p P'' \quad (69)$$

Approximate equation:

$$\sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)^\circ} C_p^{(k)} P_p'' + \Delta_p [r^{(k)^\circ} C_p^{(k)} U^{(k)***} P'' - \Delta_p [r^{(k)^\circ} \rho^{(k)*} (r^{(k)^\circ} \mathbf{D}^{(k)**} \nabla P'') \cdot \mathbf{S}]] \right\} \\ = - \sum_k \left\{ \frac{r_p^{(k)^\circ} \rho_p^{(k)*} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)^\circ} \rho^{(k)*} U^{(k)***}] \right\} \quad (70)$$

A global MCBA-PISO iteration

1. Solve implicitly for $\mathbf{u}^{(k)}$ using the old pressure and density fields.
2. Calculate the $\mathbf{D}^{(k)}$ fields.
3. Solve the pressure-correction equation and correct $\mathbf{u}^{(k)}$, P , and $\rho^{(k)}$.
4. Solve implicitly for $r^{(k)}$.
5. Solve implicitly the energy equation and update the density fields.
6. Solve the momentum equations explicitly and calculate the $\mathbf{D}^{(k)}$ fields.
7. Solve the pressure-correction equation and correct $\mathbf{u}^{(k)}$, P , and $\rho^{(k)}$.
8. Return to step 1 and iterate until convergence.

The MCBA following SIMPLEX (MCBA-SIMPLEX): Symbolic form.

Predictor:

$$\mathbf{u}_p^{(k)*} = \mathbf{HP}_p [\mathbf{u}^{(k)*}] - r^{(k)^\circ} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (71)$$

Corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}) (\mathbf{u}^{(k)**} = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}, P^* = P^o + P', \rho^{(k)*} = \rho^{(k)^\circ} + \rho^{(k)'}) \quad (72)$$

$$\therefore \mathbf{u}_p^{(k)**} = \mathbf{HP}_p [\mathbf{u}^{(k)**}] - r^{(k)^\circ} \mathbf{D}_p^{(k)} \nabla_p P^* = \mathbf{HP}_p [\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}] - r^{(k)^\circ} \mathbf{D}_p^{(k)} \nabla_p (P^o + P') \quad (73)$$

$$\therefore \begin{cases} \mathbf{u}_p^{(k)'} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)}] - r_p^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho_p^{(k)'} = C_p^{(k)} P' \end{cases} \quad (74)$$

Condition:

$$\begin{aligned} & \sum_k \left\{ \frac{r_p^{(k)o} (\rho_p^{(k)o} + \rho_p^{(k)'}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega \right. \\ & \quad \left. + \Delta_p [r_p^{(k)o} \rho_p^{(k)'} \mathbf{u}^{(k)*} \cdot \mathbf{S}] + \Delta_p [r_p^{(k)o} \rho_p^{(k)o} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \right\} \\ & = - \sum_k \{ \Delta_p [r_p^{(k)o} \rho_p^{(k)o} \mathbf{u}^{(k)*} \cdot \mathbf{S}] + \Delta_p [r_p^{(k)o} \rho_p^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}] \} \end{aligned} \quad (75)$$

Approximation:

Neglect $\Delta_p [r_p^{(k)o} \rho_p^{(k)'} \mathbf{u}^{(k)'} \cdot \mathbf{S}]$ and let

$$\mathbf{u}_p^{(k)'} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)}] - r_p^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' = -r_p^{(k)o} \mathbf{D}_p^{(k)\text{SX}} \nabla_p P' \quad (76)$$

$$\Rightarrow -r_p^{(k)o} \mathbf{D}_p^{(k)\text{SX}} \nabla_p P' = \mathbf{H}\mathbf{P}_p[-r_p^{(k)o} \mathbf{D}^{(k)\text{SX}} \nabla_p P'] - r_p^{(k)o} \mathbf{D}_p^{(k)} \nabla_p P' \quad (77)$$

Assume that the pressure difference local to the velocity is representative of all pressure differences, i.e., $\mathbf{H}\mathbf{P}_p[-r_p^{(k)o} \mathbf{D}^{(k)\text{SX}} \nabla_p P'] = -(\nabla_p P') \mathbf{H}\mathbf{P}_p[r_p^{(k)o} \mathbf{D}^{(k)\text{SX}}]$, thus

$$r_p^{(k)o} \mathbf{D}_p^{(k)\text{SX}} = \mathbf{H}\mathbf{P}_p[r_p^{(k)o} \mathbf{D}^{(k)\text{SX}}] + r_p^{(k)o} \mathbf{D}_p^{(k)} \quad (78)$$

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)o} C_p^{(k)} P'_p + \Delta_p [r_p^{(k)o} C_p^{(k)} U^{(k)*} P'] - \Delta_p [r_p^{(k)o} \rho_p^{(k)o} (r_p^{(k)o} \mathbf{D}^{(k)\text{SX}} \nabla_p P') \cdot \mathbf{S}] \right\} \\ & = - \sum_k \left\{ \frac{r_p^{(k)o} \rho_p^{(k)o} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r_p^{(k)o} \rho_p^{(k)o} U^{(k)*}] \right\} \end{aligned} \quad (79)$$

A global MCBA-SIMPLEX iteration

1. Solve implicitly for $\mathbf{u}^{(k)}$, using the old pressure and density fields.
2. Calculate the $\mathbf{D}^{(k)}$ fields.
3. Solve implicitly for the $\mathbf{D}^{(k)\text{SX}}$ fields.
4. Solve the pressure-correction equation using these $\mathbf{D}^{(k)\text{SX}}$ fields.
5. Correct $\mathbf{u}^{(k)}$, P , and $\rho^{(k)}$.
6. Solve implicitly for $r^{(k)}$.
7. Solve implicitly the energy equations and update the density fields.
8. Return to the first step and iterate until convergence.

The expanded form of the pressure-correction equation. It is obvious by now that the various simplified pressure-correction equations are similar and may be written as

$$\sum_k \left\{ \frac{\Omega}{\delta t} r_p^{(k)^\circ} C_p^{(k)} P'_p + \Delta_p [r^{(k)^\circ} C_p^{(k)} U^{(k)} P'] - \Delta_p [r^{(k)^\circ} \rho^{(k)} (r^{(k)^\circ} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right\} \\ = - \sum_k \left\{ \frac{r_p^{(k)^\circ} \rho_p^{(k)} - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega + \Delta_p [r^{(k)^\circ} \rho^{(k)} U^{(k)}] \right\} \quad (80)$$

where, depending on the algorithm used, $U^{(k)}$ and $\rho^{(k)}$ represent values from the previous iteration or from a previous corrector step. The second term on the left-hand side is similar to a convection term and may be discretized using any convective scheme (the upwind scheme is employed here). The term $\Delta_p [r^{(k)^\circ} \rho^{(k)} (r^{(k)^\circ} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}]$ is discretized following the same procedure used in discretizing the diffusion flux. Substituting the various terms in Eq. (80) by their equivalent expressions and, neglecting the nonorthogonal terms, the final form of the pressure-correction equation is written as

$$A_p^{P'} P'_p = A_E^{P'} P'_E + A_W^{P'} P'_W + A_N^{P'} P'_N + A_S^{P'} P'_S + A_T^{P'} P'_T + A_B^{P'} P'_B + B_p^{P'} \quad (81)$$

where

$$A_F^{P'} = \sum_k (\Gamma_f^{(k)} + (r^{(k)^\circ} C_p^{(k)})_f \| - U_f^{(k)}, 0 \|) \quad (82)$$

$$A_p^{P'} = \sum_{\text{NB}} A_F^{P'} + \sum_k \left(\frac{(r^{(k)^\circ} C_p^{(k)})_p \Omega_p}{\delta t} + \sum_{\text{nb}} (r^{(k)^\circ} C_p^{(k)})_f U_f^{(k)} \right) \quad (83)$$

$$B_p^{P'} = - \sum_k \left\{ \frac{(r_p^{(k)^\circ} \rho_p^{(k)} - r_p^{(k)\text{old}} \rho_p^{(k)\text{old}})}{\delta t} \Omega_p + \sum_{\text{nb}} r_f^{(k)} \rho_f^{(k)} U_f^{(k)} \right\}$$

$$\Gamma_f = r_f^{(k)^\circ} r_f^{(k)^\circ} \rho_f^{(k)} \frac{\sum_{i=1}^3 \overline{D}_f^{(k)} [u_i] (S_f^{\delta 1})^2}{\mathbf{S}_f \cdot \mathbf{d}_f} \quad (84)$$

The corrections are then applied to the velocity, pressure, and density fields using the following equations:

$$\mathbf{u}_p^{(k)*} = \mathbf{u}_p^{(k)^\circ} - r^{(k)^\circ} \mathbf{D}_p^{(k)} \nabla_p P' \quad P^* = P^\circ + P' \quad \rho^{(k)*} = \rho^{(k)^\circ} + C_p^{(k)} P' \quad (85)$$

Improvement 2: Weighted pressure correction. Numerical experiments [77] using the above approach to simulate air–water flows have shown poor conservation of the lighter fluid. To understand this behavior, the residual error of the continuity equation of the k th phase, after any global iteration, which arises because the

velocity, density, and volume-fraction fields do not yet satisfy the continuity equation, is denoted by $\text{RESC}^{(k)}$. The pressure-correction equation being derived from the global conservation equation, the intention is to correct the velocity fields so as to drive the global residual error to zero, i.e., $\text{RESC}^{(1)} + \text{RESC}^{(2)} + \dots + \text{RESC}^{(n)} \rightarrow 0$.

In the presence of a relatively very-high-density fluid such that $\rho^{(n)} \gg \rho^{(k)}$ for $k \neq n$, the residual error of the n th fluid will be of a magnitude commensurate with the respective phase density; i.e., $\text{RESC}^{(n)}$ is expected to be much larger than $\text{RESC}^{(k)}$ for $k \neq n$. In this case, only the residual of the high-density fluid will be significant, while that of the low-density fluid will be relatively negligible, and hence the pressure correction will tend to drive the high-density fluid to conservation.

This problem can be considerably alleviated by normalizing the individual continuity equations, and hence the global mass conservation equation, by means of a weighting factor such as a reference density $\rho^{(k)}$ (which is fluid dependent) to give a conservation equation of the form:

$$\sum_k \left\{ \frac{(r_p^{(k)} \rho_p^{(k)} / \rho^{(k)}) - (r_p^{(k)} \rho_p^{(k)} / \rho^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p \left[r^{(k)} \left(\frac{\rho^{(k)}}{\rho^{(k)}} \right) \mathbf{u}^{(k)} \cdot \mathbf{S} \right] \right\} = 0 \quad (86)$$

In this case the pressure correction equation is obtained by simply replacing $\rho^{(k)}$ by $\rho^{(k)} / \rho^{(k)}$.

Solving for Volume Fractions

The volume fractions can be obtained by solving the fluid continuity equations [Eq. (26)]. However, if all volume fractions are obtained by solving the continuity equations, the geometric constraint will not be enforced unless the appropriate velocity field is available, which is not the case until convergence. One remedy is to solve for $n - 1$ volume fractions using the fluid mass conservation equations, and then to employ the geometric conservation equation to find the last-volume-fraction field. Thus, for fluids $k = 1$ to $n - 1$, solve

$$r_p^{(k)*} = \mathbf{H}_p[r^{(k)*}] \text{ and for } k = n \text{ use } r_p^{(n)*} = 1 - \sum_{k \neq n} r_p^{(k)*} \quad (87)$$

A drawback of this procedure is that the volume-fraction field of any phase will not be influenced by the volume-fraction fields of other phases except when calculating the n th phase. This can affect the convergence rate negatively. Better solutions are presented below.

Improvement 3: Mutual influence of volume fractions. An improvement on the above procedure is to solve all continuity equations to obtain all volume fractions and then enforce the geometric conservation constraint on the resulting volume-fraction values using the following equation:

$$r^{(k)} = \frac{r^{(k)*}}{\sum_m r^{(m)*}} = \frac{H_p[r^{(k)*}]}{\sum_m r^{(m)*}} \text{ for all } k \quad (88)$$

The summation is carried out for all phases, and $r^{(k)}$ is the value of the volume fraction for fluid (k) which is carried into subsequent calculations. These $r^{(k)}$, of course, do sum to unity, and the values of every phase are affected by all other phases.

Improvement 4: Implicit volume-fraction equations. The solution of the volume-fraction equations can be improved by implicitly accounting for the influence of the volume fractions of the different phases on each other. The details of the procedure will be presented for a two-fluid flow and then generalized to n -fluid flow situations. For that purpose, the following simplified form of the volume-fraction equation is considered:

$$r_p^{(k)*} = H[r^{(k)*}] = \frac{\sum_{NB} A_{NB}^{(k)} r_{NB}^{(k)*} + B_p^{(k)}}{A_p^{(k)}} \quad (89)$$

For the case of a two-fluid flow, the sum-to-1 rule can be written in the following form:

$$r_p^{(1)*} + r_p^{(2)*} = 1 = \frac{\sum_{NB} A_{NB}^{(1)} r_{NB}^{(1)*} + B_p^{(1)}}{A_p^{(1)}} + \frac{\sum_{NB} A_{NB}^{(2)} r_{NB}^{(2)*} + B_p^{(2)}}{A_p^{(2)}} \quad (90)$$

Based on this equation, the volume-fraction equation for fluid (1) or (2) can be written as

$$r_p^{(1 \text{ or } 2)*} = \frac{\left(\sum_{NB} A_{NB}^{(1 \text{ or } 2)} r_{NB}^{(1 \text{ or } 2)*} + B_p^{(1 \text{ or } 2)} \right)}{A_p^{(1 \text{ or } 2)} \left(1 - \frac{RESR^{(1)}}{A_p^{(1)}} - \frac{RESR^{(2)}}{A_p^{(2)}} \right)} \quad (91)$$

For the case of n fluids, the k th volume-fraction equation can be easily deduced from the above equation and is given by

$$r_p^{(k)*} = \frac{\left(\sum_{NB} A_{NB}^{(k)} r_{NB}^{(k)*} + B_p^{(k)} \right)}{A_p^{(k)} \left(1 - \sum_m \frac{RESR^{(m)}}{A_p^{(m)}} \right)} \quad (92)$$

Improvement 5: Bounding the volume fractions. While the above technique can be used to solve the volume-fraction equations, it does not guarantee that the volume-fraction values are bounded (i.e., between 0 and 1). This is a feature of iterative methods, which are known to return intermediate values that violate the set bounds. While these restrictions can be explicitly enforced after obtaining the solution from the discretized equations, a number of techniques have been developed that lead to the implicit enforcing of these constraints.

The procedure developed by Carver [78] is an example of such methods based on a modification to the underrelaxation practice of Patankar [16]. In this approach, instead of solving the volume-fraction equation directly for $r^{(k)}$ to yield $r^{(k)\text{imp}}$, underrelaxation is used to yield a value $r^{(k)C} = \beta r^{(k)\text{imp}} + (1 - \beta) r^{(k)o}$, where β is between [0, 1] and $r^{(k)o}$ is the solution from the previous iteration. Equation (18) is thus rewritten as

$$\frac{A_p}{\beta} r_p^{(k)C} = \sum_{NB} A_{NB} r_{NB}^{(k)C} + B_p + \frac{(1-\beta)}{\beta} A_p r_p^{(k)o} \quad (93)$$

In the Carver procedure, the value of $r_p^{(k)C}$ over each control volume is monitored by explicitly calculating an intermediate value $r_p^{(k)int}$ as

$$r_p^{(k)int} = \frac{\sum_{NB} A_{NB} r_{NB}^{(k)o} + B_p + [(1-\beta)/\beta] A_p r_p^{(k)o}}{A_p/\beta} \quad (94)$$

If $r_p^{(k)int} > (1-\varepsilon)$, then the underrelaxation factor is modified to the form $\beta = \max(1 - r_p^{(k)o})$. The parameters ε and γ are small; Carver suggests values of 0.05 and 10^{-10} . The system of equations for each volume fraction is then solved implicitly using, for every control volume, the individually assigned relaxation parameter.

Solving the Energy Equations

The solutions of the energy equations follow that of the general multifluid scalar equation. As such, nothing new needs to be added in that regard (though in many cases coupling of the energy equation with the momentum and continuity equations is beneficial). Similar to interphase momentum coupling, the interphase energy term may be written out explicitly and the resulting equations rearranged and solved to obtain a pseudo-solution that resolves the interphase coupling. The resulting values may then be used in calculating the interphase terms and the full-field solution carried out using the normal calculation procedure.

PART II: GEOMETRIC CONSERVATION-BASED ALGORITHMS

The sequence of events in the geometric conservation-based algorithm (GCBA) is as follows:

1. Solve the individual mass conservation equations for volume fractions.
2. Solve the momentum equations for velocities.
3. Solve the pressure-correction equation.
4. Correct velocity, volume-fraction, density, and pressure fields.
5. Solve the individual energy equations.
6. Return to the first step and repeat until convergence.

As in the MCBA, the GCBA uses the momentum equations for a first estimate of velocities. However, the volume fractions are calculated without enforcing the geometric conservation equation. Hence, the mass conservation equations of all fluids are used to calculate the volume fractions. The pressure-correction equation is based on the geometric conservation equation and is used to restore the imbalance of volume fractions. The errors in the calculated volume fractions are expressed in terms of pressure correction (P'), which is also used to adjust the velocity and density fields. An example of a GCBA is the original IPISA, developed by Spalding [79],

which introduces a stronger coupling between the pressure and the volume fractions than the MCBA.

For compactness, the techniques introduced earlier that are also applicable here will not be repeated. Rather, attention will be directed toward the derivation of the pressure-correction equation and the introduction of the various GCBA. This is followed by a comparison between the two families.

Solving for Pressure Correction

After solving the continuity equations for the volume fraction fields and the momentum equations for the velocity fields, the next step is to correct the various fields such that the volume-fraction fields satisfy the compatibility equation and the velocity and pressure fields satisfy the continuity equations. For that purpose, an approach similar to the one used with the MCBA is adopted. The difference between the two approaches lies in the constraint equation employed in deriving the pressure or pressure-correction equation. In the MCBA, the overall mass conservation equation was utilized. In the GCBA, the pressure-correction equation is derived from the geometric conservation equation.

To start the derivation, it is noticed that initially the volume-fraction fields, denoted by $r^{(k)*}$, do not satisfy the compatibility equation and a discrepancy exists, i.e.,

$$\text{RESG}_p = 1 - \sum_k r_p^{(k)*} \quad (95)$$

A change to $r^{(k)*}$ is sought that would restore the balance. The corrected r value, denoted by $r^{(k)}$ ($r^{(k)} = r^{(k)*} + r^{(k)'}$), is such that

$$\sum_k (r^{(k)'}) = 1 - \sum_k (r^{(k)*}) = \text{RESG}_p \quad (96)$$

Correction to the volume fraction, $r^{(k)'}$, will be associated with a correction to the velocity, density, and pressure fields, $\mathbf{u}^{(k)'}$, $\rho^{(k)'}$, and P' , respectively. Thus, the corrected fields are given as

$$r^{(k)} = r^{(k)*} + r^{(k)'} \quad P = P^o + P' \quad \mathbf{u}^{(k)} = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'} \quad \rho^{(k)} = \rho^{(k)o} + \rho^{(k)'} \quad (97)$$

The discretized form of the corrected continuity equation of phase (k) can be written as

$$\frac{(r_p^{(k)*} + r_p^{(k)'}) (\rho_p^{(k)o} + \rho_p^{(k)'}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} + r^{(k)'}) (\rho^{(k)o} + \rho^{(k)'}) (\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}) \cdot \mathbf{S}] = \dot{M}_p^{(k)} (r_p^{(k)*} + r_p^{(k)'}) \Omega_p \quad (98)$$

Neglecting second- and third-order terms (i.e., $r_p^{(k)'} \rho_p^{(k)'}$, $\rho_p^{(k)'} \mathbf{u}^{(k)'}$, $r_p^{(k)'} \mathbf{u}^{(k)'}$, and $r_p^{(k)'} \rho_p^{(k)'} \mathbf{u}^{(k)'}$), its expanded form reduces to

$$\begin{aligned}
& \frac{(r_p^{(k)*} \rho_p^{(k)'} + r_p^{(k)'} \rho_p^{(k)o})}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} \mathbf{u}^{(k)'} \cdot \mathbf{S} + r^{(k)*} U^{(k)*} \rho_p^{(k)'} + \rho^{(k)o} U^{(k)*} r^{(k)'})] \\
& - \dot{M}_p^{(k)} r_p^{(k)'} \Omega_p = \frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p - \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] + \dot{M}_p^{(k)} r_p^{(k)*} \Omega_p
\end{aligned} \quad (99)$$

Writing $\mathbf{u}^{(k)'}$ as a function of P' , similar to what is usually done in a SIMPLE-like algorithm, the correction momentum equations become

$$\mathbf{u}^{(k)'} = \mathbf{HP}[\mathbf{u}^{(k)'}] - r^{(k)*} \mathbf{D}^{(k)} \nabla P' - r^{(k)'} \mathbf{D}^{(k)} \nabla P^o - r^{(k)'} \mathbf{D}^{(k)} \nabla P' \quad (100)$$

Substituting Eq. (100) into Eq. (99), rearranging, and discretizing, one gets

$$\begin{aligned}
& r_p^{(k)'} - H_p[r^{(k)'}] \\
& = -R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p \left[r^{(k)*} \rho^{(k)o} \left(\begin{array}{c} \mathbf{HP}[\mathbf{u}^{(k)'}] - r^{(k)*} \mathbf{D}^{(k)} \nabla P' \\ -r^{(k)'} \mathbf{D}^{(k)} \nabla P' \end{array} \right) \cdot \mathbf{S} + r^{(k)*} U^{(k)*} \rho^{(k)'} \right] \right. \\
& \quad \left. + \frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] - \dot{M}_p^{(k)} r_p^{(k)*} r_p^{(k)*} \Omega_p \right)
\end{aligned} \quad (101)$$

where $R_p^{(k)} = 1/A_p^{(k)}$.

Neglecting the correction to neighboring cells, Eq. (101) reduces to

$$\begin{aligned}
& r_p^{(k)'} = -R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p \left[r^{(k)*} \rho^{(k)o} \left(\begin{array}{c} \mathbf{HP}[\mathbf{u}^{(k)'}] - r^{(k)*} \mathbf{D}^{(k)} \nabla P' \\ -r^{(k)'} \mathbf{D}^{(k)} \nabla P' \end{array} \right) \cdot \mathbf{S} + r^{(k)*} U^{(k)*} \rho^{(k)'} \right] \right. \\
& \quad \left. + \frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] - \dot{M}_p^{(k)} r_p^{(k)*} r_p^{(k)*} \Omega_p \right)
\end{aligned} \quad (102)$$

Substituting this equation into the geometric conservation equation and replacing density correction in terms of pressure correction (i.e., $\rho^{(k)'} = C_p^{(k)} P'$), the pressure-correction equation is obtained as

$$\sum_k \left\{ -R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_p^{(k)}}{\delta t} P_p' + \Delta_p [r^{(k)*} U^{(k)*} C_p^{(k)} P'] \right. \right. \\
\left. \left. + \Delta_p [r^{(k)*} \rho^{(k)o} (\mathbf{HP}[\mathbf{u}^{(k)'}] - r^{(k)*} \mathbf{D}^{(k)} \nabla P' - r^{(k)'} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right. \right. \\
\left. \left. + \frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] \right) \right\} = \text{RESG}_p \quad (103)$$

As detailed next, the above equation can be expanded using any SIMPLE-like algorithm to yield the new GCBA family of multifluid flow algorithms (GCBA-SIMPLE, GCBA-SIMPLEC, GCBA-PISO, etc.).

The GCBA following SIMPLEC (GCBA-SIMPLEC): Symbolic form.

Predictor:

$$r_p^{(k)*} = H_p[r^{(k)*}] \quad (104)$$

$$\mathbf{u}_p^{(k)*} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)*}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (105)$$

Corrector:

$$(\mathbf{u}^{(k)*}, P', \rho^{(k)*}, r^{(k)*}) \left(\begin{array}{l} \mathbf{u}^{(k)**} = \mathbf{u}^{(k)*} + \mathbf{u}^{(k)*'} , P^* = P^o + P', \\ \rho^{(k)*} = \rho^{(k)o} + \rho^{(k)*'} , r^{(k)**} = r^{(k)*} + r^{(k)*'} \end{array} \right) \quad (106)$$

$$\begin{aligned} \therefore \mathbf{u}_p^{(k)**} &= \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)**}] - r_p^{(k)**} \mathbf{D}_p^{(k)} \nabla_p P^* \\ &= \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)*} + \mathbf{u}^{(k)*'}] - (r_p^{(k)*} + r_p^{(k)*'}) \mathbf{D}_p^{(k)} \nabla_p (P^o + P') \end{aligned} \quad (107)$$

$$\therefore \mathbf{u}_p^{(k)'} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P^o - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P' \quad (108)$$

Subtracting $\tilde{\mathbf{H}}\mathbf{P}_p[1]\mathbf{u}_p^{(k)'} from both sides, one gets$

$$\mathbf{u}_p^{(k)'} = \left[\begin{array}{l} \frac{\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'} - \mathbf{u}_p^{(k)'}]}{(1 - \tilde{\mathbf{H}}\mathbf{P}_p[1])} - r_p^{(k)*} \frac{\mathbf{D}_p^{(k)}}{(1 - \tilde{\mathbf{H}}\mathbf{P}_p[1])} \nabla_p P' \\ - r_p^{(k)'} \frac{\mathbf{D}_p^{(k)}}{(1 - \tilde{\mathbf{H}}\mathbf{P}_p[1])} \nabla_p P^o - r_p^{(k)'} \frac{\mathbf{D}_p^{(k)}}{(1 - \tilde{\mathbf{H}}\mathbf{P}_p[1])} \nabla_p P' \end{array} \right] \quad (109)$$

$$\therefore \left\{ \begin{array}{l} \mathbf{u}_p^{(k)'} = \frac{\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'} - \mathbf{u}_p^{(k)'}]}{(1 - \tilde{\mathbf{H}}\mathbf{P}_p[1])} - r_p^{(k)*} \tilde{\mathbf{D}}_p^{(k)} \nabla_p P' - r_p^{(k)'} \tilde{\mathbf{D}}_p^{(k)} \nabla_p P^o - r_p^{(k)'} \tilde{\mathbf{D}}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_\rho^{(k)} P' \\ r_p^{(k)'} = -\mathbf{R}_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p[(r^{(k)*} \rho^{(k)o} \mathbf{u}^{(k)'} \cdot \mathbf{S} + r^{(k)*} U^{(k)*} \rho^{(k)'} \cdot \mathbf{S})] \right) \end{array} \right. \quad (110)$$

Condition:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_\rho^{(k)}}{\delta t} P' + \Delta_p[r^{(k)*} U^{(k)*} C_\rho^{(k)} P'] - \Delta_p[r^{(k)*} \rho^{(k)o} (r^{(k)*} \tilde{\mathbf{D}}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p[(r^{(k)*} \rho^{(k)o} U^{(k)*})] + \right. \right. \\ & \quad \left. \left. \Delta_p[r^{(k)*} \rho^{(k)o} (\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'} - \mathbf{u}_p^{(k)'}] - r^{(k)'} \tilde{\mathbf{D}}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} - \text{RESG}_p \end{aligned} \quad (111)$$

Approximation:

Neglect:

$$\mathbf{HP}[\mathbf{u}^{(k)'} - \mathbf{u}_p^{(k)'}], \quad r^{(k)'} \tilde{\mathbf{D}}^{(k)} \nabla P' \Rightarrow \mathbf{u}_p^{(k)'} = -r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' \quad (112)$$

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_p^{(k)}}{\delta t} P'_p + \Delta_p [r^{(k)*} U^{(k)*} C_p^{(k)} P'] - \Delta_p [r^{(k)*} \rho^{(k)o} (r^{(k)*} \tilde{\mathbf{D}}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] \right) \right\} - \text{RESG}_p \end{aligned} \quad (113)$$

A global GCBA-SIMPLEC iteration

1. Solve implicitly for the volume-fraction fields.
2. Solve implicitly for $\mathbf{u}^{(k)}$, using the old pressure, density, and volume-fraction fields.
3. Calculate the $\tilde{\mathbf{D}}^{(k)}$ fields.
4. Solve the pressure-correction equation and correct $\mathbf{u}^{(k)}$, P , $r^{(k)}$, and $\rho^{(k)}$.
5. Solve implicitly the energy equations and update the density fields.
6. Return to the first step and iterate until convergence.

The GCBA following PRIME (GCBA-PRIME): Symbolic form.

Predictor:

$$r_p^{(k)*} = \mathbf{H}_p[r^{(k)o}] \quad (114)$$

$$u_p^{(k)*} = \mathbf{HP}_p[\mathbf{u}^{(k)o}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (115)$$

Corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}, r^{(k)'}) \left(\begin{aligned} \mathbf{u}^{(k)**} &= \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}, P^* = P^o + P', \\ \rho^{(k)*} &= \rho^{(k)o} + \rho^{(k)'}, r^{(k)**} = r^{(k)*} + r^{(k)'} \end{aligned} \right) \quad (116)$$

$$\begin{aligned} \therefore \mathbf{u}_p^{(k)**} &= \mathbf{HP}_p[\mathbf{u}^{(k)**}] - r_p^{(k)**} \mathbf{D}_p^{(k)} \nabla_p P^* \\ &= \mathbf{HP}_p[\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}] - (r_p^{(k)*} + r_p^{(k)'}) \mathbf{D}_p^{(k)} \nabla_p (P^o + P') \end{aligned} \quad (117)$$

$$\therefore \begin{cases} \mathbf{u}_p^{(k)'} = \mathbf{HP}_p[\mathbf{u}^{(k)*} - \mathbf{u}^{(k)o}] + \mathbf{HP}_p[\mathbf{u}^{(k)'}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P^o - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_p^{(k)} P' \\ r_p^{(k)'} = -R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p [(r^{(k)*} \rho^{(k)o} \mathbf{u}^{(k)'}) \cdot \mathbf{S} + r^{(k)*} U^{(k)*} \rho^{(k)'}] \right) \end{cases} \quad (118)$$

Condition:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_p^{(k)}}{\delta t} P'_p + \Delta_p [r^{(k)*} U^{(k)*} C_p^{(k)} P'] - \Delta_p [r^{(k)*} \rho^{(k)o} (r^{(k)*} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{\left(r_p^{(k)*} \rho_p^{(k)o} \right) - \left(r_p^{(k)} \rho_p^{(k)} \right)^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] \right. \right. \\ & \quad \left. \left. + \Delta_p [r^{(k)*} \rho^{(k)o} (\mathbf{HP}[\mathbf{u}^{(k)*} - \mathbf{u}^{(k)o}] + \mathbf{HP}[\mathbf{u}^{(k)'}] - r^{(k)'} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} - \text{RESG}_p \end{aligned} \quad (119)$$

Approximation:

Neglect:

$$\mathbf{HP}[\mathbf{u}^{(k)*} - \mathbf{u}^{(k)o}], \mathbf{HP}[\mathbf{u}^{(k)'}], r^{(k)'} \mathbf{D}^{(k)} \nabla P' \Rightarrow \mathbf{u}_p^{(k)'} = -r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' \quad (120)$$

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_p^{(k)}}{\delta t} P'_p + \Delta_p [r^{(k)*} U^{(k)*} C_p^{(k)} P'] - \Delta_p [r^{(k)*} \rho^{(k)o} (r^{(k)*} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{\left(r_p^{(k)*} \rho_p^{(k)o} \right) - \left(r_p^{(k)} \rho_p^{(k)} \right)^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)*})] \right) \right\} - \text{RESG}_p \end{aligned} \quad (121)$$

A global GCBA-PRIME iteration

1. Solve explicitly for the volume-fraction fields.
2. Solve explicitly for $\mathbf{u}^{(k)}$, using the old pressure and density fields.
3. Calculate the $\mathbf{D}^{(k)}$ fields.
4. Solve the pressure-correction equation and correct $\mathbf{u}^{(k)}$, P , $r^{(k)}$, and $\rho^{(k)}$.
5. Solve implicitly the energy equations and update the density fields.
6. Return to the first step and iterate until convergence.

The GCBA following SIMPLER (GCBA-SIMPLER): Symbolic form.

First predictor:

$$r_p^{(k)*} = \mathbf{H}_p[r^{(k)*}] \quad (122)$$

Calculate the coefficients of the momentum equations.

First corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}, r^{(k)'}) \left(\begin{array}{l} \mathbf{u}^{(k)*} = \mathbf{u}^{(k)o} + \mathbf{u}^{(k)'}, P^* = P^o + P', \\ \rho^{(k)*} = \rho^{(k)o} + \rho^{(k)'}, r^{(k)**} = r^{(k)*} + r^{(k)'} \end{array} \right) \quad (123)$$

$$\begin{aligned} \therefore \mathbf{u}_p^{(k)*} &= \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)*}] - r_p^{(k)**} \mathbf{D}_p^{(k)} \nabla_p P^* \\ &= \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)o} + \mathbf{u}^{(k)'}] - (r_p^{(k)*} + r_p^{(k)'}) \mathbf{D}_p^{(k)} \nabla_p (P^o + P') \end{aligned} \quad (124)$$

$$\mathbf{u}_p^{(k)o} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)o}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (125)$$

$$\therefore \begin{cases} \mathbf{u}_p^{(k)'} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P^o - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_\rho^{(k)} P' \\ r_p^{(k)'} = -R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p[(r^{(k)*} \rho^{(k)o} \mathbf{u}^{(k)'}) \cdot \mathbf{S} + r^{(k)*} U^{(k)o} \rho^{(k)'}] \right) \end{cases} \quad (126)$$

Condition:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_\rho^{(k)}}{\delta t} P'_p + \Delta_p[r^{(k)*} U^{(k)o} C_\rho^{(k)} P'] - \Delta_p[r^{(k)*} \rho^{(k)o} (r^{(k)*} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{\left(r_p^{(k)*} \rho_p^{(k)o} \right) - \left(r_p^{(k)} \rho_p^{(k)} \right)^{\text{old}}}{\delta t} \Omega_p + \Delta_p[(r^{(k)*} \rho^{(k)o} U^{(k)o})] \right. \right. \\ & \quad \left. \left. + \Delta_p[r^{(k)*} \rho^{(k)o} (\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'}] - r^{(k)'} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} - \text{RESG}_p \end{aligned} \quad (127)$$

Approximation:

Neglect:

$$\mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)'}], r^{(k)'} \mathbf{D}^{(k)} \nabla P' \Rightarrow \mathbf{u}_p^{(k)'} = -r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' \quad (128)$$

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_\rho^{(k)}}{\delta t} P'_p + \Delta_p[r^{(k)*} U^{(k)o} C_\rho^{(k)} P'] - \Delta_p[r^{(k)*} \rho^{(k)o} (r^{(k)*} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{\left(r_p^{(k)*} \rho_p^{(k)o} \right) - \left(r_p^{(k)} \rho_p^{(k)} \right)^{\text{old}}}{\delta t} \Omega_p + \Delta_p[(r^{(k)*} \rho^{(k)o} U^{(k)o})] \right) \right\} - \text{RESG}_p \end{aligned} \quad (129)$$

Apply correction to pressure, density, and volume-fraction fields.

Second predictor:

$$\mathbf{u}_p^{(k)*} = \mathbf{H}\mathbf{P}_p[\mathbf{u}^{(k)*}] - r_p^{(k)**} \mathbf{D}_p^{(k)} \nabla_p P^* \quad (130)$$

Second corrector:

$$(\mathbf{u}^{(k)''}, P'', \rho^{(k)''}, r^{(k)'') \left(\begin{aligned} \mathbf{u}^{(k)''} &= \mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}, \mathbf{P}'' = \mathbf{P}^* + \mathbf{P}', \\ \rho^{(k)''} &= \rho^{(k)*} + \rho^{(k)'}, r^{(k)''} = r^{(k)*} + r^{(k)'} \end{aligned} \right) \quad (131)$$

$$\begin{aligned} \therefore \mathbf{u}_P^{(k)''} &= \mathbf{H}\mathbf{P}_P[\mathbf{u}^{(k)''}] - r_P^{(k)''} \mathbf{D}_P^{(k)} \nabla_P P'' \\ &= \mathbf{H}\mathbf{P}_P[\mathbf{u}^{(k)*} + \mathbf{u}^{(k)'}] - (r_P^{(k)*} + r_P^{(k)'}) \mathbf{D}_P^{(k)} \nabla_P (P^* + P') \end{aligned} \quad (132)$$

$$\therefore \begin{cases} \mathbf{u}_P^{(k)''} = \mathbf{H}\mathbf{P}_P[\mathbf{u}^{(k)'}] - r_P^{(k)''} \mathbf{D}_P^{(k)} \nabla_P P'' - r_P^{(k)'} \mathbf{D}_P^{(k)} \nabla_P P^* - r_P^{(k)'} \mathbf{D}_P^{(k)} \nabla_P P' \\ \rho^{(k)''} = C_\rho^{(k)} P'' \\ r_P^{(k)''} = -R_P^{(k)} \left(\frac{r_P^{(k)''} \Omega_P}{\delta t} \rho_P^{(k)''} + \Delta_P[(r^{(k)''} \rho^{(k)*} \mathbf{u}^{(k)'}) \cdot \mathbf{S} + r^{(k)''} U^{(k)*} \rho^{(k)'}] \right) \end{cases} \quad (133)$$

Condition:

$$\begin{aligned} \sum_k \left\{ R_P^{(k)} \left(\frac{r_P^{(k)''} \Omega_P C_\rho^{(k)}}{\delta t} P'' + \Delta_P[r^{(k)''} U^{(k)*} C_\rho^{(k)} P''] - \Delta_P[r^{(k)''} \rho^{(k)*} (r^{(k)''} \mathbf{D}^{(k)} \nabla P'') \cdot \mathbf{S}] \right) \right\} \\ = - \sum_k \left\{ R_P^{(k)} \left(\frac{(r_P^{(k)''} \rho_P^{(k)*}) - (r_P^{(k)} \rho_P^{(k)})^{\text{old}}}{\delta t} \Omega_P + \Delta_P[(r^{(k)''} \rho^{(k)*} U^{(k)*})] \right) \right\} - \text{RESG}_P \end{aligned} \quad (134)$$

Approximation:

Neglect:

$$\mathbf{H}\mathbf{P}[\mathbf{u}^{(k)'}], r^{(k)'} \mathbf{D}^{(k)} \nabla P' \Rightarrow \mathbf{u}_P^{(k)'} = -r_P^{(k)''} \mathbf{D}_P^{(k)} \nabla_P P'' \quad (135)$$

Approximate equation:

$$\begin{aligned} \sum_k \left\{ -R_P^{(k)} \left(\frac{r_P^{(k)''} \Omega_P C_\rho^{(k)}}{\delta t} P'' + \Delta_P[r^{(k)''} U^{(k)*} C_\rho^{(k)} P''] - \Delta_P[r^{(k)''} \rho^{(k)*} (r^{(k)''} \mathbf{D}^{(k)} \nabla P'') \cdot \mathbf{S}] \right) \right\} \\ = - \sum_k \left\{ R_P^{(k)} \left(\frac{(r_P^{(k)''} \rho_P^{(k)*}) - (r_P^{(k)} \rho_P^{(k)})^{\text{old}}}{\delta t} \Omega_P + \Delta_P[(r^{(k)''} \rho^{(k)*} U^{(k)*})] \right) \right\} - \text{RESG}_P \end{aligned} \quad (136)$$

Apply correction to velocity fields.

A global GCBA-SIMPLER iteration

1. Solve implicitly for $r^{(k)}$.
2. Calculate the $\mathbf{D}^{(k)}$ fields.
3. Solve the pressure-correction equation and update the pressure, density, and volume-fraction fields.
4. Solve implicitly for $\mathbf{u}^{(k)}$ using the new pressure, density, and volume-fraction fields.
5. Solve the pressure-correction equation using the new velocity fields and correct $\mathbf{u}^{(k)}$.
6. Solve implicitly the energy equations and update the density fields.
7. Return to the first step and iterate until convergence.

The GCBA following SIMPLEM (GCBA-SIMPLEM): Symbolic form.

First predictor:

$$r_p^{(k)*} = \mathbf{H}_p[r^{(k)*}] \quad (137)$$

Calculate the coefficients of the momentum equations.

First corrector:

$$(\mathbf{u}^{(k)'}, P', \rho^{(k)'}, r^{(k)'}) \left(\begin{array}{l} \mathbf{u}^{(k)*} = \mathbf{u}^{(k)o} + \mathbf{u}^{(k)'}, P^* = P^o + P', \\ \rho^{(k)*} = \rho^{(k)o} + \rho^{(k)'}, r^{(k)**} = r^{(k)*} + r^{(k)'} \end{array} \right) \quad (138)$$

$$\begin{aligned} \therefore \mathbf{u}_p^{(k)*} &= \mathbf{H}_p[\mathbf{u}^{(k)*}] - r_p^{(k)**} \mathbf{D}_p^{(k)} \nabla_p P^* \\ &= \mathbf{H}_p[\mathbf{u}^{(k)o} + \mathbf{u}^{(k)'}] - (r_p^{(k)*} + r_p^{(k)'}) \mathbf{D}_p^{(k)} \nabla_p (P^o + P') \end{aligned} \quad (139)$$

$$\mathbf{u}_p^{(k)o} = \mathbf{H}_p[\mathbf{u}^{(k)o}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P^o \quad (140)$$

$$\therefore \left\{ \begin{array}{l} \mathbf{u}_p^{(k)'} = \mathbf{H}_p[\mathbf{u}^{(k)'}] - r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P^o - r_p^{(k)'} \mathbf{D}_p^{(k)} \nabla_p P' \\ \rho^{(k)'} = C_p^{(k)} P' \\ r_p^{(k)'} = -R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p [(r^{(k)*} \rho^{(k)o} \mathbf{u}^{(k)'}) \cdot \mathbf{S} + r^{(k)*} U^{(k)o} \rho^{(k)'}] \right) \end{array} \right. \quad (141)$$

Condition:

$$\begin{aligned} & \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_p^{(k)}}{\delta t} P_p' + \Delta_p [r^{(k)*} U^{(k)o} C_p^{(k)} \mathbf{P}'] - \Delta_p [r^{(k)*} \rho^{(k)o} (r^{(k)*} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ R_p^{(k)} \left(\frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} U^{(k)o})] \right. \right. \\ & \quad \left. \left. + \Delta_p [r^{(k)*} \rho^{(k)o} (\mathbf{H}_p[\mathbf{u}^{(k)'}] - r^{(k)'} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} - \text{RESG}_p \end{aligned} \quad (142)$$

Approximation:

Neglect:

$$\mathbf{HP}[\mathbf{u}^{(k)'}], r^{(k)'} \mathbf{D}^{(k)} \nabla P' \Rightarrow \mathbf{u}_p^{(k)'} = -r_p^{(k)*} \mathbf{D}_p^{(k)} \nabla_p P' \quad (143)$$

Approximate equation:

$$\begin{aligned} & \sum_k \left\{ \mathbf{R}_p^{(k)} \left(\frac{r_p^{(k)*} \Omega_p C_p^{(k)}}{\delta t} P'_p + \Delta_p [r^{(k)*} \mathbf{U}^{(k)o} C_p^{(k)} P'] - \Delta_p [r^{(k)*} \rho^{(k)o} (r^{(k)*} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_k \left\{ \mathbf{R}_p^{(k)} \left(\frac{(r_p^{(k)*} \rho_p^{(k)o}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)*} \rho^{(k)o} \mathbf{U}^{(k)o})] \right) \right\} - \text{RESG}_p \end{aligned} \quad (144)$$

Second predictor:

$$\mathbf{u}_p^{(k)**} = \mathbf{HP}_p[\mathbf{u}^{(k)**}] - r_p^{(k)**} \mathbf{D}_p^{(k)*} \nabla_p P^* \quad (145)$$

Second corrector: No corrector stage.

A global GCBA-SIMPLEM iteration

1. Solve implicitly for $r^{(k)}$.
2. Calculate the $\mathbf{D}^{(k)}$ fields based on values from the previous iteration.
3. Solve the pressure-correction equation.
4. Correct $\mathbf{u}^{(k)}$, P , $r^{(k)}$, and $\rho^{(k)}$.
5. Calculate new $\mathbf{HP}^{(k)}$ and $\mathbf{D}^{(k)}$ fields.
6. Solve implicitly for $\mathbf{u}^{(k)}$ using the new fields.
7. Solve implicitly the energy equations and update the density fields.
8. Return to the first step and iterate until convergence.

The expanded form of the pressure-correction equation. The expanded form of the pressure-correction equation, applicable to all algorithms, will be presented. For that purpose, let $r^{(k)}$, $\mathbf{U}^{(k)}$, and $\rho^{(k)}$ denote values from the previous iteration or from a previous corrector step. Then the pressure-correction equation becomes

$$\begin{aligned} & \sum_k \left\{ \mathbf{R}_p^{(k)} \left(\frac{r_p^{(k)} C_p^{(k)} \Omega_p}{\delta t} P'_p + \Delta_p [r^{(k)} \mathbf{U}^{(k)} C_p^{(k)} P'] - \Delta_p [r^{(k)} \rho^{(k)} (r^{(k)} \mathbf{D}^{(k)} \nabla (P')) \cdot \mathbf{S}] \right) \right\} \\ &= - \sum_{k=1}^{\text{nphase}} \left\{ \mathbf{R}_p^{(k)} \left(\frac{(r_p^{(k)} \rho_p^{(k)}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)} \rho^{(k)} \mathbf{U}^{(k)})] \right) \right\} - \text{RESG}_p \end{aligned} \quad (146)$$

In this form, the resemblance between this equation and the MCBA pressure-correction equation is obvious. The discretization of the above equation yields

$$A_P^{P'} P_P' = A_E^{P'} P_E' + A_W^{P'} P_W' + A_N^{P'} P_N' + A_S^{P'} P_S' + A_T^{P'} P_T' + A_B^{P'} P_B' + B_P^{P'} \quad (147)$$

where

$$A_F^{P'} = \sum_k R_P^{(k)} [\Gamma_f^{(k)} + (r^{(k)} C_p^{(k)})_f \| - U_f^{(k)}, 0 \|] \quad (148)$$

$$A_P^{P'} = \sum_{NB} A_F^{P'} + \sum_k R_P^{(k)} \left(\frac{r_P^{(k)} K_P^{(k)} \Omega_P}{\delta t} + \sum_{nb} (r_f^{(k)} C_p^{(k)})_f U_f^{(k)} \right) \quad (149)$$

$$B_P^{P'} = - \sum_k R_P^{(k)} \left\{ \frac{(r_P^{(k)} \rho_P^{(k)} - r_P^{(k)old} \rho_P^{(k)old})}{\delta t} \Omega_P + \sum_{nb} r_f^k \rho_f^{(k)} U_f^{(k)} \right\} - \text{RESG}_P \quad (150)$$

Following the calculation of the pressure-correction field, $\mathbf{u}_p^{(k)'}$, $\rho_p^{(k)'}$, and $r_p^{(k)'}$ are obtained using the following equations:

$$\begin{aligned} \mathbf{u}_p^{(k)'} &= -r^{(k)} \mathbf{D}_p^{(k)} \nabla_p(P') & \rho_p^{(k)'} &= C_p^{(k)} P' \\ r_p^{(k)'} &= -R_p^{(k)} \left(\frac{r_P^{(k)} \Omega_P}{\delta t} \rho_p^{(k)'} + \Delta_p [(r^{(k)} \rho^{(k)} \mathbf{u}^{(k)'}) \cdot \mathbf{S} + r^{(k)} \mathbf{U}^{(k)} \rho^{(k)'}] \right) \end{aligned} \quad (151)$$

Improvement 6: A newly suggested GCBAC family. The pressure-correction equation was derived in the previous section by neglecting the $H_p[r^{(k)'}]$ term. Following the SIMPLEC methodology, a better approximation could be achieved by adding and subtracting $H_p[1]r_p^{(k)'}$ from the left-hand side of Eq. (101), which results in neglecting a smaller term ($H_p[r^{(k)'} - r^{(k)'}_p]$). With this approximation, Eq. (101) becomes

$$r_p^{(k)'} = -\tilde{R}_p^{(k)} \left(\frac{r_P^{(k)*} \Omega_P}{\delta t} \rho_p^{(k)'} + \Delta_p \left[\begin{aligned} &r^{(k)*} \rho^{(k)'} (\mathbf{H} \mathbf{P}[\mathbf{u}^{(k)'}) - r^{(k)*} \mathbf{D}^{(k)} \nabla P' - r^{(k)'} \mathbf{D}^{(k)} \nabla P' \cdot \mathbf{S} \\ &+ r^{(k)*} U^{(k)*} \rho^{(k)'} \end{aligned} \right] \right. \\ \left. + \frac{(r_P^{(k)*} \rho_P^{(k)'} - (r_P^{(k)} \rho_P^{(k)})^{old})}{\delta t} \Omega_P + \Delta_p [(r^{(k)*} \rho^{(k)'} U^{(k)*})] + \dot{M}_p^{(k)} r_p^{(k)*} \Omega_P \right) \quad (152)$$

where

$$\tilde{R}_p^{(k)} = \frac{R_p^{(k)}}{(1 - H_p[1])} \quad (153)$$

The pressure-correction equation is obtained by substituting Eq. (152) into the geometric conservation equation. The expanded form of the resulting pressure-

correction equation is easily obtained from Eqs. (147)–(150) by simply substituting $\tilde{R}_p^{(k)}$ for $R_p^{(k)}$. Furthermore, depending on the approximation made to the $\mathbf{HP}[\mathbf{u}^{(k)'}]$ term, a new family of GCBA, similar to the one detailed above, can be obtained. Since this family is obtained by using ideas similar to the ones employed in SIMPLEC, the letter *C* is appended to its acronym and it is denoted as the GCBAC family.

COMPARING THE GCBA AND MCBA FORMULATIONS

Scaling GCBA to Single-Fluid Flow Simulations

Since the MCBA are derived through direct extension of the single-fluid algorithms, they scale down automatically to handle single-fluid flow simulations. On the other hand, because the GCBA algorithms are based on geometric conservation, their scaling to single-fluid flow simulations is not obvious. Such a property is useful in the sense that coding for single- and multifluid models would follow the same structure. To show how multifluid GCBA algorithms scale down to single-fluid flow simulations, attention is directed toward Eq. (102). For the case of one-fluid flow, $r_p^{(k)} = 1 = \text{Cte}$, thus $r_p^{(k)'} = 0$, removing $r_p^{(k)'}$ from that equation and setting $r_p^{(k)*}$ to 1 yields

$$0 = -R_p^{(k)} \left(\frac{\Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p [\rho^{(k)o} (\mathbf{HP}[\mathbf{u}^{(k)'}] - \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S} + \mathbf{u}^{(k)*} \rho^{(k)'}] \right. \\ \left. + \frac{(\rho_p^{(k)o}) - (\rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(\rho^{(k)o} U^{(k)*})] - \dot{M}_p^{(k)} \Omega_p \right) \quad (154)$$

Removing $R_p^{(k)}$ and rearranging, the pressure-correction equation transforms to

$$\frac{\Omega_p}{\delta t} \rho_p^{(k)'} + \Delta_p [\rho^{(k)o} (\mathbf{HP}[\mathbf{u}^{(k)'}] - \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S} + \mathbf{u}^{(k)*} \rho^{(k)'}] \\ = - \frac{(\rho_p^{(k)o}) - (\rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p - \Delta_p [(\rho^{(k)o} U^{(k)*})] + \dot{M}_p^{(k)} \Omega_p \quad (155)$$

The expansion of the above equation is straightforward and leads to the pressure-correction equation of a single-fluid flow.

The Relation Between the GCBA and the MCBA

While the derivations of the GCBA and MCBA are based on different paradigms, it is shown in this section that the GCBA formulation leads to a weighted pressure-correction equation that has close similarity with the MCBA formulation to which improvement #2 has been applied.

The respective GCBA and MCBA (with improvement #2) pressure-correction equations, as derived earlier, are respectively given by

$$\begin{aligned}
& \sum_k \left\{ R_p^{(k)} \left(\frac{r_p^{(k)} C_p^{(k)} \Omega_p}{\delta t} P'_p + \Delta_p [r^{(k)} U^{(k)} C_p^{(k)} P'] - \Delta_p [r^{(k)} \rho^{(k)} (r^{(k)} \mathbf{D}^{(k)} \nabla(P')) \cdot \mathbf{S}] \right) \right\} \\
&= - \sum_{k=1}^{\text{nphase}} \left\{ R_p^{(k)} \left(\frac{(r_p^{(k)} \rho_p^{(k)}) - (r_p^{(k)} \rho_p^{(k)})^{\text{old}}}{\delta t} \Omega_p + \Delta_p [(r^{(k)} \rho^{(k)} U^{(k)})] \right) \right\} - \text{RESG}_p
\end{aligned} \tag{156}$$

$$\begin{aligned}
& \sum_k \left\{ \frac{\Omega}{\delta t \rho^{(k)}} r_p^{(k)\circ} C_p^{(k)} P'_p + \Delta_p \left[\frac{r^{(k)\circ} C_p^{(k)} U^{(k)} P'}{\rho^{(k)}} \right] - \Delta_p \left[r^{(k)\circ} \frac{\rho^{(k)}}{\rho^{(k)}} (r^{(k)\circ} \mathbf{D}^{(k)} \nabla P') \cdot \mathbf{S} \right] \right\} \\
&= - \sum_k \left\{ \frac{r_p^{(k)\circ} - (\rho_p^{(k)} / \rho^{(k)}) - [r_p^{(k)} (\rho_p^{(k)} / \rho^{(k)})]^{\text{old}}}{\delta t} \Omega + \Delta_p \left[r^{(k)\circ} \frac{\rho^{(k)}}{\rho^{(k)}} U^{(k)} \right] \right\}
\end{aligned} \tag{157}$$

Upon comparing the two equations it is clear that the $R_p^{(k)}$ term plays the role of the reference density, i.e., a weighing factor for the mass conservation equation of the respective phase. As such, the GCBA pressure-correction equation is very similar to a weighted MCBA pressure-correction equation. The weighting procedure (normalization) is done automatically based on the local strength of the inflow to the control volume (since $R_p^{(k)} = 1/A_p^{(k)}$ of the volume fraction equation), thus, as $r_p^{(1)} \gg r_p^{(2)}$, one gets $R_p^{(1)} \ll R_p^{(2)}$. This treatment yields more robust behavior, since large fluid density differences will not mean that conservation for the lighter fluid is lost due to numerical errors.

The above equations also differ slightly in the source term, where an additional entry (RESG_p) is included in Eq. (146) to account for residuals of the geometric conservation equation. Hence, the MCBA family can be viewed as a subset of the GCBA family, and could be recovered by setting the volume-fraction corrections to zero ($r_p^{(k)'} = 0$). As such, codes based on the GCBA can easily cater for the MCBA and vice versa. The main advantage of the GCBA over the MCBA is in the attempt to correct both the velocity and volume-fraction fields.

CLOSING REMARKS

The segregated class of single-fluid flow algorithms was extended to predict multifluid flow at all speeds. The formulation was done using a unified, compact, and easy-to-understand notation. Depending on the constraint equation used to derive the pressure-correction equation, the extended algorithms were shown to fall into two categories that were denoted as mass conservation-based algorithms and the geometric conservation-based algorithms. The differences and similarities between the two categories were explained. In addition, several techniques developed to promote and accelerate the convergence of these algorithms were also discussed.

REFERENCES

1. J. Zhu and M. A. Leschziner, A Local Oscillation-Damping Algorithm for Higher Order Convection Schemes, *Comput. Meth. Appl. Mech. Eng.*, vol. 67, pp. 355–366, 1988.

2. P. H. Gaskell and A. K. C. Lau, Curvature Compensated Convective Transport: SMART, A New Boundedness Preserving Transport Algorithm, *Int. J. Numer. Meth. Fluids*, vol. 8, pp. 617–641, 1988.
3. M. S. Darwish, A New High-Resolution Scheme Based on the Normalized Variable Formulation, *Numer. Heat Transfer B*, vol. 24, pp. 353–371, 1993.
4. M. Chapman, FRAM Nonlinear Damping Algorithm for the Continuity Equation, *J. Comput. Phys.*, vol. 44, pp. 84–103, 1981.
5. S. T. Zalesak, Fully Multidimensional Flux-Corrected Transport Algorithm for Fluids, *J. Comput. Phys.*, vol. 31, pp. 335–362, 1979.
6. A. Harten, High Resolution Schemes for Hyperbolic Conservation Laws, *J. Comput. Phys.*, vol. 49, no. 3, pp. 357–393, 1983.
7. B. P. Leonard, Locally Modified Quick Scheme for Highly Convective 2-D and 3-D Flows, in C. Taylor and K. Morgan (eds.), *Numerical Methods in Laminar and Turbulent Flows*, vol. 15, pp. 35–47, Pineridge Press, Swansea, U.K., 1987.
8. M. S. Darwish and F. Moukalled, Normalized Variable and Space Formulation Methodology for High-Resolution Schemes, *Numer. Heat Transfer B*, vol. 26, pp. 79–96, 1994.
9. F. Moukalled and M. S. Darwish, A New Bounded-Skew Central Difference Scheme—Part I: Formulation and Testing, *Numer. Heat Transfer B*, vol. 31, pp. 91–110, 1996.
10. F. Moukalled and M. S. Darwish, A New Bounded-Skew Central Difference Scheme—Part II: Application to Natural Convection in an Eccentric Horizontal Cylinder, *Numer. Heat Transfer B*, vol. 31, pp. 111–133, 1996.
11. F. Moukalled and M. S. Darwish, A New Family of Streamline-Based Very High Resolution Schemes, *Numer. Heat Transfer B*, vol. 32, no. 3, pp. 299–320, 1997.
12. M. S. Darwish and F. Moukalled, Very High Resolution Schemes through Adaptive Stencils, *Numer. Heat Transfer B*, in press, 1997.
13. F. Moukalled and M. S. Darwish, A New Family of Adaptive Very High Resolutions Schemes, *Numer. Heat Transfer B*, in press, 1997.
14. M. S. Darwish and F. Moukalled, B-EXPRESS: A New Bounded Extremum Preserving Strategy for Convective Schemes, *Numer. Heat Transfer*, in press.
15. S. Patankar and D. B. Spalding, A Calculation Procedure for Heat, Mass, and Momentum Transfer in Three Dimensional Parabolic Flows, *Int. J. Heat Mass Trans.*, vol. 15, p. 1787, 1972.
16. S. V. Patankar, *Numerical Heat Transfer and Fluid Flow*, Hemisphere, New York, 1981.
17. R. I. Issa, Solution of the Implicit Discretized Fluid Flow Equations by Operator Splitting, *Mech. Eng. Rep.*, FS/82/15, Imperial College, London, 1982.
18. J. P. Van Doormaal and G. D. Raithby, Enhancement of the SIMPLE Method for Predicting Incompressible Fluid Flows, *Numer. Heat Transfer*, vol. 7, pp. 147–163, 1984.
19. D. S. Jang, R. Jetli, and S. Acharya, Comparison of the PISO, SIMPLER and SIMPLEC Algorithms for the Treatment of the Pressure-Velocity Coupling in Steady Flow Problems, *Numer. Heat Transfer*, vol. 10, pp. 209–228, 1986.
20. J. P. Van Doormaal and G. D. Raithby, An Evaluation of the Segregated Approach for Predicting Incompressible Fluid Flows, ASME Paper 85-HT-9, Natl. Heat Transfer Conf., Denver, Co, 4–7 August, 1985.
21. F. Moukalled and M. S. Darwish, A Unified Formulation of the Segregated Class of Algorithms for Fluid Flow at All Speeds, *Numer. Heat Transfer B*, vol. 37, no. 1, pp. 103–139, 2000.
22. D. Kershaw, The Incomplete Cholesky-Conjugate Gradient Method for the Iterative Solution of Systems of Linear Equations, *J. Comput. Phys.*, vol. 26, pp. 43–65, 1978.
23. H. L. Stone, Iterative Solution of Implicit Approximations of Multidimensional Partial Differential Equations, *SIAM J. Numer. Anal.*, vol. 5, no. 3, pp. 530–558, 1968.

24. A. Brandt, Multi-Level Adaptive Solutions to Boundary-Value Problems, *Math. Comput.*, vol. 31, pp. 333–390, 1977.
25. C. M. Rhie, A Pressure Based Navier-Stokes Solver Using the Multigrid Method, AIAA Paper 86-0207, 1986.
26. W. Shyy and M. H. Chen, Pressure-Based Multigrid Algorithm for Flow at All Speeds, *AIAA J.*, vol. 30, no. 11, pp. 2660–2669, 1992.
27. W. Shyy and M. E. Braaten, Adaptive Grid Computation for Inviscid Compressible Flows Using a Pressure Correction Method, AIAA Paper 88-3566-CP, 1988.
28. K. C. Karki, A Calculation Procedure for Viscous Flows at All Speeds in Complex Geometries, Ph.D. thesis, University of Minnesota, June 1986.
29. F. S. Lien and M. A. Leschziner, A General Non-orthogonal Collocated Finite Volume Algorithm for Turbulent Flow at All Speeds Incorporating Second-Moment Turbulence-Transport Closure, Part I: Computational Implementation, *Comput. Meth. Appl. Mech. Eng.*, vol. 114, pp. 123–148, 1994.
30. E. S. Politis and K. C. Giannakoglou, A Pressure-Based Algorithm for High-Speed Turbomachinery Flows, *Int. J. Numer. Meth. Fluids*, vol. 25, pp. 63–80, 1997.
31. F. Moukalled and M. S. Darwish, A Finite-Volume Algorithm for All-Speed Flows, in *Finite Volumes for Complex Applications II, Problems and Perspectives*, Duisburg, Germany, pp. 339–346, July 19–22, 1999.
32. F. Moukalled and M. Darwish, A High-Resolution Pressure-Based Algorithm for Fluid Flow at All Speeds, *J. Comput. Phys.*, vol. 168, no. 1, pp. 101–133, 2001.
33. D. B. Spalding, Mathematical Modelling of Fluid Mechanics, Heat Transfer and Mass Transfer Processes, Mech. Eng. Dept. Rep. HTS/80/1, Imperial College of Science, Technology and Medicine, London, U.K., 1980.
34. S. Acharya and F. Moukalled, Improvements to Incompressible Flow Calculation on a Non-Staggered Curvilinear Grid, *Numer. Heat Transfer B*, vol. 15, pp. 131–152, 1989.
35. C. Hsu, A Curvilinear-Coordinate Method for Momentum, Heat and Mass Transfer in Domains of Irregular Geometry, Ph.D. thesis, University of Minnesota, 1981.
36. C. Prakash, A Finite Element Method for Predicting Flow through Ducts with Arbitrary Cross Sections, Ph.D. thesis, University of Minnesota, 1981.
37. M. Peric, A Finite Volume Method for the Prediction of Three Dimensional Fluid Flow in Complex Ducts, Ph.D. thesis, Imperial College, London, U.K., 1985.
38. H. Aksoy and C. J. Chen, Numerical Solution of Navier-Stokes Equations with Non-Staggered Grids Using the Finite Analytic Method, *Numer. Heat Transfer B*, vol. 21, pp. 287–306, 1992.
39. T. F. Miller and F. W. Schmidt, Use of a Pressure-Weighted Interpolation Method for the Solution of the Incompressible Navier-Stokes Equations on a Non-Staggered Grid System, *Numer. Heat Transfer*, vol. 14, pp. 213–233, 1988.
40. S. Majumdar, W. Rodi, and S. P. Vanka, On the Use of Non-Staggered Pressure-Velocity Arrangement for Numerical Solution of Incompressible Flows, Rep. SFB 210/T/35, University of Karlsruhe, November 1987.
41. C. M. Rhie, A Numerical Study of the Flow Past an Isolated Airfoil with Separation, Ph.D. thesis, University of Illinois at Urbana—Champaign, 1981.
42. C. M. Rhie and W. L. Chow, A Numerical Study of the Turbulent Flow Past an Isolated Airfoil with Trailing Edge Separation, *AIAA J.*, vol. 21, pp. 1525–1532, 1983.
43. M. Peric, R. Kessler, and G. Scheuerer, Comparison of Finite Volume Numerical Methods with Staggered and Collocated Grids, *Comput. Fluids*, vol. 16, no. 4, pp. 289–403, 1988.
44. S. K. Choi, H. Y. Nam, and M. Cho, A Calculation Procedure for Incompressible Flow in Complex Geometries Using Momentum Interpolation Method, *7th Int. Conf. on Numerical Methods in Laminar & Turbulent Flow*, vol. VII, part 2, pp. 1634–1644, 1991.

45. S. M. H. Karimian and G. E. Schneider, Pressure-Based Control-Volume Finite Element Method for Flow at All Speeds, *AIAA J.*, vol. 33, no. 9, pp. 1611–1618, 1995.
46. K. H. Chen and R. H. Pletcher, Primitive Variable, Strongly Implicit Calculation Procedure for Viscous Flows at All Speeds, *AIAA J.*, vol. 29, no. 8, pp. 1241–1249, 1991.
47. I. Demirdzic, Z. Lilek, and M. Peric, A Collocated Finite Volume Method for Predicting Flows at All Speeds, *Int. J. Numer. Meth. Fluids*, vol. 16, pp. 1029–1050, 1993.
48. C. H. Marchi and C. R. Maliska, A Nonorthogonal Finite-Volume Methods for the Solution of All Speed Flows Using Co-located Variables, *Numer. Heat Transfer B*, vol. 26, pp. 293–311, 1994.
49. D. B. Spalding, The Calculation of Free-Convection Phenomena in Gas-Liquid Mixtures, Rep. HTS/76/11, Imperial College, London, U.K., 1976.
50. D. B. Spalding, Numerical Computation of Multi-phase Fluid Flow and Heat Transfer, in C. Taylor and K. Morgan (eds.), *Recent Advances in Numerical Methods in Fluid*, vol. 1, pp. 139–167, 1980.
51. D. B. Spalding, A General Purpose Computer Program for Multi-dimensional, One and Two Phase Flow, Rep. HTS/81/1, Imperial College, London, U.K., 1981.
52. D. B. Spalding, Development in the IPSA Procedure for Numerical Computation of Multiphase-Flow Phenomena with Interphase Slip, Unequal Temperatures, in T. M. Shih (ed.), *Numerical Methodologies in Heat Transfer, Proc. Second National Symposium*, pp. 421–436, New York, Hemisphere, 1983.
53. F. M. Harlow and A. A. Amsden, Numerical Calculations of Multiphase Flow, *J. Comput. Phys.*, vol. 17, pp. 19–52, 1975.
54. H. B. Stewart, Stability of Two-Phase Flow Calculation Using Two-Fluid Models, *J. Comput. Phys.*, vol. 33, pp. 259–270, 1979.
55. W. W. Rivard and M. D. Torrey, KFIX: A Program for Transient Two Dimensional Two Fluid Flow, Rep. LA-NUREG-6623, 1978.
56. A. A. Amsden and F. H. Harlow, KACHINA: A Eulerian Computer Program for Multifield Flows, Rep. LA-NUREG-5680, 1975.
57. A. A. Amsden and F. H. Harlow, KTIFA: Two-Fluid Computer Program for Down Comer Flow Dynamics, Rep. LA-NUREG-6994, 1977.
58. J. H. Mahaffy, A Stability Enhancing Two-Step Method for One Dimensional Two-Phase Flow, Rep. NUREG/CR-0971, 1979.
59. H. B. Stewart, Fractional Step Methods for Thermohydraulic Calculation, *J. Comput. Phys.*, vol. 40, pp. 77–80, 1981.
60. H. B. Stewart and B. Wendroff, Two-Phase Flow: Models and Methods, *J. Comput. Phys.*, vol. 56, pp. 363–409, 1984.
61. L. L. Smith, SIMMER-II: A Computer Program for LMFBR Disrupted Core Analysis, Rep. NUREG/VR-0453, 1980.
62. D. R. Liles, TRAC-PF1, An Advanced Best Estimate Computer Program for Pressurized Water Reactor Analysis, LANL, NUREG/CR-0065, 1982.
63. M. B. Carver, Numerical Computation of Phase Distribution in Two Fluid Flow Using the Two Dimensional TOFFEA Code, Rep. AECL-8066, Atomic Energy of Canada Limited, 1983.
64. M. B. Carver, Numerical Computation of Phase Separation in Two Fluid Flow, *J. Fluid Eng.*, vol. 106, pp. 147–153, 1985.
65. A. H. A. Baghdadi, Numerical Modelling of Two-Phase Flow with Inter-Phase Slip, Ph.D. thesis, Imperial College, London, U.K., 1979.
66. D. B. Spalding, Developments in the IPSA Procedure for Numerical Computation of Multi-phase Flow Phenomena with Inter-phase Slip, Unequal Temperatures, etc., Rep. HTS/81/11, Imperial College, London, U.K., 1981.

67. S. M. Lo, Multiphase Flow Model in Harwell-FLOW#D Computer Code, Rep. AEA-InTec-0062, 1990.
68. D. B. Spalding and N. C. Markatos, Computer Simulation of Multi-phase Flows: A Course of Lectures and Computer Workshops, Rep. CFD/83/4, Imperial College, London, U.K., 1983.
69. D. B. Spalding, The Numerical Computation of Multi-phase Flows, Rep. CFD/85/7, Imperial College, London, U.K., 1985.
70. P. J. Zwart, G. D. Raithby, and M. J. Raw, An Integrated Space-Time Finite-Volume Method for Moving-Boundary Problems, *Numer. Heat Transfer B*, vol. 34, pp. 257–270, 1998.
71. B. S. Baldwin and H. Lomax, Thin Layer Approximation and Algebraic Model for Separated Turbulent Flows, AIAA Paper 78-257, 1978.
72. F. Sotiropoulos and V. C. Patel, Application of Reynolds-Stress Transport Models to Stern and Wake Flow, *J. Ship Res.*, vol. 39, p. 263, 1995.
73. D. Cokljat, V. A. Ivanov, F. J. Srasola, and S. A. Vasquez, Multiphase K-Epsilon Models for Unstructured Meshes, ASME 2000 Fluids Engineering Division Summer Meeting, Boston, MA, 11–15 June 2000.
74. R. C. Mehta and T. Jayachandran, A Fast Algorithm to Solve Viscous Two-Phase Flow in an Axi-symmetric Rocket Nozzle, *Int. J. Numer. Meth. Fluids*, vol. 26, pp. 501–517, 1998.
75. J. Y. Tu and C. A. Fletcher, Numerical Computation of Turbulent Gas-Solid Particle Flow in a 90° Bend, *AIChE J.*, vol. 41, pp. 2187–2197, 1995.
76. M. J. Schuh, C. A. Schuler, and J. A. C. Humphrey, Numerical Calculation of Particle-Laden Gas Flows Past Tubes, *AIChE J.*, vol. 35, pp. 466–480, 1989.
77. W. T. Hancox and S. Banerjee, Numerical Standards for Flow Boiling Analysis, *Nuclear Sci. Eng.*, vol. 64, p. 106, 1977.
78. M. B. Carver, A Method of Limiting Intermediate Values of Volume Fraction in Iterative Two-Fluid Computations, *J. Mech. Eng. Sci.*, vol. 24, pp. 221–224, 1982.
79. D. B. Spalding, Calculation of Two Dimensional Two-Phase Flows Two-Phase Momentum, in F. Durst et al. (eds.), *Heat and Mass Transfer in Chemical Process and Energy Engineering Systems*, Hemisphere, Washington, DC, 1979.