Mass Transfer

Spring 2017

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http://www.jamescannon.net/teaching/mass-transfer

http://raw.githubusercontent.com/NanoScaleDesign/MassTransfer/master/mass_transfer.pdf

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Contents

0	Cou	rse information 5
	0.1	This course
		0.1.1 What you need to do
		0.1.2 How this works
		0.1.3 Assessment
	0.2	Timetable
	0.3	Presentations
	0.4	Hash-generation
1	Diff	usion 11
	1.1	Definition of Mass Transfer
	1.2	Diffusion in the long time limit
	1.3	Definitions of quantities I
	1.4	Definitions of quantities II
	1.5	Mass diffusivity
	1.6	Cases of diffusion
	1.7	Diffusion coefficient equivalency
	1.8	Saturated water vapour pressure
	1.9	Evaporation through a pore
	1.10	Evaporation pan
	1.11	Stationary Medium
	1.12	Stationary Medium Approximation
	1.13	Steady-state definition
	1.14	Steady-state diffusion planer example I
	1.15	Steady-state diffusion planer example II
	1.16	Steady-state diffusion through flat surface
	1.17	Steady-state diffusion in pipe walls
	1.18	Raoult's law
\mathbf{A}	Sup	porting challenges 31
	A.1	Partial pressure and humidity
	A.2	Pressure and molar density
	A.3	Specific volume
		Molar density of air

Chapter 0

Course information

0.1 This course

This is the Spring 2017 Mass Transfer graduate course at Kyushu University.

0.1.1 What you need to do

- Borrow the book "Principles of Heat and Mass Transfer", 7th Edition, by Incropera et. al. from the Mechanical Engineering Office on the 4th floor of West 4. The course will be based on that book and you will need to refer to it in class.
- Prepare a challenge-log in the form of a workbook or folder where you can clearly write the calculations you perform to solve each challenge. This will be used in the final assessment and will be occasionally reviewed by the teacher.
- Submit a weekly feedback form by **8am on Monday** before class at https://goo.gl/forms/bFAcVvwXstWgwXbG3.
- Please bring a wifi-capable internet device to class, as well as headphones if you need to access online components of the course during class. If you let me know in advance, I can lend computers and provide power extension cables for those who require them (limited number).

0.1.2 How this works

- This booklet forms part of an active-learning segment in the course. The learning is self-directed in contrast to the traditional lecture-style model.
- Learning is guided through solving a series of challenges combined with instant feedback about the correctness of your answer.
- Traditional lectures are replaced by discussion time. Here, you are encouraged to discuss any issues with your peers, teacher and any teaching assistants. You can also learn from explaining concepts to your peers.
- Discussion-time is from 10:30 to 12:00 on Mondays at room Engineering-2.
- Peer discussion is encouraged, however, if you have help to solve a challenge, always make sure you do understand the details yourself. You will need to be able to do this in an exam environment. The questions on the exam will be similar in nature to the challenges. If you can do all of the challenges, you can get 100% on the exam.
- Every challenge in the book typically contains a **Challenge** with suggested **Resources** which you are recommended to utilise in order to solve the challenge. **Solutions** will be given. Occasionally the teacher will provide extra **Comments** to help guide your thinking.
- For deep understanding, it is recommended to study the suggested resources beyond the minimum required to complete the challenge.
- The challenge document has many pages and is continuously being developed. Therefore it is advised to view the document on an electronic device rather than print it. The date on the front page denotes the version of the document. You will be notified when the document is updated.
- A target challenge will be set each week. This will set the pace of the course and define the examinable material. It's ok if you can't quite reach the target challenge for a given week, but you should be careful not to fall behind, since the date of the exam cannot be delayed.

0.1.3 Assessment

In order to prove to outside parties that you have learned something from the course, we must perform summative assessments. You will receive a weighted score based on:

- \bullet Challenge-log (20%) final state at the end of the course, showing your calculations for all the challenges in the course.
- Presentation (30%)
- Final exam (50%)

 $\label{eq:final score} Final\ score = MAX(Weighted\ score,\ Final\ exam)$

0.2 Timetable

	Discussion	Target	Note
1	5 June	-	
2	12 June	1.7	
3	19 June	1.12	
4	26 June	1.17	
5	3 July		
6	13 July		Presentations
-	24 July	-	Final exam

So for example, you should aim to complete challenge 1.7 by the 12th of June.

0.3 Presentations

Due to limited time, classes will mostly focus on diffusive mass transfer, however convective mass transfer is also an important mode of mass transport. Your task is to undertake a research project to learn about convective mass transfer, and then present to the class about any application of convective mass transfer that you find interesting. Presentation time will be 8 minutes. Chapter 9 of the book has a good summary of the subject.

For maximum marks you should do the following:

- Ensure that your presentation is 7:00-8:00 minutes long. Timing will be strictly kept.
- Include a basic description of equations related to your chosen subject.
- Include at least 1 graph.
- Clearly demonstrate understanding (showing calculation examples is a good way to do this).
- Demonstrate a novel application of convective heat mass transfer.
- Ensure the work is your own and you cite all references, as well as images and text taken from other sources.
- Pitch the presentation at a level whereby your classmates can follow your discussion.
- Explain accuratly and clearly.
- Talk in either English or Japanese.
- Write any text on the slides mostly (90%+) in English.

Note: The application that you describe can does not have to be originally invented by you (although you are welcome to propose an application like this if you wish). The application may already exist, but you will need to demonstrate understanding about the application and calculations involved in the use of convective mass transfer.

0.4 Hash-generation

Some solutions to challenges are encrypted using MD5 hashes. In order to check your solution, you need to generate its MD5 hash and compare it to that provided. MD5 hashes can be generated at the following sites:

- Wolfram alpha: (For example: md5 hash of "q_1.00") http://www.wolframalpha.com/input/?i= md5+hash+of+%22q_1.00%22
- www.md5hashgenerator.com

Since MD5 hashes are very sensitive to even single-digit variation, you must enter the solution exactly. This means maintaining a sufficient level of accuracy when developing your solution, and then entering the solution according to the format below:

Unless specified otherwise, any number from 0.00 to ± 9999.99 should be represented as a normal number to two decimal places. All other numbers should be in scientific form. See the table below for examples.

Solution	Input
1	1.00
-3	-3.00
-3.5697	-3.57
0.05	0.05
0.005	5.00e-3
50	50.00
500	500.00
5000	5000.00
50,000	5.00e4
5×10^{-476}	5.00e-476
5.0009×10^{-476}	5.00e-476
$-\infty$	-infinity (never "infinite")
2π	6.28
i	im(1.00)
2i	im(2.00)
1+2i	re(1.00)im(2.00)
-0.0002548 i	im(-2.55e-4)
1/i = i/-1 = -i	im(-1.00)
$e^{i2\pi} \left[= \cos(2\pi) + i\sin(2\pi) = 1 + i0 = 1 \right]$	1.00
$e^{i\pi/3} [= \cos(\pi/3) + i\sin(\pi/3) = 0.5 + i0.87]$	re(0.50)im(0.87)
Choices in order A, B, C, D	abcd

Entry format is given with the problem. So "q_X" means to enter "q_X" replacing "X" with your solution. The first 6 digits of the MD5 sum should match the given solution $(MD5(q_X) = ...)$.

Note that although some answers can usually only be integers (eg, number of elephants), unless otherwise indicated you should always enter an integer to two decimal places (ie, with ".00" after it) to generate the correct hash.

Chapter 1

Diffusion

1.1 Definition of Mass Transfer

Resources

ullet Chapter 14, introduction

Challenge

Add the points of the following conditions which constitute diffusive mass-transfer

1 point: Evaporation of water vapour into the air

2 points: Water being pumped through a pipe

4 points: Dissolving of sugar into tea

8 points: Aeration of waste-water

16 points: Motion of air around a room due to the presence of a fan

Solution

(Enter as an integer)

 $MD5(a_X) = b786dd...$

1.2 Diffusion in the long time limit

Resources

• Book: 14.1.1 to 14.1.2

• Video: https://www.youtube.com/watch?v=-FLvOuxLrDI

Challenge

Consider a box of volume $1\,\mathrm{m}^3$. The box contains 1 mole of gas. At time t=0, all the gas molecules in the left 1/4 of the box are labeled A. As time goes to $t=\infty$, what will the density of the molecules labeled A be in the right half of the box? Note that there is only 1 species of gas in the box.

Solution

Units: Moles / m^3 (enter to two decimal places) $\mathrm{MD5(b_X)} = 13c60a...$

1.3 Definitions of quantities I

Resources

• Book: 14.1.1 to 14.1.2

• Video: https://www.youtube.com/watch?v=-FLvOuxLrDI

Challenge

Assuming air is made up exclusively of oxygen and nitrogen with their partial pressures in the ratio 0.21:0.79, what are their mass-fractions?

Solutions

Oxygen: 0.233 Nitrogen: 0.767

1.4 Definitions of quantities II

Resources

• Book: 14.1.1 to 14.1.2

• Video: https://www.youtube.com/watch?v=-FLvOuxLrDI

Challenge

Japan imports substantial amounts of LNG which is a mixture of the following gases:

Liquid	Mol %
Methane	93.5
Ethane	4.6
Propane	1.2
Carbon dioxide	0.7

The masses of Methane, Ethane, Propane and Carbon Dioxide are 16, 30, 44 and 44 g/mol respectively. Assuming ideal gases, calculate the following:

- 1. The mole-fraction of ethane
- 2. The mass-fraction of ethane
- 3. The average molecular mass of the mixture
- 4. The mass-density of the gas when heated to 207 K under a total pressure of $1.4 \times 10^5 \, \mathrm{Pa}$
- 5. The partial pressure of the methane when the total pressure is $1.4 \times 10^5 \,\mathrm{Pa}$

Solutions

- 1. (enter as a decimal to 3 decimal places) $MD5(c_X) = 117398...$
- 2. (enter as a decimal to 3 decimal places) MD5(d₋X) = 6801da...
- 3. (enter as a decimal to 3 decimal places in units of g/mol) $MD5(e_X) = e3a65e...$
- $4. 1397 \,\mathrm{kg} \,\mathrm{m}^{-3}$
- 5. (enter as an integer in units of kPa) $MD5(f_X) = f54c28...$

Mass diffusivity 1.5

Resources

 \bullet Book: 14.1.3 - 14.1.4, Table A-8

Challenge

Estimate the mass diffusivity of the following gases in air at $350~\mathrm{K}$ and $1~\mathrm{atm}$ pressure:

- 1. Ammonia
- 2. Hydrogen

Solutions

- $\begin{array}{l} 1. \;\; 0.36 \times 10^{-4} \; \mathrm{m^2 \, s^{-1}} \\ 2. \;\; 0.52 \times 10^{-4} \; \mathrm{m^2 \, s^{-1}} \end{array}$

1.6 Cases of diffusion

Resources

• Book: 14.1.3 - 14.1.4

Challenge

Considering air in a closed, cylindrical container with its axis vertical and with opposite ends maintained at different temperatures. Assume the total pressure of the air is uniform throughout the container.

Consider each of the following conditions:

- 1. The bottom surface is colder than the top surface
- 2. The top surface is colder than the bottom surface

For each condition, write a few sentences explaining a) if there is any motion of the air and b) if mass transfer occurs.

Solutions

Please compare your answer with your partner.

1.7 Diffusion coefficient equivalency

Resources

• Video: https://www.youtube.com/watch?v=NTlR18NyqAE

${\bf Challenge}$

Prove that in a binary mixture, the diffusion coefficient of gas "A" in "B" is the same as the diffusion coefficient of gas "B" in "A" (ie, $D_{AB} = D_{BA}$).

1.8 Saturated water vapour pressure

Resources

• http://www.chemguide.co.uk/physical/phaseeqia/vapourpress.html

Challenge

Write a few sentences briefly explaining what is meant by "Saturated Vapour Pressure".

Solution

Compare your answer with your partner

1.9 Evaporation through a pore

Resources

• Book 14.2 (be sure to follow the derivation of column evaporation)

Challenge

In your challenge log, work through example 14.2 (you do not need to include the "comments" part in your challenge log).

1.10 Evaporation pan

Resources

- Book 14.2, Tables A-6 and A-8
- Challenges in Appendix A

Comments

You have studied that the molar fraction of species i (x_i) can be calculated directly from the ratio of molar densities (C_i/C) or equivalently through Dalton's law (p_i/p). In the case where p is the saturation partial pressure of water vapour (ie, $p_{\rm wv}/p_{\rm wv,sat}$), the molar fraction $x_{\rm wv}$ is equivalent to the relative humidity.

Challenge

Evaporation pans like the one shown are used to measure the rate of evaporation of water in a local area.



(image: Bidgee, Wikipedia)

An evaporation pan is placed in a location with an ambient air temperature of $300\,\mathrm{K}$ and relative humidity of 25%. The pan contains water at the same temperature as the surrounding air. The pan has a diameter of $20\,\mathrm{cm}$ and height of $160\,\mathrm{mm}$, and it starts half-full of water.

- 1. Assuming only diffusive mass transport, what is the initial evaporation rate?
- 2. Including the effects of advection, what is the initial evaporation rate?

Solution

- 1. $1.087 \times 10^{-8} \,\mathrm{kmol}\,\mathrm{s}^{-1}$
- 2. $1.108 \times 10^{-8} \,\mathrm{kmol}\,\mathrm{s}^{-1}$

1.11 Stationary Medium

Resources

• Video: https://www.youtube.com/watch?v=F0deXOH_YEM

Challenge

- 1. Briefly explain what is meant by a stationary medium.
- 2. Considering a stationary medium of 3 species "A", "B" and "C", if the flux of species "A" is $2 \,\mathrm{kmol}\,\mathrm{m}^{-2}\,\mathrm{s}^{-1}$ and "B" is $-8 \,\mathrm{kmol}\,\mathrm{m}^{-2}\,\mathrm{s}^{-1}$, what is the flux of species "C"?
- 3. Considering a binary system of atoms "A" and "B" with concentration $5 \,\mathrm{kmol}\,\mathrm{m}^{-3}$ and $10 \,\mathrm{kmol}\,\mathrm{m}^{-3}$ respectively, if the molar velocity of species "A" is $2 \,\mathrm{m}\,\mathrm{s}^{-1}$, what is the molar velocity of species "B"?

Solutions

- 1. Please compare your answer with your partner
- 2. (enter to two decimal places in units of kmol m⁻² s⁻¹) $MD5(g_X) = 2c32d8...$
- 3. (enter to two decimal places in units of $\rm m\,s^{-1})~MD5(h_X) = 3ccbb4...$

1.12 Stationary Medium Approximation

Resources

• Book 14.3

${\bf Challenge}$

In a few sentences, describe what is meant by the stationary medium approximation. Give at least one real-world example each of case where the stationary medium approximation would and would-not be appropriate.

Solution

Compare your answer with your partner

1.13 Steady-state definition

Resources

• Web: http://www.virginia.edu/bohr/mse209/chapter5.htm

Challenge

The example in section 14.4.3 talks of steady state conditions.

- 1. Write a sentence or two explaining what is meant by steady-state conditions in this context.
- 2. What is $\delta J(x)/\delta t$ at any given position x under a steady-state condition?

Solutions

1. Please compare your answer with your partner

2.

X = Your solution

Form: Decimal, to 1 decimal place

Place the indicated letter in front of the number Example: aX where X=42.5 is entered as a42.5

hash of aX = 9497cd

1.14 Steady-state diffusion planer example I

Resources

• Book: 14.4.1 to 14.4.3

• Video: https://youtu.be/4KACai1gYzc

Challenge

Work through the calculation from equations 14.51 to 14.54, showing your reasoning along the way. Don't worry about the concept of diffusion resistance for now.

1.15 Steady-state diffusion planer example II

Resources

• Book: 14.4.1 to 14.4.3

• Video: https://youtu.be/4KACai1gYzc

${\bf Challenge}$

Work through example 14.3 in section 14.4.3.

1.16 Steady-state diffusion through flat surface

Resources

• Book: 14.4.1 to 14.4.3

Challenge

A thin plastic membrane is used to maintain separation between helium and an outer chamber. Under steady-state conditions, the concentration of helium is $0.02\,\mathrm{kmol\,m^{-3}}$ and $0.005\,\mathrm{kmol\,m^{-3}}$ at the inner and outer boundaries respectively. If the membrane is $1\,\mathrm{mm}$ thick and the binary diffusion coefficient of helium in the plastic membrane is $10^{-9}\,\mathrm{m^2\,s^{-1}}$, what is the diffusive flux through the membrane in terms of kmol s⁻¹ m⁻² and kg s⁻¹ m⁻²?

Solution

$$\begin{array}{l} 1.5\times10^{-8}\,\mathrm{kmol\,s^{-1}\,m^{-2}} \\ 6.0\times10^{-8}\,\mathrm{kg\,s^{-1}\,m^{-2}} \end{array}$$

1.17 Steady-state diffusion in pipe walls

Resources

• Book: 14.4.1 to 14.4.3

Challenge

A pipe with inner-radius $10\,\mathrm{cm}$ and outer-radius $13\,\mathrm{cm}$ is carrying hydrogen. The concentration of hydrogen inside the pipe is $0.07\,\mathrm{kmol}\,\mathrm{m}^{-3}$ and outside the pipe is $0.04\,\mathrm{kmol}\,\mathrm{m}^{-3}$. If the hydrogen has a diffusion coefficient of $10^{-8}\,\mathrm{m}^2\,\mathrm{s}^{-1}$ in the walls of the pipe, at what rate is hydrogen lost from the pipe, per metre length of pipe?

Solution

 $7.18\times 10^{-9}\,{\rm kmol\,s^{-1}}$

1.18 Raoult's law

Resources

• Book: 14.5.1

Challenge

Considering a puddle of water exposed to the atmosphere at 17 °C, calculate:

- 1. The molar fraction of water vapour on the air-side of the water-air interface.
- 2. The mass fraction of water vapour on the air-side of the water-air interface.
- 3. The molar fraction of water vapour on the water-side of the water-air interface.
- 4. The mass fraction of water vapour on the water-side of the water-air interface.

Solution

1. 0.019

2. 0.012

3.

X = Your solution

Form: Decimal, to 3 decimal places

Place the indicated letter in front of the number Example: aX where X = 42.544 is entered as a42.544

ab bX = 4b5ab9

4.

X = Your solution

Form: Decimal, to 3 decimal places

Place the indicated letter in front of the number Example: aX where X=42.544 is entered as a42.544

hash of cX = 737b49

Appendix A

Supporting challenges

A.1 Partial pressure and humidity

Challenge

If the saturation pressure of water in air at a given temperature is $0.02\,\mathrm{bar}$ and the relative humidity of the air is 30%, calculate the partial pressure of the water vapour in the air.

Solution

X = Your solution

Form: Decimal, to 3 decimal places

Place the indicated letter in front of the number Example: aX where X=42.544 is entered as a42.544

 $hash\ of\ dX=f8dcaa$

A.2 Pressure and molar density

Challenge

Given that the saturation pressure of water in air at a given temperature is $0.05\,\mathrm{bar}$ with a saturated molar density of $5\,\mathrm{kmol}\,\mathrm{m}^{-3}$, if the partial pressure of water in the air is $0.01\,\mathrm{bar}$, calculate the molar density of the water in the air.

Solution

X = Your solution

Form: Decimal, to 1 decimal place

Place the indicated letter in front of the number Example: aX where X=42.5 is entered as a42.5

hash of eX = 1c8d37

A.3 Specific volume

Challenge

Referring to the specific volume of saturated water at 290 K in table A-6 (v_g) , what is the saturated molar concentration? You cannot assume this is an ideal gas.

Solution

 $7.97 \times 10^{-4} \, \rm kmol \, m^{-3}$

A.4 Molar density of air

Challenge

Assuming air to be an ideal gas, calculate the molar density of air, C_{air} at 300 K and atmospheric pressure.

Solution

 $4.1 \times 10^{-2} \, \rm kmol \, m^{-3}$