

**Pandit Deendayal Energy University**  
**Academic Year 2023-2024**  
**Computational Engineering Laboratory**

**PRESENTATION ON MATLAB CASE STUDY**

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# Case Study 1

# Problem Statement

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**To Solve a problem on Heat Transfer of Natural Convection in H – Shaped Cavity.**

# Derivations

## Case Study -1 Equations

\* The derivation ~~the~~ the equations we need :-

1) Governing equations :-

$$\nabla \cdot \mathbf{V} = 0$$

It's represents conservation of mass.

2) Navier Stokes equation :-

$$\rho \left( \frac{\partial \mathbf{V}}{\partial t} + \mathbf{V} \cdot \nabla \mathbf{V} \right)$$

$$= -\nabla P + \mu \nabla^2 \mathbf{V} + \rho \mathbf{g}$$

It's represents the Conservation Momentum.

3) Energy equations :-

$$\rho c_p \left( \frac{\partial T}{\partial t} + \mathbf{V} \cdot \nabla T \right) = k \nabla^2 T$$

It's represents the Conservation of energy.

# Assumptions on Equation

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1. **Steady State Conduction :  $d/dt=0$**
2. **Incompressible Flow :  $\nabla \cdot \mathbf{v} = 0$**
3. **Boussinesq approximation (Density Variation with Compression):  $\rho = \rho_0(1 - \beta(T - T_0))$**
4. **Negligible viscous Dissipation : Neglecting the Various terms  $\mu \nabla^2 \mathbf{v}$**
5. **Constant Fluid Properties :  $\rho, \mu, k$  and  $C_p$  are Constant within the Domain**

# Matlab Code

```
title('Temperature Distribution in H-Shaped Cavity');
% Parameters
L = 1; % Length of cavity
W = 1; % Width of cavity
H = 0.1; % Height of cavity
T_hot = 100; % Temperature of hot wall
T_cold = 0; % Temperature of cold walls
nx = 51; % Number of grid points in x-direction
ny = 51; % Number of grid points in y-direction
dx = L/(nx-1); % Grid spacing in x-direction
dy = W/(ny-1); % Grid spacing in y-direction
max_iter = 1000; % Maximum number of iterations
tolerance = 1e-5; % Convergence tolerance

% Initialization
T = ones(nx, ny) * T_cold; % Initialize temperature array

% Main loop (iterate until convergence)
for iter = 1:max_iter
    % Boundary conditions
    T(:,1) = T_cold; % Left cold wall
    T(:,end) = T_cold; % Right cold wall
    T(1,:) = T_hot; % Hot wall

    % Compute temperature field using simple averaging
    T_new = T;
    for i = 2:nx-1
        for j = 2:ny-1
            % Average of neighboring points
            T_new(i,j) = 0.25*(T(i+1,j) + T(i-1,j) + T(i,j+1) + T(i,j-1));
        end
    end

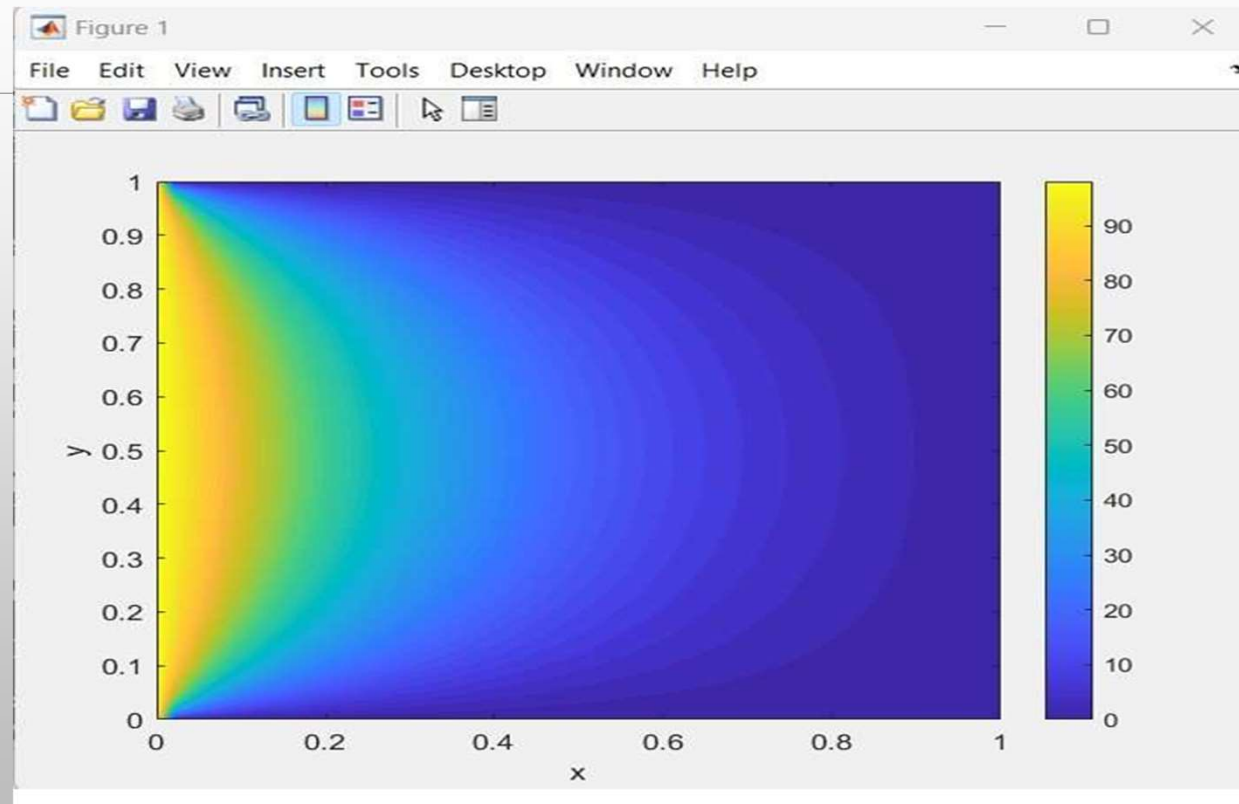
    % Check for convergence
```

```
if max(abs(T_new(:) - T(:))) < tolerance
    disp(['Converged at iteration ', num2str(iter)]);
    break;
end

% Update temperature array
T = T_new;
end

% Plotting the results
[X, Y] = meshgrid(linspace(0,L,nx), linspace(0,W,ny));
contourf(X, Y, T', 50, 'LineColor', 'none');
colorbar;
xlabel('x');
ylabel('y');
```

# Results





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# Case Study 2

# Problem Statement

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**To Update the code on the problem on Heat Transfer of Natural Convection in H – Shaped Cavity.**

# Derivations

## Case Study 2 Equations

\* To derive the equations:-

⇒ Governing equations:-

Start with the continuity equation:-

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

By using Navier-Stokes equations (momentum equation):

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + g_x$$

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) + g_y$$

Then,

$$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha \left( \frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right)$$

# Matlab Code

```
% Parameters
L = 1;           % Length of cavity
W = 1;           % Width of cavity
H = 0.1;        % Height of cavity
T_hot = 100;     % Temperature of hot wall
T_cold = 0;      % Temperature of cold walls
nx = 51;         % Number of grid points in x-direction
ny = 51;         % Number of grid points in y-direction
dx = L/(nx-1);  % Grid spacing in x-direction
dy = W/(ny-1);  % Grid spacing in y-direction
max_iter = 100; % Maximum number of iterations
tolerance = 1e-5; % Convergence tolerance
alpha = 0.1;    % Thermal diffusivity

% Initialize temperature array
T = ones(nx, ny) * T_cold;

% Set up VideoWriter object

writerObj = VideoWriter('temperature_evolution.avi'); % Specify the file name
writerObj.FrameRate = 10; % Set the frame rate

% Open the video writer object
open(writerObj);

% Create a figure for animation
figure;

% Main loop (iterate until convergence)
for iter = 1:max_iter
    % Boundary conditions
    T(:,1) = T_cold;           % Left cold wall
    T(:,end) = T_cold;         % Right cold wall
    T(1,:) = T_hot;            % Hot wall
    T(ceil(end/2-round(H/(2*dy))):floor(end/2+round(H/(2*dy))), end) = T_cold; % Middle cold wall

    % Compute temperature field using finite difference method
    T_new = T;
    for i = 2:nx-1
        for j = 2:ny-1
            % Finite difference equation
```

# Matlab Code

```
        T_new(i,j) = T(i,j) + alpha * ( (T(i+1,j) - 2*T(i,j) + T(i-1,j))/dx^2 + (T(i,j+1) - 2*T(i,j) + T(i,j-1))/dy^2 );
    end
end

% Check for convergence
if max(abs(T_new(:) - T(:))) < tolerance
    disp(['Converged at iteration ', num2str(iter)]);
    break;
end

% Update temperature array
T = T_new;

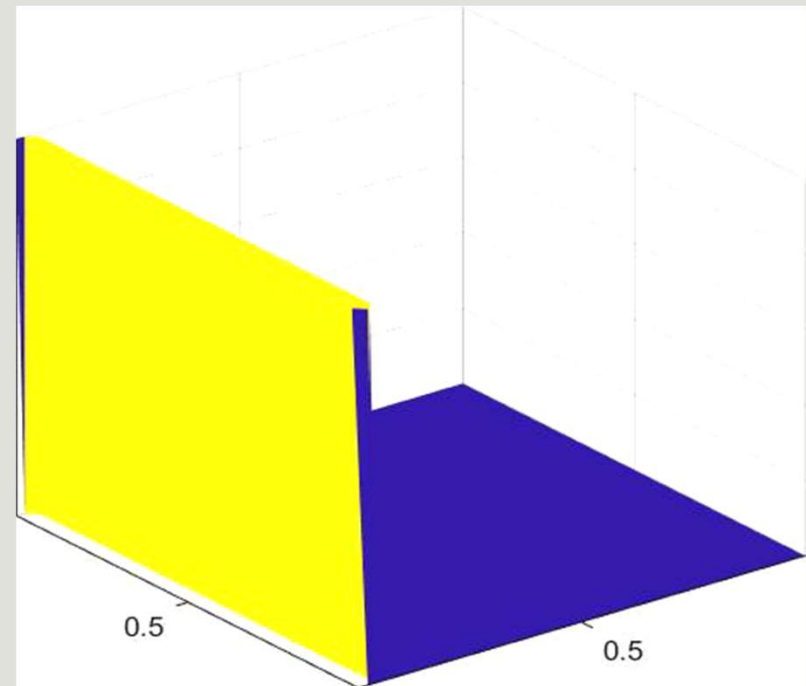
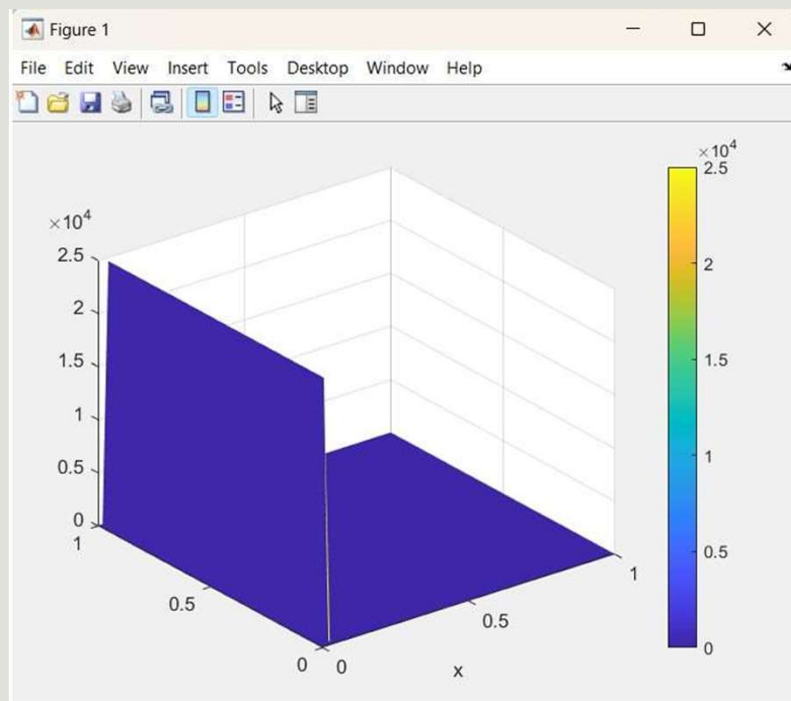
% Plot the current temperature distribution in 3D
[X, Y] = meshgrid(linspace(0,L,nx), linspace(0,W,ny));
surf(X, Y, T, 'EdgeColor', 'none');
colorbar;
xlabel('x');
title(['Iteration: ', num2str(iter)]);
axis([0 L 0 W 0 100]); % Set axis limits for consistency

% Capture the frame
frame = getframe(gcf);

% Write the frame to the video file
writeVideo(writerObj, frame);
end

% Close the video writer object
close(writerObj);
```

# Results



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**Thank You**