

The Reynolds Transport Theorem

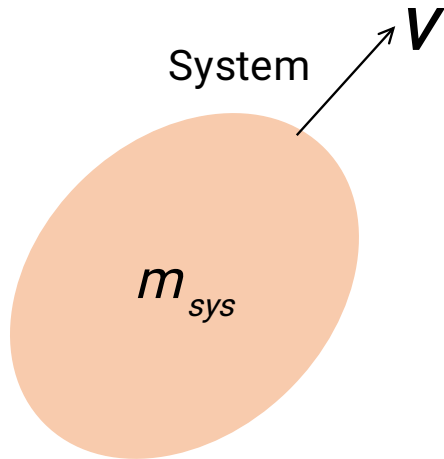
Conservation parameters: mass (m), momentum ($m\vec{V}$) and energy (E)

	B	$b=B/m$
Mass	m	1
Momentum	$m\vec{V}$	\vec{V}
Energy	E	e

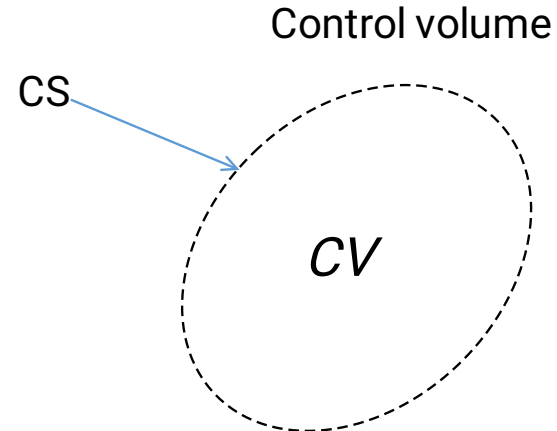
B - Any flow parameter

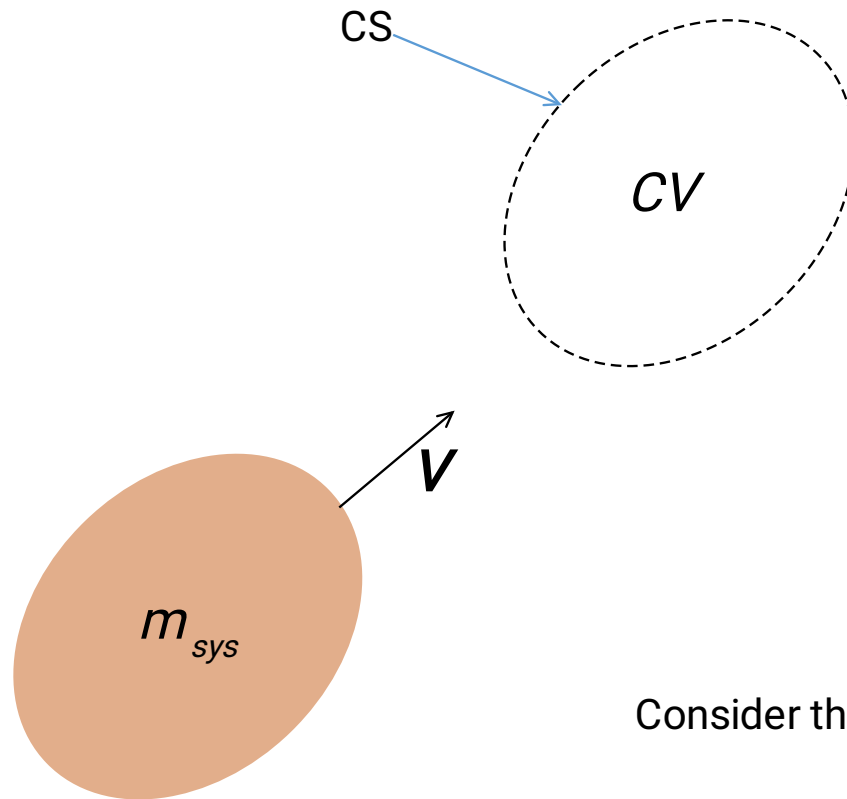
b - Amount of that parameter per unit mass = B/m

Consider a



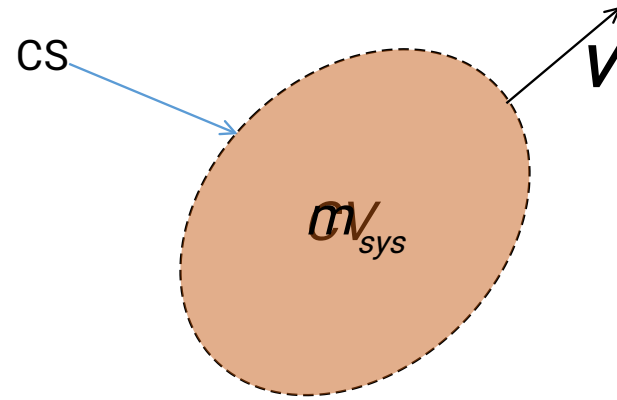
and





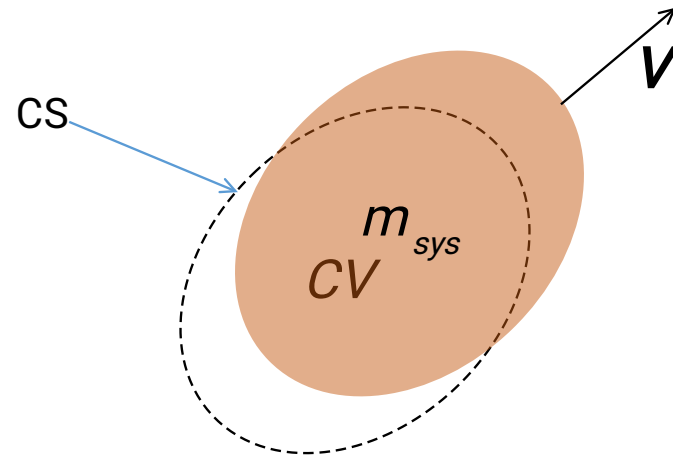
Consider the case of System flowing through the Control Volume

At a time instant t



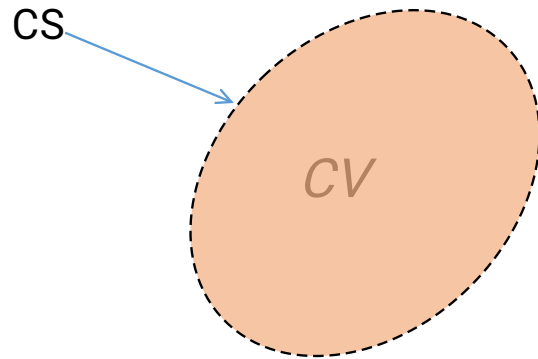
the system occupies the control volume

At a time instant $t + \delta t$



the system moves out of CV

At time t



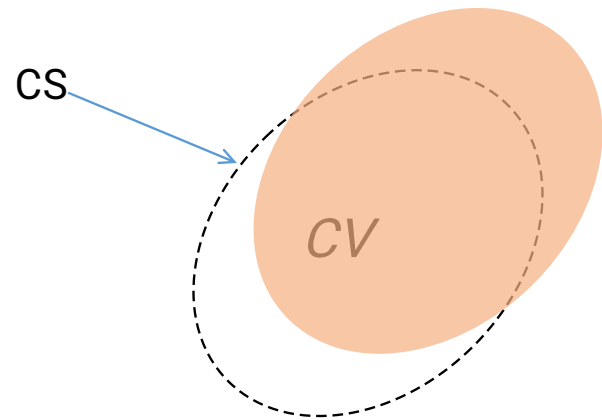
At time t , the system occupies the control volume

$$\text{Sys} = \text{CV}$$

At time t ,

$$B_{\text{sys}}(t) = B_{\text{CV}}(t)$$

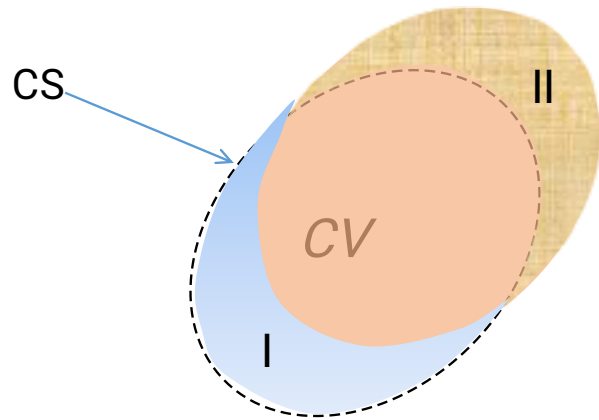
At time $t + \delta t$



At time $t + \delta t$, the system moving out of CV

System =

At time $t + \delta t$



At time $t + \delta t$, the system moving out of CV

$$\text{Sys} = \text{CV} - \text{I} + \text{II}$$

At time $t + \delta t$,

$$B_{\text{sys}}(t + \delta t) = B_{\text{CV}}(t + \delta t) - B_{\text{I}}(t + \delta t) + B_{\text{II}}(t + \delta t)$$

Change in the amount of B in the system in the time interval δt is:

$$\begin{aligned}\frac{\delta B_{sys}}{\delta t} &= \frac{B_{sys}(t + \delta t) - B_{sys}(t)}{\delta t} \\&= \frac{B_{cv}(t + \delta t) - B_i(t + \delta t) + B_{ii}(t + \delta t) - B_{sys}(t)}{\delta t} \\&= \frac{B_{cv}(t + \delta t) - B_i(t + \delta t) + B_{ii}(t + \delta t) - B_{cv}(t)}{\delta t} \\ \Rightarrow \frac{\delta B_{sys}}{\delta t} &= \frac{B_{cv}(t + \delta t) - B_{cv}(t)}{\delta t} + \frac{B_{ii}(t + \delta t)}{\delta t} - \frac{B_i(t + \delta t)}{\delta t}\end{aligned}$$

Simplifying the above equation in the limit of $\delta t \rightarrow 0$

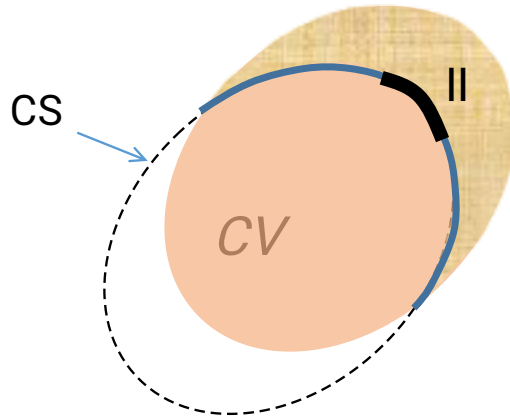
LHS:

$$\lim_{\delta t \rightarrow 0} \frac{\delta B_{sys}}{\delta t} = \frac{dB_{sys}}{dt} = \frac{DB_{sys}}{Dt}$$

First term on RHS:

$$\lim_{\delta t \rightarrow 0} \frac{B_{cv}(t + \delta t) - B_{cv}(t)}{\delta t} = \frac{\partial B_{cv}}{\partial t} = \frac{\partial}{\partial t} \iiint_{cv} \rho b \, dV$$

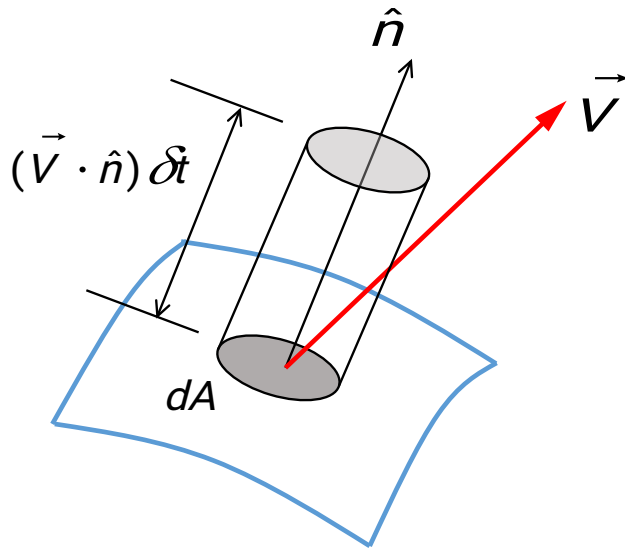
Second term on RHS:



$$\lim_{\delta t \rightarrow 0} \frac{B_{II}(t + \delta t)}{\delta t} = \dot{B}_{out}$$

the rate at which the extensive parameter B flows from the control volume across the control surface

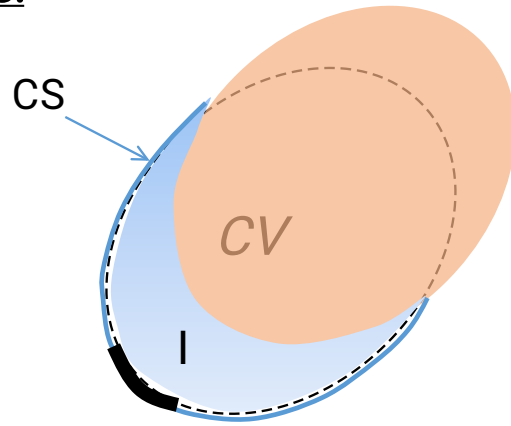
$$B_{II}(t + \delta t) = \iint_{CS_{out}} \rho b (\vec{V} \cdot \hat{n}) \delta t dA$$



$$\frac{B_{II}(t + dt)}{\delta t} = \iint_{CS_{out}} \rho b (\vec{V} \cdot \hat{n}) dA$$

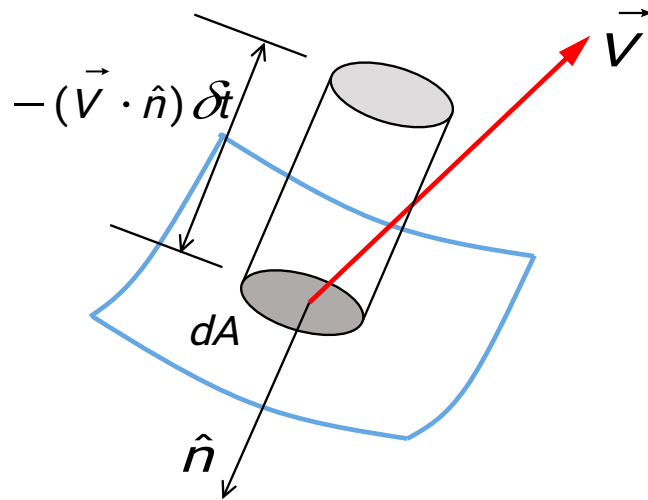
$$\Rightarrow \dot{B}_{out} = \iint_{CS_{out}} \rho b (\vec{V} \cdot \hat{n}) dA$$

Third term on RHS:



$$\lim_{\delta t \rightarrow 0} \frac{B_I(t + \delta t)}{\delta t} = \dot{B}_{in}$$

the rate at which the extensive parameter B flows into the control volume across the control surface



$$B_I(t + \delta t) = - \iint_{CS_{in}} \rho b (\vec{V} \cdot \hat{n}) \delta t dA$$

$$\Rightarrow \dot{B}_{in} = - \iint_{CS_{in}} \rho b (\vec{V} \cdot \hat{n}) dA$$

$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho b \, d\forall + \dot{B}_{out} - \dot{B}_{in}$$

$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho b \, d\forall + \iint_{CS_{out}} \rho b (\vec{V} \cdot \hat{n}) \, dA - \left(- \iint_{CS_{in}} \rho b (\vec{V} \cdot \hat{n}) \, dA \right)$$

$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho b \, d\forall + \oiint_{CS} \rho b (\vec{V} \cdot \hat{n}) \, dA$$

Reynolds transport theorem – Relates System to Control Volume

$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho b \, dV + \oiint_{CS} \rho b (\vec{V} \cdot \hat{n}) \, dA$$

Time rate of change of a parameter B of a system	=	Time rate of change of parameter B within the control volume as the fluid flows through it	+	Net flux of the parameter B across the control surface
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End of Reynolds Transport Theorem Derivation

$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho b \, dV + \oiint_{CS} \rho b (\vec{V} \cdot \hat{n}) \, dA$$

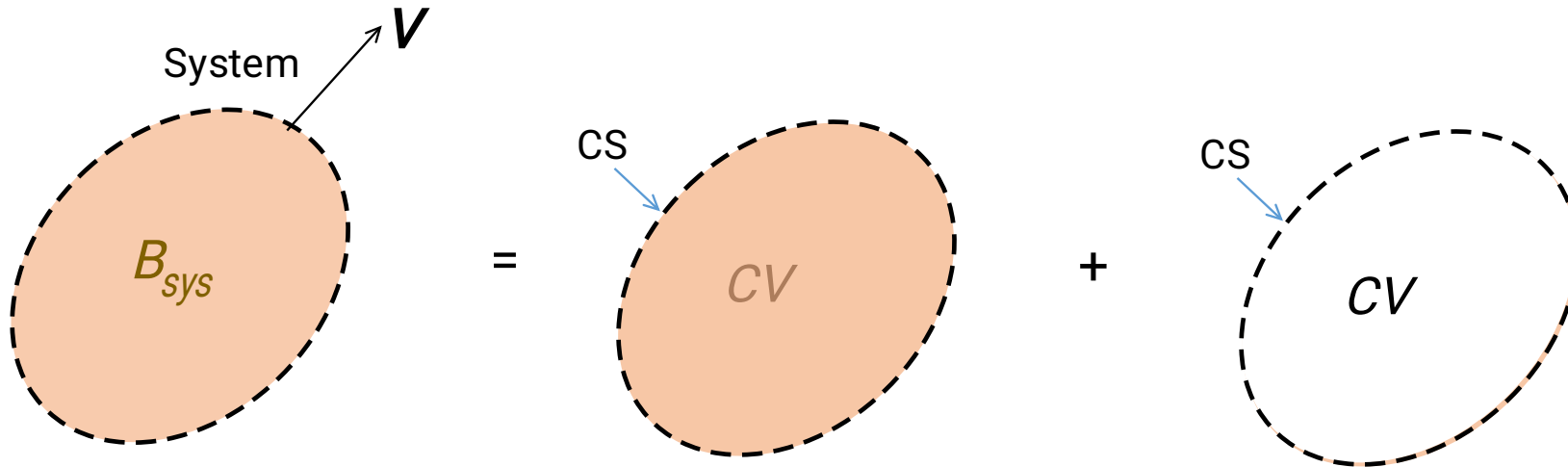
Time rate of change of a parameter B of a system

=

Time rate of change of parameter B within the control volume as the fluid flows through it

+

Net flux of the parameter B across the control surface



Governing equations expressed in Control Volume Concept:

RTT:
$$\frac{DB_{sys}}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho b \, d\forall + \oiint_{CS} \rho b (\vec{V} \cdot \hat{n}) \, dA$$

$$b = \frac{B}{m}$$

Mass conservation/Continuity:

Substituting $B = m \Rightarrow b = 1$ in RTT

$$\frac{Dm}{Dt} = \frac{\partial}{\partial t} \iiint_{CV} \rho \, d\forall + \oiint_{CS} \rho (\vec{V} \cdot \hat{n}) \, dA$$

$$\Rightarrow \frac{\partial}{\partial t} \iiint_{CV} \rho \, d\forall + \oiint_{CS} \rho (\vec{V} \cdot \hat{n}) \, dA = 0$$

Momentum conservation:

Substituting $B = m\vec{V} \Rightarrow b = \vec{V}$ in RTT

$$\frac{D(m\vec{V})}{Dt} = \frac{\partial}{\partial t} \iiint_{cv} \rho \vec{V} d\forall + \oiint_{cs} \vec{V} \rho (\vec{V} \cdot \hat{n}) dA$$

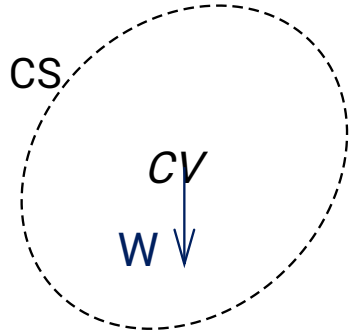
Newton's second law: $\frac{D(m\vec{V})}{Dt} = \sum \vec{F}$

$$\Rightarrow \frac{\partial}{\partial t} \iiint_{cv} \rho \vec{V} d\forall + \oiint_{cs} \vec{V} \rho (\vec{V} \cdot \hat{n}) dA = \sum \vec{F}$$

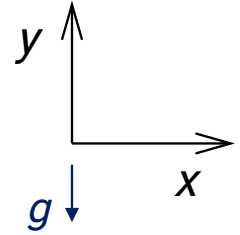
$$\Rightarrow \frac{\partial}{\partial t} \iiint_{cv} \rho \vec{V} d\forall + \oiint_{cs} \vec{V} \rho (\vec{V} \cdot \hat{n}) dA = \vec{F}_{body} + \vec{F}_{surface} + \vec{F}_{external}$$

\vec{F}_{body} :

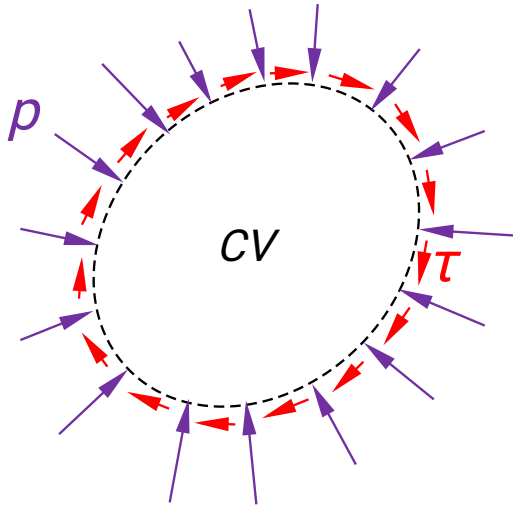
Body force – Weight of the control volume



$$\vec{F}_{body} = \vec{W} = \iiint_{CV} \rho \vec{g} d\forall$$



$\vec{F}_{surface}$:



$$\vec{F}_{surface} = \vec{F}_{pressure} + \vec{F}_{shear}$$

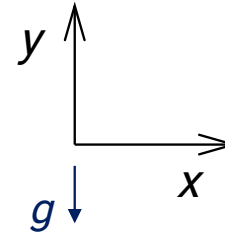
$$\vec{F}_{surface} = - \oint_{CS} p d\vec{A} + \oint_{CS} \vec{\tau} dA$$

Governing equations for control volume analysis

Continuity equation:

$$\frac{\partial}{\partial t} \iiint_{CV} \rho \, dV + \oiint_{CS} \rho (\vec{V} \cdot \hat{n}) \, dA = 0$$

$$\vec{V} = u\hat{i} + v\hat{j}$$



$$F_{x,body} = 0$$

$$F_{y,body} = -W$$

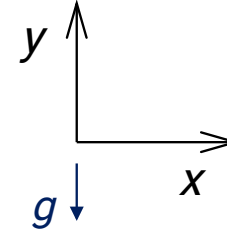
x-momentum equation:

$$\frac{\partial}{\partial t} \iiint_{CV} \rho u \, dV + \oiint_{CS} u \rho (\vec{V} \cdot \hat{n}) \, dA = F_{x,body} + F_{x,press} + F_{x,shear} + F_{x,ext}$$

y-momentum equation:

$$\frac{\partial}{\partial t} \iiint_{CV} \rho v \, dV + \oiint_{CS} v \rho (\vec{V} \cdot \hat{n}) \, dA = F_{y,body} + F_{y,press} + F_{y,shear} + F_{y,ext}$$

If the flow properties are uniform over the area
The equations can be expressed in simplified form as....



Continuity equation:

$$\frac{\partial m_{cv}}{\partial t} + \dot{m}_{out} - \dot{m}_{in} = 0$$

x-momentum equation:

$$\frac{\partial (mu)_{cv}}{\partial t} + (\dot{m}u)_{out} - (\dot{m}u)_{in} = F_{x, press} + F_{x, shear} + F_{x, ext}$$

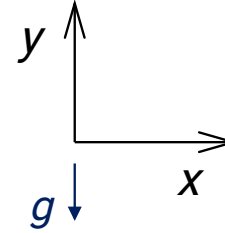
y-momentum equation:

$$\frac{\partial (mv)_{cv}}{\partial t} + (\dot{m}v)_{out} - (\dot{m}v)_{in} = -W + F_{y, press} + F_{y, shear} + F_{y, ext}$$

If the flow properties are uniform over the area and If the flow is Steady
The equations can be expressed in simplified form as....

Continuity equation:

$$\dot{m}_{out} = \dot{m}_{in}$$



x-momentum equation:

$$(\dot{m}u)_{out} - (\dot{m}u)_{in} = F_{x, press} + F_{x, shear} + F_{x, ext}$$

y-momentum equation:

$$(\dot{m}v)_{out} - (\dot{m}v)_{in} = -W + F_{y, press} + F_{y, shear} + F_{y, ext}$$