

OSCILLATING OXIDATION OF FORMIC ACID

Part 1: The Model & Solution Strategy

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Following is how the process looks:

1. Formic acid moves towards the Platinum electrode
2. At the electrode, formic acid decomposes to CO and H₂O
3. CO starts blocking the electrode
4. After a critical number of sites are blocked, the electrode starts oxidising all the CO
5. CO is oxidised to CO₂
6. The electrode is free and the cycle repeats.

This is how the reactions look like:

1. $\text{HCOOH} \leftrightarrow \text{CO (adsorbed)} + \text{H}_2\text{O}$
2. $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2 + 2\text{e}^-$ (only after reaching a critical concentration)

Variables:

Symbol	Meaning	Units
C	Concentration of Formic Acid	mol/m ³
D	Diffusivity of Formic Acid	m ² /s
ρ	Surface Density of total active sites	mol/m ²
θ	Fraction of Active sites blocked by CO	-
k_1	First order surface reaction rate constant	m/s
j	Current Flux	A/m ²
F	Faraday's Constant	C/mol
j_0	Exchange Current Density	A/m ²
Y	Hysteresis Function	-
α	Charge Transfer Coefficient	-
η	Overpotential	V
k_2	Zeroth-order rate constant for CO oxidation	mol/m ² /s
S	Sigmoidal function	-
H	Heaveside function	-
C*	Bulk concentration of Formic Acid	mol/m ³

Let's model the system

1. Bulk Diffusion of Formic Acid

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial x^2} \quad (0 < x < \delta) \quad (1)$$

2. Surface Coverage of CO

$$\rho \frac{d\theta}{dt} = k_1 * C(0, t) * (1 - \theta) - \frac{j}{nF} \quad (2)$$

3. Butler Volmer Kineitcs with hysteresis

$$j = j_0 * Y * \left[\exp\left(\frac{\alpha n F}{RT} \eta\right) - \exp\left(\frac{(\alpha - 1)n F}{RT} \eta\right) \right] \quad (3)$$

$$j_0 = n F k_2 \theta \quad (4)$$

$$Y = S(\theta - \theta_{on}) * H\left(\frac{d\theta}{dt}\right) + S(\theta - \theta_{off}) * H\left(-\frac{d\theta}{dt}\right) \quad (5)$$

4. Boundary Conditions

$$C = C^* \quad (x = \delta) \quad (6)$$

$$D \frac{\partial C}{\partial x} = k_1 * C(0, t) * (1 - \theta) \quad (x = 0) \quad (7)$$

5. Initial Conditions

$$C = C^* \quad (8)$$

$$\theta = 0 \quad (9)$$

Key Assumptions:

1. Negligible side reactions
2. All parameters like k_1 , D etc are constant during the experiments
3. δ is constant due to constant mixing

Checks performed:

1. Sanity Check: All equations are physically reasonable
2. Dimension Check: All terms are dimensionally homogeneous
3. Sign Check: All the signs are checked multiple times to make sure they are correct

Key Attributes:

1. Deposition and oxidation of CO are surface phenomena, hence k_1 has the unit m/s while k_2 has the unit mol/m²/s.
2. The physical phenomena of starting the oxidation when a critical coverage is reached and stopping it when the entire eletrode is cleaned is perfectly modelled by the mentioned hysteresis function. As far as the author is aware, there is **no literature** that uses this model for the formic acid oxidation process.
3. Note that the j and η are considered positive when oxidising

Solution Steps

After modelling the system, let's attempt to solve it.

For this purpose, the solution is divided into 5 parts:

1. $\frac{\partial C}{\partial t} = 0$; Constant potential : This case will create a foundation for the system
2. $\frac{\partial C}{\partial t} \neq 0$; Constant potential: This is the base case on which analysis will be established
3. $\frac{\partial C}{\partial t} \neq 0$; Step change in potential: This is the first layer of complication
4. $\frac{\partial C}{\partial t} \neq 0$; Cyclic Voltametry: This is where effect of frequency of potential change is found
5. $\frac{\partial C}{\partial t} \neq 0$; Sinusoidal Voltage: This is the final stage where we try to find resonance

Each of these cases is solved in a different code and their explanations and code can be found in this directory.