

ANÁLISIS DE LA ECUACIÓN ASOCIADA A LOS CONTROLADORES PID



Ing. Carlos Alberto Cardona Coy
carlos.cardona@usantoto.edu.co

	SISTEMAS DE CONTROL PARA INGENIERÍA; Nise, N.	SISTEMA DE CONTROL AUTOMÁTICO; Kuo, B.
PI	$G_c(s) = K_1 + \frac{K_2}{s} = \frac{K_1 \left(s + \frac{K_2}{K_1} \right)}{s}$	$G_c(s) = K_P + \frac{K_I}{s}$
PD	$G_c(s) = K_2 s + K_1 = K_2 \left(s + \frac{K_1}{K_2} \right)$	$G_c(s) = K_D s + K_P$
PID	$G_c(s) = K_1 + \frac{K_2}{s} + K_3 s = \frac{K_1 s + K_2 + K_3 s^2}{s}$ $= \frac{K_3 \left(s^2 + \frac{K_1}{K_3} s + \frac{K_2}{K_3} \right)}{s}$	$G_c(s) = K_P + \frac{K_I}{s} + K_D s$



	SISTEMAS DE CONTROL PARA INGENIERÍA; Nise, N.	INGENIERÍA DE CONTROL ; Bolton, W.
PI	$G_c(s) = K_1 + \frac{K_2}{s} = \frac{K_1 \left(s + \frac{K_2}{K_1} \right)}{s}$	$G_c(s) = \frac{K_P \left(s + \frac{K_I}{K_P} \right)}{s} = \frac{K_P \left(s + \frac{1}{\tau_i} \right)}{s}; \tau_i = \frac{K_P}{K_I}$
PD	$G_c(s) = K_2 s + K_1 = K_2 \left(s + \frac{K_1}{K_2} \right)$	$G_c(s) = K_D s + K_P = K_D \left(s + \frac{1}{\tau_d} \right); \tau_d = \frac{K_D}{K_P}$
PID	$\begin{aligned} G_c(s) &= K_1 + \frac{K_2}{s} + K_3 s \\ &= \frac{K_1 s + K_2 + K_3 s^2}{s} \\ &= \frac{K_3 \left(s^2 + \frac{K_1}{K_3} s + \frac{K_2}{K_3} \right)}{s} \end{aligned}$	$\begin{aligned} G_c(s) &= K_P \left(1 + \frac{K_I}{K_P s} + \frac{K_D s}{K_P} \right) \\ &= K_P \left(1 + \frac{1}{\tau_i s} + \tau_d s \right); \tau_i = \frac{K_P}{K_I}; \tau_d = \frac{K_D}{K_P} \end{aligned}$



	EQUIVALENTES ENTRE LA ECUACIONES PROPUESTAS POR N. NISE VS W. BOLTON
PI	$K_1 = K_P; K_2 = K_I; \tau_i = \frac{K_P}{K_I}$
PD	$K_1 = K_P; K_2 = K_D; \tau_d = \frac{K_D}{K_P}$
PID	$K_1 = K_P; K_2 = K_I; K_3 = K_D \left \tau_i = \frac{K_1}{K_2}; \tau_d = \frac{K_3}{K_1} \right \tau_i = \frac{K_P}{K_I}; \tau_d = \frac{K_D}{K_P}$



BIBLIOGRAFÍA

