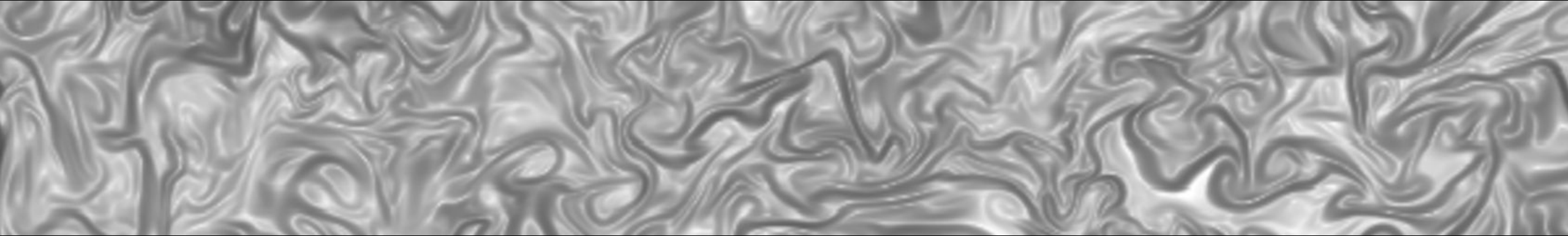


# Incompressible NS solver with staggered grid

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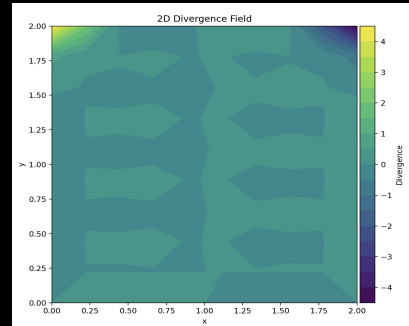
**Update: 29th October 24'**



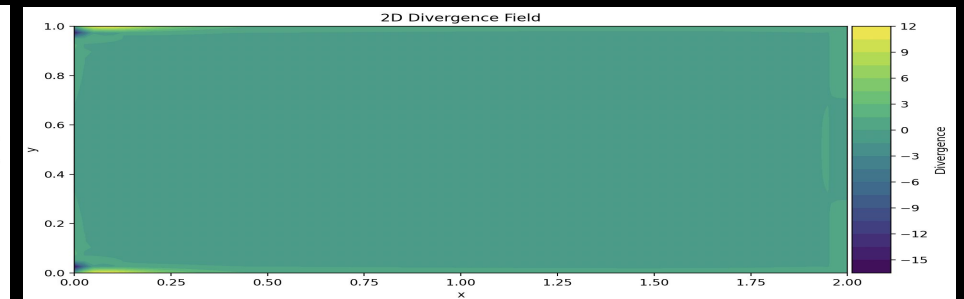
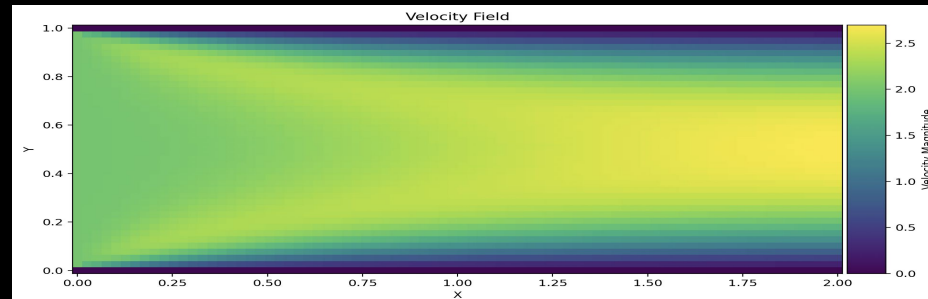
# Issues with the collocated solver

I can't get rid of divergence...

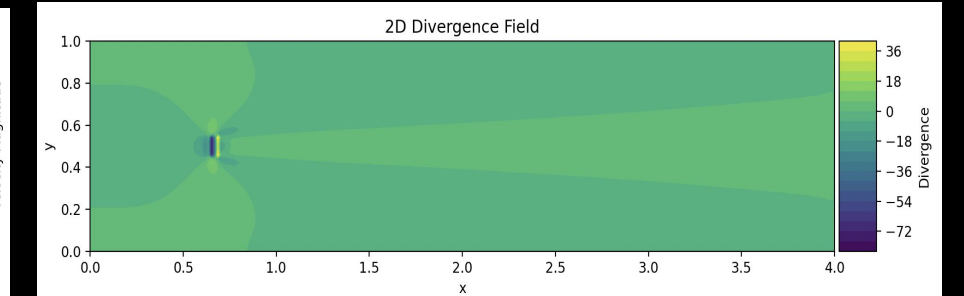
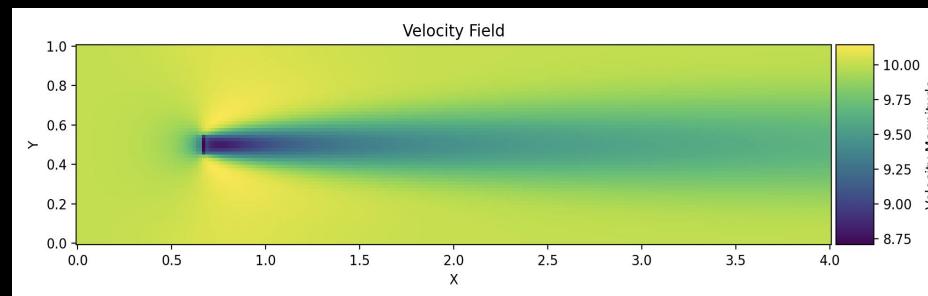
Lid cavity



Channel flow



Wind turbine



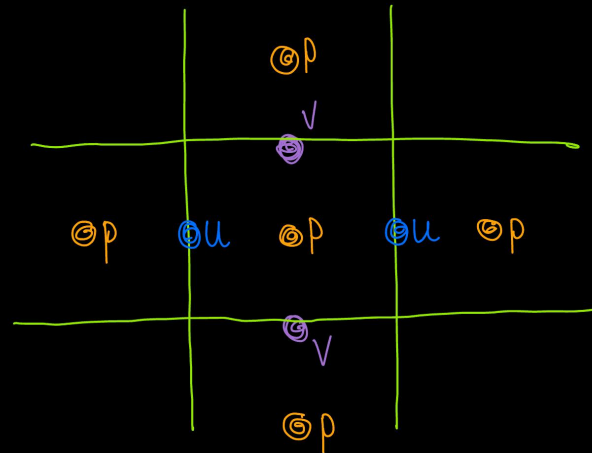
# Staggered grid: a potential solution.

**Pressure Gradient.** The pressure gradient can be directly calculated between adjacent pressure points (which are at the cell centers). This avoids interpolation errors that occur in a collocated grid when computing the pressure gradient at the cell faces.

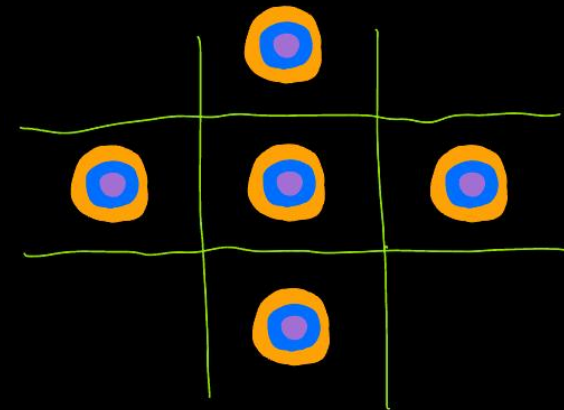
**Divergence.** The discretized divergence can be directly computed as the difference of face-centered velocities without the need for interpolation. This gives a more accurate representation of the fluxes in and out of the cell.

**Pressure Poisson equation.** Velocities are naturally aligned with the pressure cells in a way that ensures a better coupling between pressure and velocity during the solution of the pressure-Poisson equation.

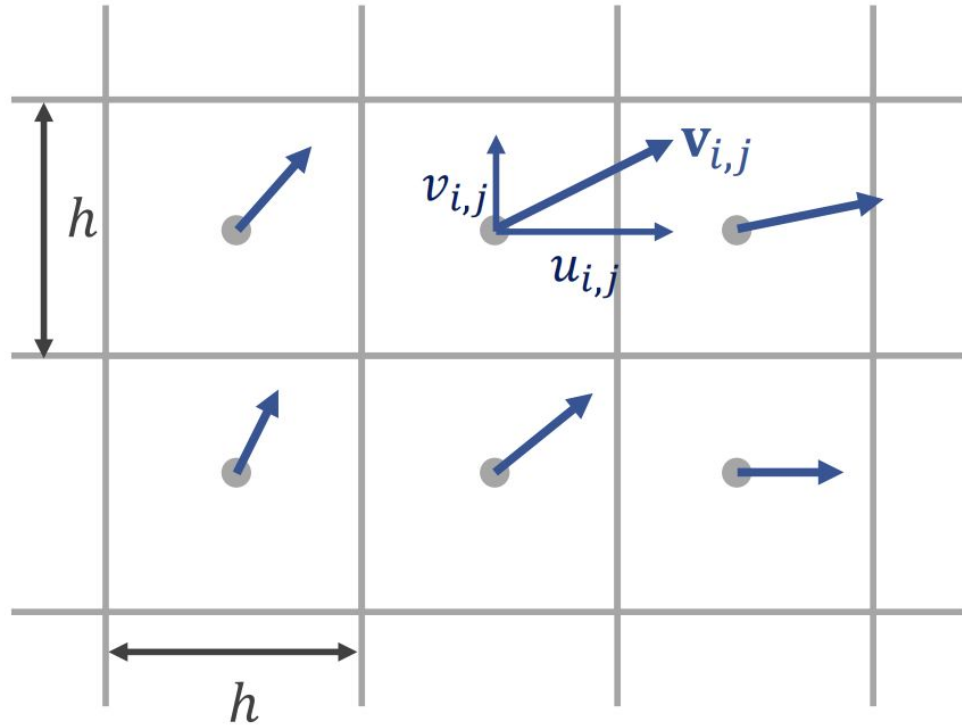
Staggered



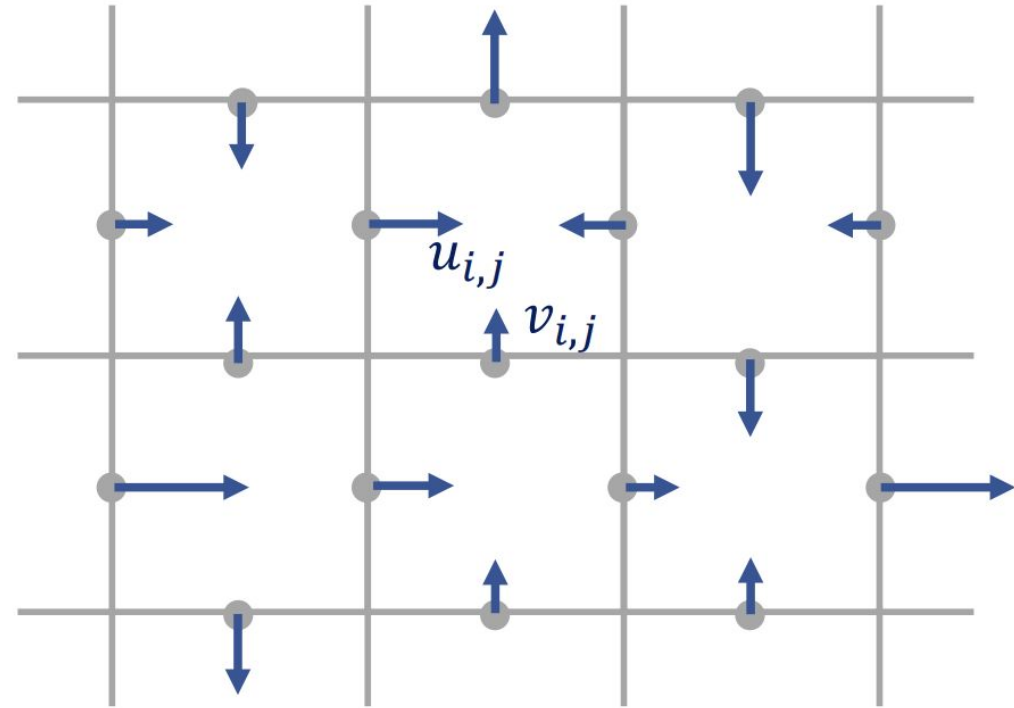
Collocated



# Types of grids



collocated grid

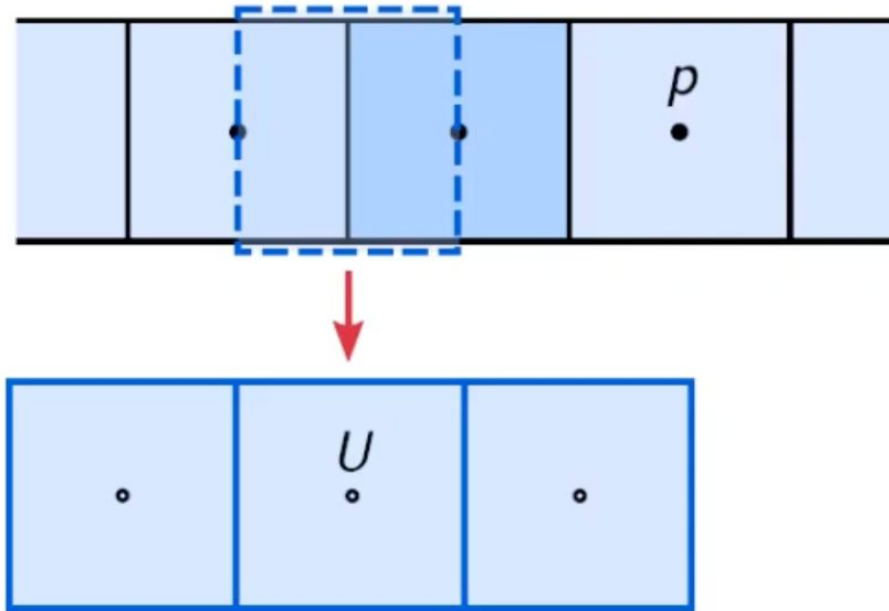


staggered grid

The previous solver used a collocated grid. Let's explore the staggered grid, it might solve the problem.

# Staggered grids

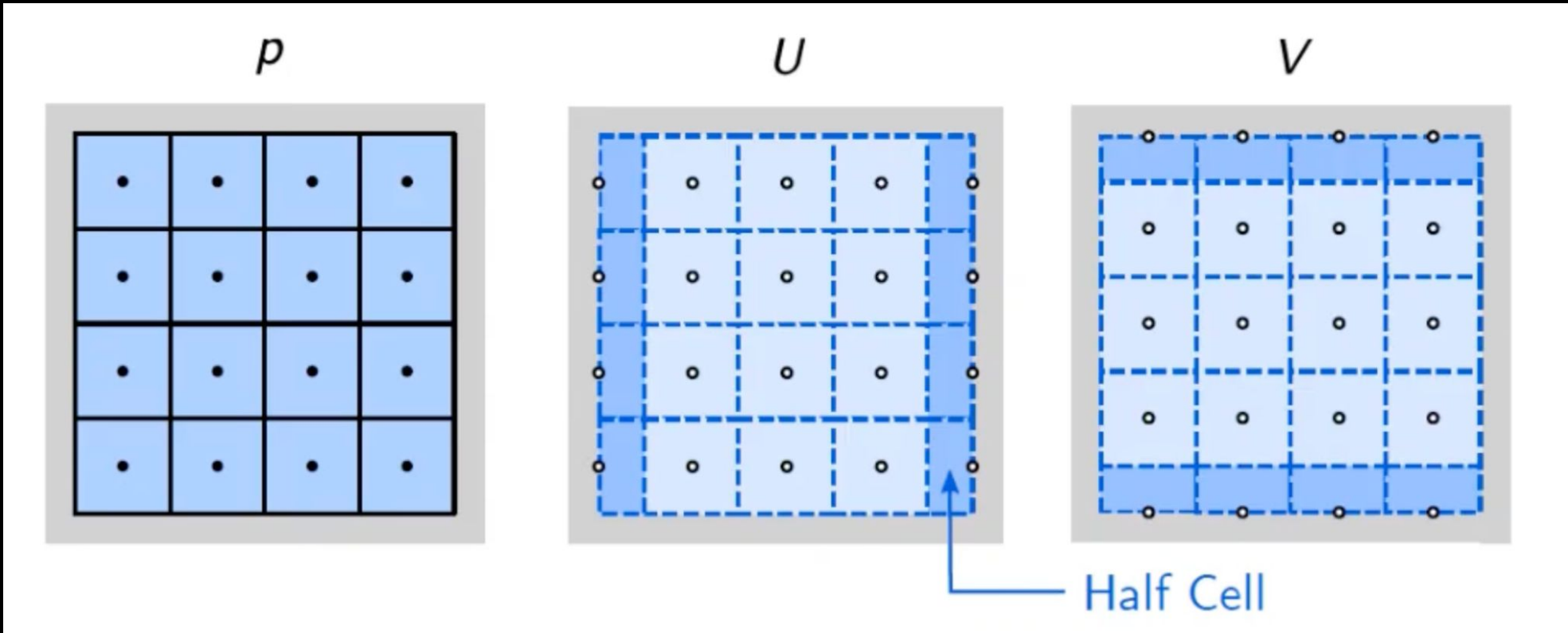
- ▶ In a staggered grid, all flow variables are stored at the centroid, except for **velocity**.
- ▶ Velocity is calculated and stored on the **cell faces**.



Original Grid

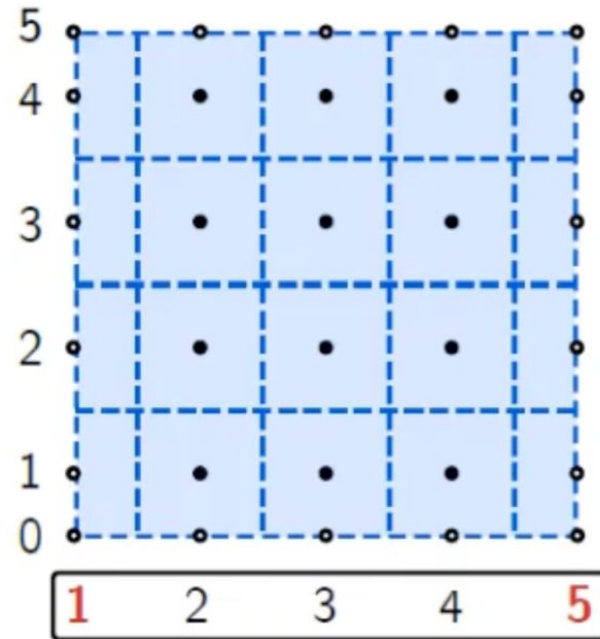
Velocity Grid

## 2D staggered grid

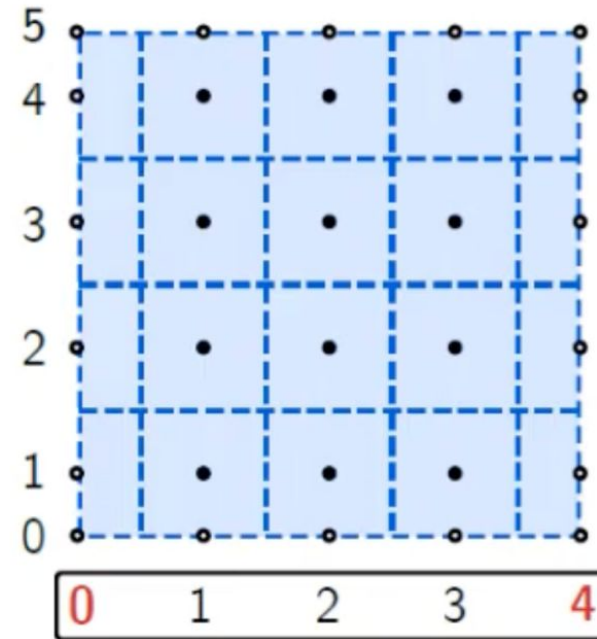


In 3D, we got 3 grids (all variables,  $u$  and  $v$ ).

On a **staggered grid**, we have to choose between *forward* staggering and *backwards* staggering because of the half cells



(a) Forwards



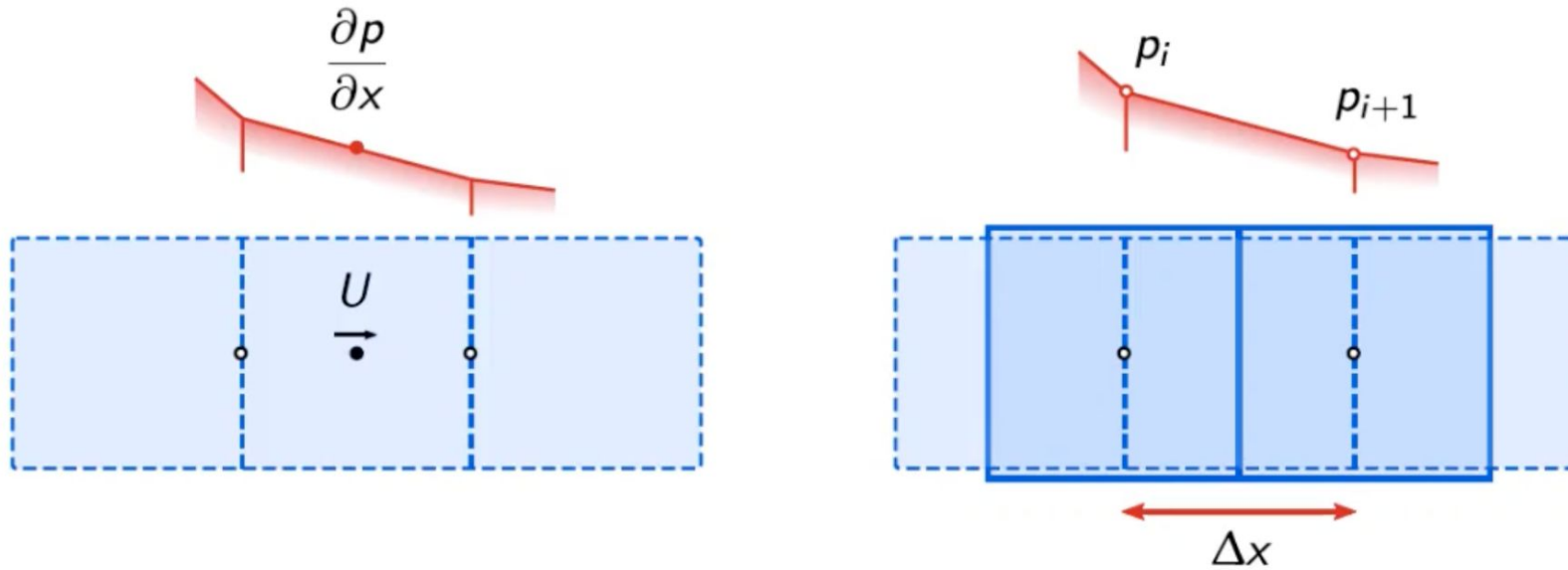
(b) Backwards

We need extra  $u$ 's on the top and bottom boundaries and extra  $v$ 's on left and right. Here, they directly set the boundaries instead of using ghost points. Is it practically the same?

# Pressure grid

## Pressure Gradient

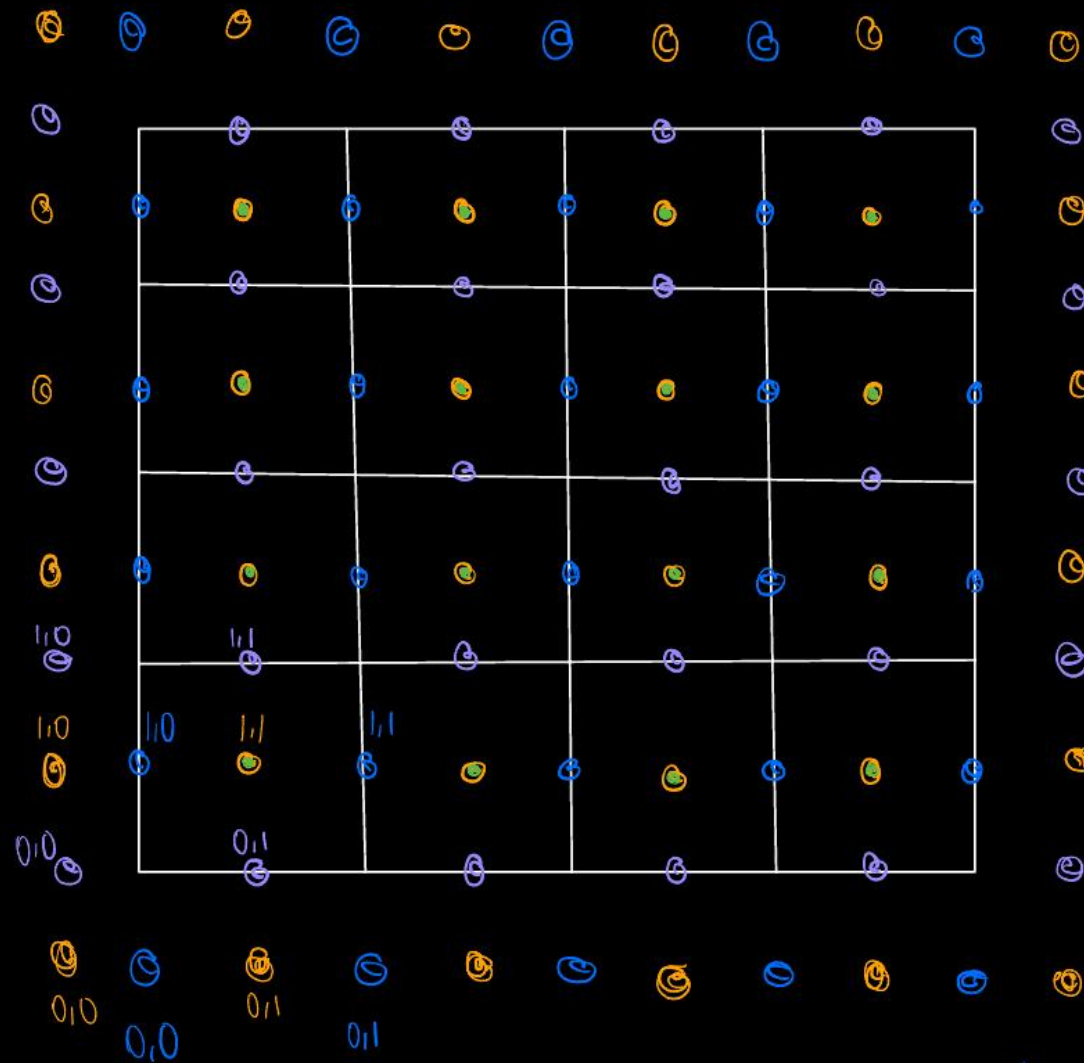
- The pressure gradient across the  $U$  cell is calculated from the pressure at the centroids on the *original* grid.



$$\frac{\partial p}{\partial x} = \frac{p_{i+1} - p_i}{\Delta x}$$



# My staggered grid



U-velocity ( $N+2, N+1$ )

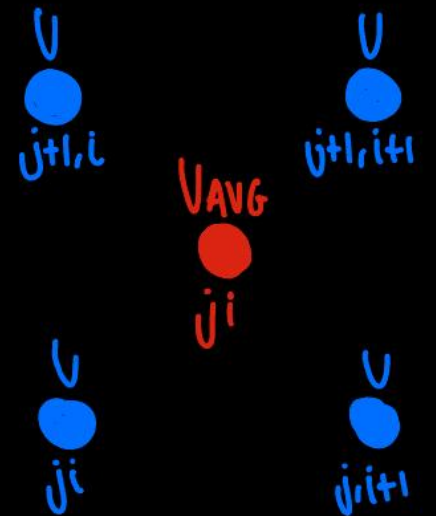
V-velocity ( $N+1, N+2$ )

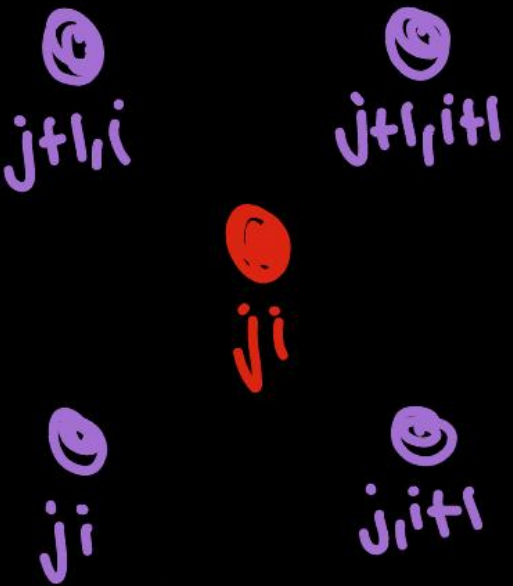
p ( $N+2, N+2$ )

b-term ( $N, N$ )

# Interpolated velocities

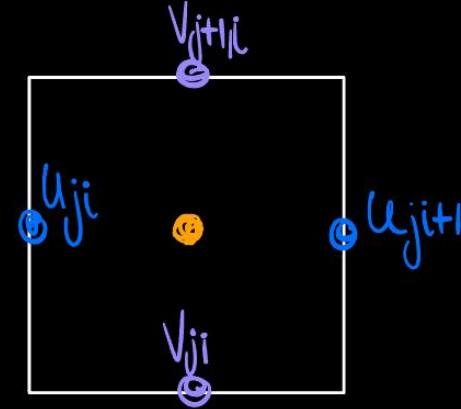
- To compute  $du/dy$  and  $dv/dx$ , we'll need to know the u-velocities at the v-positions and vice versa.
- Average velocities  $u\_avg$  and  $v\_avg$  are calculated using linear interpolation, assuming square cells.
- **Warning!!!!** This method is exclusively designed for square-cell grids!


$$u_{avg}^i = \frac{u_{j,i} + u_{j+1,i} + u_{j+1,i+1} + u_{j,i+1}}{4}$$


$$v_{avg}^i = \frac{v_{j,i} + v_{j+1,i} + v_{j+1,i+1} + v_{j,i+1}}{4}$$

# Divergence

$$\text{Div}_{ji} = \frac{u_{j,i+1} - u_{j,i}}{dx} + \frac{v_{j+1,i} - v_{j,i}}{dy}$$



- Since it is a gradient, the divergence is associated to the center point.
- Units are [1/s].

# Poisson solver: b-term, poisson, algorithm.

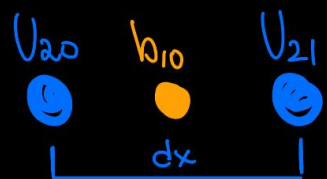
$$\frac{p_{i+1,j}^n - 2p_{i,j}^n + p_{i-1,j}^n}{\Delta x^2} + \frac{p_{i,j+1}^n - 2p_{i,j}^n + p_{i,j-1}^n}{\Delta y^2} = \rho \left[ \frac{1}{\Delta t} \left( \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} + \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y} \right) - \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} - 2 \frac{u_{i,j+1} - u_{i,j-1}}{2\Delta y} \frac{v_{i+1,j} - v_{i-1,j}}{2\Delta x} - \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y} \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y} \right]$$

Rearrange

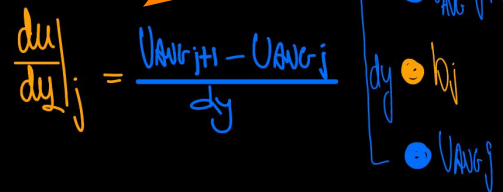
Spans 2 cells cuz it comes from 2nd order central difference

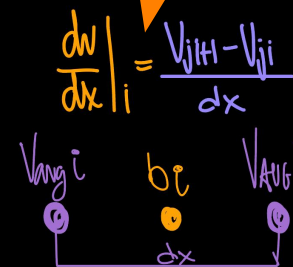
$$p_{i,j}^n = \frac{(p_{i+1,j}^n + p_{i-1,j}^n) \Delta y^2 + (p_{i,j+1}^n + p_{i,j-1}^n) \Delta x^2}{2(\Delta x^2 + \Delta y^2)} - \frac{\rho \Delta x^2 \Delta y^2}{2(\Delta x^2 + \Delta y^2)} \times \left[ \frac{1}{\Delta t} \left( \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} + \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y} \right) - \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} \frac{u_{i+1,j} - u_{i-1,j}}{2\Delta x} - 2 \frac{u_{i,j+1} - u_{i,j-1}}{2\Delta y} \frac{v_{i+1,j} - v_{i-1,j}}{2\Delta x} - \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y} \frac{v_{i,j+1} - v_{i,j-1}}{2\Delta y} \right]$$

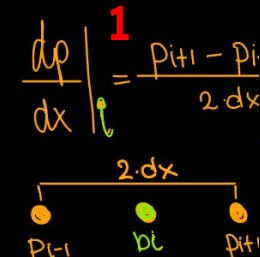
**B-term**

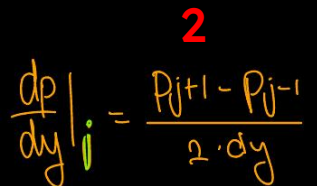
$$\left. \frac{du}{dx} \right|_i = \frac{u_{i+1} - u_i}{dx}$$


$$\left. \frac{dv}{dy} \right|_{j,i} = \frac{v_{i,j+1} - v_{i,j}}{dy}$$


$$\left. \frac{du}{dy} \right|_j = \frac{u_{i+1,j+1} - u_{i,j+1}}{dy}$$


$$\left. \frac{dv}{dx} \right|_i = \frac{v_{i+1,j} - v_{i,j}}{dx}$$


$$\left. \frac{dp}{dx} \right|_i = \frac{p_{i+1} - p_i}{2 \cdot dx}$$


$$\left. \frac{dp}{dy} \right|_i = \frac{p_{i,j+1} - p_{i,j-1}}{2 \cdot dy}$$


$$\left. \frac{dp}{dy} \right|_i = \frac{p_{i,j+1} - p_{i,j-1}}{2 \cdot dy}$$


# Poisson solver: b-term, poisson, algorithm.

$$\frac{p_{j,i+1}^n - 2p_{ji}^n + p_{j,i-1}^n}{\Delta x^2} + \frac{p_{j+1,i}^n - 2p_{ji}^n + p_{j-1,i}^n}{\Delta y^2} = \rho \left[ \frac{1}{\Delta t} \left( \frac{u_{j,i+1} - u_{ji}}{\Delta x} + \frac{v_{j+1,i} - v_{ji}}{\Delta y} \right) - \left( \frac{u_{j,i+1} - u_{ji}}{2\Delta x} \right)^2 - 2 \frac{u_{avg,j+1,i} - u_{avg,ji}}{\Delta y} \cdot \frac{v_{avg,j,i+1} - v_{avg,ji}}{\Delta x} - \left( \frac{v_{j+1,i} - v_{ji}}{\Delta y} \right)^2 \right]$$

explicit

$$p_{ji}^n = \frac{(p_{j,i+1}^n + p_{j,i-1}^n) \cdot \Delta y^2 + (p_{j+1,i}^n + p_{j-1,i}^n) \cdot \Delta x^2}{2(\Delta x^2 + \Delta y^2)} - \frac{\rho \Delta x^2 \Delta y^2}{2(\Delta x^2 + \Delta y^2)} \cdot \left[ \frac{1}{\Delta t} \left( \frac{u_{j,i+1} - u_{ji}}{\Delta x} + \frac{v_{j+1,i} - v_{ji}}{\Delta y} \right) - \left( \frac{u_{j,i+1} - u_{ji}}{\Delta x} \right)^2 - 2 \frac{u_{avg,j+1,i} - u_{avg,ji}}{\Delta y} \cdot \frac{v_{avg,j,i+1} - v_{avg,ji}}{\Delta x} - \left( \frac{v_{j+1,i} - v_{ji}}{\Delta y} \right)^2 \right]$$

$$\left. \frac{du}{dx} \right|_i = \frac{u_{i+1} - u_i}{\Delta x}$$

Diagram: A horizontal line segment of length  $\Delta x$  with a blue circle at the left end labeled  $u_{ao}$  and a blue circle at the right end labeled  $u_{21}$ . A yellow circle is in the middle labeled  $b_{10}$ .

$$\left. \frac{dv}{dy} \right|_{ji} = \frac{v_{j+1,i} - v_{ji}}{\Delta y}$$

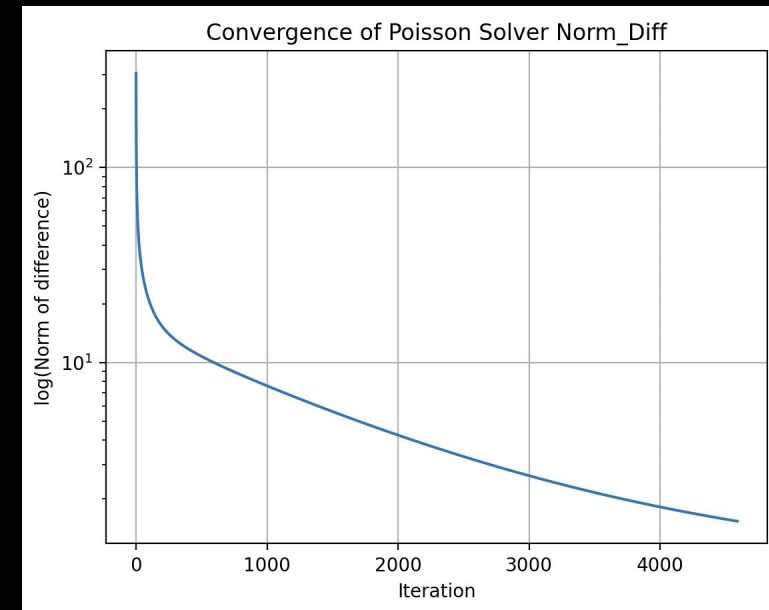
Diagram: A vertical line segment of length  $\Delta y$  with a purple circle at the top labeled  $v_{j+1}$  and a purple circle at the bottom labeled  $v_j$ . A yellow circle is in the middle labeled  $b_j$ .

$$\left. \frac{du}{dx} \right|_i = \frac{u_{avg,j+1,i} - u_{avg,ji}}{\Delta x}$$

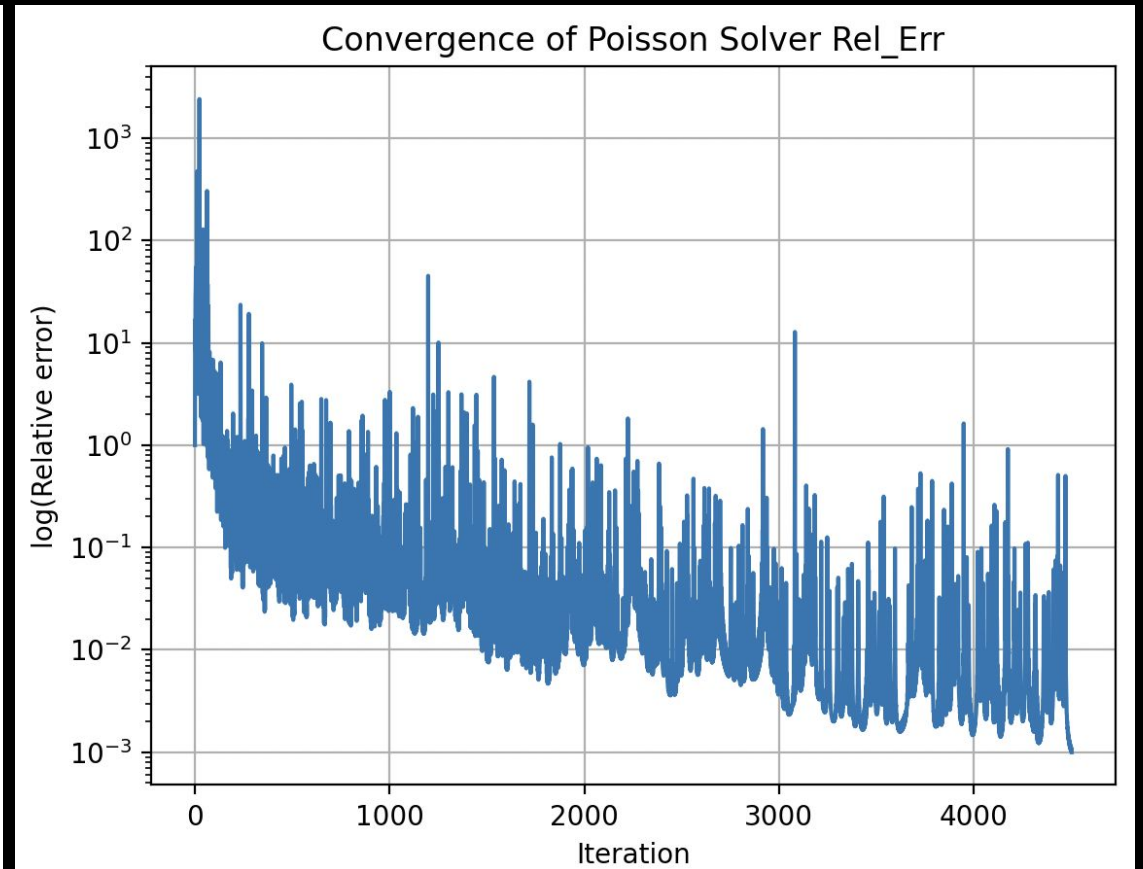
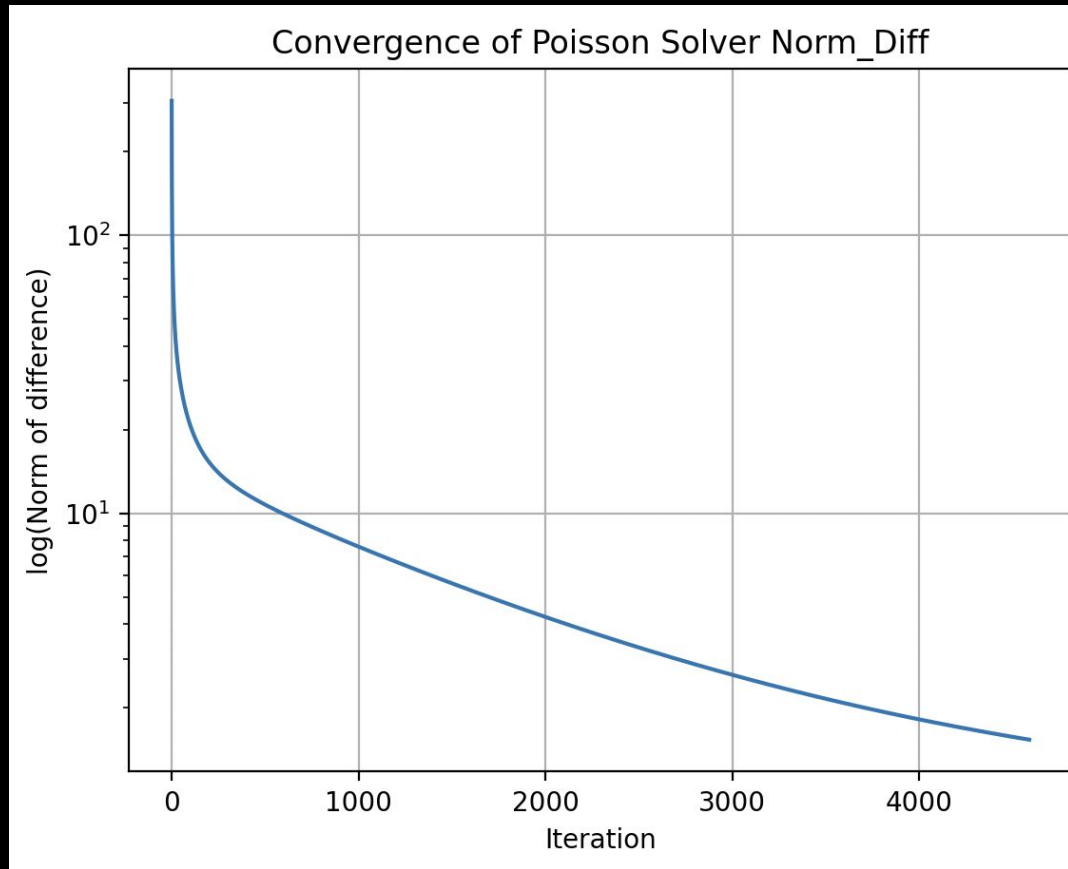
Diagram: A horizontal line segment of length  $\Delta x$  with a purple circle at the left end labeled  $u_{avg,i}$  and a purple circle at the right end labeled  $u_{avg,i+1}$ . A yellow circle is in the middle labeled  $b_i$ .

$$\left. \frac{dv}{dy} \right|_j = \frac{v_{avg,j+1,i} - v_{avg,ji}}{\Delta y}$$

Diagram: A vertical line segment of length  $\Delta y$  with a blue circle at the top labeled  $u_{avg,j+1}$  and a blue circle at the bottom labeled  $u_{avg,j}$ . A yellow circle is in the middle labeled  $b_j$ .



# Poisson solver: Convergence test



\*Iterative resolution of the poisson equation using a randomly initialized velocities on a 80x80 grid.

\*The norm of difference and relative error are computed in between two consecutive pressure arrays.

Why does the relative error have so much noise but the norm of difference doesn't? Because rel\_err is relative (way more variability) and norm\_diff is absolute.

# Staggered Discretization of Advection-Diffusion: U-velocity

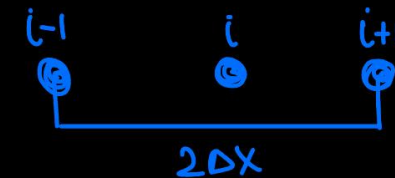
$$\frac{U_{ji}^{n+1} - U_{ji}^n}{\Delta t} + U_{ji}^n \cdot \frac{\tilde{U}_{j,i+1} - \tilde{U}_{j,i-1}}{2 \cdot \Delta x} + V_{avg,ji} \cdot \frac{\tilde{U}_{j+1,i} - \tilde{U}_{j-1,i}}{2 \Delta y} - \frac{1}{\rho} \cdot \frac{P_{j,i+1} - P_{ji}}{\Delta x} + \nu \left( \frac{\tilde{U}_{j,i+1} - 2\tilde{U}_{ji} + \tilde{U}_{j,i-1}}{2 \cdot \Delta x} + \frac{\tilde{U}_{j+1,i} - 2\tilde{U}_{ji} + \tilde{U}_{j-1,i}}{2 \cdot \Delta y} \right)$$

explicit

$$U_{ji}^{n+1} = U_{ji}^n - U_{ji}^n \cdot \Delta t \cdot \frac{\tilde{U}_{j,i+1} - \tilde{U}_{j,i-1}}{2 \Delta x} - V_{avg,ji} \cdot \Delta t \cdot \frac{\tilde{U}_{j+1,i} - \tilde{U}_{j-1,i}}{2 \Delta y} - \frac{\Delta t}{\rho} \cdot \frac{P_{j,i+1} - P_{ji}}{\Delta x} + \nu \cdot \Delta t \left( \frac{\tilde{U}_{j,i+1} - 2\tilde{U}_{ji} + \tilde{U}_{j,i-1}}{\Delta x^2} + \frac{\tilde{U}_{j+1,i} - 2\tilde{U}_{ji} + \tilde{U}_{j-1,i}}{\Delta y^2} \right)$$

$$\left[ \begin{array}{c} \textcircled{U}_{j+1} \\ \textcircled{U}_j \\ \textcircled{U}_{j-1} \end{array} \right]_{2\Delta y} \quad \begin{array}{l} 2 \frac{du}{dy}|_j = \frac{U_{j+1} - U_{j-1}}{2\Delta y} \\ 5 \frac{d^2u}{dy^2}|_j = \frac{U_{j+1} - 2U_j + U_{j-1}}{\Delta y^2} \end{array}$$

$$3 \frac{dp}{dx}|_i = \frac{P_{i+1} - P_i}{\Delta x}$$



$$1 \frac{du}{dx}|_i = \frac{U_{i+1} - U_{i-1}}{2\Delta x}$$

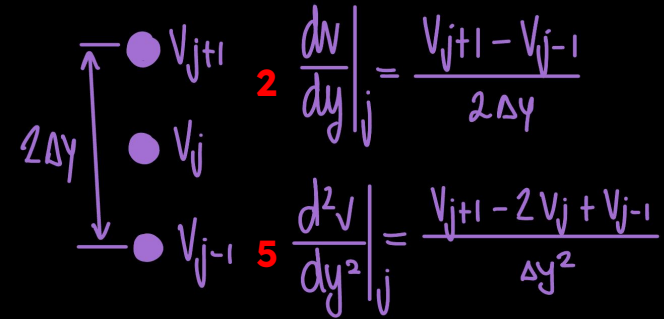
$$4 \frac{d^2u}{dx^2}|_i = \frac{U_{i+1} - 2U_i + U_{i-1}}{\Delta x^2}$$



# Staggered Discretization of Advection Diffusion: V-velocity

$$\frac{V_{ji}^{n+1} - V_{ji}^n}{\Delta t} + u_{\text{ANG},ji}^n \cdot \frac{V_{j,i+1}^n - V_{j,i-1}^n}{2 \cdot \Delta x} + V_{ji}^n \cdot \frac{V_{j+1,i}^h - V_{j-1,i}^h}{2 \cdot \Delta y} =$$

$$- \frac{1}{\rho} \frac{p_{j+1,i} - p_{j,i}}{\Delta y} + \nu \left( \frac{V_{j,i+1}^n - 2V_{j,i}^h + V_{j,i-1}^n}{\Delta x^2} + \frac{V_{j+1,i}^h - 2V_{ji}^n + V_{j-1,i}^h}{\Delta y^2} \right)$$



$$\frac{dv}{dy}\bigg|_j = \frac{V_{j+1} - V_{j-1}}{2\Delta y}$$

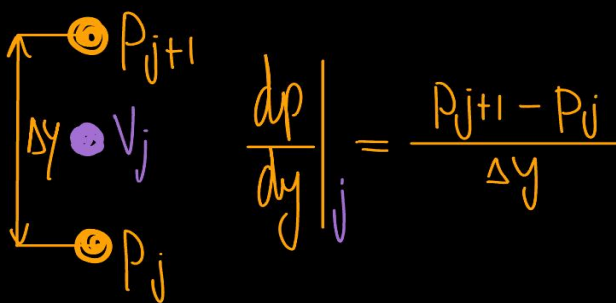
$$\frac{d^2v}{dy^2}\bigg|_j = \frac{V_{j+1} - 2V_j + V_{j-1}}{\Delta y^2}$$

Explicit form

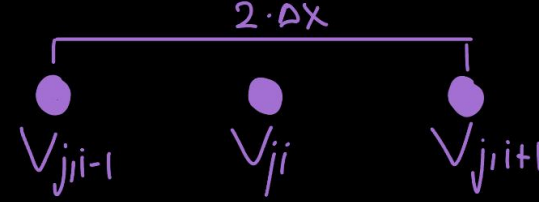
$$V_{ji}^{n+1} = V_{ji}^n - u_{\text{ANG},ji}^n \cdot \frac{\Delta t}{2\Delta x} \cdot (V_{j,i+1}^n \text{ 1} - V_{j,i-1}^n) - V_{ji}^n \cdot \frac{\Delta t}{2\Delta y} (V_{j+1,i}^h \text{ 2} - V_{j-1,i}^h)$$

$$- \frac{\Delta t}{\rho \Delta y} (p_{j+1,i} \text{ 3} - p_{j,i}) + \nu \cdot \Delta t \left( \frac{V_{j,i+1}^n - 2V_{j,i}^h + V_{j,i-1}^n}{\Delta x^2} \text{ 4} + \frac{V_{j+1,i}^h - 2V_{ji}^n + V_{j-1,i}^h}{\Delta y^2} \text{ 5} \right)$$

3



$$\frac{dp}{dy}\bigg|_j = \frac{p_{j+1} - p_j}{\Delta y}$$



$$\frac{dv}{dx}\bigg|_i = \frac{V_{i+1} - V_{i-1}}{2 \cdot \Delta x}$$

$$\frac{d^2v}{dx^2}\bigg|_i = \frac{V_{i+1} - 2V_i + V_{i-1}}{\Delta x^2}$$

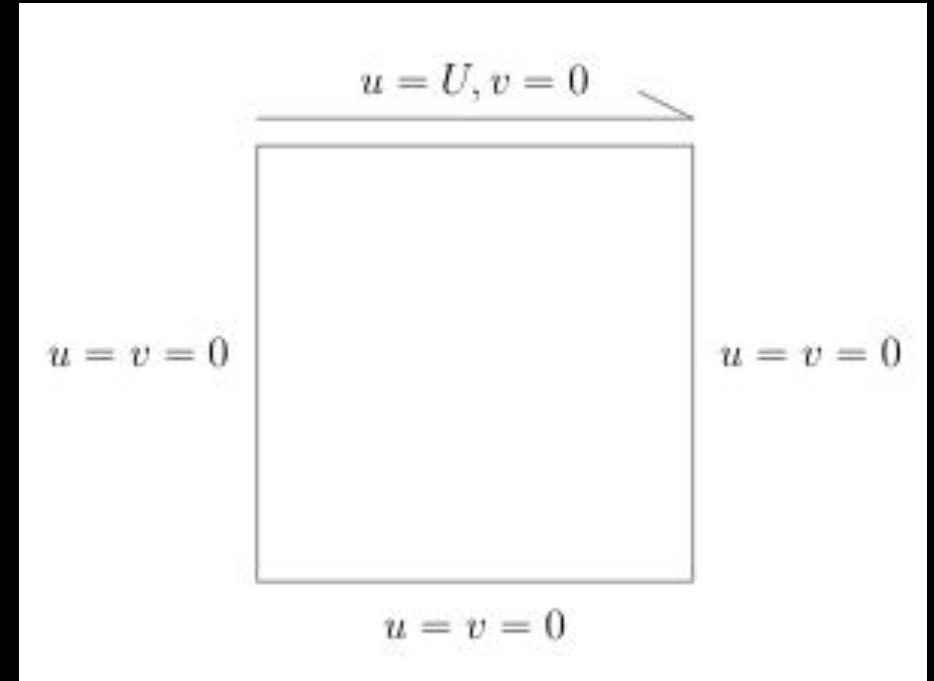


# Cavity with moving Lid Simulation set-up

- Square domain
- 2D
- Uniform cartesian grid made out of square cells

Boundary conditions:

- Velocity -> No Slip condition on all 4 walls:
  - Left, Bottom, Right walls:  $\underline{u} = \langle 0, 0 \rangle$
  - Top wall (moving lid):  $\underline{u} = \langle U_{lid}, 0 \rangle$
- Pressure -> Neumann:
  - Zero gradient at all 4 walls.



# The Algorithm: Predictor Corrector (Fractional Step Method)

We couldn't get rid of divergence, so we'll try this new algorithm, that is the one used by Matthias Muller.

1

Solve Momentum

Neglect pressure gradient term

—

2

Solve Poisson equation

Jacobi solver  
(Gauss-Seidel could be way faster)

Root mean square error (RMS)  
Threshold value.

—

3

Correct velocities

Apply the pressure gradient term.

Ensures a divergence free flow

# Other Updates

- Everytime we modify velocities we update the BCs. Because the way they are defined now, they are affected by the interior points.
- We introduce a conservative dynamic timestep, taking into account advection and diffusivity:

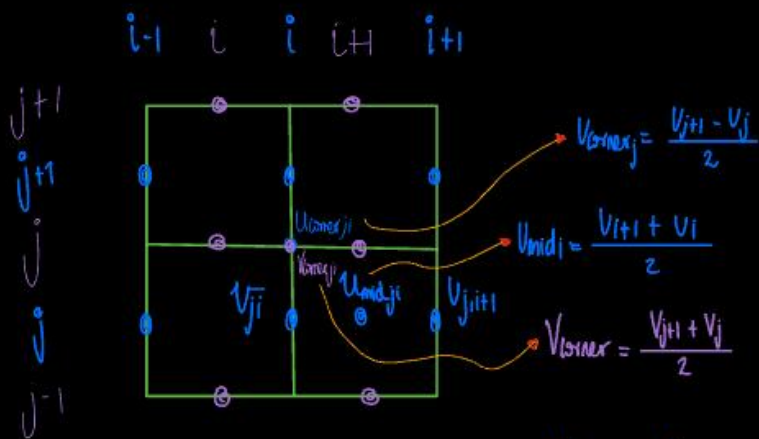
$$\textcircled{C} \quad C_{ADV} \rightarrow \Delta t = \frac{cfl \cdot \Delta x}{u_{max}} \quad (\text{Updated at every step})$$
$$\textcircled{D} \quad C_{DIFF} \rightarrow \Delta t = \frac{C}{2\gamma \left( \frac{1}{\Delta x^2} + \frac{1}{\Delta y^2} \right)} \quad (\text{Constant})$$

→ Ensure stability

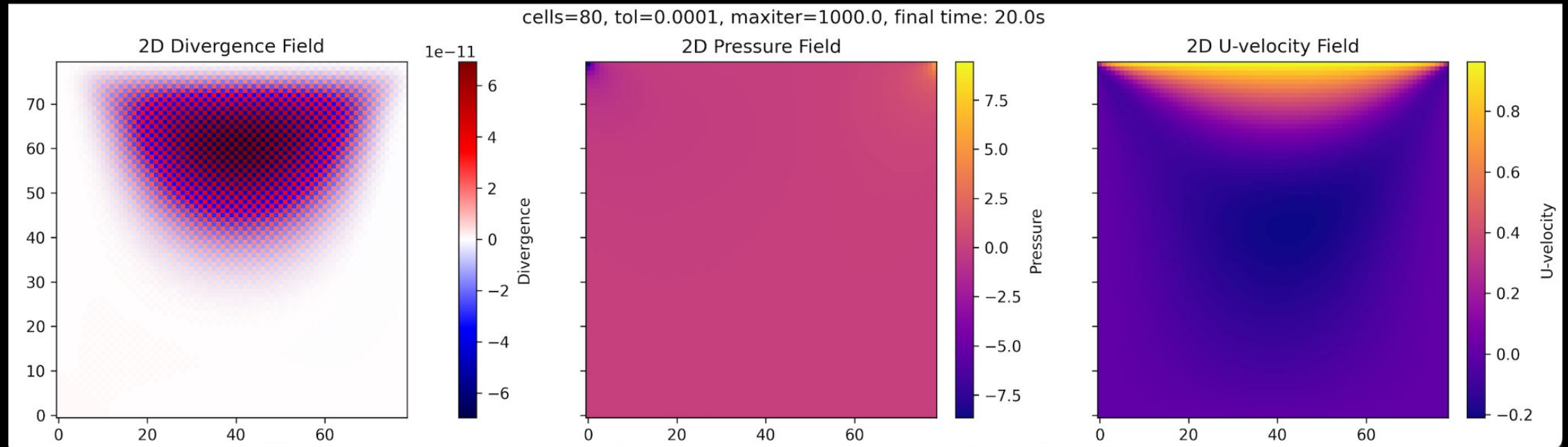
- Discretization on advection points is performed using the interpolated values in the corners (see next slide).

## New advection approach (conservative form)

$$U_{ji}^{n+1} = U_{ji}^n + \Delta t \cdot \left[ \overset{\text{diffusion}}{\nu u \cdot \left( \frac{d^2 u}{dx^2} + \frac{d^2 u}{dy^2} \right)} - \overset{u\text{-advection}}{\frac{d}{dx} u^2} - \overset{v\text{-advection}}{\frac{d}{dy} uv} \right]$$



# Solutions



# How does the divergence evolves for different Poisson tolerance?

Tolerance

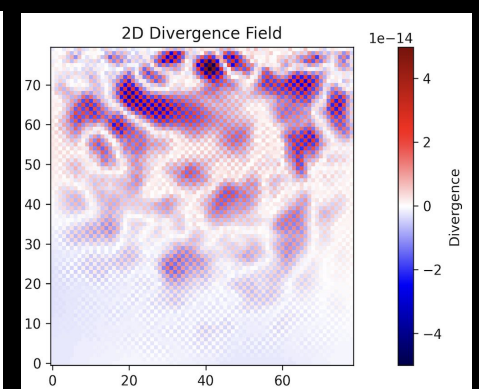
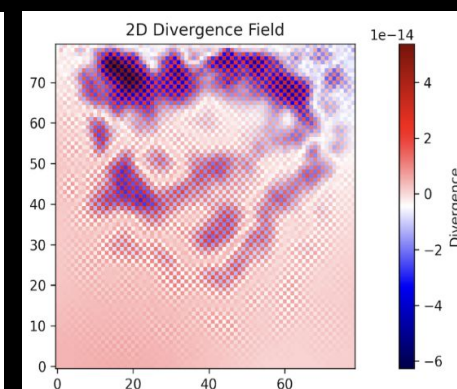
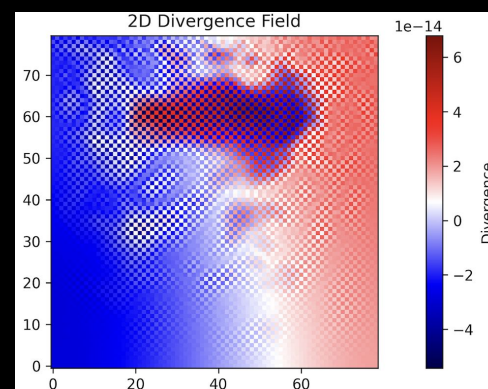
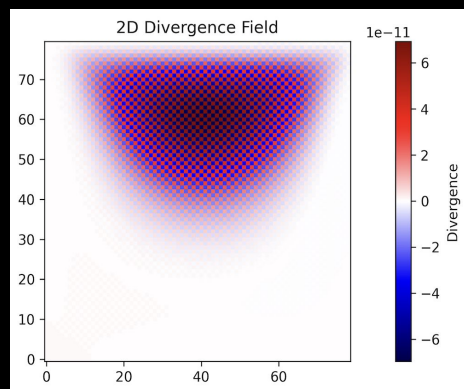
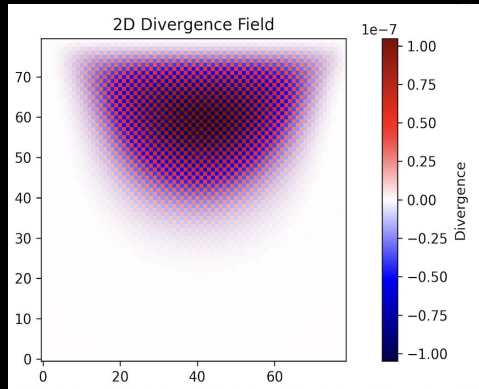
$1e-3$

$1e-4$

$1e-5$

$1e-6$

$1e-7$



Would be interesting to indicate how long it took to run, even though this is a future worry.

# Channel Flow set-up

BC's:

Inlet:

$$u=2, v=0$$

$$dP/dx=0$$

Outlet:

$$du/dx=0, dv/dx=0$$

$$dp/dx=0$$

Top and bottom:

$$u=0, v=0 \text{ (non-slip)}$$

$$dp/dy=0$$

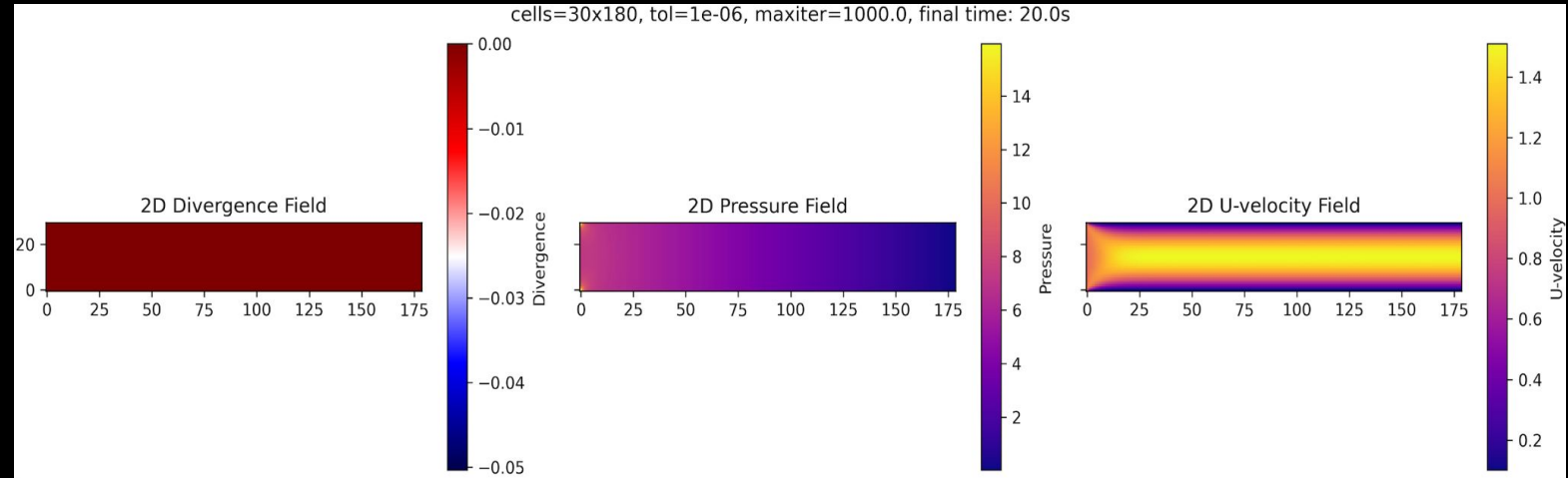
A hand-drawn diagram of a rectangular channel flow domain. The domain is bounded by a top and bottom wall, and a left and right wall. The left wall is marked with a blue vertical line. The right wall is marked with a blue vertical line. The top and bottom walls are marked with a blue horizontal line. The domain is divided into three horizontal sections by two horizontal lines. The top section is labeled with  $\bar{u} = \langle 0, 0 \rangle$  (no-slip) in blue,  $\frac{dp}{dy} = 0$  in green, and  $\frac{du}{dx} = 0$  in blue. The middle section is labeled with  $\bar{u} = \langle v_{in}, 0 \rangle$  in blue,  $\frac{dp}{dx} = 0$  in green, and  $\frac{dv}{dx} = 0$  in blue. The bottom section is labeled with  $\bar{u} = \langle 0, 0 \rangle$  (no slip) in blue,  $\frac{dp}{dy} = 0$  in green, and  $\frac{dv}{dx} = 0$  in blue.

It's running super slow compared with the same domain and resolution with previous BCs.  
Why?

# Channel flow - Solutions

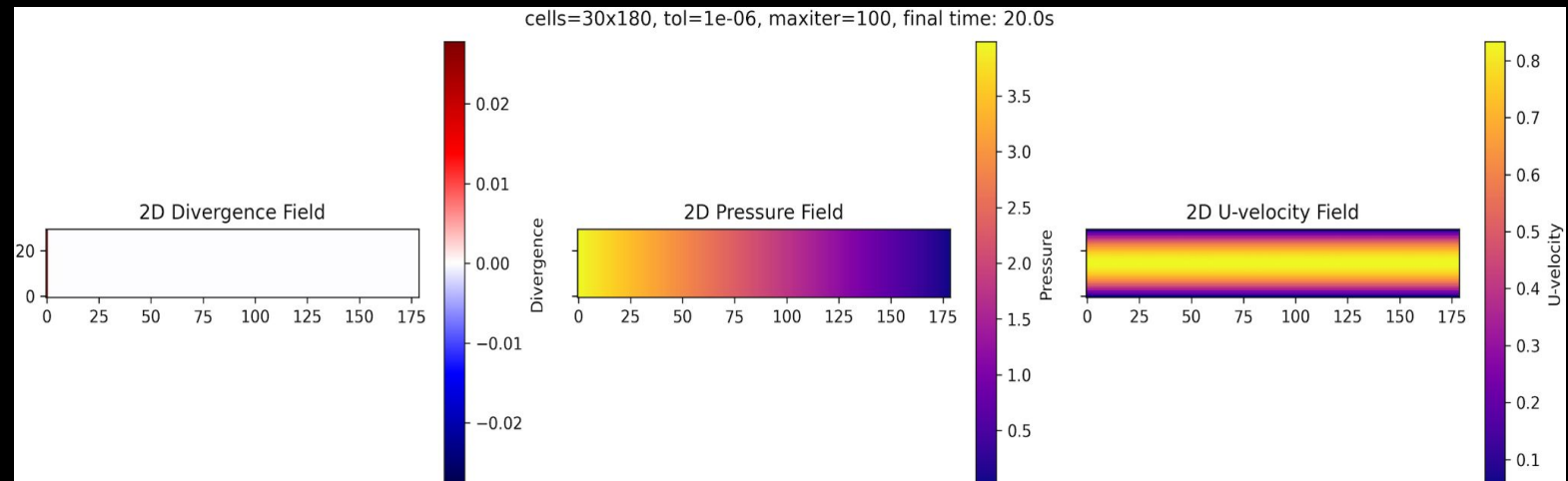
## BC's:

- Velocities.
  - In:  $invel\ u=<1,0>$
  - Out:  $du/dx=dv/dx=0$
  - Top & bottom: Non-slip  $u=<0,0>$
- Pressure.
  - Top & bottom:  $dp/dy=0$
  - Inlet:  $dp/dx=0$
  - Outlet:  $p=0$



## BC's

- Velocities
  - In & Out:  $du/dx=dv/dx=0$
  - Top & bottom: Non-slip  $u=<0,0>$
- Pressure
  - In:  $p=4$
  - Out:  $p=0$
  - Top & bottom:  $dp/dy=0$

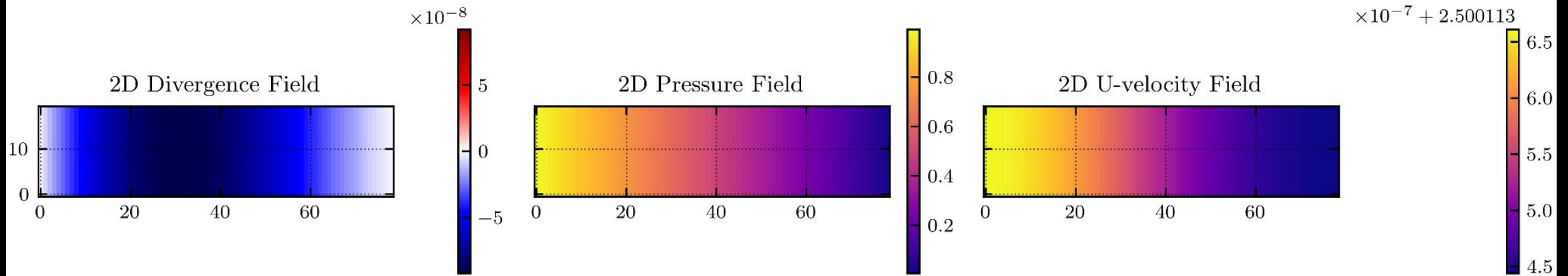


Comments: Both cases are divergence free except of at the inlet (or maybe outlet)  
A way to solve this could be adding u-vel ghost nodes for properly setting  $du/dx$  at  $x=0$ .



# Channel flow with extra nodes - Solutions

Open Flow,  $P_{x0} = 1.0$ ,  $P_{x1} = 0.0$ , BCs are CENTERED zero-gradient.  
tf=10.0, cfl=0.1, tol=1.0e-07, maxiter=1.0e+03



## BC's:

- Velocities.
  - In & Out:  $du/dx=dv/dx=0$
  - Top & bottom:  $du/dy=dv/dy=0$
- Pressure.
  - Top & bottom:  $dp/dy=0$
  - Inlet:  $p=1$
  - Outlet:  $p=0$

## What is new?

- New ghost cells -> Allows defining BCs at the actual boundary.

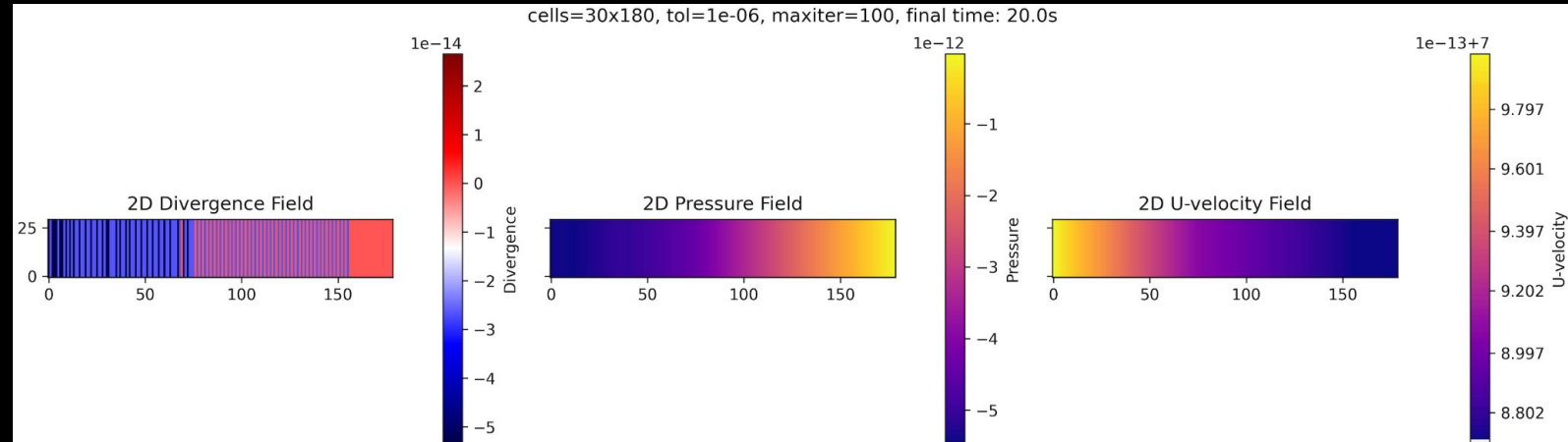
## Comments

This solves the problem of the non-zero divergence at the outlet.

# Open field - Solutions

## BC's:

- Velocities.
  - In:  $invel\ u=<7,0>$
  - Out:  $du/dx=dv/dx=0$
  - Top & bottom:  $du/dy=dv/dy=0$
- Pressure.
  - Top & bottom:  $dp/dy=0$
  - Inlet:  $dp/dx=0$
  - Outlet:  $p=0$



## BC's:

- Velocities.
  - In:  $invel\ u=<7,0>$
  - Out:  $du/dx=dv/dx=0$
  - Top & bottom:  $du/dy=dv/dy=0$
- Pressure.
  - Top & bottom:  $dp/dy=0$
  - Inlet:  $dp/dx=0$
  - Outlet:  $dp/dx=0$

