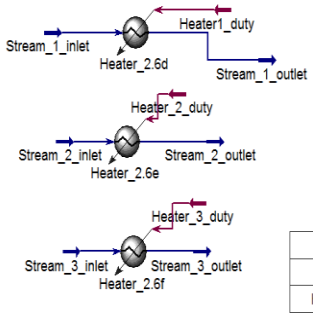

Material Streams							
		Stream_1_inlet	Stream_1_outlet	Stream_2_inlet	Stream_2_outlet	Stream_3_inlet	Stream_3_outlet
Vapour Fraction		0.6000	0.8000	1.0000	0.0000	1.0000	0.0000
Temperature	C	150.0	150.0	250.0	170.4	250.0	250.0
Pressure	kPa	476.0	476.0	800.0	800.0	800.0	3978
Molar Flow	kgmole/h	5.551e-002	5.551e-002	5.551e-002	5.551e-002	5.551e-002	5.551e-002
Mass Flow	kg/h	1.000	1.000	1.000	1.000	1.000	1.000
Liquid Volume Flow	m3/h	1.002e-003	1.002e-003	1.002e-003	1.002e-003	1.002e-003	1.002e-003
Heat Flow	kJ/h	-1.403e+004	-1.360e+004	-1.297e+004	-1.520e+004	-1.297e+004	-1.484e+004

Energy Streams				
		Heater1_duty	Heater_2_duty	Heater_3_duty
Heat Flow	kJ/h	422.8	-2230	-1865

2.6d: 1 kg/h = 1/60 kg/s, 422.8 kJ/h = 7.046 kW; $\text{deltaH}_{\text{specific}}$ = (7.046 kJ/s)/(1/60 kg/s) = 422.8 kJ/kg

deltaH = m*$\text{deltaH}_{\text{specific}}$ = (3 kg)(422.8 kJ/kg) = 1268 kJ

2.6e: 1 kg/h = 1/60 kg/s, -2230 kJ/h = -37.16 kW; $\text{deltaH}_{\text{specific}}$ = (-37.16 kJ/s)/(1/60 kg/s) = -2230 kJ/kg

deltaH = m*$\text{deltaH}_{\text{specific}}$ = (3 kg)(-2230 kJ/kg) = -6690 kJ

2.6f: 1 kg/h = 1/60 kg/s, -1865 kJ/h = -31.08 kW; $\text{deltaH}_{\text{specific}}$ = (-31.08 kJ/s)/(1/60 kg/s) = -1865 kJ/kg

deltaH = m*$\text{deltaH}_{\text{specific}}$ = (3 kg)(-2230 kJ/kg) = -5595 kJ