



PT Filosofi Teknik Utama

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Reverse Engineering Pressure Vessel Air Receiver Tank SN. 006/DPT/III/2010 PT Mitra Harun Gasindo

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Reverse Engineering Pressure Vessel
Air Receiver Tank SN. 006/DPT/III/2010


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REVISION SHEET

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1. Pendahuluan

1.1 Latar Belakang

Berdasarkan pada PERMEN ESDM No. 32 tahun 2021 tentang Inspeksi Teknis dan Pemeriksaan Keselamatan Instalasi dan Peralatan Pada Kegiatan Usaha Minyak dan Gas Bumi, perihal "Pemeriksaan Peralatan Operasi MIGAS yang telah Melewati Umur Desain (Design Life) dan yang Tidak Memiliki Data". Dalam hal ini maka dilakukan penilaian *reverse engineering* pada peralatan milik PT Mitra Harun Gasindo sebagai bentuk tanggung jawab keselamatan kerja dan operasi terhadap peralatan tersebut.

1.2 Tujuan

Adapun lingkup pekerjaan yang dibahas dalam laporan penilaian *reverse engineering* ini meliputi:

- Kalkulasi enjiniring
- Gambar konstruksi bejana tekan
- Datasheet

Hasil penilaian ini digunakan sebagai pemenuhan Pemeriksaan Keselamatan untuk Sertifikat Inspeksi (COI) sesuai dengan Peraturan Menteri ESDM No. 32 Tahun 2021


1.3 Referensi

Laporan ini menguraikan tentang ketentuan inspeksi dan evaluasi data untuk menentukan integritas mekanikal dari sistem bejana tekan. Code/Standart yang digunakan sebagai referensi utama dalam pekerjaan ini adalah:

- Peraturan Menteri Energi Dan Sumber Daya Mineral Republik Indonesia No.32 Tahun 2021 tentang "Inspeksi Teknis dan Pemeriksaan Keselamatan Instalasi dan Peralatan pada Kegiatan Usaha Minyak dan Gas Bumi.
- ASME Section VIII Division 1, Rules for Construction of Pressure Vessels.
- API Publication 510, Pressure Vessel Inspection Code: Inspection, Rating, Repair, and Alteration.
- API 581 Edition 2008, Risk-Based Inspection Technology
- ASME PCC – 3, Inspection Planning Using Risk-Based Methods
- API 572, Inspection Practices for Pressure Vessels.

2. Lingkup Kerja


Cakupan dokumen ini berisi ringkasan berupa data desain, asumsi, kriteria pendesainan dan juga prinsip atau filosofi desain. Ruang lingkup ini meliputi spesifikasi, penggunaan standard/code dan perhitungan.

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3. Data Umum


Data umum bejana tekan dideskripsikan di bawah :

Owner/Operator	: PT Mitra Harun Gasindo
Service	: Air Receiver Tank
Tag No	: -
No Seri	: 006/DPT/III/2010
Code	: ASME Sec. VIII Div. 1 (Analisa)
Material	: JIS G 3101, SS 400 (SA 283 Gr.C)
Design Pressure	: 10 kg/cm ²
Tahun Pembuatan	: 2010
Joint Eff	: 0,85 (Spot)
Corrosion Allowance	: 1 mm
Size	: 950 mm (ID) x 1530 mm (T/T)

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4. Perhitungan Teknis

Perhitungan menggunakan Software PV Elite sesuai ASME Code, Section VIII, Division 1 dapat dilihat pada **Lampiran C**.

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5. Mekanisme Kerusakan

Bejana tekan rentan terhadap berbagai jenis kerusakan umum dan mekanisme kerusakannya adalah sebagai berikut:

Service	: Udara
Material	: JIS G 3101, SS 400 (SA 283 Gr.C)
DP/OP (Psi)	: - /
DT/OT (°F)	: - /
Aliran	: Hidrodinamis
Muatan	: Statis
Insulasi	: Tidak Ada
Kandungan CO	: Tidak Ada
Kandungan H ₂ S	: Tidak Ada
Kandungan H ₂ O	: Ada


Dari tabel damage mechanisms screening ASME PCC 3 - Inspection Planning Using Risk-Based Methods (**Appendix A**) ada beberapa kemungkinan jenis mekanisme kerusakan yang diduga terjadi pada bejana tekan berdasarkan parameter berikut:

- Service & Fluida
- Material
- Suhu
- Aliran
- Beban
- Insulasi

Tingkat kemungkinan (possibility) terjadinya damage mechanism (low, medium, high) berdasarkan dari banyaknya parameter yang sesuai dengan parameter screening. Dari parameter, kemungkinan jenis mekanisme kerusakan yang diduga terjadi pada bejana tekan adalah sebagai berikut:

Tabel 5.1 Mekanisme Kerusakan

No.	Mekanisme Kerusakan	Tipe	Peluang
1	External Corrosion	Penipisan	Rendah
2	General Corrosion	Penipisan	Rendah

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6. Perencanaan Inspeksi

Metode perencanaan inspeksi dilakukan berdasarkan pada kemungkinan mekanisme kerusakan yang telah ditetapkan sesuai kondisi bejana tekan. Penentuan metode inspeksi dan monitoring berdasarkan ASME PCC 3 - Inspection Planning Using Risk-Based Methods (**Appendix B**), perencanaan inspeksi yang diajukan untuk bejana tekan ini adalah sebagai berikut:

Tabel 6.1 Perencanaan Inspeksi

No	Mekanisme Kerusakan	Metode Inspeksi	Meliputi ¹	Interval Inspeksi
1.	External Corrosion	Visual Inspeksi dan UT Thickness/Scanning	Visual inspection of >95% of the exposed surface area with follow-up by UT or pit gauge as required.	4 tahun
2.	General Corrosion			

Note: 1 Ref: API 581 Edition 2008

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7. Penilaian Teknis

MAWP untuk penggunaan selanjutnya dari bejana tekan didasarkan pada perhitungan yang dilakukan menggunakan ASME code edisi terbaru atau menggunakan construction code pada saat bejana tekan dibangun/dibuat.

▪ Cylindrical Shell

$$P = \frac{SEt}{R + 0.6t}$$

▪ 2:1 Ellipsoidal Head

$$P = \frac{2SEt}{D + 0.2t}$$

8. Perhitungan Sisa Umur

Sisa umur bejana tekan (dalam tahun) yang dihitung berdasarkan rumus dari API Publication 510 adalah sebagai berikut:

$$Remaining\ life = \frac{t_{actual} - t_{required}}{corrosion\ rate}$$

Maka dari hasil perhitungan laju korosi dan sisa umur yang telah dilakukan pada bejana tekan ini dapat dilihat dalam tabel berikut:

Tabel 8.1 Perhitungan Sisa Umur (Design Pressure 10 kg/cm²)

Bagian	Ketebalan Awal (mm)	Ketebalan Aktual (mm)	Ketebalan Dibutuhkan (mm)	Corrosion Rate (mm/yr)	Sisa Umur (years)	Catatan
Bottom Head	8,00	7,61	5,30	0,127	18	Memenuhi
Shell	8,00	8,07	5,33	0,127	21	Memenuhi
Top Head	8,00	7,82	5,30	0,127	19	Memenuhi

9. Analisa Risiko

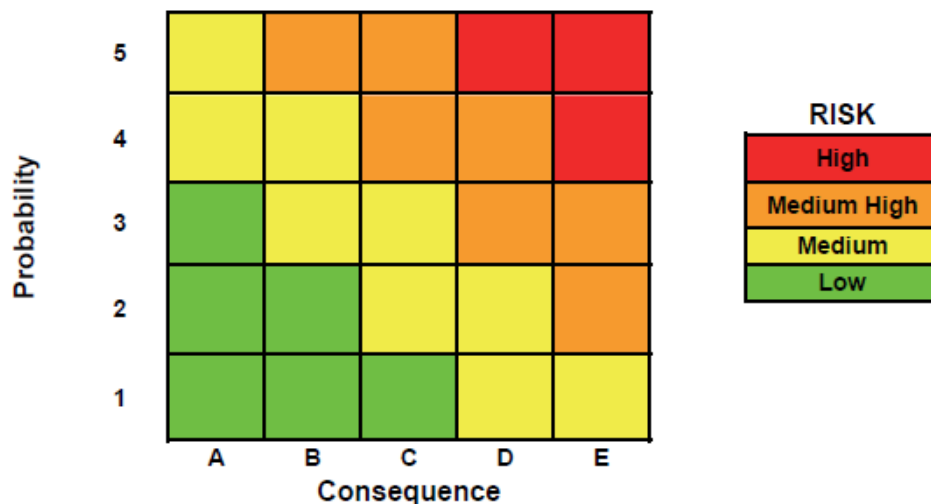
Analisis risiko merupakan aktivitas untuk mengidentifikasi dan menganalisis potensi sebab dan kemungkinan akibat risiko, baik dengan metode kualitatif, semi kuantitatif, maupun kuantitatif. Analisis risiko yang dilakukan di dalam laporan ini bersifat kualitatif.

9.1 Risk Matriks

Analisa risiko dapat dirumuskan sebagai perkalian antara Probability of Failure (PoF) dan Consequence of Failure (CoF) dengan rumus sebagai berikut:

$$\text{Risk} = \text{Probability of Failure (PoF)} \times \text{Consequence of Failure (CoF)}$$

Matrik risiko ditunjukkan pada gambar berikut:



Gambar 9-1 Risk Matrix based on API 581 2016


9.2 Probability of Failure (POF)

Kriteria Probability of Failure (PoF) ditunjukkan pada table berikut:

Tabel 9.1 Probability of Failure (POF) Kriteria

Category	Probability Range
1	$\leq 3.06E-05$
2	$3.06E-05 < 3.06E-04$
3	$3.06E-04 < 3.06E-03$
4	$3.06E-03 < 3.06E-02$
5	$> 3.06E-02$

Ref: API 518 2016 (Table 4.1M – Numerical Values Associated with POF)

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9.3 Consequence of Failure (COF)

Kriteria Consequence of Failure (CoF) ditunjukkan pada table berikut:

Tabel 9.2 Consequence of Failure (COF) Kriteria

Category	Consequence Range (m2)
1	$CA \leq 9.29$
2	$9.29 < CA \leq 92.9$
3	$92.9 < CA \leq 929$
4	$929 < CA \leq 9290$
5	$CA > 9,290$


Ref: API 518 2016 (Table 4.1M – Numerical Values Associated with Area Based COF Categories)

9.4 Hasil Penilaian Resiko

Hasil penilaian risiko secara *qualitative* pada peralatan disediakan pada tabel berikut.

Tabel 9.3 Hasil Penilaian Resiko

No	Deskripsi	Kategori		Risiko	Keterangan
		PoF	CoF		
1	Air Receiver Tank SN. 006/DPT/III/2010	3	2	Medium Risk	Tidak pernah terjadi kebocoran ataupun kegagalan pada peralatan dan juga management tanggap darurat untuk menjaga peralatan tetap <i>save and fit for service</i> .

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10. Kesimpulan dan Rekomendasi

10.1 Kesimpulan

Hasil penilaian integritas pada peralatan sesuai dengan parameter teknis berdasarkan peraturan, kode/standar dan dokumen perusahaan antara lain:

No	Bagian	Ketebalan Awal (mm)	Ketebalan Dibutuhkan (mm)	MAWP (kg/cm ²)	Remakrs
1	Bottom Head	8,00	5,30	16,08	Memenuhi
2	Shell	8,00	5,33	16,08	Memenuhi
3	Top Head	8,00	5,30	16,08	Memenuhi


Secara umum faktor keselamatan dan hasil perhitungan, **Air Receiver Tank SN. 006/DPT/III/2010** dalam kondisi baik untuk beroperasi dan layak untuk digunakan dengan parameter berikut:

MAWP : **16,08 kg/cm²**
Sisa Umur Layan : **216 Bulan**

10.2 Rekomendasi

Disarankan untuk merawat kondisi bejan tekan untuk tetap layak beroperasi dengan saran:

- Melakukan inspeksi dan perawatan secara berkala untuk mengetahui indikasi kebocoran, korosi ekstenal, kerusakan peralatan dan keadaan tidak normal lain pada peralatan proses sesuai kaidah keteknikan yang baik.
- Melakukan pengecatan coating pada bagian yang terindikasi korosi untuk mencegah korosi luar (API RP 572 – 9.3.12).
- Menandai titik pengambilan ketebalan pada bejana tekan, agar pada pengambilan ketebalan selanjutnya dilakukan pada titik yang sama.
- Melakukan kegiatan operasional dengan memperhatikan SOP dan manajemen risiko
- Melakukan pengecekan mekanisme kerusakan lain seperti korosi dan retak
- Memastikan tekanan operasi tidak melebihi MAWP peralatan bejana tekan.

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APPENDIX A

DAMAGE MECHANISM AND DEFECTS SCREENING TABLE

Mechanism	Damage/ Defect	Materials of Construction in Which Mechanism Typically Occurs													Operating Environment															
		Damage Mechanism Manufacturing Defect	Carbon Steel	Low Alloy Steel	300 Series Stainless Steel	400 Series Stainless Steel	Duplex Stainless Steel	Fe-Ni Alloys (0.6–1.3 Fe:Ni Ratios)	Ni-Based Alloys (>50% Ni)	Cu Alloys	Ti	Al Alloys	Cast Iron	Temperature (T) Range in Which Mech. May Occur	Processes in Which Mechanism May Be Suspected. Process Contains:														Flow Req.	Type of Loading
885°F embrittlement	Metallurgical damage	X			X	X								X	X															
Abrasive wear	Metal loss	X	X	X	X	X	X	X	X	X	X	X	X	X	X	X														
Acid dew point corrosion	Metal loss	X	X	X	X	X	X	X				X		X	X					X	X			X	X					
Adhesive wear	Metal loss	X	X	X	X	X	X	X	X	X	X	X		X	X															X
Amine corrosion	Metal loss	X	X	X					X					X	X				X											
Amine cracking	Cracking	X	X						X					X	X				X	X										
Ammonia grooving	Metal loss	X							X					X	X				X	X									X	
Ammonia stress corrosion cracking	Cracking	X	X						X					X	X					X								X		
Ammonium bisulfide corrosion (alkaline sourwater)	Metallurgical damage	X	X	X					X		X	X		X				X	X									X		
Brittle fracture	Cracking	X	X	X	X	X						X		X	X	X											X	X	X	X
Carbonate stress corrosion cracking	Cracking	X	X	X										X	X			X										X		
Carburization	Metallurgical damage	X	X	X	X	X	X	X					X	X			X													
Metal dusting (catastrophic carburization)	Metal loss	X		X	X			X					X				X													
Caustic stress corrosion cracking	Cracking	X	X	X	X	X	X							X	X		X								X			X		
Caustic corrosion (caustic gouging)	Metal loss	X	X	X					X		X			X	X		X								X	X				
Cavitation	Metal loss	X	X	X	X	X	X	X	X	X	X	X		X	X		X								X	X				

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Mechanism	Damage/ Defect	Materials of Construction in Which Mechanism Typically Occurs												Operating Environment																									
		Damage Mechanism	Manufacturing Defect	Carbon Steel	Low Alloy Steel	300 Series Stainless Steel	400 Series Stainless Steel	Duplex Stainless Steel	Fe-Ni Alloys (0.6—1.3 Fe:Ni Ratios)	Ni-Based Alloys (>50% Ni)	Cu Alloys	Ti	Al Alloys	Cast Iron	Temperature (T) Range in Which Mech. May Occur	Processes in Which Mechanism May Be Suspected. Process Contains:												Flow Req.	Type of Loading										
	Mode [Note (1)]													T>1,000°F	800<T<1,000°F	250<T<800°F	32<T<250°F	T<32°F	Water, Steam, Air	Hydrogen	Carbon	Sodium	Carbonate	Sulfur	Amines	Ammonia	Chloride	HF	Phenol	Crude Oil	Phosphoric Acid	Particulates	Other	Motionless—Static	Hydrodynamic	Static Stress [Note (2)]	Impact	Thermal Gradients or Shock	Cyclic Stress (e.g., Vibratory)
Under deposit corrosion	Metal loss	X		X	X	X	X	X	X	X	X	X	X			X	X			X	X	X	X	X	X	X	X	X	X	X	X	X							
Uniform corrosion	Metal loss	X		X	X	X	X	X	X	X	X	X	X			X	X			X	X	X	X	X	X	X	X	X	X	X	X	X							
Weld decay	Metal loss	X				X										X	X			X													X						
Weld metal crater cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										
Weld metal fusion line cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										
Weld metal longitudinal cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										
Weld metal root cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										
Weld metal toe cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										
Weld metal transverse cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										
Weld metal underbead cracking	Weld defects		X	X	X	X	X	X	X	X	X		X																										

GENERAL NOTE: This table does not include misapplication of materials, and damage issues rarely experienced or not typical of process environments.

NOTES:

- (1) Manufacturing, weld, and casting defects can become a factor and also can lead to other damage mechanisms.
- (2) Static stress can include residual tensile stress.

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APPENDIX B


TABLE OF INSPECTION/MONITORING METHODS

	Damage/Defect			Common Examination Methods Used to Identify [Note (1)]																
				Surface				Subsurface				Other Methods								
	Mechanism	Mode [Note (2)]	Damage Mechanism	Manufacturing Defect	Visual (Including Borescope)—VT [Note (3)]	Liquid Penetrant—PT [Note (3)]	Fluorescent Liquid Penetrant—FPT [Note (3)]	Magnetic Particle—MT [Note (4)]	Wet Fluorescent Magnetic Particle—WFMPT [Note (4)]	Ultrasonics for Thickness—UTT	Ultrasonics—Straight Beam—UTS	Ultrasonics—Shear Wave—UTSW	Ultrasonics—Shear Wave Adv. Techniques—UTSWA	Radiography—RT	Eddy-Current—ET	Acoustic Emission—AE	Dimensional Measurements	Hardness Tests	In-Place Metallography (Replication)	Boat/Plug Sample
Dissimilar metal weld cracking (DMW)	Cracking	X		X	X	X	X	X				X	X							
Dissolved O ₂ Attack	Metal loss	X		X											X					X
Electrical discharge	Metal loss	X		X																
Erosion	Metal loss	X		X					X	X	X	X					X			
Erosion—droplets	Metal loss	X		X					X	X	X	X					X			
Erosion—solids	Metal loss	X		X					X	X	X	X					X			
Erosion/corrosion	Metal loss	X		X					X	X	X	X					X			
Fatigue	Cracking	X		X	X	X	X	X		X	X	X		X	X					X
Fatigue, contact	Cracking	X		X	X	X		X							X					
Fatigue, thermal	Cracking	X		X	X	X	X	X		X	X	X		X	X					X
Fatigue, vibration	Cracking	X		X	X	X	X	X		X	X	X		X	X					X
Filiform, corrosion	Metal loss	X		X																X
Flow-accelerated corrosion (FAC)	Metal loss	X		X					X					X						
Flue gas dew point corrosion	Metal loss	X		X					X											
Fretting	Metal loss	X		X	X	X														X
Fuel ash corrosion	Metal loss	X																		
Galvanic corrosion	Metal loss	X		X																X
Graphitization	Metallurgical damage	X																X	X	X
High temp H ₂ /H ₂ S corrosion	Metal loss	X		X					X					X						
Hot cracking	Weld Defects		X	X	X	X	X	X						X		X				X
Hot tensile	Metallurgical damage	X		X													X		X	X
Hydrochloric acid corrosion	Metal loss	X		X					X											
Hydrofluoric acid corrosion	Metal loss	X		X					X					X						

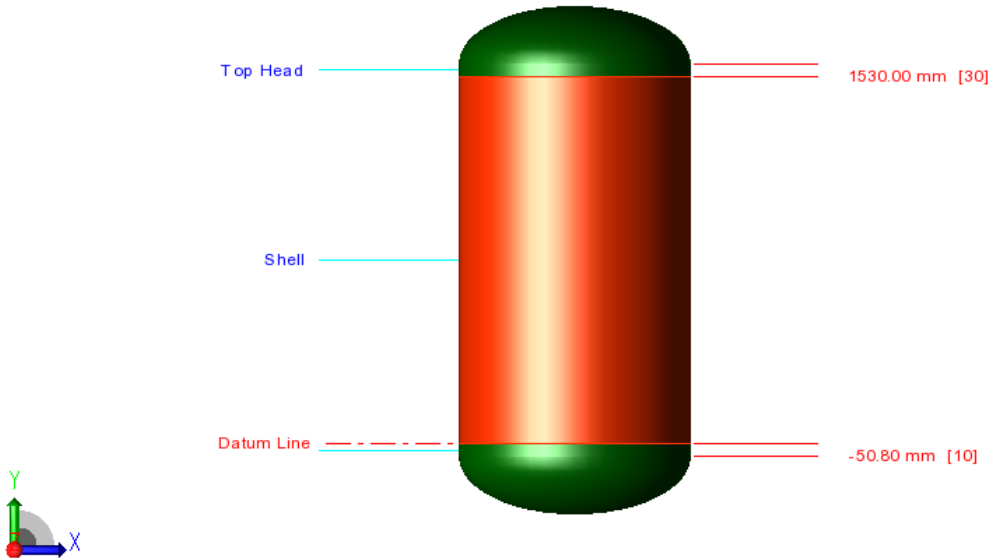
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Mechanism	Damage/Defect			Common Examination Methods Used to Identify [Note (1)]															
				Surface				Subsurface				Other Methods							
	Mode [Note (2)]	Damage Mechanism	Manufacturing Defect	Visual (Including Borescope)—VT [Note (3)]	Liquid Penetrant—PT [Note (3)]	Fluorescent Liquid Penetrant—FPT [Note (3)]	Magnetic Particle—MT [Note (4)]	Wet Fluorescent Magnetic Particle—WFMT [Note (4)]	Ultrasonics for Thickness—UTT	Ultrasonics—Straight Beam—UTS	Ultrasonics—Shear Wave—UTSW	Ultrasonics—Shear Wave Adv. Techniques—UTSWA	Radiography—RT	Eddy-Current—ET	Acoustic Emission—AE	Dimensional Measurements	Hardness Tests	In-Place Metallography (Replication)	Boat/Plug Sample
Sliding wear	Metal loss	X		X					X							X			
Softening (over aging)	Metallurgical damage	X															X		X
Sour water corrosion (acidic)	Metal loss	X		X					X				X						
Spheroidization	Metallurgical damage	X															X	X	X
Strain aging	Metallurgical damage	X															X		X
Stray current corrosion	Metal loss	X		X					X	X	X	X							
Sulfidation	Metal loss	X																X	X
Sulfide-stress cracking (SSC)	Cracking	X			X	X	X	X		X	X	X		X	X			X	X
Sulfuric acid corrosion	Metal loss	X		X					X				X						
Temper embrittlement	Metallurgical damage	X	X																X
Under deposit corrosion	Metal loss	X							X	X									X
Uniform corrosion	Metal loss	X		X					X	X	X	X				X			
Weld decay	Metal loss	X		X						X	X	X							X
Weld metal crater cracking	Weld defects		X	X	X	X	X	X		X	X	X			X				X
Weld metal fusion line cracking	Weld defects		X	X	X	X	X	X		X	X	X	X		X				X
Weld metal longitudinal cracking	Weld defects		X	X	X	X	X	X		X	X	X	X		X				X
Weld metal root cracking	Weld defects		X							X	X	X	X		X				X
Weld metal toe cracking	Weld defects		X	X	X	X	X	X		X	X	X	X		X				X
Weld metal transverse cracking	Weld defects		X	X	X	X	X	X		X	X	X	X		X				X
Weld metal underbead cracking	Weld defects		X							X	X	X	X		X				X

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APPENDIX C **ENGINEERING CALCULATION**



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APPENDIX D
DATA SHEET

FileName : Untitled

Input Echo :

Step: 1 9:17pm Mar 2,2024

PV Elite Vessel Analysis Program: Input Data

Design Internal Pressure (for Hydrotest)	142.20	psig
Design Internal Temperature	200	°F
Type of Hydrotest	UG-99(b)	
Hydrotest Position	Horizontal	
Projection of Nozzle from Vessel Top	0.0000	mm
Projection of Nozzle from Vessel Bottom	0.0000	mm
Minimum Design Metal Temperature	-20	°F
Type of Construction	Welded	
Special Service	None	
Degree of Radiography	RT 1	
Use Higher Longitudinal Stresses (Flag)	Y	
Select t for Internal Pressure (Flag)	N	
Select t for External Pressure (Flag)	N	
Select t for Axial Stress (Flag)	N	
Select Location for Stiff. Rings (Flag)	N	
Consider Vortex Shedding	N	
Perform a Corroded Hydrotest	N	
Is this a Heat Exchanger	No	
User Defined Hydro. Press. (Used if > 0)	0.0000	psig
User defined MAWP	0.0000	psig
User defined MAPnc	0.0000	psig

Load Case 1	NP+EW+WI+FW+BW
Load Case 2	NP+EW+EE+FS+BS
Load Case 3	NP+OW+WI+FW+BW
Load Case 4	NP+OW+EQ+FS+BS
Load Case 5	NP+HW+HI
Load Case 6	NP+HW+HE
Load Case 7	IP+OW+WI+FW+BW
Load Case 8	IP+OW+EQ+FS+BS
Load Case 9	EP+OW+WI+FW+BW
Load Case 10	EP+OW+EQ+FS+BS
Load Case 11	HP+HW+HI
Load Case 12	HP+HW+HE

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Load Case 13		IP+WE+EW
Load Case 14		IP+WF+CW
Load Case 15		IP+VO+OW
Load Case 16		IP+VE+EW
Load Case 17		NP+VO+OW
Load Case 18		FS+BS+IP+OW
Load Case 19		FS+BS+EP+OW
Wind Design Code		ASCE-7 93
Basic Wind Speed	[V]	70.000 mile/hr
Surface Roughness Category		C: Open Terrain
Importance Factor		1.0
Type of Surface		Moderately Smooth
Base Elevation		0.0000 mm
Percent Wind for Hydrotest		33.0
Using User defined Wind Press. Vs Elev.		N
Damping Factor (Beta) for Wind (Ope)		0.0100
Damping Factor (Beta) for Wind (Empty)		0.0000
Damping Factor (Beta) for Wind (Filled)		0.0000
Seismic Design Code		UBC 94
UBC Seismic Zone (1=1,2=2a,3=2b,4=3,5=4)		0.000
UBC Importance Factor		1.000
UBC Soil Type		S1
UBC Horizontal Force Factor		3.000
UBC Percent Seismic for Hydrotest		0.000
Design Nozzle for Des. Press. + St. Head		Y
Consider MAP New and Cold in Noz. Design		N
Consider External Loads for Nozzle Des.		Y
Use ASME VIII-1 Appendix 1-9		N
Material Database Year	Current w/Addenda or Code Year	

Configuration Directives:

Do not use Nozzle MDMT Interpretation VIII-1 01-37	No
Use Table G instead of exact equation for "A"	Yes

FileName : Untitled

Input Echo :

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Shell Head Joints are Tapered	Yes
Compute "K" in corroded condition	Yes
Use Code Case 2286	No
Use the MAWP to compute the MDMT	Yes
Using Metric Material Databases, ASME II D	No

Complete Listing of Vessel Elements and Details:

Element From Node	10
Element To Node	20
Element Type	Elliptical
Description	Bottom Plate
Distance "FROM" to "TO"	50.800 mm
Inside Diameter	950.00 mm
Element Thickness	8.0000 mm
Internal Corrosion Allowance	1.0000 mm
Nominal Thickness	0.0000 mm
External Corrosion Allowance	0.0000 mm
Design Internal Pressure	142.20 psig
Design Temperature Internal Pressure	200 °F
Design External Pressure	15.000 psig
Design Temperature External Pressure	200 °F
Effective Diameter Multiplier	1.2
Material Name	SA-283 C
Allowable Stress, Ambient	15700. psi
Allowable Stress, Operating	15700. psi
Allowable Stress, Hydrotest	20410. psi
Material Density	0.2800 lb/in ³
P Number Thickness	30.988 mm
Yield Stress, Operating	27500. psi
UCS-66 Chart Curve Designation	A
External Pressure Chart Name	CS-2
UNS Number	K02401
Product Form	Plate
Efficiency, Longitudinal Seam	1.0
Efficiency, Circumferential Seam	1.0
Elliptical Head Factor	2.0

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Input Echo :

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Element From Node	20
Element To Node	30
Element Type	Cylinder
Description	Shell
Distance "FROM" to "TO"	1530.0 mm
Inside Diameter	950.00 mm
Element Thickness	8.0000 mm
Internal Corrosion Allowance	1.0000 mm
Nominal Thickness	0.0000 mm
External Corrosion Allowance	0.0000 mm
Design Internal Pressure	142.20 psig
Design Temperature Internal Pressure	200 °F
Design External Pressure	15.000 psig
Design Temperature External Pressure	200 °F
Effective Diameter Multiplier	1.2
Material Name	SA-283 C
Efficiency, Longitudinal Seam	1.0
Efficiency, Circumferential Seam	1.0

Element From Node	30
Element To Node	40
Element Type	Elliptical
Description	Top Head
Distance "FROM" to "TO"	50.800 mm
Inside Diameter	950.00 mm
Element Thickness	8.0000 mm
Internal Corrosion Allowance	1.0000 mm
Nominal Thickness	0.0000 mm
External Corrosion Allowance	0.0000 mm
Design Internal Pressure	142.20 psig
Design Temperature Internal Pressure	200 °F
Design External Pressure	15.000 psig
Design Temperature External Pressure	200 °F
Effective Diameter Multiplier	1.2

FileName : Untitled

Input Echo :

Step:

1

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Material Name	SA-283 C
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Efficiency, Longitudinal Seam	1.0
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Efficiency, Circumferential Seam	1.0
----------------------------------	-----

Elliptical Head Factor	2.0
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XY Coordinate Calculations

From	To	X (Horiz.)	Y (Vert.)	DX (Horiz.)	DY (Vert.)	
		mm	mm	mm	mm	

Bottom Pla		...	50.8000	...	50.8000	
Shell		...	1580.80	...	1530.00	
Top Head		...	1631.60	...	50.8000	

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Internal Pressure Calculations : Step: 3 9:17pm Mar 2,2024

Element Thickness, Pressure, Diameter and Allowable Stress :

		Int. Press	Nominal	Total Corr	Element	Allowable
From	To	+ Liq. Hd	Thickness	Allowance	Diameter	Stress (SE)
		psig	mm	mm	mm	psi

Bottom Pla		142.20	...	1.0000	950.00	15700.
Shell		142.20	...	1.0000	950.00	15700.
Top Head		142.20	...	1.0000	950.00	15700.

Element Required Thickness and MAWP :

		Design	M.A.W.P.	M.A.P.	Minimum	Required
From	To	Pressure	Corroded	New & Cold	Thickness	Thickness
		psig	psig	psig	mm	mm

Bottom Pla		142.200	228.863	263.976	8.00000	5.30314
Shell		142.200	228.863	261.776	8.00000	5.33484
Top Head		142.200	228.863	263.976	8.00000	5.30314
Minimum			228.863	261.775		

MAWP: 228.863 psig, limited by: Top Head.

Internal Pressure Calculation Results :**ASME Code, Section VIII, Division 1, 2015****Elliptical Head From 10 To 20 SA-283 C , UCS-66 Crv. A at 200 °F**

Bottom Plate

Material UNS Number: K02401

Required Thickness due to Internal Pressure [tr]:

$$= (P \cdot D \cdot K_{cor}) / (2 \cdot S \cdot E - 0.2 \cdot P) \text{ Appendix 1-4 (c)}$$

$$= (142.200 \cdot 952.0000 \cdot 0.997) / (2 \cdot 15700.00 \cdot 1.00 - 0.2 \cdot 142.200)$$

$$= 4.3031 + 1.0000 = 5.3031 \text{ mm}$$

Max. Allowable Working Pressure at given Thickness, corroded [MAWP]:

$$\begin{aligned}
 &= (2 * S * E * t) / (K_{cor} * D + 0.2 * t) \text{ per Appendix 1-4 (c)} \\
 &= (2 * 15700.00 * 1.00 * 7.0000) / (0.997 * 952.0000 + 0.2 * 7.0000) \\
 &= 231.188 \text{ psig}
 \end{aligned}$$

Maximum Allowable Pressure, New and Cold [MAPNC]:

$$\begin{aligned}
 &= (2 * S * E * t) / (K * D + 0.2 * t) \text{ per Appendix 1-4 (c)} \\
 &= (2 * 15700.00 * 1.00 * 8.0000) / (1.000 * 950.0001 + 0.2 * 8.0000) \\
 &= 263.976 \text{ psig}
 \end{aligned}$$

Actual stress at given pressure and thickness, corroded [Sact]:

$$\begin{aligned}
 &= (P * (K_{cor} * D + 0.2 * t)) / (2 * E * t) \\
 &= (142.200 * (0.997 * 952.0000 + 0.2 * 7.0000)) / (2 * 1.00 * 7.0000) \\
 &= 9656.819 \text{ psi}
 \end{aligned}$$

Straight Flange Required Thickness:

$$\begin{aligned}
 &= (P * R) / (S * E - 0.6 * P) + c \text{ per UG-27 (c) (1)} \\
 &= (142.200 * 476.0000) / (15700.00 * 1.00 - 0.6 * 142.200) + 1.000 \\
 &= 5.335 \text{ mm}
 \end{aligned}$$

Straight Flange Maximum Allowable Working Pressure:

$$\begin{aligned}
 &= (S * E * t) / (R + 0.6 * t) \text{ per UG-27 (c) (1)} \\
 &= (15700.00 * 1.00 * 7.0000) / (476.0000 + 0.6 * 7.0000) \\
 &= 228.863 \text{ psig}
 \end{aligned}$$

Factor K, corroded condition [Kcor]:

$$\begin{aligned}
 &= (2 + (\text{Inside Diameter} / (2 * \text{Inside Head Depth}))^2) / 6 \\
 &= (2 + (952.000 / (2 * 238.500))^2) / 6 \\
 &= 0.997208
 \end{aligned}$$

$$\text{Percent Elong. per UCS-79, VIII-1-01-57 } (75 * t_{nom} / R_f) * (1 - R_f / R_o) = 3.625 \%$$

MDMT Calculations in the Knuckle Portion:

$$\text{Govrn. thk, } t_g = 8.000, t_r = 6.930, c = 1.0000 \text{ mm, } E^* = 1.00$$

$$\text{Stress Ratio} = t_r * (E^*) / (t_g - c) = 0.990, \text{ Temp. Reduction} = 1 \text{ } ^\circ\text{F}$$

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Internal Pressure Calculations : Step: 3 9:17pm Mar 2,2024

Min Metal Temp. w/o impact per UCS-66, Curve A	18 °F
Min Metal Temp. at Required thickness (UCS 66.1)	17 °F
Min Metal Temp. w/o impact per UG-20(f)	-20 °F

MDMT Calculations in the Head Straight Flange:

Govrn. thk, tg = 8.000 , tr = 7.000 , c = 1.0000 mm , E* = 1.00

Stress Ratio = tr * (E*)/(tg - c) = 1.000 , Temp. Reduction = 0 °F

Min Metal Temp. w/o impact per UCS-66, Curve A	18 °F
Min Metal Temp. w/o impact per UG-20(f)	-20 °F

Cylindrical Shell From 20 To 30 SA-283 C , UCS-66 Crv. A at 200 °F

Shell

Material UNS Number: K02401

Required Thickness due to Internal Pressure [tr]:

$$\begin{aligned}
 &= (P \cdot R) / (S \cdot E - 0.6 \cdot P) \text{ per UG-27 (c) (1)} \\
 &= (142.200 \cdot 476.0000) / (15700.00 \cdot 1.00 - 0.6 \cdot 142.200) \\
 &= 4.3348 + 1.0000 = 5.3348 \text{ mm}
 \end{aligned}$$

Max. Allowable Working Pressure at given Thickness, corroded [MAWP]:

$$\begin{aligned}
 &= (S \cdot E \cdot t) / (R + 0.6 \cdot t) \text{ per UG-27 (c) (1)} \\
 &= (15700.00 \cdot 1.00 \cdot 7.0000) / (476.0000 + 0.6 \cdot 7.0000) \\
 &= 228.863 \text{ psig}
 \end{aligned}$$

Maximum Allowable Pressure, New and Cold [MAPNC]:

$$\begin{aligned}
 &= (S \cdot E \cdot t) / (R + 0.6 \cdot t) \text{ per UG-27 (c) (1)} \\
 &= (15700.00 \cdot 1.00 \cdot 8.0000) / (475.0000 + 0.6 \cdot 8.0000) \\
 &= 261.776 \text{ psig}
 \end{aligned}$$

Actual stress at given pressure and thickness, corroded [Sact]:

$$\begin{aligned}
 &= (P \cdot (R + 0.6 \cdot t)) / (E \cdot t) \\
 &= (142.200 \cdot (476.0000 + 0.6 \cdot 7.0000)) / (1.00 \cdot 7.0000) \\
 &= 9754.920 \text{ psi}
 \end{aligned}$$

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Internal Pressure Calculations : Step: 3 9:17pm Mar 2,2024

Percent Elongation per UCS-79 $(50 \cdot t_{nom}/R_f) \cdot (1 - R_f/R_o)$ 0.835 %**Minimum Design Metal Temperature Results:**Govrn. thk, $t_g = 8.000$, $t_r = 7.000$, $c = 1.0000$ mm , $E^* = 1.00$ Stress Ratio = $t_r \cdot (E^*) / (t_g - c) = 1.000$, Temp. Reduction = 0 °F

Min Metal Temp. w/o impact per UCS-66, Curve A 18 °F

Min Metal Temp. w/o impact per UG-20(f) -20 °F

Elliptical Head From 30 To 40 SA-283 C , UCS-66 Crv. A at 200 °F**Top Head**

Material UNS Number: K02401

Required Thickness due to Internal Pressure [tr]:

$$\begin{aligned}
 &= (P \cdot D \cdot K_{cor}) / (2 \cdot S \cdot E - 0.2 \cdot P) \text{ Appendix 1-4 (c)} \\
 &= (142.200 \cdot 952.0000 \cdot 0.997) / (2 \cdot 15700.00 \cdot 1.00 - 0.2 \cdot 142.200) \\
 &= 4.3031 + 1.0000 = 5.3031 \text{ mm}
 \end{aligned}$$

Max. Allowable Working Pressure at given Thickness, corroded [MAWP]:

$$\begin{aligned}
 &= (2 \cdot S \cdot E \cdot t) / (K_{cor} \cdot D + 0.2 \cdot t) \text{ per Appendix 1-4 (c)} \\
 &= (2 \cdot 15700.00 \cdot 1.00 \cdot 7.0000) / (0.997 \cdot 952.0000 + 0.2 \cdot 7.0000) \\
 &= 231.188 \text{ psig}
 \end{aligned}$$

Maximum Allowable Pressure, New and Cold [MAPNC]:

$$\begin{aligned}
 &= (2 \cdot S \cdot E \cdot t) / (K \cdot D + 0.2 \cdot t) \text{ per Appendix 1-4 (c)} \\
 &= (2 \cdot 15700.00 \cdot 1.00 \cdot 8.0000) / (1.000 \cdot 950.0001 + 0.2 \cdot 8.0000) \\
 &= 263.976 \text{ psig}
 \end{aligned}$$

Actual stress at given pressure and thickness, corroded [Sact]:

$$\begin{aligned}
 &= (P \cdot (K_{cor} \cdot D + 0.2 \cdot t)) / (2 \cdot E \cdot t) \\
 &= (142.200 \cdot (0.997 \cdot 952.0000 + 0.2 \cdot 7.0000)) / (2 \cdot 1.00 \cdot 7.0000) \\
 &= 9656.819 \text{ psi}
 \end{aligned}$$

Straight Flange Required Thickness:

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Internal Pressure Calculations : Step: 3 9:17pm Mar 2,2024

$$= (P \cdot R) / (S \cdot E - 0.6 \cdot P) + c \quad \text{per UG-27 (c) (1)}$$

$$= (142.200 \cdot 476.0000) / (15700.00 \cdot 1.00 - 0.6 \cdot 142.200) + 1.000$$

$$= 5.335 \text{ mm}$$

Straight Flange Maximum Allowable Working Pressure:

$$= (S \cdot E \cdot t) / (R + 0.6 \cdot t) \quad \text{per UG-27 (c) (1)}$$

$$= (15700.00 \cdot 1.00 \cdot 7.0000) / (476.0000 + 0.6 \cdot 7.0000)$$

$$= 228.863 \text{ psig}$$

Factor K, corroded condition [Kcor]:

$$= (2 + (\text{Inside Diameter} / (2 \cdot \text{Inside Head Depth}))^2) / 6$$

$$= (2 + (952.000 / (2 \cdot 238.500))^2) / 6$$

$$= 0.997208$$

Percent Elong. per UCS-79, VIII-1-01-57 $(75 \cdot t_{nom} / R_f) \cdot (1 - R_f / R_o)$ 3.625 %**MDMT Calculations in the Knuckle Portion:**Govrn. thk, $t_g = 8.000$, $t_r = 6.930$, $c = 1.0000$ mm, $E^* = 1.00$ Stress Ratio = $t_r \cdot (E^*) / (t_g - c) = 0.990$, Temp. Reduction = 1 °F

Min Metal Temp. w/o impact per UCS-66, Curve A	18 °F
Min Metal Temp. at Required thickness (UCS 66.1)	17 °F
Min Metal Temp. w/o impact per UG-20 (f)	-20 °F

MDMT Calculations in the Head Straight Flange:Govrn. thk, $t_g = 8.000$, $t_r = 7.000$, $c = 1.0000$ mm, $E^* = 1.00$ Stress Ratio = $t_r \cdot (E^*) / (t_g - c) = 1.000$, Temp. Reduction = 0 °F

Min Metal Temp. w/o impact per UCS-66, Curve A	18 °F
Min Metal Temp. w/o impact per UG-20 (f)	-20 °F

Note: Heads and Shells Exempted to -20F (-29C) by paragraph UG-20F

Hydrostatic Test Pressure Results:

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Internal Pressure Calculations : Step: 3 9:17pm Mar 2,2024

Pressure per UG99b	= 1.3 * M.A.W.P. * Sa/S	297.522	psig
Pressure per UG99b[36]	= 1.3 * Design Pres * Sa/S	184.860	psig
Pressure per UG99c	= 1.3 * M.A.P. - Head(Hyd)	338.957	psig
Pressure per UG100	= 1.1 * M.A.W.P. * Sa/S	251.749	psig
Pressure per PED	= 1.43 * MAWP	327.274	psig
Pressure per App 27-4	= 1.3 * M.A.W.P. * Sa/S	297.522	psig

UG-99(b), Test Pressure Calculation:

= Test Factor * MAWP * Stress Ratio
 = 1.3 * 228.863 * 1.000
 = 297.522 psig

Horizontal Test performed per: UG-99b

*Please note that Nozzle, Shell, Head, Flange, etc MAWPs are all considered
 when determining the hydrotest pressure for those test types that are based
 on the MAWP of the vessel.*

Stresses on Elements due to Test Pressure:

From To	Stress	Allowable	Ratio	Pressure
Bottom Plate	17775.4	20410.0	0.871	298.87
Shell	17924.9	20410.0	0.878	298.87
Top Head	17775.4	20410.0	0.871	298.87

Stress ratios for Vessel Elements:

Description	Ambient	Operating	ratio
Bottom Plate	15700.00	15700.00	1.000
Shell	15700.00	15700.00	1.000
Top Head	15700.00	15700.00	1.000
Minimum			1.000

Elements Suitable for Internal Pressure.

External Pressure Calculation Results :**ASME Code, Section VIII, Division 1, 2015****Elliptical Head From 10 to 20 Ext. Chart: CS-2 at 200 °F**

Bottom Plate

Elastic Modulus from Chart: CS-2 at 200 °F : 0.290E+08 psi

Results for Maximum Allowable External Pressure (MAEP):

Tca	OD	D/t	Factor A	B
7.000	966.00	138.00	0.0010064	12399.87

$$EMAP = B / (K0 * D/t) = 12399.8711 / (0.9000 * 138.0000) = 99.8379 \text{ psig}$$

Results for Required Thickness (Tca):

Tca	OD	D/t	Factor A	B
2.501	966.00	386.22	0.0003596	5214.32

$$EMAP = B / (K0 * D/t) = 5214.3184 / (0.9000 * 386.2229) = 15.0009 \text{ psig}$$

*Check the requirements of UG-33(a)(1) using $P = 1.67 * \text{External Design pressure for this head.}$*

Material UNS Number: K02401

Required Thickness due to Internal Pressure [tr]:

$$\begin{aligned}
 &= (P * D * K_{cor}) / (2 * S * E - 0.2 * P) \text{ Appendix 1-4 (c)} \\
 &= (25.050 * 952.0000 * 0.997) / (2 * 15700.00 * 1.00 - 0.2 * 25.050) \\
 &= 0.7575 + 1.0000 = 1.7575 \text{ mm}
 \end{aligned}$$

Max. Allowable Working Pressure at given Thickness, corroded [MAWP]:

$$\begin{aligned}
 &= ((2 * S * E * t) / (K_{cor} * D + 0.2 * t)) / 1.67 \text{ per Appendix 1-4 (c)} \\
 &= ((2 * 15700.00 * 1.00 * 7.0000) / (0.997 * 952.0000 + 0.2 * 7.0000)) / 1.67 \\
 &= 138.436 \text{ psig}
 \end{aligned}$$

Maximum Allowable External Pressure [MAEP]:

$$= \min(MAEP, MAWP)$$

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External Pressure Calculations : Step: 4 9:17pm Mar 2,2024

$$= \min(99.84 , 138.4359)$$

$$= 99.838 \text{ psig}$$

Thickness requirements per UG-33(a)(1) do not govern the required thickness of this head.

Cylindrical Shell From 20 to 30 Ext. Chart: CS-2 at 200 °F

Shell

Elastic Modulus from Chart: CS-2 at 200 °F : 0.290E+08 psi

Results for Maximum Allowable External Pressure (MAEP):

Tca	OD	SLen	D/t	L/D	Factor A	B
7.000	966.00	1789.93	138.00	1.8529	0.0004322	6267.06

$$\text{EMAP} = (4*B) / (3*(D/t)) = (4*6267.0625) / (3*138.0000) = 60.5513 \text{ psig}$$

Results for Required Thickness (Tca):

Tca	OD	SLen	D/t	L/D	Factor A	B
4.003	966.00	1789.93	241.33	1.8529	0.0001872	2715.03

$$\text{EMAP} = (4*B) / (3*(D/t)) = (4*2715.0261) / (3*241.3271) = 15.0005 \text{ psig}$$

Results for Maximum Stiffened Length (Slen):

Tca	OD	SLen	D/t	L/D	Factor A	B
7.000	966.00	6569.47	138.00	6.8007	0.0001071	1553.30

$$\text{EMAP} = (4*B) / (3*(D/t)) = (4*1553.3014) / (3*138.0000) = 15.0077 \text{ psig}$$

Elliptical Head From 30 to 40 Ext. Chart: CS-2 at 200 °F

Top Head

Elastic Modulus from Chart: CS-2 at 200 °F : 0.290E+08 psi

Results for Maximum Allowable External Pressure (MAEP):

Tca	OD	D/t	Factor A	B
7.000	966.00	138.00	0.0010064	12399.87

$$\text{EMAP} = B / (K0*D/t) = 12399.8711 / (0.9000 * 138.0000) = 99.8379 \text{ psig}$$

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External Pressure Calculations : Step: 4 9:17pm Mar 2,2024

Results for Required Thickness (Tca):

Tca	OD	D/t	Factor A	B
2.501	966.00	386.22	0.0003596	5214.32

$$\text{EMAP} = B / (K_0 * D/t) = 5214.3184 / (0.9000 * 386.2229) = 15.0009 \text{ psig}$$

*Check the requirements of UG-33(a)(1) using $P = 1.67 * \text{External Design pressure for this head.}$*

Material UNS Number: K02401

Required Thickness due to Internal Pressure [tr]:

$$\begin{aligned}
 &= (P * D * K_{cor}) / (2 * S * E - 0.2 * P) \text{ Appendix 1-4 (c)} \\
 &= (25.050 * 952.0000 * 0.997) / (2 * 15700.00 * 1.00 - 0.2 * 25.050) \\
 &= 0.7575 + 1.0000 = 1.7575 \text{ mm}
 \end{aligned}$$

Max. Allowable Working Pressure at given Thickness, corroded [MAWP]:

$$\begin{aligned}
 &= ((2 * S * E * t) / (K_{cor} * D + 0.2 * t)) / 1.67 \text{ per Appendix 1-4 (c)} \\
 &= ((2 * 15700.00 * 1.00 * 7.0000) / (0.997 * 952.0000 + 0.2 * 7.0000)) / 1.67 \\
 &= 138.436 \text{ psig}
 \end{aligned}$$

Maximum Allowable External Pressure [MAEP]:

$$\begin{aligned}
 &= \min(\text{MAEP}, \text{MAWP}) \\
 &= \min(99.84, 138.4359) \\
 &= 99.838 \text{ psig}
 \end{aligned}$$

Thickness requirements per UG-33(a)(1) do not govern the required thickness of this head.

External Pressure Calculations

From	To	Section Length mm	Outside Diameter mm	Corroded Thickness mm	Factor A	Factor B psi
10	20	No Calc	966.000	7.00000	0.0010064	12399.9
20	30	1789.93	966.000	7.00000	0.00043221	6267.06
30	40	No Calc	966.000	7.00000	0.0010064	12399.9

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External Pressure Calculations : Step: 4 9:17pm Mar 2,2024

External Pressure Calculations

		External	External	External	External
From	To	Actual T.	Required T.	Des. Press.	M.A.W.P.
		mm	mm	psig	psig

10	20	8.00000	3.50115	15.0000	99.8379
20	30	8.00000	5.00287	15.0000	60.5513
30	40	8.00000	3.50115	15.0000	99.8379
Minimum					60.551

External Pressure Calculations

		Actual Len.	Allow. Len.	Ring Inertia	Ring Inertia
From	To	Bet. Stiff.	Bet. Stiff.	Required	Available
		mm	mm	in**4	in**4

10	20	No Calc	No Calc	No Calc	No Calc
20	30	1789.93	6569.47	No Calc	No Calc
30	40	No Calc	No Calc	No Calc	No Calc

[Elements Suitable for External Pressure.](#)**[PV Elite is a trademark of Intergraph CADWorx & Analysis Solutions, Inc. 2016](#)**

Element and Detail Weights

From	To	Element Metal Wgt. lbf	Element ID Volume in ³	Corroded Metal Wgt. lbf	Corroded ID Volume in ³	Extra due Misc % lbf
10	20	171.047	9046.06	149.666	9098.66	...
20	30	629.440	66180.1	551.335	66459.0	...
30	40	171.047	9046.06	149.666	9098.66	...
Total		971	84272	850	84656	0

Weight Summation: lbf

Fabricated	Shop Test	Shipping	Erected	Empty	Operating
971.5	971.5	971.5	971.5	971.5	971.5
...	3043.2
...
...
...
971.5	4014.7	971.5	971.5	971.5	971.5

Note:

The shipping total has been modified because some items have been specified as being installed in the shop.

Weight Summary

Fabricated Wt.	- Bare Weight W/O Removable Internals	971.5 lbf
Shop Test Wt.	- Fabricated Weight + Water (Full)	4014.7 lbf
Shipping Wt.	- Fab. Wt + Rem. Intls.+ Shipping App.	971.5 lbf
Erected Wt.	- Fab. Wt + Rem. Intls.+ Insul. (etc)	971.5 lbf
Ope. Wt. no Liq	- Fab. Wt + Intls. + Details + Wghts.	971.5 lbf
Operating Wt.	- Empty Wt + Operating Liq. Uncorroded	971.5 lbf
Field Test Wt.	- Empty Weight + Water (Full)	4014.7 lbf
Mass of the Upper 1/3 of the Vertical Vessel		327.3 lbf

Outside Surface Areas of Elements

		Surface	
From	To	Area	
		in ²	

10	20	1806.83	
20	30	7196.99	
30	40	1806.83	
Total		10810.652 in ²	[75.1 Square Feet]

Element and Detail Weights

	To	Total Ele.	Total. Ele.	Total. Ele.	Total Dtl.	Oper. Wgt.	
From	To	Empty Wgt.	Oper. Wgt.	Hydro. Wgt.	Offset Mom.	No Liquid	
		lbm	lbm	lbm	ft-lb	lbm	

10	20	171.047	171.047	497.710	...	171.047	
20	30	629.440	629.440	3019.28	...	629.440	
30	40	171.047	171.047	497.710	...	171.047	

Cumulative Vessel Weight

		Cumulative Ope	Cumulative	Cumulative	
From	To	Wgt. No Liquid	Oper. Wgt.	Hydro. Wgt.	
		lbm	lbm	lbm	

10	20	971.533	971.533	4014.70	
20	30	800.487	800.487	3516.99	
30	40	171.047	171.047	497.710	

Note: The cumulative operating weights no liquid in the column above
are the cumulative operating weights minus the operating liquid
weight minus any weights absent in the empty condition.

Cumulative Vessel Moment

FileName : Untitled

Element and Detail Weights : Step: 5 9:17pm Mar 2,2024

		Cumulative	Cumulative	Cumulative	
From	To	Empty Mom.	Oper. Mom.	Hydro. Mom.	
		ft-lb	ft-lb	ft-lb	

10	20	
20	30	
30	40	

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Shop/Field Installation Options :

Note : The CG is computed from the first Element From Node

Center of Gravity of Bare Shell New and Cold	815.800 mm
Center of Gravity of Bare Shell Corroded	815.800 mm
Vessel CG in the Operating Condition	815.800 mm
Vessel CG in the Fabricated (Shop/Empty) Condition	815.800 mm

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Minimum Design Metal Temperature Results Summary :

Description	Notes	Curve	Basic MDMT °F	Reduced MDMT °F	UG-20 (f) MDMT °F	Thickness ratio	Gov Thk mm	E*
Bottom Plate	[10]	A	18	17	-20	0.990	8.000	1.000
Bottom Plate	[7]	A	18	18	-20	1.000	8.000	1.000
Shell	[8]	A	18	18	-20	1.000	8.000	1.000
Top Head	[10]	A	18	17	-20	0.990	8.000	1.000
Top Head	[7]	A	18	18	-20	1.000	8.000	1.000
Required Minimum Design Metal Temperature						-20	°F	
Warmest Computed Minimum Design Metal Temperature						-20	°F	

Notes:

- [!] - This was an impact tested material.
- [1] - Governing Nozzle Weld.
- [4] - ANSI Flange MDMT Calcs; Thickness ratio per UCS-66(b)(1)(c).
- [5] - ANSI Flange MDMT Calcs; Thickness ratio per UCS-66(b)(1)(b).
- [6] - MDMT Calculations at the Shell/Head Joint.
- [7] - MDMT Calculations for the Straight Flange.
- [8] - Cylinder/Cone/Flange Junction MDMT.
- [9] - Calculations in the Spherical Portion of the Head.
- [10] - Calculations in the Knuckle Portion of the Head.
- [11] - Calculated (Body Flange) Flange MDMT.
- [12] - Calculated Flat Head MDMT per UCS-66.3
- [13] - Tubesheet MDMT, shell side, if applicable
- [14] - Tubesheet MDMT, tube side, if applicable
- [15] - Nozzle Material
- [16] - Shell or Head Material
- [17] - Impact Testing required

UG-84(b)(2) was not considered.

UCS-66(g) was not considered.

UCS-66(i) was not considered.

Notes:

Impact test temps were not entered in and not considered in the analysis.

UCS-66(i) applies to impact tested materials not by specification and

UCS-66(g) applies to materials impact tested per UG-84.1 General Note (c).

The Basic MDMT includes the (30F) PWHT credit if applicable.

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FileName : Untitled

Vessel Design Summary :

Step: 8 9:17pm Mar 2,2024

ASME Code, Section VIII, Division 1, 2015

Diameter Spec : 950.000 mm ID

Vessel Design Length, Tangent to Tangent 1631.60 mm

Distance of Bottom Tangent above Grade 0.00 mm

Distance of Base above Grade 0.00 mm

Specified Datum Line Distance 50.80 mm

Shell Material SA-283 C

Internal Design Temperature 200 °F

Internal Design Pressure 142.200 psig

External Design Temperature 200 °F

External Design Pressure 15.000 psig

Maximum Allowable Working Pressure 228.863 psig

External Max. Allowable Working Pressure 60.551 psig

Hydrostatic Test Pressure 297.522 psig

Required Minimum Design Metal Temperature -20 °F

Warmest Computed Minimum Design Metal Temperature -20 °F

Wind Design Code ASCE-93

Earthquake Design Code UBC-94

Element Pressures and MAWP: psig

Element Desc	Design Pres.	External	M.A.W.P	Corrosion
	+ Stat. head	Pressure		Allowance
Bottom Plate	142.200	15.000	228.863	1.0000
Shell	142.200	15.000	228.863	1.0000
Top Head	142.200	15.000	228.863	1.0000

Element Type	"To" Elev	Length	Element Thk	R e q d	T h k	Joint Eff
	mm	mm	mm	Int.	Ext.	Long Circ

FileName : Untitled

Vessel Design Summary :

Step:

8

9:17pm

Mar 2, 2024

Ellipse	0.0	50.8	8.0	5.3	3.5	1.00	1.00
Cylinder	1530.0	1530.0	8.0	5.3	5.0	1.00	1.00
Ellipse	1580.8	50.8	8.0	5.3	3.5	1.00	1.00

Element thicknesses are shown as Nominal if specified, otherwise are Minimum

Weights:


Fabricated - Bare	W/O Removable Internals	971.5	lbm
Shop Test - Fabricated + Water (Full)		4014.7	lbm
Shipping - Fab. + Rem. Intls.+ Shipping App.		971.5	lbm
Erected - Fab. + Rem. Intls.+ Insul. (etc)		971.5	lbm
Empty - Fab. + Intls. + Details + Wghts.		971.5	lbm
Operating - Empty + Operating Liquid (No CA)		971.5	lbm
Field Test - Empty Weight + Water (Full)		4014.7	lbm

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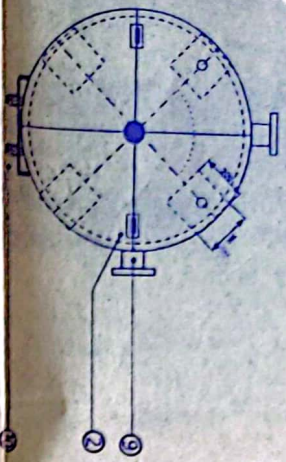
Revision : -

1. All dimensions are in millimeter and inch, unless otherwise specified.

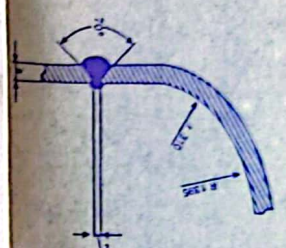
	Reverse Engineering Pressure Vessel Air Receiver Tank SN. 006/DPT/III/2010	Rev. 0
	FTU-056/02/R-RLA/II/2024	Page 23

APPENDIX E

DRAWING



TOP VIEW



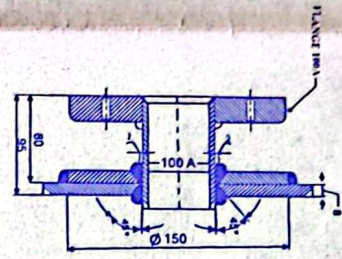
DETAIL CIRCUMSEAM



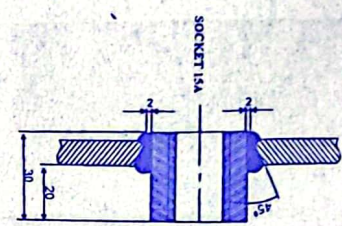
DETAIL LONG SEAM



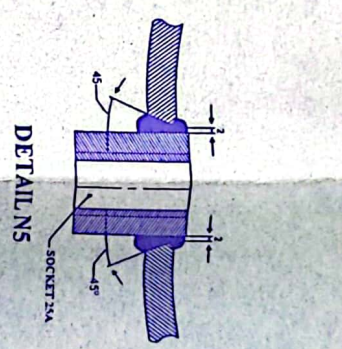
DETAIL N1



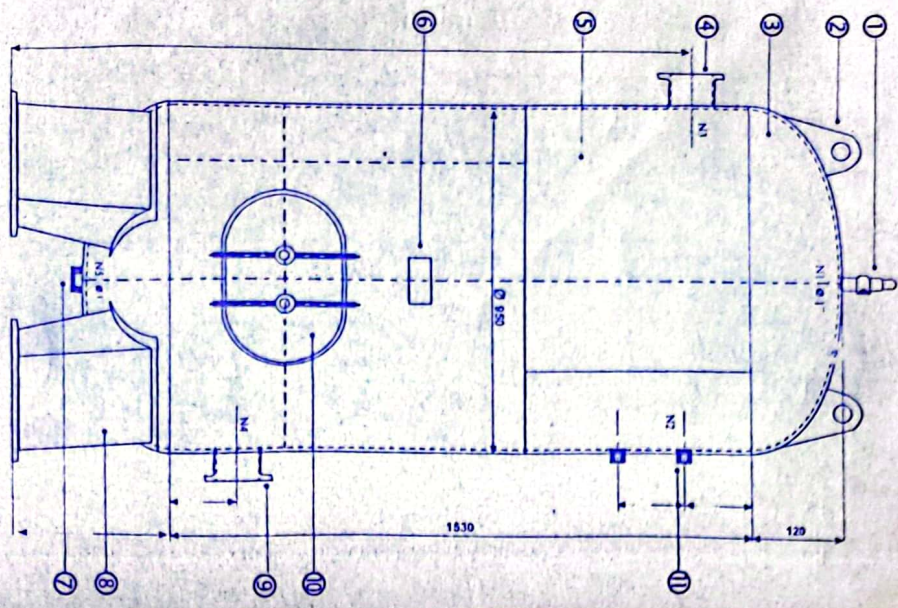
DETAIL N3 - N4



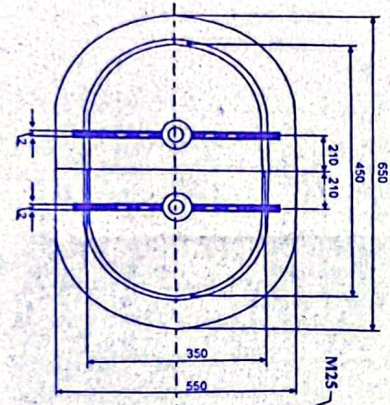
DETAIL N2



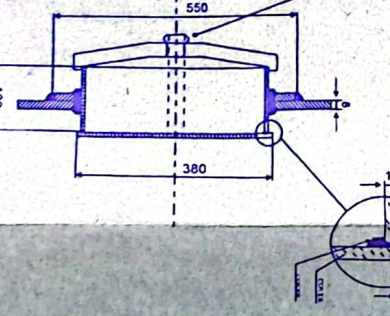
DETAIL N5



FRONT VIEW



DETAIL MANHOLE



PT DAVA PERKASA TEKNIK
 Jl. Agung Karna II Blok D 12 Komplek Indoflora
 Sateja Agung Podomoro
 Telp. (021) 6510518 - 6510716 - 687080
 Fax. (021) 682113
 JAKARTA

NO	DESCRIPTION	DATE	DESIGN	THICK	UNIT
1	FLANG 100A				
2	SOCKET 15A				
3	SOCKET 15A				
4	SOCKET 15A				
5	SOCKET 15A				
6	SOCKET 15A				
7	SOCKET 15A				
8	SOCKET 15A				
9	SOCKET 15A				
10	SOCKET 15A				
11	SOCKET 15A				
12	SOCKET 15A				
13	SOCKET 15A				
14	SOCKET 15A				
15	SOCKET 15A				
16	SOCKET 15A				
17	SOCKET 15A				

NO	DESCRIPTION	DATE	DESIGN	THICK	UNIT
1	FLANG 100A				
2	SOCKET 15A				
3	SOCKET 15A				
4	SOCKET 15A				
5	SOCKET 15A				
6	SOCKET 15A				
7	SOCKET 15A				
8	SOCKET 15A				
9	SOCKET 15A				
10	SOCKET 15A				
11	SOCKET 15A				
12	SOCKET 15A				
13	SOCKET 15A				
14	SOCKET 15A				
15	SOCKET 15A				
16	SOCKET 15A				
17	SOCKET 15A				

**PRESSURE VESSEL
 STANDARD**

AIR RECEIVER TANK 1.000 L

NO	DESCRIPTION	DATE	DESIGN	THICK	UNIT
1	FLANG 100A				
2	SOCKET 15A				
3	SOCKET 15A				
4	SOCKET 15A				
5	SOCKET 15A				
6	SOCKET 15A				
7	SOCKET 15A				
8	SOCKET 15A				
9	SOCKET 15A				
10	SOCKET 15A				
11	SOCKET 15A				
12	SOCKET 15A				
13	SOCKET 15A				
14	SOCKET 15A				
15	SOCKET 15A				
16	SOCKET 15A				
17	SOCKET 15A				