

## Terminal Velocity

at constant terminal velocity

$$\begin{aligned} F_D &= \frac{1}{2} \rho_f C_D U_t^2 \\ F_g - F_b &= (\rho_p - \rho_f) V_p g \\ \frac{1}{2} \rho_f C_D U_t^2 &= (\rho_p - \rho_f) V_p g \end{aligned}$$

$$V_p = \frac{\pi d_p^3}{6} \quad A_p = \frac{\pi d_p^2}{4}$$

$$U_t = \sqrt{\frac{4(\rho_p - \rho_f)g d_p}{3 C_D \rho_f}}$$

$$\begin{aligned} &= 24/Re \quad \text{if } Re < 1 \\ C_D &= \frac{24}{Re} (1 + 0.15 Re^{0.687}) \quad \text{if } 1 < Re < 800 \\ &= 0.44 \quad Re > 1000 \text{ to } 10^5 \end{aligned}$$

$$Re = \frac{\rho U_t d_p}{\mu}$$

So  $U_t \rightarrow Re \rightarrow \text{Regime} \rightarrow C_D \rightarrow U_t$

Problem Oil droplets of diameter 2 mm are to be settled from air with  $\rho_f = 1.18 \text{ kg/m}^3$ . The density of oil is  $900 \text{ kg/m}^3$ . Calculate the terminal settling velocity of the particles. For air at these conditions  $\mu = 1.85 \times 10^{-5} \text{ kg/m.s}$

$C_D$  is given by  $C_D = \frac{24}{Re} (1 + 0.15 Re^{0.687})$

Sol<sup>n</sup> try with successive substitution using MTS Excel

$$U_t^{k+1} = f(U_t^k)$$

Start from  $U_t^k (k=0) \rightarrow Re^k \rightarrow C_D^k \rightarrow \underline{U_t^{k+1}}$

$$U_t^{k+1} \rightarrow Re^{k+1} \rightarrow C_D^{k+1} \rightarrow U_t^{k+2}$$

till  $\left| \frac{U_t^{k+1} - U_t^k}{U_t^{k+1}} \right| < \text{tol}$

tol =  $10^{-3}$