

Overview of classical control

Minseok Kim and Hiro Farre

Tue, Feb 18th, 2025

ML Tokamak subgroup meeting

Linear Time-Invariant System

- Linear system



Linear combination of input will result in linear combination of output.



$$y(t) = \int_0^t u(\tau) \underbrace{h(t - \tau)}_{\text{Impulse response}} d\tau$$

Sum of impulses by superposition.

Transfer function

Laplace transform

$$y(t) = \int_0^t u(\tau)h(t - \tau)d\tau \quad \Rightarrow \quad Y(s) = H(s)U(s)$$

$$H(s) = \frac{Y(s)}{U(s)} \quad : \text{Transfer function}$$

Transfer function can be obtained from system dynamics.

Transfer function

Laplace transform

$$T \frac{dy}{dt} + y = Ku(t) \quad \Rightarrow \quad sTY(s) + Y(s) = KU(s)$$

$$H(s) = \frac{Y(s)}{U(s)} = \frac{K}{sT + 1}$$

First-order model

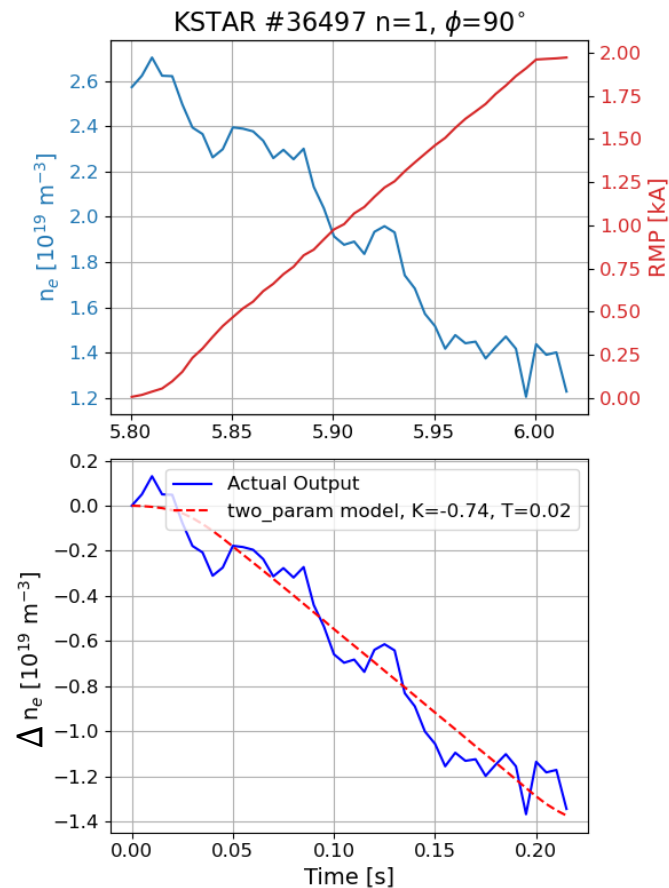
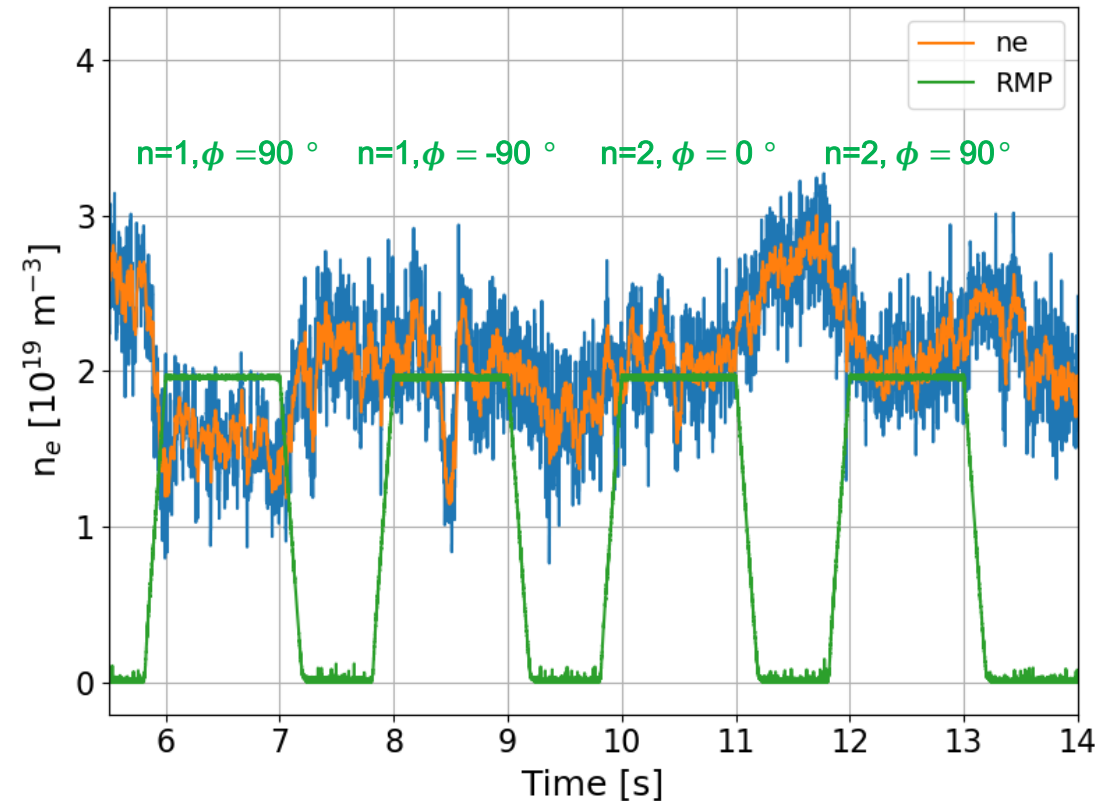
$$sT + 1 = 0 \Rightarrow s = -\frac{1}{T}$$

Pole of the plant

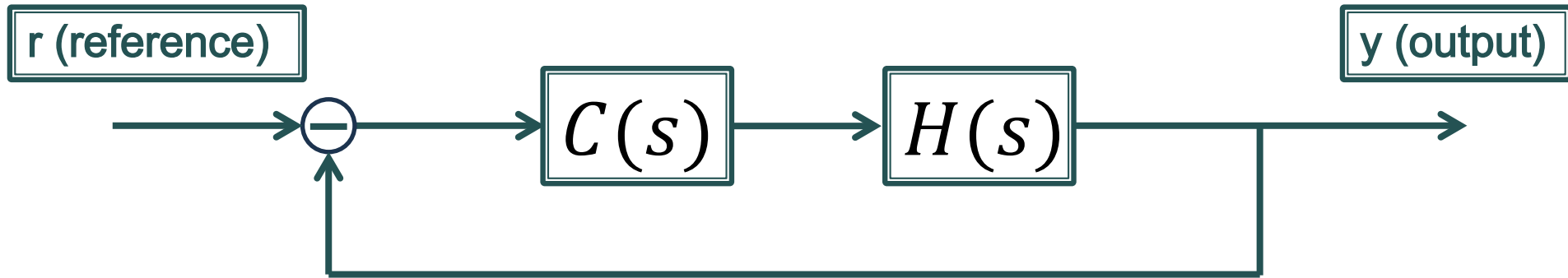
System Identification

4/10

KSTAR @36497



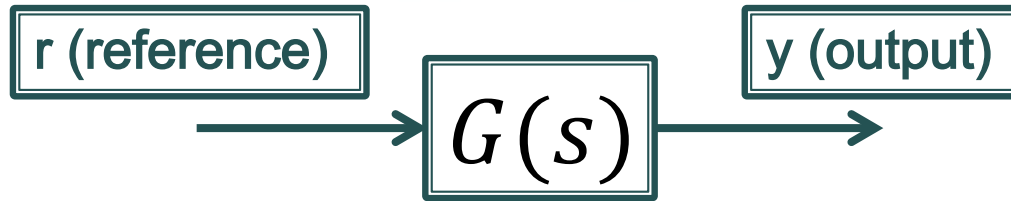
Controller design



$$C(s) = K_p + K_i \frac{1}{s} \quad \Rightarrow \quad Y(s) = \frac{HC}{1 + HC} R(s)$$

$G(s)$:
Closed-loop
transfer function

Controller design



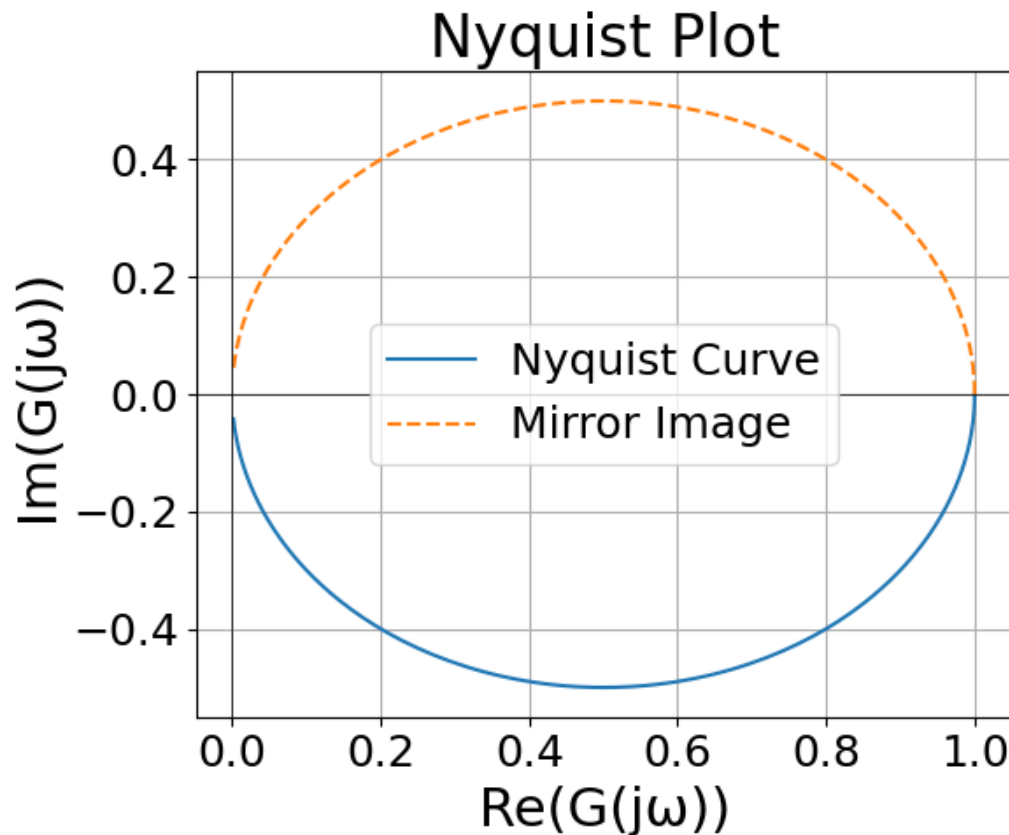
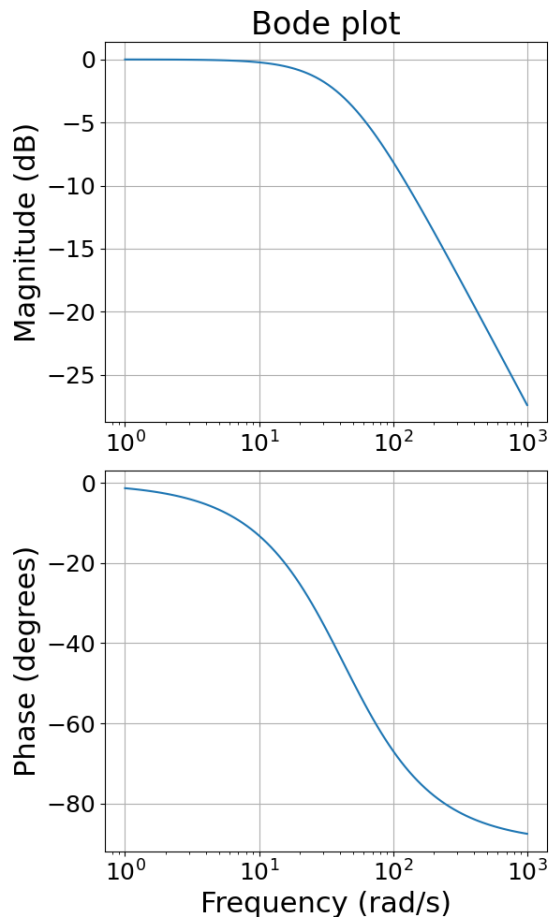
$$G(s) = \frac{K/T(K_p s + K_I)}{s^2 + [(K \cdot K_p + 1)/T]s + K \cdot K_I/T}$$



Place the closed-loop pole to be the same value with the plant

$$K_p = \frac{1}{K} \text{ and } K_I = \frac{1}{KT}$$

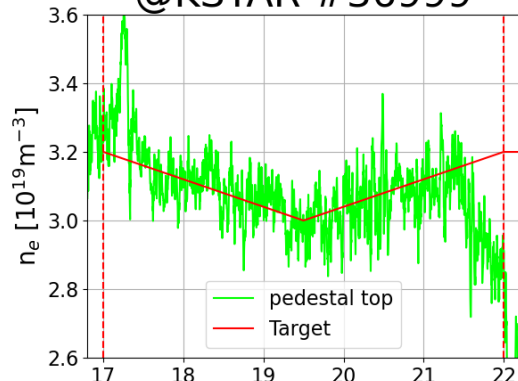
Bode and Nyquist plot



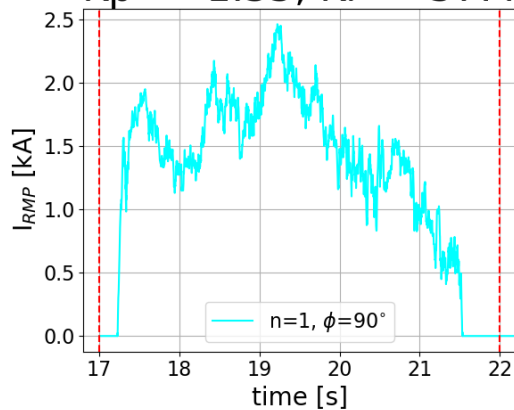
Experimental results

No PVD

@KSTAR #36999

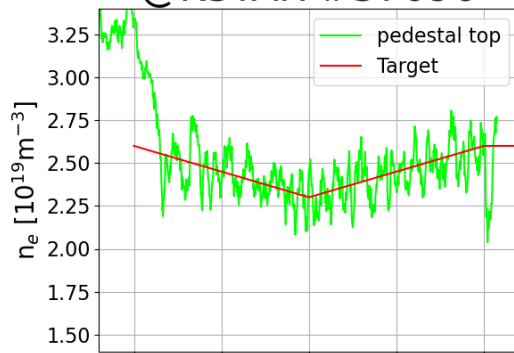


$K_p = -1.35, K_i = -57.4$

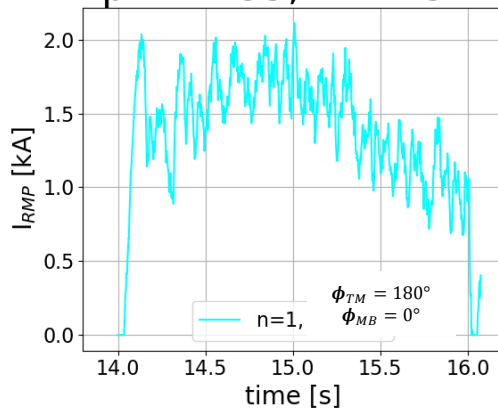


PVD D2 0.3V

@KSTAR #37096

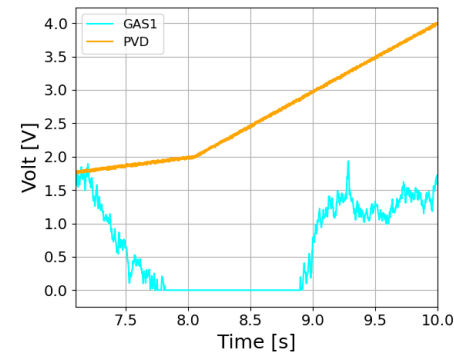
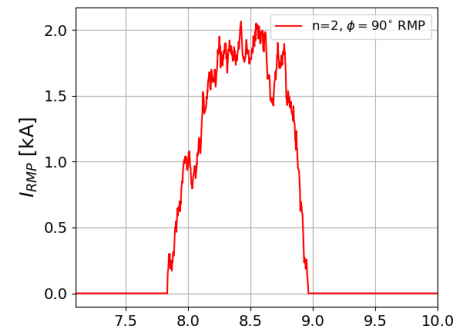
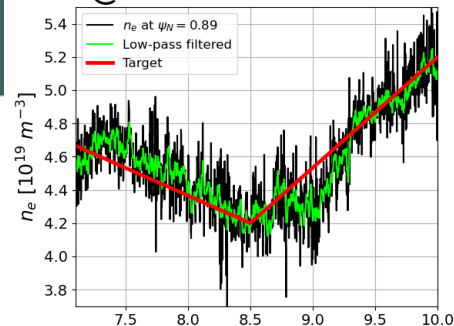


$K_p = -1.35, K_i = -57.4$



@KSTAR #37650

8/10



Modern control

Classical	Modern
Transfer functions	State space
$Y(s) = G(s) \cdot U(s)$	$\dot{\mathbf{x}} = \mathbf{A}\mathbf{x} + \mathbf{B}\mathbf{u}$
	$\mathbf{y} = \mathbf{C}\mathbf{x} + \mathbf{D}\mathbf{u}$
Frequency domain	Time domain
Bode, Nyquist plots	Controllability, observability
PID controllers	State feedback, observers
Manual tuning of gains	Systematic methods, optimal control

Table 5.1: Differences between classical and modern control tools.

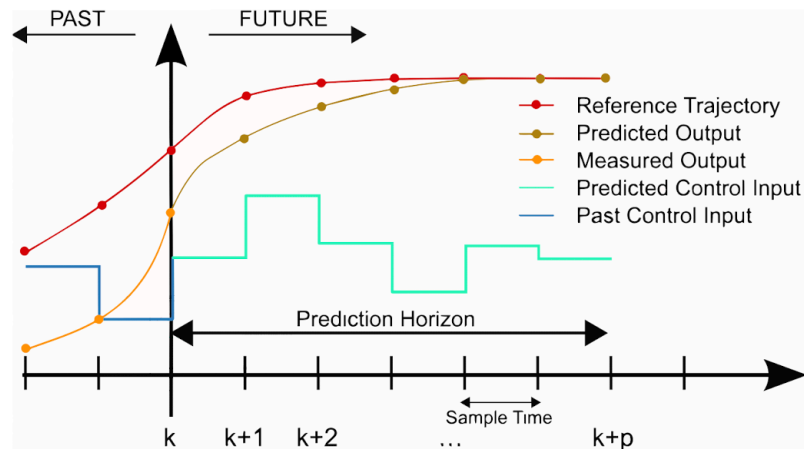
Model Predictive Control

- Use a model to forecast a t (prediction horizon) timesteps
- Calculate the actuation trajectory t timesteps in future to minimize cost (error) given actuation limits
- Grab only 1st actuation and send command
- Problem can be solved with QP solver in real time for small models
- Attempted for TCV shape ctrl, but preliminary

$$x_{t+1} = Ax_t + Bu_t$$

$$Cost = \sum_t (x_{target} - x_t)^T Q (x_{target} - x_t) + u_t^T R u_t$$

$$u_{min} < u_t < u_{max} \quad -\infty < z_t < \infty$$



Appendix

Response to sinusoidal inputs

We can use the solution (2.6) to verify the claim we made in Section 2.1, in particular that for a linear system, the response to a sinusoidal input is sinusoidal. We will consider more generally the complex exponential input

$$u(t) = e^{st}, \quad s \in \mathbb{C},$$

recognizing that sinusoidal inputs are a special case of this, for $s = i\omega$ (as explained in Section 2.1, page 28). From (2.6), the response is then

$$\begin{aligned} y(t) &= \int_0^\infty h(\tau) e^{s(t-\tau)} d\tau \\ &= e^{st} \int_0^\infty e^{-s\tau} h(\tau) d\tau \\ &= e^{st} H(s), \end{aligned}$$

where $H(s)$ is a complex number defined by

$$H(s) = \int_0^\infty e^{-s\tau} h(\tau) d\tau. \quad (2.7)$$

This function $H(s)$ is thus the transfer function, as defined in Definition 2.3.