



INDIAN INSTITUTE OF TECHNOLOGY BOMBAY

AE 593 - DUAL DEGREE PROJECT I

A Comparative Study of Turbulence Modelling for Smoothed Particle Hydrodynamics

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DEPARTMENT OF AEROSPACE ENGINEERING

Indian Institute of Technology Bombay

Abstract

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by K T Prajwal Prathiksh

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Keywords: Fluid Mechanics, Turbulence Modelling, Smoothed Particle Hydrodynamics, Reynolds Averaging, Large Eddy Simulation, Lagrangian Averaging

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List of Symbols

Symbol	Description
\mathbf{a}	Vector Field
$\underline{\underline{\mathbf{A}}}$	Second-rank Tensor Field
$\hat{\mathbf{e}}_i$	i^{th} Basis
$\frac{D(\)}{Dt}$	Lagrangian Derivative
$\langle \underline{\underline{\mathbf{A}}}, \underline{\underline{\mathbf{B}}} \rangle_F$	Frobenius Inner Product of $\underline{\underline{\mathbf{A}}}$ and $\underline{\underline{\mathbf{B}}}$
$\ \underline{\underline{\mathbf{A}}}\ _F$	Frobenius Norm of $\underline{\underline{\mathbf{A}}}$ ($= \sqrt{\langle \underline{\underline{\mathbf{A}}}, \underline{\underline{\mathbf{A}}} \rangle_F}$)
$\Delta(\)$	Component-wise Laplacian Operator
$(1 - \alpha^2 \Delta)$	Helmholtz Operator
i	Reference Particle
j	Neighboring Particle
$(\dots)_i$	Property of i^{th} SPH particle
$(\dots)_j$	Property of j^{th} SPH particle
$(\dots)_{ij}$	$(\dots)_i - (\dots)_j$
t	Time
\mathbf{r}	Position
\mathbf{v}	Velocity
m	Mass
P	Pressure
ρ	Density
Δt	Time Step
Δx	Inter Particle Spacing
W_h	SPH Interpolating Kernel
h	Kernel Smoothing Length

Table 1 continued from previous page

Symbol	Description
$W_{h,ij}$	$W(\mathbf{r}_{ij}, h)$
$\nabla_i W_{h,ij}$	$\nabla_i W(\mathbf{r}_{ij}, h) = \frac{\mathbf{r}_{ij}}{ \mathbf{r}_{ij} } \frac{\partial W_{h,ij}}{\partial r_i}$
\mathcal{V}_i	Volume of i^{th} SPH particle
φ_i	Particle Density of i^{th} SPH particle
\mathbf{F}	External Body Force
ν	Kinematic Viscosity
η	Dynamic Viscosity ($= \nu\rho$)
ξ	Machine Epsilon
M_0	Reference Mass
P_0	Reference Pressure
ρ_0	Reference Density
c_s	Speed of Sound
γ	Exponent - Equation of State
$\boldsymbol{\omega}$	Vorticity ($= \nabla \times \mathbf{v}$)
ν_t	Turbulent Eddy Viscosity
$\underline{\underline{S}}$	Strain-Rate Tensor ($= [1/2][\nabla \mathbf{v} + \nabla \mathbf{v}^T]$)
$\underline{\underline{R}}$	Rate of Rotation Tensor ($= [1/2][\nabla \mathbf{v} - \nabla \mathbf{v}^T]$)
ϵ	Turbulent Dissipation Rate
k	Turbulent Kinetic Energy
$\underline{\underline{\tau}}$	Stress Tensor
C_s	Smagorinsky Constant
u_{max}	Maximum Particle Velocity
ϵ	Smoothing Parameter (XSPH)

Chapter 1

Introduction

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1.1 Project Motivation

1.2 Research Aims & Objectives

1.3 Report Structure

Chapter 2

Turbulence Modelling

2.1 Viscosity-Based Models

Violeau et al. (VIOLEAU, PICCON, and CHABARD 2002) were amongst the early pioneers who tried to incorporate a turbulence model in SPH. They came up with two techniques to tackle the problem of turbulence in a Lagrangian framework, which so far had been neglected till then in research, namely, the eddy viscosity model and a generalised Langevin model. For each of their techniques, they considered the following equation of state 2.1, continuity equation 2.2 and momentum equation 2.3, based on the work of (J. J. Monaghan 1992):

$$P_i = B \left[\left(\frac{\rho_i}{\rho_0} \right)^\gamma - 1 \right], B = \frac{\rho_0 c_s^2}{\gamma} \quad (2.1)$$

$$\frac{D\rho_i}{Dt} = \sum_j m_j \mathbf{v}_{ij} \cdot \nabla_i W_{h,ij} \quad (2.2)$$

$$\frac{D\mathbf{v}_i}{Dt} = - \sum_j m_j \left(\frac{P_i}{\rho_i^2} + \frac{P_j}{\rho_j^2} + \Pi_{ij} \right) \nabla_i W_{h,ij} + \mathbf{F}_i \quad (2.3)$$

Where the viscous term is defined as:

$$\Pi_{ij} = - \frac{16\nu}{\rho_i + \rho_j} \frac{\mathbf{v}_{ij} \cdot \mathbf{r}_{ij}}{|\mathbf{r}_{ij}|^2 + \xi^2} \quad (2.4)$$

2.1.1 Eddy Viscosity Model

The eddy viscosity model was devised as a first-order closure model, which consisted of a relationship between the Reynolds stress tensor and the mean velocity gradients. Therefore, the momentum equation is similar to the momentum equation, except that the kinematic viscosity is replaced by the eddy viscosity (ν_t), and the velocities are Reynolds-averaged. In the SPH formalism, the diffusion term occurring is therefore defined as given in 2.5, with the eddy viscosity defined according to 2.6.

$$\tilde{\Pi}_{ij} = -8 \frac{\nu_{t,i} + \nu_{t,j}}{\rho_i + \rho_j} \frac{\langle \mathbf{v} \rangle_{ij} \cdot \mathbf{r}_{ij}}{|\mathbf{r}_{ij}|^2 + \xi^2} \quad (2.5)$$

$$\nu_t = L_m^2 ||\underline{\underline{\mathbf{S}}}||_F = L_m^2 \sqrt{\langle \underline{\underline{\mathbf{S}}}, \underline{\underline{\mathbf{S}}} \rangle_F} \quad (2.6)$$

Where $\langle \mathbf{v} \rangle$ is Reynolds-averaged velocity, and L_m refers to the mixing length scales. The SPH formulation for the mean velocity gradients are given in 2.7.

$$\nabla \langle \mathbf{v} \rangle_i = -\frac{1}{\rho_i} \sum_j m_j \langle \mathbf{v} \rangle_{ij} \otimes \nabla_i W_{h,ij} \quad (2.7)$$

On simulating Poiseuille flow for a high Reynolds number case, the authors could show that the velocity profile showed only a slight discrepancy with theory, with the expected log-law profile near the walls 2.1. This indicated that the model is appropriate for turbulent mixing problems or for cases involving spatially-varying viscosity while restricted to shear flows.

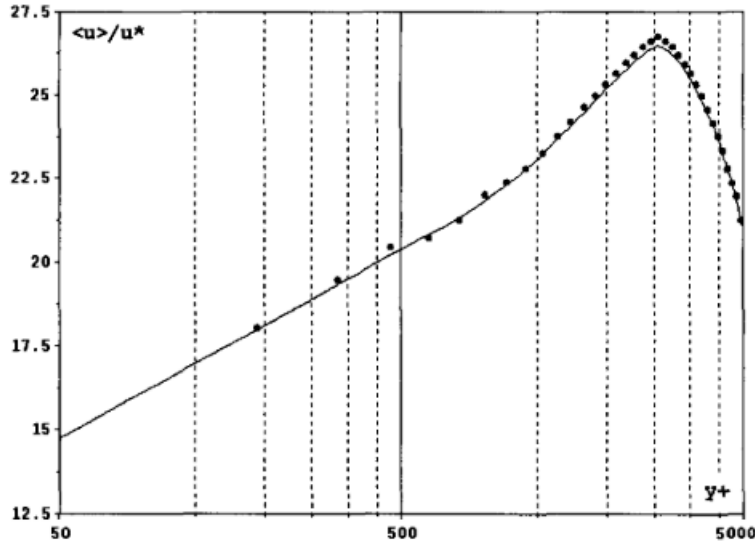


FIGURE 2.1: Turbulent Poiseuille flow in a pipe ($Re = 64e3$) modelled using the eddy viscosity model. Computed mean velocity profiles after ($t = 1s$) (solid circles), against theory (solid line). Ref: (VIOLEAU, PICCON, and CHABARD 2002)

2.1.2 Generalized Langevin Model

Violeau et al. also considered a stochastic approach, where the main idea is built on the concept of prescribing particle velocities as a random process, with properties fulfilling the theoretical turbulence hypotheses (S. Pope 1994). Hence, came about the Generalised Langevin model (GLM), where the particle acceleration is defined as:

$$d\mathbf{v} = -\frac{1}{\rho} \nabla \langle P \rangle + \underline{\underline{G}}(\mathbf{v} - \langle \mathbf{v} \rangle)dt + \sqrt{C_0 \epsilon} d\mathbf{\zeta}, \quad (2.8)$$

Where $\mathbf{\zeta}$ is a random vector statistically non-correlated with velocities. The closure for this model was defined by specifying $\underline{\underline{G}}$ as:

$$\underline{\underline{G}} = \frac{1}{2} C_1 \frac{\epsilon}{k} \underline{\underline{I}} + C_2 \nabla \langle \mathbf{v} \rangle \quad (2.9)$$

Where (k) is the turbulent kinetic energy, (ϵ) the dissipation rate, and (C_i) being constants - ($C_1 = 1.8, C_2 = 0.6$). By modelling turbulence as GLM in SPH, the

momentum equation derived was given by:

$$\frac{D\mathbf{v}_i}{Dt} = -\sum_j m_j \left(\frac{\langle P \rangle_i}{\rho_i^2} + \frac{\langle P \rangle_j}{\rho_j^2} \right) \nabla_i W_{h,ij} - \frac{1}{2} C_1 \frac{\epsilon_i}{k_i} \mathbf{v}'_i + C_2 \nabla \langle \mathbf{v} \rangle_i \cdot \mathbf{v}'_i + \sqrt{\frac{C_0 \epsilon_i}{\delta t}} \bar{\xi}_i \quad (2.10)$$

$$\langle \mathbf{v} \rangle = \sum_j \frac{m_j}{\rho_j} \mathbf{u}_j W_h(\mathbf{r}_j) \quad (2.11)$$

Where the fluctuations are defined as $\mathbf{v}' = \mathbf{v} - \langle \mathbf{v} \rangle$, and the local values of turbulent kinetic energy and dissipation rate are:

$$\epsilon_i = 2\nu_{t,i} + \|\underline{\mathbf{S}}_i\|_F^2 \quad (2.12)$$

$$k_i = \frac{\epsilon_i \nu_{t,i}}{C_\mu}, C_\mu = 0.009 \quad (2.13)$$

It is to be noted that the authors did not estimate the dissipation rate through the proper velocity gradients since the fluctuations of random velocities do not reproduce the small eddies. The same test case as mentioned in 2.1.1 was considered for the performance of GLM. The authors observed large fluctuations. They attributed the discrepancy to the mean operator being redefined as given by 2.11 instead of being a Reynolds average. In fact, by redefining the mean operator in such a fashion, they appeared to have constructed a rudimentary LES filter. As observed in 2.2, the fluctuations have an order of magnitude of $k^{1/2}$. However, as claimed by the authors, unlike the eddy viscosity model, the GLM method can be used for different flows instead of being restricted to only shear flows.

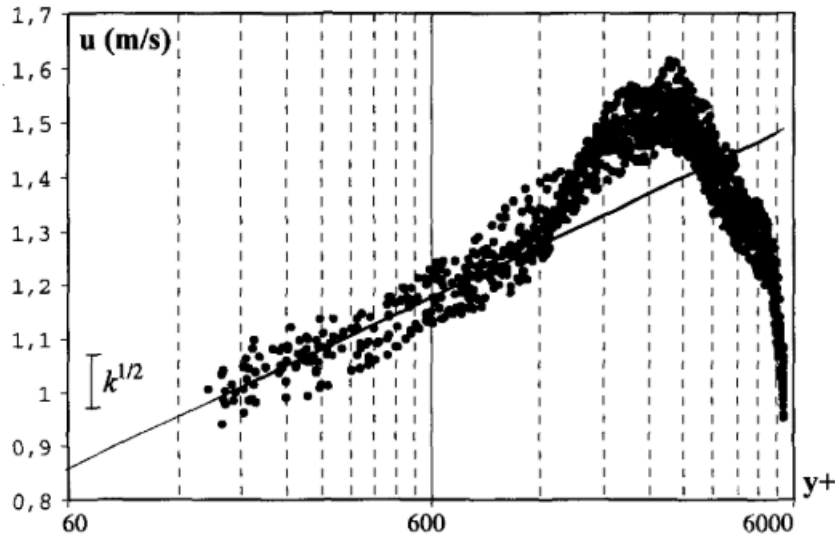


FIGURE 2.2: Turbulent Poiseuille flow in a pipe ($Re = 64e3$) modelled using the generalised Langevin model. Computed mean velocity profiles after ($t = 1s$) (solid circles), against theory (solid line).

Ref: (VIOLEAU, PICCON, and CHABARD 2002)

2.2 mSPH

Adami et al. (Adami, X. Y. Hu, and N. A. Adams 2012) devised a model built on their observation of SPH simulations, wherein the absence of viscosity in typical SPH formulations produced purely noisy particle motion. At finite viscosities, the method would over-predict dissipation. Hence to counter this, they essentially "modified" (hence the name: Modified SPH [mSPH]) the momentum equation and the equation of state to advect the particles in order to homogenise the particle distribution, in turn stabilising the numerical scheme. They were also able to reduce the artificial dissipation in transitional flows.

The authors considered summation density (2.15), which is a function of the volume of the respective SPH particle as given by 2.14, as opposed to evolving density through the continuity equation (Xiang Yu Hu and Nikolaus A Adams 2006). The modified equation of state as given by 2.16, is equivalent to the classical SPH equation-of-state with $\gamma = 1$.

$$\mathcal{V}_i = \frac{1}{\sum_j W_{h,ij}} \quad (2.14)$$

$$\rho_i = \frac{m_i}{\mathcal{V}_i} = m_i \sum_j W_{h,ij} \quad (2.15)$$

$$P_i = c_s^2(\rho_i - \rho_0) \quad (2.16)$$

The momentum equation, which provides the acceleration of the particle, is a function of just the gradient and viscous shear forces as given by 2.17. The corresponding SPH formulation was derived as given by 2.18, which built on the earlier work of Hu and Adams (X. Hu and Nikolaus A Adams 2007).

$$\frac{D\mathbf{v}}{Dt} = -\frac{1}{\rho}\nabla P + \nu\Delta(\mathbf{v}) + \mathbf{F} \quad (2.17)$$

$$\frac{D\mathbf{v}_i}{Dt} = -\frac{1}{m_i} \sum_j (\mathcal{V}_i^2 + \mathcal{V}_j^2) \frac{P_i\rho_j + P_j\rho_i}{\rho_i + \rho_j} \nabla_i W_{h,ij} - \frac{\eta}{m_i} \sum_j (\mathcal{V}_i^2 + \mathcal{V}_j^2) \frac{\mathbf{v}_{ij}}{|\mathbf{r}_{ij}|} \nabla_i W_{h,ij} + \mathbf{F}_i \quad (2.18)$$

This scheme takes advantage of the regularisation of the particle motion stemming from the additional background pressure ($P_0 = \rho_0 c_s^2$). The additional force exerted by the background pressure counteracts non-homogeneous particle distributions, therein reducing numerical dissipation.

The authors estimated the energy spectra of the flow simulations in order to analyse the results of their test cases, using first and second-order moving-least-squares (MLS) method (GOSSLER 2001) and its subsequent Fourier transform (Frigo and Johnson 2005). Their first test case, the 2D variant of the Taylor-Green Vortex (TGV) problem, involved 8×8 counter-rotating vortices, requiring 64^2 particles. They considered the viscosity to be zero. As seen in the time evolution of the

The time evolution of the velocity field is given in 2.3, where it can be observed that the 2D turbulence is characterised by merging and pairing of small vortices. The energy spectra given in 2.4 show that at low wave numbers, both interpolation schemes give the same results, but at high wave numbers, the results differ. The energy spectrum of the standard SPH has a linear slope of magnitude $m = 1$ in a log-log scale equivalent to a purely noisy velocity field. Theoretically, however, 2D turbulence has an energy cascade with a slope of $m = -3$ in the inertial range, which is reasonably predicted using mSPH.

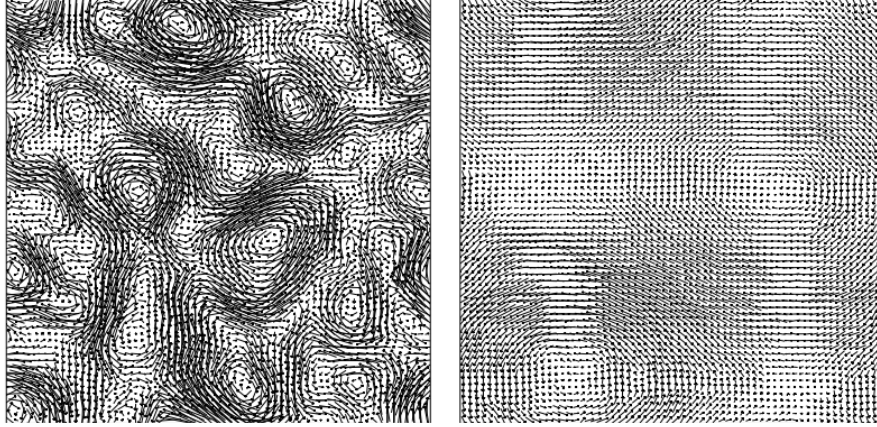


FIGURE 2.3: Velocity vector plot at $t = 2$ (left) and $t = 30$ (right).
 $Re = \infty$. Ref: (Adami, X. Y. Hu, and N. A. Adams 2012)

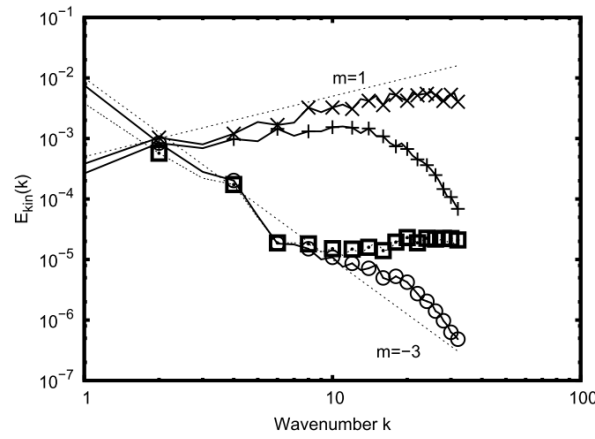


FIGURE 2.4: Comparison of energy spectra $t = 10$. + and \times denote standard SPH results with quintic spline and MLS interpolation; \circ and \square denote mSPH results with quintic spline and MLS interpolation. Ref: (Adami, X. Y. Hu, and N. A. Adams 2012)

The second test case employed by the authors was that of the 3D TGV problem requiring 64^3 particles for a wide range of Reynolds numbers. The dissipation rate of the flow simulations are shown in 2.5 and 2.6. It can be observed that the standard SPH is unable to simulate transitional flows due to excessive dissipation. In contrast, mSPH can reproduce the dissipation rate reasonably well. This implies that the corrected particle transport velocity is an analogous eddy-viscosity model on scales below the numerical resolution.

2.3 Large Eddy Simulation-based Models

2.3.1 Implicit Pressure Poisson-based Models

Gotoh et al. (Hitoshi Gotoh, Songdong Shao, and Memita 2004) were amongst the first to integrate Large Eddy Simulation techniques with the SPH method. They derived this LES-SPH model, based on incompressible flow, to tackle the problem of reflection and transmission characteristics of regular waves by a partially immersed

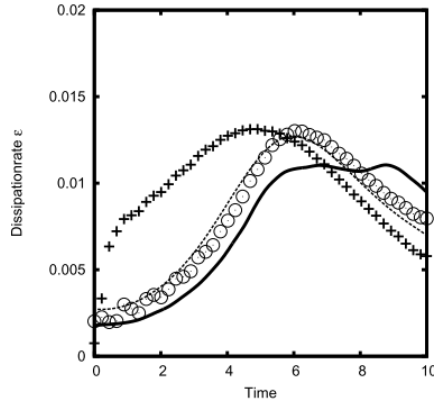


FIGURE 2.5: Dissipation rate at $Re = 400$ using DNS (solid line), Smagorinsky model (dashed line), standard SPH (+) and mSPH (o). Ref: (Adami, X. Y. Hu, and N. A. Adams 2012)

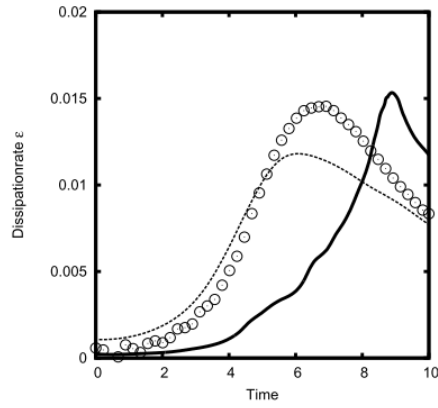


FIGURE 2.6: Dissipation rate at $Re = 3000$ using DNS (solid line), Smagorinsky model (dashed line) and mSPH (o). Ref: (Adami, X. Y. Hu, and N. A. Adams 2012)

curtain-type breakwater. In order to compare the dissipation efficiencies, they considered the non-overtopping and overtopping cases of the problem.

The governing equations of the system were described as given by the continuity equation in 2.19 and the momentum equation in 2.17.

$$\frac{1}{\rho} \frac{D\rho}{Dt} + \nabla \cdot \mathbf{v} = 0 \quad (2.19)$$

The LES mass and momentum conservation equations for the flow were derived by filtering the respective equations using a spatial filter $\overline{(\dots)}$ to obtain their filtered counter-parts as given by 2.20 and 2.21 respectively.

$$\frac{1}{\rho} \frac{D\rho}{Dt} + \nabla \cdot \bar{\mathbf{v}} = 0 \quad (2.20)$$

$$\frac{D\bar{\mathbf{v}}}{Dt} = -\frac{1}{\rho} \nabla \bar{P} + \nu \Delta(\bar{\mathbf{v}}) + \frac{1}{\rho} \nabla \cdot \underline{\underline{\tau}} + \mathbf{F} \quad (2.21)$$

$$\frac{1}{\rho} \underline{\underline{\tau}} = \bar{\mathbf{v}} \otimes \bar{\mathbf{v}} - \overline{\mathbf{v} \otimes \mathbf{v}} \quad (2.22)$$

The stress tensor defined in 2.22 is closed using Boussinesq's Hypothesis as defined in 2.23.

$$\frac{1}{\rho} \underline{\underline{\tau}} = 2\nu_t \underline{\underline{S}} - \frac{2}{3} k \underline{\underline{I}} \quad (2.23)$$

The turbulent eddy viscosity is estimated using a modified Smagorinsky model as given in 2.24. This allows wall effects to be incorporated into the model, which the authors required to tackle the problem they were working on.

$$\nu_t = \min(C_s \Delta x, \kappa d_{wall})^2 \sqrt{2 \langle \underline{\underline{S}}, \underline{\underline{S}} \rangle_F} \quad (2.24)$$

$$C_s = 0.1, \kappa = 0.4 \quad (2.25)$$

Where (C_s) is the Smagorinsky constant, (κ) is the von Karman constant and d_{wall} is the normal distance of the particle to the closest wall. The first term in 2.24 dominates the flow far away from the solid wall, thereby recovering the standard Smagorinsky model. However, the second term dominates for flow close to the wall; hence, the eddy viscosity is a function of the particle distance to the wall. This overcomes the disadvantage of the standard Smagorinsky being over-dissipative inside the laminar layer.

In order to solve the system of equations and evolve them in time, the authors employed the Predictive-Corrective time integrator, similar to the two-step projection method of Chorin (Chorin 1968). The prediction stage is outlined by 2.26 - 2.28.

$$\Delta \mathbf{v}_* = \left(\nu \Delta(\bar{\mathbf{v}}) + \frac{1}{\rho} \nabla \cdot \underline{\underline{\tau}} + \mathbf{F} \right) \Delta t \quad (2.26)$$

$$\mathbf{v}_* = \mathbf{v}_t + \Delta \mathbf{v}_* \quad (2.27)$$

$$\mathbf{r}_* = \mathbf{r}_t + \mathbf{v}_* \Delta t \quad (2.28)$$

The correction stage is outlined by 2.29 - 2.32. (\bar{P}) which is required to update the (\mathbf{v}_{t+1}) term is calculated implicitly from 2.30, which is based on the filtered continuity equation given by 2.20 and assuming incompressibility $\frac{D\rho}{Dt} = 0$.

$$\Delta \mathbf{v}_{**} = -\frac{1}{\rho} \nabla \bar{P}_{t+1} \Delta t \quad (2.29)$$

$$\nabla \cdot \left(\frac{1}{\rho_*} \nabla \bar{P}_{t+1} \right) = \frac{\rho_0 - \rho_*}{\rho_0 \Delta t^2} \quad (2.30)$$

$$\mathbf{v}_{t+1} = \mathbf{v}_* + \Delta \mathbf{v}_{**} \quad (2.31)$$

$$\mathbf{r}_{t+1} = \mathbf{r}_t + (\mathbf{v}_t + \mathbf{v}_{t+1}) \frac{\Delta t}{2} \quad (2.32)$$

In order to solve the system of equations given by 2.26 - 2.32 in an SPH setting, the authors presented the following SPH formulation for the flow property. *Note:* The over-line ($\overline{\dots}$) convention used to denote filtered flow properties will be dropped in this sub-section unless stated otherwise.

The fluid density is given using a simple summation density 2.33.

$$\rho_i = \sum_j m_j W_{h,ij} \quad (2.33)$$

The pressure gradient term is defined in 2.34 in a symmetric form.

$$\left(\frac{1}{\rho}\nabla P\right)_i = \sum_j m_j \left(\frac{P_i}{\rho_i^2} + \frac{P_j}{\rho_j^2}\right) \nabla_i W_{h,ij} \quad (2.34)$$

The divergence of \mathbf{v} is also defined symmetrically as given by 2.35.

$$\nabla \cdot \mathbf{v}_i = \rho_i \sum_j m_j \left(\frac{\mathbf{v}_i}{\rho_i^2} + \frac{\mathbf{v}_j}{\rho_j^2}\right) \cdot \nabla_i W_{h,ij} \quad (2.35)$$

The pressure Laplacian, defined in 2.36, is formulated as a hybrid of a standard SPH first derivative with a finite difference approximation for the first derivative to aid particle pressure stability (Cummins and Rudman 1999).

$$\nabla \cdot \left(\frac{1}{\rho}\nabla P\right)_i = \sum_j m_j \frac{8}{(\rho_i + \rho_j)^2} \frac{P_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.36)$$

The divergence of the stress tensor is defined in 2.37.

$$\left(\frac{1}{\rho}\nabla \cdot \underline{\underline{\tau}}\right)_i = \sum_j m_j \left(\frac{1}{\rho_i^2} \underline{\underline{\tau}}_i + \frac{1}{\rho_j^2} \underline{\underline{\tau}}_j\right) \cdot \nabla_i W_{h,ij} \quad (2.37)$$

Finally, the laminar stress term, consisting of the velocity Laplacian term, is defined as given by 2.38.

$$(v\Delta(\mathbf{v}))_i = \sum_j m_j \frac{4(\eta_i + \eta_j)}{(\rho_i + \rho_j)^2} \frac{\mathbf{v}_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.38)$$

The authors used this SPH-LES model to investigate the wave interaction with a partially immersed breakwater and compared the results with experimentally obtained values of a similar setup. Their computational domain was 2D populated by $\approx 12e3$ particles.

As observed in the comparative plots given in 2.7, the model proves to be accurate in tracking free surfaces of large deformation without numerical diffusion. The authors also observed the model's capability to simulate turbulence and eddy vortices realistically near the curtain wall. However, the authors also conclude that a more refined turbulence model will be required for further accuracy in predicting flow involving wave interactions.

Building on the work mentioned above, Shao and Gotoh (Songdong Shao and Hitoshi Gotoh 2005) performed a comparative study of SPH and the Moving Particle Semi-Implicit (MPS) method coupled with an LES model. They also validated these models against experimental data.

The filtered conservation equations which the authors considered were the same as given by 2.20 - 2.23. However, they incorporated the standard Smagorinsky model (Smagorinsky 1963) given by 2.39 as opposed to the modified model 2.24.

$$\nu_t = (C_s \Delta x)^2 \quad (2.39)$$

The authors consider the same predictive-corrective scheme to evolve their system as detailed in 2.26 - 2.32. Similarly, they follow the same SPH formulation outlined in 2.33 - 2.38. They do however, slightly modify the pressure and velocity

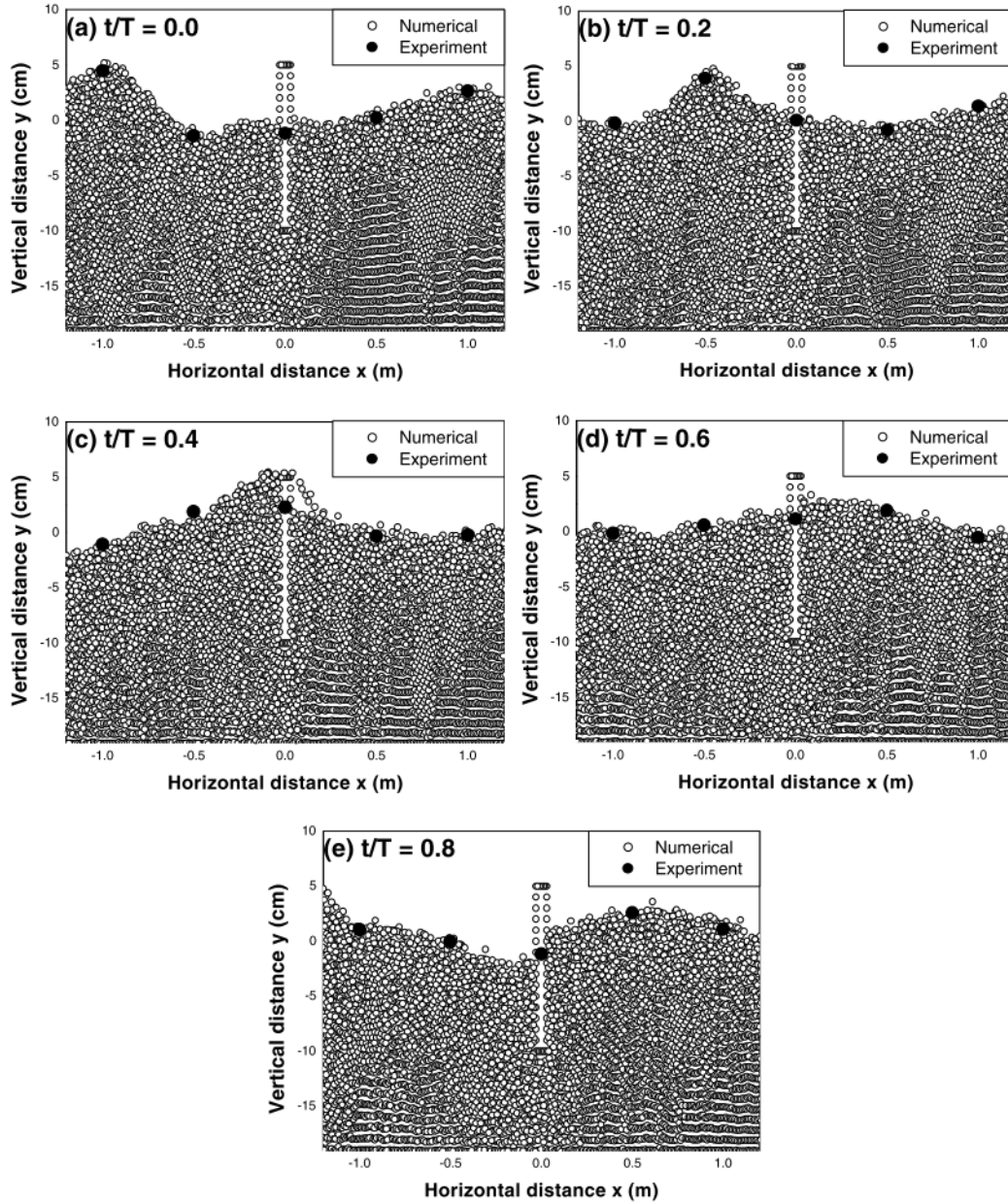


FIGURE 2.7: Time sequences of computational and experimental wave profiles near curtain wall (overtopping). Ref: (Hitoshi Gotoh, Songdong Shao, and Memita 2004)

Laplacian terms as given in 2.40 and 2.41 respectively.

$$(\nabla^2 P)_i = \sum_j m_j \frac{4}{\rho_i + \rho_j} \frac{P_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.40)$$

$$(\nu \Delta(\mathbf{v}))_i = \sum_j m_j \frac{2(\nu_i + \nu_j)}{\rho_i + \rho_j} \frac{\mathbf{v}_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.41)$$

The authors validated this SPH-LES Model using experimental data from the experimental data corresponding to a solitary wave breaking on the beach (Synolakis 1986). Their computational domain was 2D and consisted of $\approx 18e3$ particles. From

the computed wave profiles shown in 2.8, it can be visually observed that there is reasonable agreement between the experimental and computation data. This verifies the model's accuracy in tracking free surfaces with less or no numerical diffusion. Furthermore, by performing a convergence study of the SPH-LES model using the dam-break problem, the authors could show that the scheme's spatial and temporal accuracy is $O(\Delta t + \Delta x^{1.25})$.

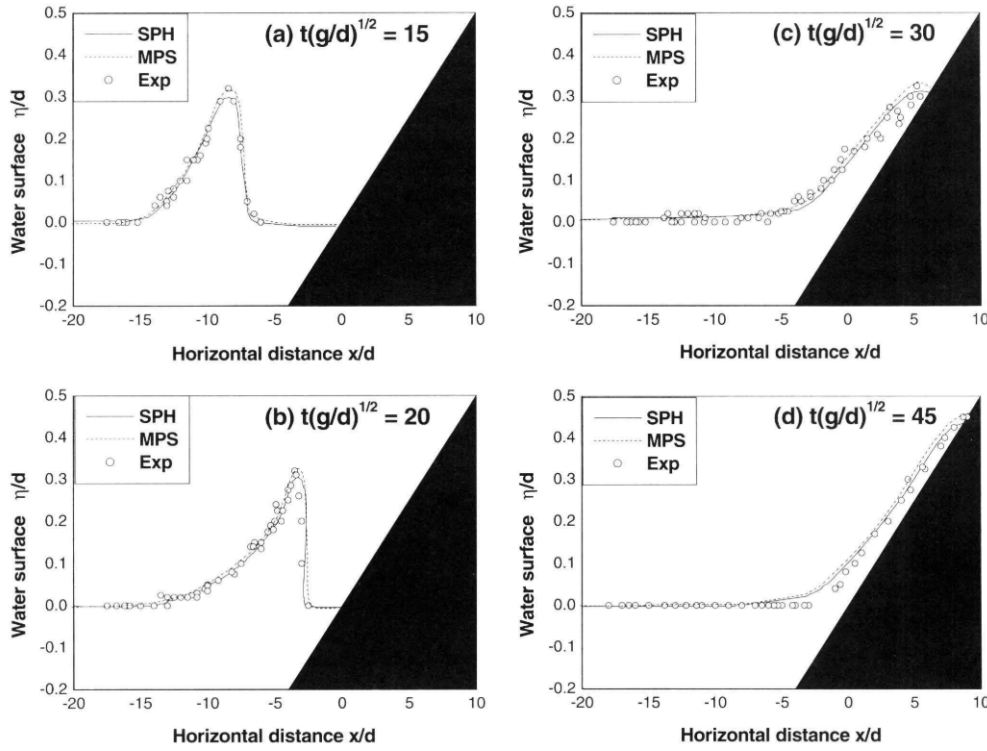


FIGURE 2.8: Experimental and computational wave profiles by SPH and MPS model. Ref: (Songdong Shao and Hitoshi Gotoh 2005)

2.3.2 Explicit Pressure Equation of State-based Solvers

Standard Smagorinsky Model

Rogers and Dalrymple (ROGERS and DALRYMPLE 2005), similar to the work on SPH-LES modelling detailed in 2.3.1, came up with an LES-type sub-particle-scale (SPS) formulation based on the weakly compressible assumption in order to develop a turbulence model for SPH.

The authors considered the mass and momentum conservation equations as already given in 2.19 and 2.17 respectively, along with the equation of state 2.1. However, for the value of (B) in the state equation, the authors considered the definition given in 2.42:

$$B = 10u_{max} \quad (2.42)$$

They subsequently filtered the compressible conservation equations using Favre averaging as given by 2.43.

$$\tilde{f} = \frac{\overline{\rho f}}{\bar{\rho}} \quad (2.43)$$

The derived filtered conservation equations for mass and momentum are detailed in 2.44 and 2.45.

$$\frac{D\bar{\rho}}{Dt} = -\bar{\rho}\nabla \cdot \tilde{\mathbf{v}} \quad (2.44)$$

$$\frac{D\tilde{\mathbf{v}}}{Dt} = -\frac{1}{\bar{\rho}}\nabla\bar{P} + \frac{1}{\bar{\rho}}(\nabla \cdot \bar{\rho}\mathbf{v}\nabla)\tilde{\mathbf{v}} + \frac{1}{\bar{\rho}}\nabla \cdot \underline{\underline{\tau}} + \mathbf{F} \quad (2.45)$$

Where the SPS stress tensor and turbulent eddy viscosity is given by 2.46 and 2.47 respectively.

$$\underline{\underline{\tau}} = \bar{\rho}\left(2\nu_t\underline{\underline{S}} - \frac{2}{3}\text{tr}[\underline{\underline{S}}]\underline{\underline{I}}\right) - \frac{2}{3}\bar{\rho}C_I\bar{\Delta}^2\underline{\underline{I}}, C_I = 6.6e - 4 \quad (2.46)$$

$$\nu_t = (C_s\Delta x)^2\sqrt{2\langle\underline{\underline{S}}, \underline{\underline{S}}\rangle_F}, C_s = 0.12 \quad (2.47)$$

As for the SPH formulations of the aforementioned governing equations, the authors

The authors derived the SPH formulations of the aforementioned governing equations. The continuity equation takes the form as detailed in 2.2. The pressure gradient term is given in 2.34. The laminar stress term, consisting of the velocity Laplacian is given by 2.48, which itself was built on the work of Morris et al. (Morris, Fox, and Zhu 1997) as given in 2.49. Finally the stress divergence is defined by 2.37.

$$\left(\frac{1}{\rho}(\nabla \cdot \eta\nabla)\mathbf{v}\right)_i = \sum_j m_j \frac{\nu(\rho_i + \rho_j)}{\rho_{ij}^2} \frac{\mathbf{v}_{ij}\mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2 + \xi} \quad (2.48)$$

$$\left(\frac{1}{\rho}(\nabla \cdot \eta\nabla)\mathbf{v}\right)_i = \sum_j m_j \frac{(\eta_i + \eta_j)\mathbf{v}_{ij}}{\rho_i\rho_j} \left(\frac{1}{|\mathbf{r}_{ij}|} \frac{\partial W_{h,ij}}{\partial r_i}\right), \nabla_i W_{h,ij} = \frac{\mathbf{r}_{ij}}{|\mathbf{r}_{ij}|} \frac{\partial W_{h,ij}}{\partial r_i} \quad (2.49)$$

The authors noted that the LES description of viscous effects in slightly compressible SPH could lead to unphysical behaviour at free surfaces due to density variations being magnified by the equation of state. The lack of artificial viscosity implies that such variations are not damped. They subsequently noted that averaging the density would ensure smooth and physically acceptable free surfaces, based on the work of Panizzo (Panizzo 2004). Hence, they performed Shepard filtering of the density as defined in 2.50 every 40-time steps.

$$\rho_i = \frac{\sum_j \rho_j W_{h,ij} \mathcal{V}_j}{\sum_j W_{h,ij} \mathcal{V}_j} \quad (2.50)$$

The authors simulated the problem of a weakly plunging breaker in 2D and 3D to ascertain the performance and capability of the model. Their 2D computational domain consisted of $\approx 1e5$ particles, with the 3D domain consisting $\approx 2e4$ particles. The authors could show that in the case of the 2D problem, the model could predict regions of high vorticity that persisted longer when compared to standard SPH utilising conventional artificial viscosity. The model also displayed the turbulent bore, which generated reverse breaking, leading to the downbursting-like phenomenon, as observed in experiments (Kubo and Sunamura 2001). In the case of the 3D problem, the authors showed the model's capability to capture near vertically-oriented eddies despite the lower resolution.

Building on this work, Dalrymple and Rogers (Dalrymple and Rogers 2006) used

this scheme on a wide variety of problems, ranging from 2D Green water overtopping, 2D waves on a beach, 3D dam break and 3D waves on a beach. The quantitative analysis of the results allowed the authors to conclude that the model is especially suited for problems involving splash or flow separation. The authors also warn about the model's requirement of a large number of particles for sufficient resolution. That and the finite speed of sound stemming from the compressible flow implied that time steps had to be $O(10^{-5}s)$. Hence, the authors remain cautiously optimistic about the model since the method performs well for smaller regions where the number of particles is reasonable. However, they believe that extended Boussinesq codes would more efficiently model larger domains.

Modified Smagorinsky Model

Canelas et al. (Canelas et al. 2016) constructed the wall-adapting local eddy viscosity (WALE) model to be incorporated in the SPH-LES scheme. They noted that studying turbulent flow fields required the identification of vortices themselves to study their interactions in the flow. They used the definition of Lagrangian Coherent Structures (LCS) to help capture these vortices. As a Lagrangian method, SPH is preferable for studying LCS since the technique provides the motion of individual fluid particles, thereby eliminating the need for expensive post-processing inherent to Eulerian solutions. However, they noted that typically employed SPS strategies for LES simulations, based on the standard Smagorinsky model, cannot correctly enforce wall conditions and non-vanishing stresses with laminar flows. Hence they devised the WALE model.

The authors consider the compressible Navier-Stokes (NS) along the continuity equation as their governing equation. They subsequently present the SPH formulation of the continuity equation as defined by 2.51.

$$\frac{D\rho_i}{Dt} = -\rho_i \sum_j m_j \mathbf{v}_{ij} \cdot \nabla_i W_{h,ij} \quad (2.51)$$

The pressure gradient term is given in 2.34. The laminar stress term, consisting of the velocity Laplacian, is given by 2.52.

$$(\nu \Delta(\mathbf{v}))_i = \sum_j m_j \frac{4\nu}{\rho_i + \rho_j} \frac{\mathbf{v}_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.52)$$

Finally the stress divergence is defined by 2.37, with the stress tensor being defined by 2.53

$$\underline{\underline{\tau}} = \rho \left(2\nu_t \underline{\underline{S}} - \frac{2\nu_t}{3} \text{tr}[\underline{\underline{S}}] \underline{\underline{I}} \right) - \frac{4}{3} \rho C_I \Delta^2 \underline{\underline{I}} \langle \underline{\underline{S}}, \underline{\underline{S}} \rangle_F, C_I = 6.6e - 3 \quad (2.53)$$

The WALE model redefines the turbulent eddy viscosity as given by 2.54.

$$\nu_t = \rho (C_w \Delta x)^2 \frac{\langle \underline{\underline{S}}^d, \underline{\underline{S}}^d \rangle_F^{3/2}}{\langle \underline{\underline{S}}, \underline{\underline{S}} \rangle_F^{5/2} + \langle \underline{\underline{S}}^d, \underline{\underline{S}}^d \rangle_F^{5/4}}, C_w = 0.325 \quad (2.54)$$

Where

$$\underline{\underline{S}}^d = \frac{1}{2} \left((\nabla \mathbf{v})^2 + ((\nabla \mathbf{v})^T)^2 \right) - \frac{1}{3} \text{tr}[(\nabla \mathbf{v})^2] \underline{\underline{I}} \quad (2.55)$$

In order to test their model, the authors considered an array of cylinders in fluid flow as shown in 2.9, with a constant body force. They computed the vorticity field and the Finite-Time Lyapunov Exponents (FTLE) field to study the LCSs in the flow. These fields are shown in 2.10 and 2.11 respectively.

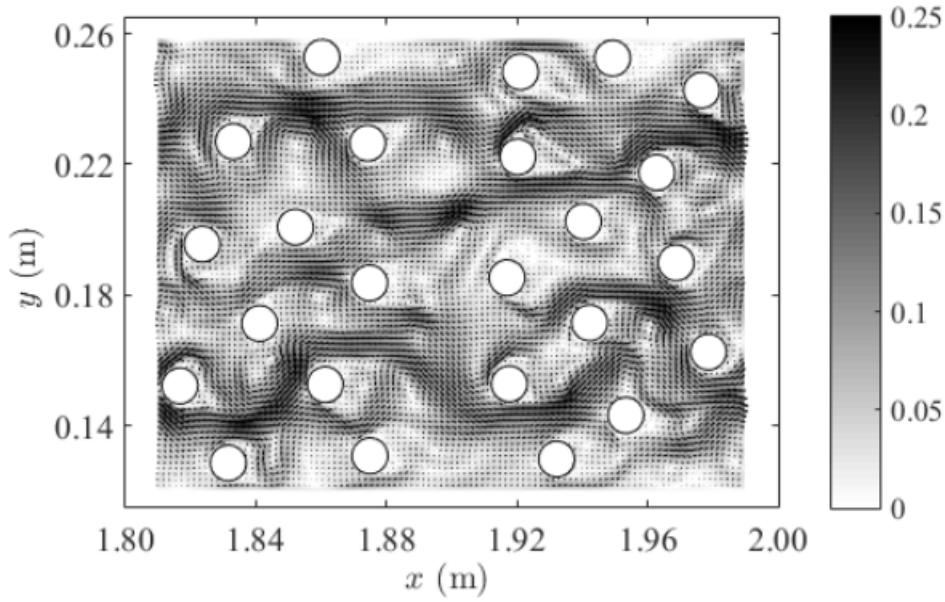


FIGURE 2.9: Cylinder distribution and instantaneous velocity overlapped by velocity vectors. Velocity in m/s , at $t = 20s$. The flow direction is from left to right. Ref: (Canelas et al. 2016)

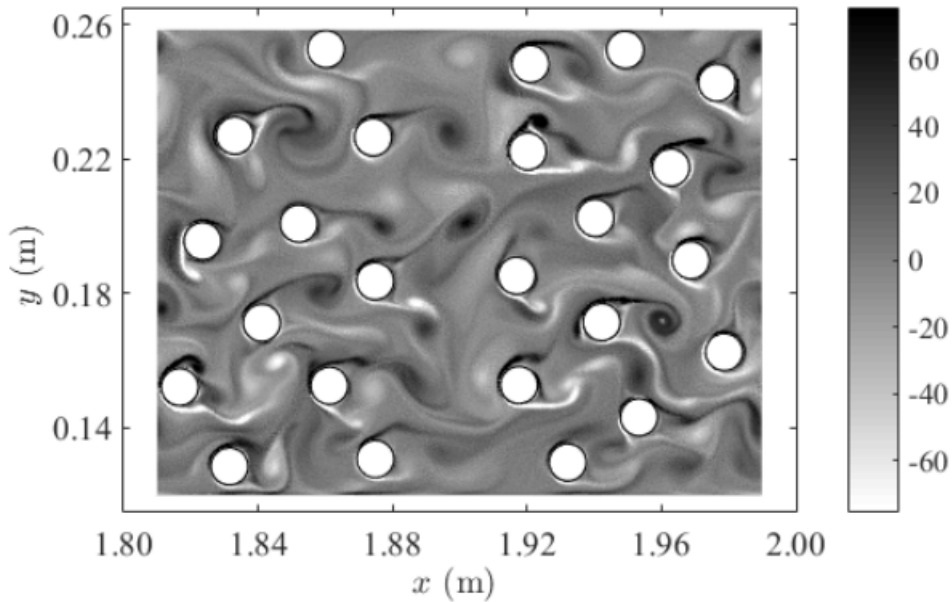


FIGURE 2.10: Vorticity field. Vorticity in Hz , at $t = 20s$. Ref: (Canelas et al. 2016)

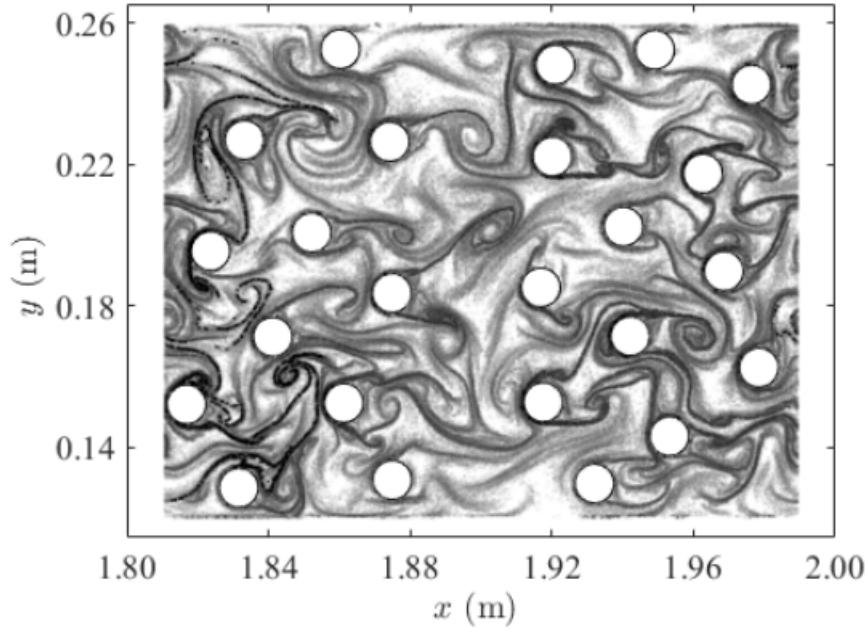


FIGURE 2.11: FTLE field with negative integration time ($T = -0.4s$) (unstable manifolds - attracting LCS) at $t = 20s$. Ref: (Canelas et al. 2016)

2.3.3 Quasi-Lagrangian Models

2.3.4 RANS-based $k - \epsilon$ Models

Shao (Songdong Shao 2006) demonstrated that the two-equation $k - \epsilon$ model, an extensively studied model derived from the Reynolds-averaged Navier–Stokes (RANS) equations, can be incorporated in the truly incompressible version of SPH (ISPH). By attempting to extend RANS equations, which are hugely successful in practical fields, to a mesh-free method such as SPH, the author provides a framework to build on the wide variety of closure models available.

To discretise the RANS equations to an SPH form, the author considers the Reynolds averaged mass and momentum conservation equations as given in 2.56 and 2.57 respectively. *Note:* The averaged flow properties are represented without any over-line ($\overline{\dots}$) hereafter.

$$\frac{1}{\rho} \frac{D\rho}{Dt} + \nabla \cdot \mathbf{v} = 0, \quad \frac{D\rho}{Dt} = 0 \text{ (Incompressible)} \quad (2.56)$$

$$\frac{D\mathbf{v}}{Dt} = -\frac{1}{\rho} \nabla P + \nu \Delta(\mathbf{v}) + \frac{1}{\rho} \nabla \cdot \underline{\underline{\tau}} + \mathbf{F} \quad (2.57)$$

The stress tensor is given by 2.23, while the turbulent eddy viscosity is defined as 2.58.

$$\nu_t = c_d \frac{k^2}{\epsilon} \quad (2.58)$$

The transport equations for the turbulent kinetic energy and dissipation rate is given by 2.59 and 2.60 respectively.

$$\frac{Dk}{Dt} = \nabla \cdot \left(\frac{\nu_t}{\sigma_k} \nabla k \right) + P_k - \epsilon \quad (2.59)$$

$$\frac{D\epsilon}{Dt} = \nabla \cdot \left(\frac{\nu_t}{\sigma_\epsilon} \nabla \epsilon \right) + c_{1\epsilon} \frac{\epsilon}{k} P_k - c_{2\epsilon} \frac{\epsilon^2}{k} \quad (2.60)$$

$$P_k = 2\nu_t \langle \underline{\underline{S}}, \underline{\underline{S}} \rangle_F \quad (2.61)$$

Where, $(\sigma_k, \sigma_\epsilon, c_{1\epsilon}, c_{2\epsilon}) = (1.0, 1.3, 1.44, 1.92)$ are empirical constants dependent on the nature of the flow, and (P_k) is the turbulence production rate, which satisfies the relation given by 2.62 (Stephen B Pope and Stephen B Pope 2000).

$$\frac{P_k}{\epsilon} = c_d \left(\frac{\sqrt{2\langle \underline{\underline{S}}, \underline{\underline{S}} \rangle_F}}{\epsilon} \right) \quad (2.62)$$

These governing equations are solved and evolved using the same predictive-corrective time integrator as seen in the work of (Hitoshi Gotoh, Songdong Shao, and Memita 2004), and outlined in 2.26 - 2.32.

As for the SPH formulations of the governing equations, the author builds on the work of (Hitoshi Gotoh, Songdong Shao, and Memita 2004), and uses the same discretization as defined in 2.33 - 2.37. However, the author uses a slightly modified version of the laminar stress term given in 2.38 and redefines it as given in 2.63.

$$(\nu \Delta(\mathbf{v}))_i = \sum_j m_j \frac{2(\nu_i + \nu_j)}{\rho_i + \rho_j} \frac{\mathbf{v}_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.63)$$

The author tested the model on the problem of 2D wave breaking and overtopping of a sloping wall and compared the results obtained against experimental data (Li, Troch, and De Rouck 2004) to validate the model—the computational domain of $\approx 6e3$ particles.

As seen from the evolution of the water surface elevation plotted in 2.12, the author could ascertain that the proposed model produced better results than those of Li et al. (Li, Troch, and De Rouck 2004), compared to the experimental data in 2.12(a) and 2.12(b). This could be attributed to the free surfaces being accurately tracked by particles without numerical diffusion. In 2.12(c) and 2.12(d), despite the wave profiles being consistent with each other in phase and shape, the proposed model predicts smaller elevation levels. Li et al. use a dynamic Smagorinsky model, whereas the proposed model uses constant empirical coefficients. The author believes these coefficients derived from a quasi-steady state may behave sub-optimally in transient flow, such as the problem at hand.

The author concludes that the $k - \epsilon$ model would require further sensitivity analysis for the turbulence model and spatial resolution for improved results, despite being reasonably accurate in tracking free surfaces.

Wang and Liu (Wang and Liu 2020) build on the work of Shao (Songdong Shao 2006) to further improve the ISPH $k - \epsilon$ model. They achieved this by using the modelling and computational developments which SPH has benefited from since the work of Shao. The authors here consider the same SPH discretised equations and two-step time integrator as Shao, with two distinct modifications in the Pressure Poisson equation as given by 2.64 instead of 2.30. They also redefined propagation equation for (\mathbf{r}) using 2.65 instead of 2.32.

$$\nabla \cdot \left(\frac{1}{\rho_0} \nabla P_{t+1} \right) = \frac{1}{\Delta t} \nabla \cdot \mathbf{u}_* \quad (2.64)$$

$$\mathbf{r}_{t+1} = \mathbf{r}_* + \Delta \mathbf{v}_{**} \Delta t \quad (2.65)$$

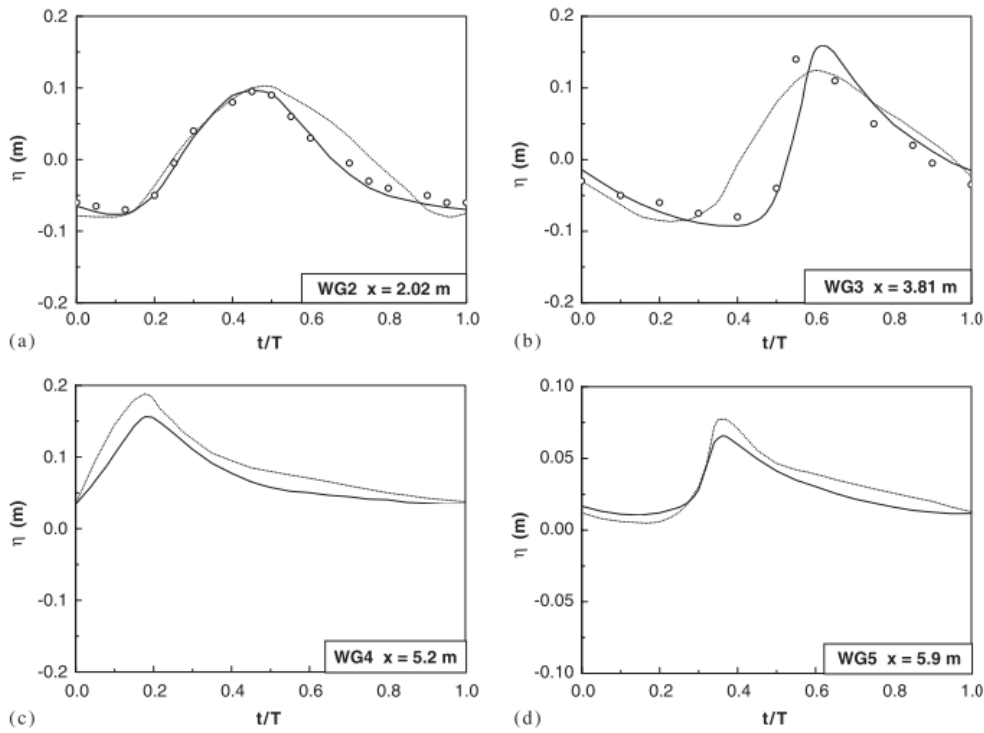


FIGURE 2.12: Comparisons of computed water surface elevations by SPH (solid lines) with experimental (○) and numerical (dotted lines) data of Li et al. (Li, Troch, and De Rouck 2004). Ref: (Songdong Shao 2006)

The authors also provided SPH discretization for the transport equations for (k) and (ϵ) using 2.67 and 2.68 which requires the use of particle density (φ) as given in 2.66.

$$\varphi_i = \sum_j W_{h,ij} \quad (2.66)$$

$$\nabla \cdot \left(\frac{v_t}{\sigma_k} \nabla k \right)_i = - \sum_j \frac{1}{\varphi_j} \left(\frac{v_{t,i}}{\sigma_k} + \frac{v_{t,j}}{\sigma_k} \right) \frac{k_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.67)$$

$$\nabla \cdot \left(\frac{v_t}{\sigma_\epsilon} \nabla \epsilon \right)_i = - \sum_j \frac{1}{\varphi_j} \left(\frac{v_{t,i}}{\sigma_\epsilon} + \frac{v_{t,j}}{\sigma_\epsilon} \right) \frac{\epsilon_{ij} \mathbf{r}_{ij} \cdot \nabla_i W_{h,ij}}{|\mathbf{r}_{ij}|^2} \quad (2.68)$$

The authors also derived an SPH formulation for the strain rate tensor defined in 2.69, which is based on the studies done on kernel correction (Bonet and Lok 1999; Khayyer, Gotoh, and SD Shao 2008) and given by 2.70 and 2.71.

$$\underline{\underline{S}}_i = \frac{1}{2} \left(\nabla \mathbf{v}_i + (\nabla \mathbf{v}_i)^T \right) \quad (2.69)$$

$$\nabla \mathbf{v}_i = - \sum_j \frac{1}{\varphi_j} \mathbf{v}_{ij} \otimes \underline{\underline{L}}_i \cdot \nabla_i W_{h,ij} \quad (2.70)$$

$$\underline{\underline{L}}_i = \left(- \sum_j \frac{1}{\varphi_j} \nabla_i W_{h,ij} \otimes \mathbf{r}_{ij} \right)^{-1} \quad (2.71)$$

The authors validated the model against the problem of a solitary wave propagating over a bottom-mounted barrier in 2D. Its results are shown in 2.13. They also considered the problem involving wave breaking on a slopping wall in 2D, which is shown in 2.14.

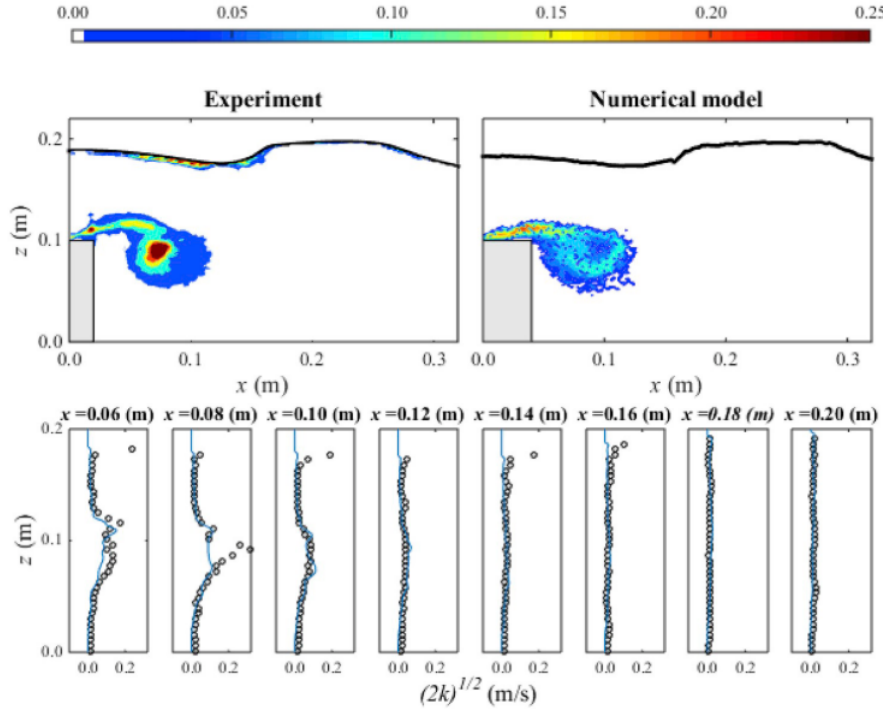


FIGURE 2.13: Comparisons between experimental data (left) and numerical results (right) for turbulence intensity (m/s) at $t = 0.6s$ (top panels) and the corresponding vertical cross-sections (lower panels). In the lower panels, solid lines and \circ represent the numerical and experimental results, respectively. Ref: (Wang and Liu 2020)

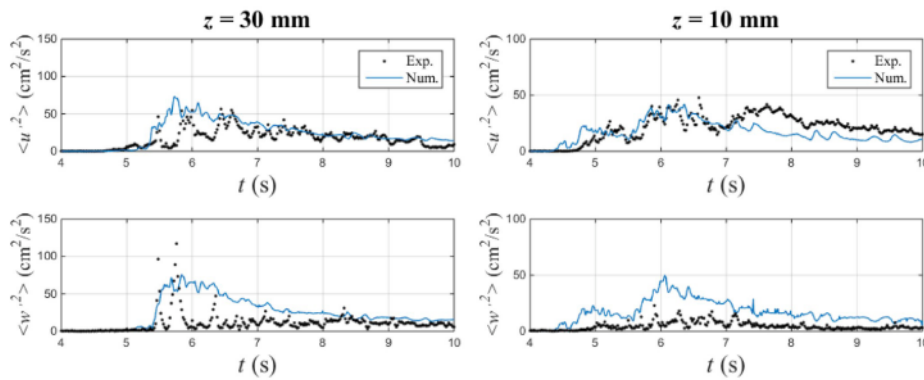


FIGURE 2.14: Comparisons of numerical and experimental turbulent kinetic energy in x-direction and y-direction. Ref: (Wang and Liu 2020)

Given the model's accuracy, as observed from the figures, the authors conclude that the model's capabilities have been demonstrated, especially in tracking transient-free surfaces. They also reproduce the evolution of turbulence and its intensity due

to flow separation. However, they note that the model under-predicts the max turbulent kinetic energy and is sensitive to the initial seeding of the turbulent kinetic energy property. The authors also state that the counteracting effects of the physical viscous dissipation and numerical dissipation, dependent on the particle resolution, would have to be appropriately balanced. Finally, the authors conclude on the importance of boundary treatment and the need for more sophisticated boundary models to extend the model to 3D domains.

2.3.5 LANS-based Models

So far, having dealt with RANS and LES models of turbulence, a few fundamental drawbacks of these techniques have been brought to light. In the case of RANS, the flow field is decomposed into an averaged mean flow and a fluctuating field. Such a decomposition of the NS equations provides differential equations for the mean flow containing contributions from the time-varying turbulent motion. Therefore a closure model is required to capture the effects of the fluctuations on the mean flow. However, by studying only the mean flow quantities, the complete nature of the flow, notwithstanding the complex structures stemming from these fluctuations, cannot be studied, let alone appreciated.

On the face of it, LES would have made for a reasonable alternative to model turbulent flows. This is because the large scales in the flow are resolved by the standard NS equations, while the effects of smaller scales are modelled. However, this remains easier said than done since inhomogeneous and wall-bounded flows necessitate the LES filter width to vary dynamically to capture the average size of turbulent eddies.

The other widespread method of tackling turbulence involves Direct Numerical Simulation (DNS). However, because of the exponentially increasing degrees of freedom as the Reynolds number increases, this technique effectively places an inviolable upper bound on the Re for a given simulation because of computational limitations.

In order to tackle the issues above and address them reasonably, we look for possible solutions. One such solution is the Lagrangian averaging method introduced by Holm et al. (Holm, Jerrold E Marsden, and Ratiu 1998) and Marsden and Shkoller (J. E. Marsden and Shkoller 2001). In this method, unlike the averaging or filtering of the NS equations as done in RANS or LES, the Lagrangian averaging approach averages at the level of the variational principle from which the Navier–Stokes equations are derived. This procedure yields the Lagrangian-averaged Navier Stokes- α (LANS- α) equations, which describe the time evolution of large eddies in turbulent flows. It can be stated that this approach is similar to that of LES.

The LANS- α equations, assuming incompressibility and isotropic turbulence, are derived and simplified by Mohseni et al. (Mohseni et al. 2003). These equations are as follows:

$$\nabla \cdot \mathbf{v} = 0 \quad (2.72)$$

$$\frac{D\mathbf{v}}{Dt} = \underline{\underline{\sigma}}(\mathbf{v}) \quad (2.73)$$

$$\underline{\underline{\sigma}}(\mathbf{v}) = -P\underline{\underline{I}} + 2\nu(1 - \alpha^2\Delta)\underline{\underline{S}} + 2\alpha^2\dot{\underline{\underline{S}}} \quad (2.74)$$

$$\dot{\underline{\underline{S}}} = \frac{D\underline{\underline{S}}}{Dt} + \underline{\underline{SR}} - \underline{\underline{RS}} \quad (2.75)$$

$$\underline{\underline{R}} = \frac{1}{2} \left(\nabla \mathbf{v} - (\nabla \mathbf{v})^T \right) \quad (2.76)$$

Where α denotes the scale of rapid fluctuations in the flow map, wherein, for scales smaller than α , the wave activity is filtered by a nonlinear energy redistribution.

Monaghan (J. J. Monaghan 2002), building on the work of Holm (Holm, Jerrold E Marsden, and Ratiu 1998), attempted to formulate an SPH version of the continuum LANS- α equations. His work provided one of the earliest models of turbulence in compressible flow. The author incorporated some of his earlier work on XSPH (J. Monaghan 1989), in which particles are moved with a smoothed velocity, leaving the acceleration equation unchanged. The smoothed velocity denoted an average over the velocities of the neighbouring particles. This facilitated the author in writing the Lagrangian analysed by Holm in an SPH form, allowing for the subsequent derivation of the momentum equation, albeit being elaborate and highly complicated. Nevertheless, in conjunction with the continuity equation, the derived momentum equation formulated the SPH- α model, which essentially consisted of an SPH particle moving with the transport velocity smoothed from momentum velocity by an iterative algorithm with an additional dissipation term meant to mimic the standard LES model.

Hu and Adams (X. Y. Hu and N. A. Adams 2015) also devised a turbulence model for incompressible flow based on spatial filtering of the NS equations using SPH approximations termed the SPH- σ model. The model shares similarities with the LANS- α model and the SPH- α model, differing by the additional stress term in the model and its approach in evaluating the particle transport velocity. The proposed model is also built on the authors' previous work (X. Hu and Nikolaus A Adams 2007), and hence shares similar numerical techniques. The authors also validated the proposed model on 2D flow comprising decaying and forced turbulence cases. Their results suggested that the model could simulate incompressible turbulent flow.

Monaghan (J. J. Monaghan 2011; J. J. Monaghan 2017) subsequently improved on the SPH- α model and derived a more amenable variant of the momentum equation. Since, in this case, the model was parameterised around the smoothing parameter (ϵ), the turbulence model was termed the SPH- ϵ model. The linearly smoothed velocity is given by 2.77.

$$\hat{\mathbf{v}}_i = \mathbf{v}_i - \epsilon \sum_j \frac{m_j}{M_0} \mathbf{v}_{ij} K_{h',ij}, \epsilon \in [0, 1] \quad (2.77)$$

Where (K) is a smoothing kernel, which can be different from the kernel used in SPH, its corresponding smoothing length being (h'). It is noted that the smoothed velocity preserves the shape of the spectrum of the unsmoothed velocity for short-length scales. However, it reduces the magnitude of the unsmoothed velocity by a factor $(1 - \epsilon)$.

The equation of state is given by 2.1, and the momentum equation is given by 2.78. The momentum equation's third term on the right-hand side is an extra stress term determined by the smoothing. Its overall effect is to redistribute energy without dissipation.

$$\frac{D \mathbf{v}_i}{Dt} = - \sum_j m_j \left(\frac{P_i}{\rho_i^2} + \frac{P_j}{\rho_j^2} \right) \nabla_i W_{h,ij} - \sum_j m_j \Pi_{ij} \nabla_i W_{h,ij} + \frac{\epsilon}{2} \sum_j \frac{m_j}{M_0} |\mathbf{v}_{ij}|^2 \nabla_i W_{h,ij} \quad (2.78)$$

Where the viscosity term (Π_{ij}) is given by 2.79, in which (α) is a constant.

$$\Pi_{ij} = -\frac{2\alpha c_s \mathbf{v}_{ij} \cdot \mathbf{r}_{ij}}{(\rho_i + \rho_j)|\mathbf{r}_{ij}|^2} \quad (2.79)$$

The particles are subsequently transported using 2.80.

$$\frac{D \mathbf{r}_i}{D t} = \hat{\mathbf{v}}_i \quad (2.80)$$

The author validated the proposed model by simulating 2D flow past a cylinder oscillating sinusoidally in both x and y directions. The author demonstrated the model's capabilities to predict satisfactory results for the velocity correlation functions, energy spectrum and mixing while having particle resolution be half of that required for a DNS with a resolution the Reynolds length. The author concludes that the model's effectiveness for higher Reynolds numbers and other boundary conditions, such as free surfaces, will need to be studied further.

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