```
In[\bullet]:= P = 4.76; T_w = 160;
  In[*]:= T<sub>sat</sub> = ThermodynamicData["Water", "LiquidVaporPhaseBoundary",
                  {"Pressure" → Quantity[P, "bar"]}] [1] - 273.15;
         \mu_l = ThermodynamicData["Water", "Viscosity",
                {"Temperature" → Quantity[T<sub>sat</sub>, "DegreesCelsius"]}][1];
         h_f =
            ThermodynamicData["Water", "Enthalpy", {"Pressure" → Quantity[P, "bar"]}][1];
         h<sub>g</sub> = ThermodynamicData["Water", "Enthalpy",
                {"Pressure" → Quantity[P, "bar"], "Quality" → 1}] [[1]];
         h_{fg} = h_g - h_f;
         v<sub>f</sub> = ThermodynamicData["Water",
                "SpecificVolume", {"Pressure" → Quantity[P, "bar"]}][1];
         v<sub>g</sub> = ThermodynamicData["Water", "SpecificVolume",
                \{"Pressure" \rightarrow Quantity[P, "bar"], "Quality" \rightarrow 1\}][[1]];
        \rho_{l} = \frac{1}{V_{f}}; \quad \rho_{V} = \frac{1}{V_{g}};
         cpl = ThermodynamicData["Water",
                "IsobaricHeatCapacity", {"Pressure" → Quantity[P, "bar"]}][1];
         \kappa_l = ThermodynamicData["Water", "ThermalConductivity",
                {"Pressure" \rightarrow Quantity[P, "bar"], "Quality" \rightarrow 1}][[1];
         Pr_{l} = \frac{\mu_{l} c_{pl}}{\kappa_{l}};
         \Delta T_e = T_w - T_{sat};
         c_{sf} = 0.0128;
 In[*]:= qs = \mu_l h_{fg} \left( \frac{g (\rho_l - \rho_v)}{\sigma} \right)^{1/2} \left( \frac{c_{pl} \Delta T_e}{c_{sf} h_{fg} Pr_l^n} \right)^3 /. \{g \rightarrow 9.81, \sigma \rightarrow 0.0482, n \rightarrow 1\}
         4210.45
 In[•]:= Q = qs \frac{\pi D^2}{4} /. {D \rightarrow 0.2}
         132.275
 ln[*]:= qsMax = 0.149 h_{fg} \rho_v \left( \frac{\sigma g (\rho_l - \rho_v)}{\rho_v^2} \right)^{1/4} /. \{g \rightarrow 9.81, \sigma \rightarrow 0.0482\}
Out[0]=
         2.94837 \times 10^{6}
```