

Name :- Jitul Peron

Scholar Id :- 1916083

Sub :- Applied Thermodynamics

Sub code :- ME 206

Sec B :- Year II

Sem :- 4<sup>th</sup>

Branch :- Mechanical Engineering

Assignment 1

① Air is drawn in a gas turbine unit at  $15^\circ\text{C}$  and 1.01 bar and pressure ratio is 7:1. The compressor is driven by the HP Turbine and LP Turbine drives a separate power shaft. The Isentropic efficiencies of the compressor, HP and LP Turbines are 0.82, 0.85 & 0.85 respectively. If the maximum cycle temperature is  $610^\circ\text{C}$  calculate

② The pressure and temperature of the gases entering the Power Turbine.

③ The net power developed by unit per kg/s mass flow.

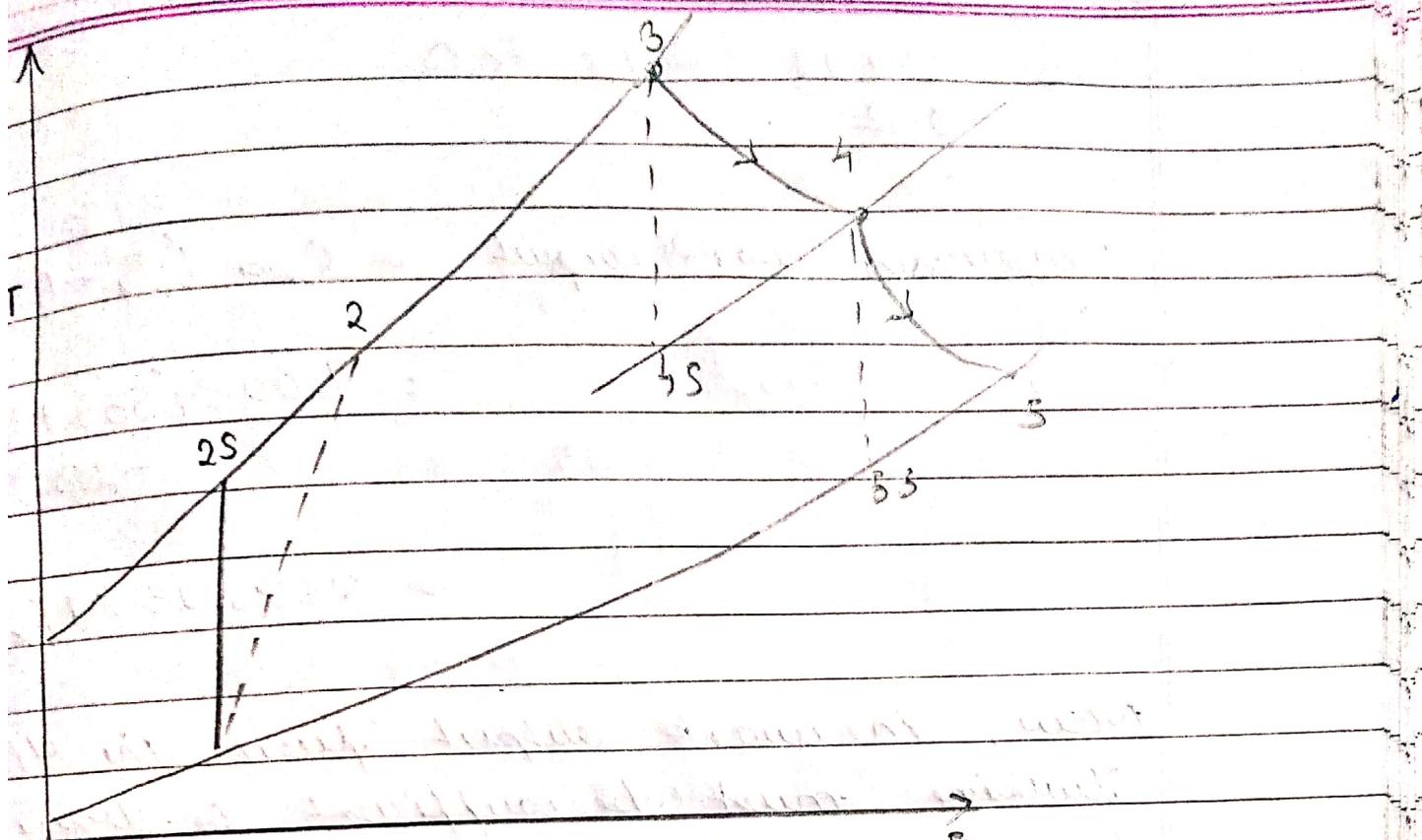
④ The work Ratio.

⑤ The thermal efficiency of unit.

For compression process  $C_{pg} = 1.005 \text{ kJ/kg K}$  and  $\gamma = 1.4$ .

For Combustion & expansion process,

$C_{pg} = 1.15 \text{ kJ/kg K}$  and  $\gamma = 1.33$



For the process  $1-2S \Rightarrow$

$$\frac{T_{2S}}{T_1} = \left( \frac{P_{2S}}{P_1} \right)^{\frac{(k-1)}{k}}$$

$$\therefore T_{2S} = (15 + 283) \left( \frac{2}{1} \right)^{\frac{(1.4-1)}{1.4}}$$

$$= 502.17 \text{ K}$$

Given,

$$\gamma_{\text{comp}} = 0.82$$

$$\Rightarrow \frac{T_{2S} - T_1}{T_2 - T_1} = 0.82$$

$$\Rightarrow \frac{502.17 - 288}{T_2 - 288} = 0.82$$

$$\Rightarrow \frac{214.17}{0.82} = T_2 - 288$$

$$\text{Compressor work input} = C_p a (T_2 - T_1) \\ = 1.005 (555.7 - 288)$$

$$= 269.05 \text{ kJ/kg}$$

Now, the work output from the HP Turbine must be sufficient to drive the Compressor,

Turbine work output from HP Turbine

$$= C_p (T_3 - T_4)$$

$$= 269.05 \text{ kJ/kg}$$

$$\Rightarrow T_3 - T_4 = \frac{269.05}{1.15}$$

$$\Rightarrow T_4 = 883 - \frac{269.05}{1.15}$$

$$= 699.04 \text{ K}$$

$$T_2 = 549.18 \text{ K}$$

Compressor work input =  $c_p a (T_2 - T_1)$

$$= 1.005 (549.18 - 288)$$

$$= 262.49 \text{ kJ/kg}$$

Now, the work output from the H.P. Turbine must be sufficient to drive the compressor,

Turbine work output from H.P. Turbine.

$$= c_p (T_3 - T_4) = 262.49 \text{ kJ/kg}$$

$$\Rightarrow T_3 - T_4 = \frac{262.49}{1.15}$$

$$\Rightarrow T_4 = 883 - \frac{262.49}{1.15}$$

$$\Rightarrow T_4 = 654.75 \text{ K}$$

Again,

$$\eta_{HP} \text{ for HP Turbine} = 0.85.$$

$$\Rightarrow \frac{T_3 - T_4}{T_3 - T_{4S}} = \frac{883 - 654.75}{883 - T_{4S}} = 0.85$$

$$\Rightarrow \frac{228.25}{0.85} = 883 - T_{4S}$$

$$\Rightarrow T_{4S} = 883 - \frac{228.25}{0.85}$$

$$\Rightarrow T_{4S} = 614.47 \text{ K}$$

Again for Turbine we know

$$\frac{T_3}{T_{4S}} = \left( \frac{P_3}{P_{4S}} \right)^{\frac{(\gamma - 1)}{\gamma}}$$

$$\Rightarrow \frac{P_3}{P_{4S}} = \left( \frac{T_3}{T_{4S}} \right)^{\frac{1}{\gamma - 1}}$$

$$= \left( \frac{883}{614.47} \right)^{\frac{1.333}{0.333}}$$

$$= 4.27$$

$$\Rightarrow P_{4S} = \frac{P_3}{4.27}$$

$$= \frac{7 \times 1.01}{4.27}$$

$$= 1.66 \text{ bar}$$

① The Pressure and Temperature of gases entering the I.P. Turbine are 1.66 bar & 657.75 K

② Now,

$$\frac{P_4}{P_5} = \frac{P_4 \times P_3}{P_3 \times P_5}$$

$$C/I/W \Rightarrow P_2 = P_3 \text{ & } P_S = P_1$$

$$\therefore \frac{P_{4S}}{P_{SS}} = \frac{P_{4S}}{P_3} \times \frac{P_{2S}}{P_1}$$

$$\frac{P_{4S}}{P_{SS}} = \frac{7}{21.27} = 1.64$$

$$\text{Again } \therefore \frac{T_4}{T_{SS}} = \left( \frac{P_{4S}}{P_{2S}} \right)^{\left( \frac{8-1}{8} \right)} = (1.64)^{\frac{0.33}{1.33}} = 1.13$$

$$\therefore T_{SS} = \frac{654.75}{1.13} = 579.42 \text{ k}$$

$n_{work}$  for the LP. turbine = 0.85

$$\Rightarrow \frac{T_4 - T_B}{T_4 - T_{SS}} = 0.85$$

$$\Rightarrow \frac{T_4 - T_S}{654.75 - 579.42} = 0.85$$

$$\Rightarrow T_4 - T_S = 64.003 \text{ k}$$

$\therefore$  Work output from LP turbine

$$= c_{ps} (T_4 - T_S)$$

$$= 73.63 \text{ kg/kg}$$

$\therefore$  Net power output

$$= 73.63 \times 1 = 73.63 \text{ kJ/KW}$$

Q1) work ratio =  $\frac{\text{Net work output}}{\text{gross work output}}$

$$= \frac{73.63}{73.63 + 26.249}$$
$$= 0.2191$$

Q2) Now,

$$\text{Heat supplied} = c_p g (T_3 - T_2)$$
$$= 1.15 (883 - 549.18)$$
$$= 383.89 \text{ kJ/Kg}$$

Hence the thermal efficiency of unit,

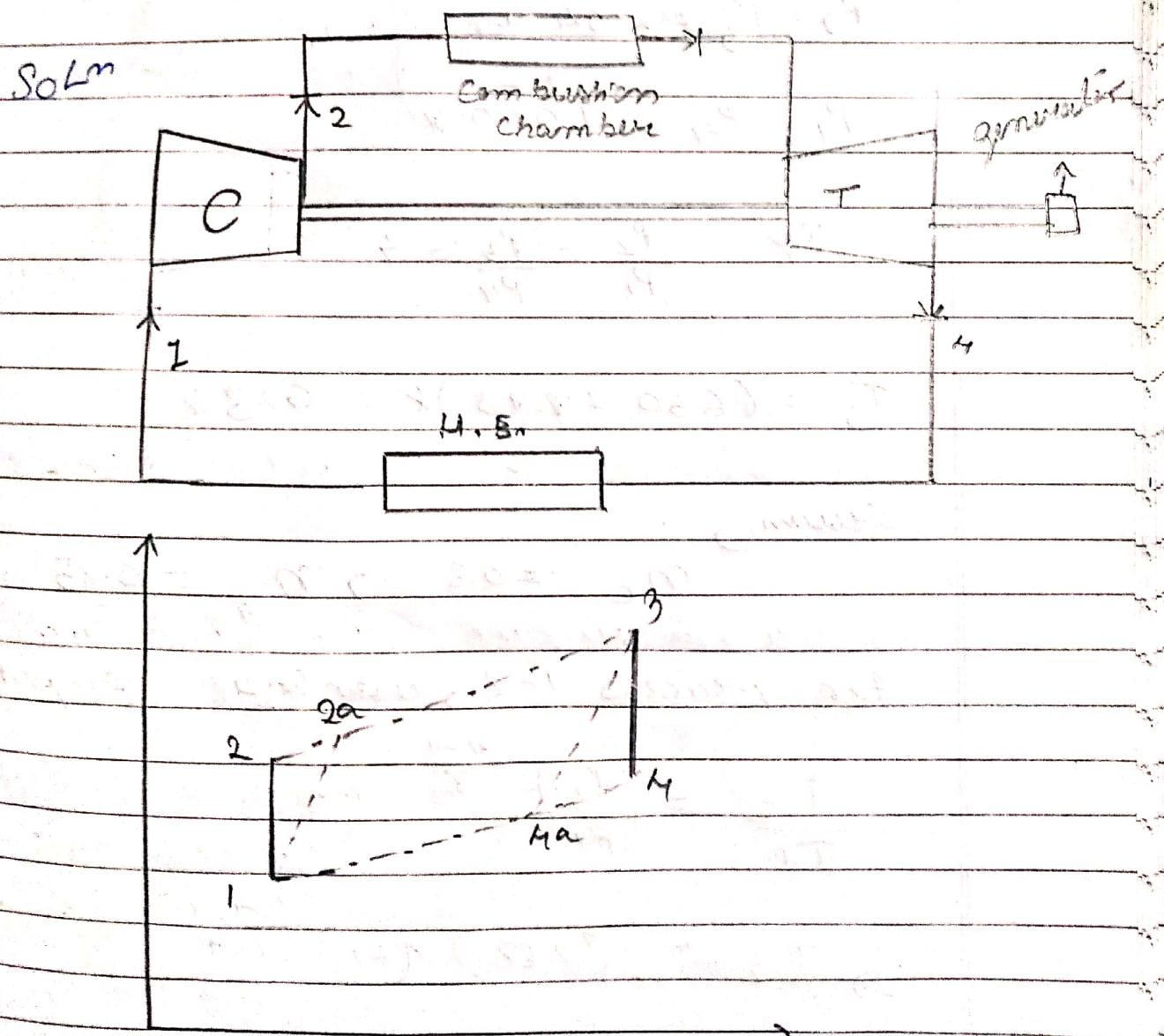
$$\eta_m = \frac{\text{Net work output}}{\text{Heat supplied}}$$

$$= \frac{73.63}{383.89}$$

$$\therefore \eta_m = 0.1918$$

Q2 In a gas turbine plant, air is compressed from 1.01 bar and  $15^{\circ}\text{C}$  through a pressure ratio of 4:1. It is then heated to  $650^{\circ}\text{C}$  in a combustion chamber and expanded back to original pressure of 1.01 bar.

Calculate the cycle efficiency and the specific power output if a perfect heat exchanger is employed. The isentropic efficiencies of the turbine and compressor are 0.85 & 0.5 respectively.



$$P_1 = 1.01 \text{ bar}, T_1 = 15^\circ\text{C}$$

$$= 15 + 273$$

$$= 288 \text{ K}$$

$$\gamma_p = \frac{P_2}{P_1} \Rightarrow 4$$

$$\Rightarrow P_2 = 4 \times P_1 = 4 \times 1.01 \text{ bar} = 4.04 \text{ bar}$$

$$\therefore \gamma_p = 4$$

$$\therefore P_2 = 4.04 \text{ bar}$$

$$P_2 = P_3 = 4.04 \text{ bar}$$

$$P_1 = P_4 = 1.01 \text{ bar}$$

$$\gamma_p = \frac{P_2}{P_1} = \frac{P_3}{P_4} = 4$$

$$T_3 = (650 + 273) \text{ K} = 928 \text{ K}$$

Außen

$$\eta_c = 0.8 \Rightarrow \eta_{\tau} = 0.85$$

for process 1-2, isentropic compression

$$\frac{T_2}{T_1} = \left( \frac{P_2}{P_1} \right)^{\frac{1}{\gamma}}$$

$$\Rightarrow T_2 = (288) \times (1.1)^{\frac{1.1-1}{1.1}}$$

$$\rightarrow T_2 = 427.96 \text{ K}$$

$$n_C = 0.8$$

$$\frac{T_2 - T_1}{T_{29} - T_1} = 0.8$$

$$\rightarrow T_{29} = \frac{427.96 - 288}{0.80} = 462.95 \text{ K}$$

For process 3-4,

Isoentropic expansion,

$$\frac{T_4}{T_3} = \left( \frac{P_4}{P_3} \right)^{\frac{1.4-1}{1.4}}$$

$$T_4 = T_3 \left( \frac{1}{\gamma} \right)^{\frac{1.4-1}{1.4}}$$

$$= 923 \left( \frac{1}{\gamma} \right)^{\frac{0.4}{1.4}}$$

$$= 621.13 \text{ K}$$

$$m_T = 0.85$$

$$\frac{T_3 - T_{49}}{T_3 - T_4} = 0.85$$

$$\Rightarrow T_3 - T_{4a} = 0.85(423 - 621.13) \\ = 256.58$$

$$\Rightarrow T_{4a} = 666.41 \quad [\because T_3 = 923 \text{ K}]$$

$\therefore$  cycle efficiency,

$$\eta_{th} = 1 - \left(\frac{1}{r_p}\right)^{\frac{\gamma-1}{\gamma}}$$

$$= 1 - \left(\frac{1}{3}\right)^{\frac{1.4-1}{1.4}}$$

$$= 0.32$$

$$\eta_{th} = 32\%$$

Now,

$$\text{Network output} = c_p (T_3 - T_{4a}) \\ - c_p (T_{2a} - T_1)$$

$$= 1.005(923 - 666.4) \\ - 462.95 + 288$$

$$= 82.05 \text{ kJ/kg}$$

Q3 Net power output (or) the specific

$$\text{Power output} = 82.05 \times 1 \\ = 82.05 \text{ kw}$$

Q3 In a gas turbine installation air is supplied at 1 bar,  $25^\circ\text{C}$  into compressor. The pressure after compression is 3.2 bar. The gas leaves the combustion chamber at  $1100^\circ\text{C}$ . A heat exchanger having effectiveness of 0.8 is fitted at exit of turbines for heating the air before its inlet into combustion chamber. Isentropic efficiency of the compressor and turbines are 0.8 and 0.85 respectively. The heat transfer inside the combustion chamber is 148 MW.

The adiabatic index is 1.3 for air and 1.33 for the gas produced by combustion. The specific heat  $C_p$  is  $1005 \text{ kJ/kg K}$  for air and  $1.5 \text{ kJ/kg K}$  for the gas. Determine the following.

- Mass flow rate
- net power output
- Thermal efficiency of cycle.

Soln

Given,

adiabatic index  $\Rightarrow \gamma = 1.4$

$$\eta_{is03} = 0.8$$

$$\eta_{is07} = 0.85$$

Let compression under be denoted by  $n_c$

$$\therefore \left( \frac{n_c - 1}{n_c} \right) = \left( \frac{8 - 1}{8 \cdot n_{iso,c}} \right)$$

$$\Rightarrow \frac{n_c - 1}{n_c} = \frac{(1.4 - 1)}{(1.4)(0.8)}$$

$$\Rightarrow n_c - 1 = 0.36 n_c$$

$$\Rightarrow 0.64 n_c = 1$$

$$\Rightarrow n_c = 1.5625$$

Let the expansion under be  $n_T$

$$\therefore \left( \frac{n_T - 1}{n_T} \right) = \left( \frac{n_{iso,T} \cdot (r - 1)}{r} \right)$$

$$\frac{n_T - 1}{n_T} = \frac{(0.85)(1.33 - 1)}{1.53} = 0.21$$

$$\Rightarrow n_T = 1.2658$$

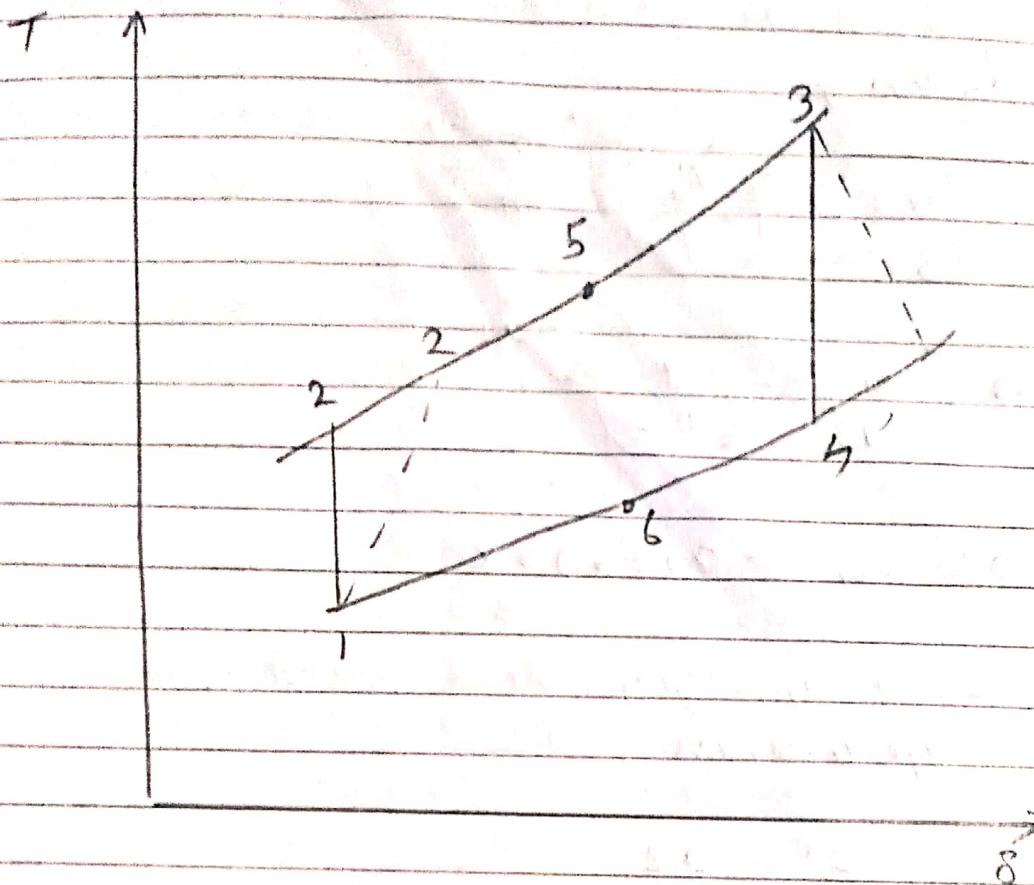


Fig : T - S plot

for process 1-2 :-

$$\frac{T_2}{T_1} = \left( \frac{P_2}{P_1} \right)^{\frac{n_c - 1}{n_c}}$$

$$\Rightarrow \frac{T_2}{298} = \left( \frac{7.2}{1} \right)^{0.36}$$

$$\Rightarrow T_2 = 298 \left( 7.2 \right)^{0.36}$$

$$\Rightarrow T_2 = 606.54K$$

$$\Rightarrow T_3 = 1100^{\circ}C = 1100 + 273 = 1373K$$

Again,

$$\frac{T_4}{T_3} = \left( \frac{P_4}{P_3} \right)^{\frac{n-1}{n}}$$

$$\Rightarrow \frac{T_4}{1373} = \left( \frac{1}{\gamma} \right)^{0.21}$$

$$\Rightarrow T_4 = 907.05 \text{ K}$$

Now applying heat on changes effectiveness,

$$\epsilon = 0.8$$

$$\left( \frac{T_5 - T_2}{T_4 - T_2} \right) \frac{c_p}{c_g} = 0.8$$

$$\Rightarrow \left( \frac{1.005}{1.15} \right) \frac{1.005}{1.005 - 0.8} = 0.8$$

$$\Rightarrow T_5 = 606.54 + \frac{276.4892}{1.005}$$

$$\Rightarrow T_5 = 881.63 \text{ K}$$

Heat added in combustion chamber,

$$Q_{\text{add}} = c_p (T_3 - T_5)$$
$$= (1.005) (1373 - 881.63)$$

$$= 493.83 \text{ kJ/kg}$$

Compressor work,  $w_c = c(T_2 - T_1)$

$$= 310.08 \text{ kJ/kg}$$

Turbine Work,  $w_t = c_p g (T_3 - T_4)$

$$= 1.15 (1373 - 907.05)$$

$$= 535.84 \text{ kJ/kg}$$

$\therefore$  Net work output,

$$w = w_t - w_c$$

$$= 535.84 - 310.08$$

$$= 225.76 \text{ kJ/kg}$$

Given,

heat transfer rate at the  
combustion chamber,  $w = 1.48 \text{ MW}$

$$\therefore \text{Mass flow rate } m = \frac{h}{w}$$

$$= 1.48 \text{ MW}$$

$$225.76 \text{ kJ/kg}$$

$$= \frac{1.48 \times 10^6 \text{ kJ}}{225.76 \text{ kJ/kg}}$$

$$= 6.56 \text{ kg/s}$$

$$\text{Net power output} = 225.76 \times 1 \\ = 227.76 \text{ kW}$$

∴ The thermal efficiency of cycles is given by

$$\eta_m = \frac{W_f - W_c}{Q_{add}} \\ = \frac{W}{Q_{add}} \\ = \frac{227.76}{493.83}$$

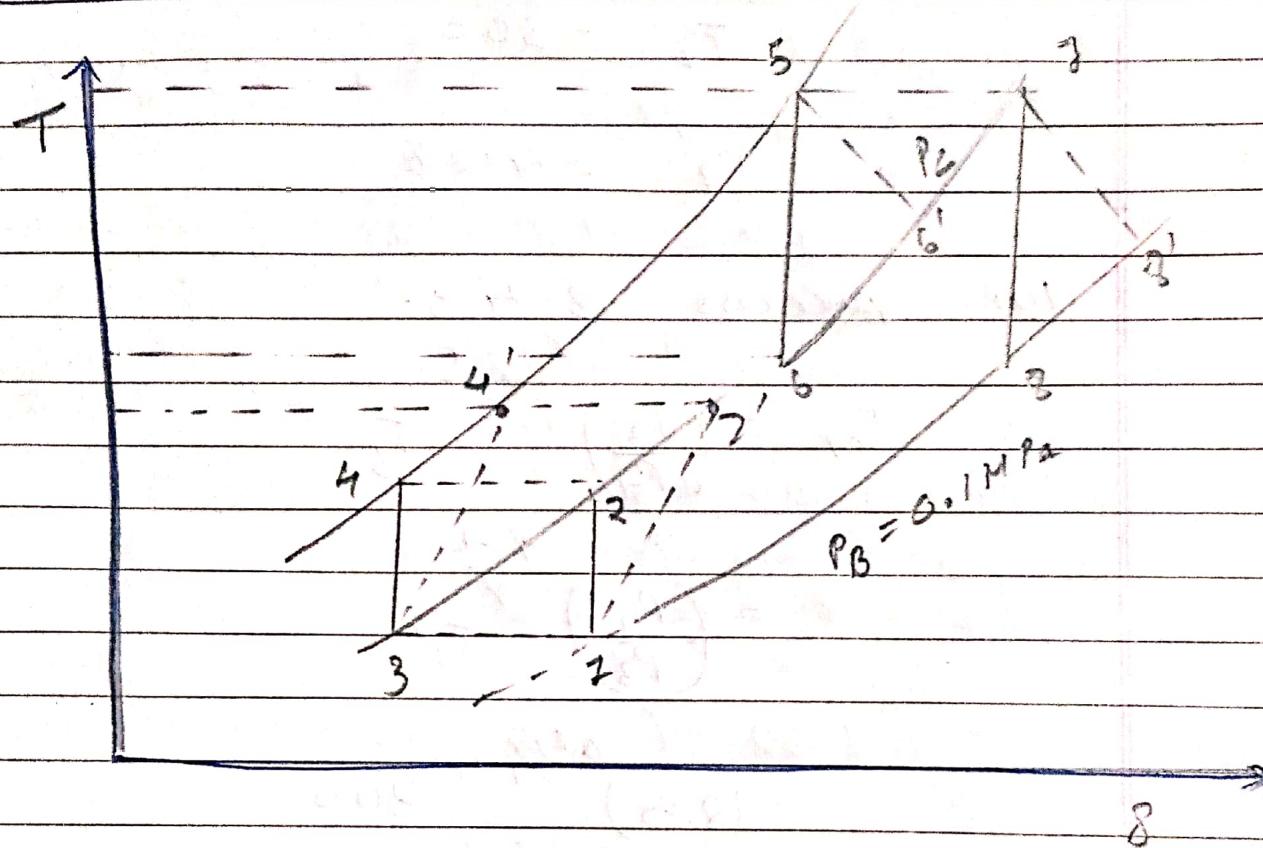
$$\eta_{th} = 0.4572 \\ \eta_{th} = 45.72\%$$

Q4 In a gas turbine plant cooled on the Brayton cycle the air at inlet is at  $28^\circ\text{C}$ ,  $0.1 \text{ MPa}$ . Compression is divided into 1000 stages, each of pressure ratio 2.5 and efficiency 80% with inter cooling to  $27^\circ\text{C}$  and efficiency 80% with inter cooling to  $27^\circ\text{C}$ . The maximum temperature of cycle is  $800^\circ\text{C}$ . Turbine inlet nozzle efficiency is 80%

Find  
The cycle efficiency.

The turbine exhaust temperature

Soln:



Carnot,

$$T_1 = T_3 = 300\text{K}$$

$$\frac{P_C}{P_B} = 2.5$$

For process 1-2:

$$T_2 = (2.5)^{0.4} \times 300$$

$$T_2 = 389.78\text{K}$$

Again,

$$\eta = \frac{T_2 - T_1}{T_2' - T_1} = 0.8$$

$$\Rightarrow \frac{389.77 - 300}{T_2' - 300} = 0.8$$

$$\Rightarrow T_2' = 412K$$

For process 3-4

$$T_4 = \left(\frac{P_3}{P_4}\right)^{\frac{1-\gamma}{\gamma}} T_3$$

$$= \left(\frac{P_4}{P_3}\right)^{\frac{\gamma-1}{\gamma}} T_3$$

$$= (2.5)^{\frac{0.4}{1.4}} 300$$

$$= 389.22K$$

Again,

$$\frac{T_4 - T_3}{T_4' - T_3} = 0.8$$

$$T_4' - T_3$$

$$\Rightarrow \frac{389.77 - 300}{T_4' - 300} = 0.8$$

$$\rightarrow T_2' = 412 \text{ K}$$

For process 5-6:

$$T_6 = \left( \frac{P_5}{P_6} \right)^{\frac{1-\gamma}{\gamma}} \cdot T_5$$

$$= (2.5)^{\frac{-0.4}{1.4}} (1073)$$

$$\rightarrow T_6 = 825.86 \text{ K}$$

$$\rightarrow T_7 = 1073 \text{ K}$$

Again  $\frac{T_5 - T_6'}{T_5 - T_6} = 0.8$

$$\rightarrow \frac{1073 - T_6'}{1073 - 825.86} = 0.8$$

$$\rightarrow T_6' = 875.29 \text{ K}$$

For process 7-8:

$$T_8 = \left( \frac{P_7}{P_8} \right)^{\frac{1-\gamma}{\gamma}} \cdot T_7$$

$$= (2.5)^{\frac{-0.4}{1.4}} (1073)$$

$$= 825.86 \text{ K}$$

$$\eta_T = 0.8$$

$$\Rightarrow \frac{1073 - T_8'}{1073 - 828.86} = 0.8$$

$$\Rightarrow T_8' = 875.29 \text{ K}$$

$\rightarrow$  Work done by compressors,

$$w_c = c_v (T_2' - T_1) + c_p (T_4' - T_3)$$

$$= 1.005 (412 - 300) + 1.005 (412 - 300)$$

$$= 825.12 \text{ kJ/kg}$$

Turbine work,

$$w_t = c_p (T_3 - T_6') + c_p (T_2 - T_8')$$

$$= 1.005 (1073 - 875.29) + 1.005 (1073 - 875.29)$$

$$= 397.40 \text{ kJ/kg}$$

Effectiveness of the generator

$$\epsilon = \frac{T_a - T_7}{T_8' - T_7}$$

$$\Rightarrow 0.25 = \frac{T_a - 412}{875.29 - 412}$$

$$\Rightarrow T_a = 859.47 \text{ K}$$

Heat supplied,

$$Q_s = c_p (T_3 - T_a) + c_p (T_2 - T_e')$$

$$= 1.005(1073 - 759.47) + 1.005(1073 - 875.29)$$

$$\Rightarrow Q_s = 513.80 \text{ kJ/kg}$$

Net work output,

$$W_{net} = w_T - w_C$$

$$= (397.40 - 225.12) \text{ kJ/kg}$$

$$W_{net} = 172.28 \text{ kJ/kg}$$

Efficiency of cycle,

$$\eta_{cycle} = \frac{W_{net}}{Q_s}$$

$$= \frac{172.28}{513.80}$$

$$= 0.3353$$

$$\Rightarrow \eta_{cycle} = 33.53\%$$

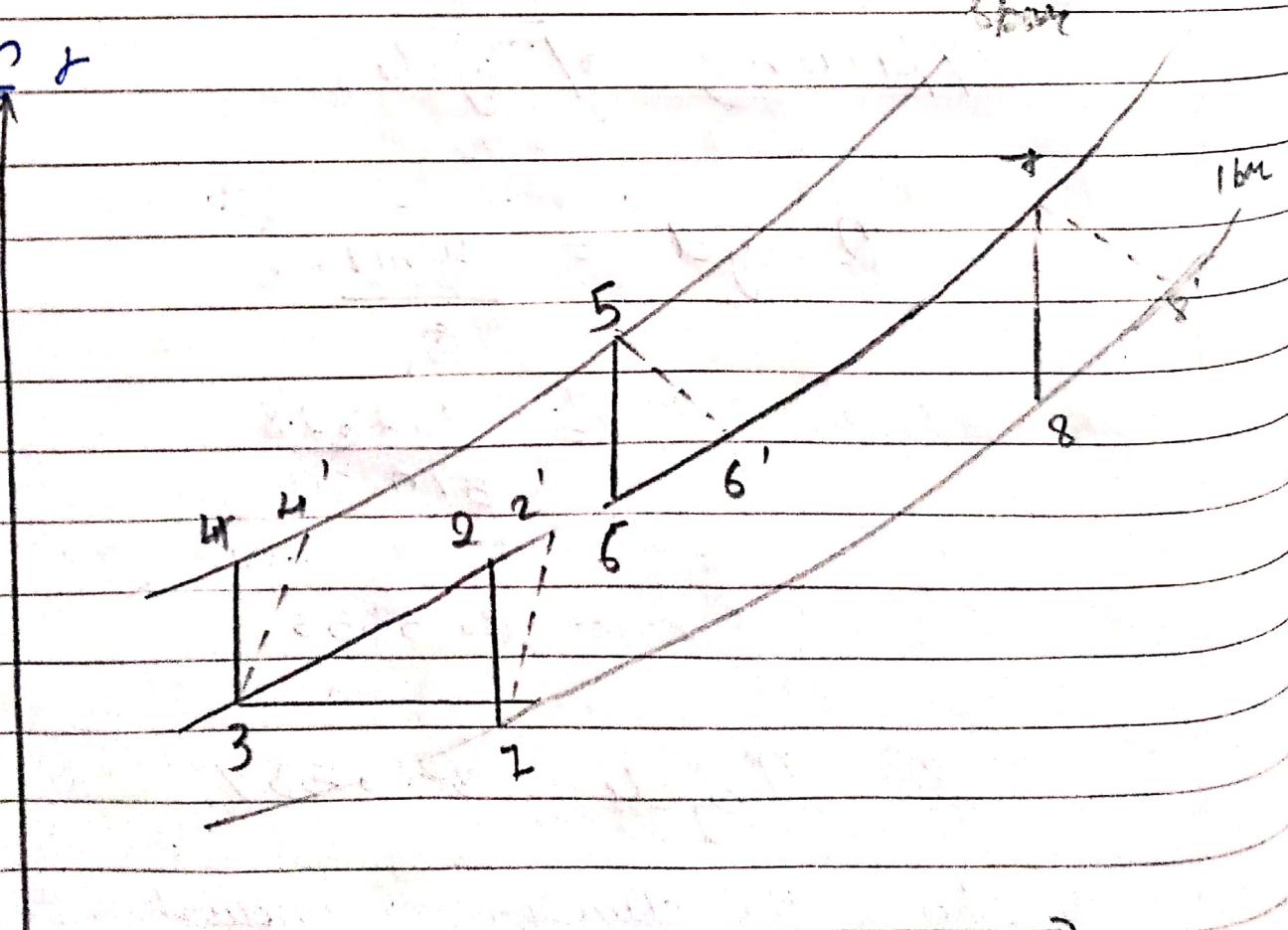
Also, the turbine exhaust temperature

$$T_{8'} = 875.29 \text{ K}$$

Q5 The air supplied to a gas turbine plant is 10 kg/s. The pressure ratio at 6 and pressure at the inlet of the compressor is 1 bar. The compressor is two stage and provided with perfect intercooler. The inlet temperature is 300 K & maximum temperature of cycle is limited to 1073 K.

i) Isentropic efficiency of compressor stage is 80% and turbine stage is 85%.  
 ii) If regenerator having effectiveness of 0.7 is included. Neglecting the mass of fuel determine the power output and the thermal efficiency of the plant

Sohm



For perfect intercooling the pressure ratio of each compression stage =  $\sqrt{6}$

$$= 2.45$$

$$\text{Hence, } T_1 = T_3 = 300\text{K} \rightarrow T_B = 1073\text{K}$$

For process 1-2:

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}}$$

$$\rightarrow T_2 = T_1 \left(\frac{P_2}{P_1}\right)^{\frac{\gamma-1}{\gamma}} = 300 (2.45)^{\frac{1.4-1}{1.4}} \\ = 387.54\text{K}$$

Again,

$$\eta_c = \frac{T_2 - T_1}{T_2' - T_1} = 0.8$$

$$\Rightarrow \frac{387.54 - 300}{T_2' - 300} = 0.8$$

$$\Rightarrow T_2'^2 = 300 + \left( \frac{387.54 - 300}{0.8} \right)$$

$$= 409.425$$

$$= 409.43\text{N (Approx)}$$

For process 3-4

$$\frac{T_4}{T_3} = \left(\frac{P_4}{P_3}\right)^{\frac{r-1}{r}}$$

$$\Rightarrow T_4 = 300 \left(2.45\right)^{\frac{0.4}{1.4}} \\ = 387.54 \text{ K}$$

Again,

$$\frac{T_4 - T_3}{T_{4'} - T_3} = 0.8$$

$$\Rightarrow \frac{387.54 - 300}{T_{4'} - 300} = 0.8$$

$$\Rightarrow T_{4'} = 300 + \left( \frac{387.54 - 300}{0.8} \right) \\ = 409.43 \text{ K}$$

For process 5-6 :-

$$\frac{T_6}{T_5} = \left(\frac{P_6}{P_5}\right)^{\frac{8-1}{8}} \\ = \left(\frac{P_5}{P_6}\right)^{\frac{1-8}{r}}$$

$$T_6 = (1073)(2.45)^{1.7} \quad (\because T_5 = 1073K)$$

$$\rightarrow T_6 = 830.63K$$

Also,

$$T_2 = T_5 = 1073K$$

Now,

$$\frac{T_5 - T_6'}{T_5 - T_6} = 0.85$$

$$T_5 - T_6$$

$$\Rightarrow \frac{1073 - T_6'}{1073 - 830.63} = 0.85$$

$$\Rightarrow (1073 - T_6') = (0.85)(1073 - 830.63)$$

$$\Rightarrow T_6' = 1073 - (0.85)(1073 - 830.63)$$

$$\rightarrow T_6' = 866.99K$$

for process 2-8

$$\frac{T_8}{T_2} = \left(\frac{P_7}{P_8}\right)^{\frac{1-8}{r}}$$

$$\rightarrow T_8 = (1073)(2.45)^{1.7} \quad \left(\frac{-0.5}{r}\right)$$

$$\rightarrow T_8 = 830.63K$$

$$\eta_r = \frac{T_2 - T_8'}{T_2 - T_8} = 0.85$$

$$\Rightarrow \frac{1073 - T_8'}{1073 - 830.63} = 0.85$$

$$\Rightarrow T_8' = -(0.85)(1073 - 830.63) + 1073$$

$$\Rightarrow T_8' = 1073 - (0.85)(1073 - 830.63)$$

$$= 866.994$$

Work done by Compressor

$$w_c = C_p(T_2' - T_1) + C_p(T_3' - T_3)$$

$$= (1.005)[409.43 - 300 + 409.43]$$

$$- 300]$$

$$= 219.95 \text{ kJ/kg}$$

Turbine Work,

$$w_t = C_p(T_3 - T_4') - C_p(T_2 - T_8')$$

$$= 1.005[1073 - 866.99 + 1073 - 866.99]$$

$$= 414.08 \text{ kJ/kg}$$

## Effectiveness of regenerator

$$\epsilon = \frac{T_a - T_g'}{T_g' - T_a}$$

$$0.3 = \frac{T_a - 409.43}{866.99 - 409.43}$$

$$\Rightarrow T_a = (409.43) + (0.3)(866.99 - 409.43)$$

$$\Rightarrow T_a = 729.82 \text{ K}$$

Heat supplied,

$$Q_s = c_p (T_3 - T_a) + c_p (T_2 - T_e')$$

$$= 1.005 (1073 - 729.82) + 1.005 (1073 - 866.99)$$

$$= 552.04 \text{ kJ/kg}$$

∴ Net work output,

$$W_{net} = W_T - W_C$$

$$= (414.08 - 219.95)$$

$$= 194.13 \text{ kJ/kg}$$

∴ Power output,

$$P = m \cdot \alpha \cdot w_{net}$$

$$= 100 \text{ kg/s} \times 1941.3 \text{ kJ/kg}$$

$$= 19413 \text{ kW}$$

$$= 19413 \text{ kW}$$

Efficiency of the gas turbine plant,

$$\eta = \frac{w_{net}}{\dot{Q}_s}$$

$$= \frac{194.13}{552.04}$$

$$\eta = 0.3517$$

$$\therefore \eta = 35.17\%$$