

Assignment #2

(Submission Date: on or before 6 PM, 27/03/24)

Prob 1

Consider the following dynamic model of biochemical reactor

$$\begin{aligned} \bullet \quad \frac{dC_b}{dt} &= (\mu - F_d)C_b \\ \bullet \quad \frac{dC_s}{dt} &= F_d(C_{sf} - C_s) - \frac{\mu C_b}{P} \\ \mu &= \frac{\mu_m C_s}{k_m + C_s + k_1 C_s^2} \end{aligned}$$

Where, C_b and C_s are the biomass and substrate concentration respectively.

- Derive linear state space model for the system to control c_b by manipulating F_d
- Show that this reactor is not fully state controllable irrespective of parameter and steady state values.

Prob 2

Consider the following dynamic model of an isothermal reactor

$$\begin{aligned} \bullet \quad \frac{dC_A}{dt} &= \frac{F}{V}(C_{Af} - C_A) - k_1 C_A - k_3 C_A^2 \\ \bullet \quad \frac{dC_B}{dt} &= -\frac{F}{V}C_B + k_1 C_A - k_2 C_B \end{aligned}$$

Data: $k_1 = 50$, $k_2 = 100$, $k_3 = 10$, $C_{Af} = 10$, $V = 1$

- Find the steady state values of C_A and C_B for steady state $F=60$.
- Derive linear state-space model for the system to control C_B by manipulating F .
- Design state feedback controller for the reactor using Bass-Gura method by judiciously placing the closed loop poles at desired location of your choice.