

Heat TransferHeat transfer through Variable cross-sectional area

$T_1 > T_2$ .  $K = \text{constant}$ .

$$\frac{dQ}{dt} = -K (4\pi r^2) \left( \frac{dT}{dr} \right)$$

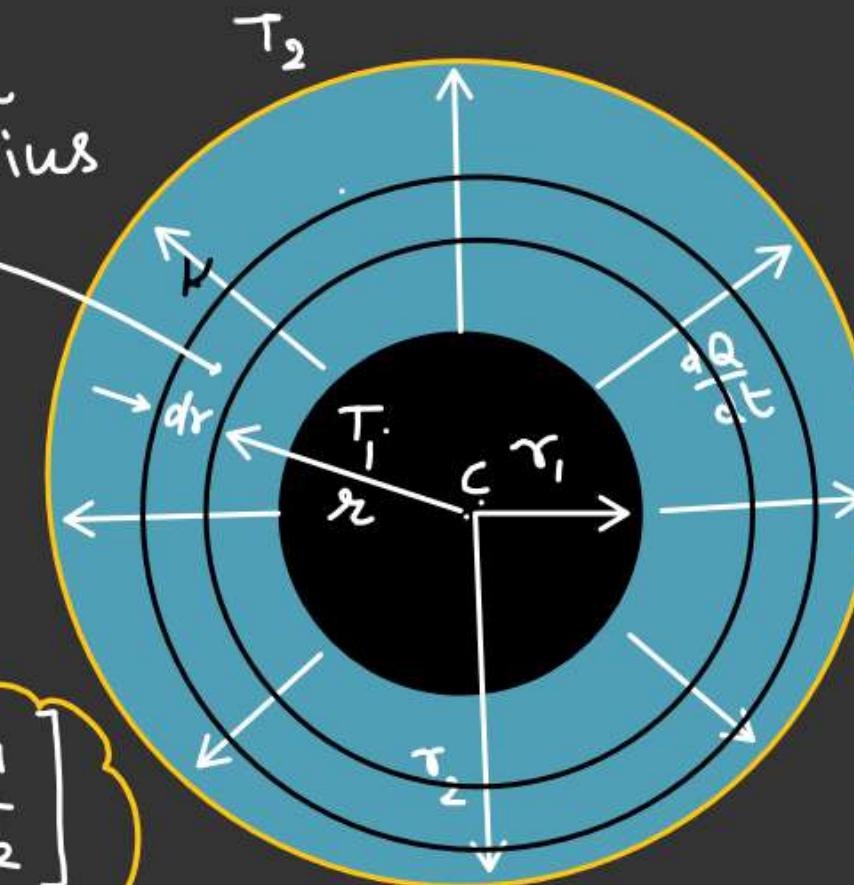
$$P \frac{dJ}{ds} = -(4\pi r^2) K \frac{dT}{dr}$$

$$P \int_{r_1}^{r_2} \frac{dr}{r^2} = - \frac{4\pi K}{T_1} \int_{T_1}^{T_2} dT$$

$$P \left[ -\frac{1}{r} \right]_{r_1}^{r_2} = -4\pi K (T_2 - T_1)$$

$$P \left[ \frac{1}{r_1} - \frac{1}{r_2} \right] = 4\pi K (T_1 - T_2)$$

Spherical  
Shell of radius  
 $r$  and  
thickness  $dr$



$$P = \frac{T_1 - T_2}{\frac{1}{4\pi K} \left[ \frac{r_2 - r_1}{r_1 r_2} \right]}$$

Heat current

Thermal Resistance

$$R_{th} = \frac{1}{4\pi K} \left( \frac{r_2 - r_1}{r_1 r_2} \right)$$

Heat Transfer

Case when temperature of one end of the rod is a function of time

Total Steady state heat flow from left to right.

$$100 = 20 + 2t$$

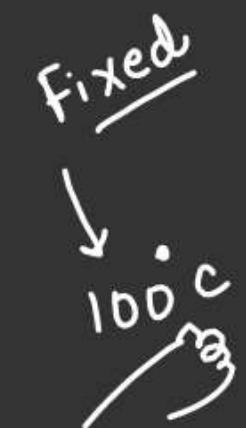
$$t = \frac{80}{2} = 40 \text{ sec}$$

At every moment  $(\frac{dQ}{dt})$  is different

$$\text{At } t = t$$

$$\frac{dQ}{dt} = \frac{KA}{L} [100 - (20 + 2t)]$$

$$\frac{dQ}{dt} = \frac{KA}{L} (80 - 2t)$$



$$\rightarrow \frac{dQ}{dt} \quad (20 + 2t) = T$$

$$\int_0^Q dQ = \frac{KA}{L} \int_0^{40} (80 - 2t) dt$$

$$Q = \frac{KA}{L} \left[ 80[t]_0^{40} - 2[\frac{t^2}{2}]_0^{40} \right]$$

$$Q = \frac{KA}{L} [80 \times 40 - (600)]$$

$$Q = \frac{1600 KA}{L} \text{ J}$$

Heat Transfer

$$K = \left( \frac{\alpha}{T} \right) \quad \text{where } \alpha \text{ is a constant.}$$

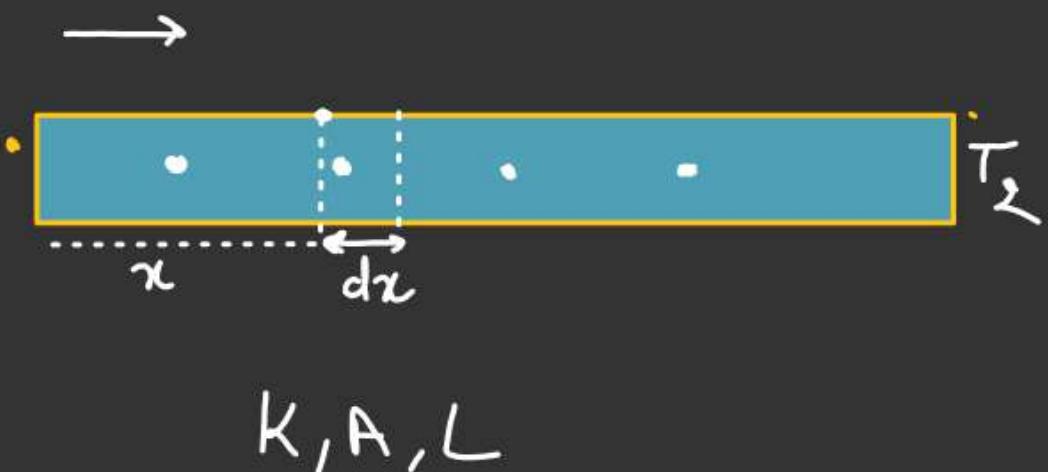
$$\left( \frac{dQ}{dt} \right) = -KA \frac{dT}{dx} = -\left( \frac{A\alpha}{T} \right) \frac{dT}{dx}$$

P J/s

$$T_1 > T_2$$

$$P \int_0^L dx = -A\alpha \int_{T_1}^{T_2} \frac{dT}{T} \longrightarrow P \int_0^x dx = -A\alpha \int_{T_1}^T \frac{dT}{T}$$

Temp. as a function of  $x$ .



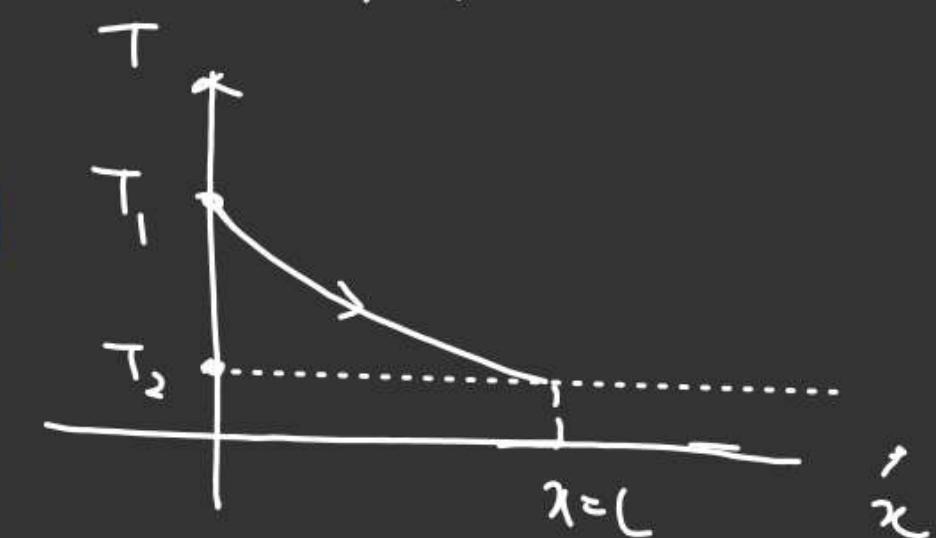
$$PL = -A\alpha \ln\left(\frac{T_2}{T_1}\right)$$

$$P = \left( \frac{A\alpha}{L} \right) \ln\left(\frac{T_1}{T_2}\right) \checkmark$$

$$P\alpha x = -A\alpha \ln\left(\frac{T}{T_1}\right)$$

$$-\frac{P\alpha x}{A\alpha} = \ln\left(\frac{T}{T_1}\right)$$

$$\underline{T = T_1 e^{-\frac{P}{A\alpha} x}}$$



Heat Transfer

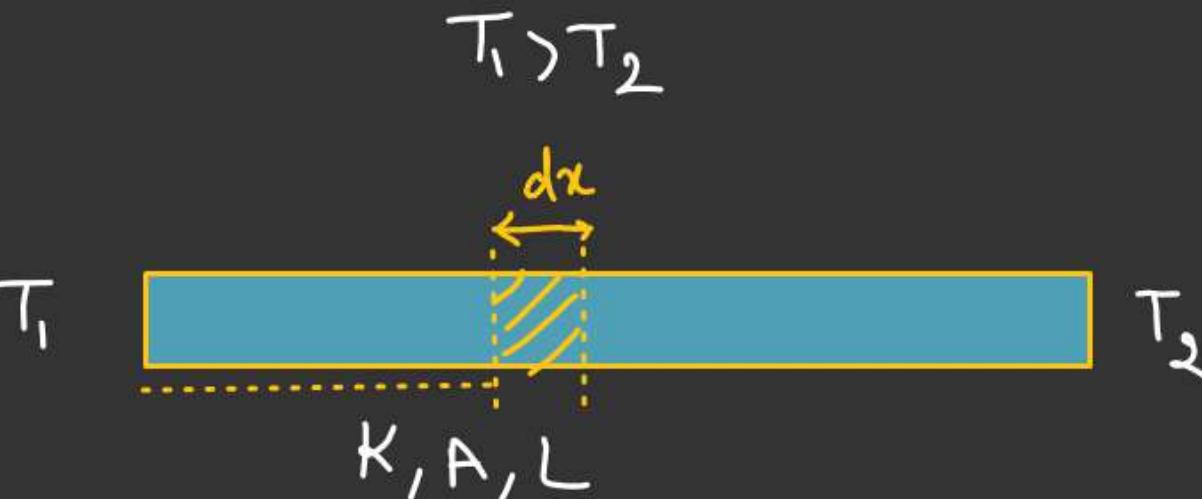
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$$K = (K_0 + \alpha x)$$

$K_0$  &  $\alpha$  are  
constant.

$$\frac{dQ}{dt} = K_A A \left( -\frac{dT}{dx} \right)$$

||



$$P = A (K_0 + \alpha x) \left( -\frac{dT}{dx} \right)$$

$$P \int_0^L \left( \frac{dx}{K_0 + \alpha x} \right) = -A \int_{T_1}^{T_2} dT$$

$$\frac{P}{\alpha} \ln \left[ \frac{K_0 + \alpha L}{K_0} \right] = -A (T_2 - T_1)$$

$$\frac{P}{\alpha} \ln \left( \frac{K_0 + \alpha L}{K_0} \right) = A (T_1 - T_2)$$

$$P = \frac{(T_1 - T_2)}{\frac{1}{\alpha A} \ln \left( \frac{K_0 + \alpha L}{K_0} \right)}$$

Thermal  
Resistance

$$R = \int_0^L \frac{dx}{(K_0 + \alpha x) A}$$

Heat Transfer ~~$\Delta T_{imp}$~~ Heat Transfer into a Sink

$S \rightarrow$  Specific heat of block. (constant)  $A + t = 0$   
 $T_1 > T_2$

$m \rightarrow$  mass of block.

$$(dQ = mSdT) \checkmark$$

$A + t = 0$ ,  $T_1$  &  $T_2$  be the temp  
of one end of the rod and sink.

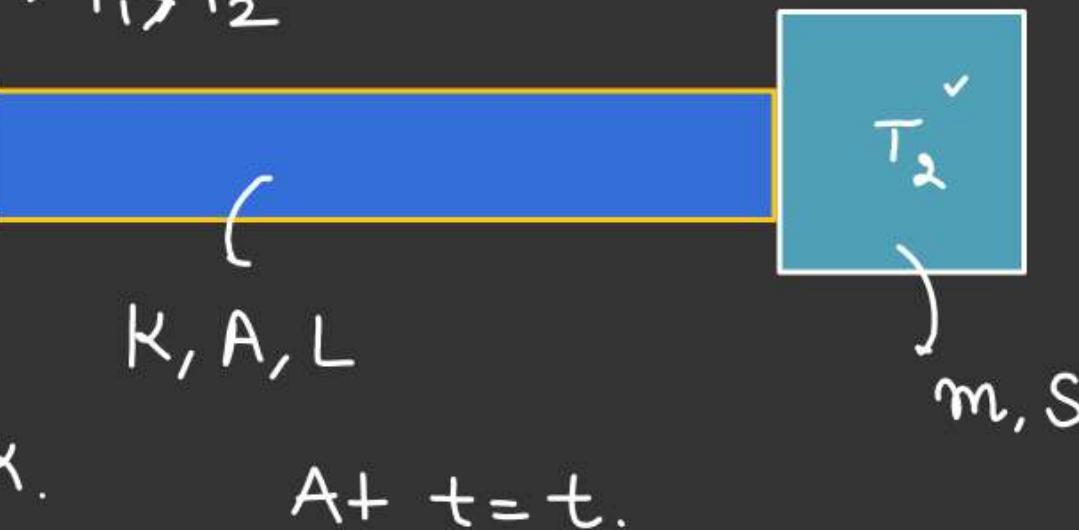
$$T_2 \rightarrow f(t)$$

Equation of Rod

$$\frac{dQ}{dt} = \frac{KA}{L} (T_1 - T) \quad \textcircled{1}$$

Equation of block.

$$dQ = mSdT \rightarrow \frac{dQ}{dt} = mS \frac{dT}{dt} \quad \textcircled{2}$$



$$A + \rightarrow (t + dt)$$

$$\frac{dQ}{(T + dT)}$$

Heat TransferEquation of Rod ✓

$$\frac{dQ}{dt} = \frac{KA}{L} (T_1 - T) \quad \textcircled{1}$$

Equation of block K.

$$dQ = ms dT \rightarrow \frac{dQ}{dt} = ms \frac{dT}{dt} \quad \textcircled{2}$$

$$ms \frac{dT}{dt} = \frac{KA}{L} (T_1 - T)$$

$$\int_{T_2}^T \frac{dT}{(T_1 - T)} = \frac{KA}{msL} \int_0 t dt$$

$$\ln \left[ \frac{T_1 - T}{T_2} \right] = \frac{KA}{msL} t$$

$$\ln \left( \frac{T_1 - T}{T_1 - T_2} \right) = - \frac{KA}{msL} t$$

$$(T_1 - T) = (T_1 - T_2) e^{-\frac{KA}{msL} t}$$

$$T = T_1 - (T_1 - T_2) e^{-\frac{KA}{msL} t}$$

Heat Transfer

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$$T = T_1 - (T_1 - T_2) e^{-\frac{KA}{msL}t}$$

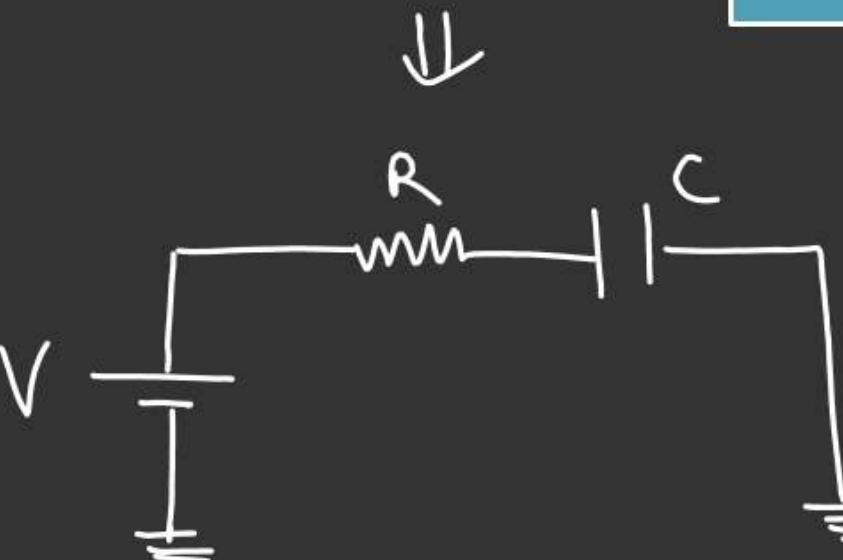
$$ms = \underset{\downarrow}{C}$$

heat capacity

$$\frac{L}{KA} = R.$$

$$T = T_1 - (T_1 - T_2) e^{-\frac{t}{(ms)(\frac{L}{KA})}}$$

$$T = T_1 - (T_1 - T_2) e^{-\frac{t}{RC}}$$

Block  $\rightarrow$  CapacitorRod  $\rightarrow$  Resistance

Heat Transfer

$$T = T_1 - (T_1 - T_2) e^{-\frac{KA}{msL} t}$$

Ans

At  $t=0$ 

ice cube.

 $\downarrow m L_f S$ 100°C  
↓  
(fixed)

Find total time taken to convert ice cube to 0°C water

Let,  $t_1$  be the time taken to change the temp. of ice cube from -10°C to 0°C

$$T_1 = 100^\circ\text{C}, \quad T_2 = -10^\circ\text{C}, \quad T = 0^\circ\text{C}$$

$$0 = 100 - (110) e^{-\frac{KA}{msL} t_1}$$

$$e^{-\frac{KA}{msL} t_1} = \frac{10}{11}$$

$$-\frac{KA}{msL} t_1 = \ln\left(\frac{10}{11}\right)$$

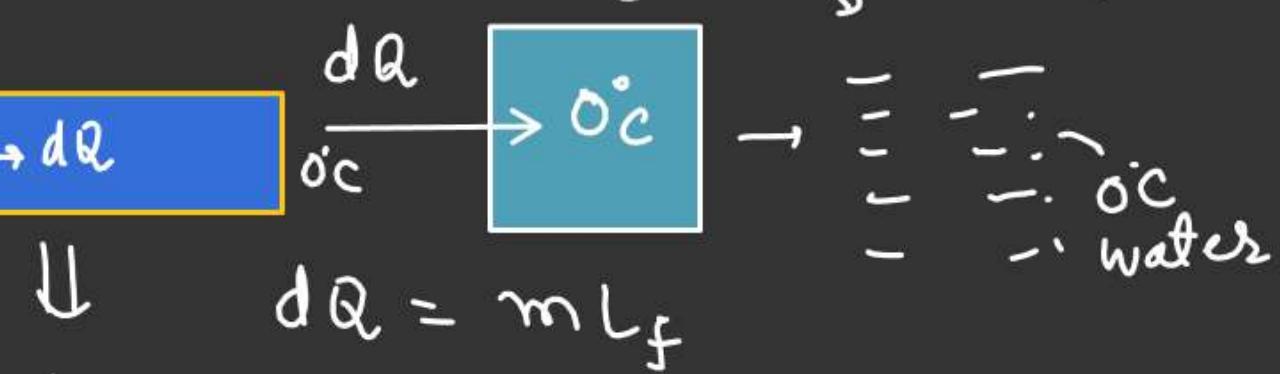
$$t_1 = \frac{msL}{KA} \ln\left(\frac{11}{10}\right)$$

K, A, L

-10°C

L = latent heat of fusion of ice

S = Specific heat of ice



$$\frac{dQ}{dt} = \frac{100-0}{L/KA}$$

Heat TransferAt  $t = 0$ 

ice cube.

 $\downarrow m L_f S$ 

$$m \int_0^t dm = \frac{100KA}{L} \int_0^{t_2} dt$$

$100^\circ C$   
(fixed)

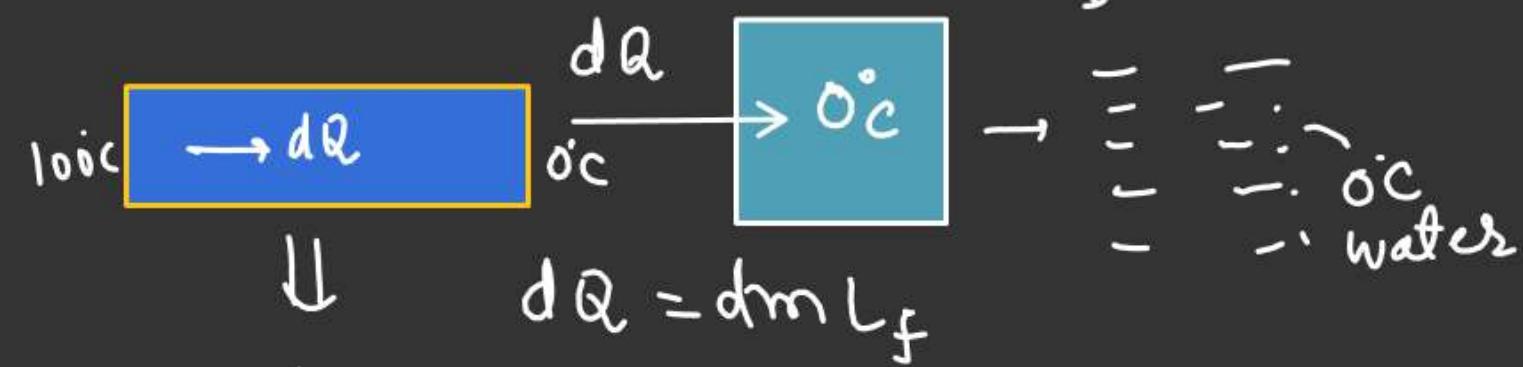


$L$  = latent heat of fusion of ice

$$m L_f = \frac{100KA}{L} t_2$$

$$t_2 = \left( \frac{m L_f L}{100KA} \right)$$

$$(t = t_1 + t_2)$$



$$\frac{dQ}{dt} = \frac{100 - 0}{\frac{L}{KA}}$$

$$L_f \frac{dm}{dt} = \frac{KA(100)}{L}$$

Heat Transfer

\* Find temp difference  
of vessel as a  
function of time

At  $t = 0$

$T_1 > T_2$

