

(6)

0.1 mol
H₂O

0.9 ethanol

$$\Delta T_f = K_f \times m$$

$$\Delta T_f = 2 \times \frac{0.1}{0.9 \times 46} \times 1000$$

$$P_T = X_A P_A^0 + \cancel{X_B P_B^0}^0$$

$$P_T = 0.9 \times P_{\text{ethanol}}^0$$

(8)

0.9 mol
H₂O

0.1 mol

$$\Delta T_b = K_b \times \frac{0.1}{0.9 \times 18} \times 1000$$

↑
H₂O

$$(20) \frac{P_0 - P_s}{P_s} = \frac{n}{N}$$

$$(11) \Delta T_b = K_b \times m$$

$$2 = 0.76 \times (m)$$

$$\frac{760 - P_s}{760} \quad \frac{P_0 - P_s}{P_0} = m \times \frac{18}{1000}$$

$$(33) \quad 0-2$$

$$0.15 = K_b \times m$$

$$\Delta T_f = K_f \times \frac{m}{2}$$

$$(42) \quad 27^\circ \text{C}$$

$$(47)$$

$$A \rightarrow \frac{1}{3} A_3$$

$$\eta = \frac{1}{3}$$

$$i = 1 + \left(\frac{1}{3} - 1\right) \alpha = \frac{1}{3}$$

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Solvent

52

$$\frac{P_0 - P_s}{P_0} = \frac{m \times \frac{M_{\text{solvent}}}{1000} \times 1}{1}$$

$$0.1 \times 2$$

$$0.1 \times 2$$

$$0.1 \times 3$$

$$2 : 2 : 3$$

$$\Delta T_b \propto m \times i$$

$$\Delta T_f \propto m \times i$$

$$\pi \propto C \times i$$

$$\frac{P_0 - P_s}{P_0} \propto m \times i$$

$$T_f$$

$$\text{vap. pr}$$

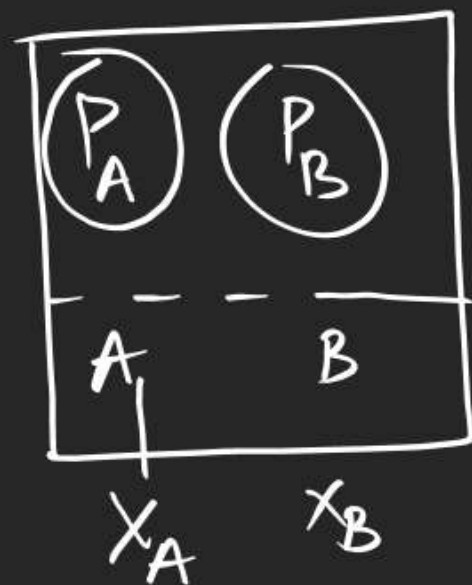
$$K_b = \frac{RT_b^2}{1000 L_v}$$

$$= \frac{2 \times (373.15)^2}{1000 \times \frac{9.72 \times 10^3}{18}}$$

23

$$1.24 = 0.512 \times \frac{288/M}{600} \times 1000$$

Non-ideal solution : \rightarrow An ideal solⁿ is formed when intermolecular forces remain unchanged on mixing. i.e.

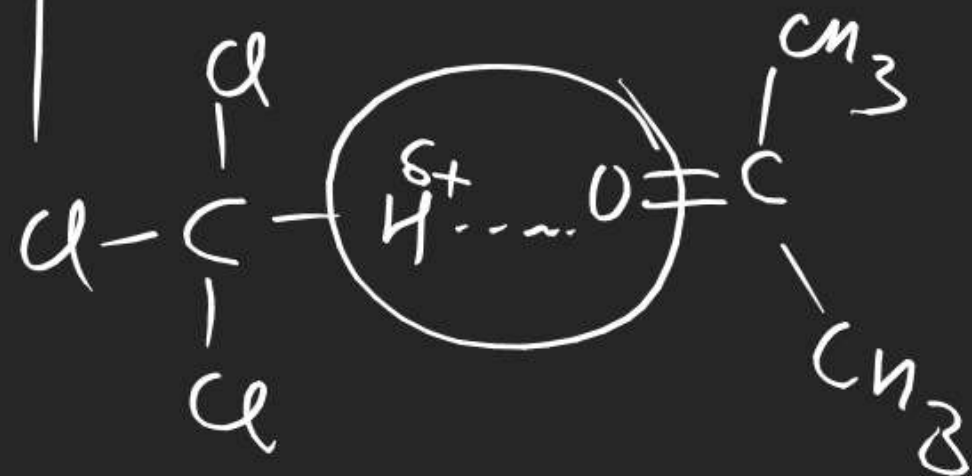


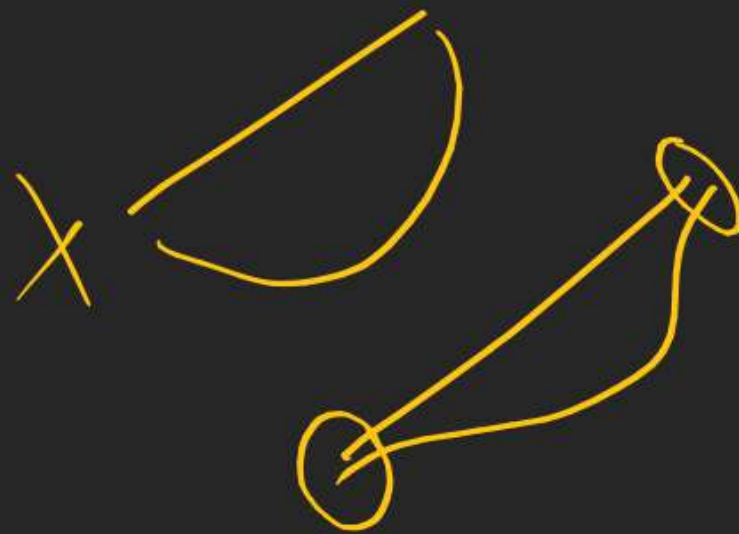
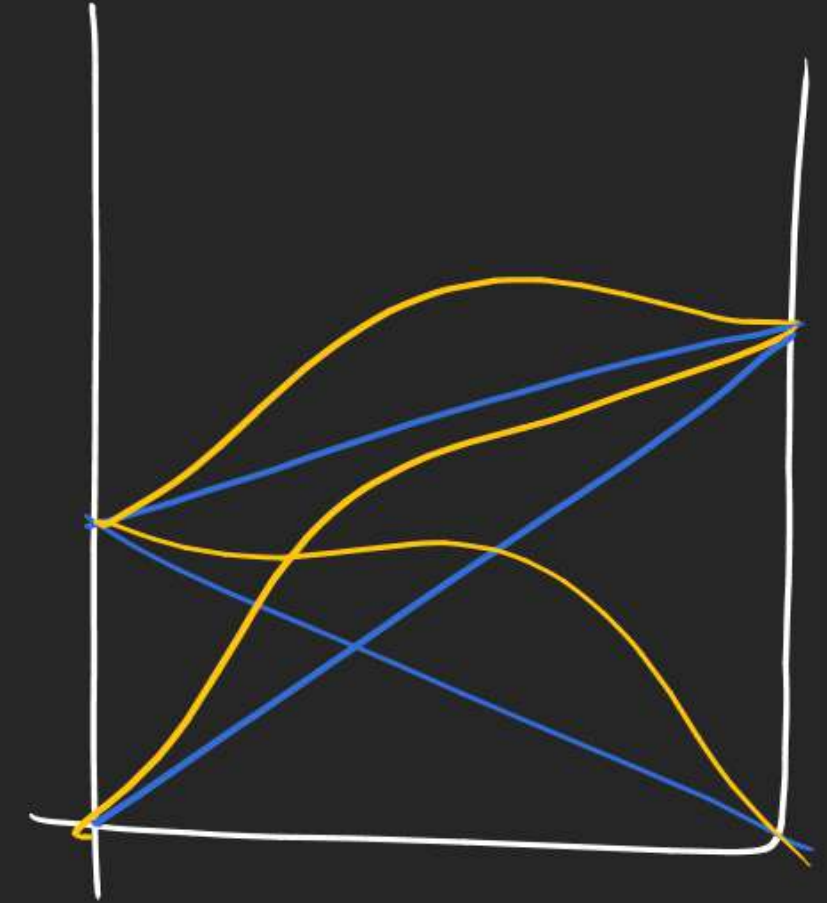
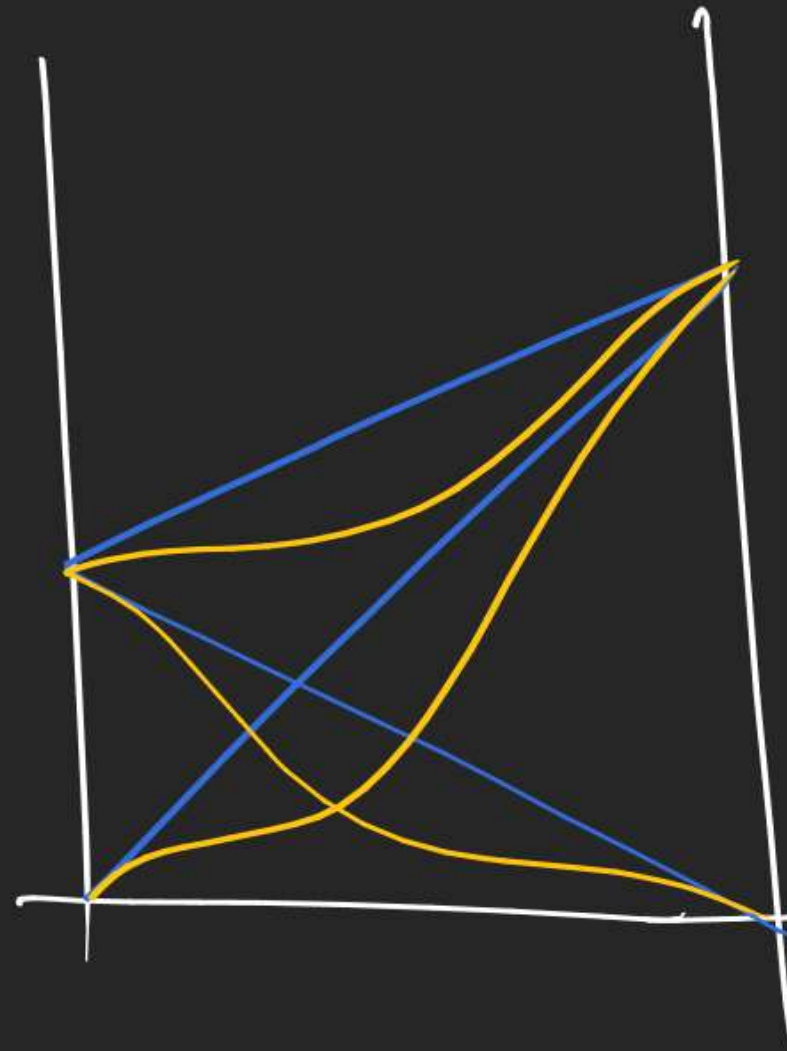
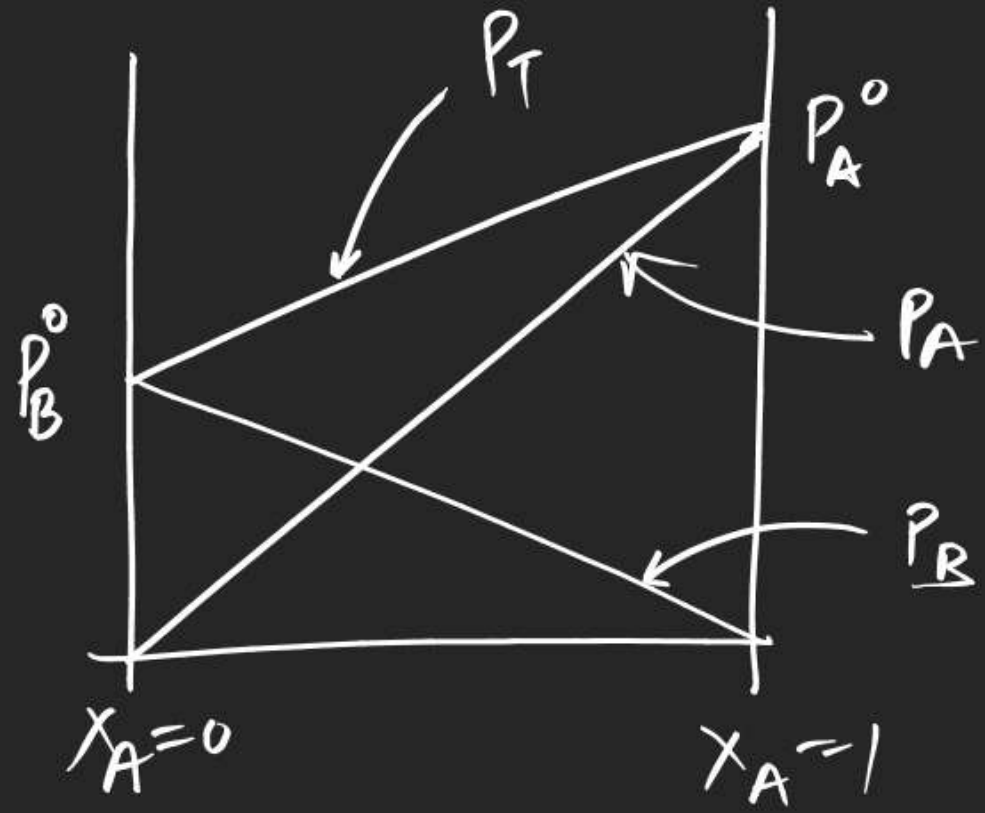
$$\langle A-A \rangle = \langle A-B \rangle = \langle B-B \rangle$$

This condⁿ is however not fulfilled by most of the liq pairs thus they form non-ideal solution.

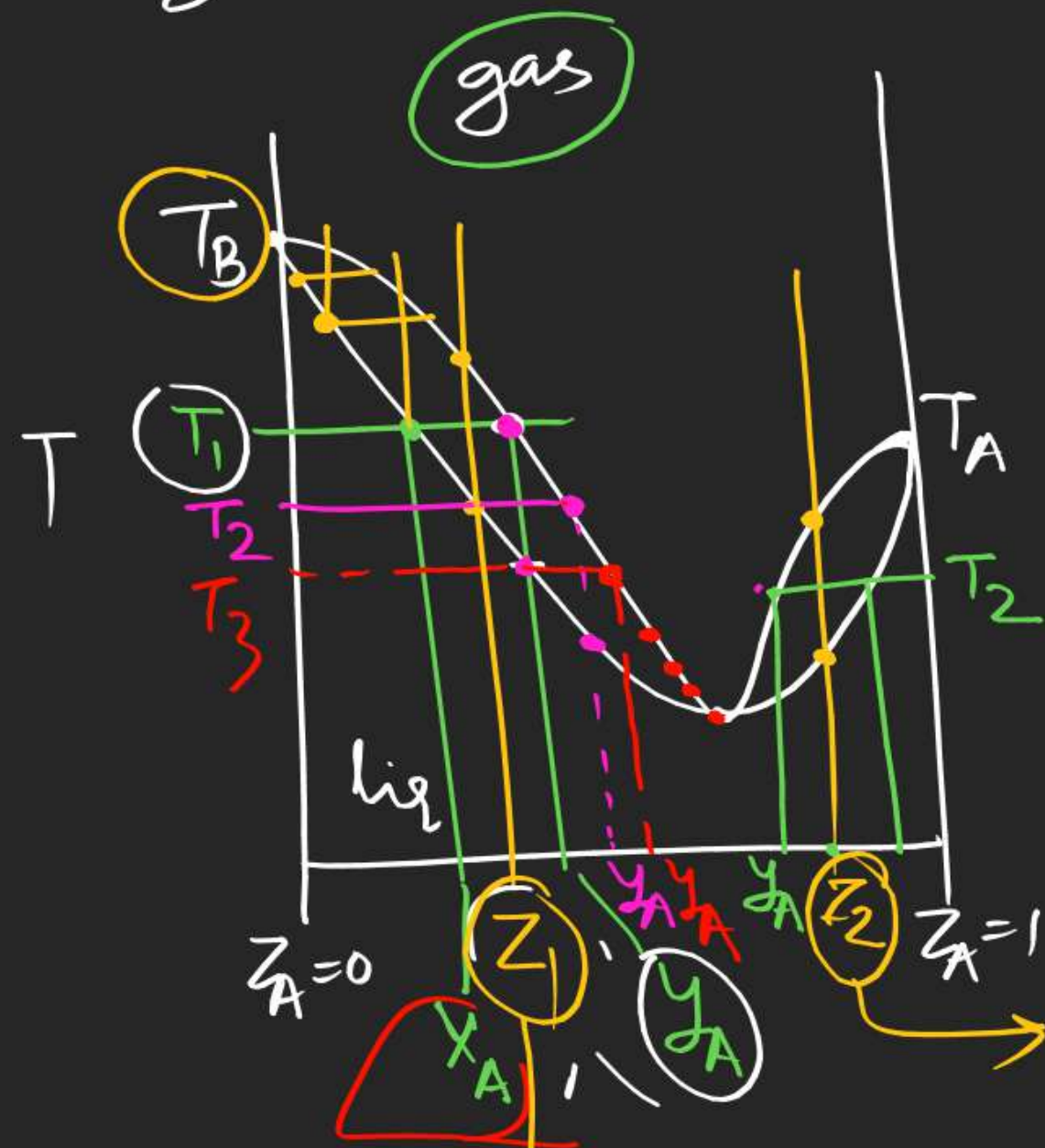
ideal sol ⁿ	Non-ideal sol ⁿ -ive deviation	+ive deviation
obey Raoult's law	① do not obey	do not obey
I.F. remain unchanged on mixing.	② I.F. increase on mixing	I.F. ↓ es.
$P_A = X_A P_A^0$ $P_B = X_B P_B^0$	③ $(P_A)_{\text{actual}} < X_A P_A^0$ $(P_B)_{\text{actual}} < X_B P_B^0$	$(P_A)_{\text{actual}} > X_A P_A^0$ $(P_B)_{\text{actual}} > X_B P_B^0$
④ $\Delta H_{\text{mix}} = 0$	$\Delta H_{\text{mix}} < 0$ exo	> 0 endo
⑤ $\Delta V_{\text{mix}} = 0$	→ $\Delta V_{\text{mix}} < 0$	> 0
⑥ $\Delta S_{\text{mix}} > 0$	$\Delta S_{\text{mix}} > 0$	> 0
⑦ $\Delta S_{\text{mix}} < 0$	$\Delta S_{\text{mix}} < 0$	< 0
⑧ $\Delta S_{\text{sur}} = 0$	$\Delta S_{\text{sur}} > 0$	< 0
⑨ $\Delta S_{\text{univ}} > 0$	> 0	> 0

e.g.
 n-hexane & n-heptane
 Benzene + Toluene
 $C_2H_5Cl + C_2H_5Br$
 $C_6H_5Cl + C_6H_5Br$



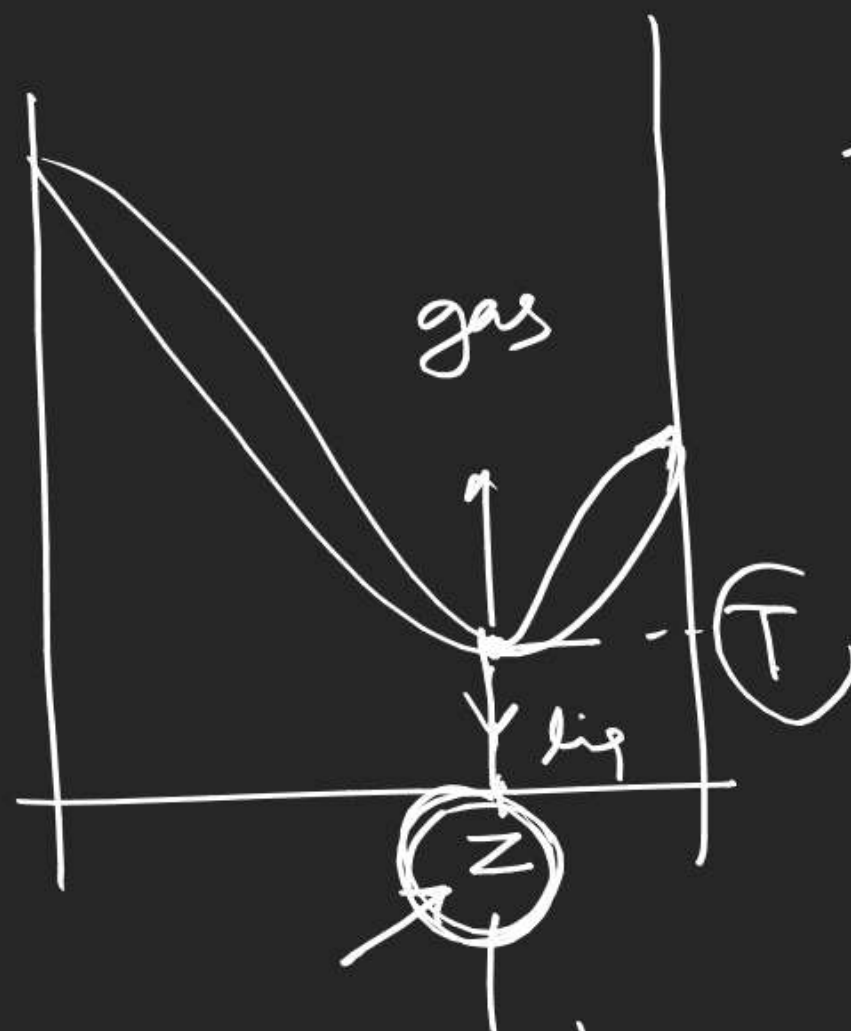


Azeotrope



but not pure A pure B can be obtained

distillation method can not be used to separate the components of azeotrope.



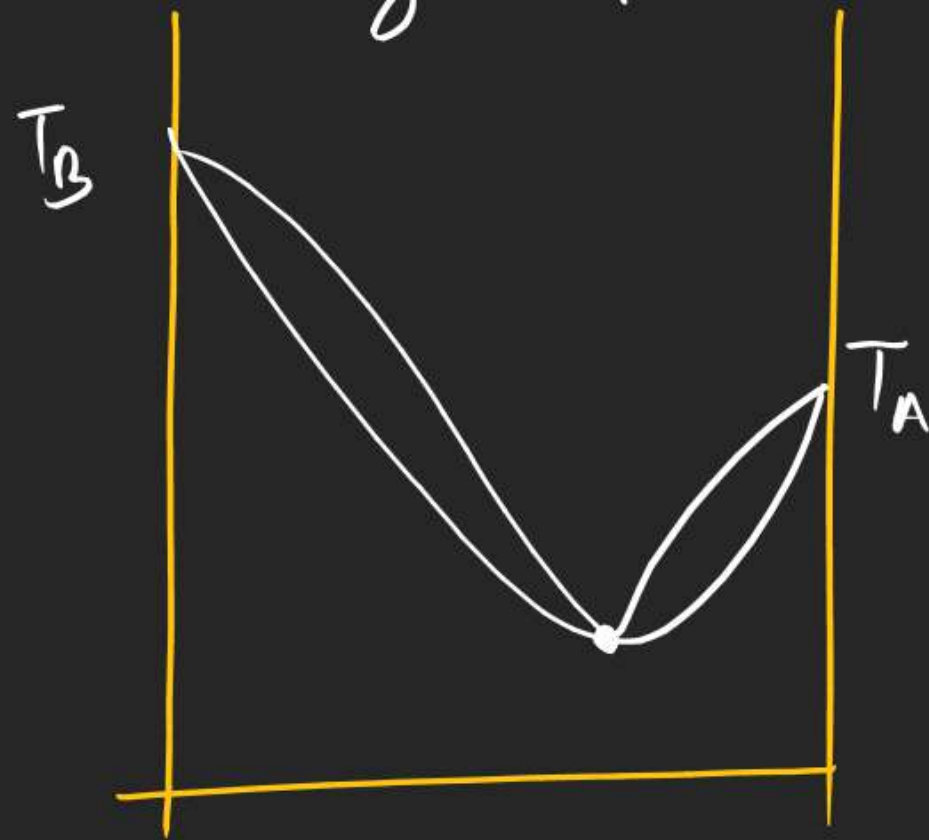
for an azeotrope

$$x_A = y_A$$

$$x_B = y_B$$

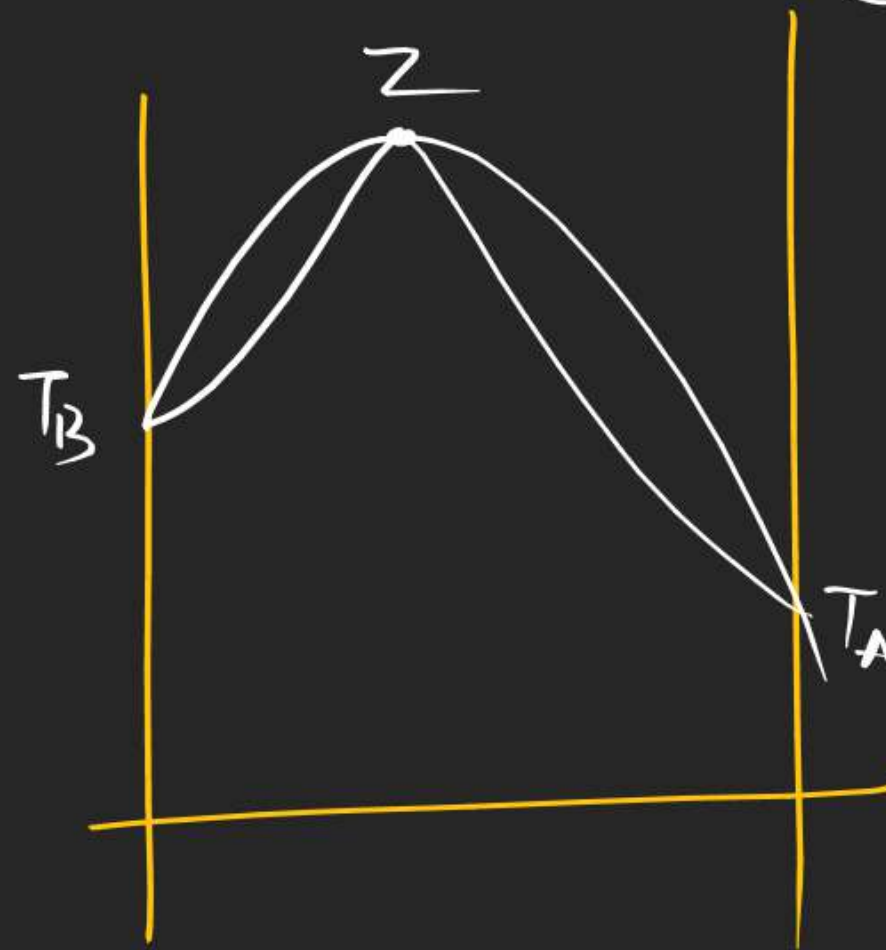
Azeotrope: It has sharp bpt like pure liq

minimum b.pt
azeotrope



five

max b.pt



-ive deviation

0-1
53-75