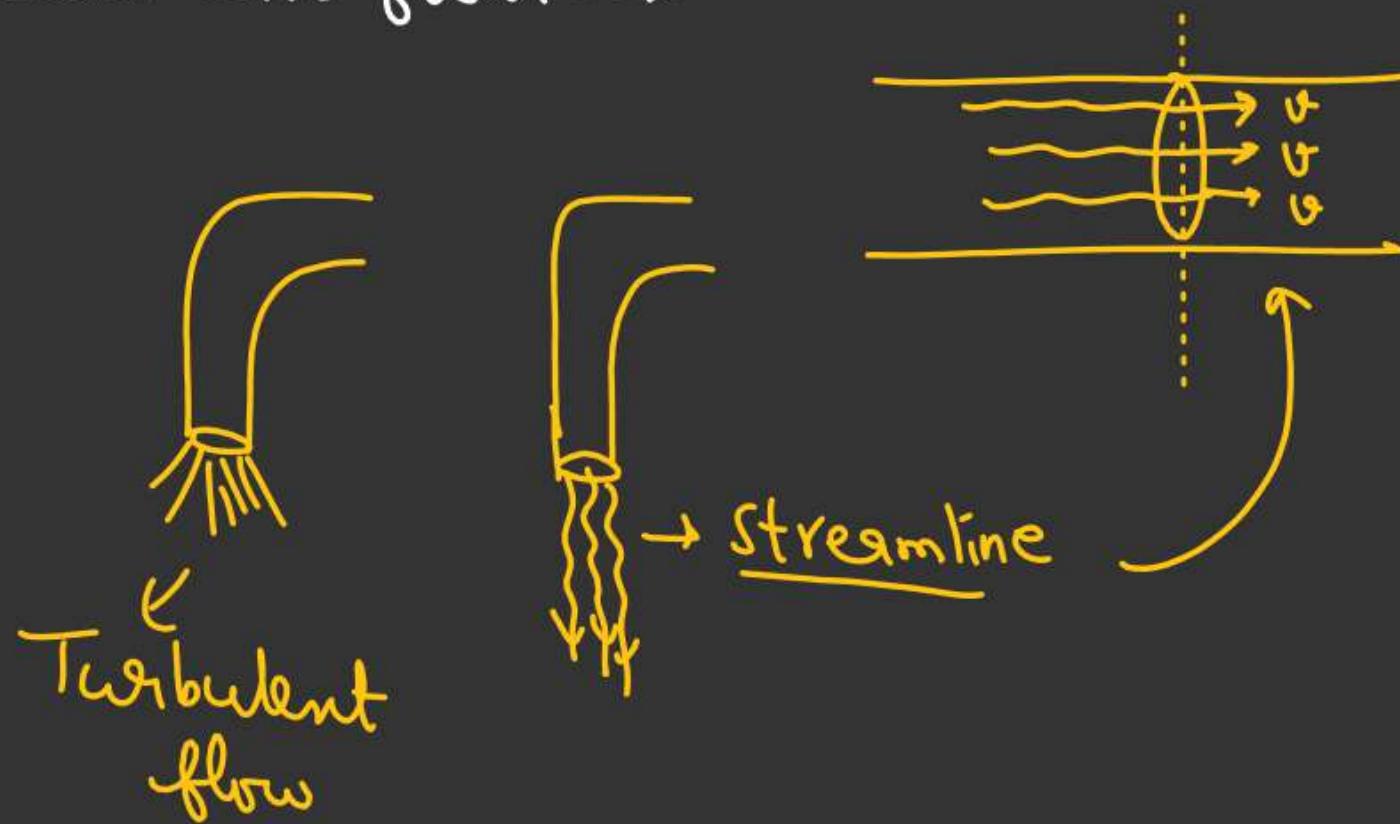


FLUID DYNAMICSAssumptions:-

For Ideal liquid

- In Compressible  $\rightarrow$  (Density of the liquid through-out its volume remain constant)
- Non - Viscidous.  $\rightarrow$  (Any two consecutive layer doesn't apply any tangential force)
- Stream line flow.  $\rightarrow$



FLUID DYNAMICS★ LAW OF CONTINUITY

(Based on Conservation of mass)

$$dm = \rho A_1 \underline{dl}_1 = \rho A_2 \underline{dl}_2$$

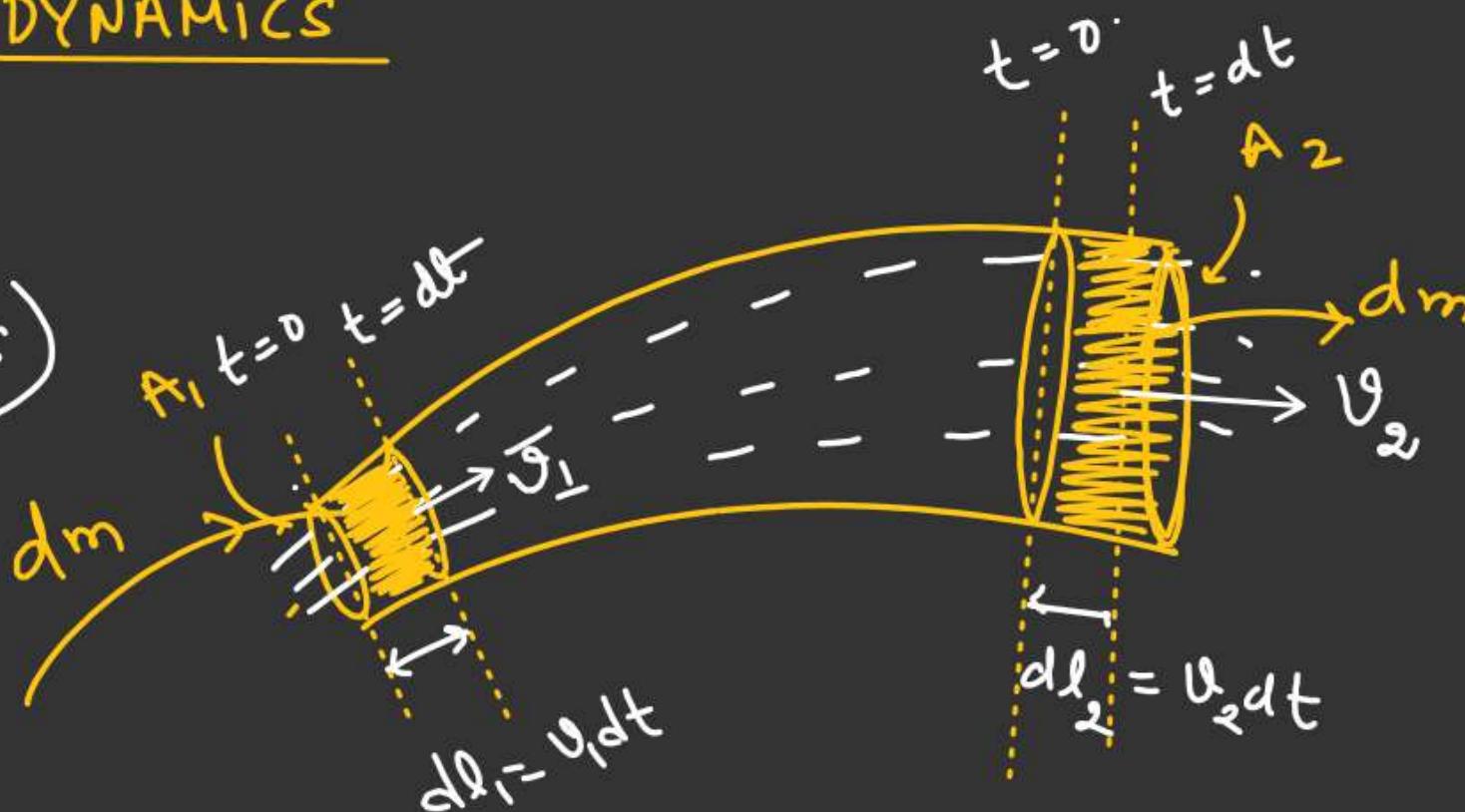
$$\Rightarrow \rho A_1 \vartheta_1 dt = \rho A_2 \vartheta_2 dt$$

$$\Rightarrow \boxed{A_1 \vartheta_1 = A_2 \vartheta_2}$$

$$\downarrow \quad \downarrow \\ m^2 \times \frac{m}{s} \\ \Downarrow \\ m^3/s$$

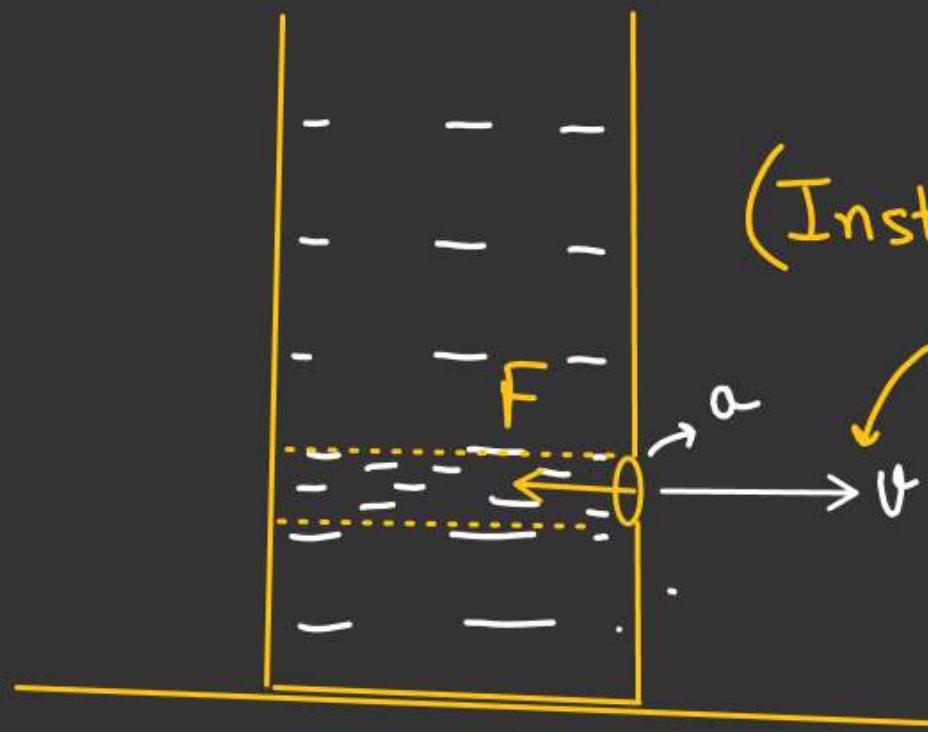
$$\boxed{A_1 \vartheta_1 = A_2 \vartheta_2 = \frac{dV}{dt}}$$

$\frac{dV}{dt}$  = Volume flow rate



FLUID DYNAMICS

Hydrostatic thrust when liquid exit from a Small hole



$a$  = Cross sectional  
area of hole.



By Continuity

$$\rho = \frac{m}{V}$$

$$\frac{dV}{dt} = C$$

$$V = \left( \frac{m}{\rho} \right)$$

$$V = \frac{1}{\rho} \left( \frac{dm}{dt} \right)$$

$$F = \frac{dp}{dt}$$

$$F = \frac{d(mv)}{dt}$$

$$F = v \left( \frac{dm}{dt} \right)$$

$$F = pav = \frac{dm}{dt}$$

$v$  → Relative  
to container

$$F = pav^2$$

$\rho$  = density of liquid  
 $a$  = Cross sectional area  
of hole.

FLUID DYNAMICS

Find net hydrostatic torque  
acting on the vessel.

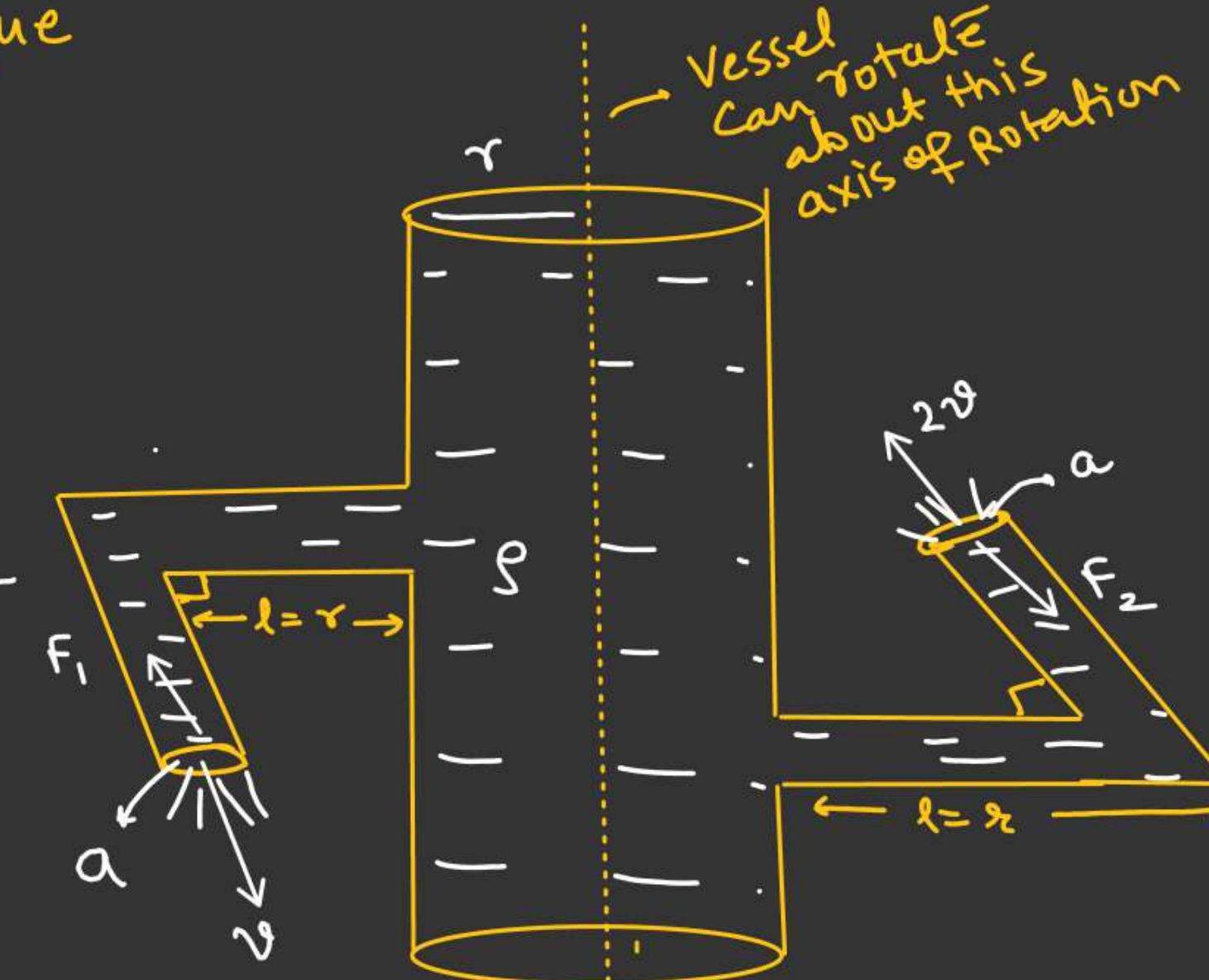
$$\tau = F_1(2r) + F_2(2r)$$

$$= (F_1 + F_2) 2r$$

$$= [ \rho a v^2 + \rho a (2v)^2 ] 2r$$

$$= (5 \rho a v^2) \cdot (2r)$$

$$= \underline{10 \rho a v^2 r} \quad \checkmark$$



FLUID DYNAMICSBERNOULLI'S EQUATION

→ (Based on Conservation of Energy)

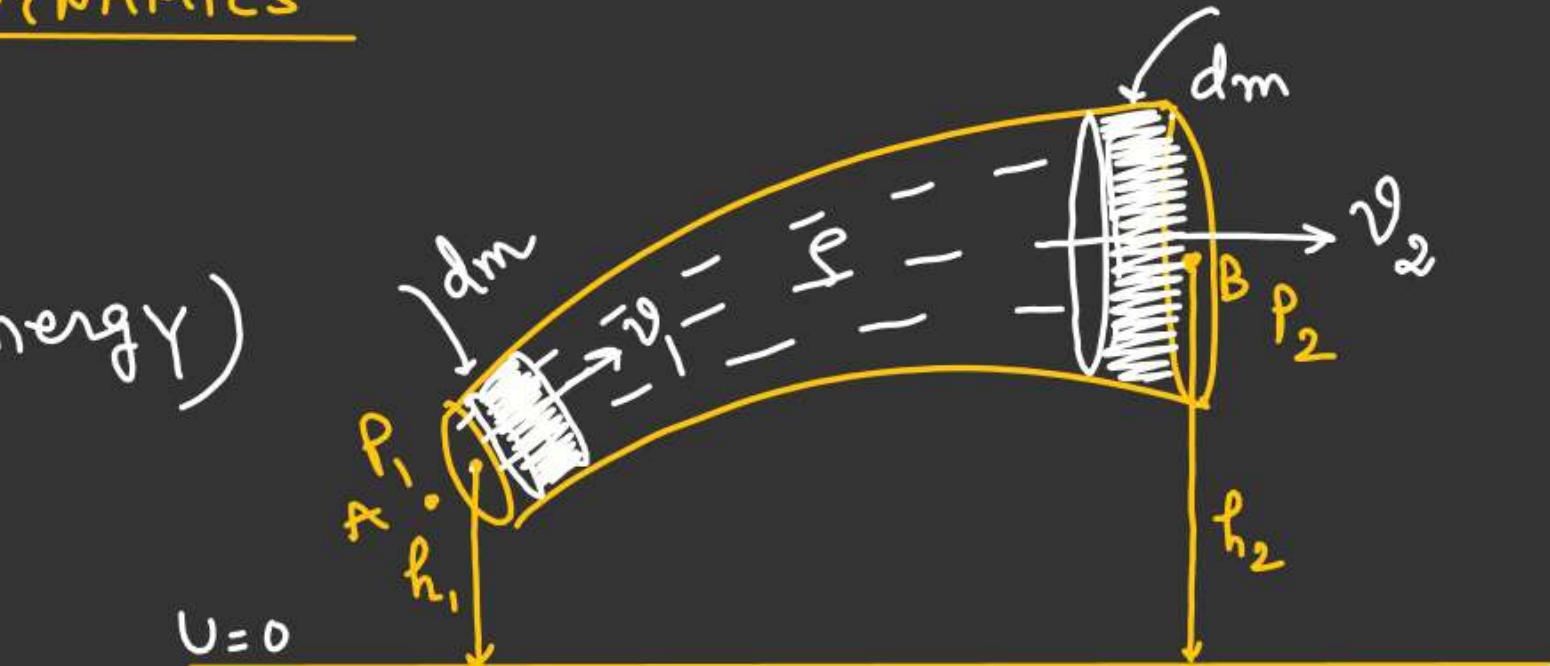
$$P + \frac{1}{2} \rho v^2 + \rho g h = C$$

$$\frac{1}{2} \rho v^2 = K.E \text{ per unit volume}$$

$$d(K.E) = \frac{1}{2} (dm) v^2$$

K.E per Unit Volume  $\frac{d(K.E)}{dV} = \frac{1}{2} \rho v^2$

$$\rho = \frac{m}{V}$$



$$P_1 + \rho g h_1 + \frac{1}{2} \rho v_1^2 = P_2 + \frac{1}{2} \rho v_2^2 + \rho g h_2$$

FLUID DYNAMICSApplication of Bernoulli'svelocity of Efflux

Bernoulli's b/w point 1 and 2

~~$$P_{atm} + \rho gh + \frac{1}{2} \rho v_1^2 = P_{atm} + \frac{1}{2} \rho v_2^2$$~~

$$\rho gh = \frac{1}{2} \rho (v_2^2 - v_1^2)$$

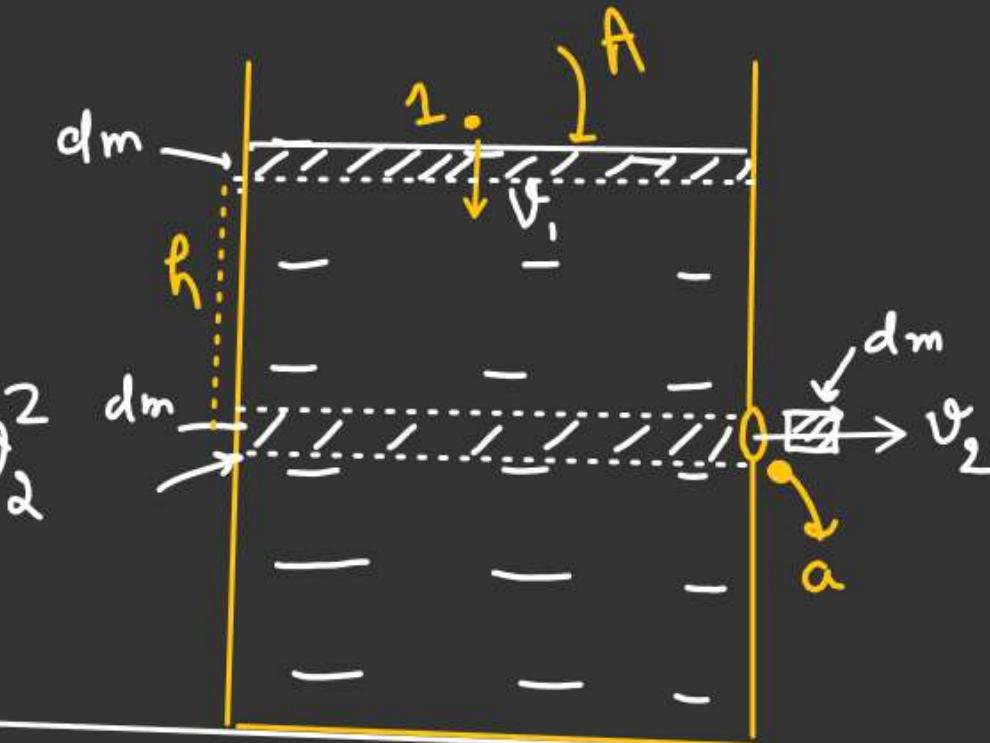
Law of Continuity

$$A v_1 = a v_2$$

$$v_1 = \left( \frac{a v_2}{A} \right)$$

$$\rho gh = \frac{1}{2} \rho v_2^2 \left( 1 - \frac{a^2}{A^2} \right)$$

$$\sqrt{\frac{2gh}{\left( 1 - \frac{a^2}{A^2} \right)}} = v_2$$



$A$  = Cross sectional area of container

$a$  = Cross sectional area of hole

FLUID DYNAMICSApplication of Bernoulli'svelocity of Efflux

$$\sqrt{\frac{2gh}{(1 - \frac{a^2}{A^2})}} = v_2$$

$h$  = depth of the orifice from the liquid surface

if

$$A \gg a$$

$$v_2 = \sqrt{2gh}$$

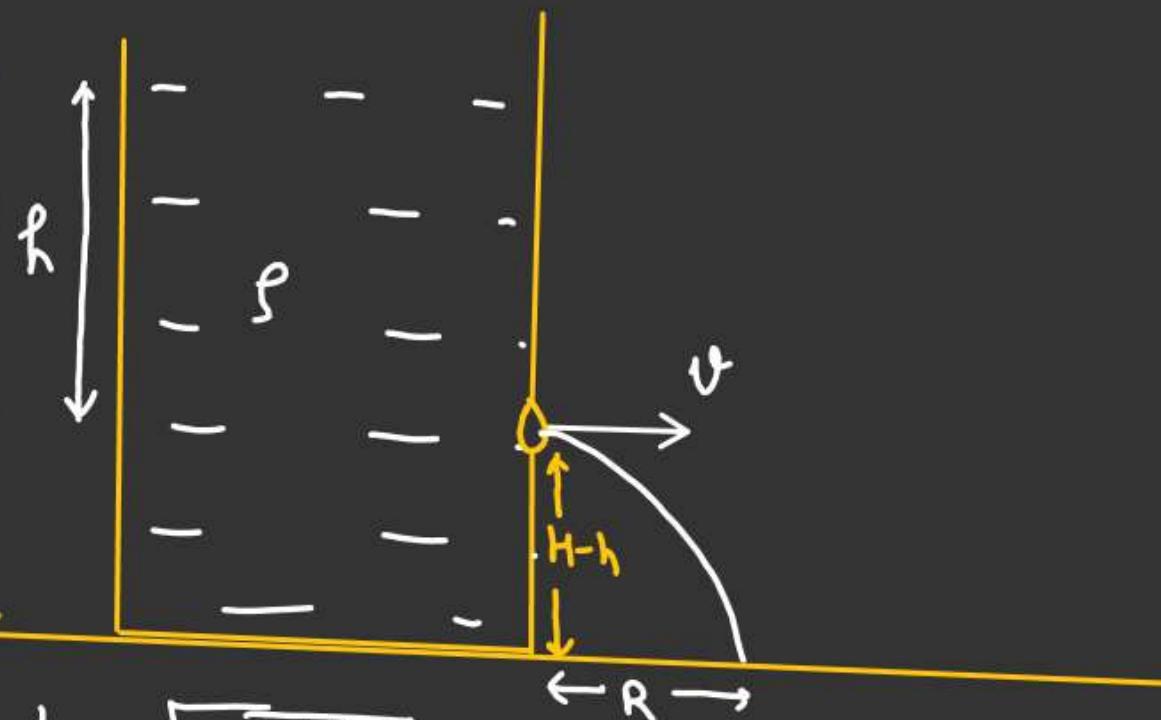
Velocity of Efflux

$$R = v \times t$$

$$R = (\sqrt{2gh}) \sqrt{\frac{2(H-h)}{g}}$$

$$R = 2\sqrt{h(H-h)}$$

$$R \rightarrow f(h)$$



$$t = \sqrt{\frac{2(H-h)}{g}}$$

For  $R$  to be max

$$\frac{dR}{dh} = 0$$

$$h = \frac{H}{2}$$

FLUID DYNAMICS

$$R_1 = 2\sqrt{h_1(H-h_1)}$$

$$R_1 = R_2 = R$$

$$R_2 = 2\sqrt{(H-h_2)(H-(H-h_2))}$$

$$= 2\sqrt{(H-h_2)h_2}$$

$$R_1 = R_2$$

$$h_1(H-h_1) = (H-h_2)h_2$$

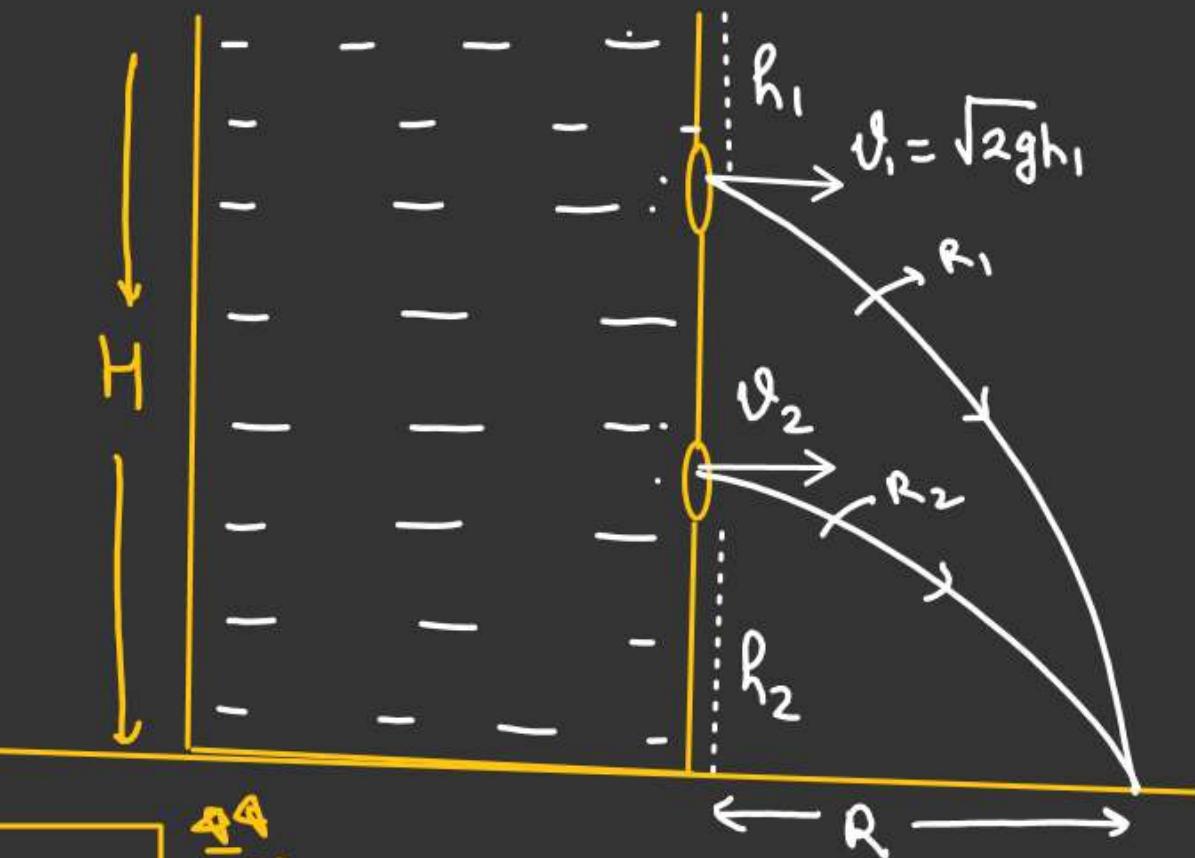
$$h_1H - h_2H = h_1^2 - h_2^2$$

$$(h_1-h_2)H = (h_1-h_2)(h_1+h_2)$$

$$(h_1-h_2)\left[H - \underline{\underline{R_1+h_2}}\right] = 0$$

$$\Downarrow \neq 0$$

$$V_2 = \sqrt{2g(H-h_2)}$$



$\boxed{h_1 = h_2}$

FLUID DYNAMICS

Bernoulli's in two or more than two immisible liquid

$$\frac{1 \rightarrow 4}{\cancel{P_{atm} + \rho_1 gh_1 + \rho_2 gh_2 + \rho_3 gh_3} = \cancel{P_{atm}} + \frac{1}{2} \rho_3 v^2}$$

$$v = \sqrt{\frac{2g(\rho_1 h_1 + \rho_2 h_2 + \rho_3 h_3)}{\rho_3}}$$

