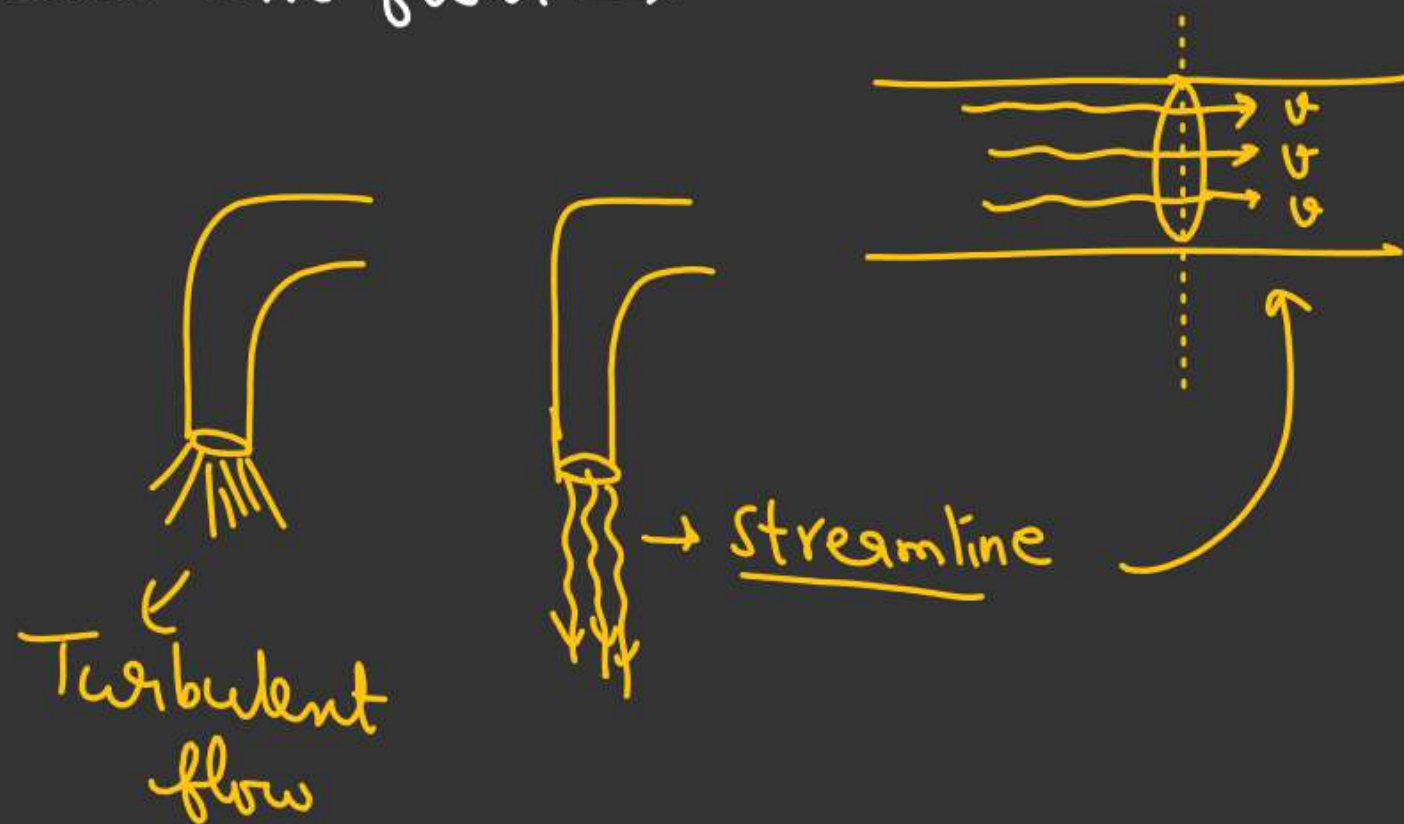


Assumptions:-

For Ideal liquid

- Incompressible  $\rightarrow$  (Density of the liquid through-out its volume remain constant)
- Non-Viscous.  $\rightarrow$  (Any two consecutive layers doesn't apply any tangential force)
- Stream line flow.  $\rightarrow$



★ LAW OF CONTINUITY

(Based on Conservation of mass)

$$dm = \rho A_1 dl_1 = \rho A_2 dl_2$$

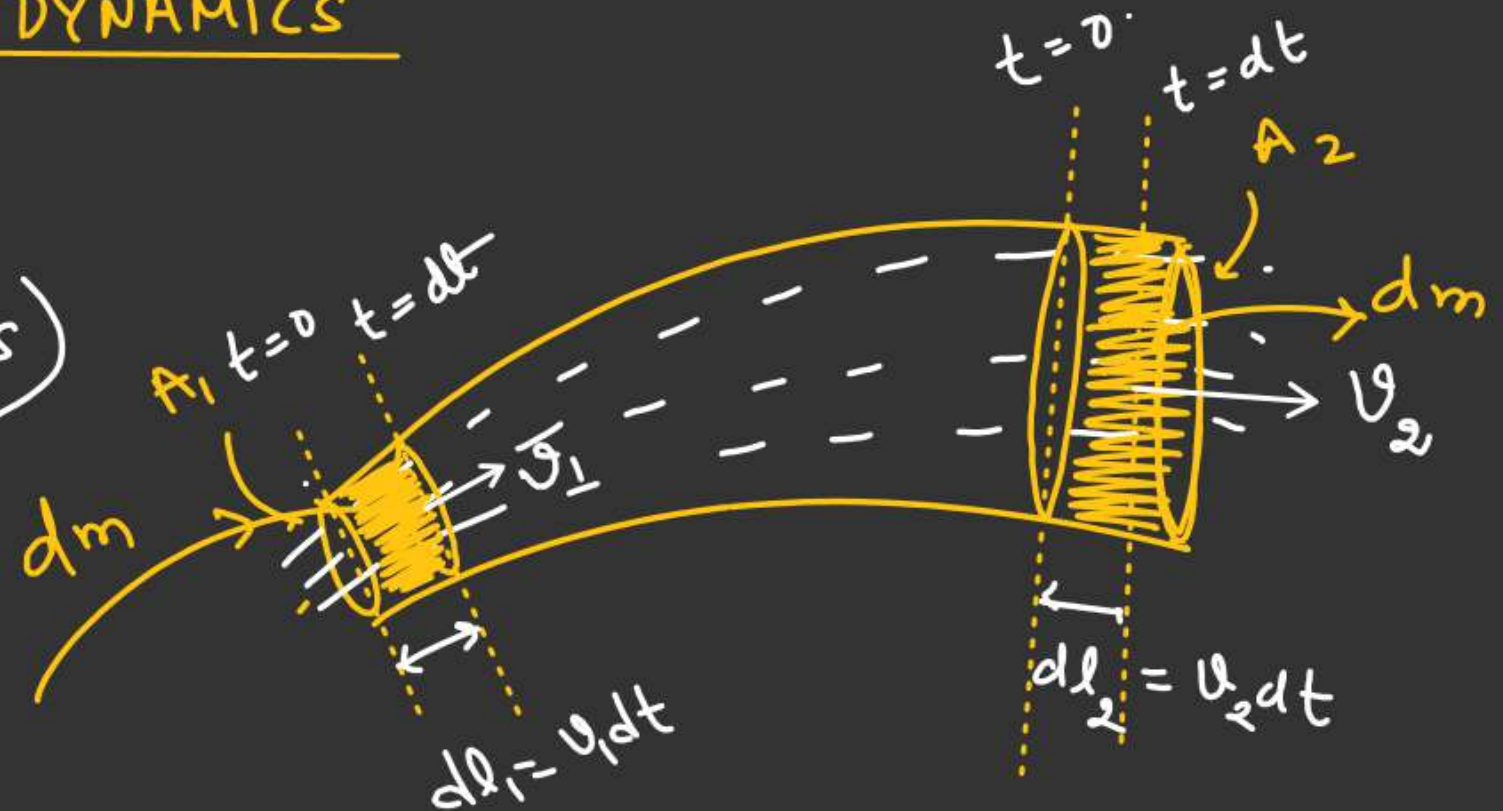
$$\Rightarrow \rho A_1 v_1 dt = \rho A_2 v_2 dt$$

$$\Rightarrow \boxed{A_1 v_1 = A_2 v_2}$$

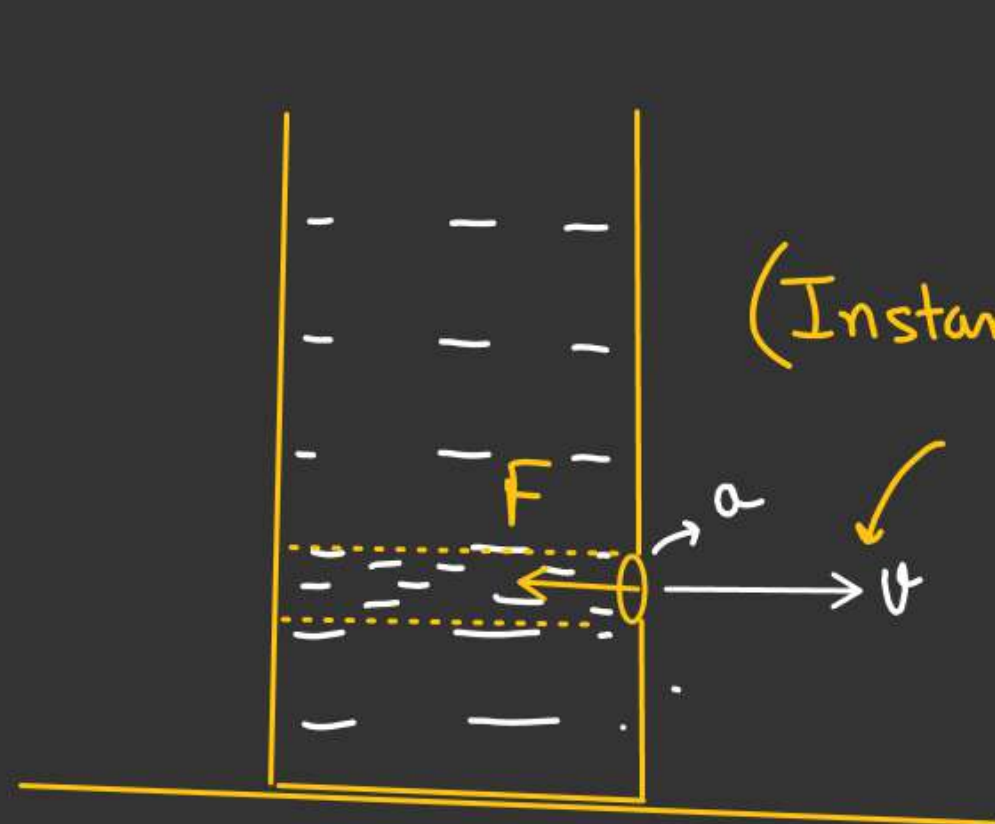
$$\begin{array}{c} \downarrow \quad \downarrow \\ m^2 \times \frac{m}{s} \\ \Downarrow \\ m^3/s \end{array}$$

$$\boxed{A_1 v_1 = A_2 v_2 = \frac{dV}{dt}}$$

$$\frac{dV}{dt} = \text{Volume flow rate}$$





Hydrostatic thrust when liquid exit from a small hole

$a$  = cross-sectional area of hole.



By Continuity

$$\frac{dV}{dt} = c$$

$$V = \left(\frac{m}{\rho}\right)$$

$$V = \frac{1}{\rho} \left(\frac{dm}{dt}\right)$$

$$\rho a v = \frac{dm}{dt}$$

$$\left(\rho = \frac{m}{V}\right)$$

$$F = \frac{dp}{dt}$$

$$F = \frac{d(mv)}{dt}$$

$$F = v \left(\frac{dm}{dt}\right)$$

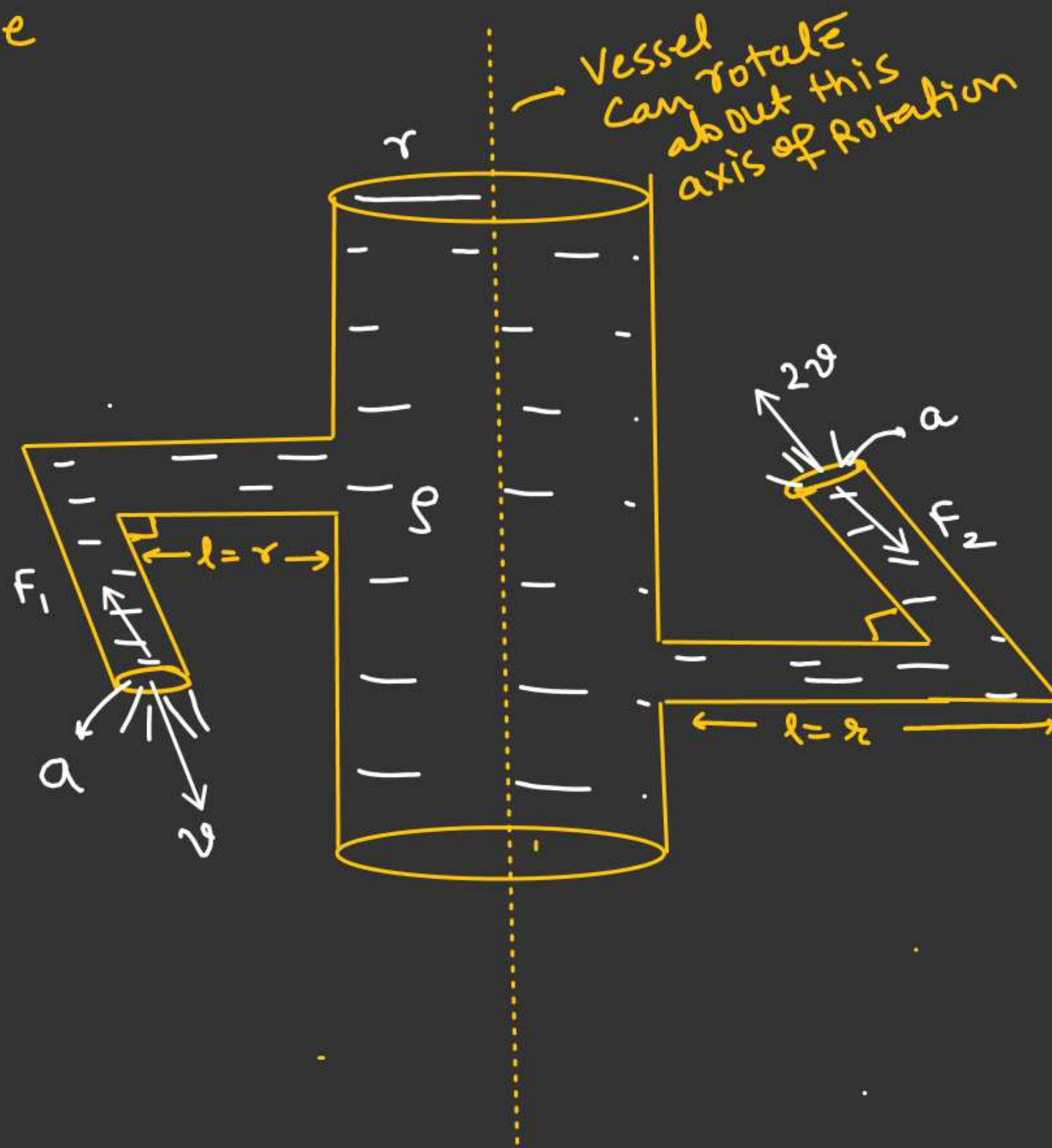
$$F = \rho a v^2$$

$v \rightarrow$  Relative to container ✓

$\rho$  = density of liquid  
 $a$  = cross-sectional area of hole.

Find net hydrostatic torque acting on the vessel.

$$\begin{aligned}
 T &= F_1(2r) + F_2(2r) \\
 &= (F_1 + F_2) 2r \\
 &= [\rho a v^2 + \rho a (2v)^2] 2r \\
 &= (5\rho a v^2) \cdot (2r) \\
 &= \underline{10\rho a v^2 r} \quad \checkmark
 \end{aligned}$$





# ★★: BERNOULLI'S EQUATION

↳ (Based on Conservation of Energy)

$$P + \frac{1}{2} \rho v^2 + \rho gh = C$$

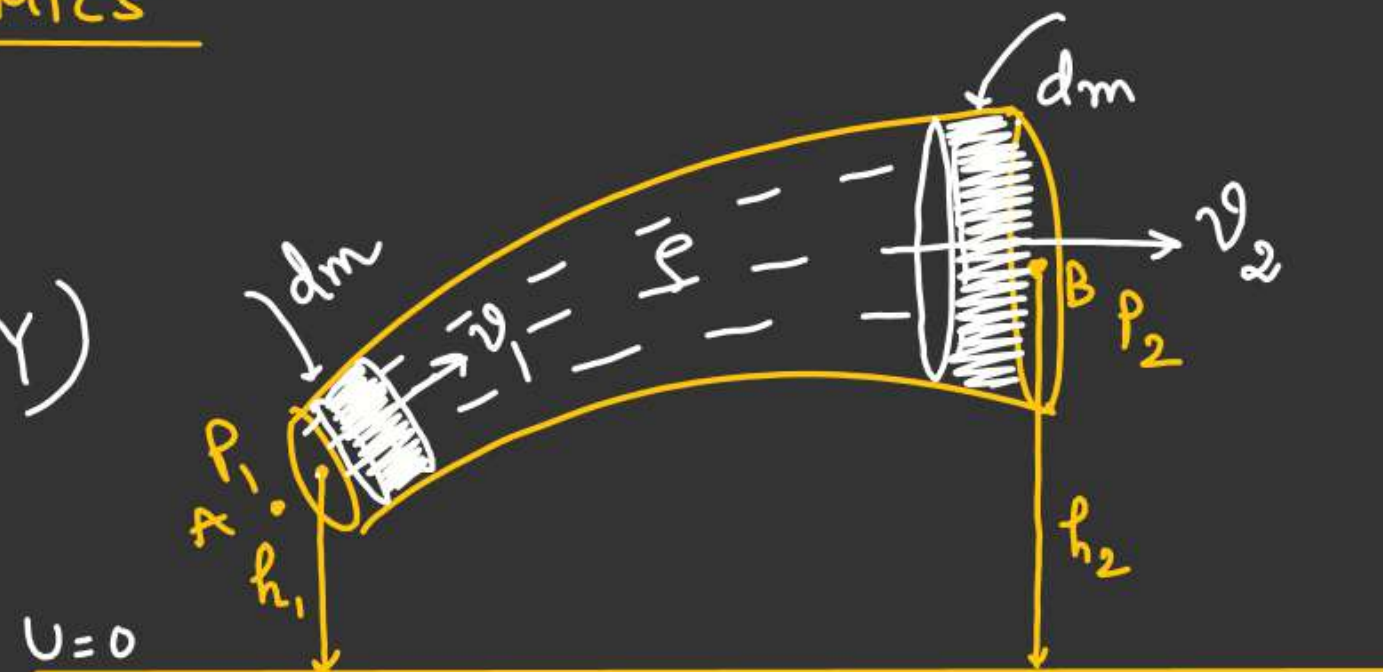
$$\frac{1}{2} \rho v^2 = \text{K.E per unit volume}$$

$$d(\text{K.E}) = \frac{1}{2} (dm) v^2$$

K.E per unit volume ←  $\frac{d(\text{K.E})}{dV} = \frac{1}{2} \rho v^2$

$$av = \frac{dV}{dt} = \frac{1}{\rho} \frac{dm}{dt}$$

$$\rho \frac{dV}{dt} = dm$$



$$P_1 + \rho gh_1 + \frac{1}{2} \rho v_1^2 = P_2 + \frac{1}{2} \rho v_2^2 + \rho gh_2$$

Application of Bernoulli'svelocity of Efflux

Bernoulli's b/w point 1 and 2

$$P_{atm} + \rho gh + \frac{1}{2} \rho v_1^2 = P_{atm} + \frac{1}{2} \rho v_2^2$$

$$\rho gh = \frac{1}{2} \rho (v_2^2 - v_1^2)$$

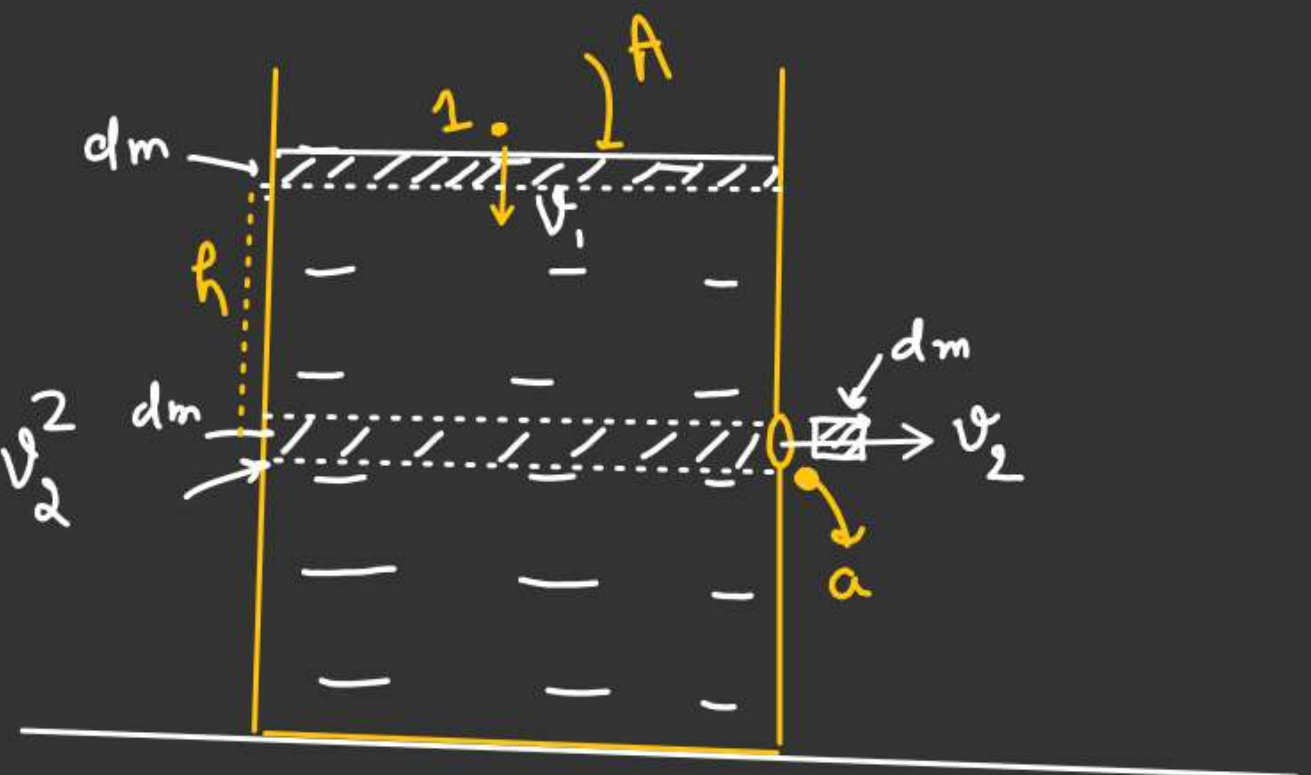
Law of Continuity

$$A v_1 = a v_2$$

$$v_1 = \left( \frac{a v_2}{A} \right)$$

$$\rho gh = \frac{1}{2} \rho v_2^2 \left( 1 - \frac{a^2}{A^2} \right)$$

$$\sqrt{\frac{2gh}{\left( 1 - \frac{a^2}{A^2} \right)}} = v_2$$



A = Cross-sectional area of container

a = Cross-sectional area of hole



Application of Bernoulli's

\*\*:

velocity of Efflux

$$\sqrt{\frac{2gh}{(1 - \frac{a^2}{A^2})}} = v_2$$

if

$$A \gg a$$

$$v_2 = \sqrt{2gh}$$

↓  
velocity of Efflux

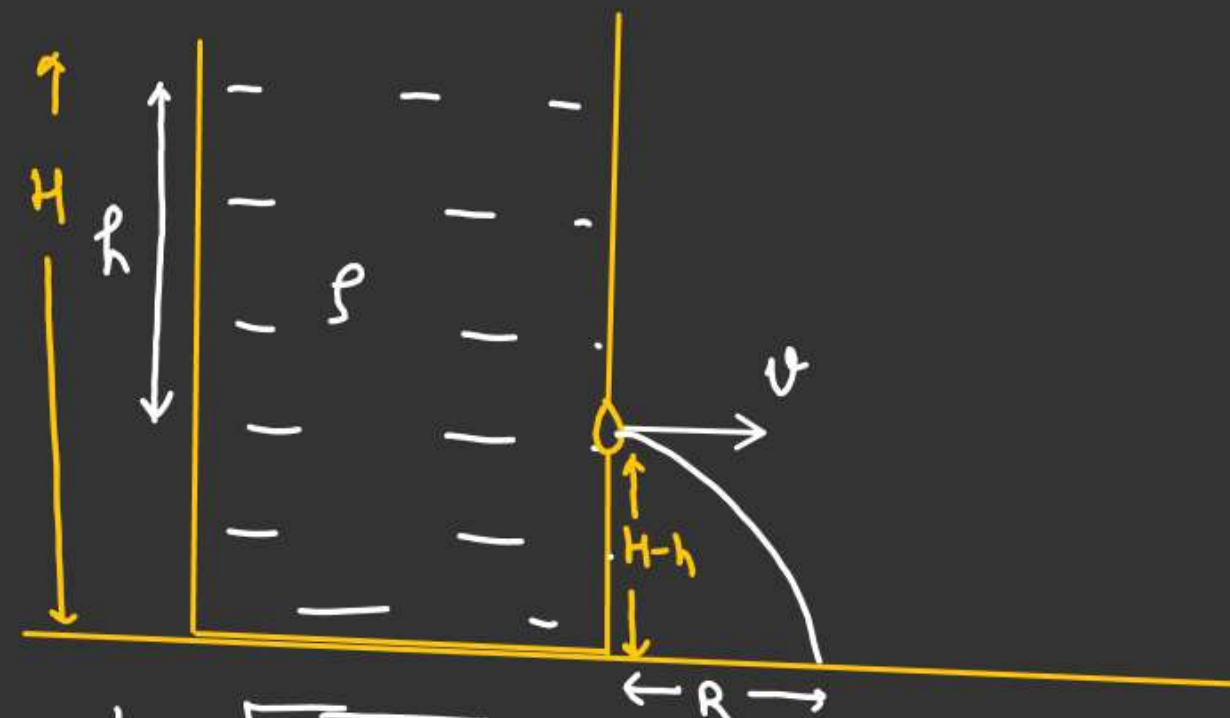
$h$  = depth of the  
orifice from  
the liquid surface

$$R = v \times t$$

$$R = (\sqrt{2gh}) \sqrt{\frac{2(H-h)}{g}}$$

$$R = 2\sqrt{h(H-h)}$$

$$R \rightarrow f(h)$$



$$t = \sqrt{\frac{2(H-h)}{g}}$$

For  $R$  to be max

$$\frac{dR}{dh} = 0$$

$\Rightarrow$

$$h = \frac{H}{2}$$

FLUID DYNAMICS

$$R_1 = 2\sqrt{h_1(H-h_1)}$$

$$R_2 = 2\sqrt{(H-h_2)(H-(H-h_2))}$$

$$= 2\sqrt{(H-h_2)h_2}$$

$$R_1 = R_2$$

$$h_1(H-h_1) = (H-h_2)h_2$$

$$h_1H - h_2H = h_1^2 - h_2^2$$

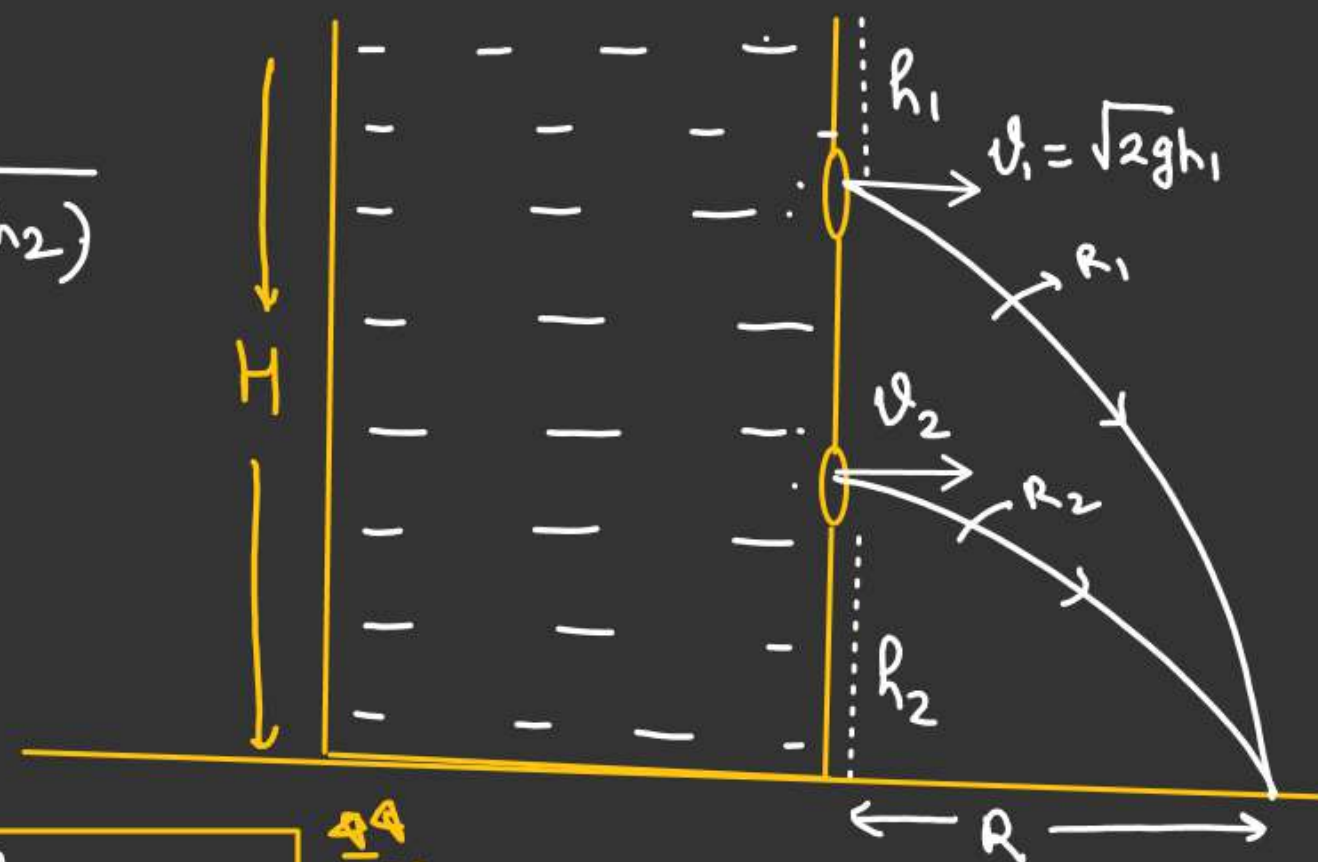
$$(h_1 - h_2)H = (h_1 - h_2)(h_1 + h_2)$$

$$(h_1 - h_2) \underline{[H - (h_1 + h_2)]} = 0$$

$\Downarrow$   
 $\neq 0$

$$R_1 = R_2 = R$$

$$v_2 = \sqrt{2g(H-h_2)}$$



$$h_1 = h_2$$



★: Bernoulli's in two or more than two immisible liquid

$$\frac{1 \rightarrow 4}{P_{atm} + \cancel{P_1 g h_1} + \cancel{P_2 g h_2} + P_3 g h_3 = \cancel{P_{atm}} + \frac{1}{2} P_3 v^2}$$

$$v = \sqrt{\frac{2g(P_1 h_1 + P_2 h_2 + P_3 h_3)}{P_3}}$$

