

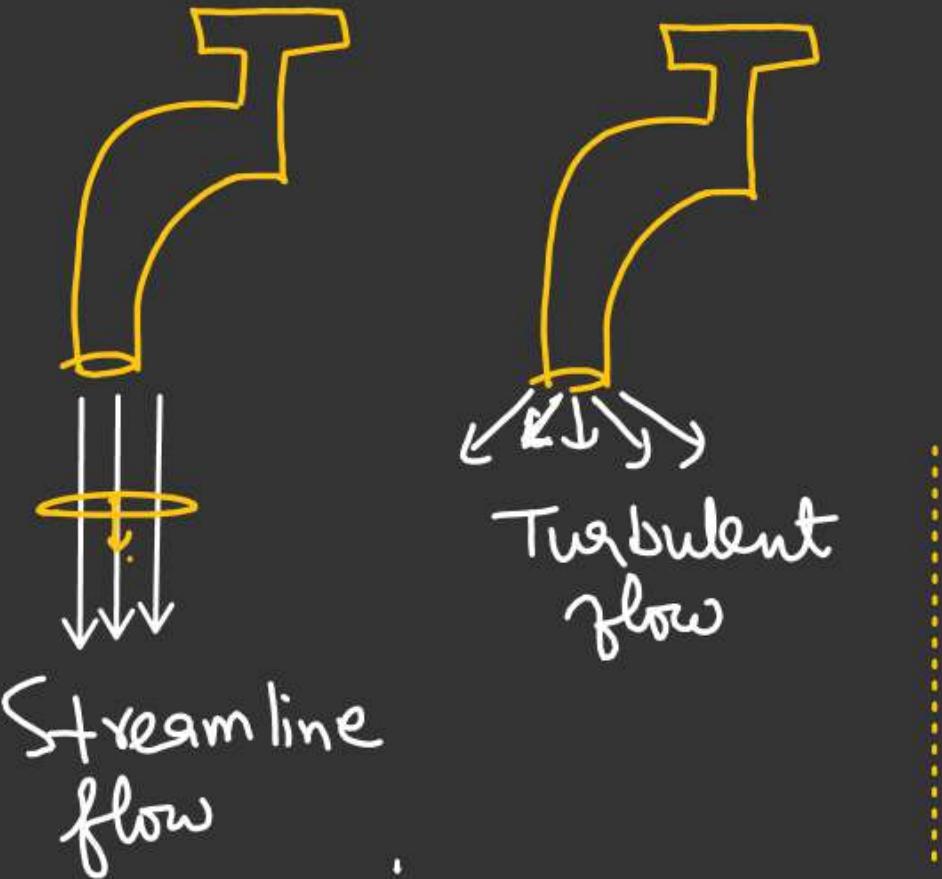


Fluid dynamics

Assumptions:-

- ① Fluid is Ideal
 - Incompressible
 - Non-viscous.

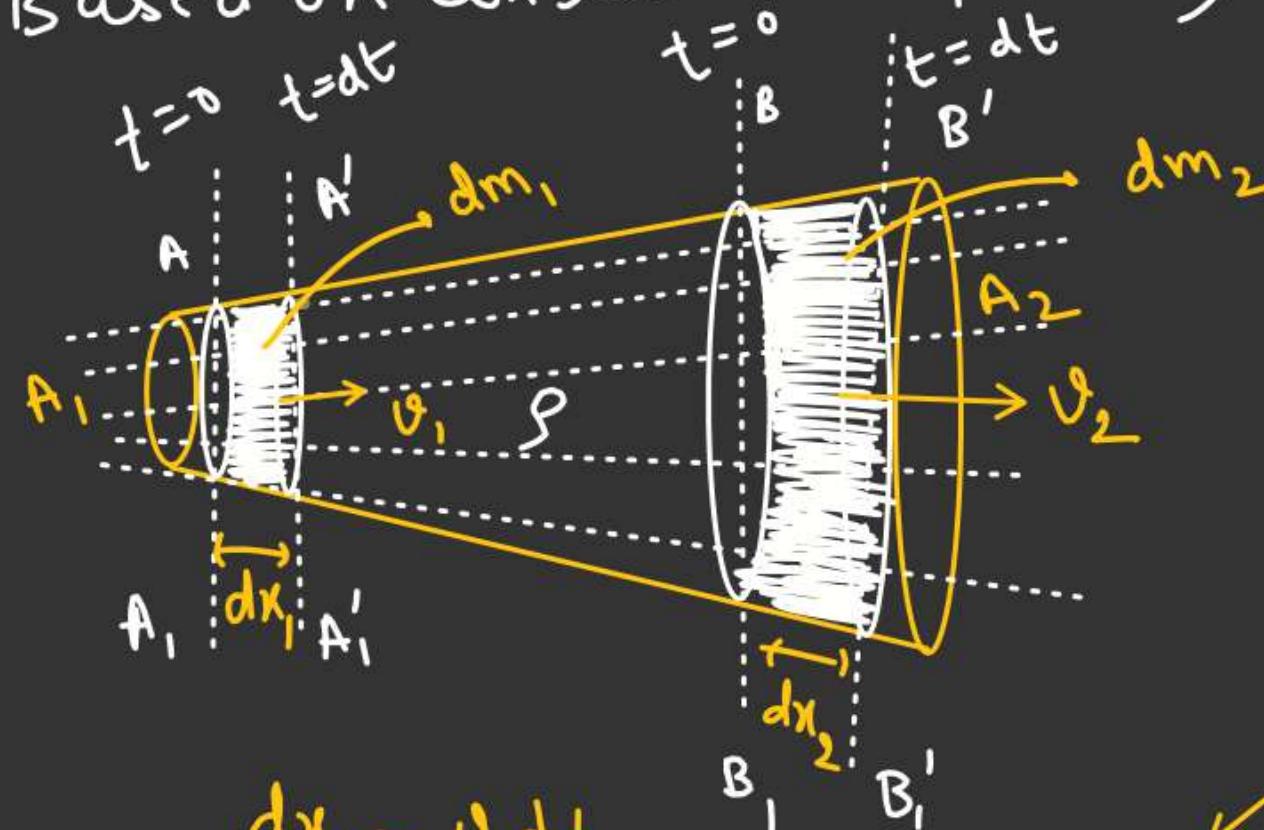
- ② Streamline flow ✓
 - ↳ All liquid layers have parallel flow.
 - No interruption of one layer with other
 - Velocity of each particle passing through any point remain constant with time.





law of Continuity

(Based on Conservation of mass)



$$dx_1 = v_1 dt$$

$$dx_2 = v_2 dt$$

$$\rho = \frac{m}{V}$$

$$V = \frac{m}{\rho}$$

By mass conservation

$$dm_1 = dm_2$$

$$\rho A_1 dx_1 = \rho A_2 dx_2$$

$$\cancel{\rho A_1 v_1 dt} = \cancel{\rho A_2 v_2 dt}$$

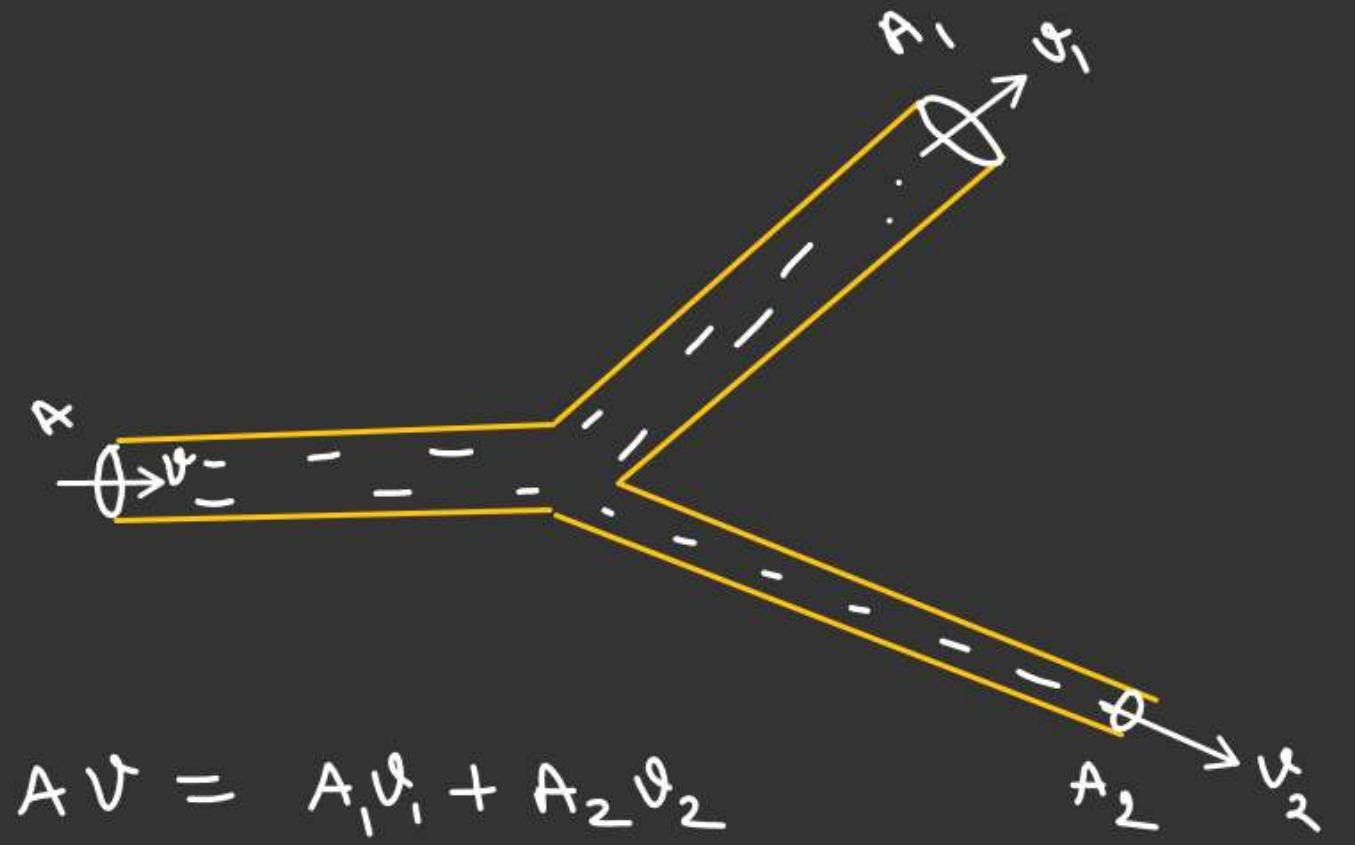
$$A_1 v_1 = A_2 v_2$$

$$m^2 \times \frac{m}{s} \rightarrow \frac{m^3}{s}$$

Volume per Second.

$$\frac{1}{\rho} \frac{dm}{dt} = \frac{dV}{dt} = A_1 v_1 = A_2 v_2$$

Volume flow rate

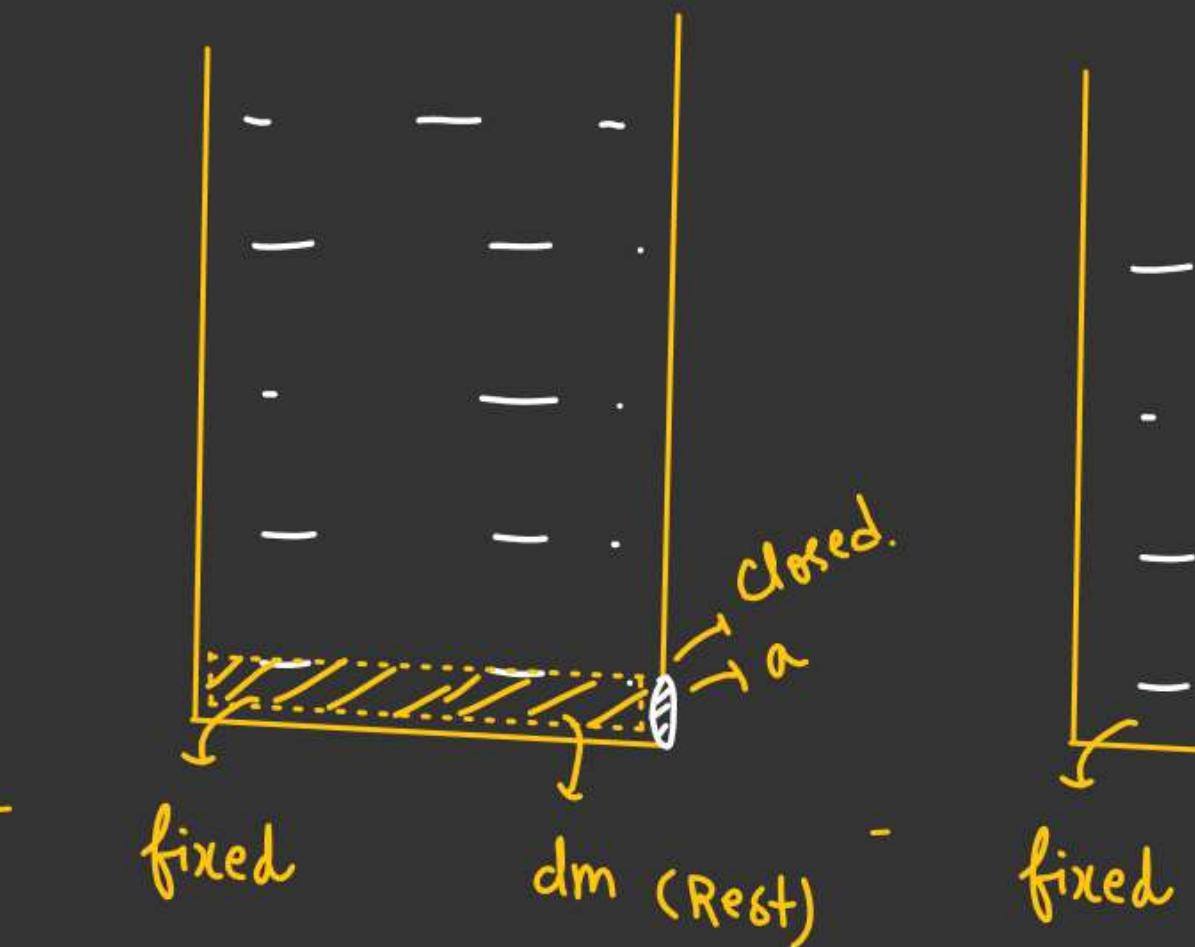


$$A = A_1 v_1 + A_2 v_2$$



Force acting on a vessel when liquid coming out from a hole

$$p = \rho g$$



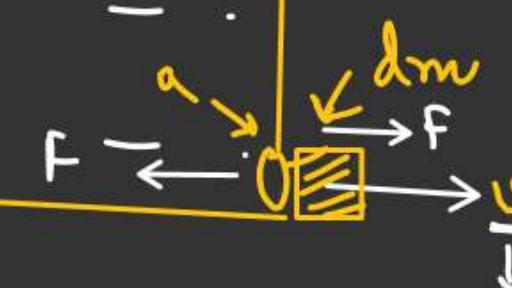
$$F = \frac{dp}{dt} = \rho \left(\frac{dm}{dt} \right) v$$

By Continuity

$$\frac{dV}{dt} = \frac{1}{\rho} \left(\frac{dm}{dt} \right) = av$$

$$\frac{dm}{dt} = \rho av$$

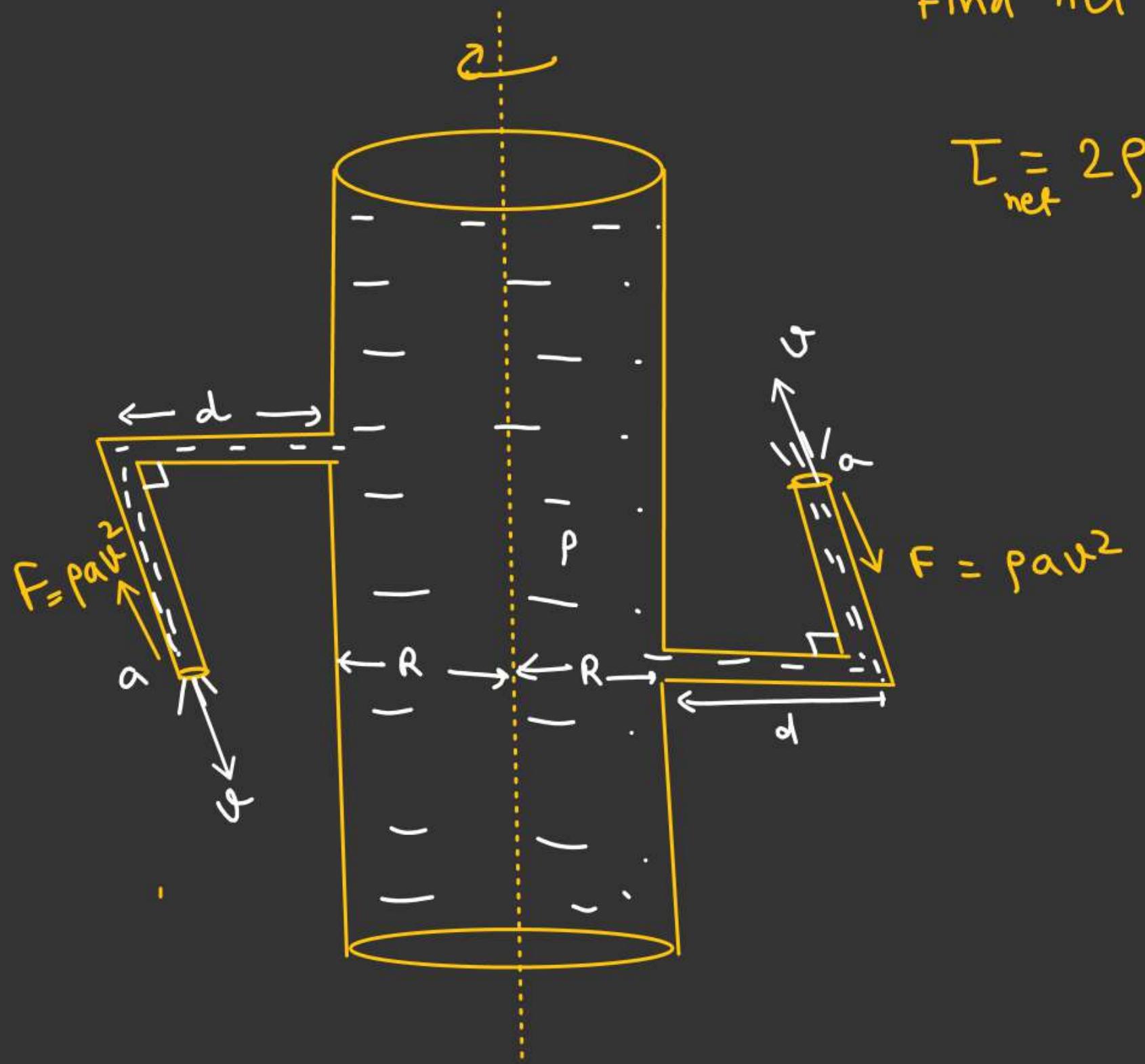
$$F = \rho av^2$$



(Relative to vessel) thrust

a = cross-section area of hole from where liquid exit

Find net torque on the vessel



$$\tau_{\text{net}} = 2 \rho a v^2 (R + d)$$

BERNOULLI'S EQUATION

(Based on Conservation of Energy)

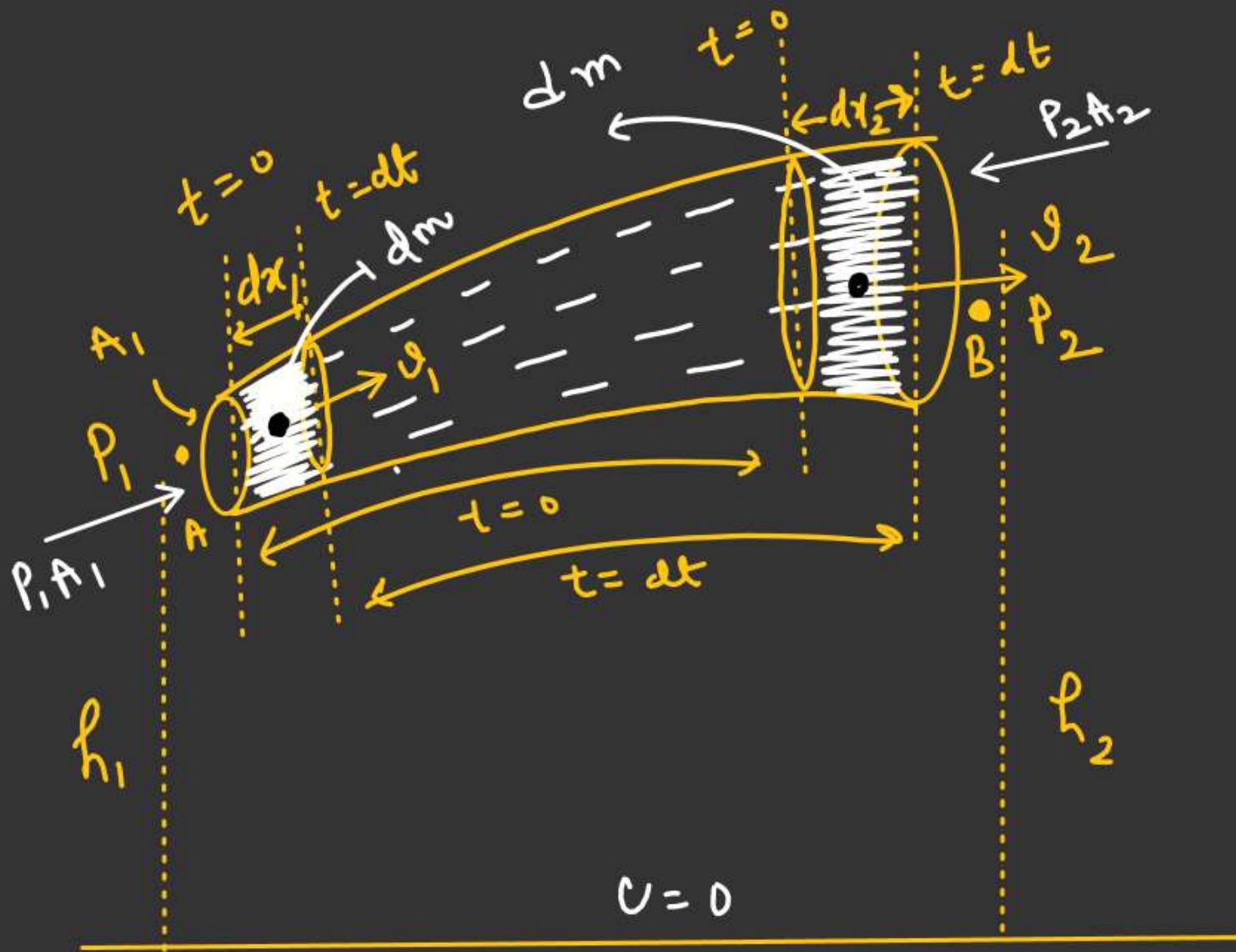
By Work-Energy theorem:

$$W_{\text{pressure force}} + W_{\text{gravity}} = \Delta K.E$$

$$\begin{aligned} dW_{\text{pressure force}} &= P_1 A_1 dx_1 - P_2 A_2 dx_2 \\ &= P_1 A_1 \underline{v_1 dt} - P_2 A_2 \underline{v_2 dt} \end{aligned}$$

$$(A_1 v_1 = A_2 v_2 = \frac{dV}{dt})$$

$$= \underline{(P_1 - P_2) dV}$$



$$\begin{aligned} dW_{\text{gravity}} &= -dU \\ &= dU_i - dU_f \\ &= dm g (h_1 - h_2) \end{aligned}$$

$$dm = (\rho dV)$$

$$dW_{\text{gravity}} = \rho g (h_1 - h_2) dV$$

$$dW_{\text{pressure force}} + W_{\text{gravity}} = dK.E$$

$$(P_1 - P_2) dV + \rho g (h_1 - h_2) dV = \frac{1}{2} \rho (v_2^2 - v_1^2) dV$$

$$P_1 + \rho g h_1 + \frac{1}{2} \rho v_1^2 = P_2 + \rho g h_2 + \frac{1}{2} \rho v_2^2$$

$$d(K.E) = \frac{1}{2} dm (v_2^2 - v_1^2)$$

$$= \frac{1}{2} \rho (v_2^2 - v_1^2) dV$$

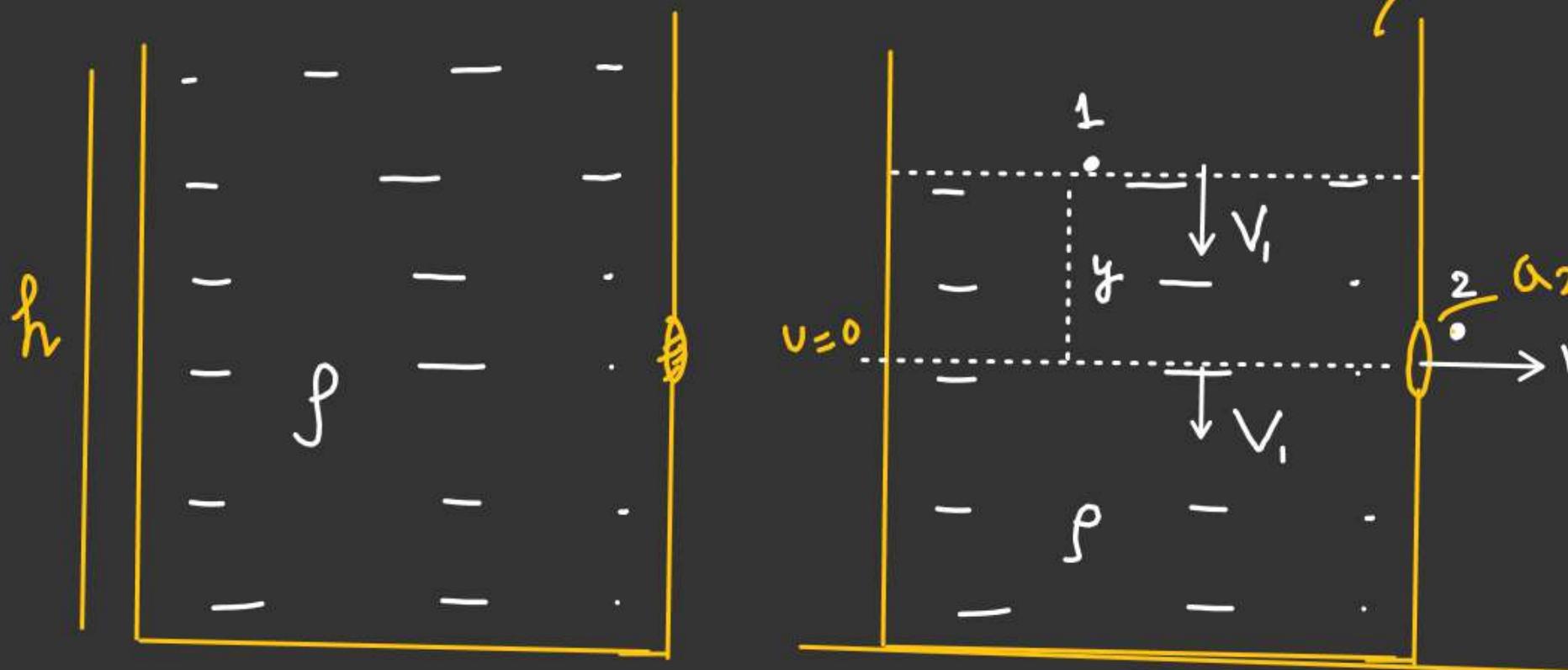
$$\frac{d(K.E)}{dV} = \frac{1}{2} \rho (v_2^2 - v_1^2)$$

\downarrow
K.E per
Unit volume

P_1 & $P_2 \rightarrow$ Work
done by
pressure force
per Unit Volume
i.e. Pressure Energy
per Unit Volume



Velocity of efflux



A_1 ((prosectional area of vessel)

Bernoulli's equation

b/w 1 & 2.

$$P_1 = P_2 = \underline{P_{atm}}$$

$$\cancel{P_1 + \rho g y + \frac{1}{2} \rho v_1^2} = \cancel{P_2 + \frac{1}{2} \rho v_2^2}$$

$$\frac{1}{2} \rho (v_2^2 - v_1^2) = \rho gy$$

$$v_2^2 - v_1^2 = 2gy$$

By continuity

$$A_1 v_1 = a_2 v_2$$

$$v_1 = \left(\frac{a_2 v_2}{A_1} \right)$$

$$v_2^2 \left(1 - \frac{a_2^2}{A_1^2} \right) = 2gy$$

$$v_2 = \sqrt{\frac{2gy}{\left(1 - \frac{a_2^2}{A_1^2} \right)}}$$



Velocity of Efflux

$$v_2 = \sqrt{\frac{2gy}{\left(1 - \frac{a_2^2}{A_1^2}\right)}}$$

if $A_1 \gg a_2$

$$\frac{a_2}{A_1} \rightarrow 0$$

$$v_2 = \sqrt{2gy}$$

Velocity of efflux

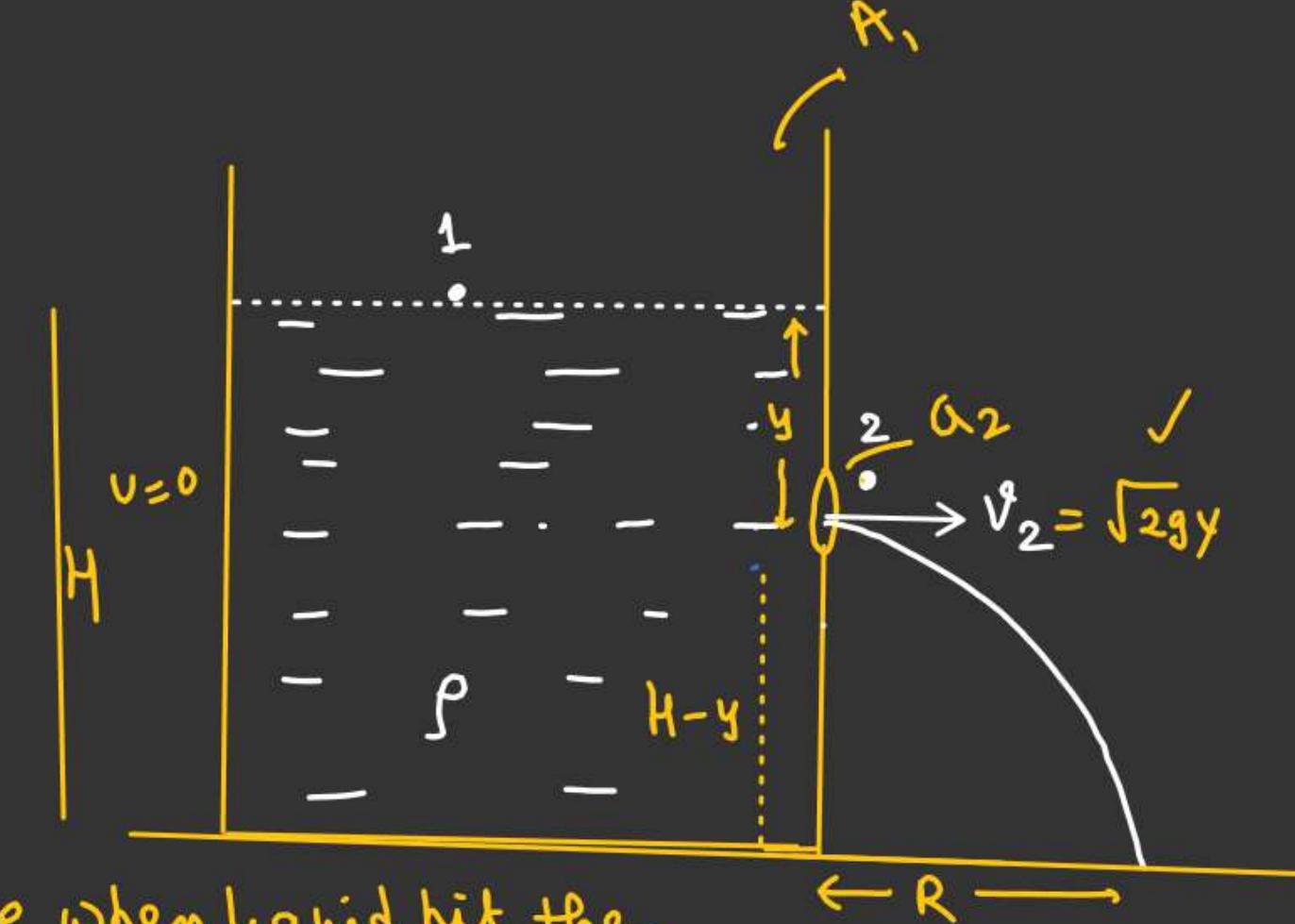
y = depth of orifice (Small hole)
from liquid surface

Time when liquid hit the ground =

$$\sqrt{\frac{2(H-y)}{g}}$$

$$R = \sqrt{2gy} \times \sqrt{\frac{2(H-y)}{g}}$$

$$R = 2 \sqrt{y(H-y)}$$



For Range to be maximum:

$$R = 2 \sqrt{y(H-y)}$$

$$\left(\frac{dR}{du} \times \frac{du}{dy} \right)$$

R_{max}

$$\frac{dR}{dy} = \cancel{2} \frac{1}{\sqrt{y(H-y)}} \quad \frac{d}{dy} (Hy - y^2)$$

↓

$$0 = \frac{1}{\sqrt{y(H-y)}} (H - 2y)$$

$$R_{\max} = 2 \sqrt{\frac{H}{2} \left(H - \frac{H}{2} \right)}$$

$$R_{\max} = H$$

$$y = \frac{H}{2}$$

For R to be same bind
relation b/w h_1 , h_2 & H

$$\sqrt{2gh_1} \times \sqrt{\frac{2(H-h_1)}{g}} = \sqrt{2g(H-h_2)} \times \sqrt{\frac{2h_2}{g}}$$

$$h_1(H-h_1) = h_2(H-h_2)$$

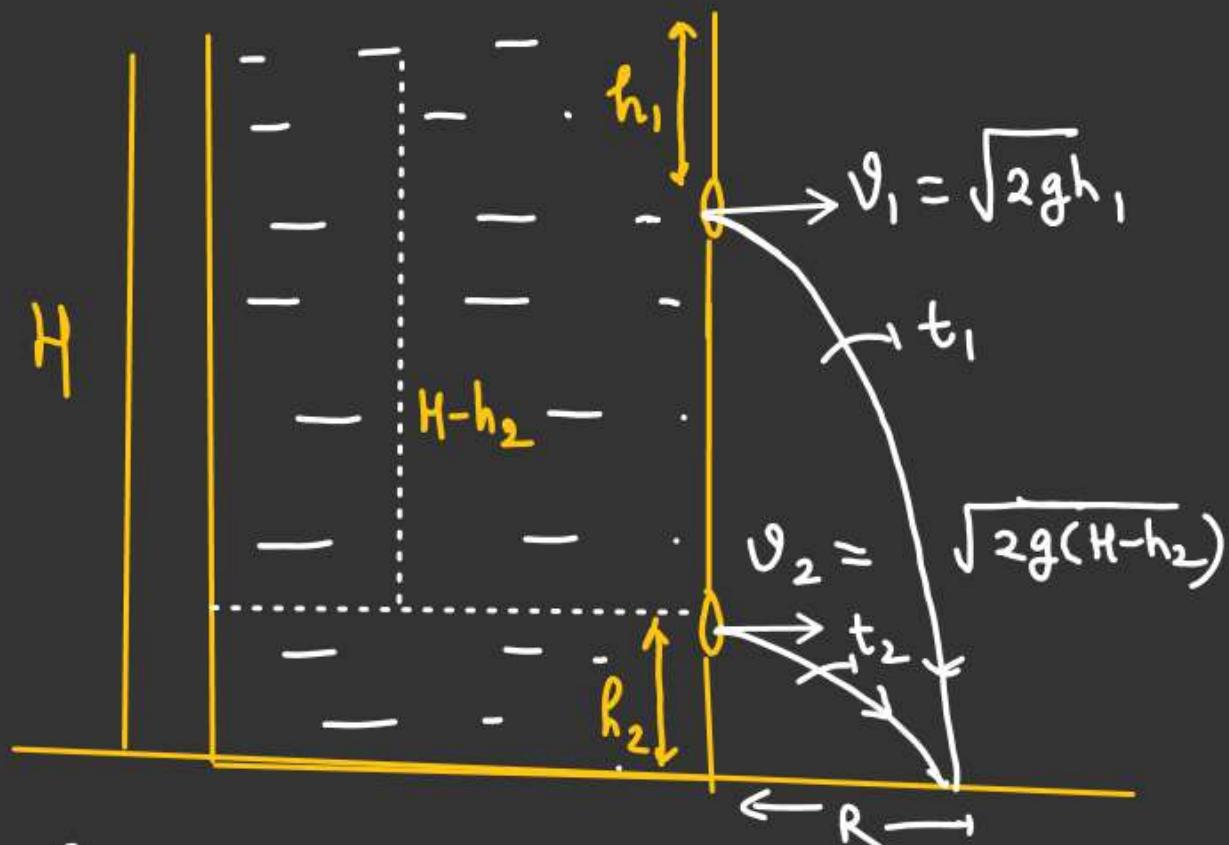
$$h_1 \cdot H - h_1^2 = h_2 H - h_2^2$$

$$(h_2^2 - h_1^2) - H(h_2 - h_1) = 0$$

$$(h_2 - h_1) \left[\underbrace{(h_1 + h_2) - H}_{\downarrow} \right] = 0$$

Never be

zero



$$h_2 - h_1 = 0$$

$$h_2 = h_1$$