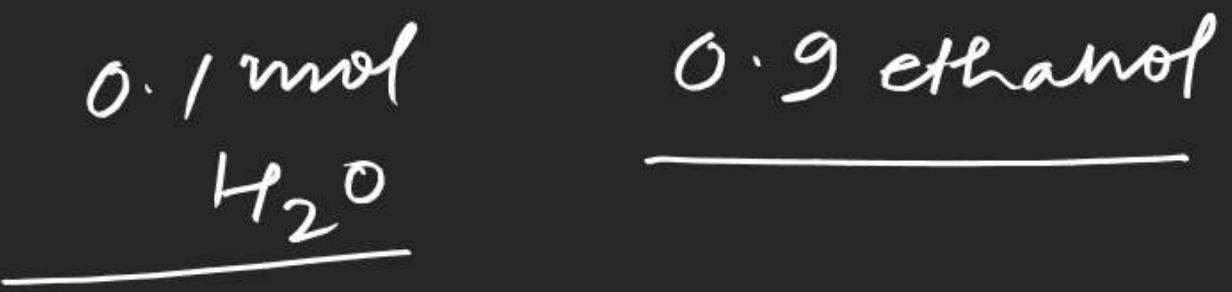


⑥



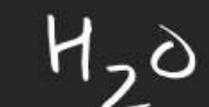
$$P_T = x_A P_A^0 + \cancel{x_B} P_B^0$$

$$\Delta T_f = k_f \times m$$

$$\Delta T_f = 2 \times \frac{0.1}{0.9 \times 46} \times 100^\circ$$

$$P_T = 0.9 \times P_{\text{ethanol}}^0$$

⑦



$$\Delta T_b = k_b \times \frac{0.1}{0.9 \times 18} \times 100^\circ$$



$$\textcircled{20} \quad \frac{P_0 - P_S}{P_S} = \frac{n}{N}$$

$$\textcircled{33} \quad 0.15 = K_b \times m$$

$$\Delta T_f = k_f \times \frac{m}{2}$$

$$\textcircled{11} \quad \Delta T_b = K_b \times m$$

$$\textcircled{42} \quad 27^\circ C$$

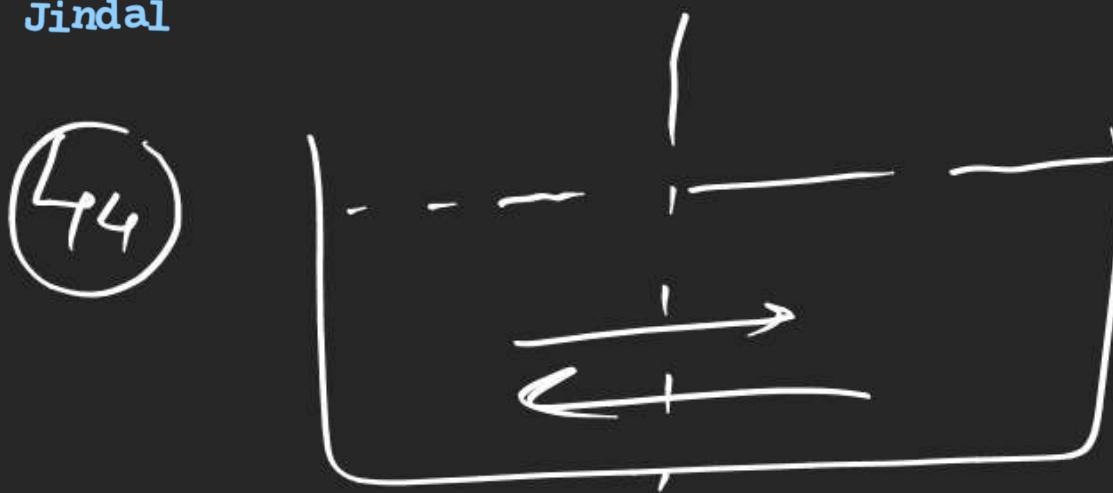
$$2 = 0.76 \times \textcircled{m}$$

$$\frac{760 - P_S}{760} = m \times \frac{18}{100}$$

$$\textcircled{47} \quad A \rightarrow \frac{1}{3} A_3$$

$$\eta = \frac{1}{3}$$

$$i = 1 + \left(\frac{1}{3} - 1\right) \alpha = \frac{1}{3}$$



52

$$\frac{P_0 - P_s}{P_0} = \frac{m \times \frac{M_{\text{Solvent}}}{1000}}{1000} \times \frac{1}{L}$$

0.1 × 2 0.1 × 2 0.1 × 3

2 : 2 : 3

Solvent

$$\Delta T_b \propto m \times i$$

$$\Delta T_f \propto m \times i$$

T_f

$$\pi l \propto C \times i$$

$$\frac{P_0 - P_s}{P_0} \propto m \times i$$

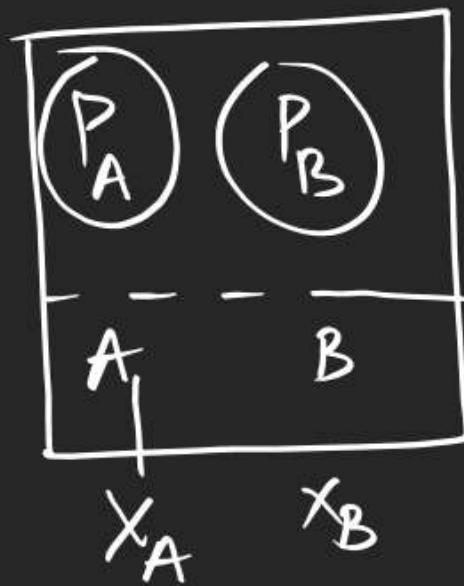
vap. pr

$$k_b = \frac{R T_b^2}{1000 L_v} = \frac{2 \times (373.15)^2}{1000 \times 9.72 \times 10^3}$$

23

$$1.24 = 0.512 \times \frac{288/M}{600} \times 1000$$

Non-ideal solution : An ideal solⁿ is formed when intermolecular forces remain unchanged on mixing i.e.



$$\langle A - A \rangle = \langle A - B \rangle = \langle B - B \rangle$$

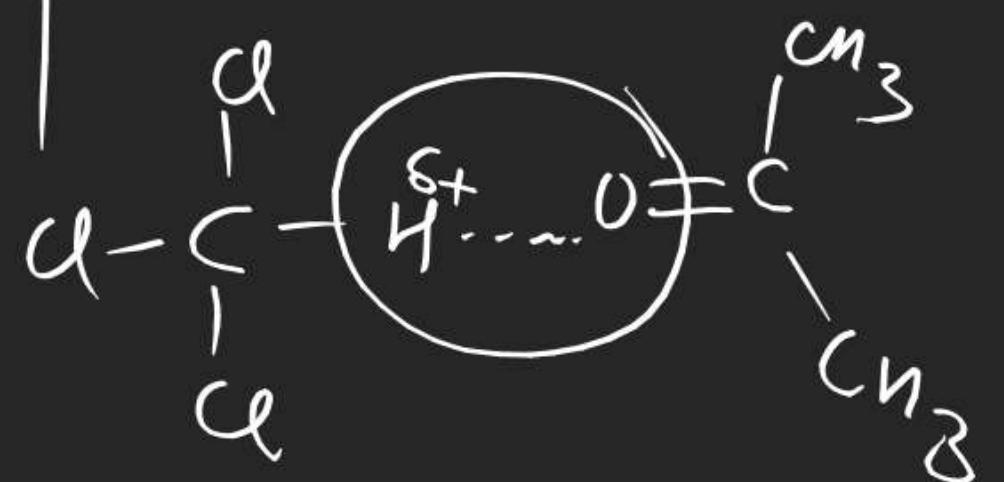
This condⁿ is however not fulfilled by most of the lig pairs thus they form non-ideal solution.

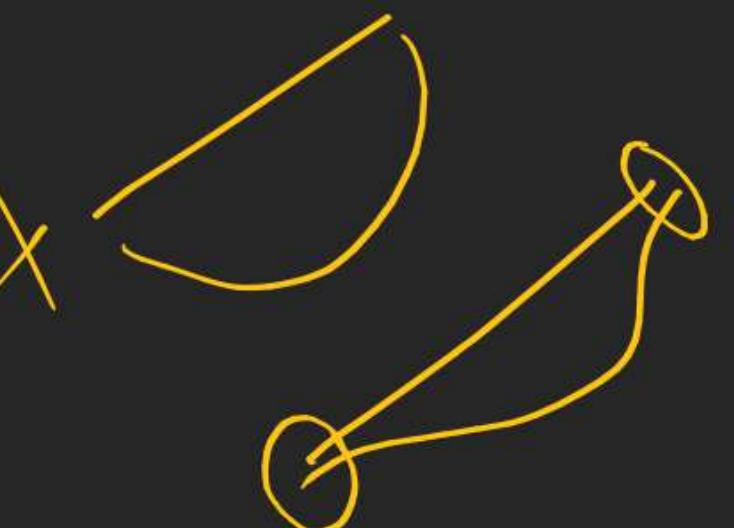
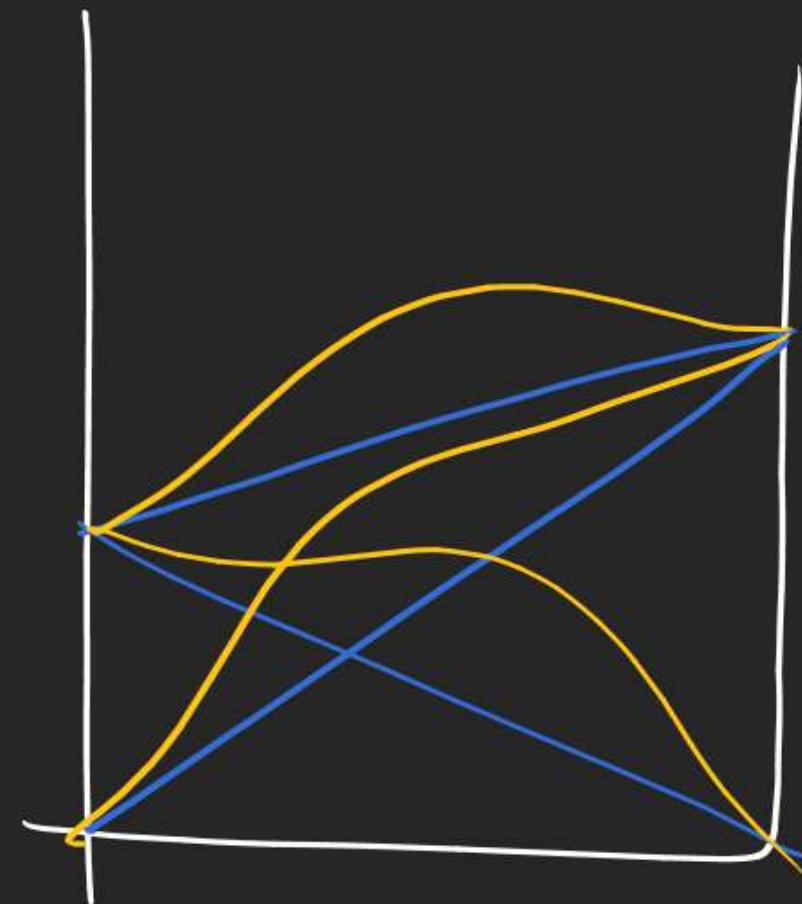
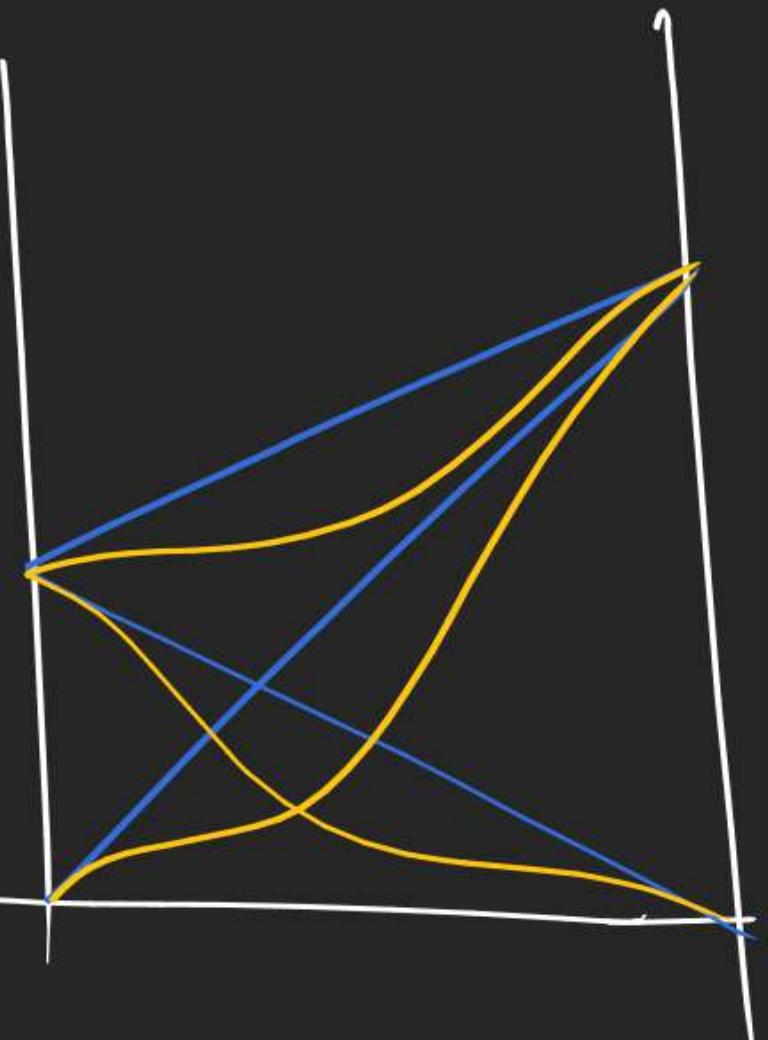
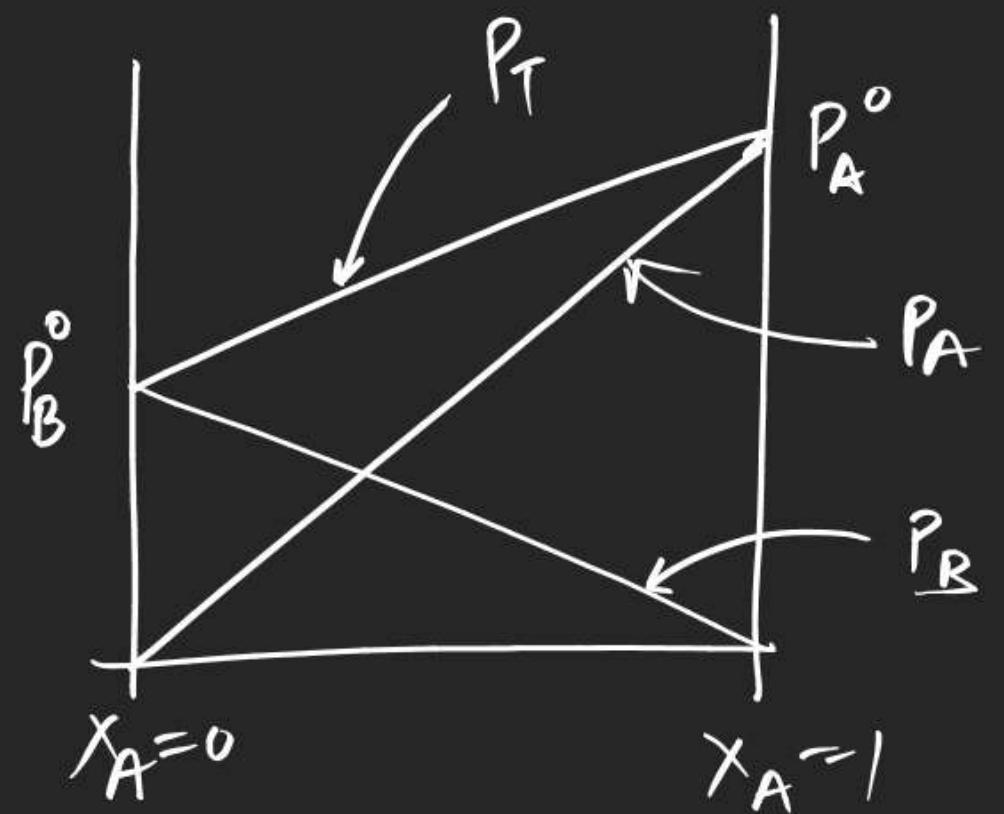
| Nishant Jindal | ideal sol ⁿ | Non-ideal sol ⁿ |
|---------------------------------------------------------------------|---------------------------------------|-------------------------------------|
| | -ive deviation | +ive deviation |
| obey Raoult's law | ① do not obey | do not obey |
| I.F. remain unchanged on mixing. | ② I.F. increase on mixing | I.F. ↓ es. |
| $P_A = X_A P_A^0$ | ③ $(P_A)_{\text{actual}} < X_A P_A^0$ | $(P_A)_{\text{actual}} > X_A P_A^0$ |
| $P_B = X_B P_B^0$ | $(P_B)_{\text{actual}} < X_B P_B^0$ | $(P_B)_{\text{actual}} > X_B P_B^0$ |
| ④ $\Delta H_{\text{mix}} = 0$ | $\Delta H_{\text{mix}} < 0$ exo | > 0 endo |
| ⑤ $\Delta V_{\text{mix}} = 0 \rightarrow \Delta V_{\text{mix}} < 0$ | | > 0 |
| ⑥ $\Delta S_{\text{mix}} > 0$ | $\Delta S_{\text{mix}} > 0$ | > 0 |
| ⑦ $\Delta \xi_{\text{mix}} < 0$ | $\Delta \xi_{\text{mix}} < 0$ | < 0 |
| ⑧ $\Delta S_{\text{surr}} = 0$ | $\Delta S_{\text{surr}} > 0$ | < 0 |
| ⑨ $\Delta S_{\text{univ}} > 0$ | > 0 | > 0 |

C.G

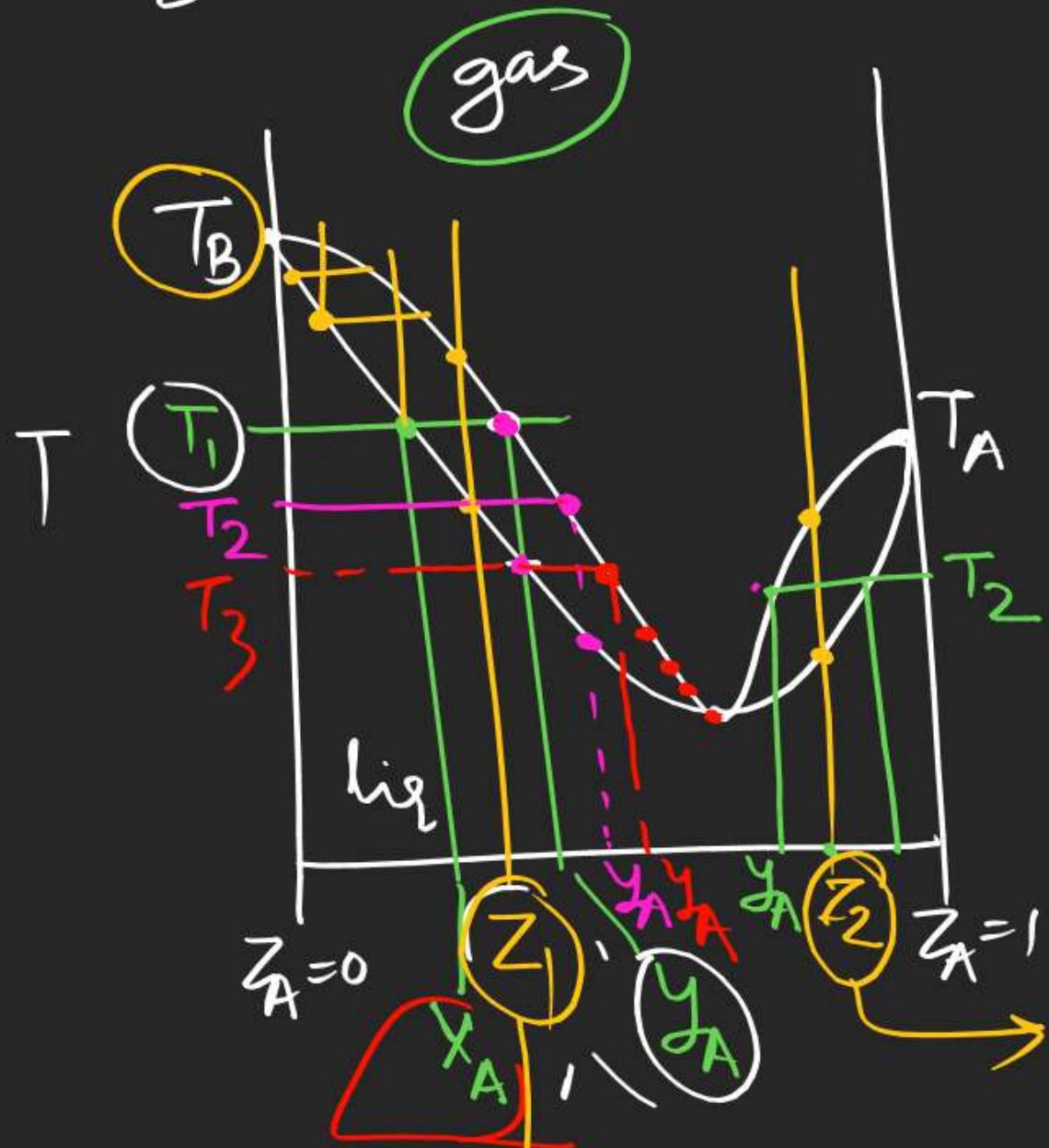
n-hexane & n-heptane

Benzene + Toluene

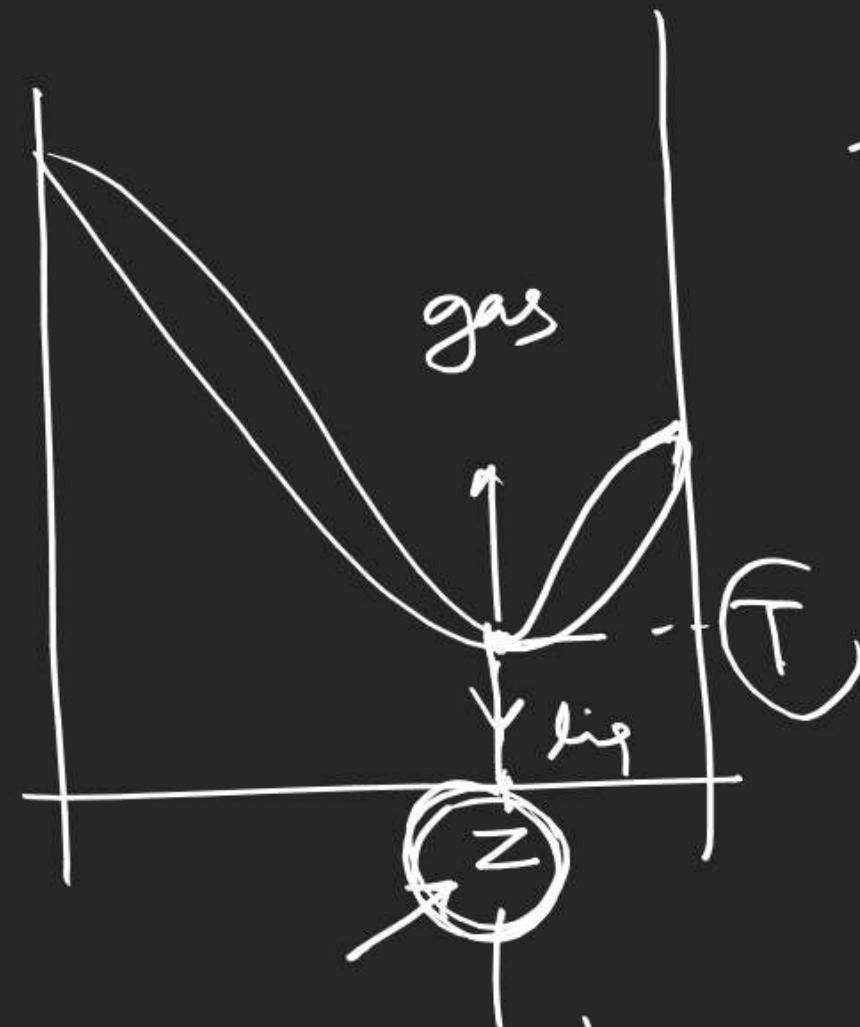
 $C_2H_5Cl + C_2H_5Br$ $C_6H_5Cl + C_6H_5Br$ $HNO_3 + H_2O$ $HCl + H_2O$ $C_6H_5OH + C_6H_5NH_2$ $CHCl_3 + CH_3COCH_3$  $C_2H_5OH + H_2O$ $C_2H_5OH + H_2O$ $CS_2 + \text{acetone}$ $CS_2 + CCl_4$ $Benzene + CCl_4$



Azeotrope



'but not pure A
pure B
(can be
obtained)



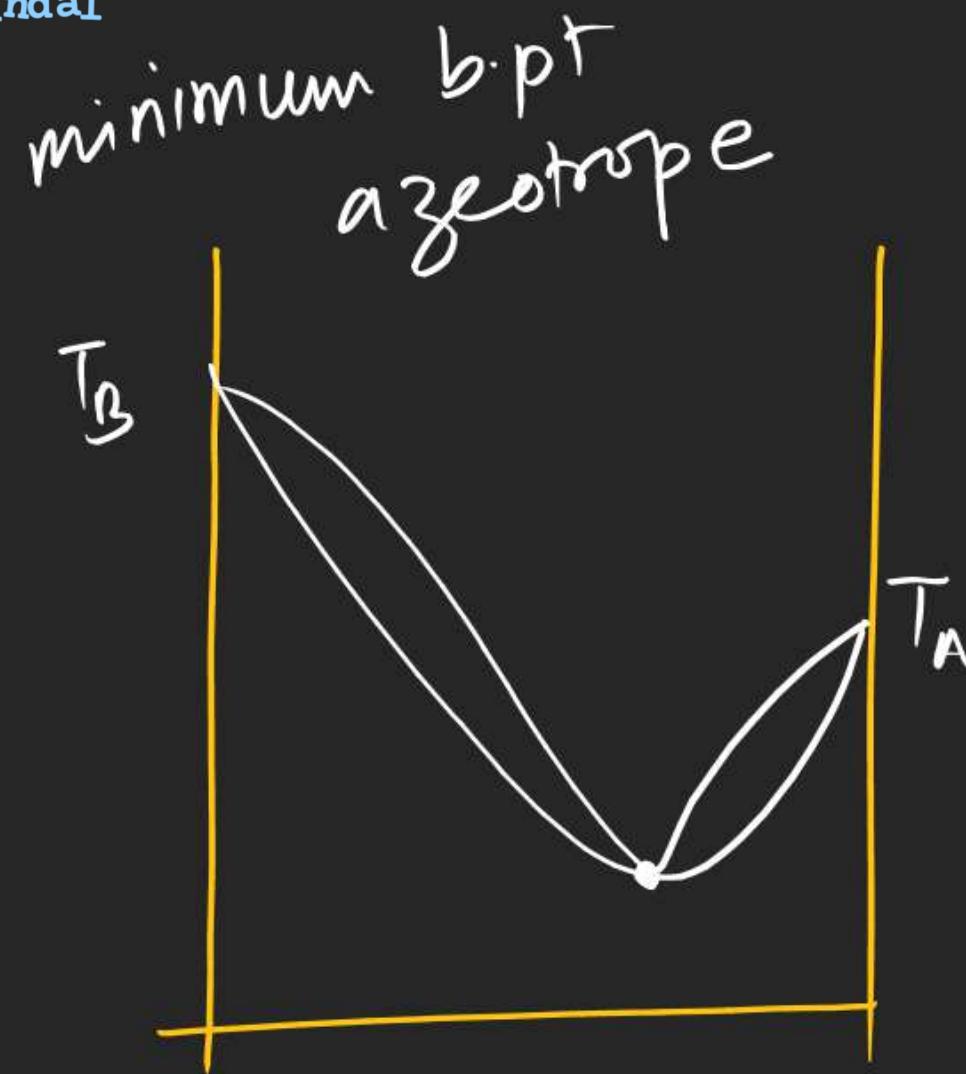
for an azeotrope

$$x_A = y_A$$

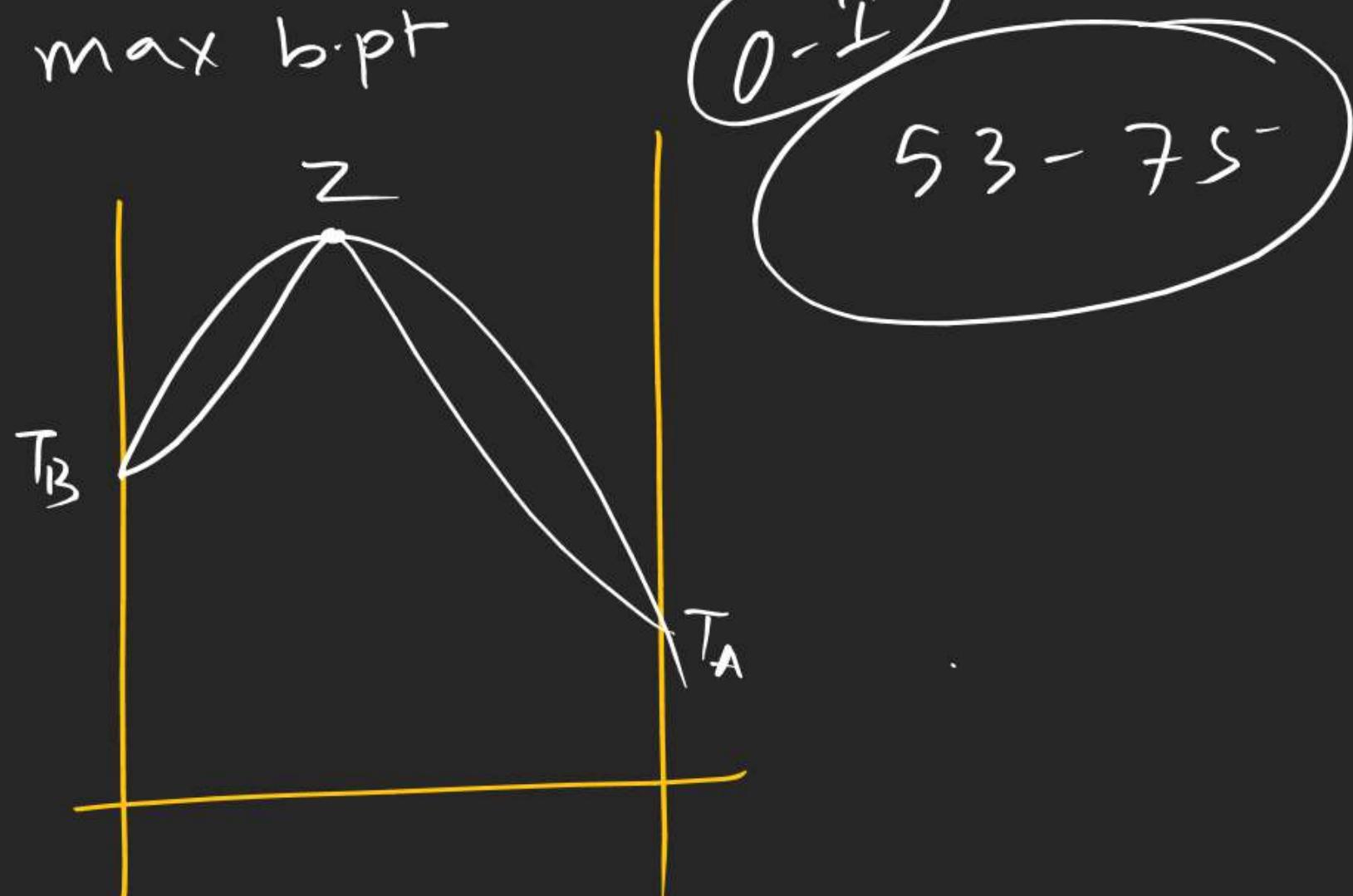
$$x_B = y_B$$

Azeotrope: It has sharp
bpt like pure liq

distillation method can not be used to
separate the components of azeotrope.



tire



-ive deviation