

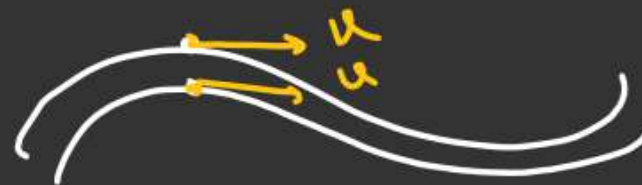
FLUID

* Fluid:- Which Can flow.
(gases & liquid)

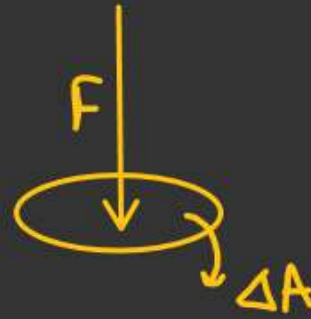
(*) Ideal Fluid

(*) Incompressible :- Density of liquid through its volume remain constant

(*) Non-Viscous :- Any two consecutive layer does not apply any tangential force on each other.

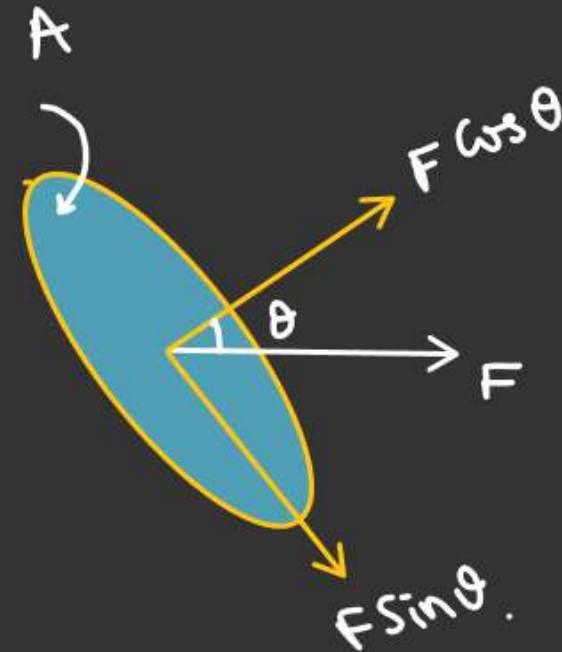


$$\begin{array}{|c|} \hline \rightarrow u \\ \hline \rightarrow u \\ \hline \end{array} f=0$$

FLUIDPRESSURE

$$p = \lim_{\Delta A \rightarrow 0} \left(\frac{F}{\Delta A} \right)$$

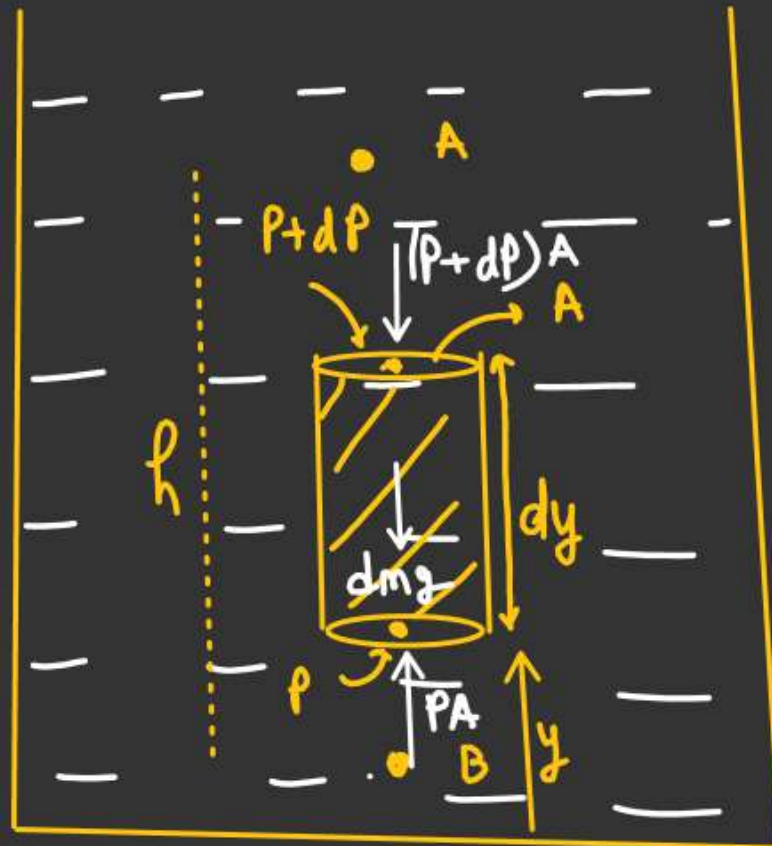
(F always \perp to Area)



$$p = \frac{F \cos \theta}{A}$$

FLUIDPRESSURE DIFFERENCE IN STATIC LIQUID

Newton first law for 'dy' length of liquid column



$$P = \frac{F}{A}$$

$$F = (PA)$$

$$PA = (P + dP)A + dm g$$

$$dm = \rho dV = \rho A dy$$

$$PA = (P + dP)A + \rho A dy g$$

$$0 = dPA + \rho A dy g$$

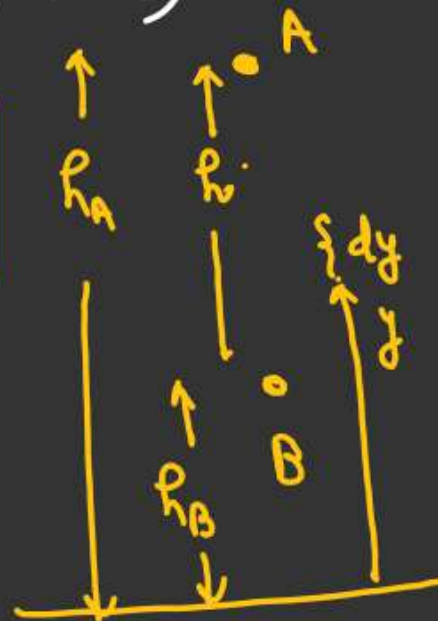
$$-\frac{dP}{dy} = \rho g$$

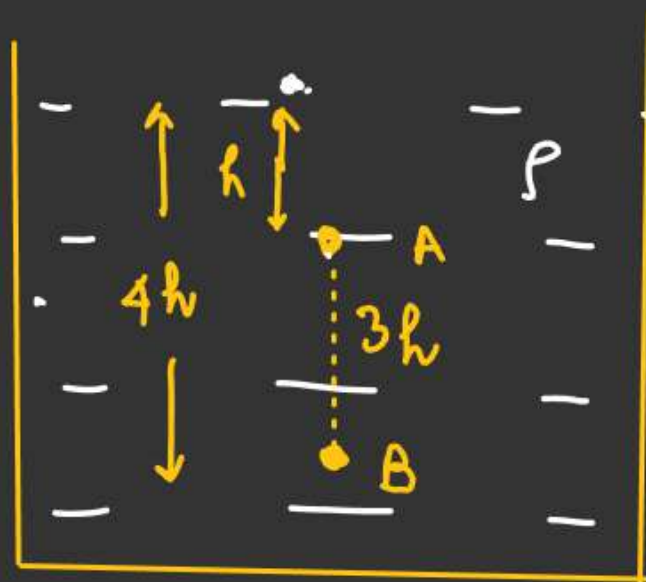
$$\int_{P_B}^{P_A} dP = \rho g \int_{h_B}^{h_A} dy$$

$$-(P_A - P_B) = \rho g (h_A - h_B)$$

$$P_B - P_A = \rho g (h_A - h_B)$$

$$P_B - P_A = \rho g h$$



FLUID

$$P_A = P_{atm} + \rho g h$$

$$P_B = P_{atm} + \rho g 4h$$

$$P_B - P_A = (3\rho g h)$$

Absolute pressure of A & B

$\rho = (a + by)$
 ↓
 Density of liquid
 $y =$ height from bottom.

$$P_A - P_B = ??$$

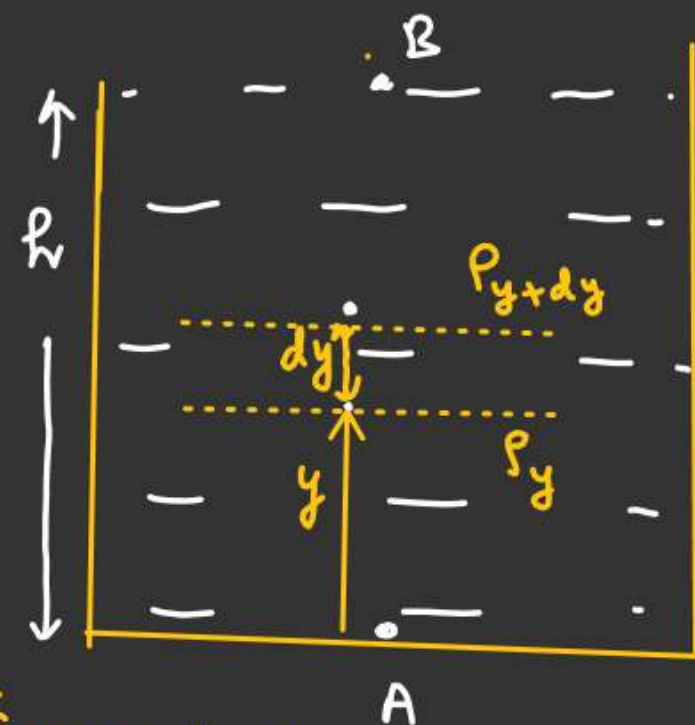
$$-\frac{dP}{dy} = \rho g$$

$$P_B \quad dP = -\rho_y \cdot g \, dy$$

$$\int_{P_A}^{P_B} dP = -g \int_0^h (a + by) \, dy$$

$$P_B - P_A = -g \left[a \int_0^h dy + b \int_0^h y \, dy \right]$$

$$P_B - P_A = -g \left[ah + \frac{b h^2}{2} \right]$$



Since dy is very small

$$\text{So } P_y \approx P_{y+dy}$$

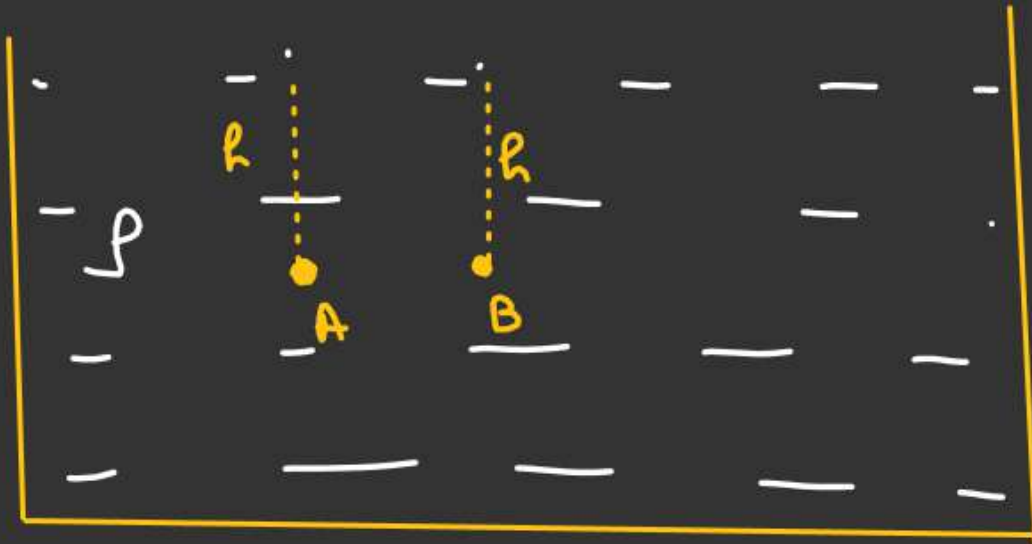
$dP \rightarrow$ Pressure difference for dy height

$$P_A - P_B = \left(agh + \frac{bgh^2}{2} \right)$$

FLUID

AA

Pressure difference b/w any two point at
Same horizontal level

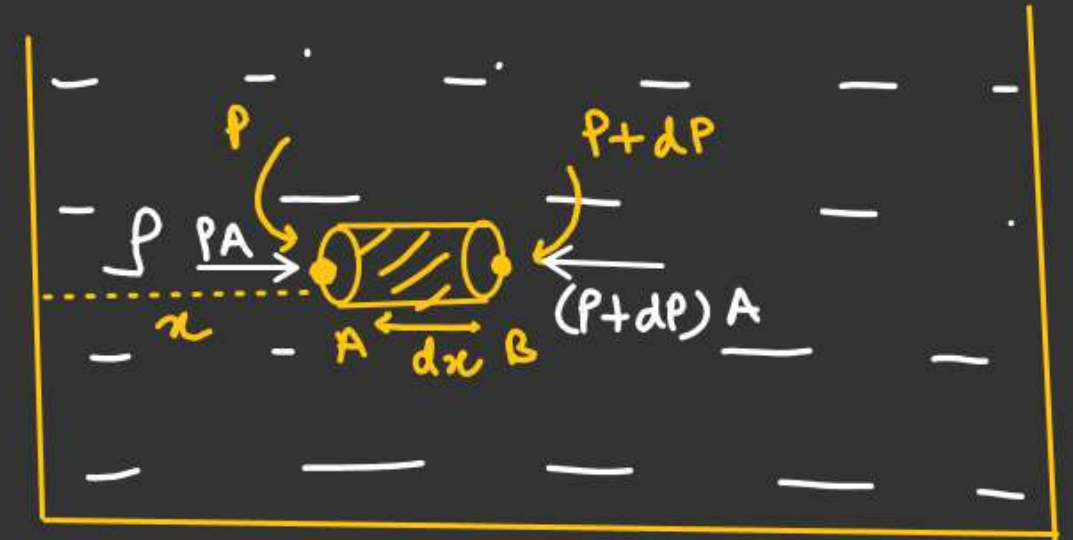


$$P_A = P_{atm} + \rho gh$$

$$P_B = P_{atm} + \rho gh$$

$$P_A - P_B = 0$$

$$P_A = P_B$$



For 'dx' length liquid

$$P A = (P + dP) A$$

$$dP = 0$$

FLUIDPressure difference in accelerated frameAccelerated in y-direction

$$dm = \rho A dy$$

$$P_A - (P + dP)A - dm g = dm a_y$$

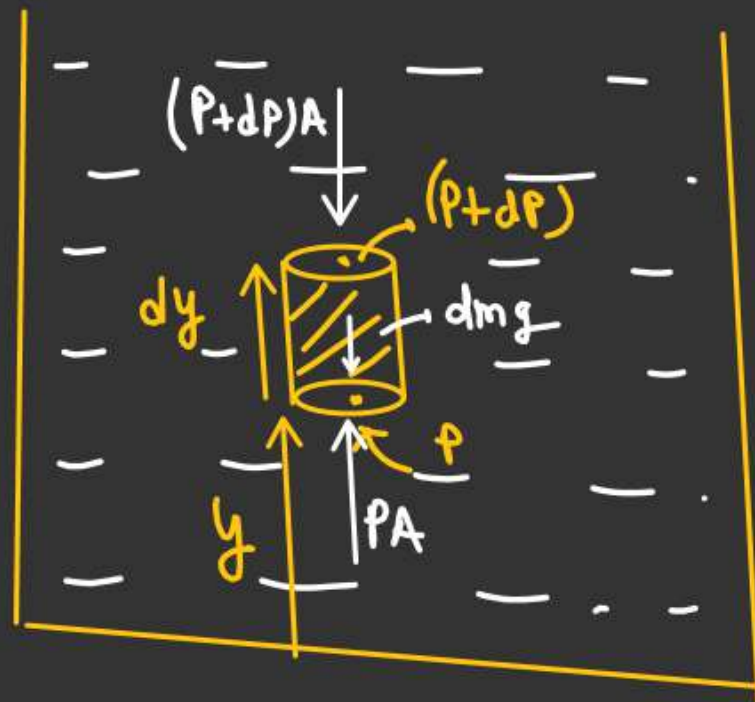
$$\cancel{P_A} - \cancel{P_A} - dP \underline{A} = \rho \underline{A} dy (g + a_y)$$

$$-\frac{dP}{dy} = \rho (g + a_y)$$

$$-\frac{dP}{dy} = \rho g_{\text{eff}}$$

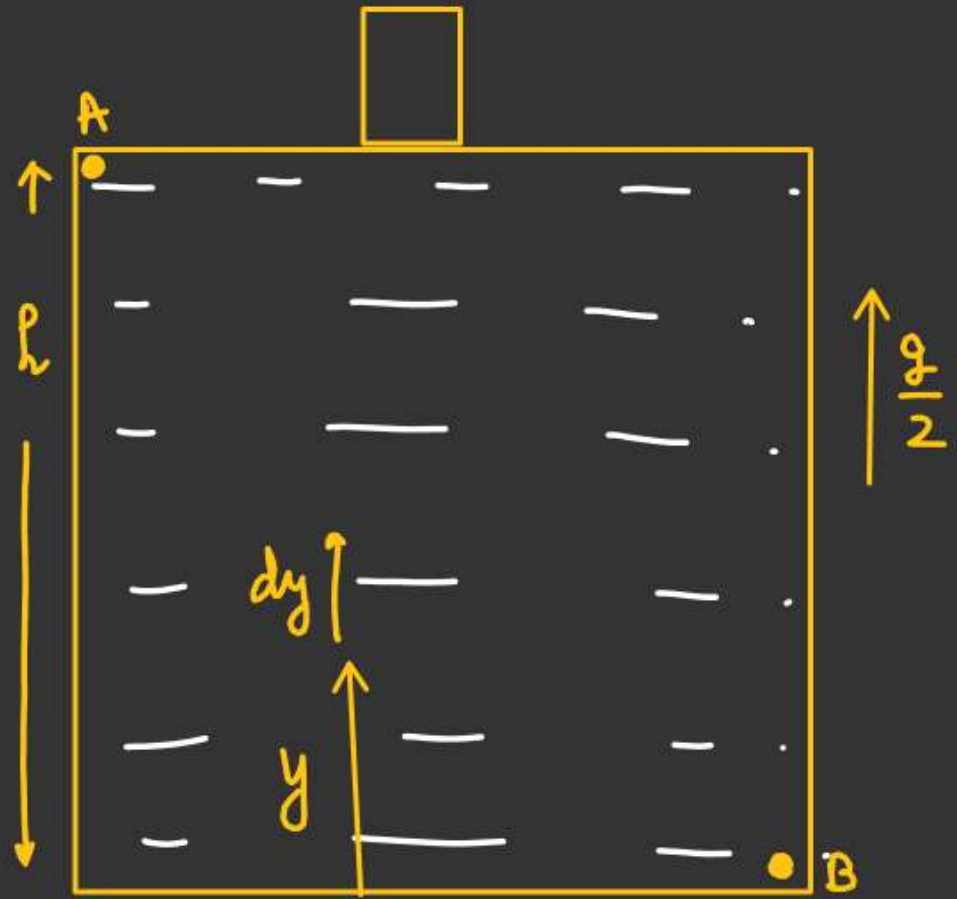
$$g_{\text{eff}} = (g + a_y) \quad \text{When elevator moving upward}$$

$$g_{\text{eff}} = (g - a_y) \quad \text{When elevator moving downward}$$



FLUID

$$P_B - P_A = ??$$

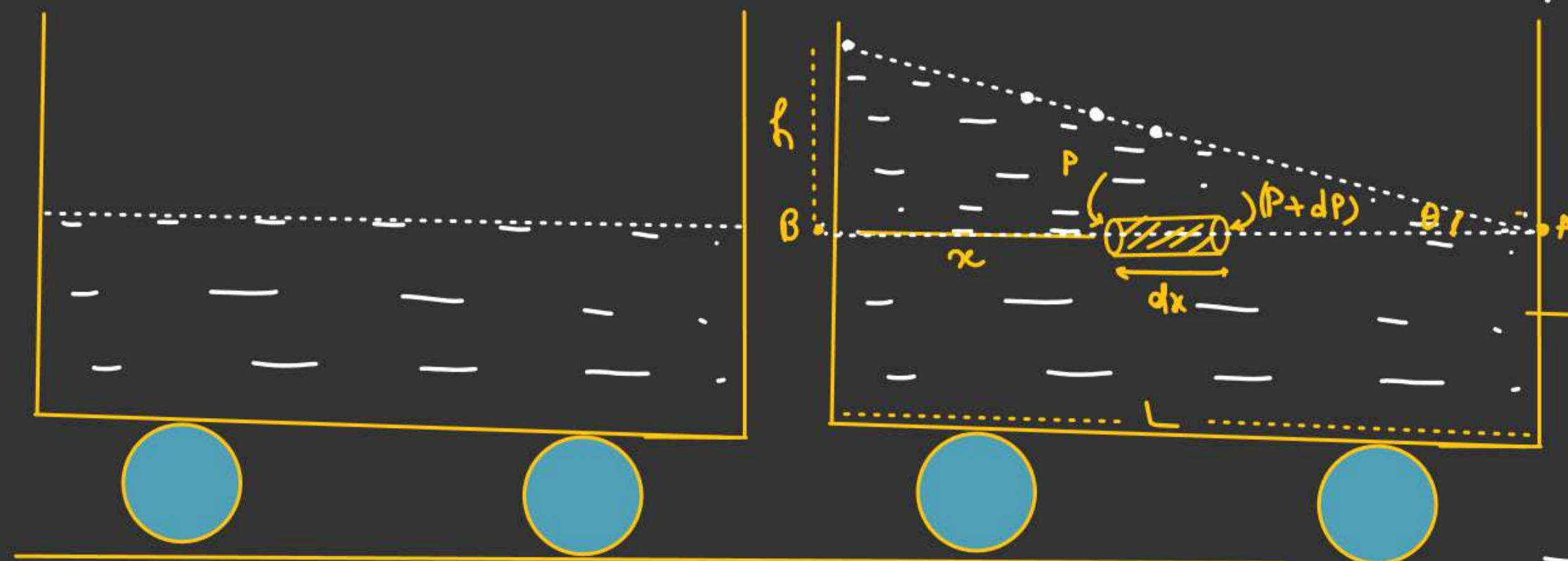


$$-\frac{dP}{dy} = \rho \left(g + \frac{g}{2} \right)$$

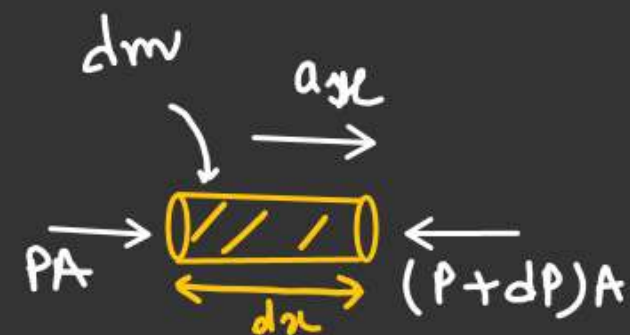
$$-\frac{dP}{dy} = \frac{3\rho g}{2}$$

$$-\int_{P_B}^{P_A} dP = \frac{3\rho g}{2} \int_0^h dy$$

$$P_B - P_A = \frac{3\rho g h}{2} \checkmark$$

FLUIDAccelerated in x-direction

$$dm = \rho A dx$$



$$PA - (P + dP)A = dm a_x$$

$$-dP \cdot A = \rho A dx \cdot a_x$$

$$\boxed{-\frac{dP}{dx} = \rho a_x}$$

$$-\int_{P_B}^{P_A} dP = \rho a_x \int_0^L dx$$

$$P_B - P_A = \rho a_x L \rightarrow (2)$$

From ① & ②

$$\rho g h = \rho a_x L$$

$$\boxed{\frac{a_x}{g} = \frac{h}{L} = \tan \theta}$$

$$P_A = P_{atm}$$

$$P_B = P_{atm} + \rho g h$$

$$P_B - P_A = \rho g h \rightarrow (1)$$

FLUID

$$P_A = P_{atm}$$

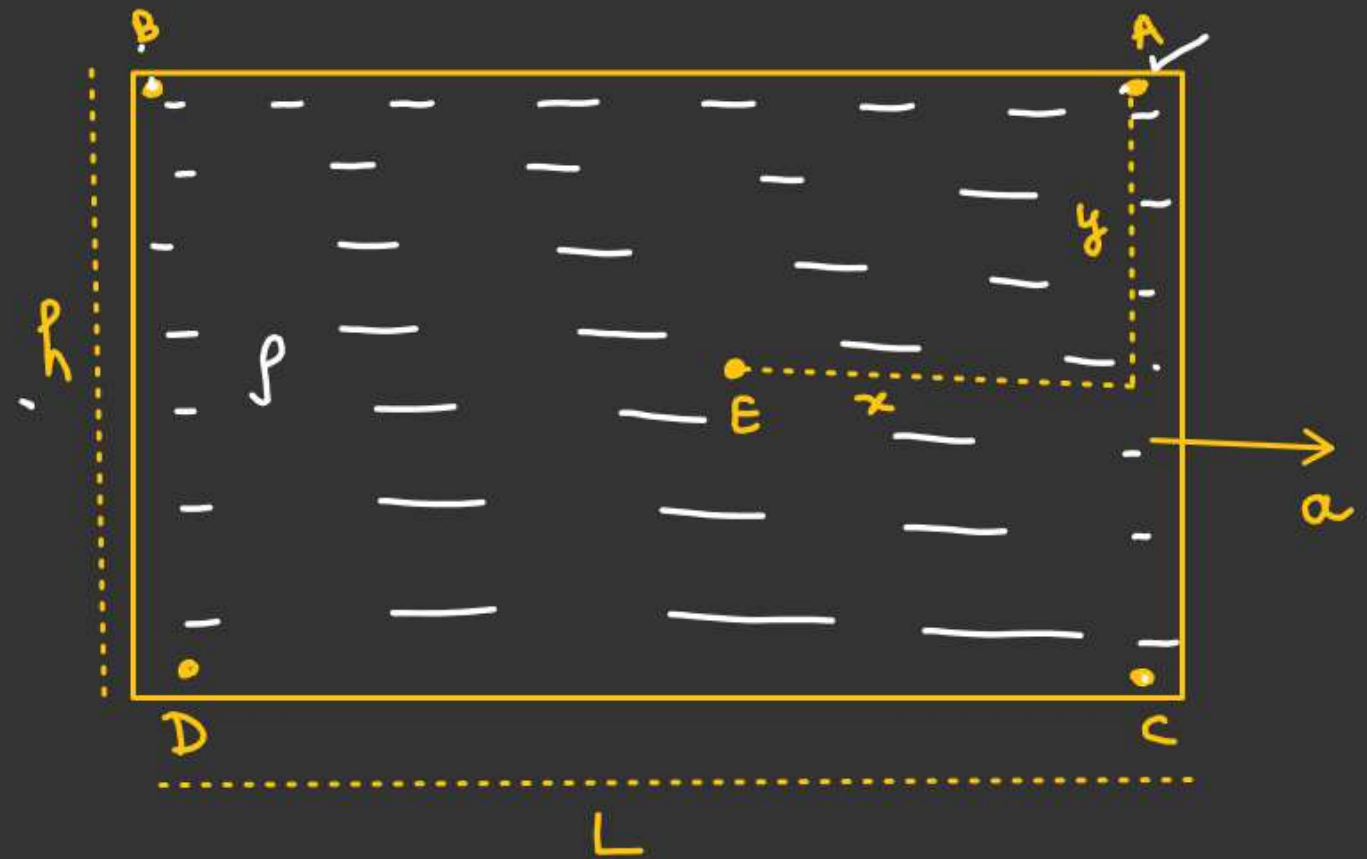
$$P_B = P_{atm} + \rho a L \quad \checkmark$$

$$P_C = P_{atm} + \rho g h$$

$$P_D = P_{atm} + \rho a L + \rho g h$$

$$P_E = P_{atm} + \rho g y + \rho a x$$

$$P_D = \underline{P_B} + \rho g h.$$



$$-\frac{dP}{\rho a dx} = \underline{\rho a}$$

$$-\int_{P_B}^{P_A} dP = \rho a \int_0^L dx$$

$$P_B - P_A = \rho a L$$