The vander weaks equation

$$\left(P + \frac{\alpha n^2}{v^2}\right) \left(V - nb\right) = nRI - \overline{D}$$

$$\left(P + \frac{a}{\sqrt{2}}\right) \left(V - b\right) = RT - 2$$

on expanding the above equation 3

$$\frac{1}{2} + \frac{9}{4} - \frac{9}{4} - \frac{ab}{\sqrt{2}} - RT = 0 - 3$$

multiply eqn by V2/p

$$V^{2} + \frac{aV}{p} - bv^{2} - \frac{ab}{p} - \frac{RTV^{2}}{p} = 0 - 4$$

Recovering the equation in passer of V  $V^3 - (\frac{RT}{P} + b)V^2 + \frac{aV}{P} - \frac{ab}{P} = a - G$ The eqn G is a cubic equation in V. V = Vc V - Vc = 0  $(V - Vc)^3 = 0$   $V^3 - 3VcV^2 + 3Vc^2V - Vc^3 = 0$   $V^3 - 3VcV^2 + 3Vc^2V - Vc^3 = 0$ Equate the coefficients  $ab = v^2$ , v and constant terms in  $ab = v^3$ .  $ab = v^3 - ab = v^3$   $ab = v^3 - ab = v^3$ 

$$3V_c^2 N = aN$$

$$3V_c^2 = \frac{aN}{P_c}$$

$$4V_c^3 = 4ab$$

$$V_c^3 = \frac{ab}{P_c}$$

$$V_c^3 = \frac{ab}{P_c}$$

$$V_c^3 = \frac{ab}{P_c} \times \frac{P_c}{P_c}$$

$$\frac{V_c^3}{3V_0^3} = \frac{ab}{P_c} \times \frac{P_c}{P_c}$$

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$$\frac{V_c}{3V_0^3} = \frac{ab}{P_c} \times \frac{P_c}{P_c}$$

$$3(3b)^2 = \frac{a}{Pc}$$

$$27b^2 = \frac{a}{Pc}$$

$$27b^2 = \frac{a}{Pc}$$

$$\frac{Pc}{27b^2} = \frac{a}{27b^2}$$

$$9b-b = \frac{27RT_cb^2}{a}$$

$$8bb = 27RT_cb^2$$

$$Tc = \frac{8ab}{27Rb^2}$$

The critical constants can be calculated using the volues of van der waals constant of a gas & vice verse.

$$V_c = 3b$$

$$b = V_c$$
3

$$Re = \frac{a}{21b^2}$$

$$Re = \frac{a}{3vc^2} = \frac{a}{Rc}$$

$$3vc^2 Pc = a$$

$$P_{c} = \frac{a}{3V_{c}^{2}} = \frac{a}{3(3b^{2})} = \frac{a}{3 \times 9b^{2}} = \frac{a}{27b^{2}}$$

$$P_{c} = \frac{a}{27b^{2}} - \cdots - (6.32)$$

stituting the values of V<sub>c</sub> and P<sub>c</sub> in

$$y_c = b + \frac{R T_c}{P}$$
 $y_c = b + \frac{R T_c}{P}$ 
 $y_c = b + \frac{R T_c}{A}$ 

$$b = \left(\frac{R T_C}{a}\right) 27 b^2$$

$$8b = \frac{T_C R 27b^2}{a}$$

$$T_{\rm C} = \frac{8 \, a \, b}{27 \, R \, b^2} = \frac{8 \, a}{27 \, R \, b}$$

$$T_{\rm C} = \frac{8 \text{ a}}{27 \text{ R b}}$$
 ----- (6.33)

The critical constants can be calculated using the values of van der waals constant of a gas and vice versa.

$$a = 3 V_C^2 P_C$$
 and  $b = \frac{V_C}{3}$ 

## 6.7 Liquefaction of gases

For important commercial operations such as LPG and rocket fuels, we require gases in their liquid state. The liquefication methods are based on the Joule-Thomson effect. He observed appreciable cooling when the compressed gas is forced through an orifice plug into

a low-pressure region. This phenomenon of lowering of temperature when a gas is made to expand adiabatically from a region of high pressure into a region of low pressure is known as Joule-Thomson effect. This effect is observed only below a certain temperature, which is a characteristic one for each gas. This temperature below which a gas obeys Joule-Thomson effect is called inversion temperature (T<sub>1</sub>). This value is given using van der waals constants a and b.

$$T_i = \frac{2a}{Rb}$$
 ---- (6.34)

Gases like O<sub>2</sub>, He, N<sub>2</sub> and H<sub>2</sub> have very low T<sub>c</sub>, hence Joule-Thomson effect can be applied for cooling effectively. At the inversion temperature, no rise or fall in temperature of a gas occurs while expanding. But above the inversion temperature, the gas gets heated up when allowed to expand through a hole.

There are different methods used for liquefaction of gases:

- 1) In Linde's method, Joule-Thomson effect is used to get liquid air or any other gas.
- 2) In Claude's process, the gas is allowed to perform mechanical work in addition to Joule-Thomson effect so that more cooling is produced.
- 3) In Adiabatic process, cooling is produced by removing the magnetic property of magnetic material such as gadolinium sulphate. By this method, a temperature of 10<sup>-4</sup> K i.e. as low as 0 K can be achieved.

Evaluate yourself

Valume of freen(V1) = 1.5 dm

Pressure (P1) = 0.3 atm

T' is constant

1 P2 = 1.2 atm

V2 = ?

P, V1 = P2 V2

V2 = P1 V1

P2

= 0.3 atm × 1.5 dm

1.2 atm

= 0.375 dm3

$$V_1 = 0.375 \, dm^3$$
  
 $P_1 = 1.05 \, d+m$   
 $T = 6005+$   
 $P_1 V_1 = P_2 V_2$   
 $P_2 = P_1 V_1$   
 $V_2 = 0.125 \, dm^3$   
 $P_2 = 7$   
 $P_2 = 7$   
 $P_3 = 7$   
 $P_4 = 1.05 \, dm^3$   
 $P_4 = 1.05 \, dm^3$   
 $P_5 = 7$   
 $P_6 = 1.05 \, dm^3$   
 $P_6 = 1.05 \, dm^3$ 

$$V_{1} = 3.8 \, dm^{3}$$

$$T_{1} = ?$$

$$\frac{V_{1}}{T_{1}} = \frac{V_{2}}{T_{2}}$$

$$T_{1} = \frac{T_{2}}{V_{2}} \times V_{1} = \frac{273k}{2.27dm^{3}} \times 3.8 \, dm^{3}$$

$$T_{1} = 457 \, k$$

(5) 
$$T_1 = 8^{\circ}C$$
  
 $T_1 = 8 + 273 = 281 \text{ k}$   $V_1 = 2.1 \text{ md}$   
 $P_1 = 6.4 \text{ atm}$   $V_2 = ?$   
 $T_2 = 25 \text{ c}$   
 $T_2 = 25 + 273 = 298 \text{ k}$   

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$V_2 = \left(\frac{P_1 V_1}{T_1}\right) \times \frac{T_2}{P_2}$$

$$= 6.4 \text{ atm} \times 2.1 \text{ md} \times 2.1 \text{ md}$$

$$V_2 = 14.25 \text{ ml}$$

$$V_{02} = 12 dm^3$$

$$V_{He} = 46 dm^3$$

$$V_{total} = 5 dm^3$$

$$Po_{2} = X_{o_{2}} \times P_{total}$$

$$X_{o_{2}} = \frac{no_{2}}{no_{2} + n_{He}}$$

$$= \frac{o.54}{o.54 + 2.05}$$

$$= \frac{o.54}{2.59}$$

= 0.2

no ob mode = 
$$\frac{12}{22.4}$$
L

No2 =  $\frac{12}{22.4}$ L

No2 =  $\frac{12}{22.4}$ L = 0.54 bnd

Ne =  $\frac{46}{22.4}$ L = 2.45 me

6. (5)

$$P_{total} = 772 \, mm \, Hg$$

$$P_{H_{20}} = 26.7 \, mm \, Hg$$

$$P_{H_{20}} = P_{0_{1}} + P_{H_{20}}$$

$$P_{0_{2}} = P_{total} - P_{H_{20}}$$

$$P_{1} = 26.7 \, mm \, Hg \quad T_{2} = 295 \, k$$

$$T_{1} = 300 \, k \quad P_{2} = ?$$

$$\frac{P_{1}}{T_{1}} = \frac{P_{2}}{T_{2}}$$

$$P_{2} = \left(\frac{P_{1}}{T_{1}}\right) T_{2} = \frac{26.7 \, mm \, Hg}{300 \, k} \times 295 \, k$$

$$P_{0_{2}} = 772 - 26.26 = 745.74 \, mm \, Hg$$

$$P_{0_{2}} = 772 - 26.26 = 745.74 \, mm \, Hg$$

(7)

$$61 = 1.5 \, \text{min}$$
 $62 = 4.73 \, \text{min}$ 

( .. Volume const.)

Squaring by both side

(3.15)2 = 159.8

mydrocarbon

mydrocarbon

159.8

m hydro = 159.8 (3.15)<sup>2</sup> = 16.19 mon<sup>-1</sup> n(12)+(2m+2) = 16 12n+2n+2=16 14n=16-2 14n=14 n=14 n=14 n=14

: General formulas

for hydrocarbon

(nH2n+2.

(8) Critical temperature of a gas is
defined as the temperature above which
It cannot be liquefied even at high pressures.

Has will liquefied first, then followed by a NH3 & finally Con will liqueties