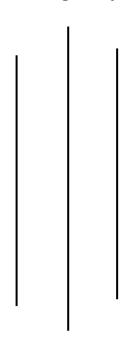
"To study the performance of refrigeration system as per the given system component and identify the energy saving opportunity in a system by optimizing the performance cycle."



## Submitted by

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#### The component specification in a system:

1) Compressor

Name Plate specification:

Refrigerant: NH<sub>3</sub> (R717) Swept Volume: 550 m<sup>3</sup> / hr

Speed: 970 RPM

Working Pressure: 18 Bar

Measured quantities:

Suction Pressure: 1.4 Bar Discharge Pressure: 9 Bar

#### **Important definition:**

i) Compressor capacity = Suction volume

(Volume of air sucked by the compressor during its suction stroke)

Swept Volume

 $Vp = (pi D^4/4)*L$ 

D = Diameter of Cylinder

L = Length of piston stroke

- 2) Condenser
- 3) Evaporators
- 4) Expansion valve

Temperature before expansion valve in chiller = 24.5 c

Temperature before Expansion valve in EXV1 and EXV2 = (4-6) c

#### Calculation of the cooling load on heat Exchanger at water chiller in present conditions:

refilled water Temperature	16	°C
outgoing temp	1.7	°C
Mean Temperature	8.85	°C
density at given mean temperature	999.74	Kg/ m3
		m3 /Min (As per the
	_	given spec in inlet
In flow volume rate	1	motor)
Specific Heat capacity	4.18	kJ/Kg/K
heat exchanging rate	59758.46	KJ /Min
mass of refrigerant		
flow in chiller section	51.96388	Kg/Min
Total cooling load	284.56	TOR

# Calculation of additional heat exchange required in heat exchanger in cooler to meet the demand criteria:

Required Additional Heat exchange rate ( i.e decreasing water temperature from 1.7 - 0.5)<sup>0</sup> C Change in temperature = 1.2

Additional Heat Exchange rate required for water = 5.016 KJ / Kg of water

Total heat exchange required in a minute = 5014.696 KJ/ min

Additional cooling capacity to be increased in heat exchanger in chiller =23.879 TOR

Total heat that needs to be rejected in condenser = 5014.96 KJ

From pressure enthalpy chart required heat rejection at condenser = 96.49 KJ / Kg

From pressure enthalpy chart; required additional temperature drop in condenser =  $21.4^{\circ}$  C

#### Calculation of the load on evaporator in refrigeration room:

Milk ingoing temp	6.8	°С
outgoing temp	4	°C
Temp difference	2.8	°C
Specific Heat capacity of milk	3.93	KJ/Kg/K
Density of milk	1028	Kg/ m <sup>3</sup>
Volume of Milk to be cooled	83	M <sup>3</sup>
Time for Cooling	11.5	Hr
heat exchanging rate	1360.73	KJ /Min
Cooling load in refrigeration room	6.479	TOR
Required enthalpy change in refrigerant	1200	KJ / Kg
Mass of refrigerant flow in evaporator of refrigeration room	1.135	Kg /Min

#### **Condenser performance Analysis:**

Heat exchanging capacity of condenser at present = 61119.05 KJ / Min

Required additional heat exchange required at condenser = 5014.96 KJ / Min

Total mass of refrigerant flowing in condenser = (51.96 + 1.135) Kg / Min

= 53.095 Kg / Min

Total additional heat rejection at condenser = 5014/53.095

= 94.434 KJ / Min / Kg of refrigerant

### Calculation of enthalpy of refrigerant entering in the compressor:

Enthalpy = (51.96\*1500 + 1.135\*1450)/(51.96+1.135) = 1498 KJ/Kg

#### **Calculation of COP:**

In present status:

Work Done by Compressor = (1850-1498) KJ /Kg \* 53.095 Kg/Min = 18689.44 KJ /Min

= 88.997 TOR

Total Refrigeration effect being produced in the system = 291.039 TOR

COP = 3.27

After improving performance in Condenser

Work done by compressor = 88.997 TOR

Total refrigeration effect being produced in system =314.918 TOR

COP = 3.53

#### Result

The condenser should be running optimally to make the additional heat rejection rate of 94.434 KJ/ min/ Kg of refrigerant i.e additional 23.879 TOR be created in system.

The COP of the system will improve from 3.27 to 3.53