

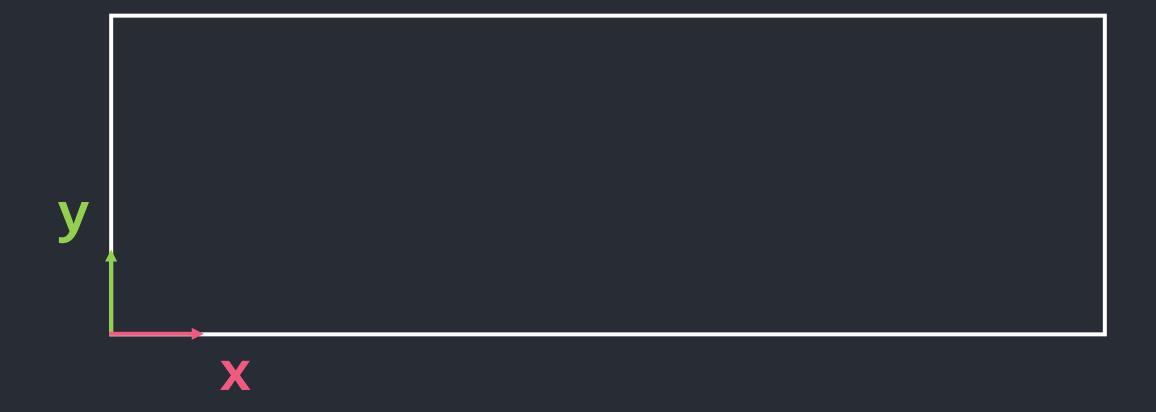
Navier-Stokes Equation

$$\rho \left(\frac{\partial u}{\partial t} + u \cdot \nabla u \right) = -\nabla p + \mu \nabla^2 u + \mathbf{F}$$

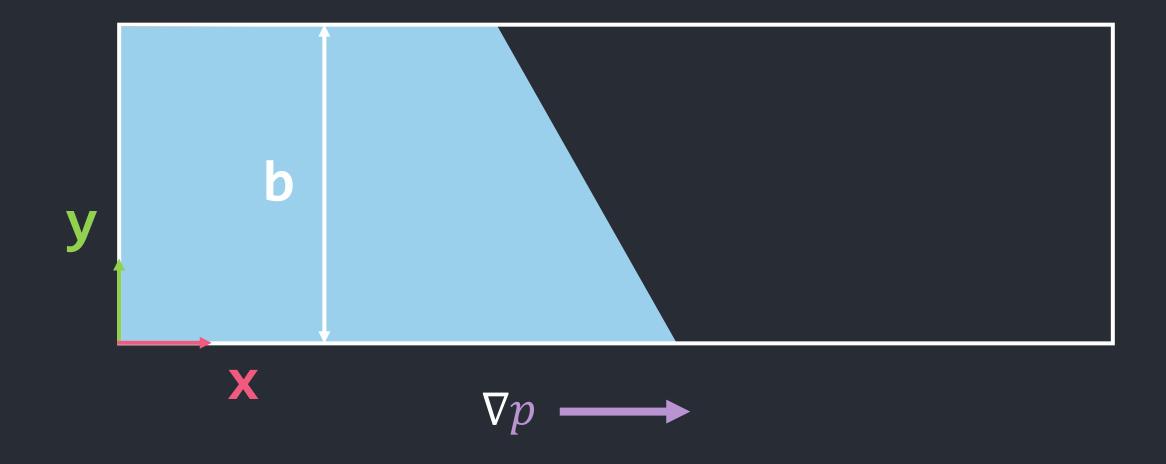


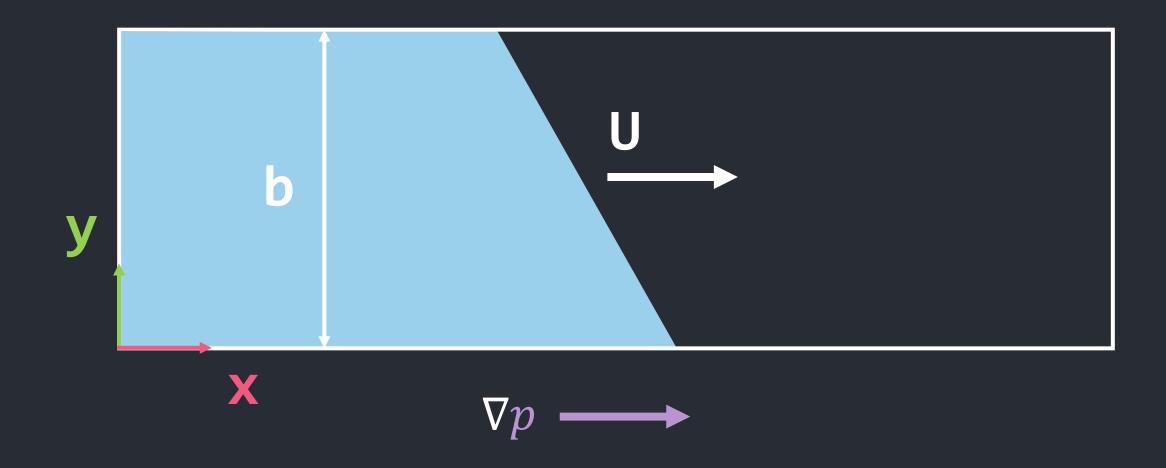




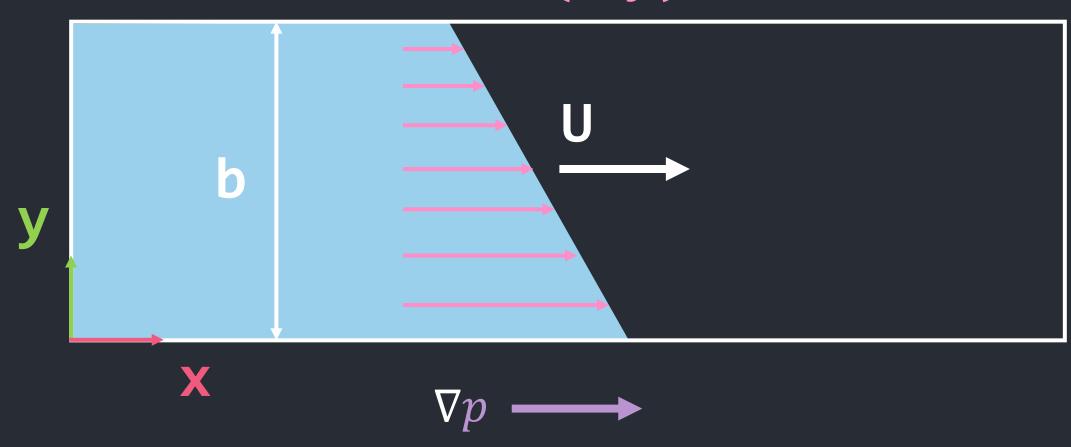




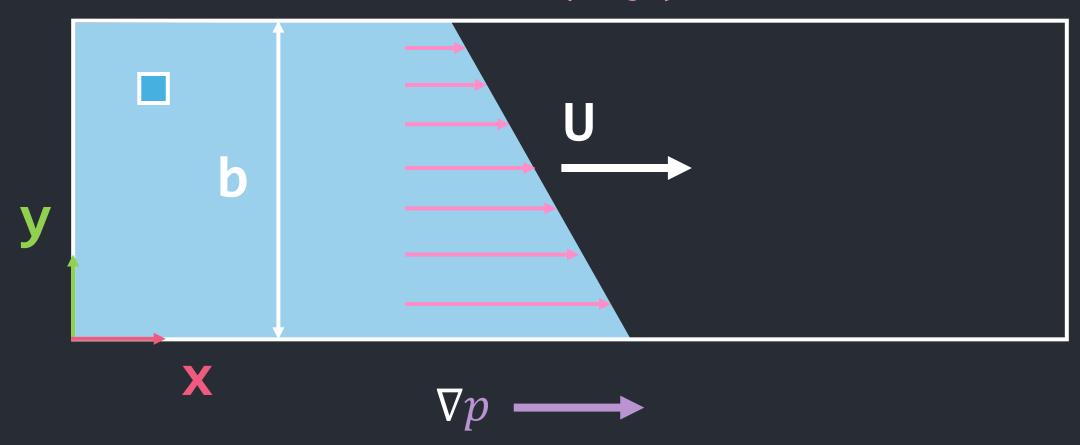


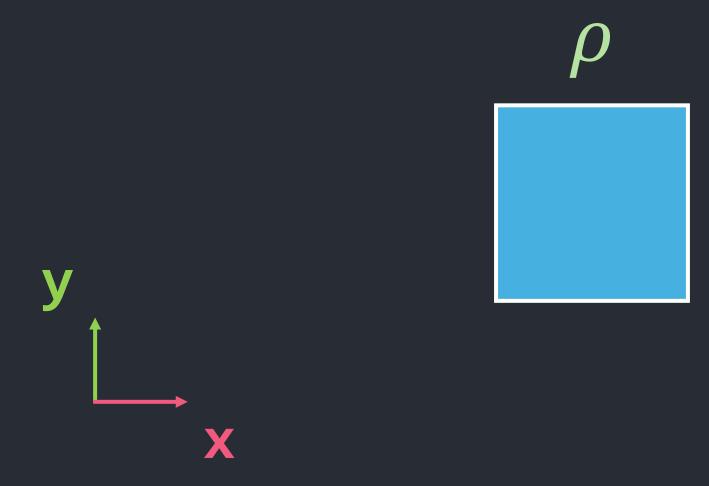


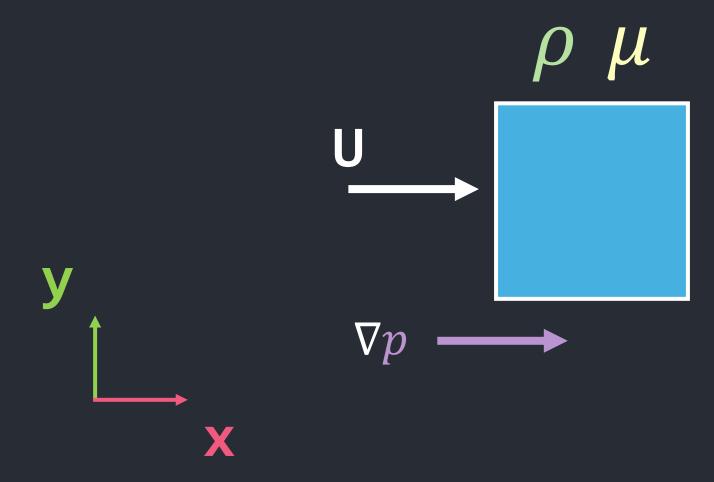
$$u=u(x,y)$$

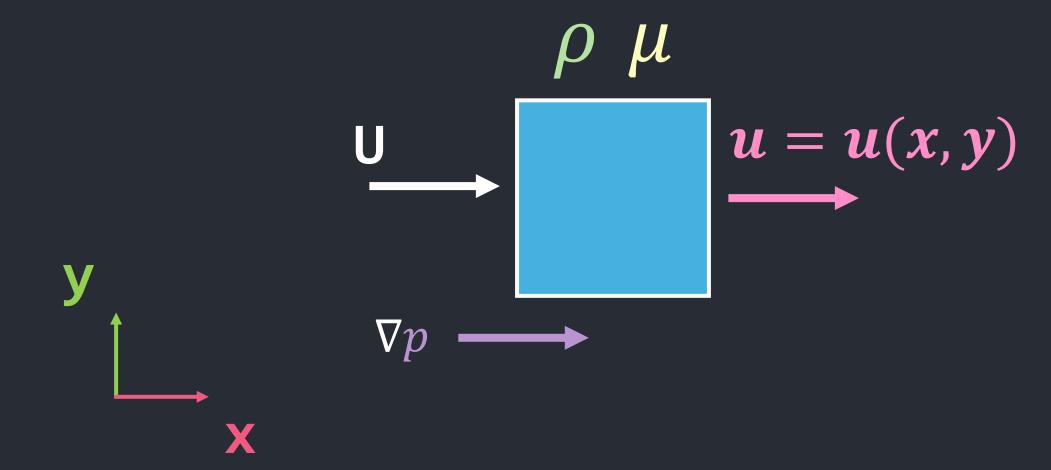


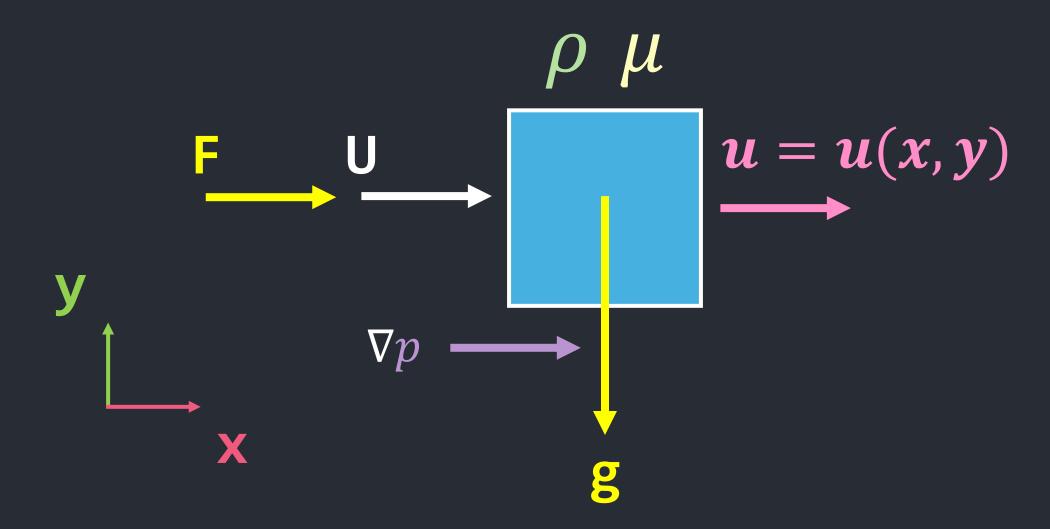
$$u=u(x,y)$$











Navier-Stokes Equation

$$\rho \left(\frac{\partial u}{\partial t} + u \cdot \nabla u \right) = -\nabla p + \mu \nabla^2 u + \mathbf{F}$$

 $u \rightarrow Speed: m/s$

 $\rho \rightarrow Fluid\ Density:\ kg/m^2$

 $p \rightarrow Pressure: Pa$

 $\mu \rightarrow Dynamic Viscousity: Pa \cdot s$

 $F \rightarrow External Force: N$

 $t \rightarrow Time: s$

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

$$\rho \left(\frac{\partial u}{\partial t} + u \cdot \nabla u \right) = -\nabla p + \mu \nabla^2 u + \mathbf{F}$$

Newton's 2nd Law

$$ma = \sum F$$

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

 $\frac{ma}{V}$

$$\rho\left(\frac{\partial u}{\partial t} + u \cdot \nabla u\right) = -\nabla p + \mu \nabla^2 u + F$$

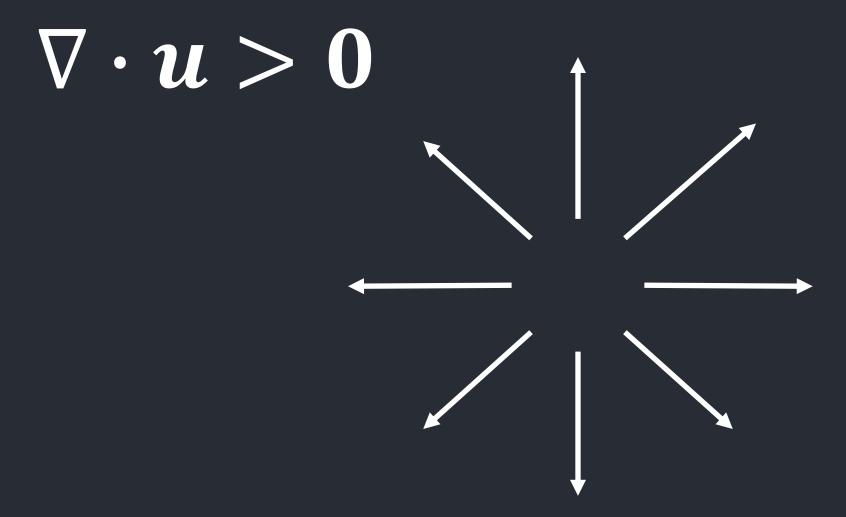
$$\frac{ma}{V}$$

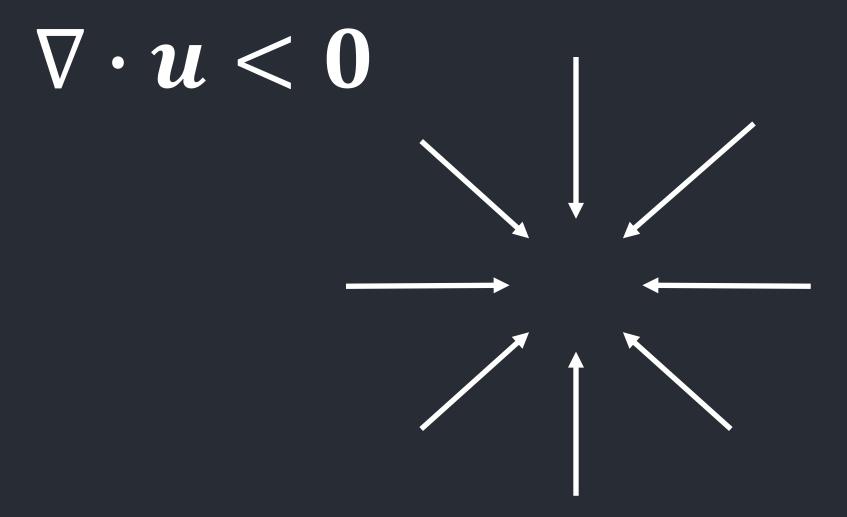
Divergence

 $\nabla \cdot u$

$$u = u(x, y)$$

$$\nabla \cdot \boldsymbol{u} = \operatorname{div} \boldsymbol{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y}$$





$\nabla \cdot u = 0$



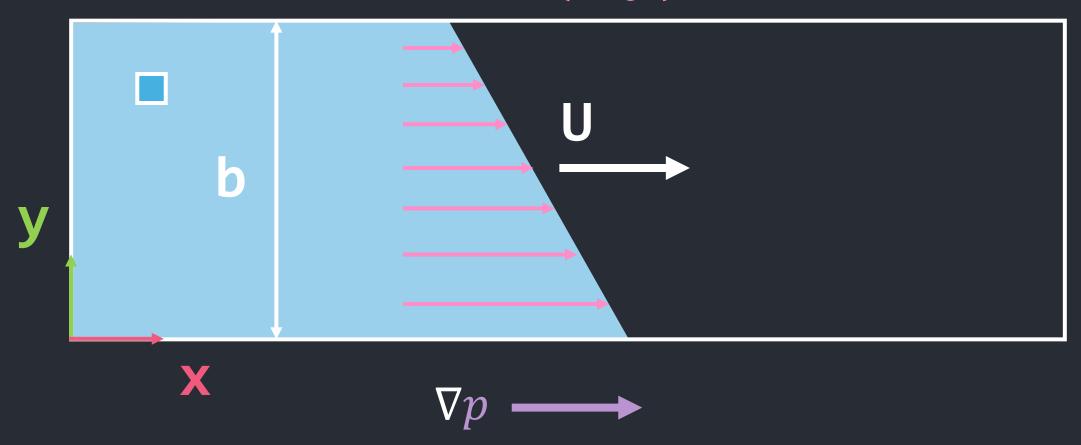
Continuity Equation

$$\nabla \cdot u = 0$$

Incompressible Flow

$$\nabla \cdot \boldsymbol{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

$$u=u(x,y)$$



Conditions

- No flow in vertical direction $\rightarrow u_y = 0 \frac{m}{s}$
- Flow driven by pressure gradient $\rightarrow \frac{\partial p}{\partial x} \neq 0$ $\frac{Pa}{m}$
- No gravity effects $\rightarrow g = 0 \frac{m}{s^2}$
- Boundary of the pipe $\rightarrow y = [0, b]$
- Incompressible Flow $\rightarrow \nabla \cdot u = 0$

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \left(u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

Incompressible Flow

$$\nabla \cdot \boldsymbol{u} = \frac{\partial u_{x}}{\partial x} + \frac{\partial u_{y}}{\partial y} = 0$$

Fully Developed Flow

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

Fully Developed Flow

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

O Noflowin y

Fully Developed Flow

$$\frac{\partial u_{x}}{\partial x} = \mathbf{0}$$

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \left(u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

Steady Flow

No flow in y

No g effects

$$\rho \left(\frac{\partial \mathbf{u}}{\partial t} + \left(u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

Fully Developed

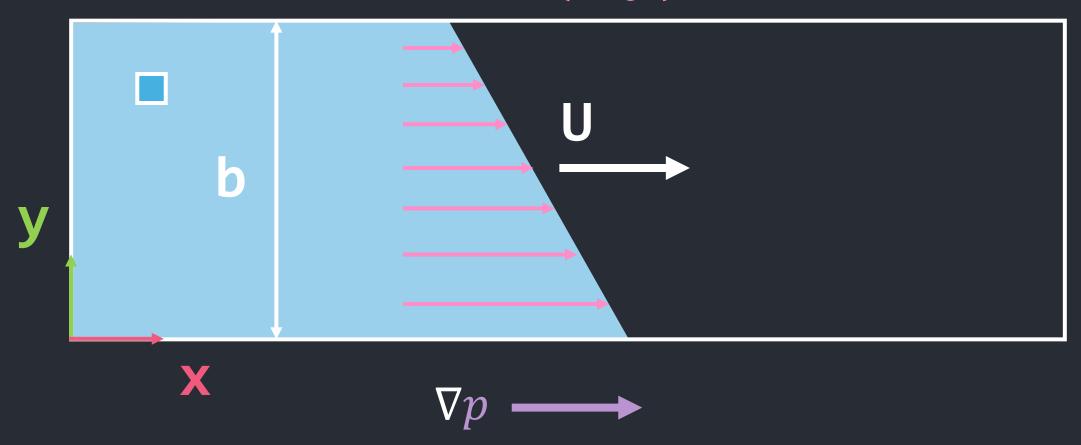
$$0 = -\nabla p + \mu \nabla^2 \mathbf{u}$$

Fully Developed

$$0 = -\nabla p + \mu \left(\frac{\partial^2 u_x}{\partial x^2} + \frac{\partial^2 u_x}{\partial y^2} \right)$$

$$0 = -\nabla p + \mu \left(\frac{\partial^2 u_x}{\partial y^2} \right)$$

$$u=u(x,y)$$



Flow Profile

$$u(y) = ???$$

$$0 = -\nabla p + \mu \left(\frac{\partial^2 u_x}{\partial y^2} \right)$$

$$\frac{\partial^2 u_x}{\partial y^2} = \frac{1}{\mu} \nabla p = const$$

Flow Profile

$$u(y) = \frac{1}{2\mu} \nabla p(b^2 - by) + U\left(1 - \frac{y}{b}\right)$$

$$b = 360 m$$

$$U = 20 \frac{m}{s}$$

$$\mu = 1001600.0 Pa \cdot s$$

$$\nabla p = 20 \frac{Pa}{m}$$

Rust



+

Bevy

