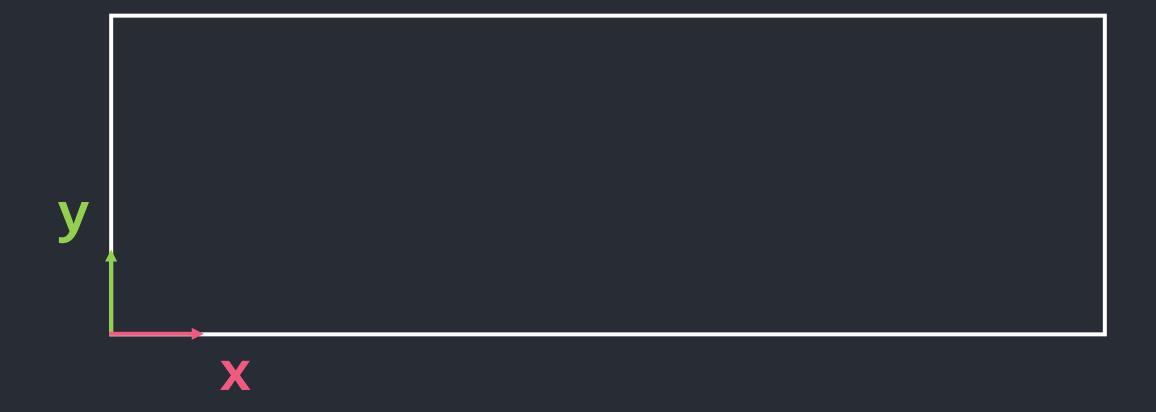
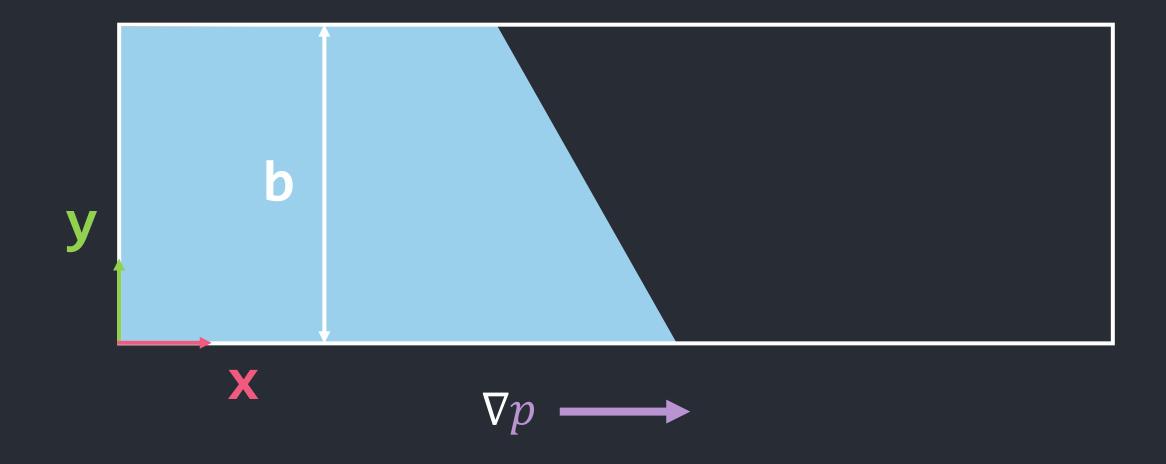


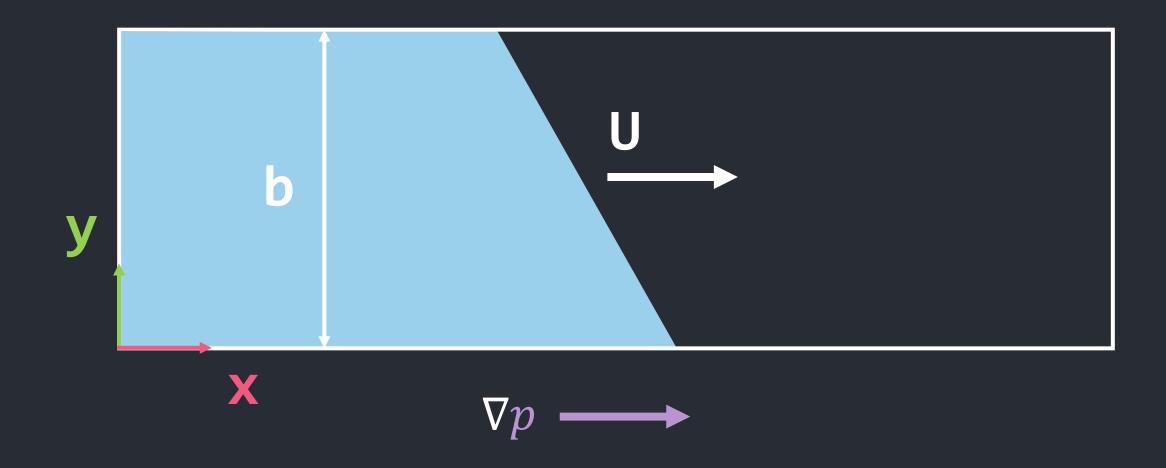
#### Navier-Stokes Equation

$$\rho \left( \frac{\partial u}{\partial t} + u \cdot \nabla u \right) = -\nabla p + \mu \nabla^2 u + \mathbf{F}$$

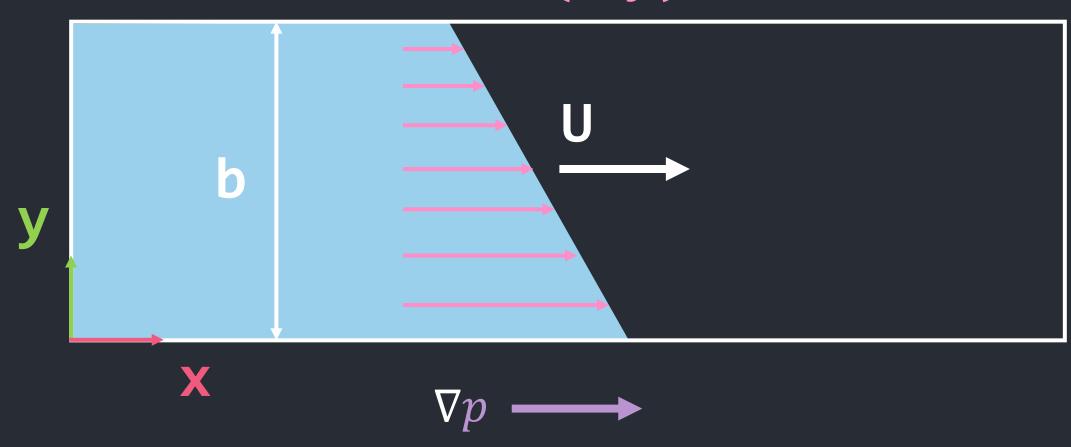




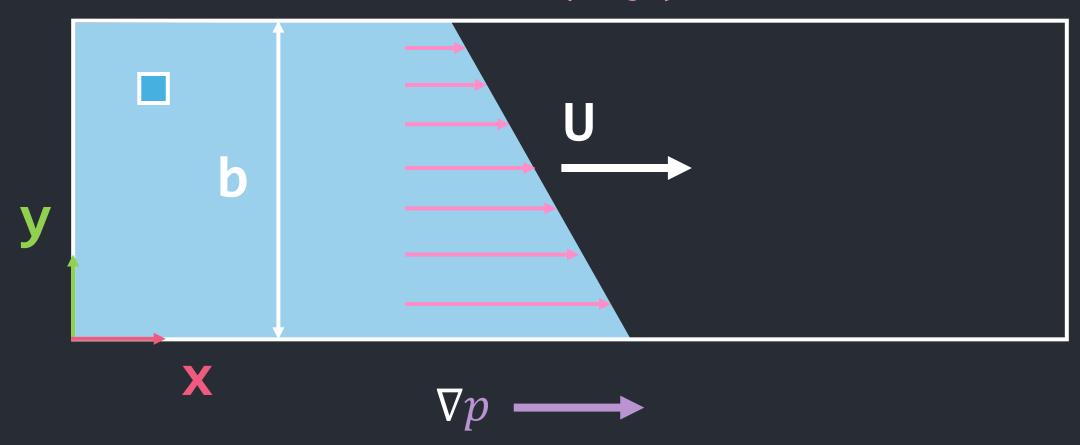


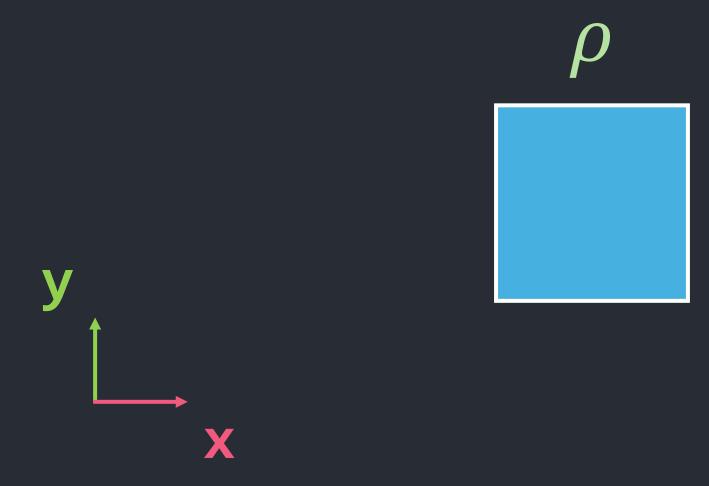


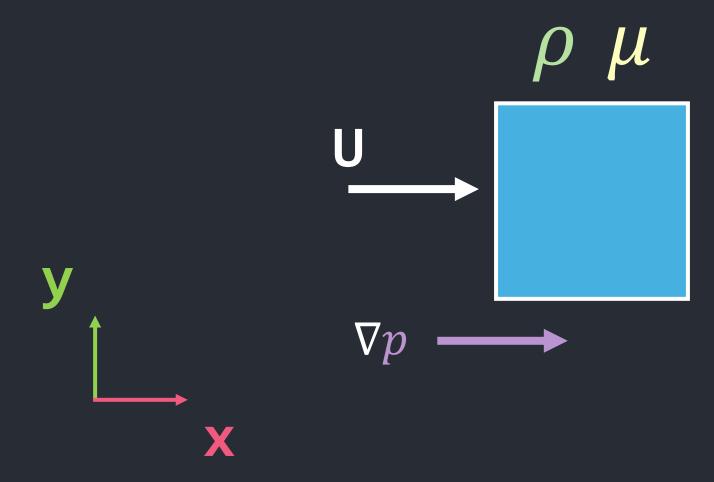
$$u=u(x,y)$$

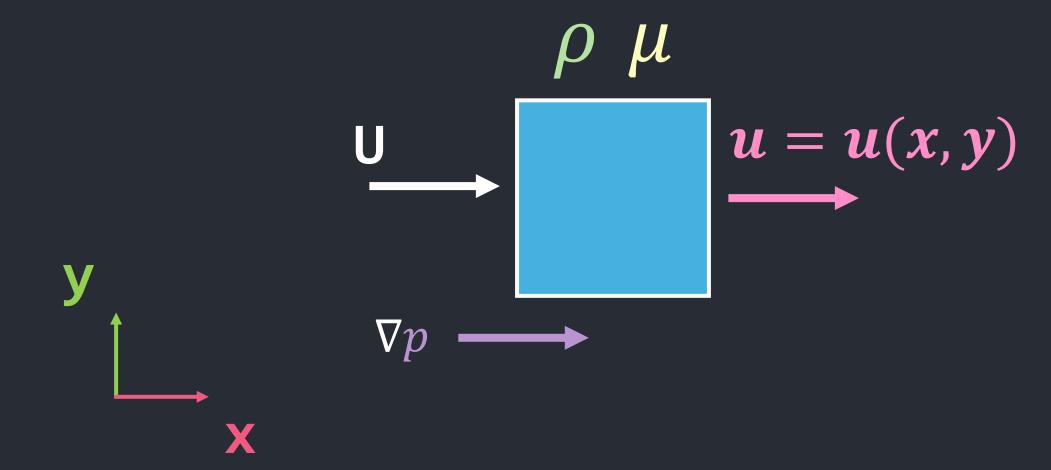


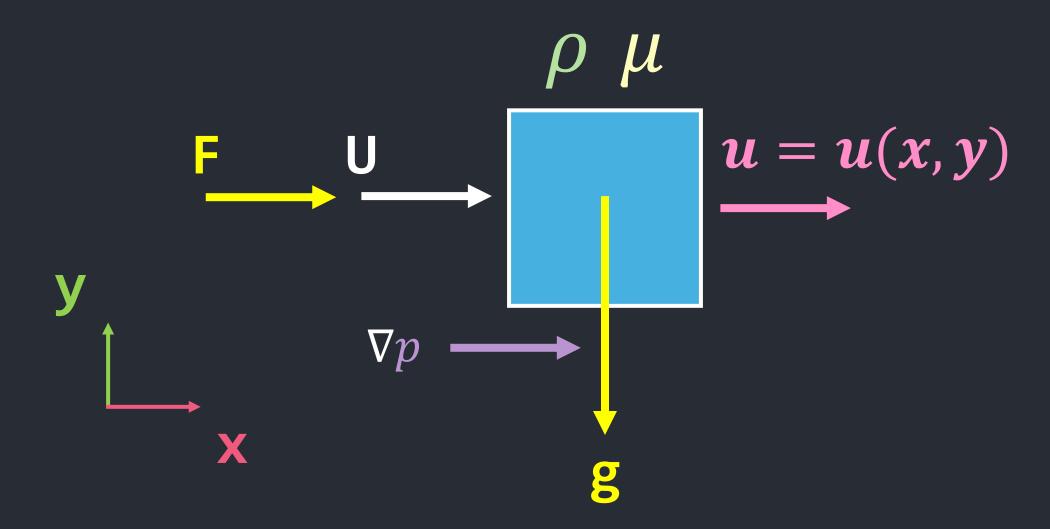
$$u=u(x,y)$$











#### Navier-Stokes Equation

$$\rho \left( \frac{\partial u}{\partial t} + u \cdot \nabla u \right) = -\nabla p + \mu \nabla^2 u + \mathbf{F}$$

- $u \rightarrow Speed: m/s$
- $\rho \rightarrow Fluid Density: kg/m^2$
- $p \rightarrow Pressure$ : Pa
- $\mu \rightarrow Dynamic Viscousity: Pa$
- $F \rightarrow External Force: N$
- $t \rightarrow Time: s$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

#### Newton's 2nd Law

$$ma = \sum F$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

 $\frac{ma}{V}$ 

$$\rho\left(\frac{\partial u}{\partial t} + u \cdot \nabla u\right) = -\nabla p + \mu \nabla^2 u + F$$

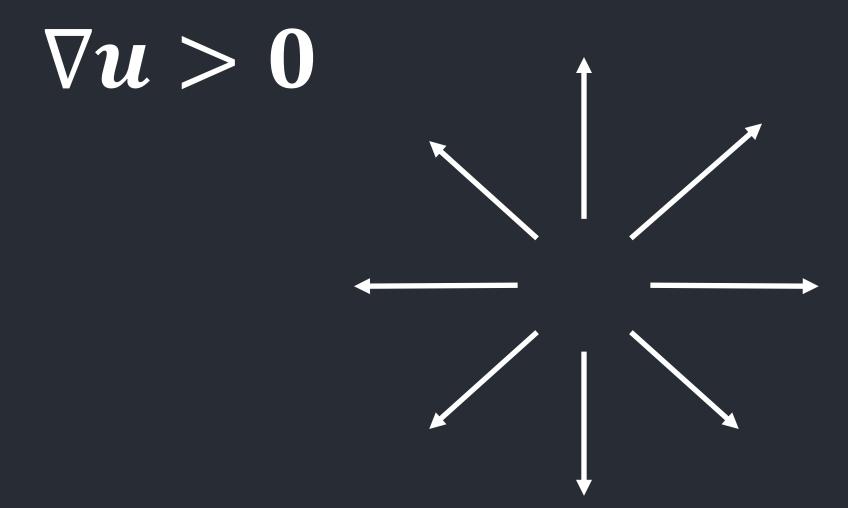
$$\frac{ma}{V}$$

## Divergence

 $\nabla \cdot u$ 

$$u = u(x, y)$$

$$\nabla \cdot \boldsymbol{u} = \operatorname{div} \boldsymbol{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y}$$





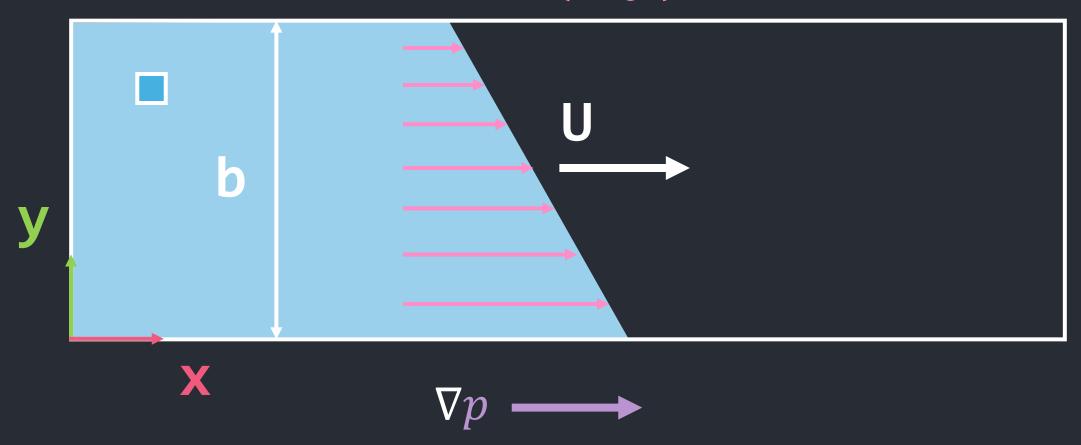
## $\nabla u = 0$



# Incompressible Flow (AKA: Continuity Equation)

$$\nabla \cdot \boldsymbol{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

$$u=u(x,y)$$



#### Conditions

- No flow in vertical direction  $\rightarrow u_y = 0 \frac{m}{s}$
- Flow driven by pressure gradient  $\rightarrow \frac{\partial p}{\partial x} \neq 0$   $\frac{Pa}{m}$
- No gravity effects  $\rightarrow g = 0 \frac{m}{s^2}$
- Boundary of the pipe  $\rightarrow y = [0, b]$
- Incompressible Flow  $\rightarrow \nabla u = 0$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \left( u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

#### Incompressible Flow

(Continuity Equation)

$$\nabla \cdot \boldsymbol{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

## Fully Developed Flow

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

## Fully Developed Flow

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

O Noflowin y

## Fully Developed Flow

$$\frac{\partial u_{x}}{\partial x} = \mathbf{0}$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \left( u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

Steady Flow No flow in y

No g effects

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \left( u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

Fully Developed

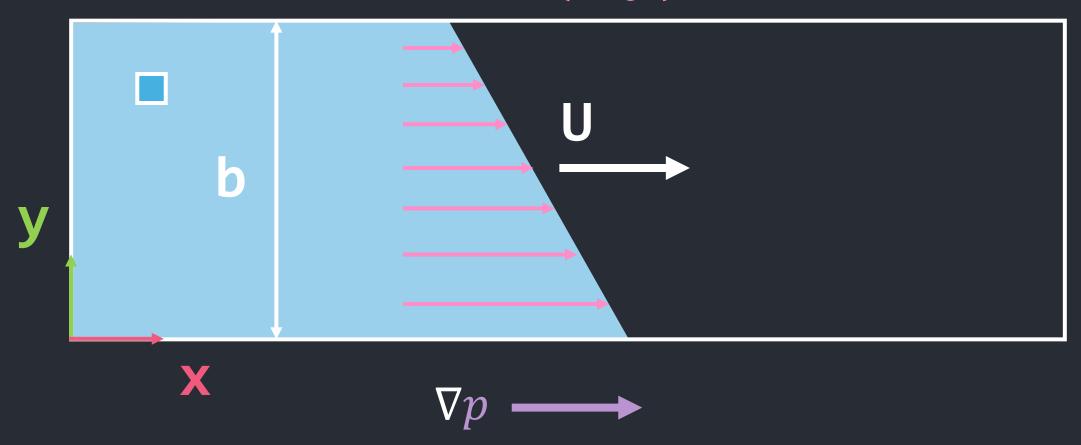
$$0 = -\nabla p + \mu \nabla^2 \mathbf{u}$$

#### Fully Developed

$$0 = -\nabla p + \mu \left( \frac{\partial^2 u_x}{\partial x^2} + \frac{\partial^2 u_x}{\partial y^2} \right)$$

$$0 = -\nabla p + \mu \left( \frac{\partial^2 u_x}{\partial y^2} \right)$$

$$u=u(x,y)$$



#### Flow Profile

$$u(y) = ???$$

$$0 = -\nabla p + \mu \left( \frac{\partial^2 u_x}{\partial y^2} \right)$$

$$\frac{\partial^2 u_x}{\partial y^2} = \frac{1}{\mu} \nabla p = const$$

### Flow Profile

$$u(y) = \frac{1}{2\mu} \nabla p(b^2 - by) + U\left(1 - \frac{y}{b}\right)$$

$$b = 360 m$$

$$U = 20 \frac{m}{s}$$

$$\mu = 1001600.0 Pa \cdot s$$

$$\nabla p = 20 \frac{Pa}{m}$$