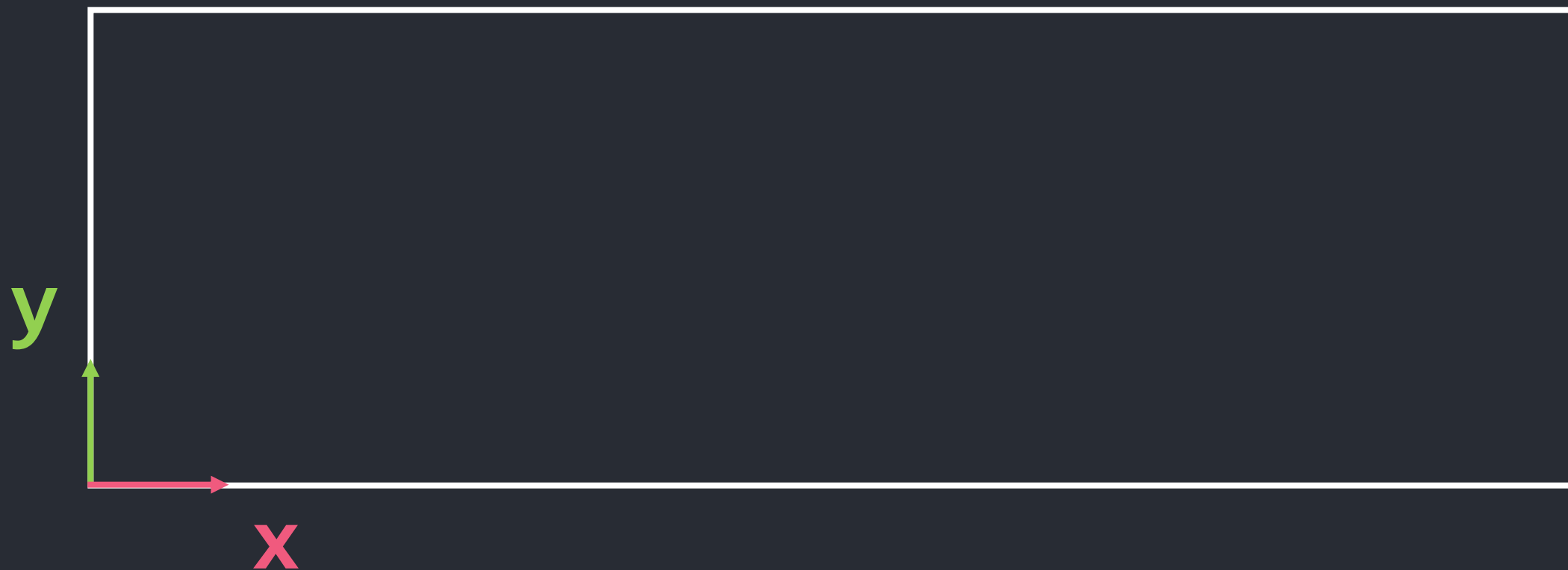


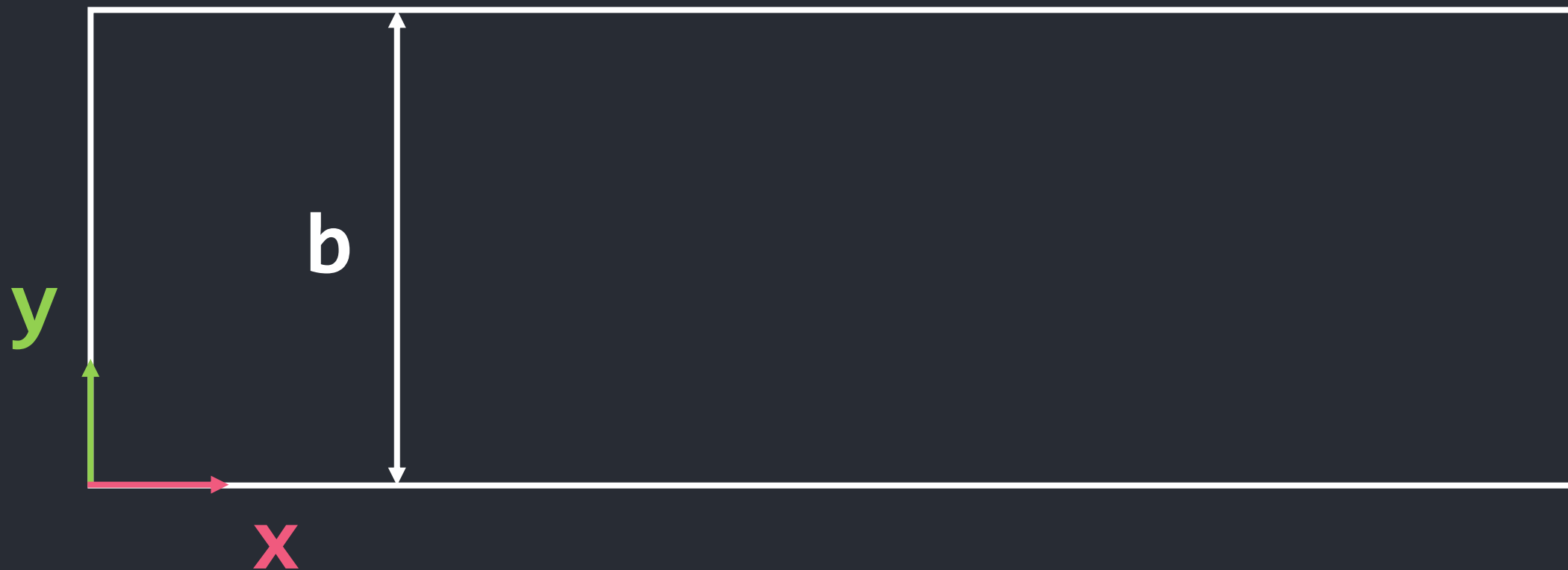
$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

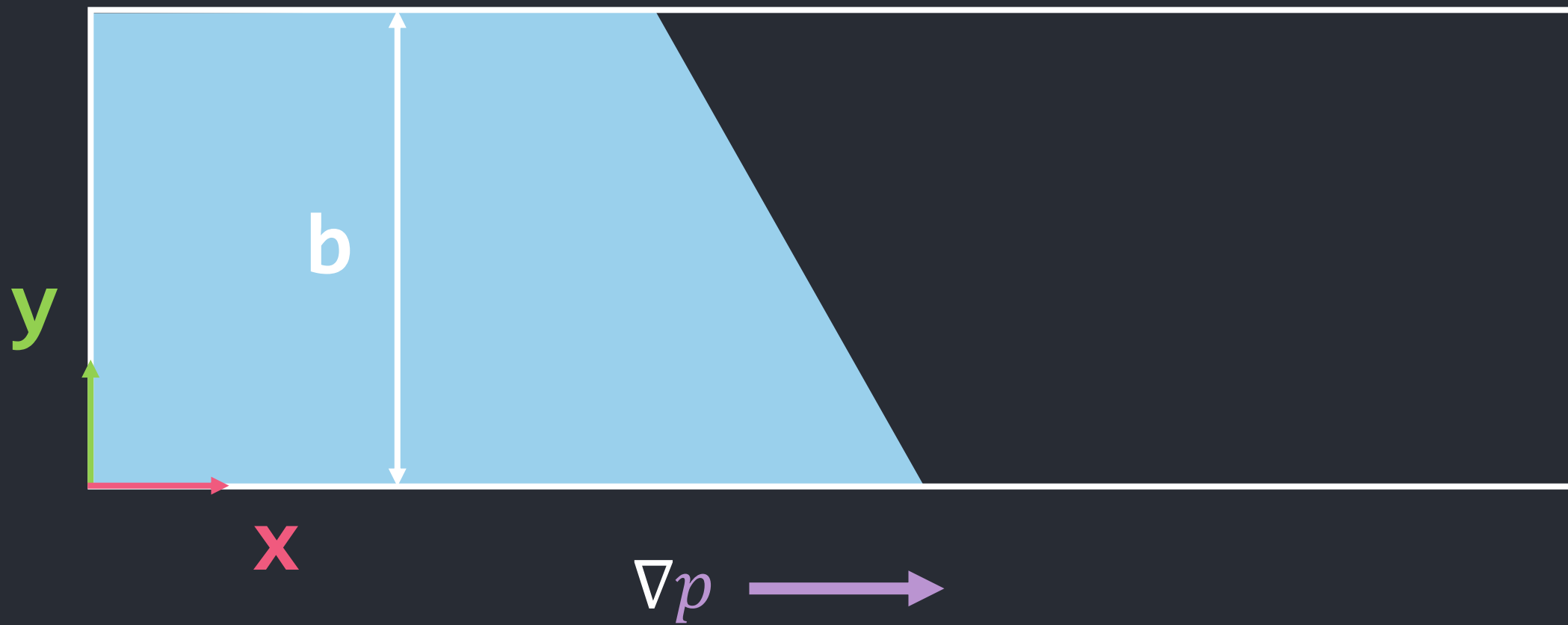
$$= -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

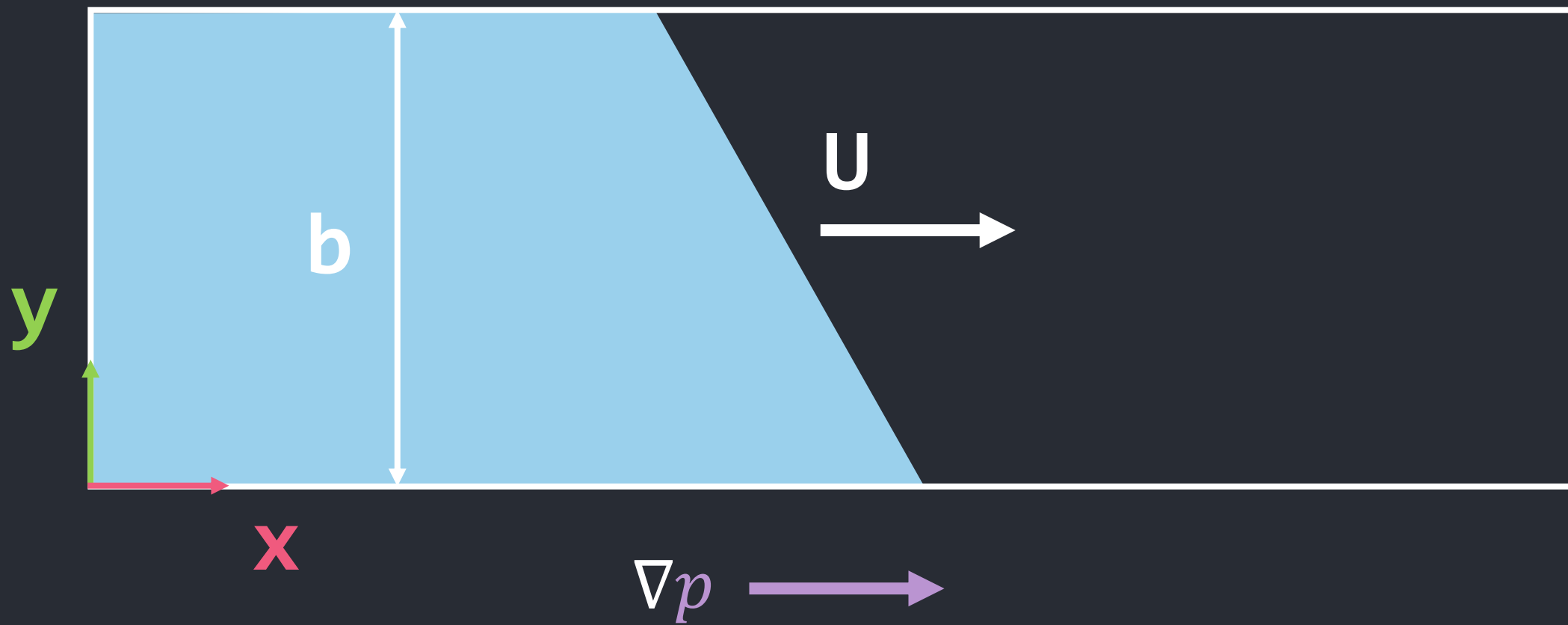
# Navier-Stokes Equation

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

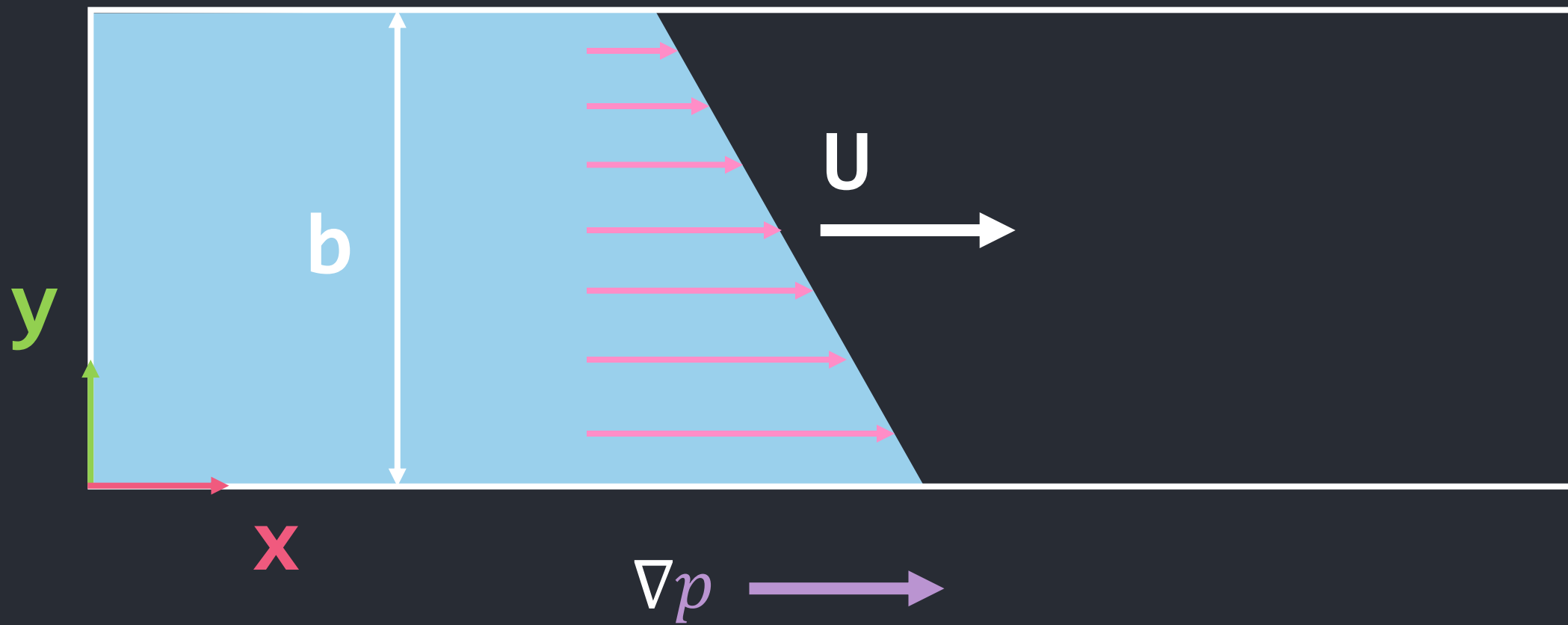




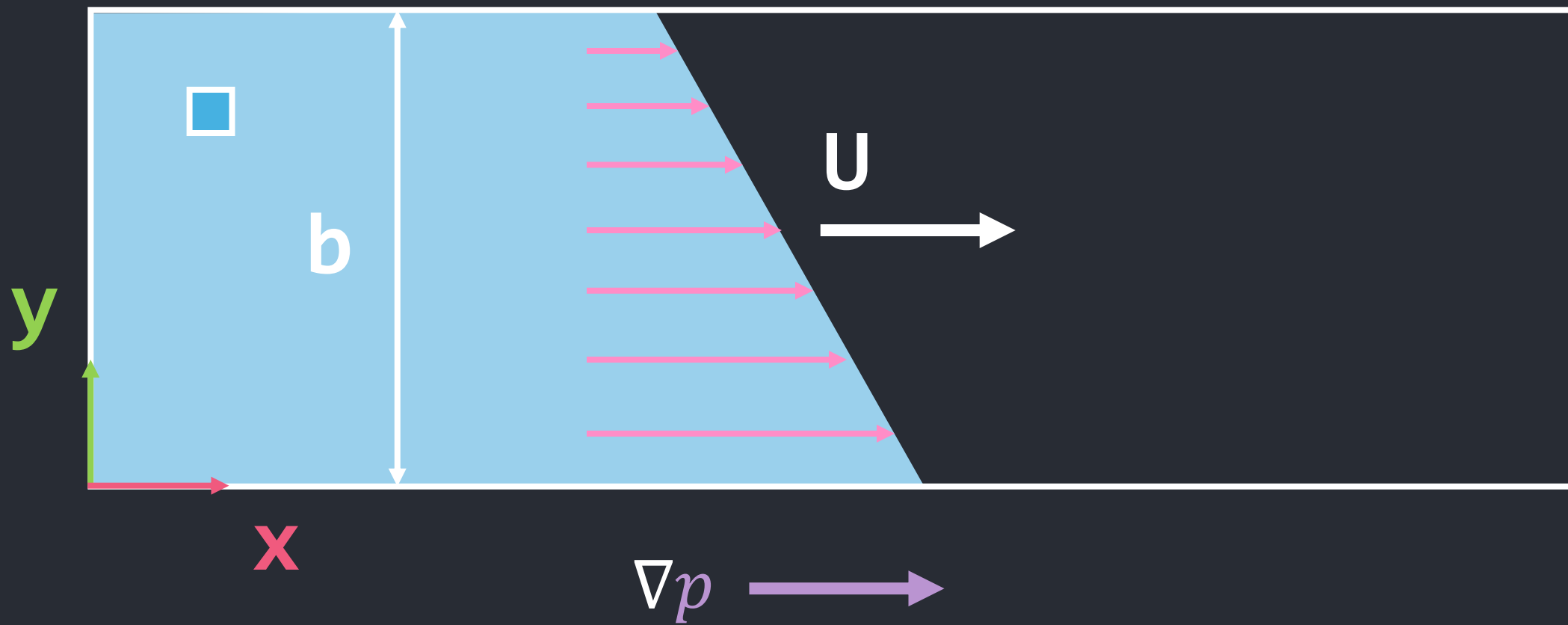




$$u = u(x, y)$$



$$u = u(x, y)$$



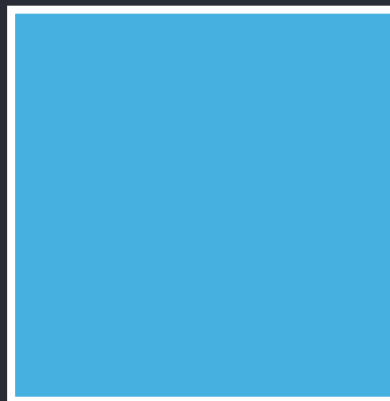


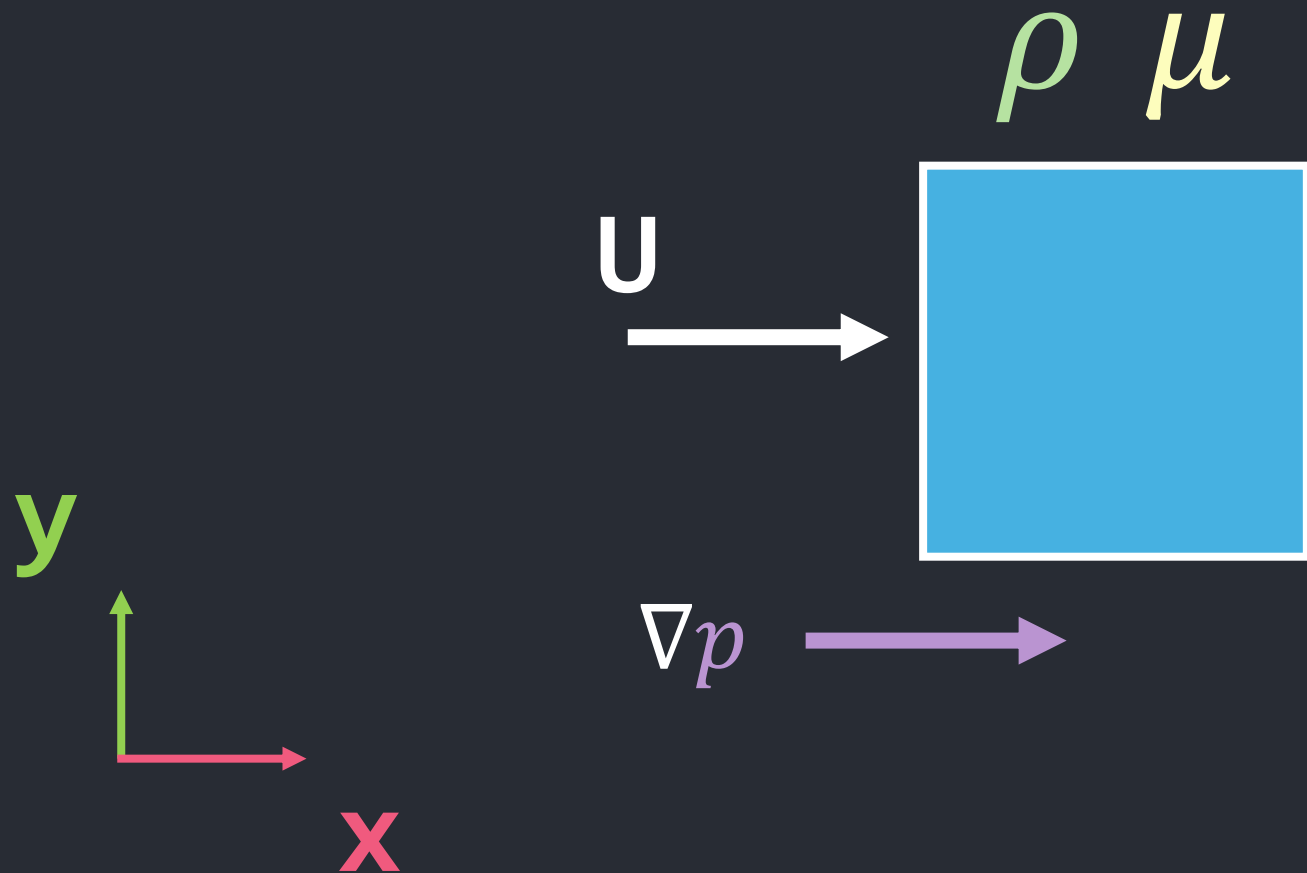
$y$

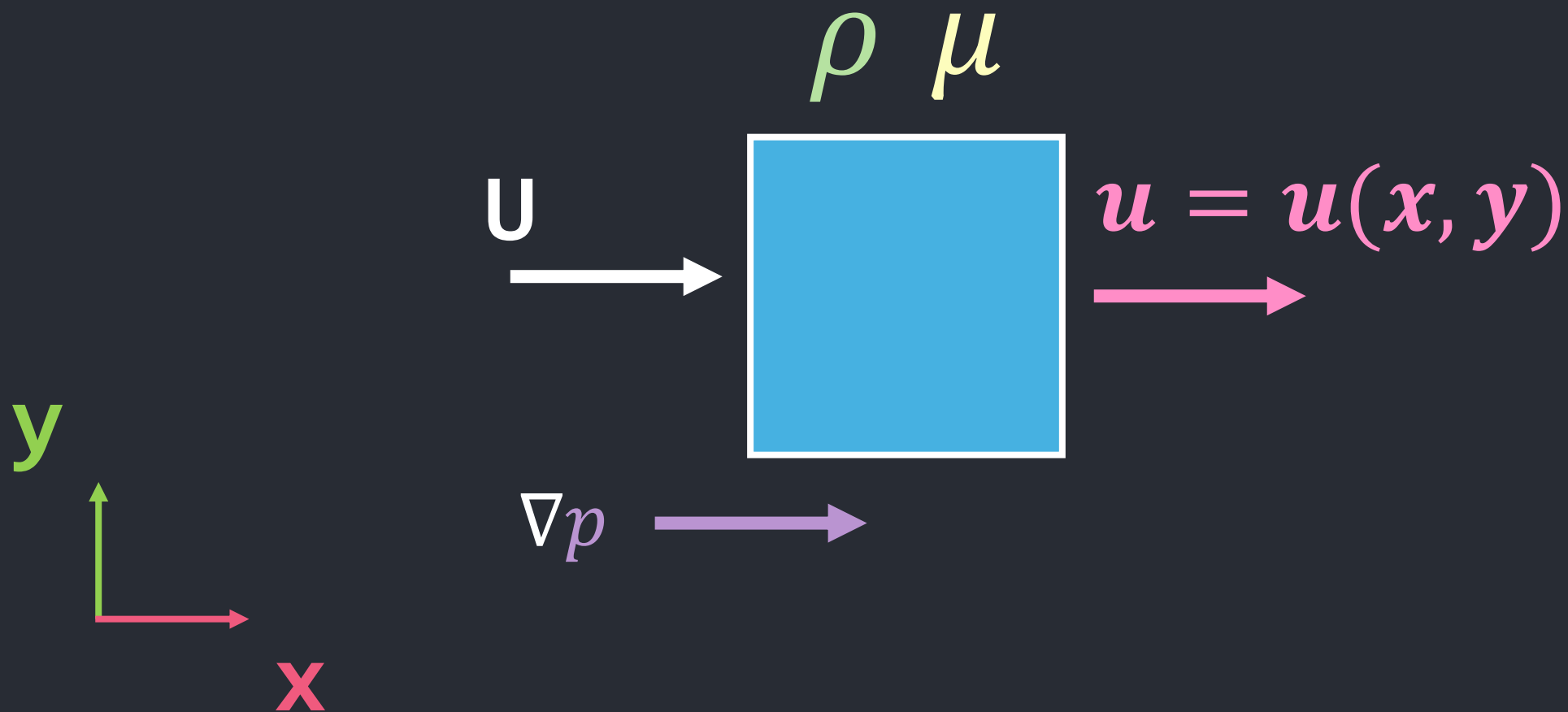


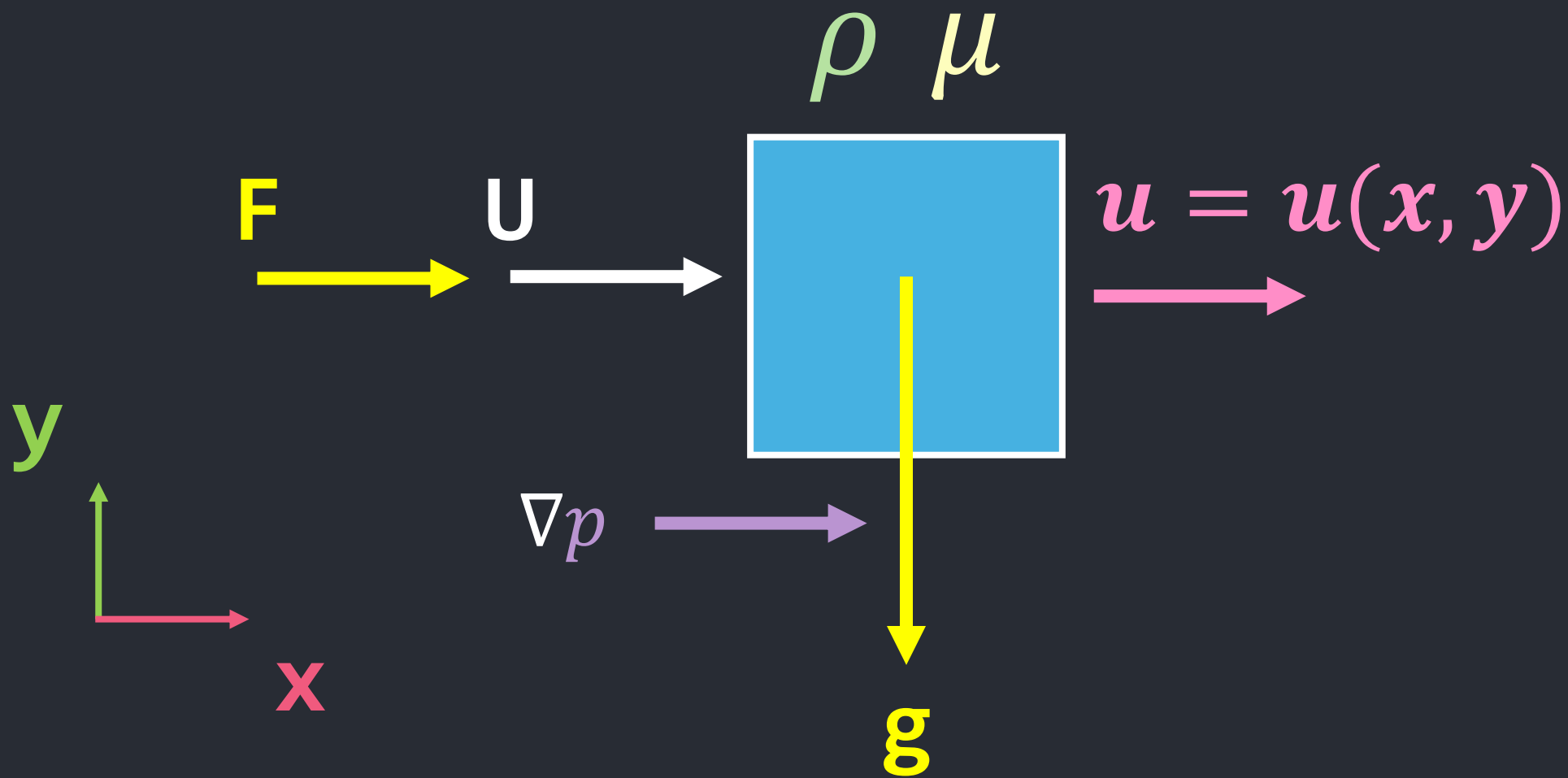
$x$

$\rho$









# Navier-Stokes Equation

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

$\mathbf{u} \rightarrow \text{Speed: } m/s$

$\rho \rightarrow \text{Fluid Density: } kg/m^2$

$p \rightarrow \text{Pressure: } Pa$

$\mu \rightarrow \text{Dynamic Viscosity: } Pa$

$\mathbf{F} \rightarrow \text{External Force: } N$

$t \rightarrow \text{Time: } s$

$$\rho \left( \frac{\partial \boldsymbol{u}}{\partial t} + \boldsymbol{u} \cdot \nabla \boldsymbol{u} \right) = -\nabla p + \mu \nabla^2 \boldsymbol{u} + \boldsymbol{F}$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$

*Newton's 2nd Law*

$$m\mathbf{a} = \sum \mathbf{F}$$



$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}$$



$ma$

$\frac{ma}{V}$

$$\underbrace{\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right)}_{\frac{ma}{V}} = \underbrace{-\nabla p + \mu \nabla^2 \mathbf{u} + \mathbf{F}}_{\frac{F}{\bar{V}}}$$

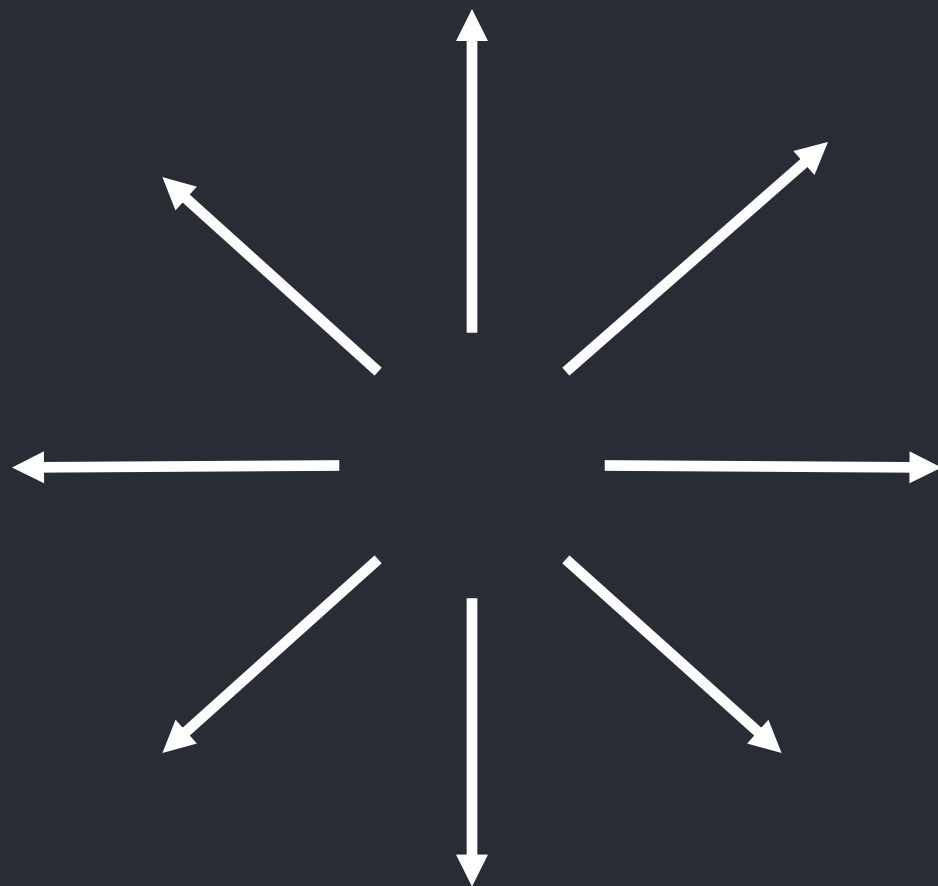
*Divergence*

$$\nabla \cdot \boldsymbol{u}$$

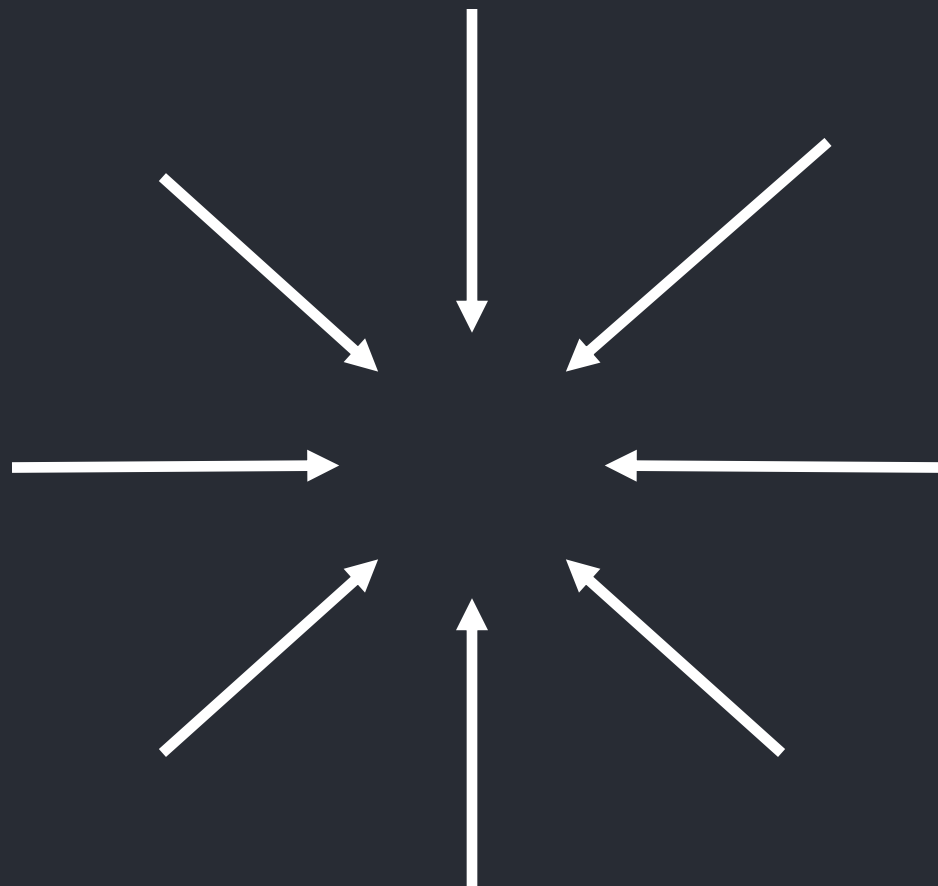
$$\boldsymbol{u} = u(x, y)$$

$$\nabla \cdot \boldsymbol{u} = \operatorname{div} \boldsymbol{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y}$$

$$\nabla u > 0$$



$$\nabla u < 0$$



$$\nabla u = 0$$



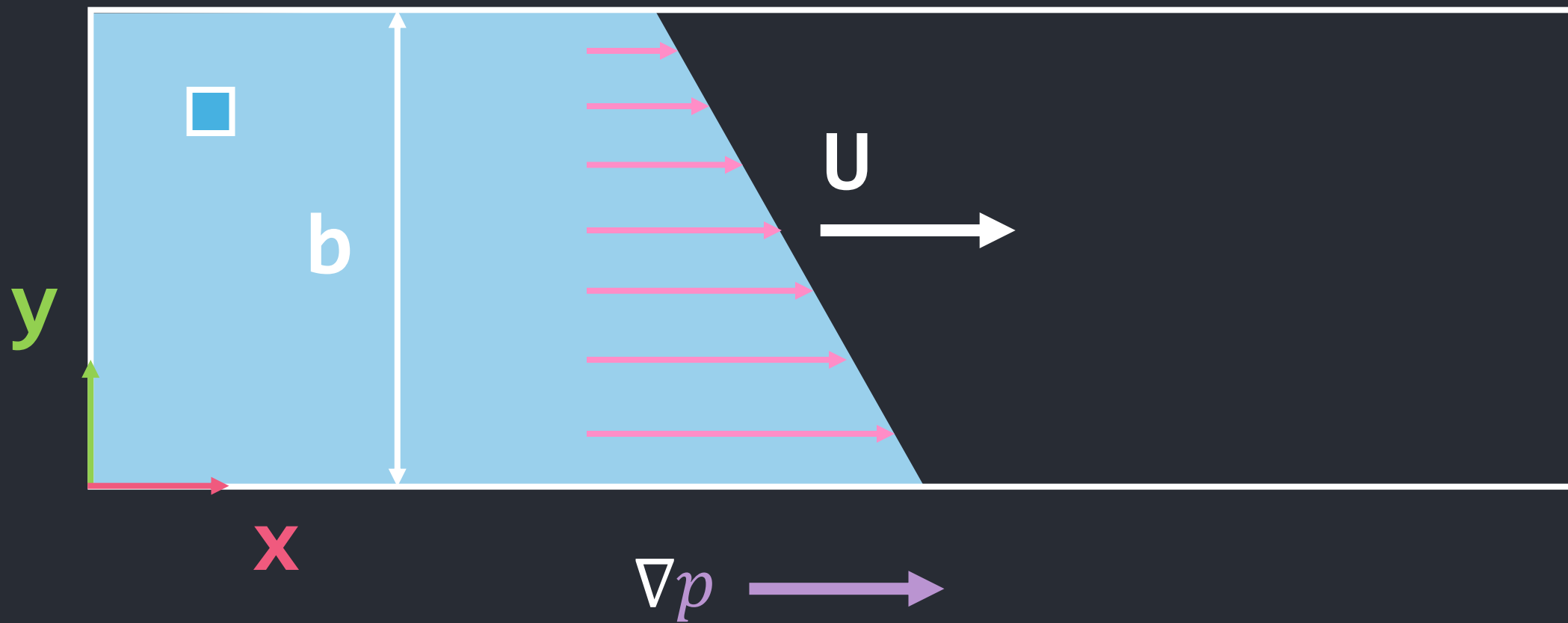
# *Incompressible Flow*

*(AKA: Continuity Equation)*

$$\nabla \cdot \mathbf{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$



$$u = u(x, y)$$



# Conditions

- *No flow in vertical direction  $\rightarrow u_y = 0 \frac{m}{s}$*
- *Flow driven by pressure gradient  $\rightarrow \frac{\partial p}{\partial x} \neq 0 \frac{Pa}{m}$*
- *No gravity effects  $\rightarrow g = 0 \frac{m}{s^2}$*
- *Boundary of the pipe  $\rightarrow y = [0, b]$*
- *Incompressible Flow  $\rightarrow \nabla \mathbf{u} = \mathbf{0}$*

$$\rho \left( \frac{\partial \boldsymbol{u}}{\partial t} + \boldsymbol{u} \cdot \nabla \boldsymbol{u} \right) = -\nabla p + \mu \nabla^2 \boldsymbol{u} + \boldsymbol{F}$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \left( u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

# *Incompressible Flow*

*(Continuity Equation)*

$$\nabla \cdot \mathbf{u} = \frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

# *Fully Developed Flow*

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

# *Fully Developed Flow*

$$\frac{\partial u_x}{\partial x} + \frac{\partial u_y}{\partial y} = 0$$

*0 No flow in y*

# *Fully Developed Flow*

$$\frac{\partial u_x}{\partial x} = 0$$



$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \left( u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

*Steady Flow*

*No flow in y*

*No g effects*

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \left( u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right) \right) = -\nabla p + \mu \nabla^2 \mathbf{u} + \rho g$$

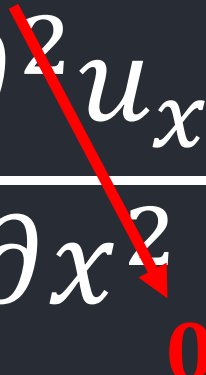
Diagram illustrating the simplification of the Navier-Stokes equation for a fully developed flow. Red arrows point from the following terms to a red '0' below them:

- $\frac{\partial \mathbf{u}}{\partial t}$  (labeled *Steady Flow*)
- $u_x \frac{\partial u_x}{\partial x}$  (labeled *No flow in y*)
- $u_y \frac{\partial u_x}{\partial y}$  (labeled *No flow in y*)
- $\rho g$  (labeled *No g effects*)

*Fully Developed*

$$0 = -\nabla p + \mu \nabla^2 u$$

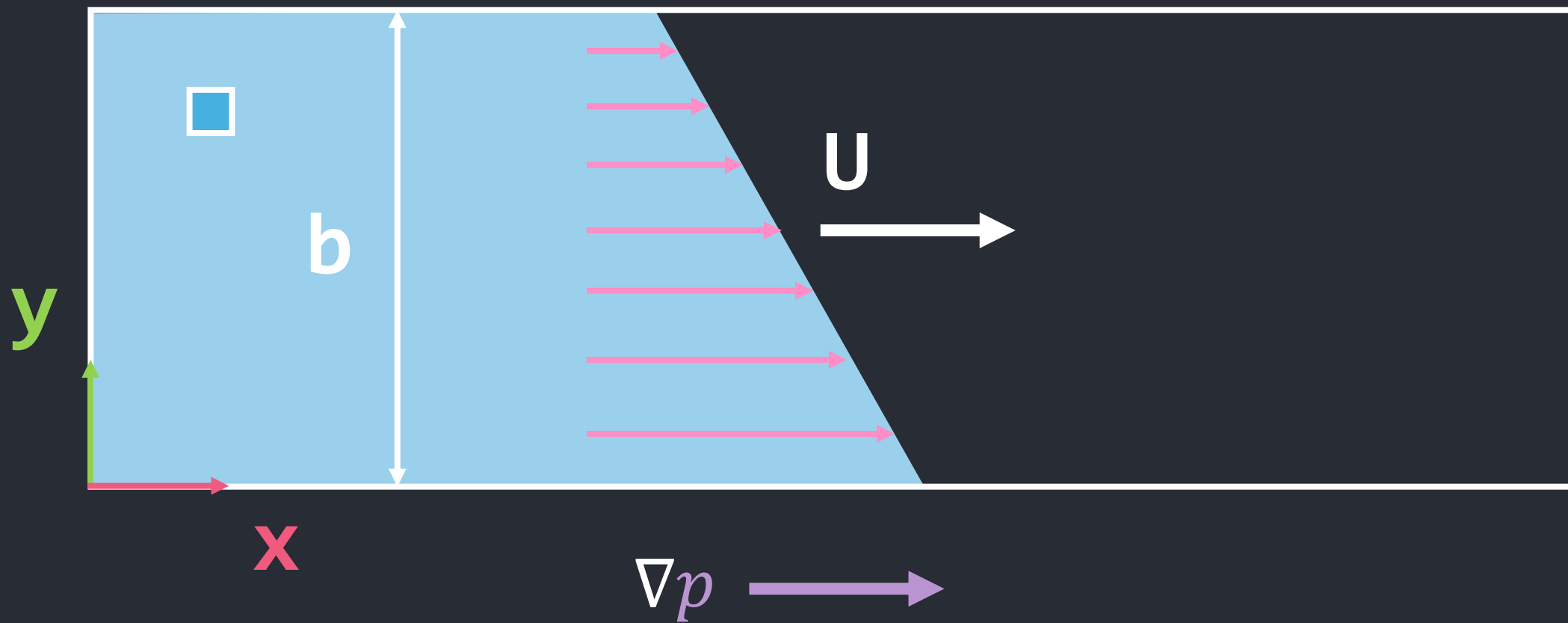
*Fully Developed*

$$0 = -\nabla p + \mu \left( \frac{\partial^2 u_x}{\partial x^2} + \frac{\partial^2 u_x}{\partial y^2} \right)$$


A red arrow points from the top of the  $\frac{\partial^2 u_x}{\partial x^2}$  term to a red zero located below the  $\partial x^2$  denominator.

$$0 = -\nabla p + \mu \left( \frac{\partial^2 u_x}{\partial y^2} \right)$$

$$u = u(x, y)$$



# *Flow Profile*

$$u(y) = ???$$

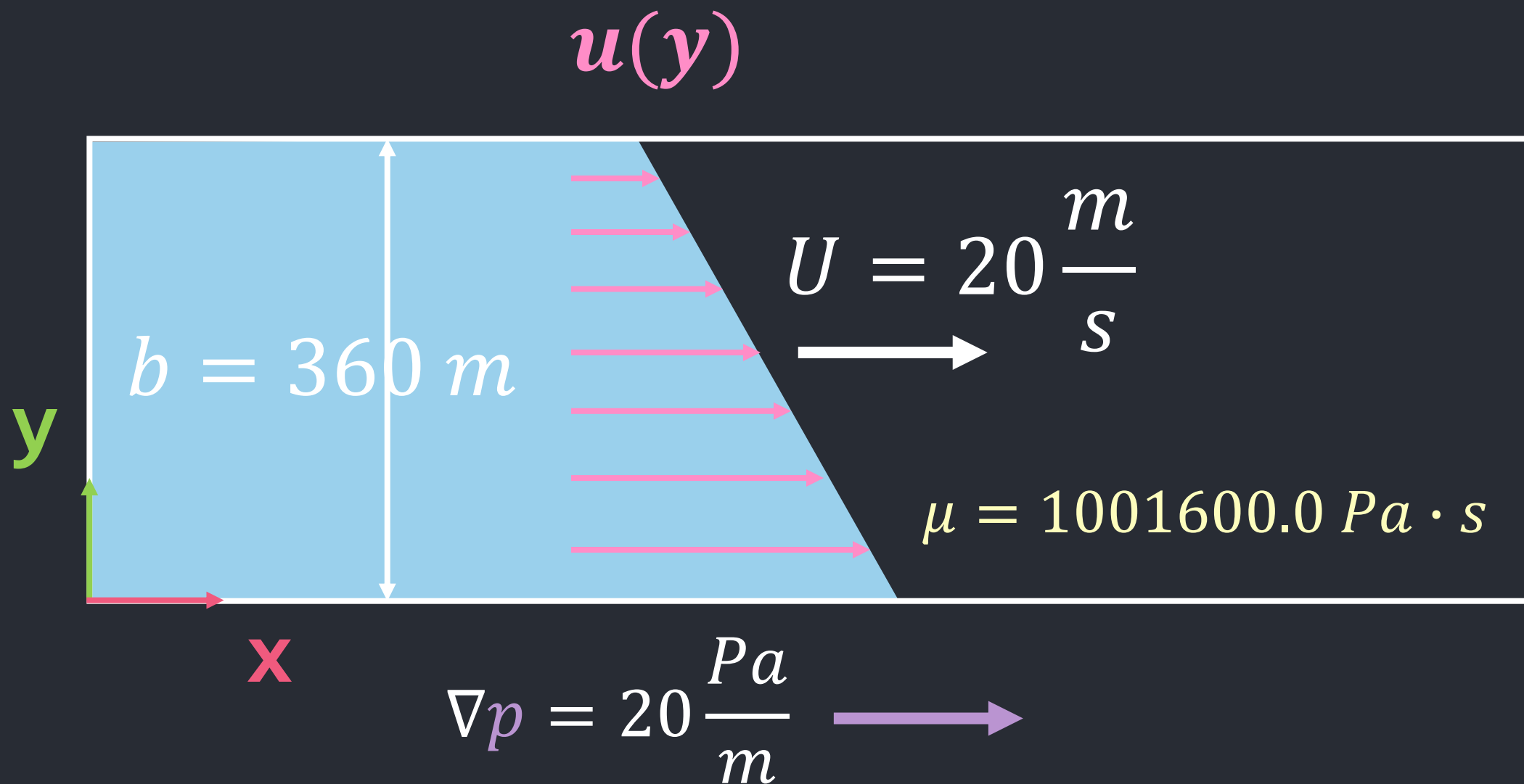
$$0 = -\nabla p + \mu \left( \frac{\partial^2 u_x}{\partial y^2} \right)$$



$$\frac{\partial^2 u_x}{\partial y^2} = \frac{1}{\mu} \nabla p = \textit{const}$$

# *Flow Profile*

$$u(y) = \frac{1}{2\mu} \nabla p (b^2 - by) + U \left( 1 - \frac{y}{b} \right)$$



# Rust

+

# Bevy

