Spatiotemporal patterns in a porous catalyst

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Gradients in Porous Catalysts

Composition

Thermal

Especially under dynamic conditions!

How to measure?

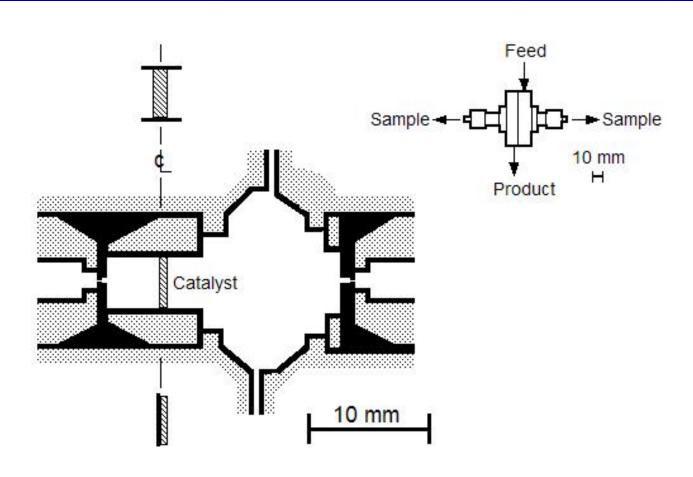
- Single Pellet Diffusion Reactor at steady state, Petersen and students
- Thermocouples in pellet, Butt and students
- Related infrared imaging parallel to pellet surface

Dynamic Diffusion Reactor

- Miniaturize single pellet diffusion reactor
- Minimize time constants

Measure composition continuously

Dynamic Diffusion Reactor



DDR - Types of Experiments

Inert response →

diffusion coefficients

Single species response →

adsorption coefficients

Reaction response →

reaction-diffusion model

DDR - Approach

- Measure concentration gradients
- Model with detailed kinetics

CO + S
$$\rightarrow$$
 S-CO
O₂ + 2S' \rightarrow 2 S'-O
S-CO + S'-O \rightarrow S + S' + CO₂

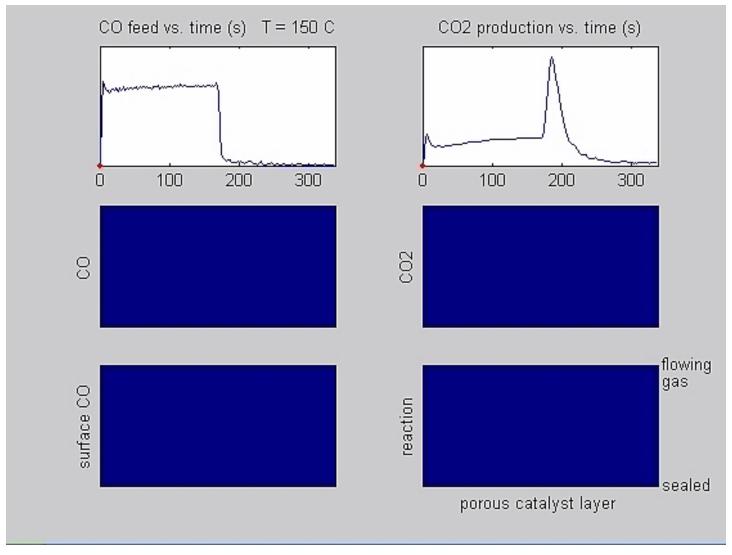
over multiple site types, don't assume adsorption equilibrium or rate-limiting step

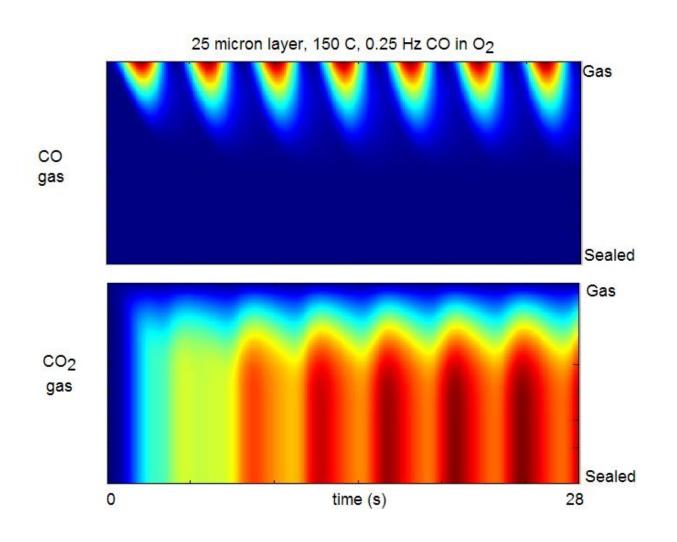
R. Herz & S. Marin, J.Catal. <u>65</u>, 281 (1980)

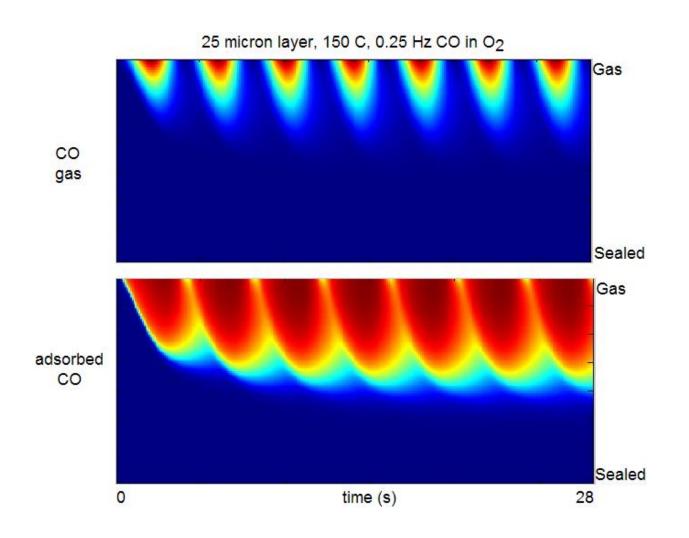
- Fit model to experiments
- Perform numerical experiments...

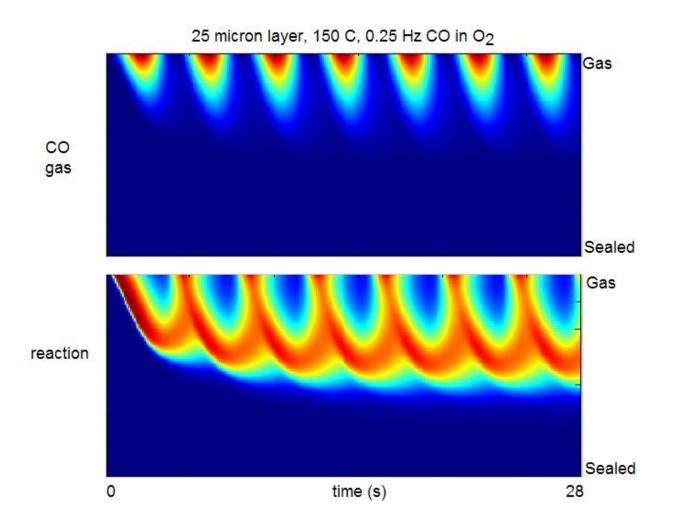
Step Responses

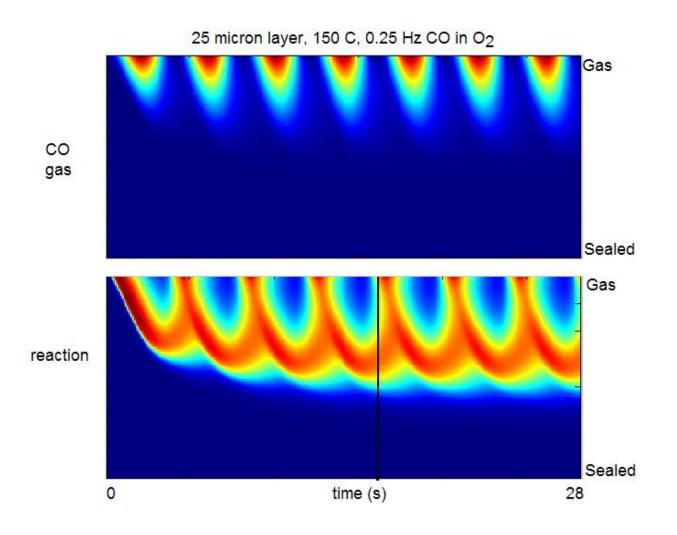
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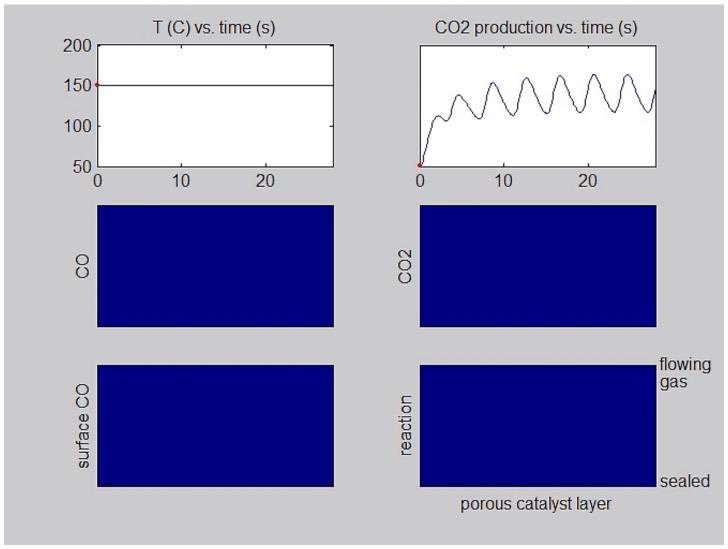


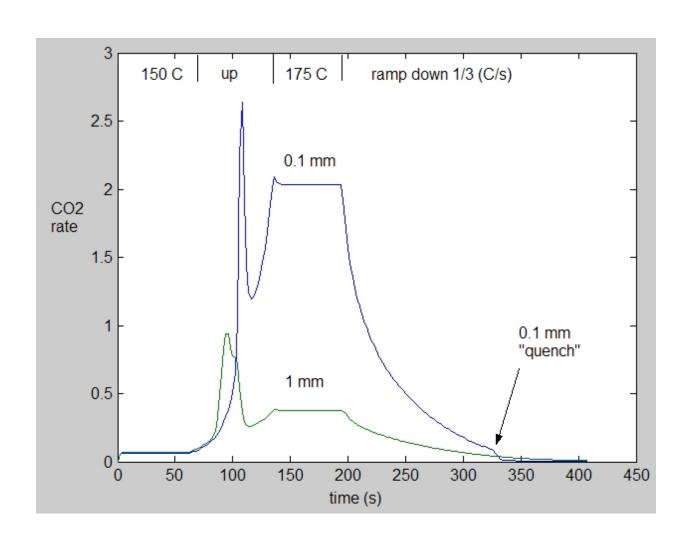




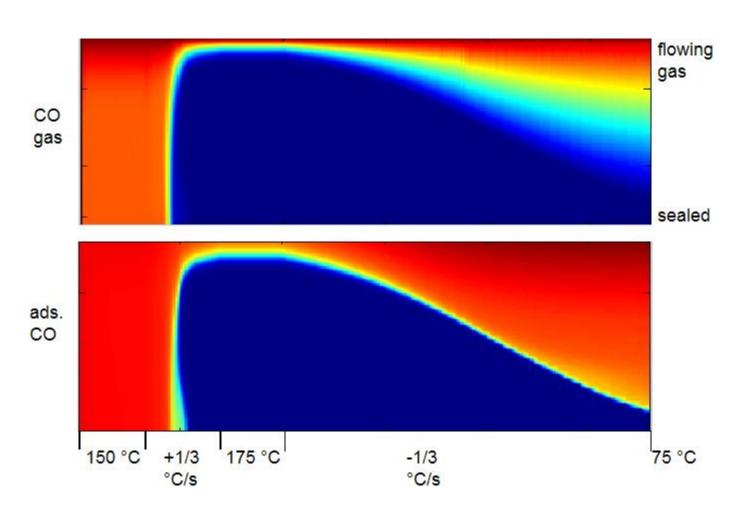


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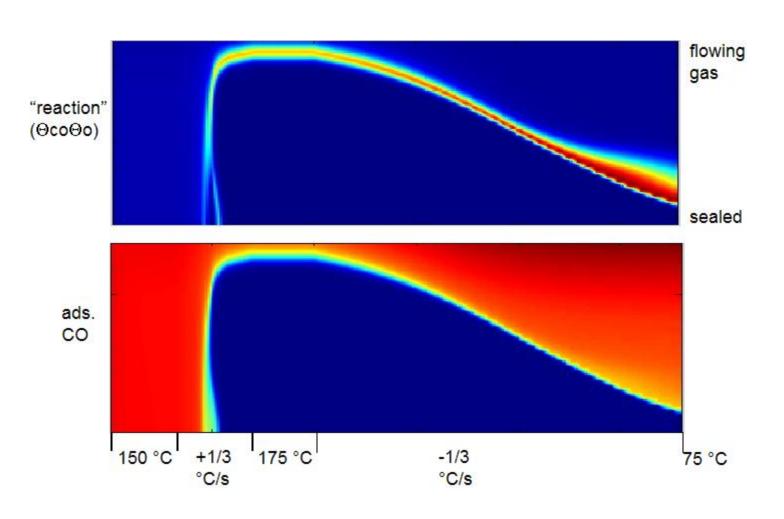




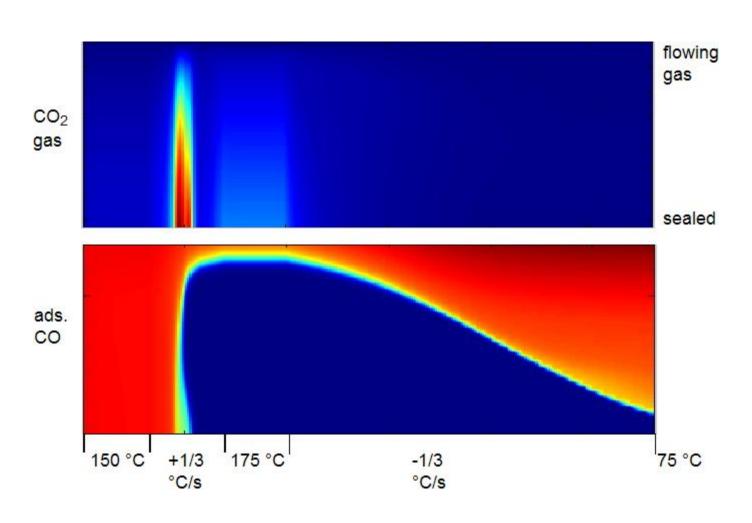
1 mm layer



1 mm layer

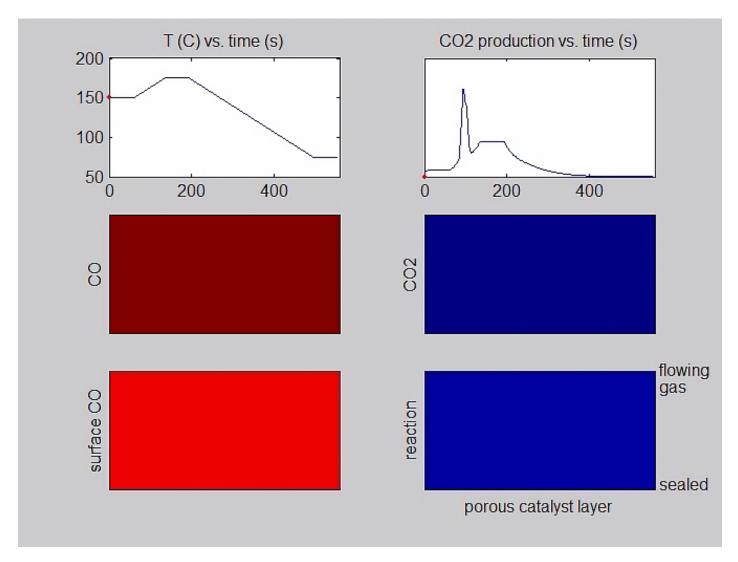


1 mm layer

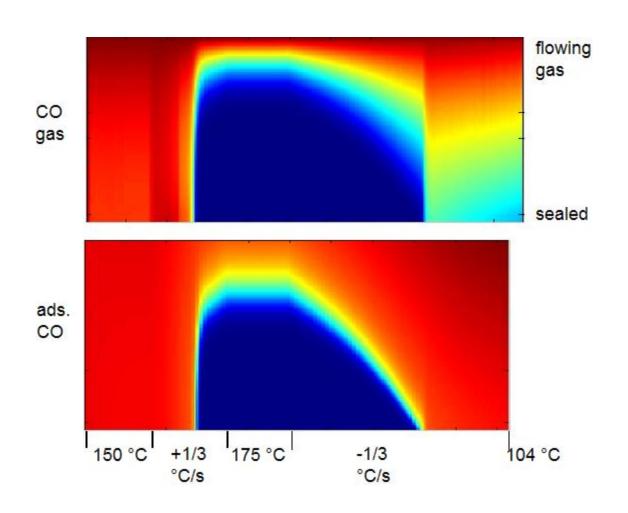


1 mm layer

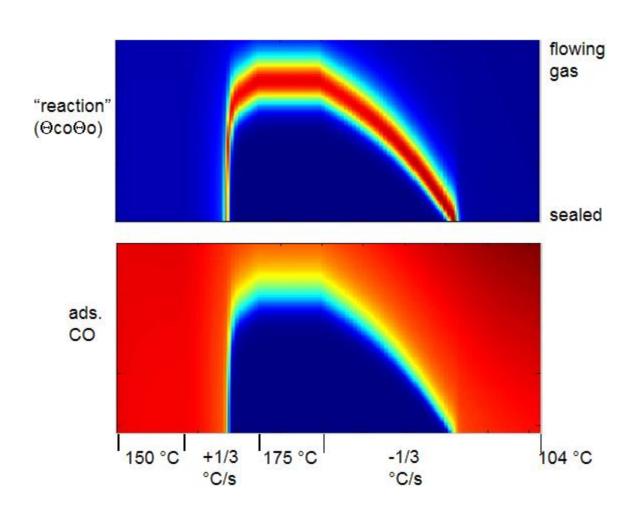
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0.1 mm layer

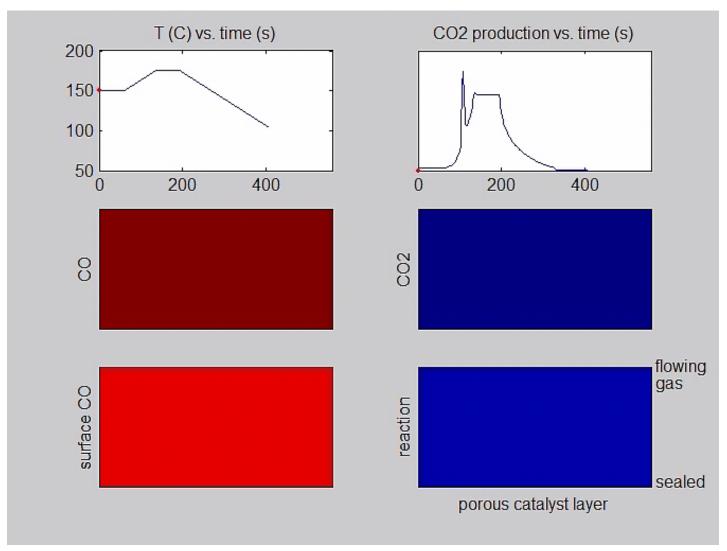


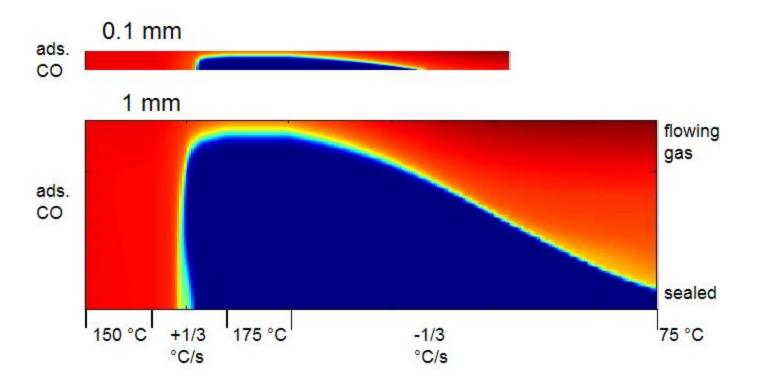
0.1 mm layer



0.1 mm layer

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- At constant total Pt, the following increase as catalyst thickness decreases:
 - overall reaction rate
 - "light off" temperature
 - "quench" temperature
- Thus, the catalyst is more active but over a narrow temperature range.

Patterns change with catalyst thickness:

1 mm – double reaction fronts move from center on "light-off"

0.1 mm – reaction "quenches" as CO front reaches center

≤ 0.06 mm – CO gas peaks in center, reaction front starts at exterior

Spatiotemporal Patterns

Questions?

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