

# SISTEMI ETEROGENEI

## **Metodi di separazione**

**Sistema eterogeneo → separazione delle fasi**

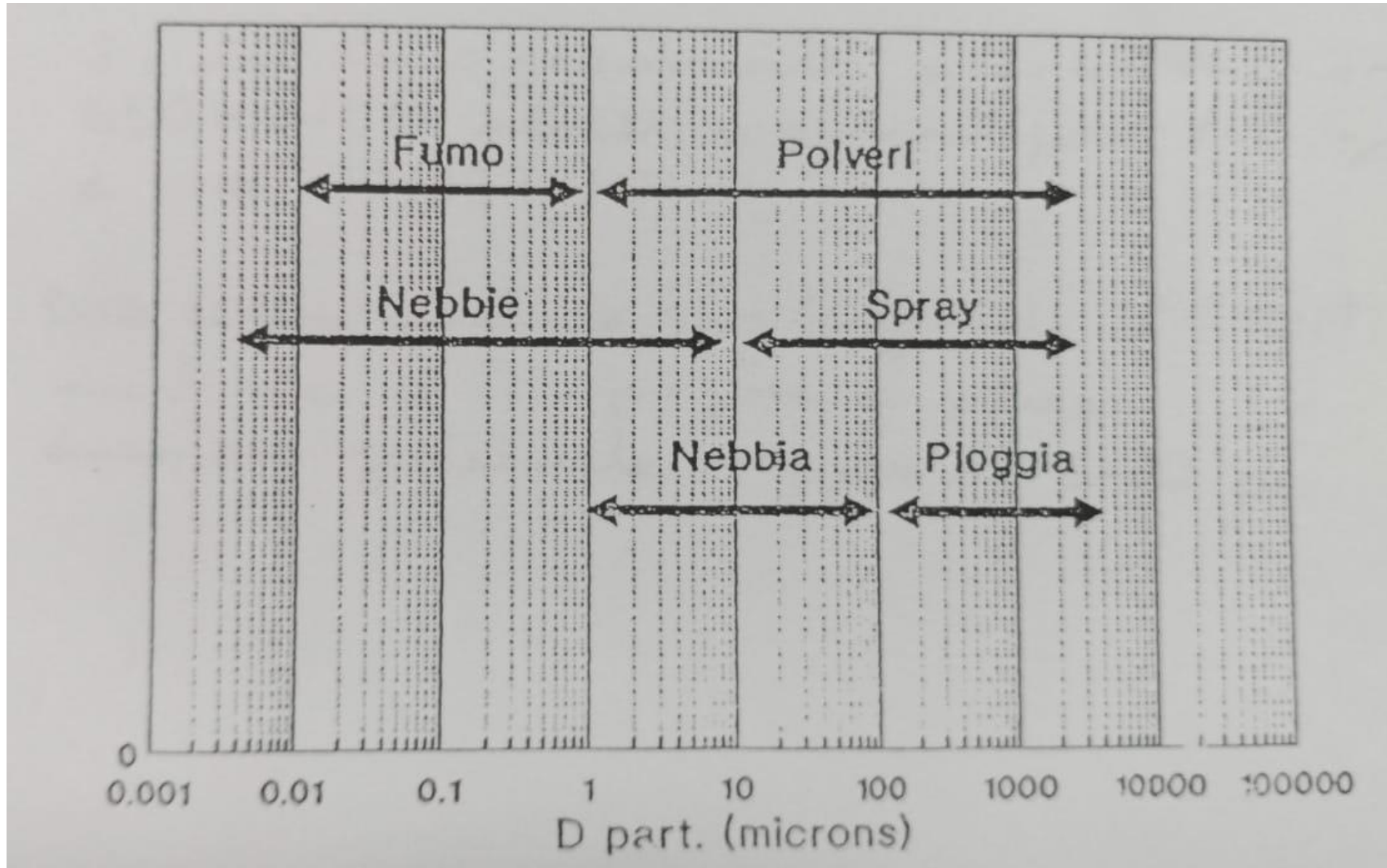
**Sistema omogeneo → creazione di una seconda fase e sua separazione**

**Se servono entrambe, si fa prima la separazione delle parti eterogenee**

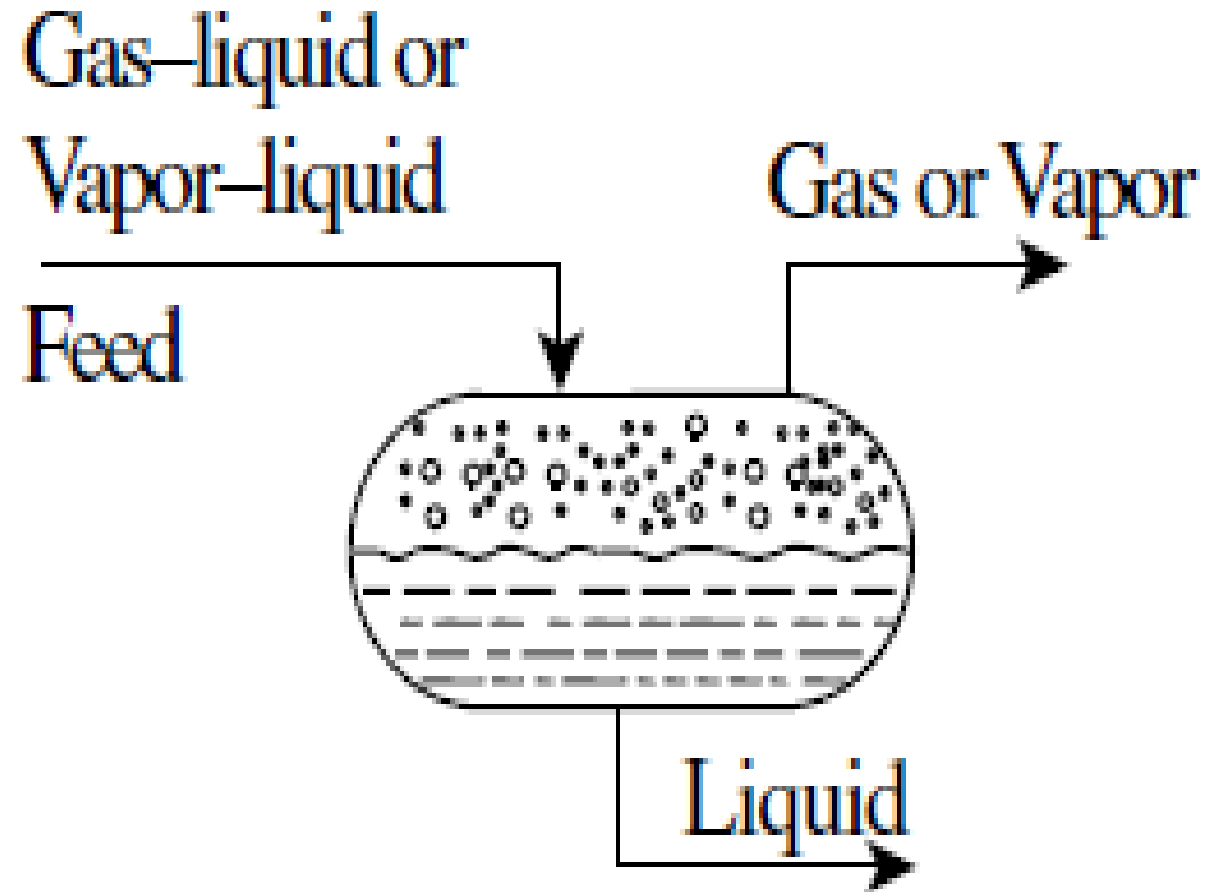
## **Sistema eterogeneo**

- **Gas-liquido (o vapore-liquido)**
- **Gas-solido (o vapore-solido)**
- **Liquido-liquido (immiscibili)**
- **Liquido-solido**
- **Solido-solido**

# Separazione da una fase gas

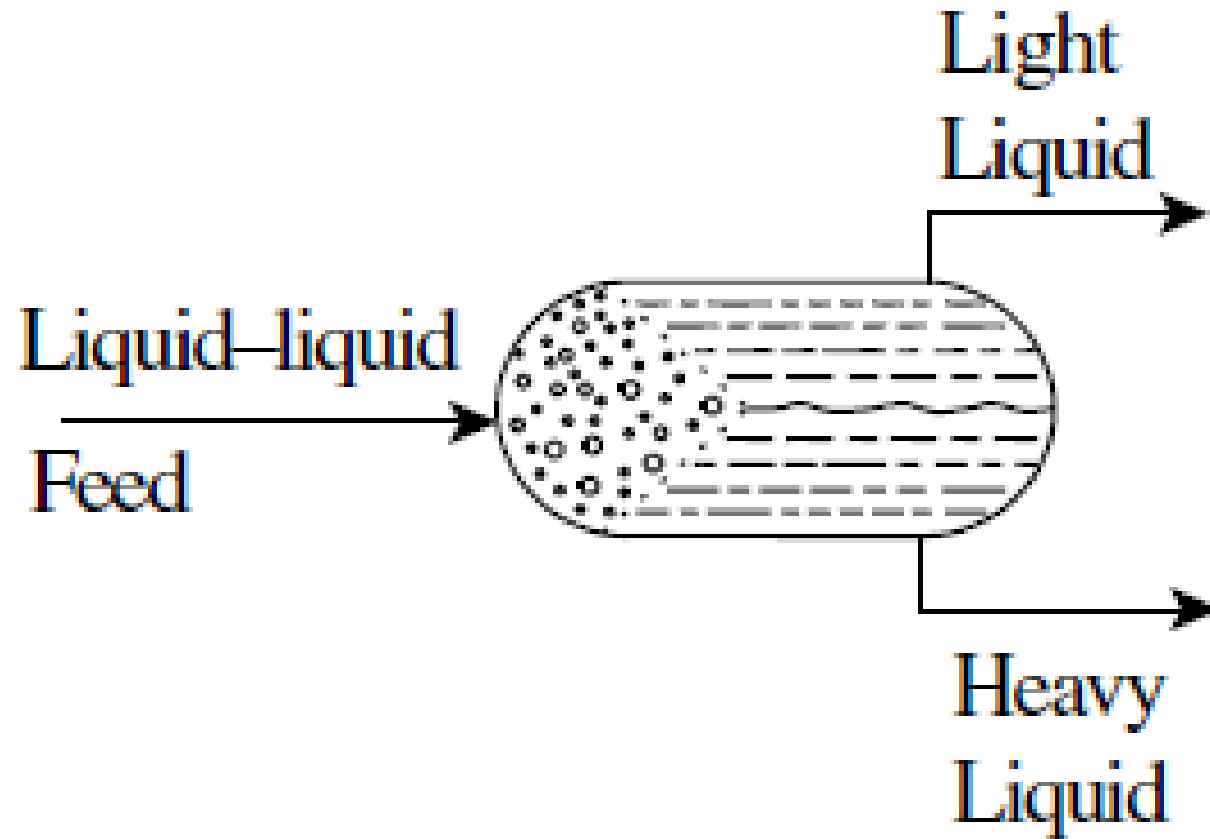


## Separatori gravitazionali

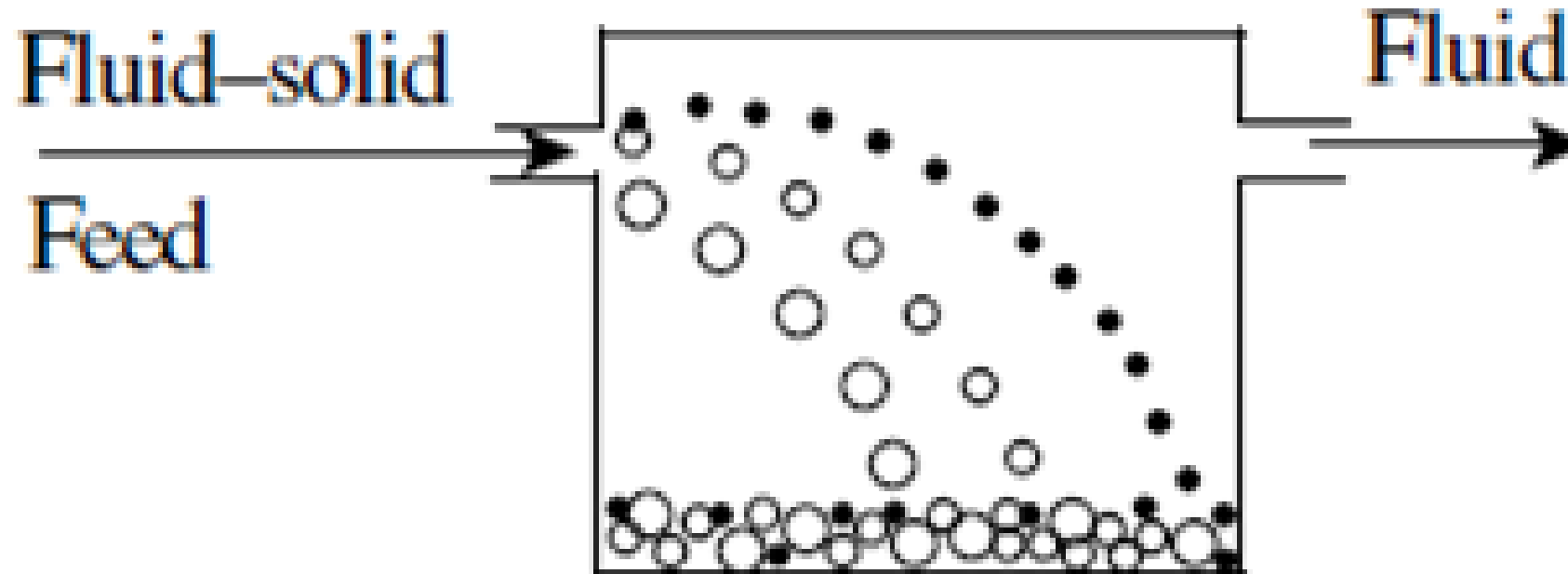


Separatore gravitazionale aeriforme-liquido

## Separatore gravitazionale liquido-liquido



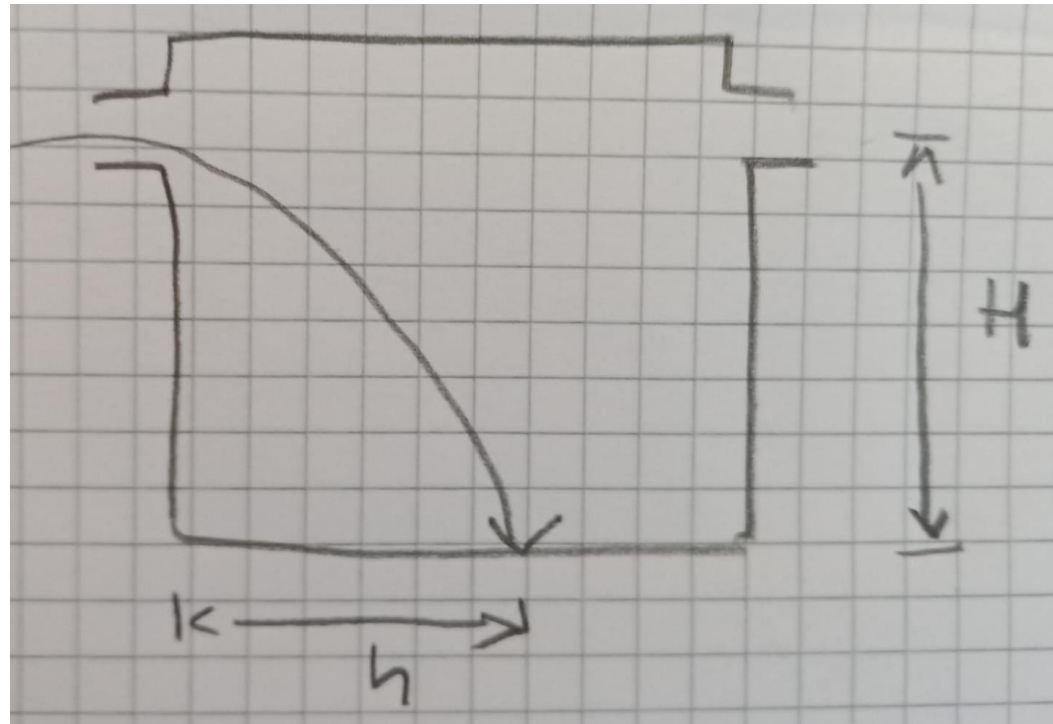
## Separatore gravitazionale fluido-solido



$$\eta = \frac{h}{H}$$

LA SEPARAZIONE è PARZIALE  
DIPENDE DAL DIAMETRO DELLE PARTICELLE  
E DAI TEMPI DI PERMANENZA

PER AUMENTARE L'EFFICIENZA SI POSSONO  
PREVEDERE PERCORSI TORTUOSI

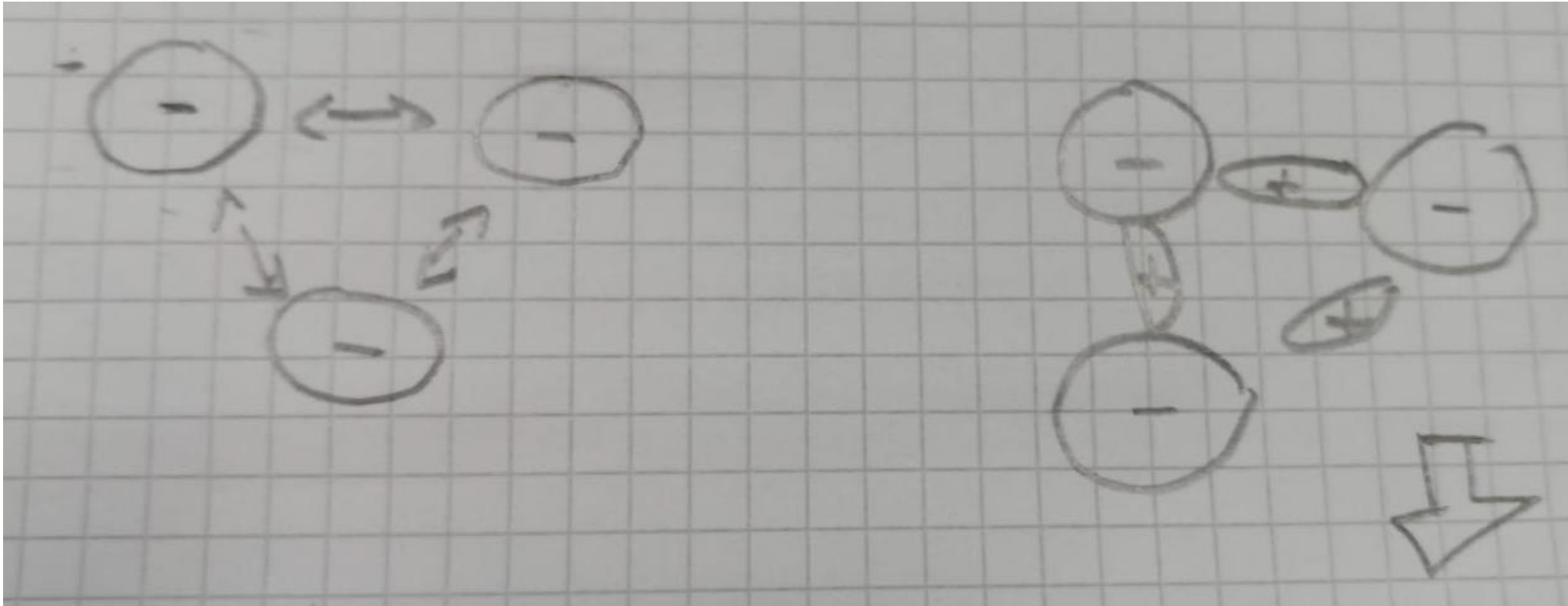




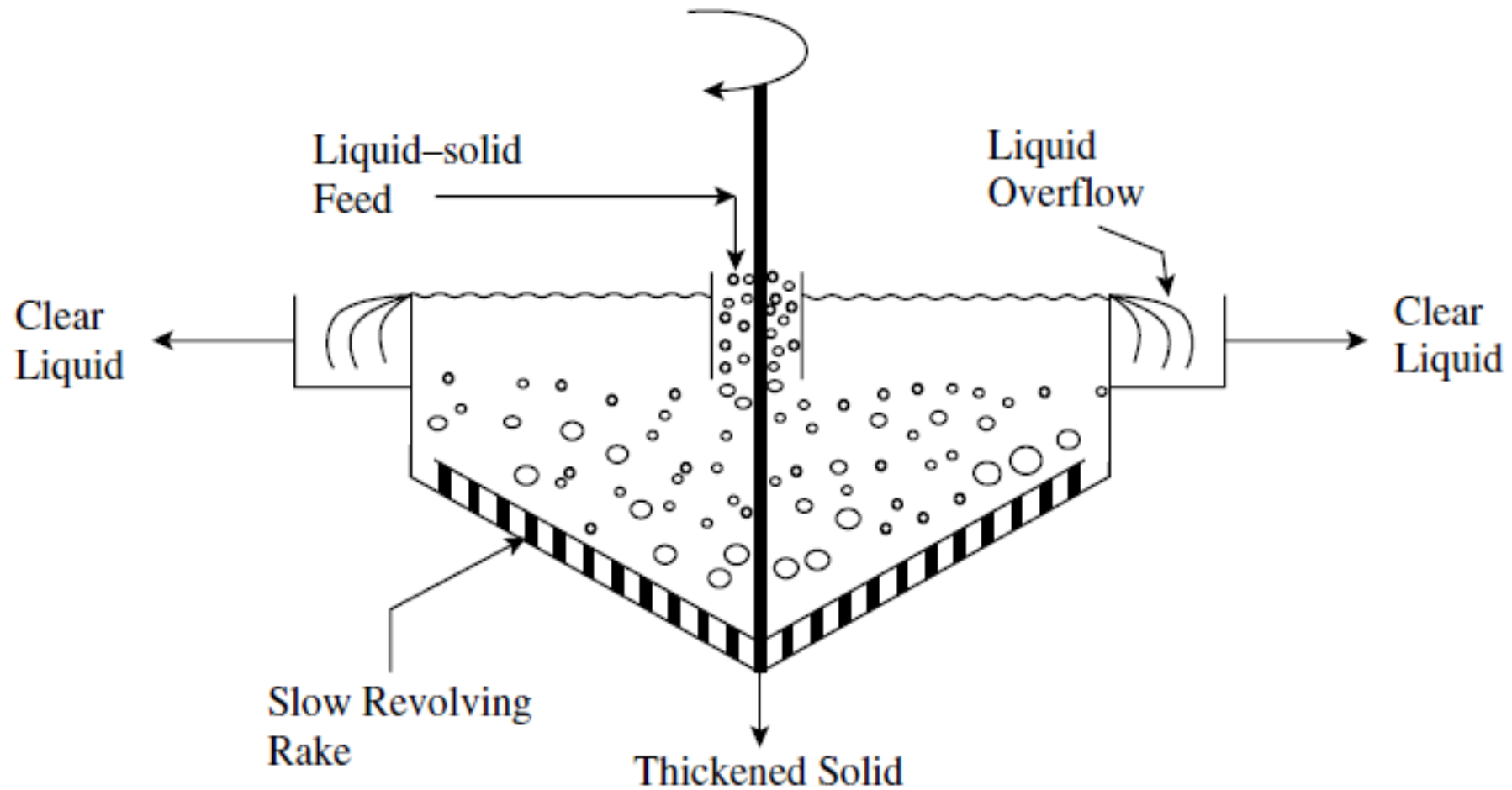
# Agente flocculante

100 micron dimensione media per sep. di gravità

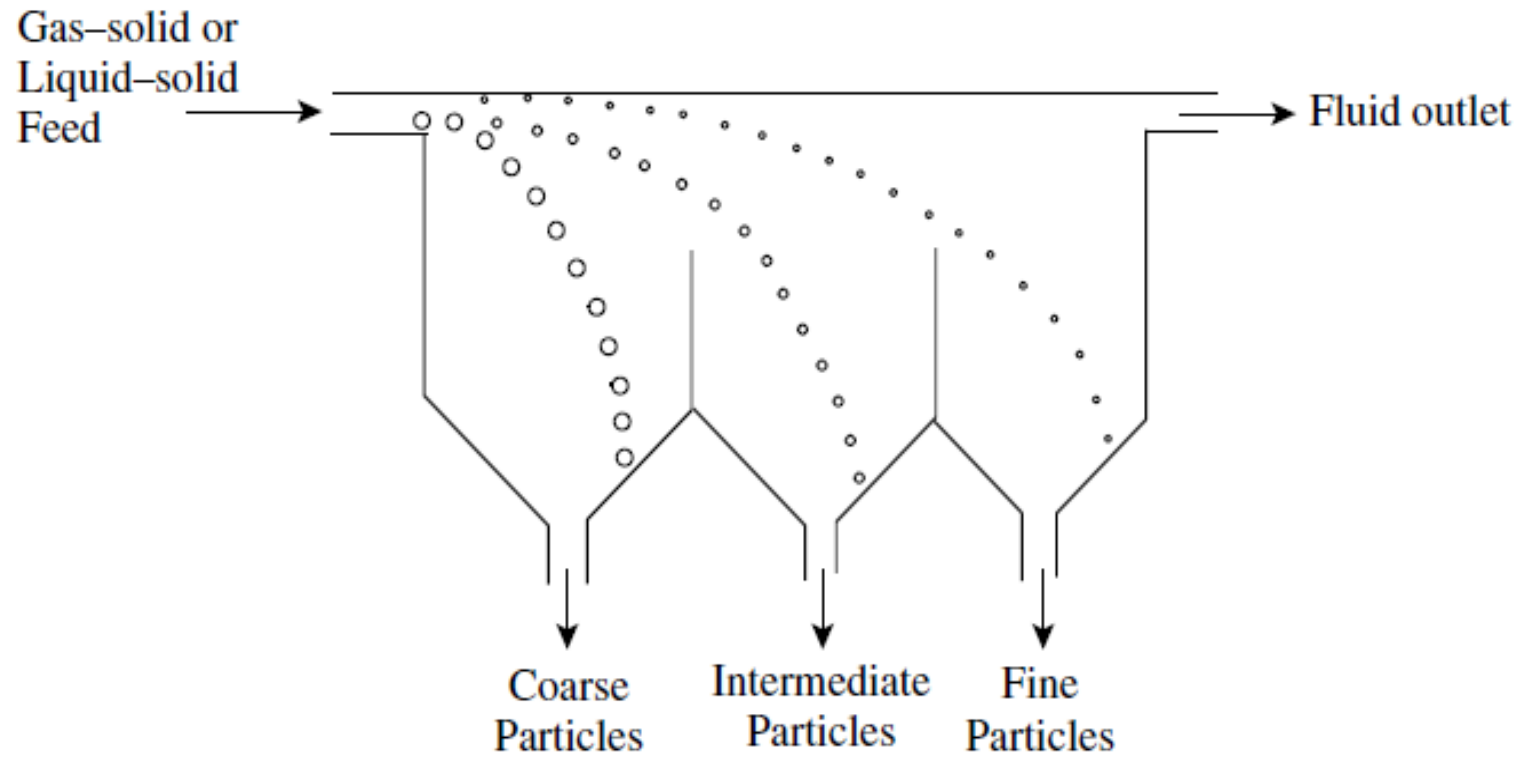
Sotto 20 micron diventa indispensabile l'uso di flocculanti



# Sedimentazione (ispessimento e chiarificazione)

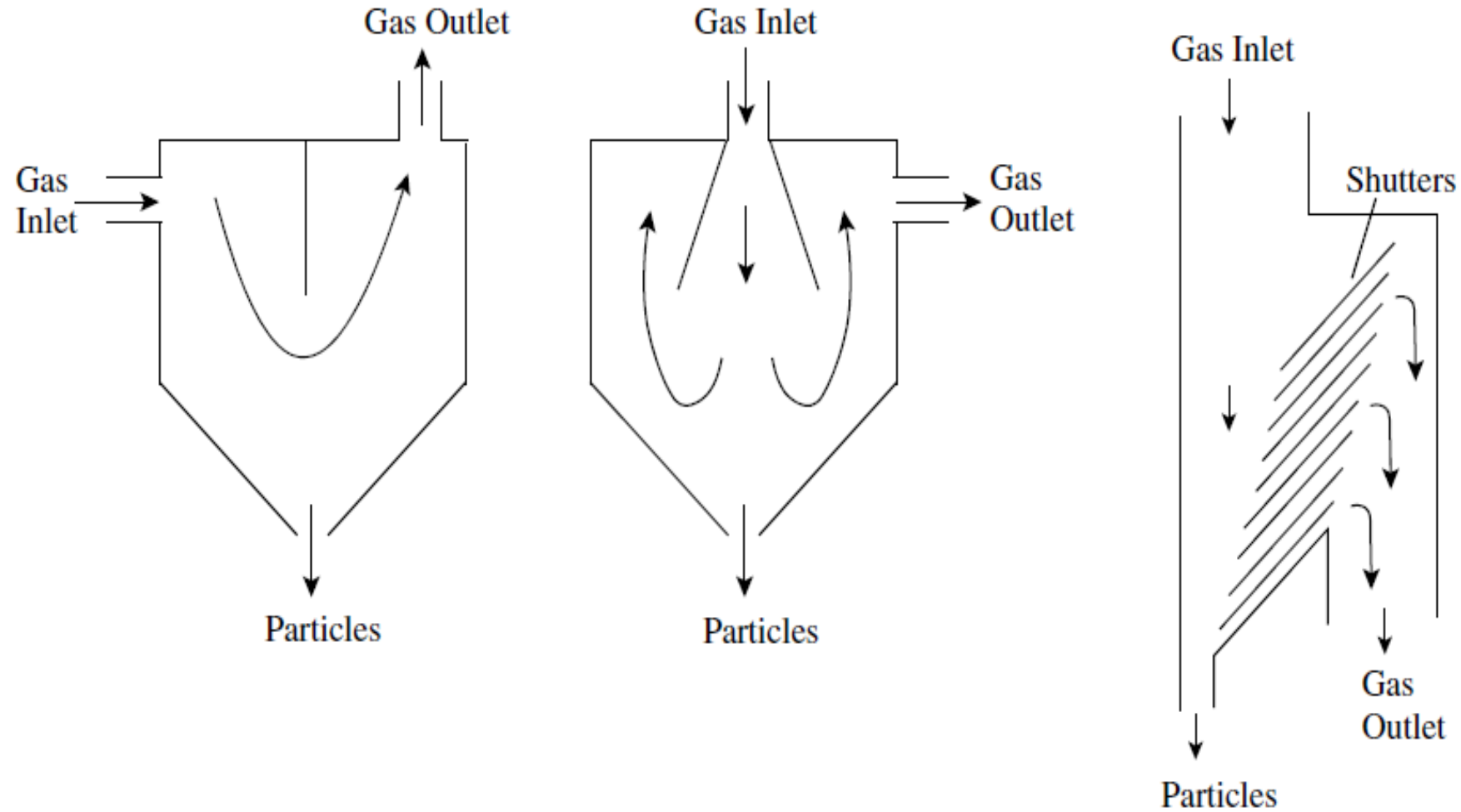


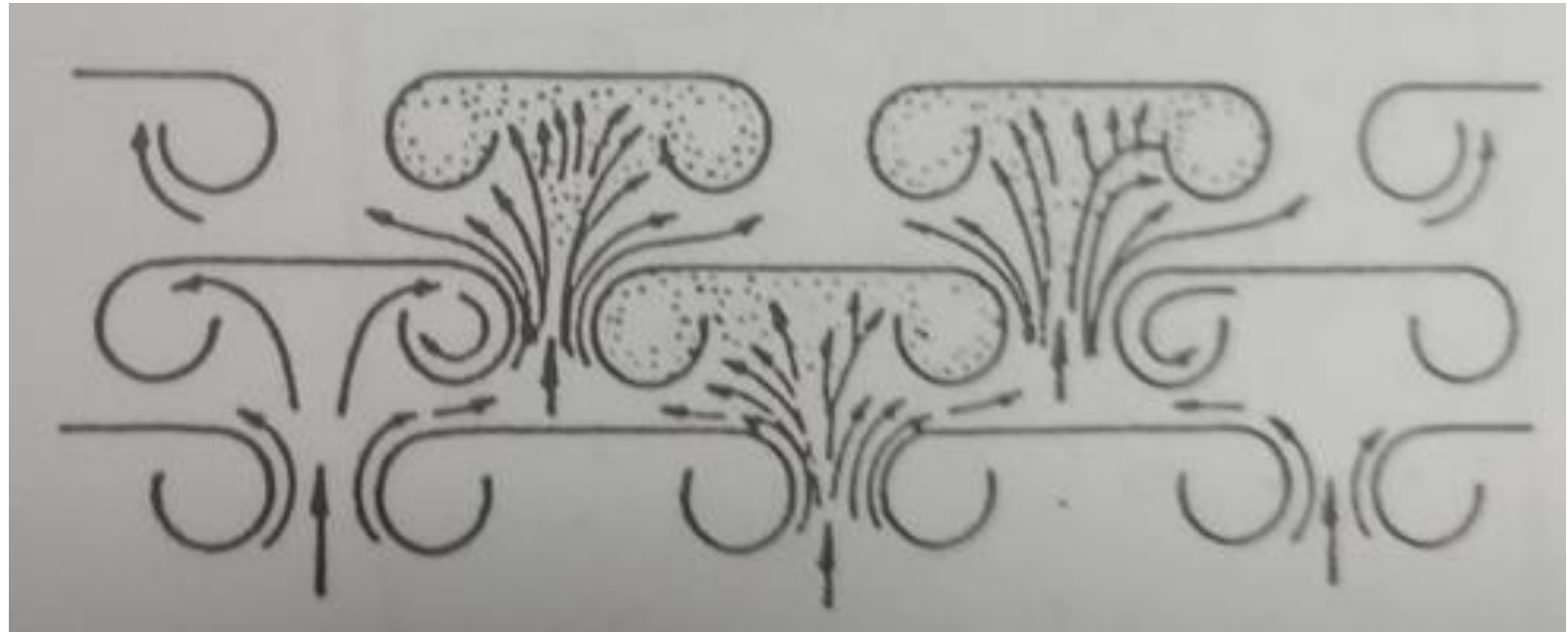
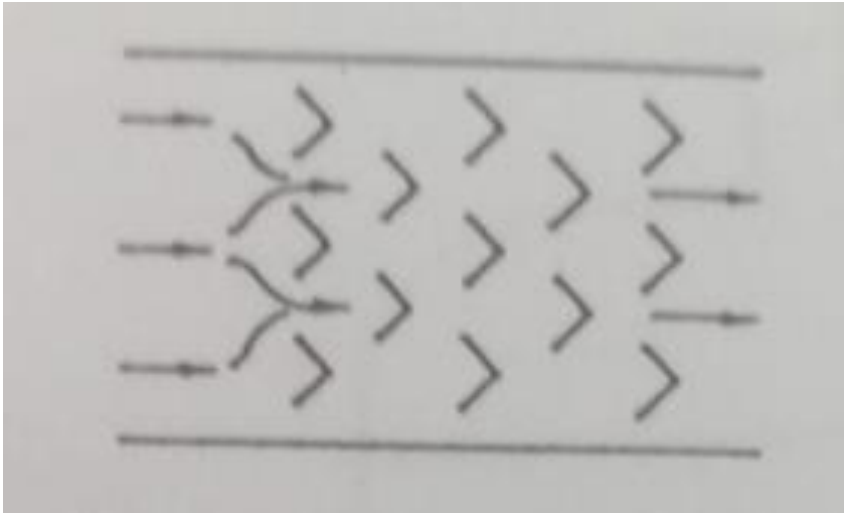
# Classificatore

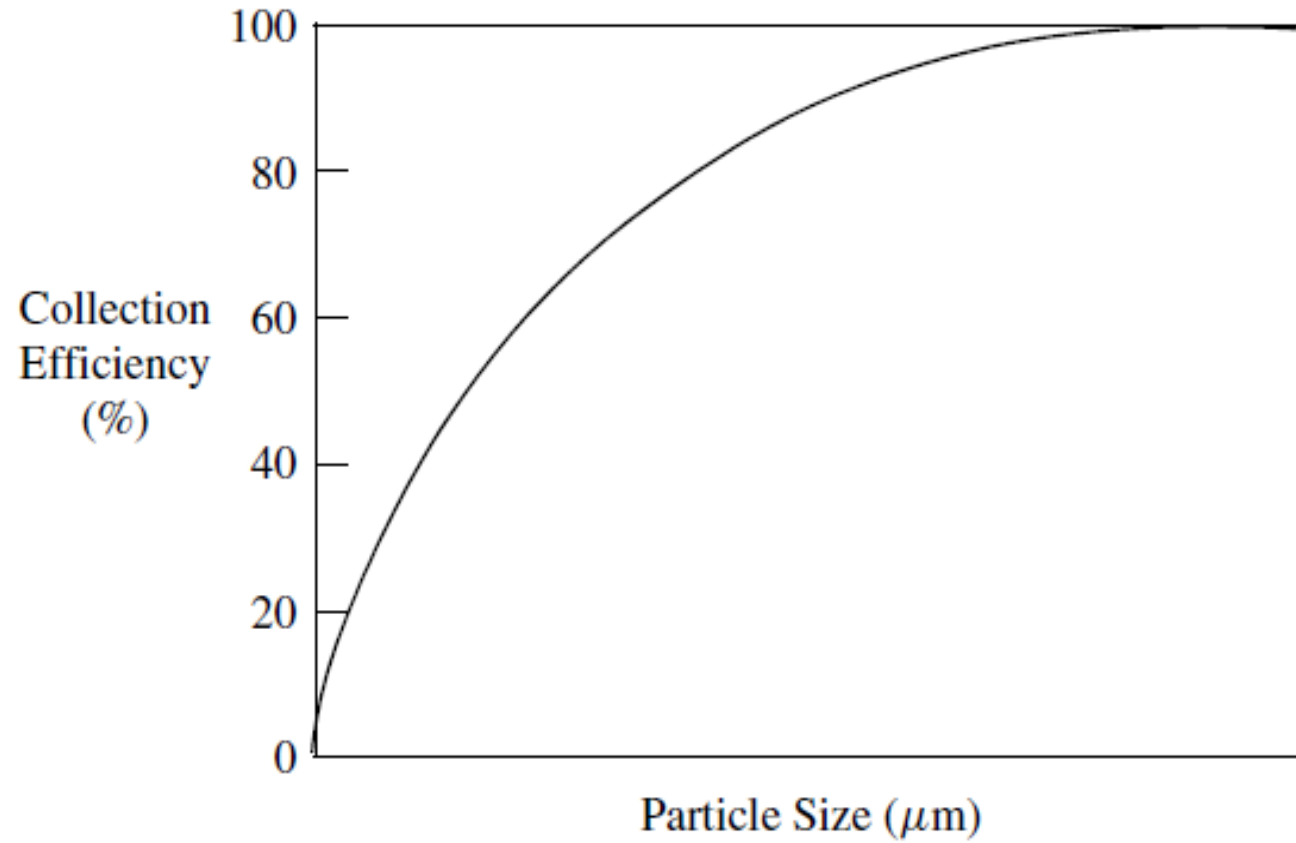


# Separazione inerziale e centrifuga

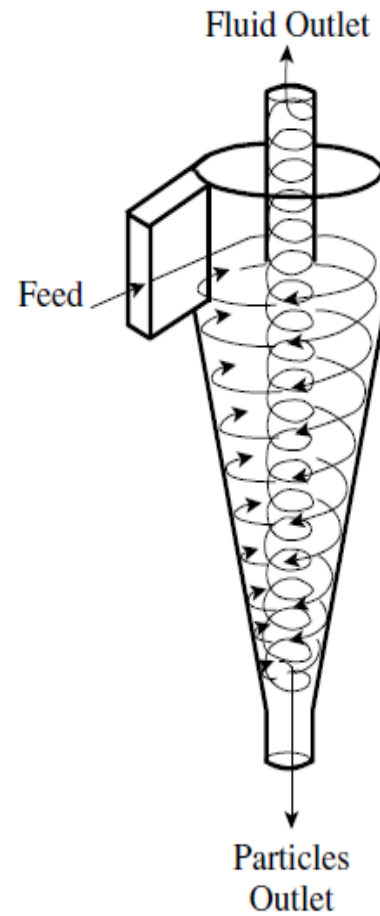
Per favorire la separazione







**Figure 8.5** A collection efficiency curve shows the fraction of particles of a given particle size that will be collected.

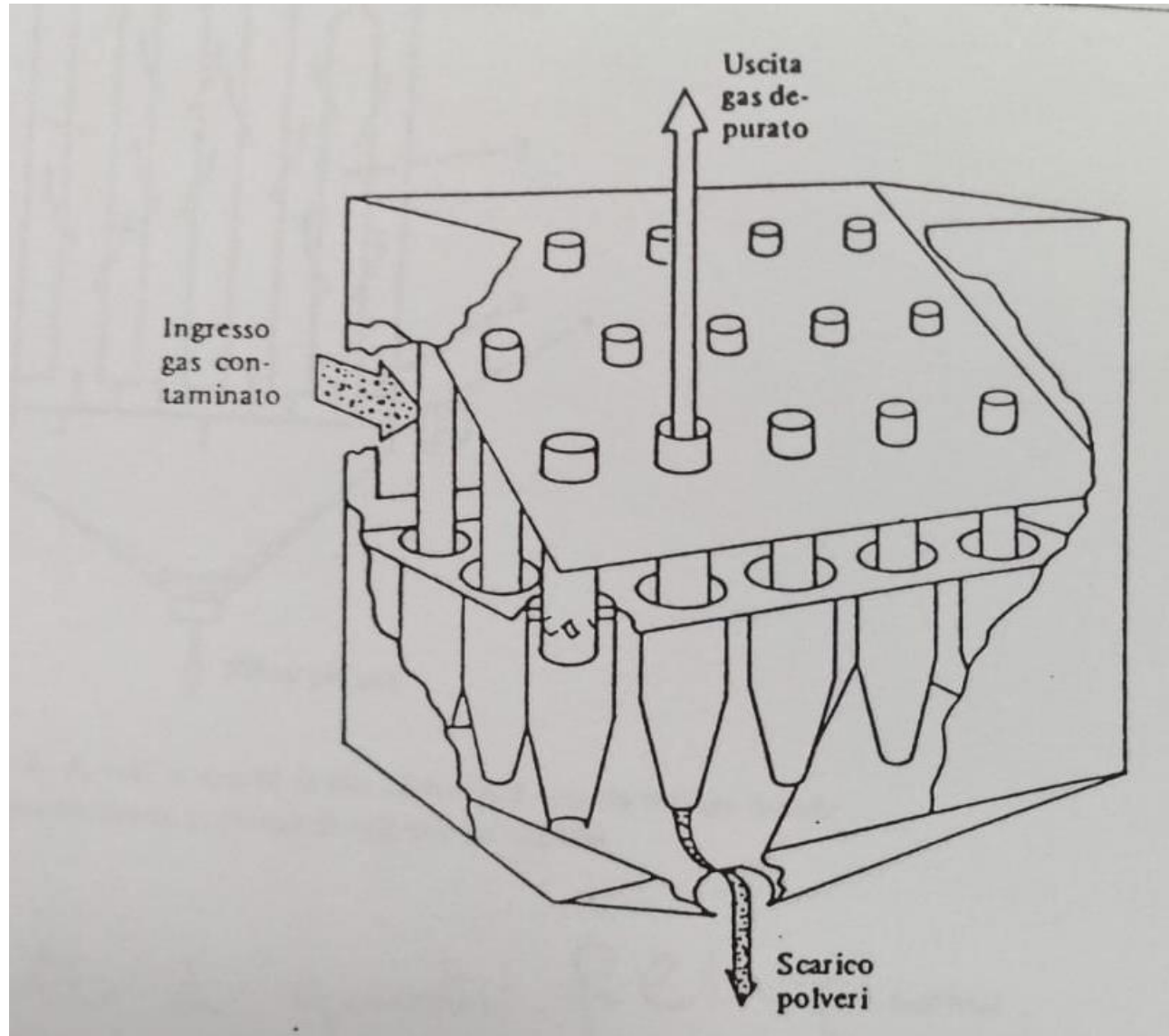


Diametro max 650 mm  
velocità 10-25 m/s

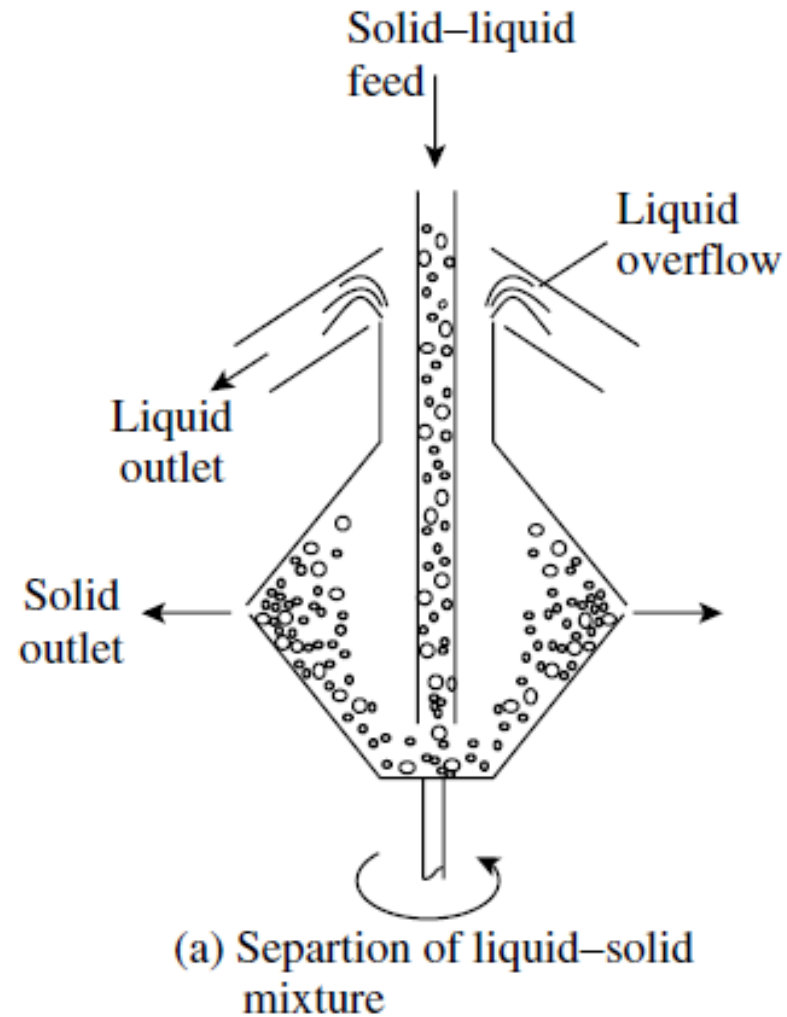
**Figure 8.6** A cyclone generates centrifugal force by the fluid motion.

# Multiciclone (portate elevate)

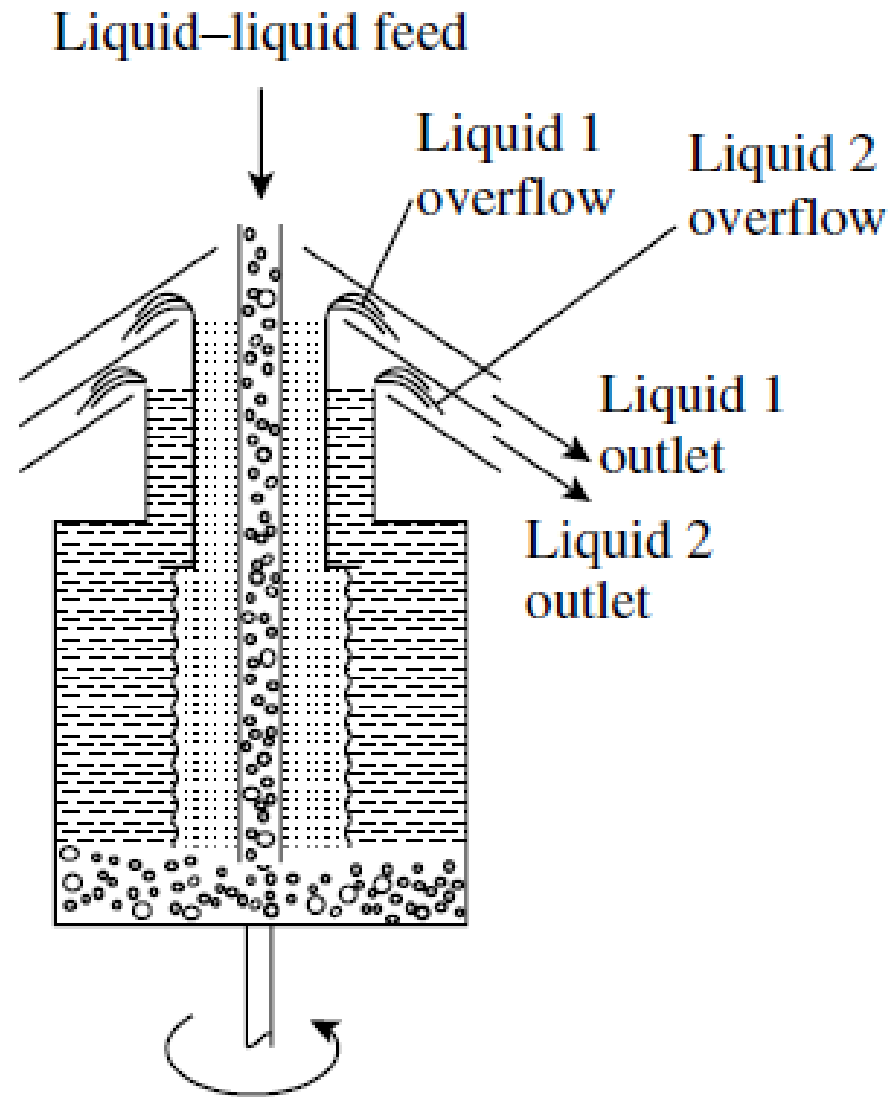
Poichè la dimesione non può aumentare







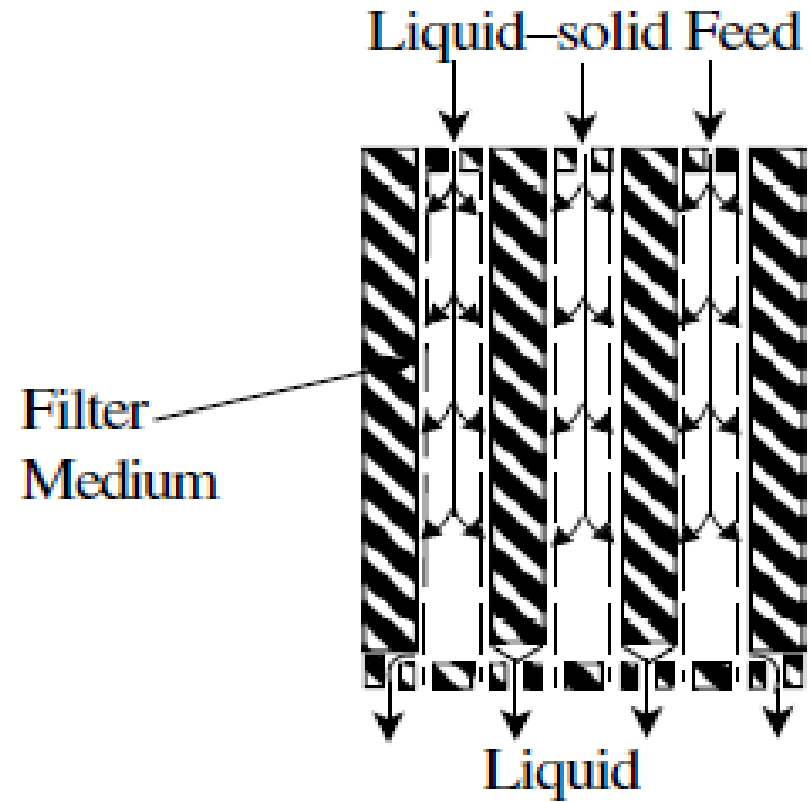
**centrifuga, nella quale una  
tazza a simmetria cilindrica  
viene messa in rotazione**



(b) Separation of liquid-liquid mixture

# Filtrazione

Filtrazione ordinaria : diametro particelle 10 micron



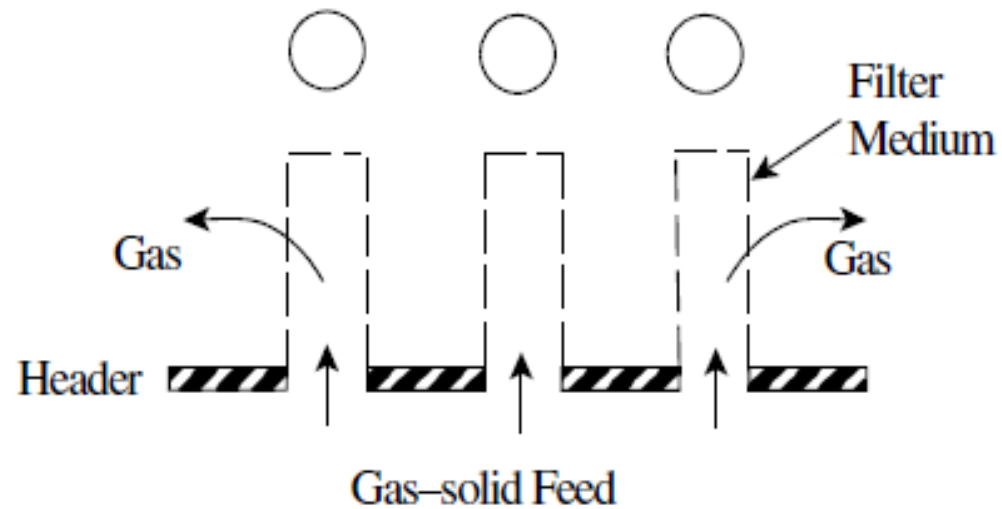
(a) Plate-and-frame filter.

**Filtro a piastre**

Dal materiale del tessuto dipende la T<sub>max</sub> di utilizzo

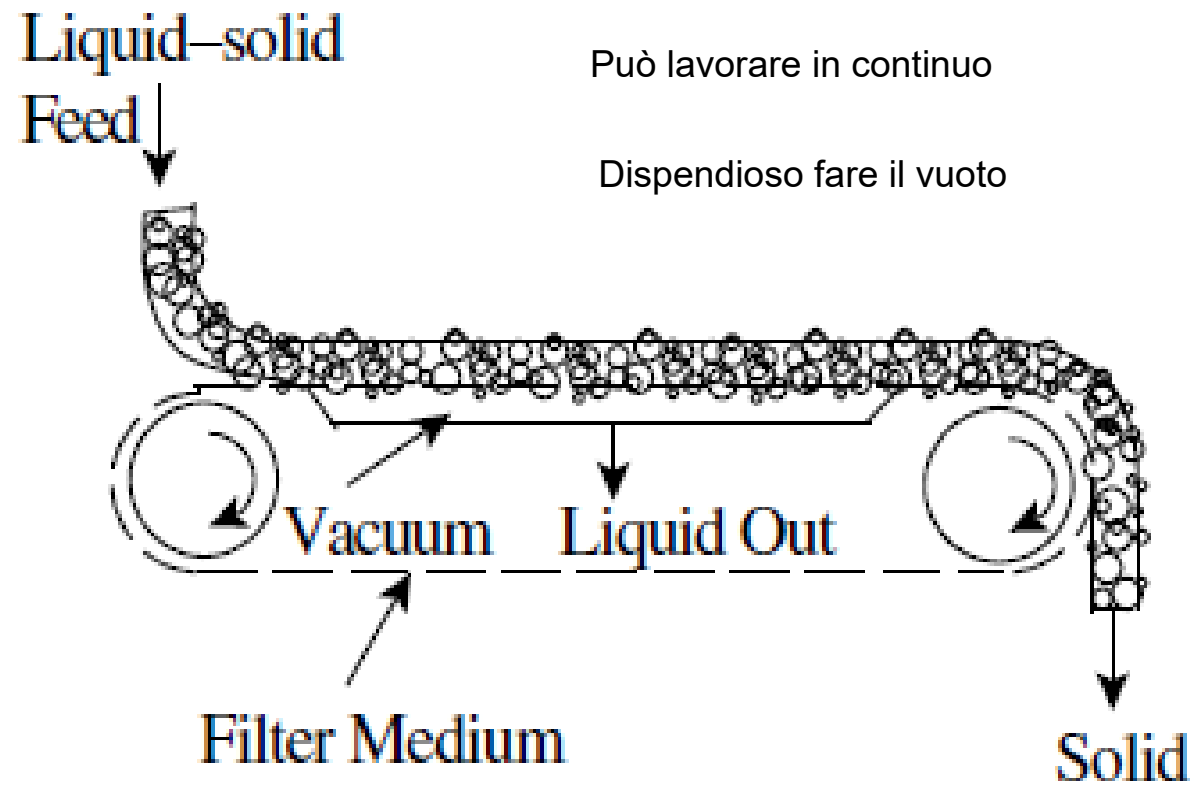
Cotone	80°C
Lana	93°C
Nylon	130°C
Teflon	290°C

Per T ancora più alte si devono sinterizzare metalli/ceramici porosi

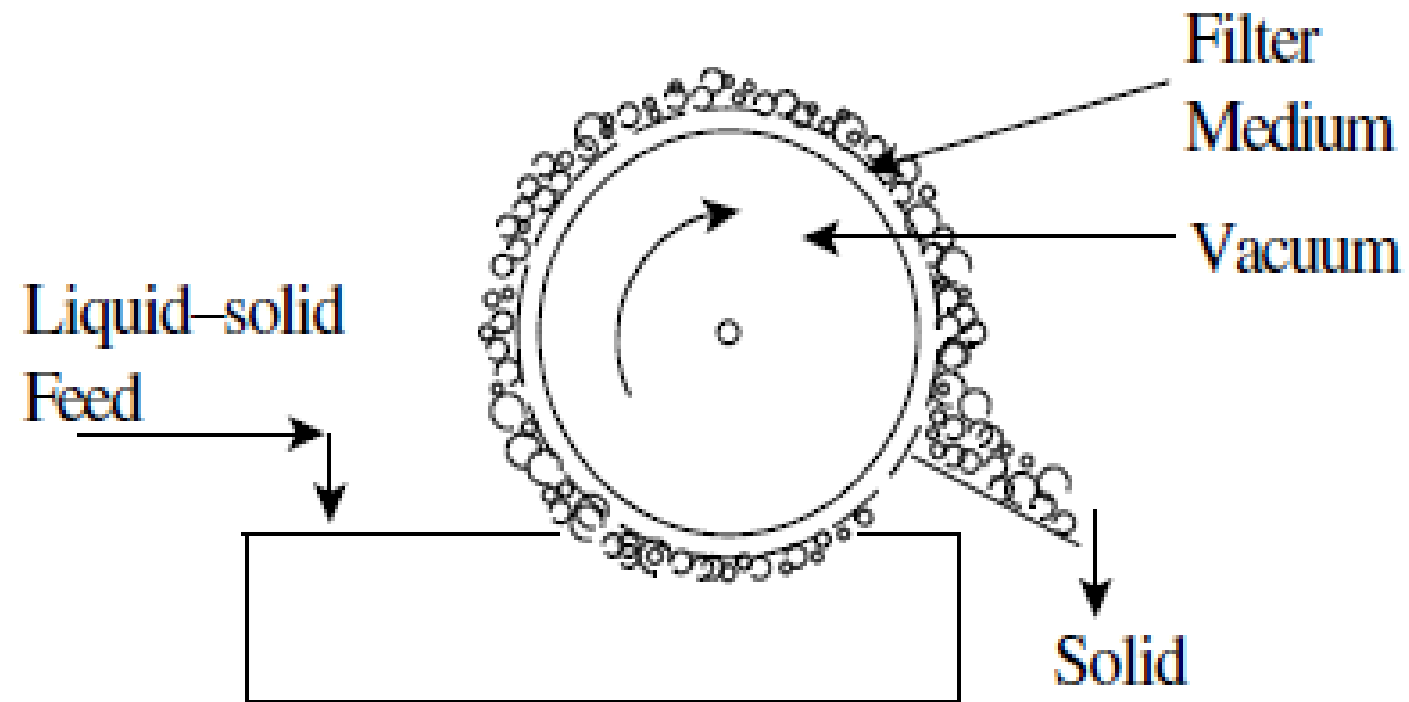


(b) Bag filter.

## Filtro a maniche

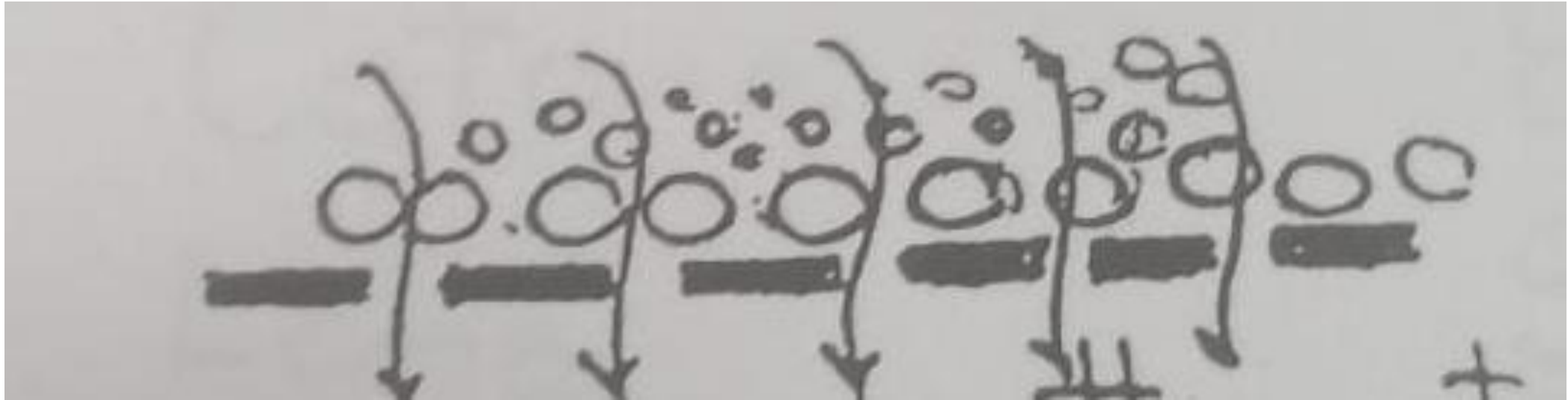


(c) Belt vacuum filter.



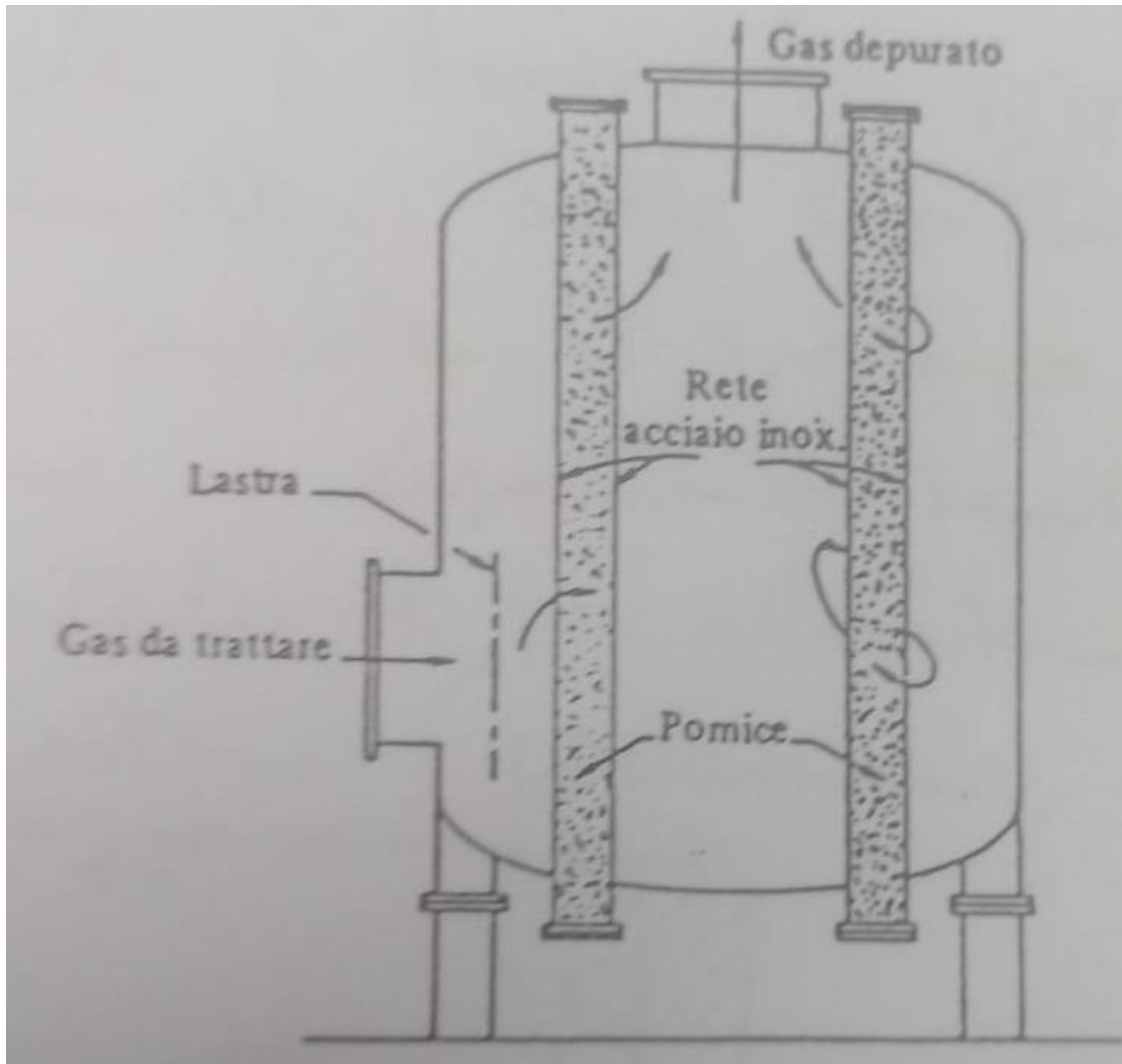
(d) Rotary vacuum filter.

**Filtro a tamburo rotante**



- CAKE FILTRATION ( SUPERFICIE )
- DEPTH FILTRATION ( PROFONDITA' )

## **Filtro a letto fisso**



## Filtro a solido poroso

### MICROFILTRAZIONE

Membrane polimeriche per arrivare a 0,05 micron  
Necessarie grandi superfici e contenere il volume:

- Spirale
- Fibra cava : tubo molto piccolo, flusso dall'esterno all'interno, sistemate in fascio con alimentazione tangenziale per far sì che si autopulisca

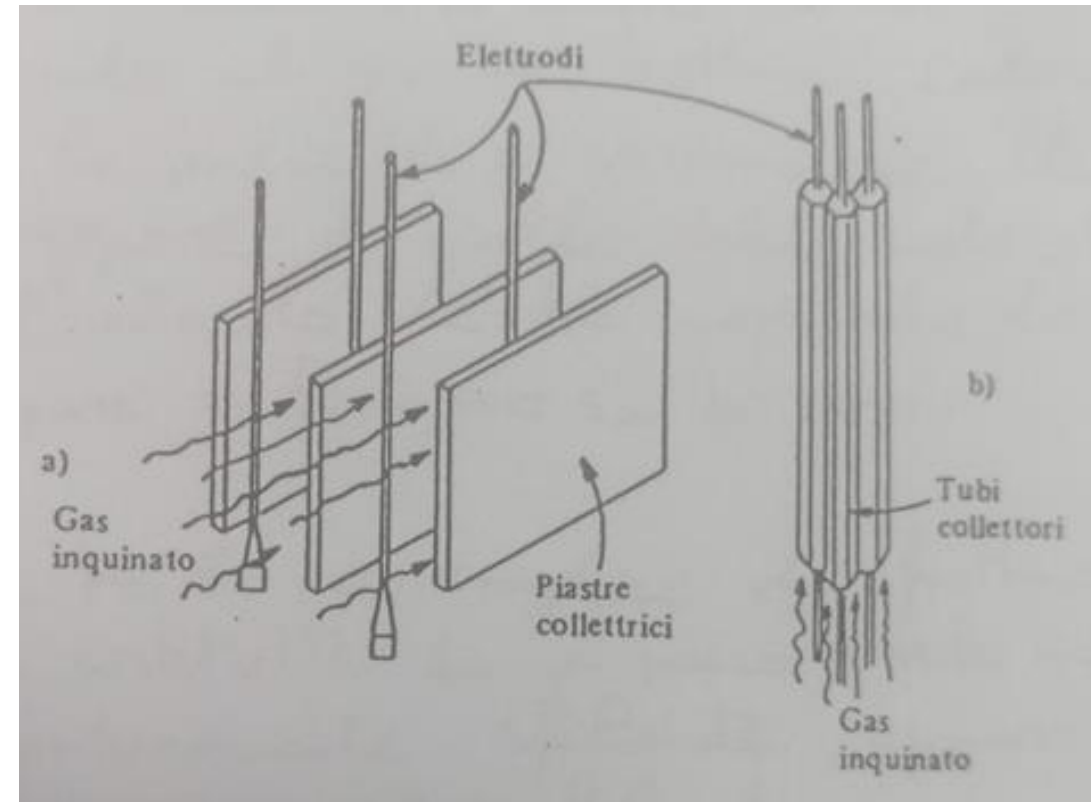
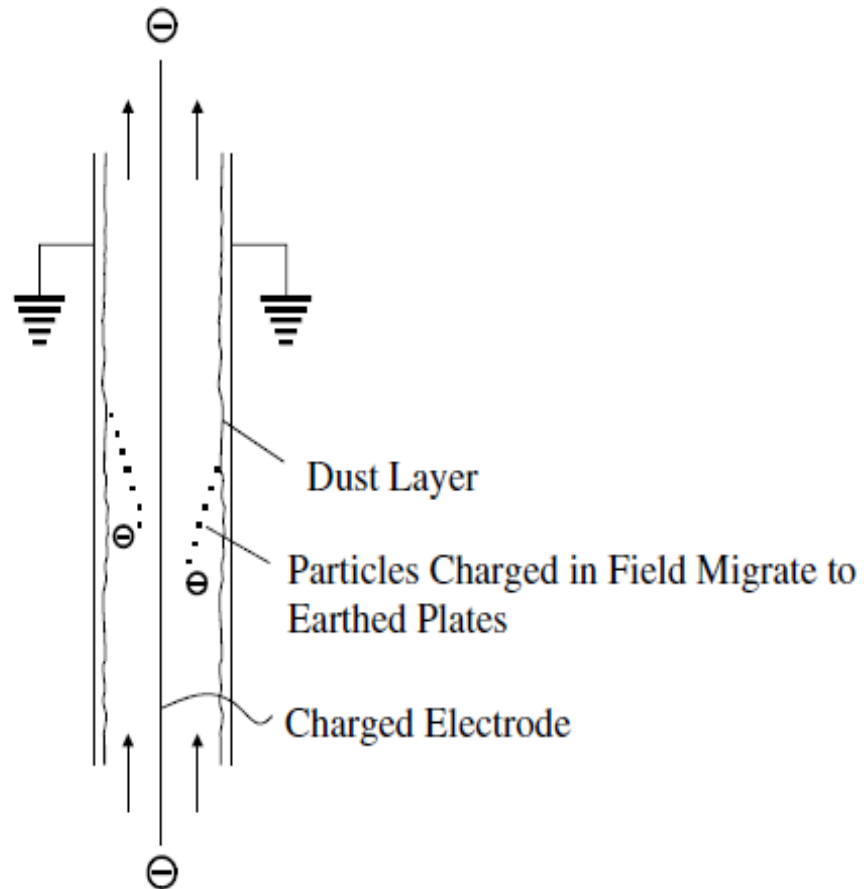


Necessario basso costo energia

Utile per alte portate e pochi solidi perchè ci sono poche perdite di carico

Utile per alte T dove si degraderebbe il filtro

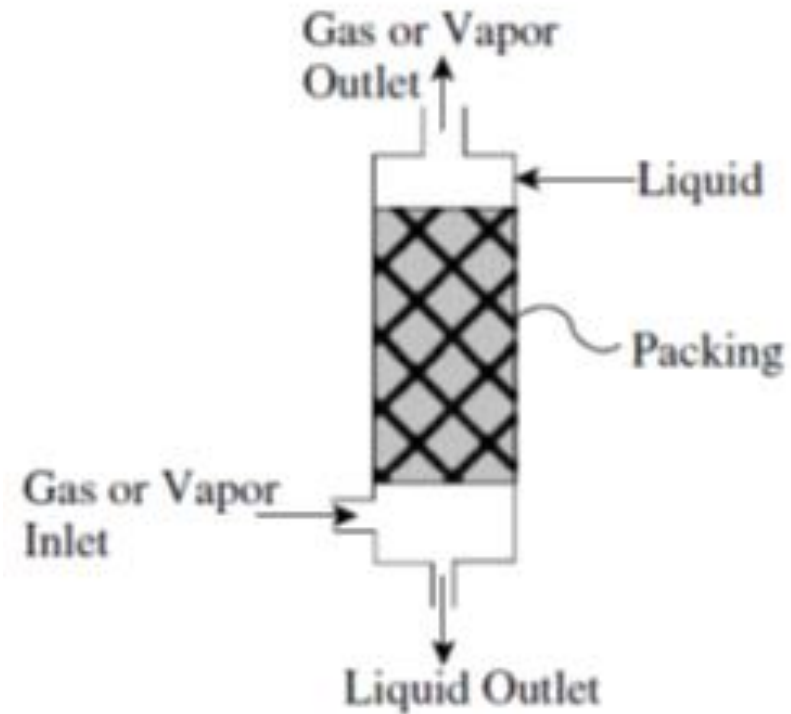
## Precipitazione elettrostatica



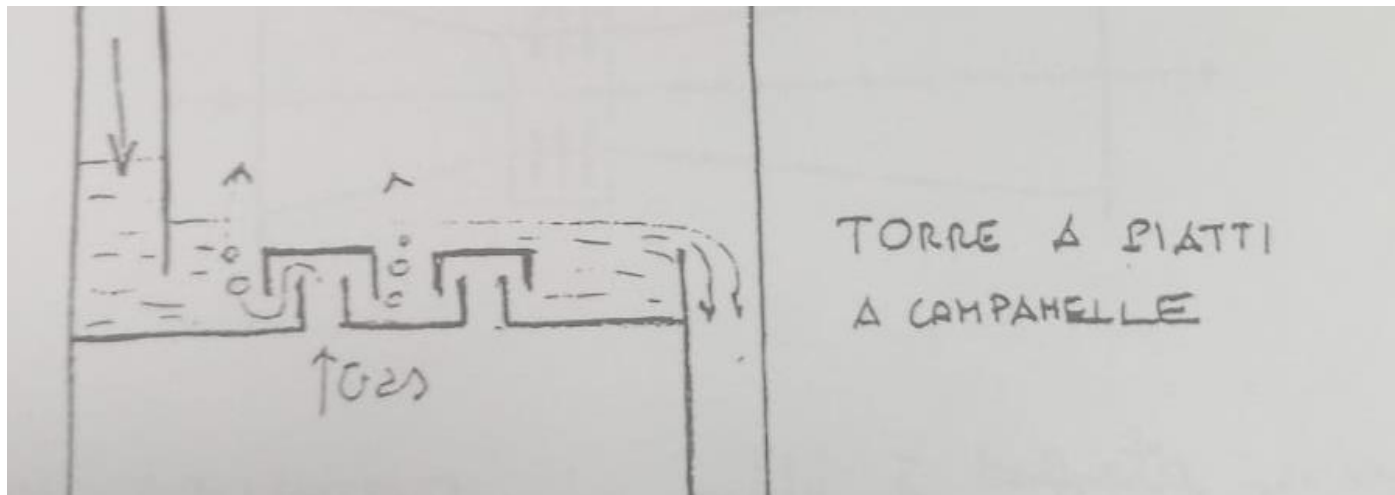
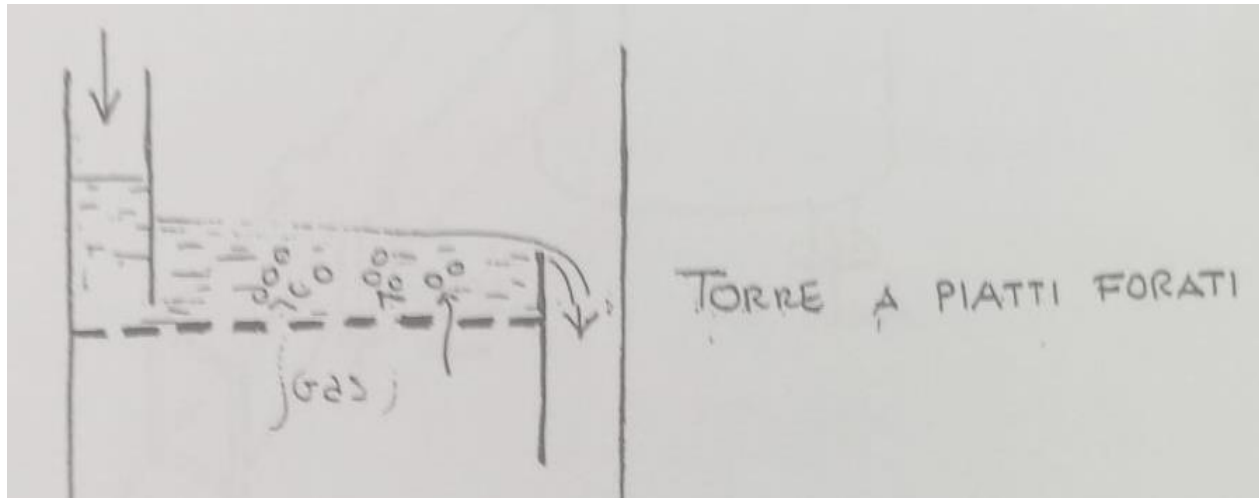
a) a piastre  
b) filo-in-tubo

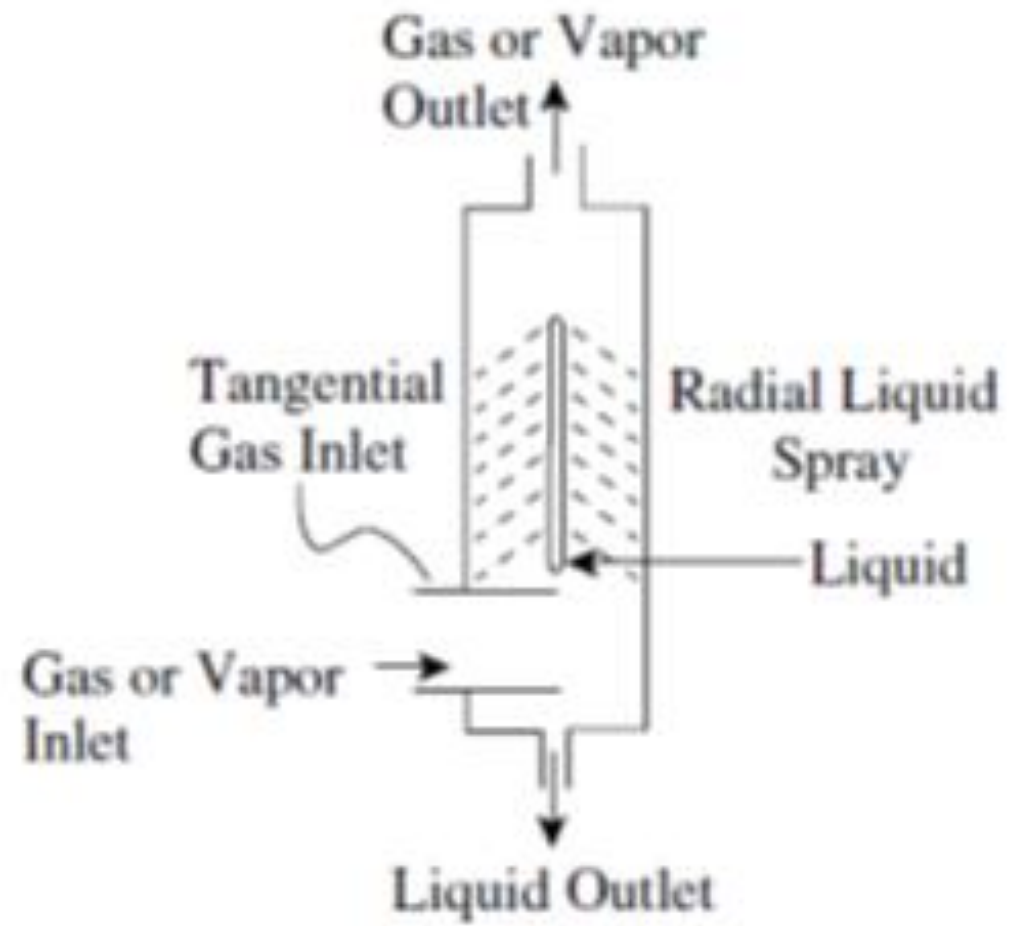
## Separazione ad umido (scrubbing)

Impaccamento comporta perdite di carico

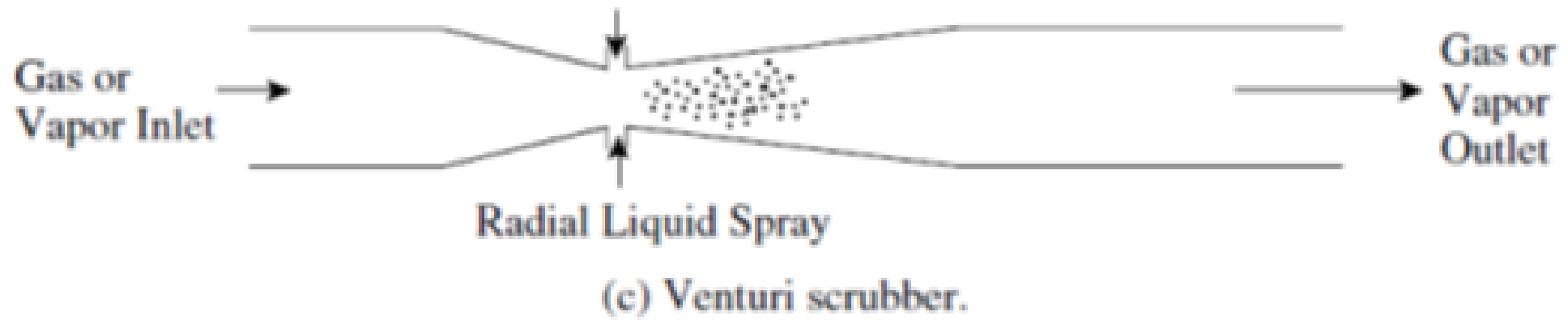


(a) Packed bed scrubber.



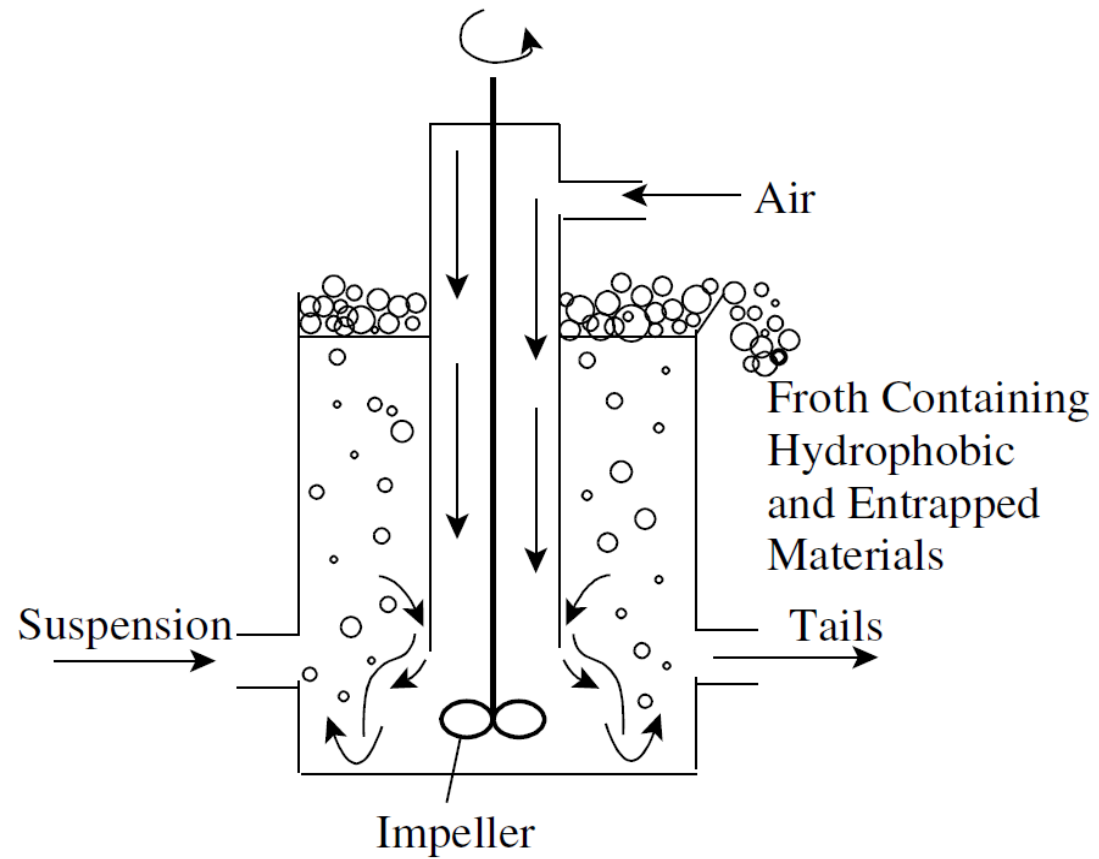


(b) Spray scrubber.

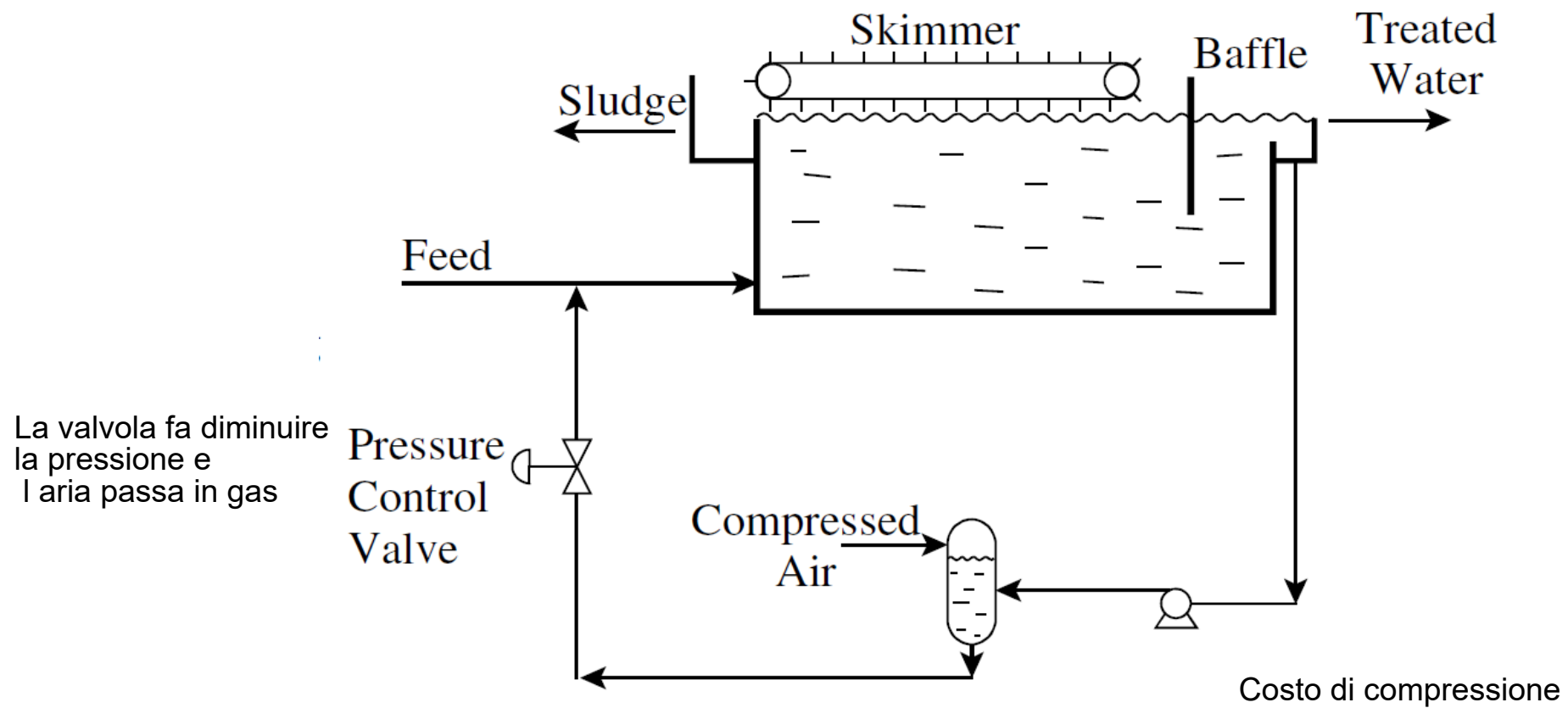


Spray e Venturi per abbassare perdite di carico

# Flottazione

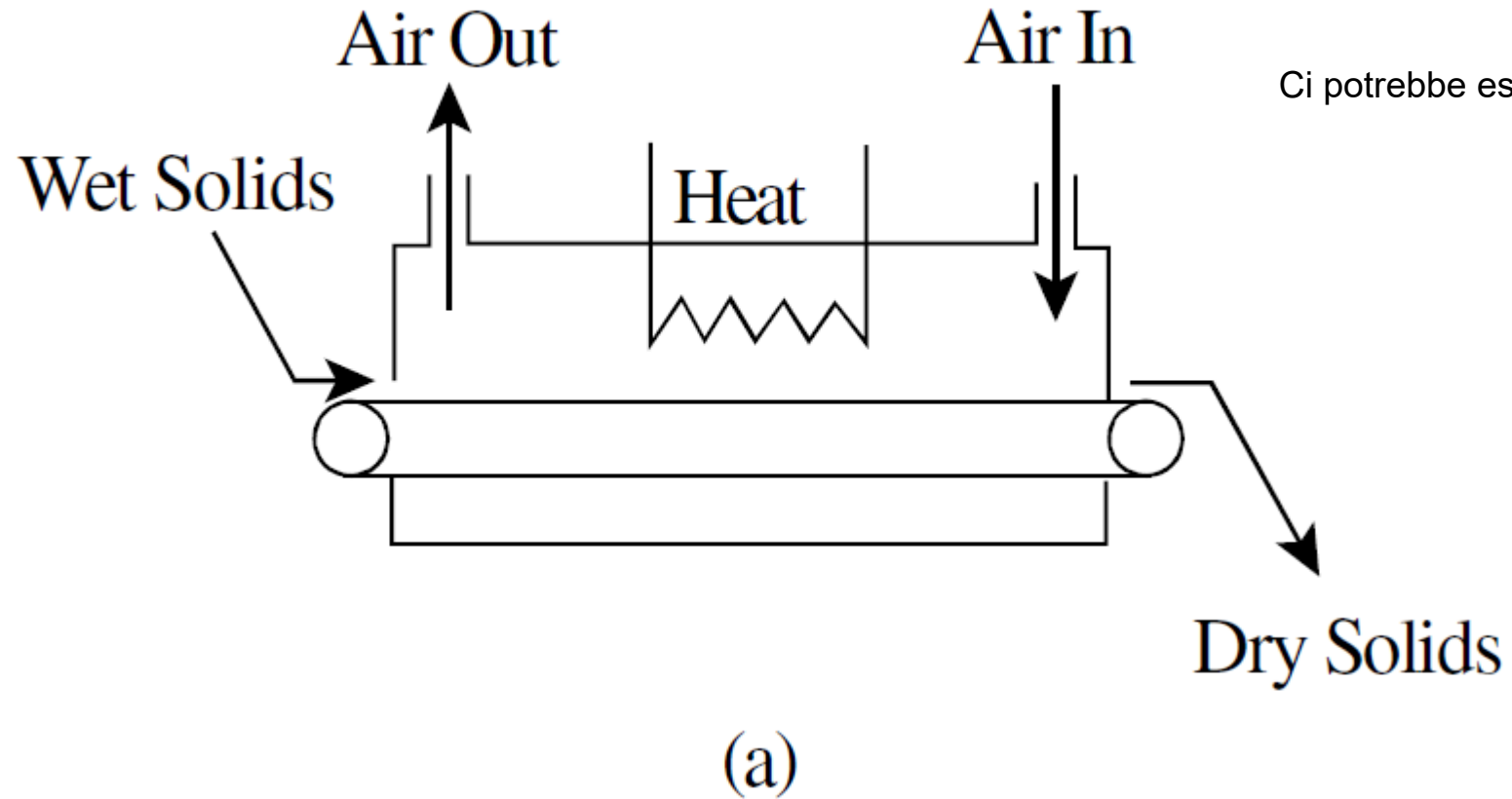


(a) A typical flotation cell for solid separation.



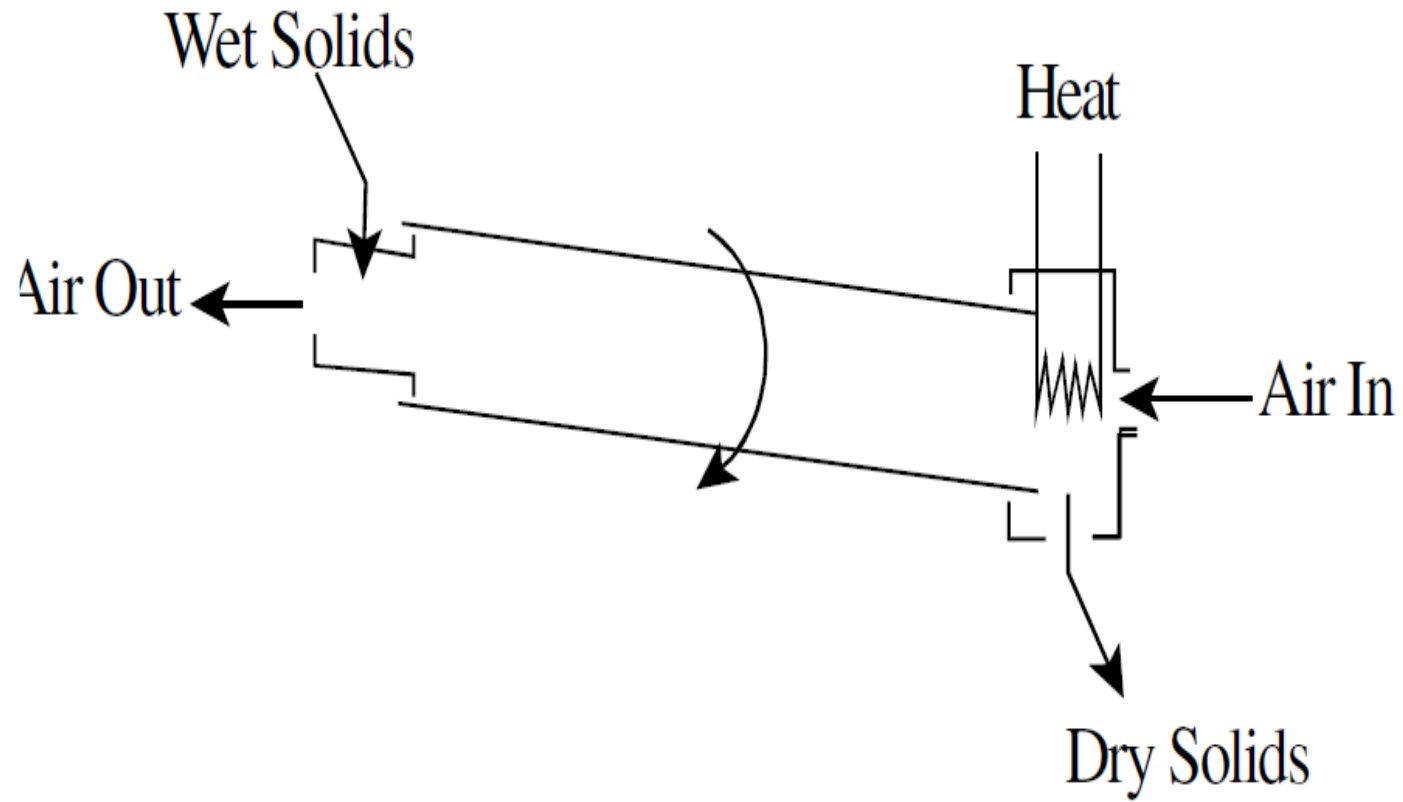
(b) Dissolved air flotation (DAF).

## Essiccamento



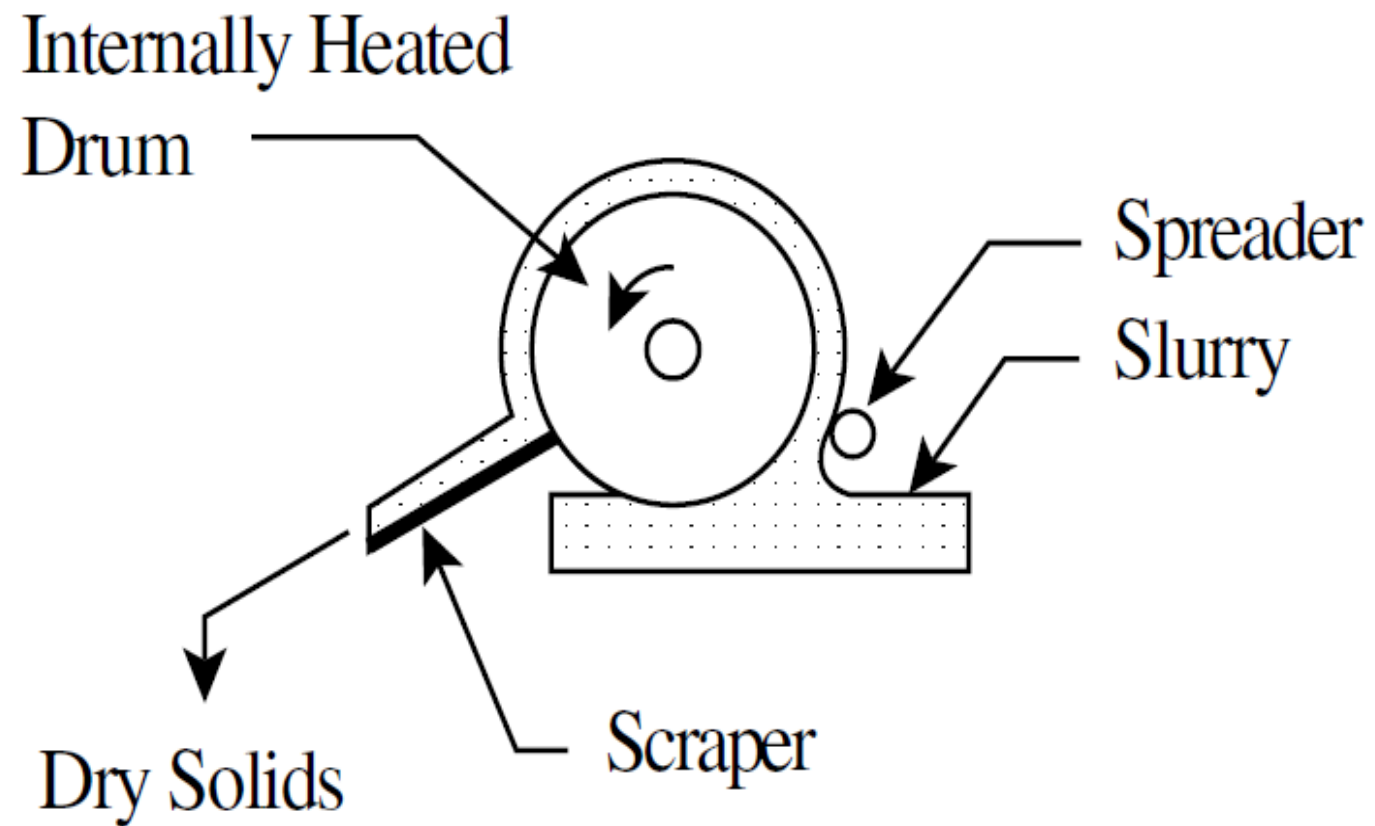
**Essiccatore a tunnel (flusso controcorrente)**





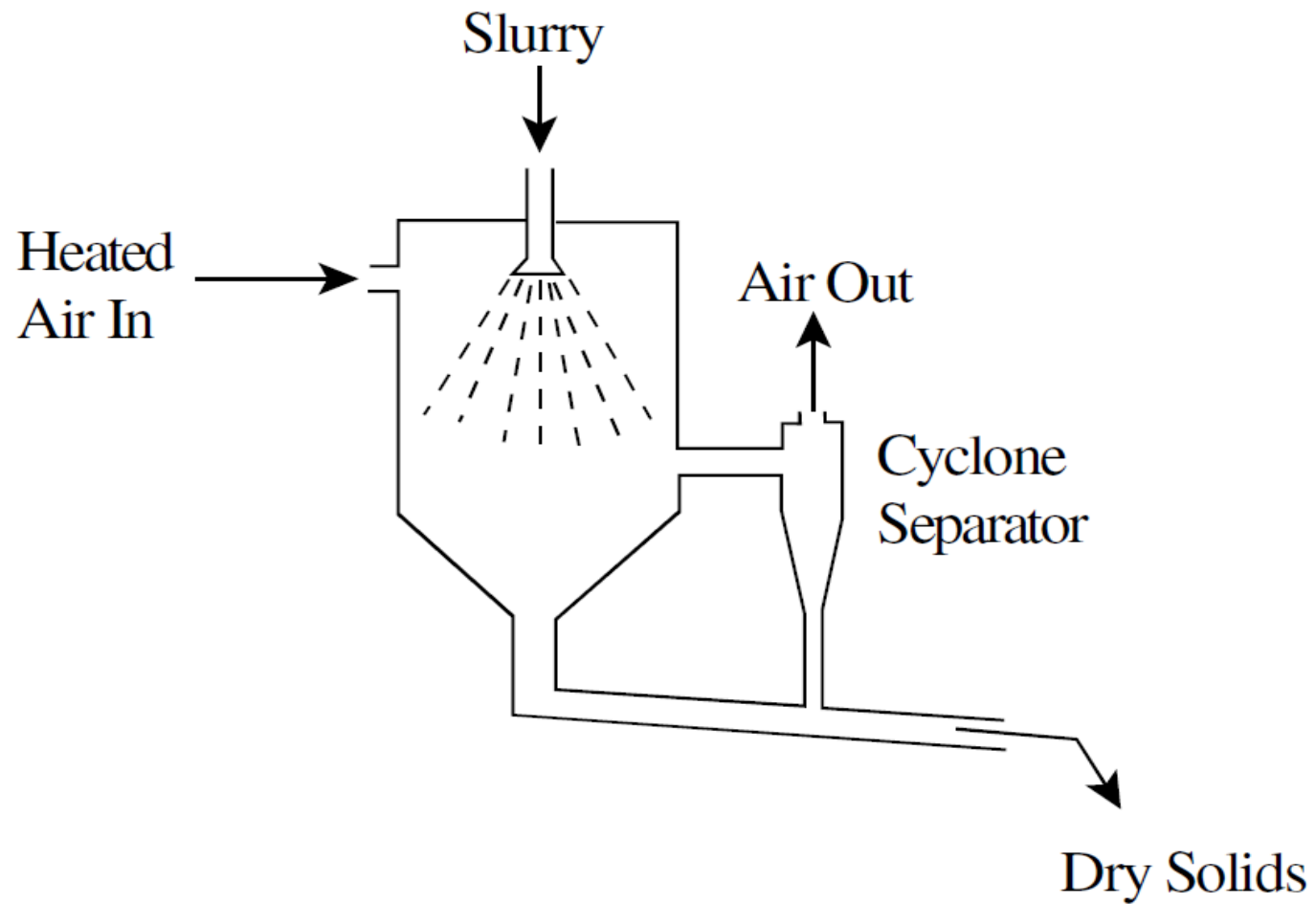
(b)

**Essiccatore a tunnel (flusso equicorrente)**



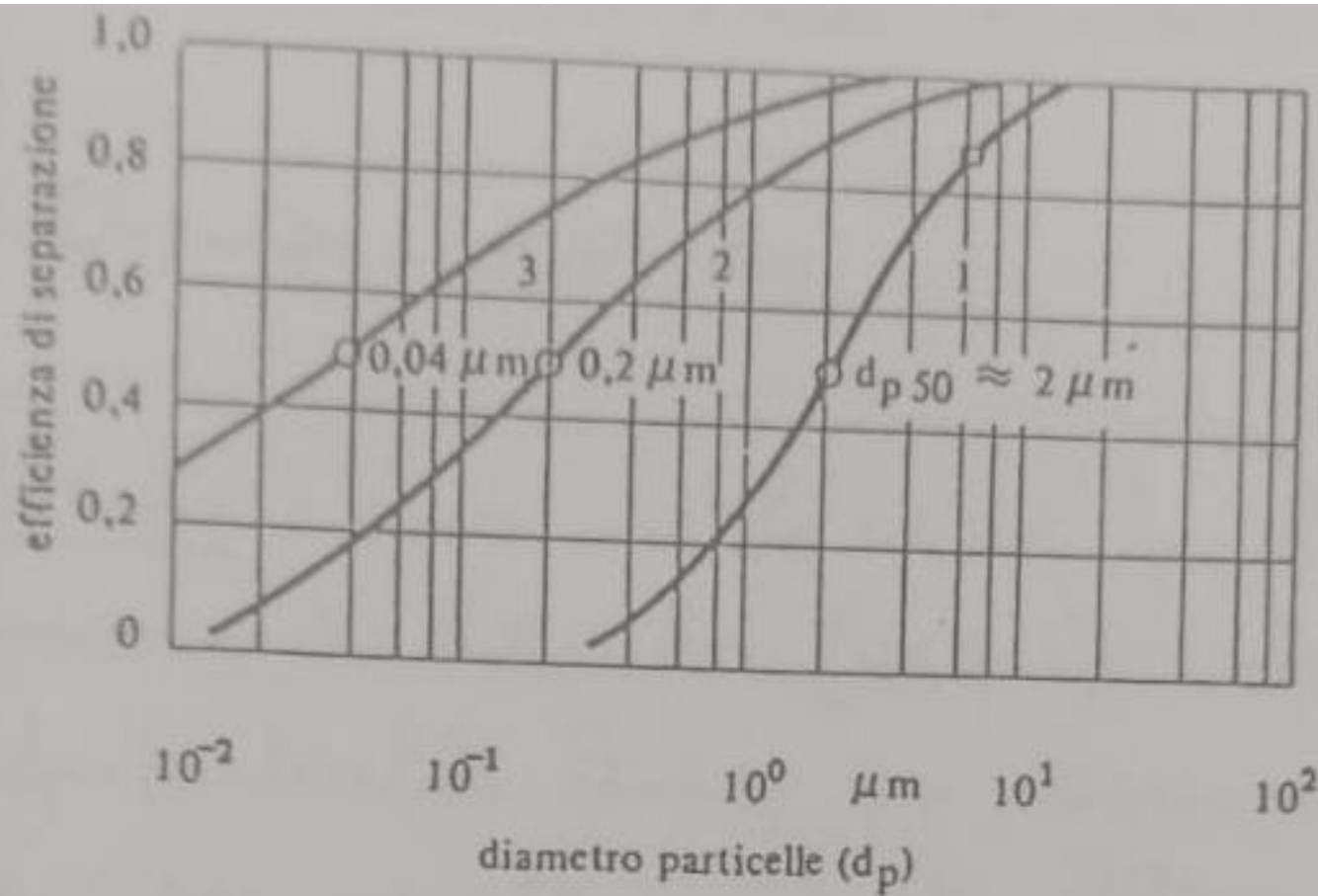
(c)

**Senza contatto diretto con l'aria**



(d)

**Essiccatore spray**



Esempi di curve di efficienza di separatori di polveri a secco e ad umido  
 1) cicloni; 2) scrubber ad umido; 3) - filtri a maniche - precipitatori elettrostatici  
 - separatori VENTURI.

