

# 北京航空航天大学

BEIJING UNIVERSITY OF AERONAUTICS AND ASTRONAUTICS

## 物理作业5

6.21  $27^{\circ}\text{C}$  和  $127^{\circ}\text{C}$  的卡诺热机, 从高温热源处吸取  $5000\text{J}$ , 该热机向低温热源放出多少热量? 对外做功? 如果是一个制冷机, 从低温吸收  $5000\text{J}$

$$(1) Q_1 = 5 \times 10^3 \text{ J}$$

$$\eta = \frac{A}{Q_1} = 1 - \frac{|Q_2|}{Q_1} = 1 - \frac{T_2}{T_1}$$

$$\text{放出热量 } |Q_2| = \frac{T_2}{T_1} Q_1 = \frac{273+27}{273+127} \times 5 \times 10^3 \text{ J} = 3.75 \times 10^3 \text{ J}$$

$$\text{对外做功 } A = \frac{T_1 - T_2}{T_1} Q_1 = \frac{127-27}{273+127} \times 5 \times 10^3 \text{ J} = 1.25 \times 10^3 \text{ J}$$

$$(2) Q_2 = 5 \times 10^3 \text{ J}$$

$$\bar{w}_c = \frac{Q_2}{|A|} = \frac{|Q_1| - |A|}{|A|} = \frac{T_2}{T_1 - T_2}$$

$$\text{放出热量 } |Q_1| = Q_2 + |A| = \frac{T_1}{T_2} Q_2 = \frac{(273+127)}{273+27} \times 5 \times 10^3 = 6.67 \times 10^3 \text{ J}$$

外界做功

$$|A| = \frac{T_1 - T_2}{T_2} Q_2 = \frac{(127-27) \times 5 \times 10^3}{273+27} = 1.67 \times 10^3 \text{ J}$$





6-23

左边压强为  $P_0$ ，右边为真空，当气体达到热平衡时其压强

解：设系统初态为  $(T_0, V_0, P_0)$  经自由膨胀后的末态为  $(T_0, V, P)$  由理想气体物态方程

$$P_0 V_0 = PV \quad V = 2V_0$$

达到热平衡的压强  $P = \frac{1}{2} P_0$





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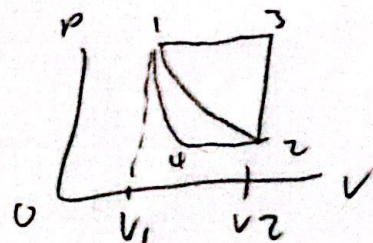
6-25 1mol 在状态 1 时  $T_1=300K$ ,  $V_1=20L$ , 到 2  $V_2=40L$

(1) 1-3-2 路径的熵变

对 1-3 等压过程, 有  $T_3 = \frac{V_2}{V_1} T_1 = 600K$

吸热  $\Delta Q_p = C_{pm} \Delta T$

对 3-2 等体过程有  $\Delta Q_v = C_{vm} \Delta T$



则 1-3-2 路径的熵变  $\Delta S_{1-3-2} = \int_1^3 \frac{\Delta Q_p}{T} + \int_3^2 \frac{\Delta Q_v}{T}$   
 $= C_{pm} \int_{T_1}^{T_3} \frac{dT}{T} + C_{vm} \int_{T_3}^{T_2} \frac{dT}{T} = C_{pm} \ln \frac{T_3}{T_1} + C_{vm} \ln \frac{T_2}{T_3}$

由于 1-2 为等温过程,  $T_1 = T_2$  所以  $\Delta S_{1-3-2} = C_{pm} \ln \frac{T_3}{T_1} - C_{vm} \ln \frac{T_3}{T_1}$   
 $= (C_{pm} - C_{vm}) \ln \frac{T_3}{T_1} = R \ln 2 = 5.76 J/K$

(2) 对 1-2 等温过程

1-2 路径的熵变

$$\Delta Q_r = \Delta A = p dV, p = \frac{p_1 V_1}{V}, T = T_1$$

$$\Delta S_{1-2} = \int_1^2 \frac{\Delta Q_r}{T} = \frac{p_1 V_1}{T_1} \int_{V_1}^{V_2} \frac{dV}{V} = R \ln \frac{V_2}{V_1} = R \ln 2 = 5.76 J/K$$

(3) 对 1-4-2

1-4 绝热过程  $\Delta Q=0, \Delta S=0, \frac{T_1}{T_4} = \left(\frac{p_1}{p_4}\right)^{\frac{\gamma-1}{\gamma}}$

对 4-2 等压过程有  $\Delta Q_p = C_{pm} \Delta T$

1-4-2 路径的熵变  $\Delta S_{1-4-2} = \int_4^2 \frac{\Delta Q_p}{T} = C_{pm} \int_{T_4}^{T_2} \frac{dT}{T}$

$$= C_{pm} \frac{\gamma-1}{\gamma} \ln \frac{p_1}{p_4}$$

利用 1-2 等温过程, 上式中  $\frac{p_1}{p_4} = \frac{p_1}{p_2} = \frac{V_2}{V_1}$  所以

$$\Delta S_{1-4-2} = C_{pm} \frac{\gamma-1}{\gamma} \ln \frac{V_2}{V_1} = R \ln 2 = 5.76 J/K$$





6-26 1kg  $20^{\circ}\text{C}$  的水与  $100^{\circ}\text{C}$  与  $100^{\circ}\text{C}$  的热源接触, 使水温  $100^{\circ}\text{C}$

(1) 水的熵变  $C = 4.18 \times 10^3 \text{ J/(kg} \cdot \text{K)}$  定压热容

1kg 质量, 水吸热  $dQ = mc dT$

水  $T$  由  $20^{\circ} \rightarrow 100^{\circ}\text{C}$  的熵变

$$\Delta S_{\text{水}} = \int \frac{dQ}{T} = mc \int_{T_1}^{T_2} \frac{dT}{T} = mc \ln \frac{T_2}{T_1} = 1 \times 4.18 \times 10^3 \times \ln \frac{373}{293} = 1.01 \times 10^3 \text{ J/K}$$

(2) 热源的熵变, 放出的热量完全被水吸收

$$Q = -mc \Delta T = -mc (T_2 - T_1)$$

热源的熵变

$$\Delta S_{\text{热源}} = \frac{Q}{T_2} = -mc \frac{\Delta T}{T_2} = -1 \times 4.18 \times 10^3 \times \frac{30}{373} = -8.97 \times 10^2 \text{ J/K}$$

(3) 水与热源系统总熵变

$$\Delta S = \Delta S_{\text{水}} + \Delta S_{\text{热源}} = (1.01 \times 10^3 - 8.97 \times 10^2) \text{ J/K} = 1.13 \times 10^2 \text{ J/K}$$

总熵变是增加的。

