

FK1

Summary: Derive the Expressions for Linear strain rate, shear strain rate, & volumetric strain rate, as well as an expression for vorticity

Assumptions: steady state, incompressible

Analysis:

1) Linear Strain Rate:

$$\epsilon_{xx} = \frac{\partial u}{\partial x} \quad \epsilon_{yy} = \frac{\partial v}{\partial y} \quad \epsilon_{zz} = \frac{\partial w}{\partial z}$$

where,

$$\frac{d}{dt} \left(\frac{(u + \frac{\partial u}{\partial x} dx) dt + dx - u - u dx - dx}{dx} \right) = \frac{\partial u}{\partial x}$$

$$\text{Shear strain rate: } \epsilon_{xy} = \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) \quad \epsilon_{xz} = \frac{1}{2} \left(\frac{\partial w}{\partial x} + \frac{\partial u}{\partial z} \right)$$

$$\epsilon_{yz} = \frac{1}{2} \left(\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right)$$

$$\begin{bmatrix} \epsilon_{xx} & \epsilon_{xy} & \epsilon_{xz} \\ \epsilon_{yx} & \epsilon_{yy} & \epsilon_{yz} \\ \epsilon_{zx} & \epsilon_{zy} & \epsilon_{zz} \end{bmatrix} = \begin{bmatrix} \frac{\partial u}{\partial x} & \frac{1}{2} \left(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right) & \frac{1}{2} \left(\frac{\partial w}{\partial x} + \frac{\partial u}{\partial z} \right) \\ \frac{1}{2} \left(\frac{\partial v}{\partial x} + \frac{\partial u}{\partial y} \right) & \frac{\partial v}{\partial y} & \frac{1}{2} \left(\frac{\partial v}{\partial z} + \frac{\partial w}{\partial y} \right) \\ \frac{1}{2} \left(\frac{\partial w}{\partial x} + \frac{\partial u}{\partial z} \right) & \frac{1}{2} \left(\frac{\partial w}{\partial y} + \frac{\partial v}{\partial z} \right) & \frac{\partial w}{\partial z} \end{bmatrix}$$

Volumetric Strain Rate:

$$\frac{1}{V} \frac{DV}{Dt} = \frac{1}{V} \frac{DV}{Dt} = \epsilon_{xx} + \epsilon_{yy} + \epsilon_{zz} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}$$

$$2) \quad \omega = \nabla \times \mathbf{U} = \begin{vmatrix} \mathbf{i} & \mathbf{j} & \mathbf{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix} \quad \begin{aligned} \omega_x &= \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} & \omega_y &= \frac{\partial v}{\partial z} - \frac{\partial w}{\partial x} \\ \omega_z &= \frac{\partial u}{\partial y} - \frac{\partial v}{\partial x} \end{aligned}$$

Results: Vorticity is a measure of local spinning within a fluid usually inside the boundary layer and is defined as the curl of the velocity field: $\omega = \nabla \times \mathbf{U}$

FK2

Summary: Explain the units of vorticity and how it is measured, find and explain the behavior of vorticity on a hydrofoil. Derive an equation for freestream vorticity.

Assumptions: Incompressible Flow, non-rotational outside of boundary layer

Analysis:

Analysis:

1) units of vorticity are sec^{-1} or Hz , and the vorticity is negligible in freestream

Assumptions

- Everything inside the boundary is rotational
- Everything outside is not

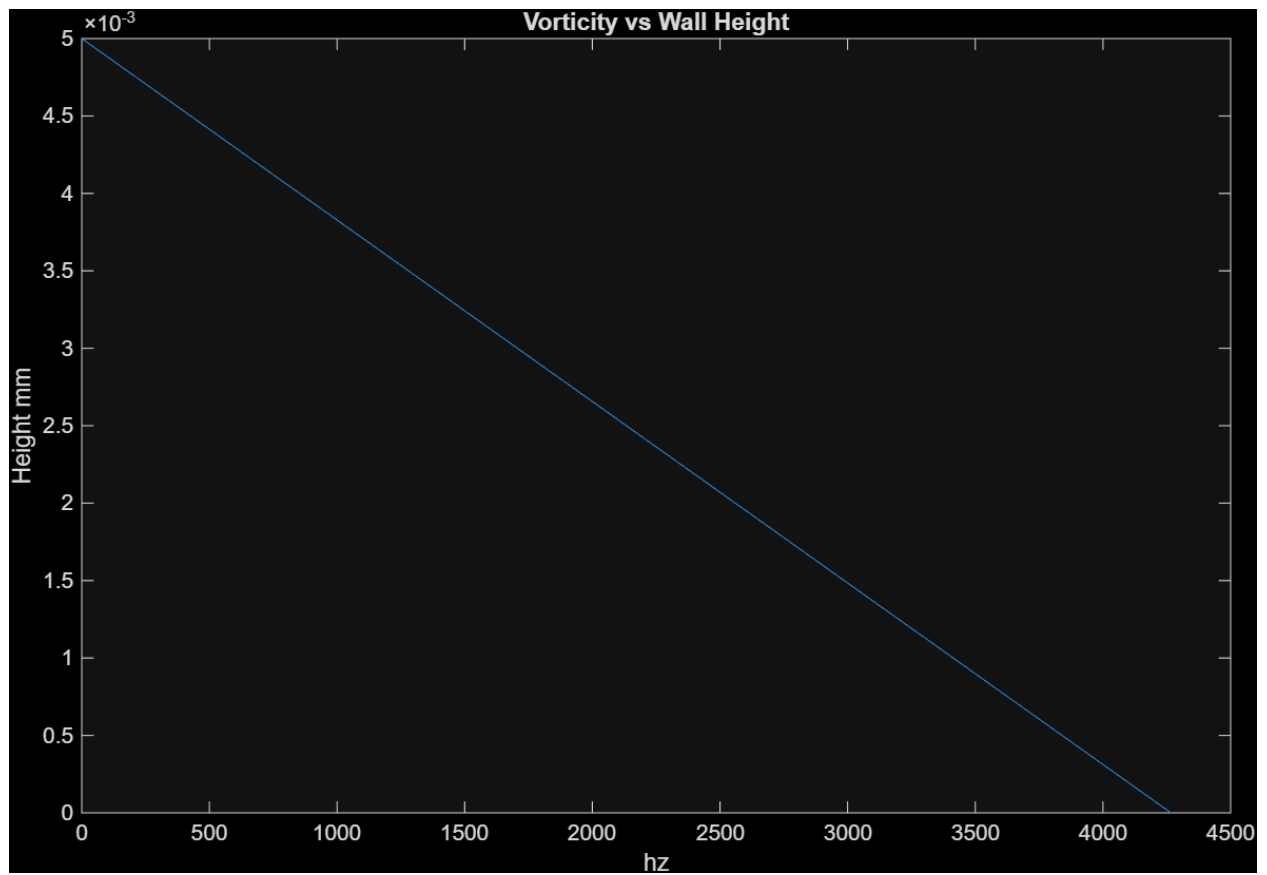
$$2) \vec{\omega} = \nabla \times \vec{U} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix}, \quad \omega_x = \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z}, \quad \omega_y = \frac{\partial u}{\partial z} - \frac{\partial w}{\partial x}, \quad \omega_z = \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y}$$

$$\omega = 0, \quad \frac{\partial}{\partial z} = 0 \rightarrow \omega_x = \omega_y = 0, \quad \frac{\partial v}{\partial x} = 0 \rightarrow \omega_z = \frac{\partial v}{\partial y} = -\frac{\rho g \sin(\theta)}{\mu} (h - y)$$

Plot in MATLAB

Vorticity at 5mm is the lowest at 0 Hz on the graph, this value should be approaching zero on the top boundary as there is a boundary condition there.

Results/Plot:



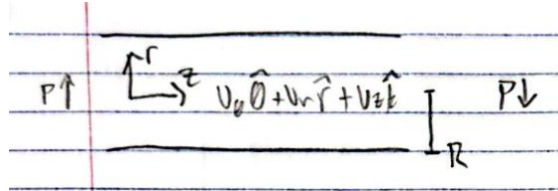
You can see the vorticity is zero at height zero and most frequent at highest height, confirming our predictions.

NSE2

Summary: Solve the Navier Stokes equations in cylindrical coordinates for fully developed flow moving in the z direction of pipe radius R and infinite length. Moving because of a pressure drop.

Assumptions: 1D Flow, P.E./Gravity negligible

Analysis:



$$\rho \left(\frac{\partial v_z}{\partial t} + u_r \frac{\partial v_z}{\partial r} + \frac{u_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} \left(\frac{1}{r} \frac{\partial(r r_{rz})}{\partial r} + \frac{1}{r} \frac{\partial^2 v_z}{\partial r^2} + \frac{\partial^2 v_z}{\partial z^2} \right) + \rho g_z$$

$$\frac{\partial P}{\partial z} = \frac{1}{r} \frac{\partial(r r_{rz})}{\partial r} \rightarrow \frac{\partial P}{\partial z} = \frac{1}{r} \frac{\partial}{\partial r} \mu r \frac{\partial v}{\partial r}$$

$$\rightarrow \frac{\partial^2 v}{\partial r^2} = \frac{r}{\mu} \frac{\partial P}{\partial z}, \text{ Boundary conditions:}$$

At center $\frac{\partial v}{\partial r} = 0$ (max)

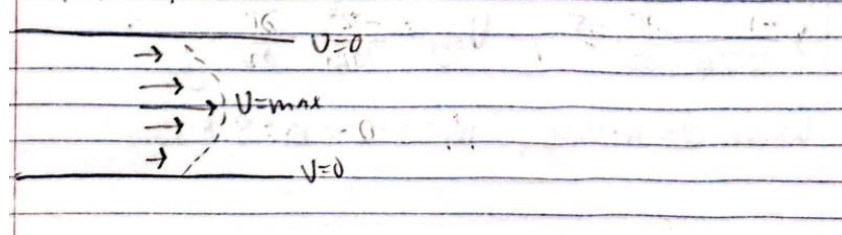
At perimeter $v = 0$

$$\text{So, } \frac{\partial v}{\partial r} = \frac{1}{2} r^2 \cdot \frac{1}{\mu} \frac{\partial P}{\partial z} + C_1 \quad \text{Where, } C_1 = 0$$

$$v(r) = \frac{1}{6} r^3 \cdot \frac{1}{\mu} \frac{\partial P}{\partial z} + C_1 + C_2 \quad C_2 = -\frac{R^3}{6\mu} \frac{\partial P}{\partial z}$$

$$\rightarrow v(r) = \frac{r^3}{6\mu} \frac{\partial P}{\partial z} - \frac{R^3}{6\mu} \frac{\partial P}{\partial z}$$

Sketch:



From old HW: $\dot{m} = S A U_{avg}$ \downarrow $U(r)$

Where, $U_{avg} = \frac{1}{A} \int_0^R \left(\frac{r^3}{6\mu} \frac{\partial P}{\partial z} - \frac{R^3}{6\mu} \frac{\partial P}{\partial z} \right) 2\pi r dr$

$$\rightarrow \frac{1}{\pi R^2} \int_0^R \left(\frac{r^3}{6\mu} \frac{\partial P}{\partial z} - \frac{R^3}{6\mu} \frac{\partial P}{\partial z} \right) 2\pi r dr$$

$$\rightarrow \frac{2}{R^2} \int_0^R \left(\frac{r^3}{6\mu} \frac{\partial P}{\partial z} - \frac{R^3}{6\mu} \frac{\partial P}{\partial z} \right) r dr$$

$$\rightarrow \frac{2}{R^2} \int_0^R \left(\frac{r^4}{6\mu} \frac{\partial P}{\partial z} - \frac{R^3 r}{6\mu} \frac{\partial P}{\partial z} \right) dr$$

$$\rightarrow U_{avg} = \frac{2 \partial P}{R^2 6\mu \partial z} \int_0^R (r^4 - R^3 r) dr$$

$$\rightarrow \frac{2 \partial P}{R^2 6\mu \partial z} \left(\frac{1}{5} r^5 - \frac{1}{2} R^3 r^2 \right) \Big|_0^R$$

$$\rightarrow \frac{2 \partial P}{R^2 6\mu \partial z} \left(\frac{1}{5} R^5 - \frac{1}{2} R^5 \right) \rightarrow \frac{1}{R^2 6\mu} \frac{\partial P}{\partial z} \left(\frac{-3}{10} R^5 \right)$$

$$\rightarrow \frac{-1}{10 R^2 \mu} \frac{\partial P}{\partial z} \cdot R^5, \quad U_{avg} = \frac{-R^3}{10\mu} \cdot \frac{\partial P}{\partial z}$$

Where $Q = A \cdot U_{avg}$, $\dot{m} = S \cdot Q \rightarrow \dot{m} = S \cdot A \cdot U_{avg}$

CNM2

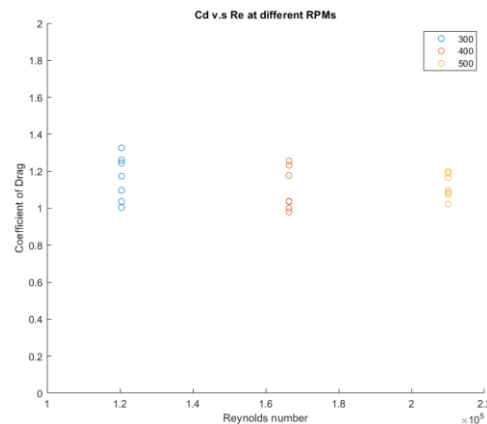
Summary: Use Ansys Fluent to solve for both Steady and Unsteady flows around a cylinder. Compare results of Cd vs Theta and Strouhal vs Re

Assumptions: 1D Flow, P.E./Gravity negligible

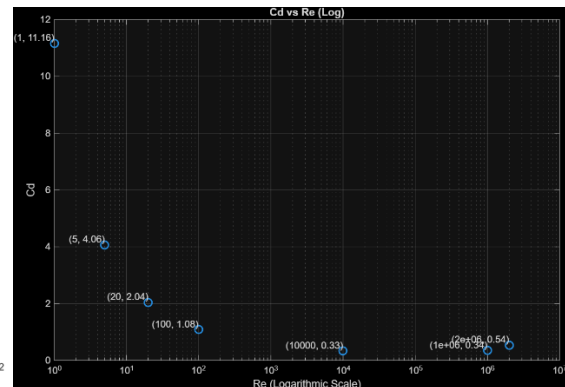
Analysis:

1. Steady Flow Past a Cylinder

- (Certificate was \$15, but course is complete)
- Results at bottom before code
- These Reynolds numbers were tested/simulated and plotted on a log scale (bottom): 1,5,20,100,10000,1000000,2000000 their corresponding Cd: 11.1628,4.0640,2.0403,1.0834,0.3286,0.34426,0.5357. A clear pattern is seen emerging, where Cd is dropping / behaving inversely to the size of the Reynolds number. This matches theory and follows the trend witnessed in lab 2 of decreasing Cd with higher Re. Although at very high Reynolds Numbers the Cd seemed to pick back up.

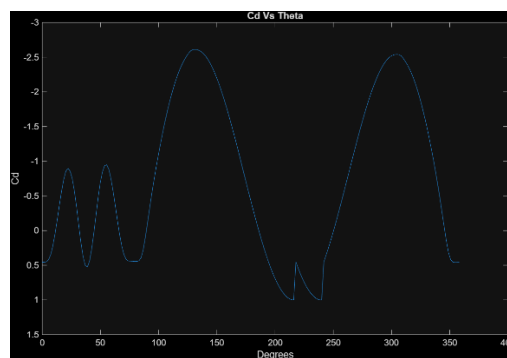


(Lab 2 Values)

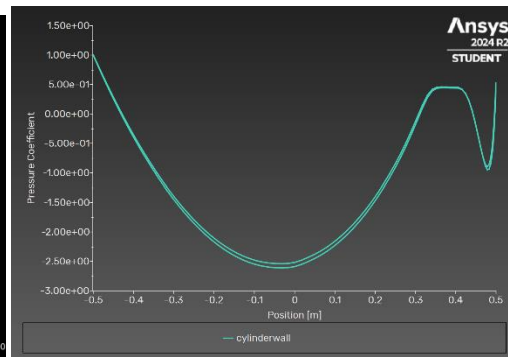


Ansys Simulated Values

- Solving for Cd at different parts of the cylinder provides two graphs that show a similar pattern seen in lab 2:



Cd vs Theta

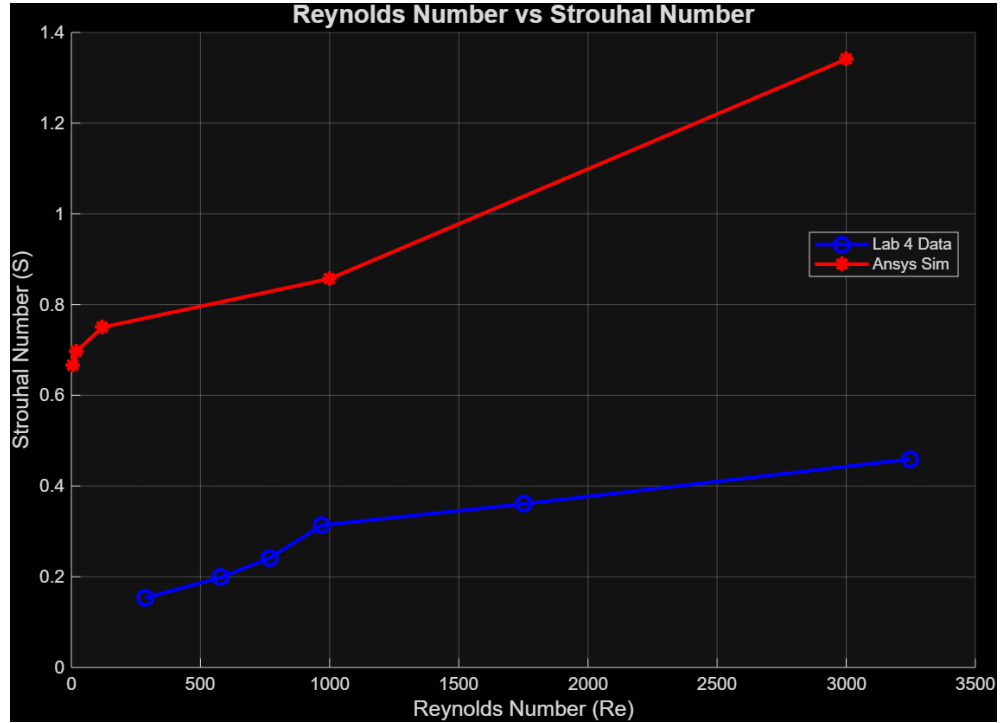


Cd vs Position

You can see in the Cd vs Position graphs there are two lines each one representing one half of the cylinder (top & bottom)

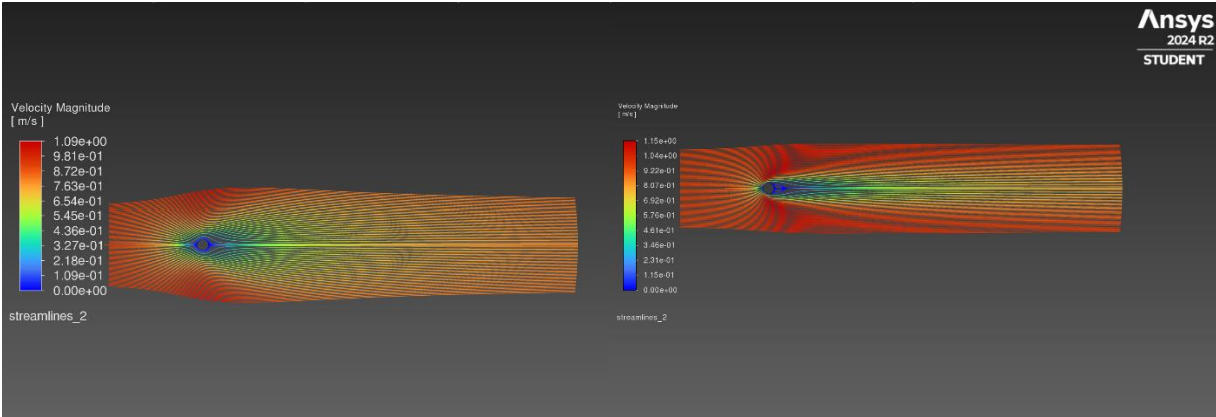
2. Unsteady Flow Past a Cylinder

- (Certificate was \$15, but course is complete)
- Will be shown below
- Analyzing the change in the Strouhal number revealed that at least for lower Reynolds numbers the Strouhal number increases with Re :



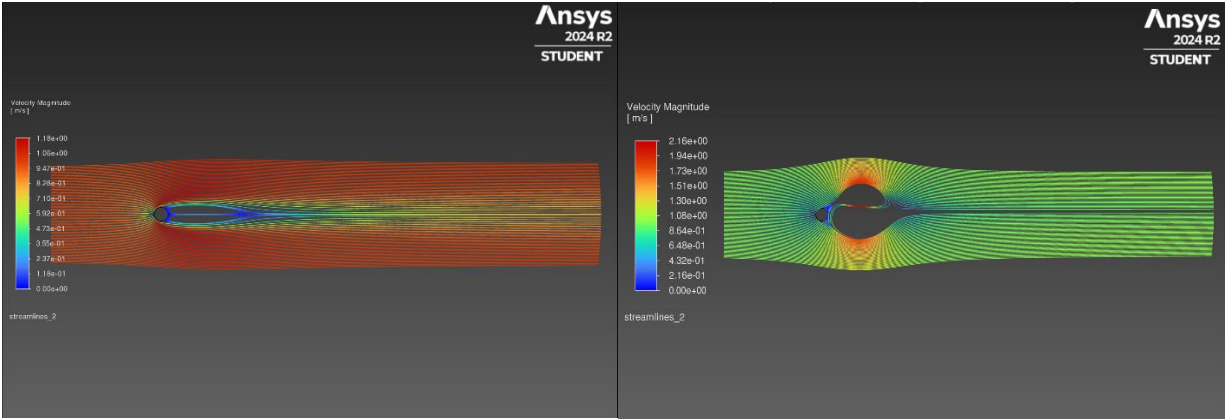
Here you can see that trend, although with a slight offset. You can still see the numbers rising.

Steady Flow Past a Cylinder: Flow Fields:



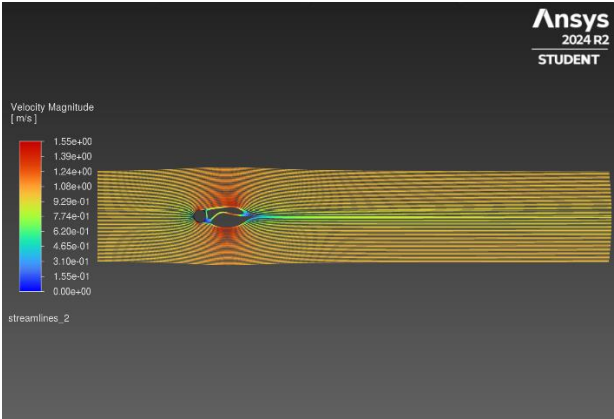
Re = 1

Re = 20



Re = 100

Re = 10,000



Re = 1,000,000

Unsteady Flow Past a Cylinder: Flow Fields:

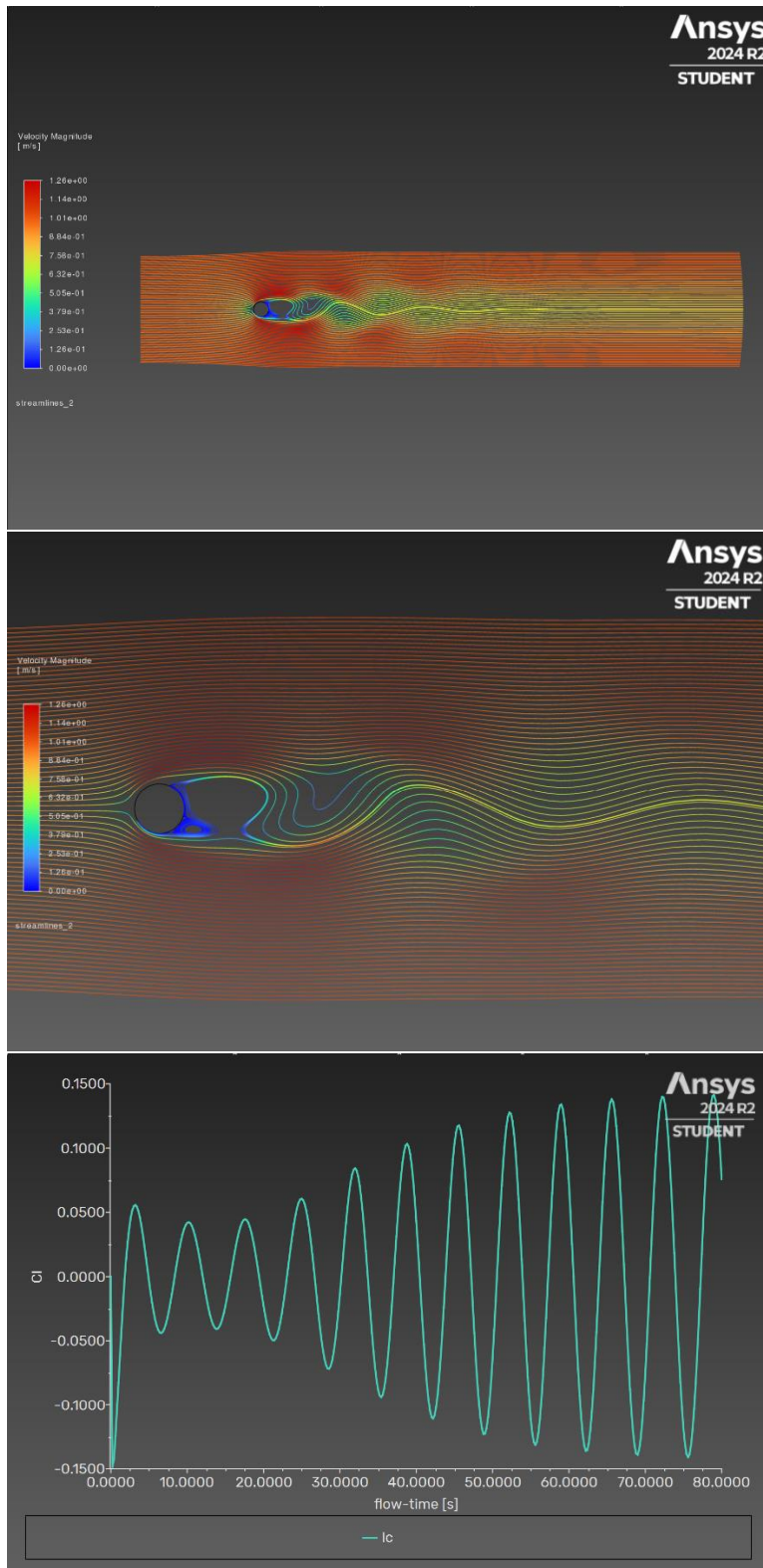


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```
%Roshan Jaiswal-Ferri
%Section - 01
%AERO 302 Homework 3 - 11/20/24
```

Workspace Prep

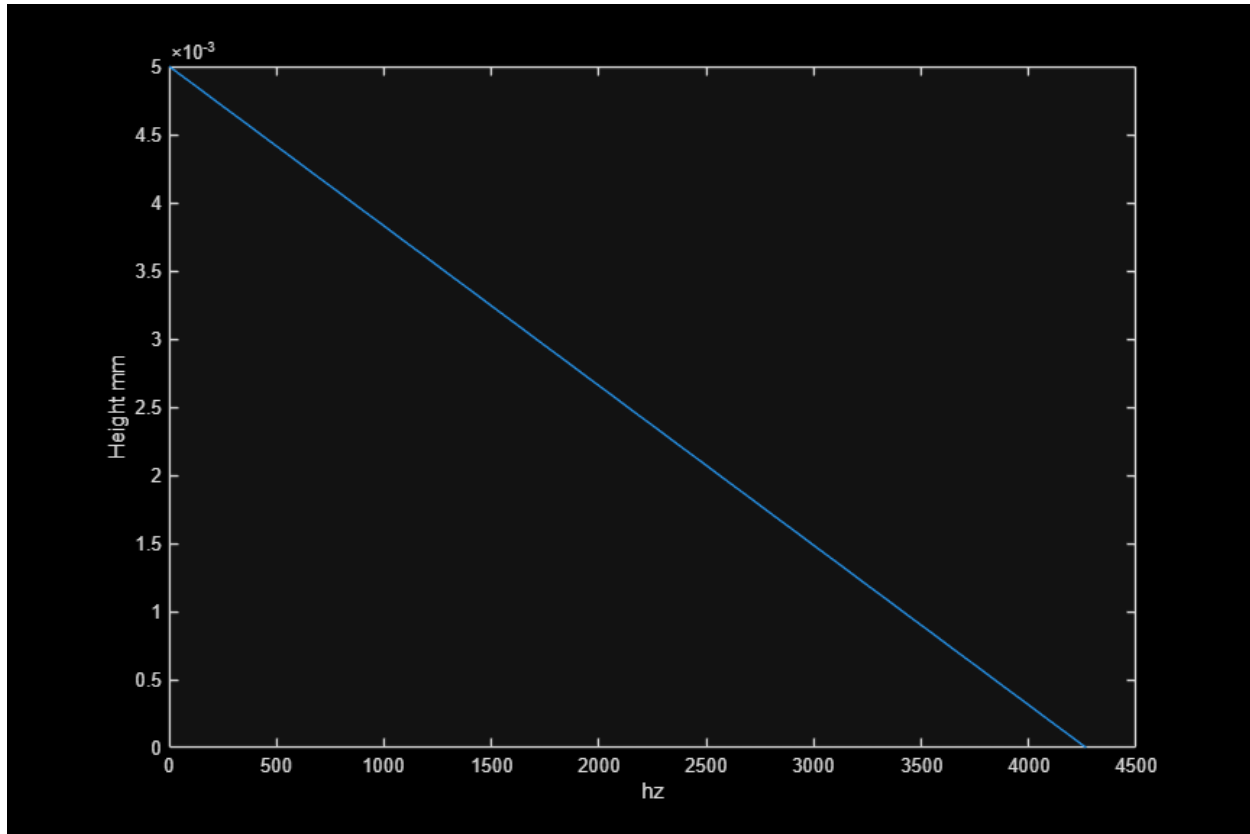
```
format long      %Allows for more accurate decimals
close all;       %Clears all
clear all;       %Clears Workspace
clc;            %Clears Command Window
```

PART 1: FK2

```
T = 293;
theta = 5;
g = -9.81;
y = linspace(0, (5/1000), 200);
mu = 1.002e-3; %pa*s
rho = 1000; %kg/m^3
h = 5/1000;

zeta = -((rho*g*sind(theta))/mu)*(h-y);

plot(zeta, y);
xlabel('hz')
ylabel('Height mm')
```



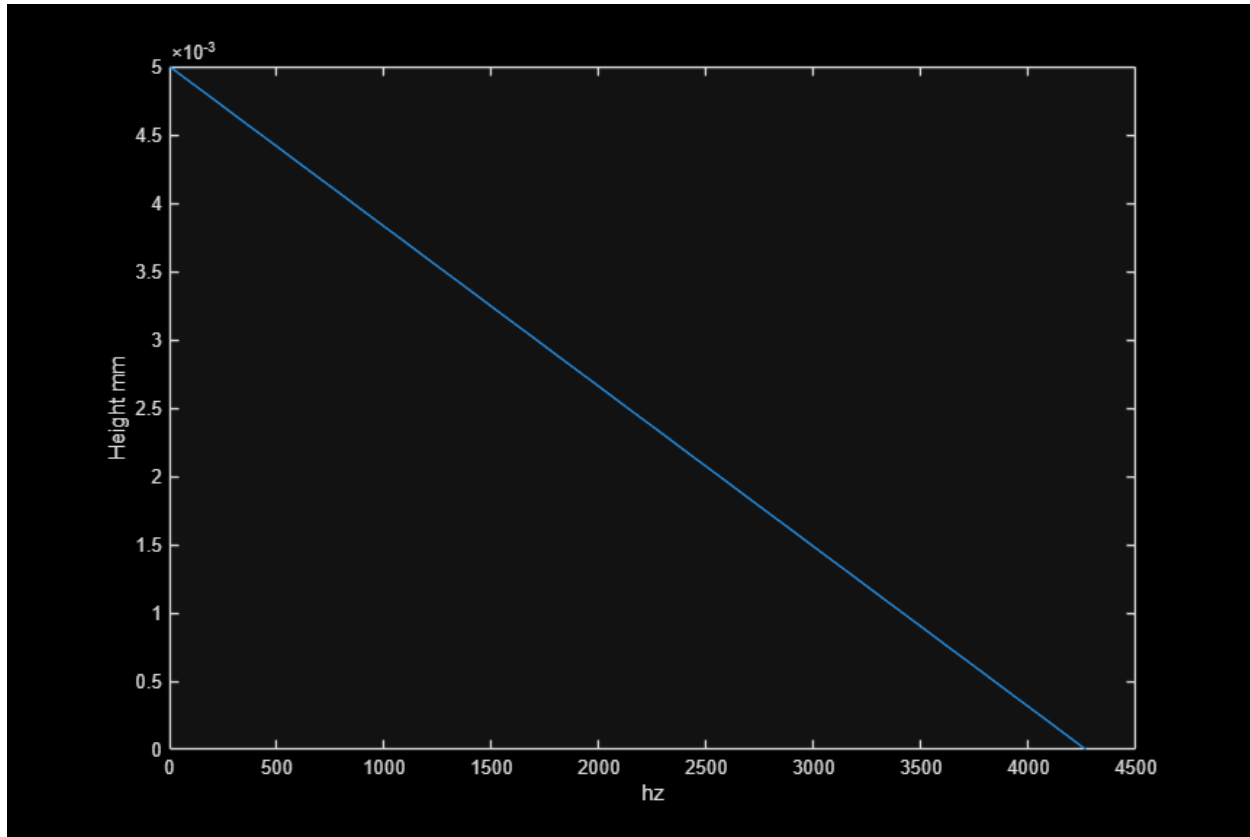
Cd vs Re

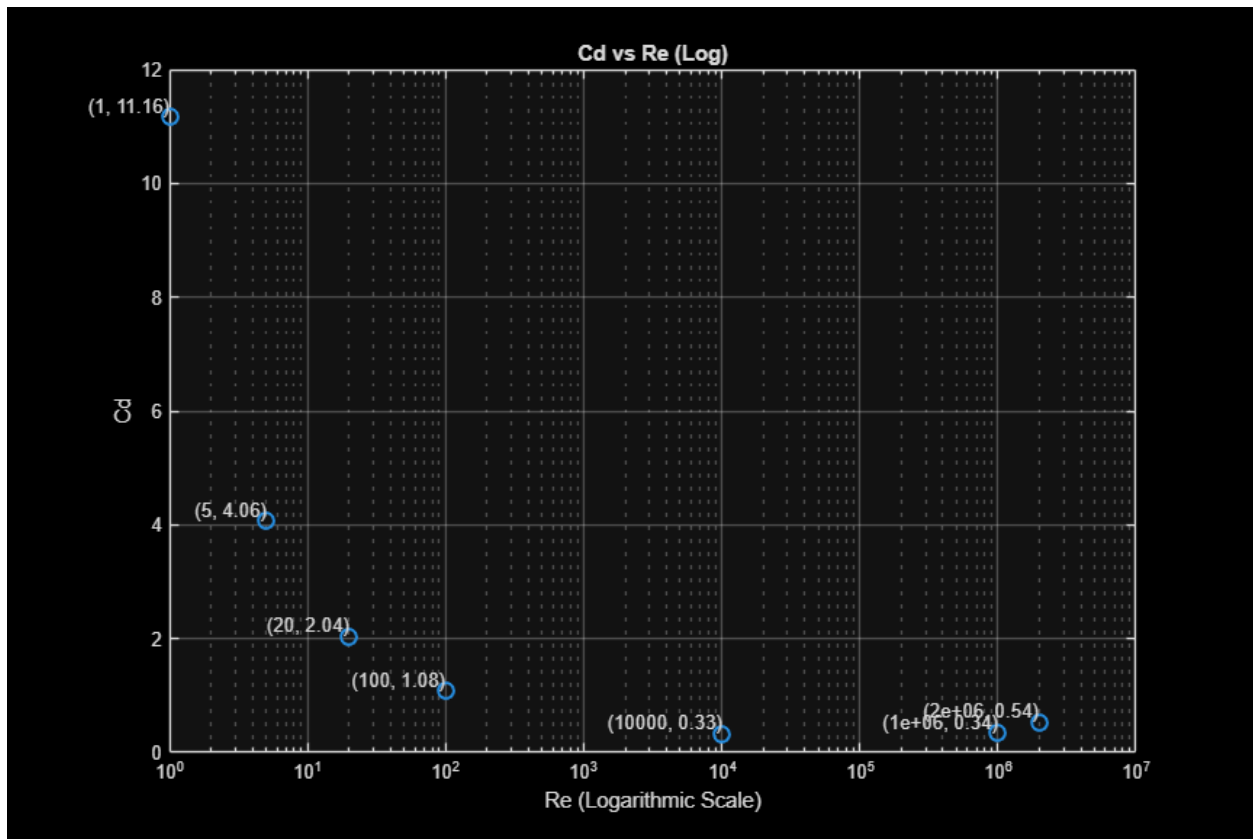
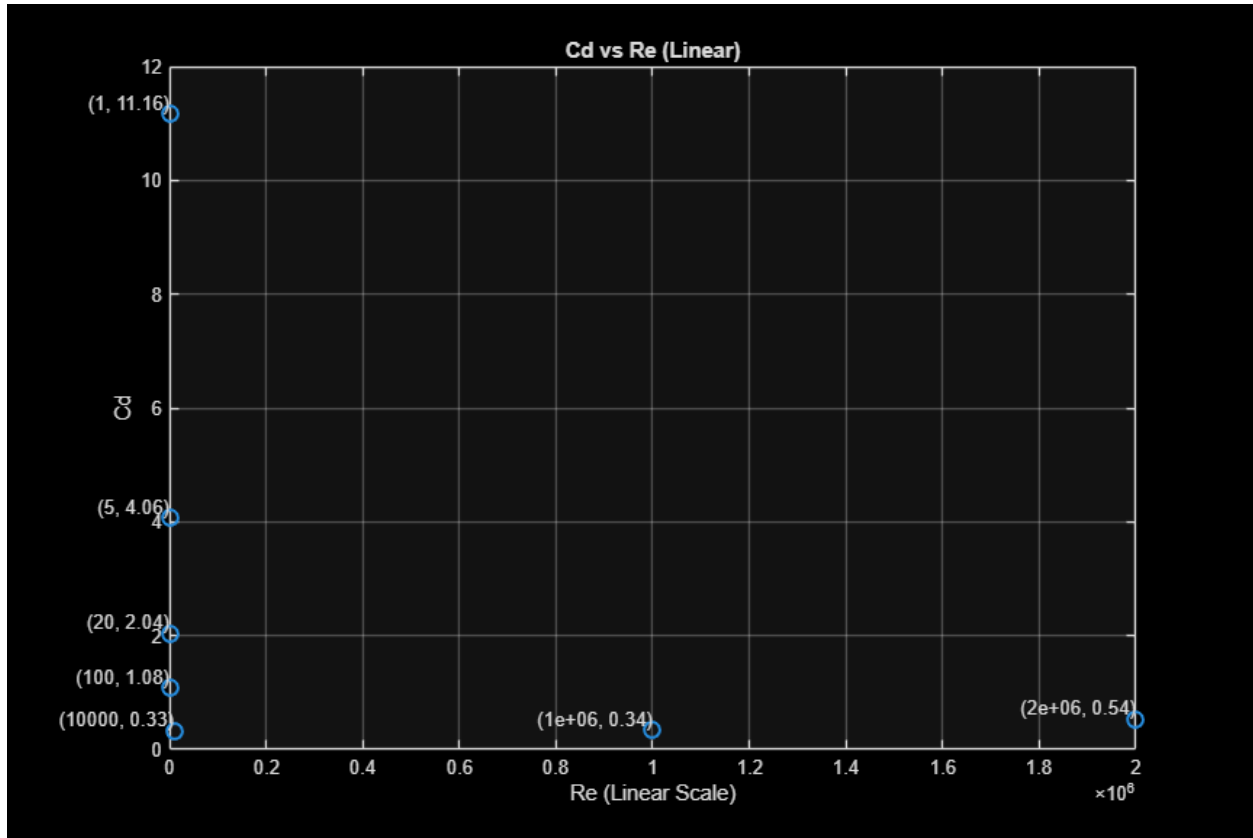
```
Re = [1,5,20,100,10000,1000000,2000000];  
Cd = [11.1628,4.0640,2.0403,1.0834,0.3286,0.34426,0.5357];
```

```
figure('Name','Cd vs Re (Linear)')  
plot(Re, Cd, 'o', 'MarkerSize', 8, 'LineWidth', 1.5);  
xlabel('Re (Linear Scale)');  
ylabel('Cd');  
title('Cd vs. Re (Linear Scale)');  
grid on;  
% Add labels to points  
for i = 1:length(Re)  
    text(Re(i), Cd(i), sprintf('(%g, %.2f)', Re(i), Cd(i)), ...  
        'VerticalAlignment', 'bottom', 'HorizontalAlignment', 'right');  
end  
title('Cd vs Re (Linear)');
```

```
figure('Name','Cd vs Re (Log)')  
plot(Re, Cd, 'o', 'MarkerSize', 8, 'LineWidth', 1.5);  
set(gca, 'XScale', 'log');  
xlabel('Re (Logarithmic Scale)');  
ylabel('Cd');  
title('Cd vs. Re (Logarithmic Scale)');  
grid on;  
% Add labels to points
```

```
for i = 1:length(Re)
    text(Re(i), Cd(i), sprintf('(%g, %.2f)', Re(i), Cd(i)), ...
        'VerticalAlignment', 'bottom', 'HorizontalAlignment', 'right');
end
title('Cd vs Re (Log)');
```





Workspace Prep

```
clear all;           %Clears Workspace
```

Strouhal #s

```
hz = 15;
U1 = 2.429*hz; %speed in mm/s
U = U1/1000; %speed in m/s

t = 54-47; %Time for 5 vorticies
vD6 = 5/t; %vorticies / second

t = 11;
vD5 = 5/t;

t = 12;
vD4 = 5/t;

t = 7;
vD3 = 3/7;

t = 11;
vD2 = 3/11;

t = 16;
vD1 = 3/16;

Di = [3.515,1.897,1.05,0.832,0.626,0.308]; % in inches
D = Di.*0.0254; %diam in meters

f = [vD1,vD2,vD3,vD4,vD5,vD6];

for i = 1:6
    S(i) = (f(i)*D(i))/U; %strouhal number
end

%Re Calc:

rho = 1000;
u = 0.0010016; %dyn visc of water at 20C

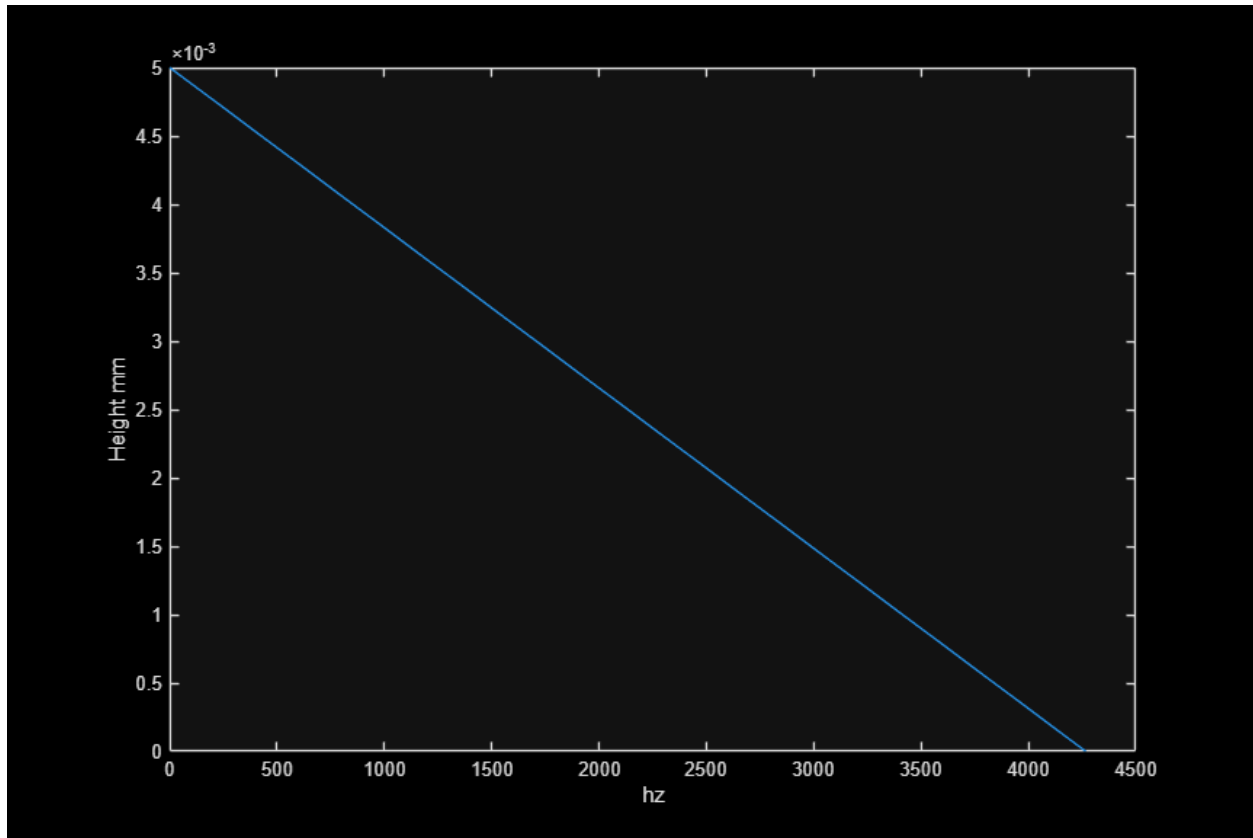
for i = 1:6
    Re(i) = (rho*U*D(i))/u;
end
```

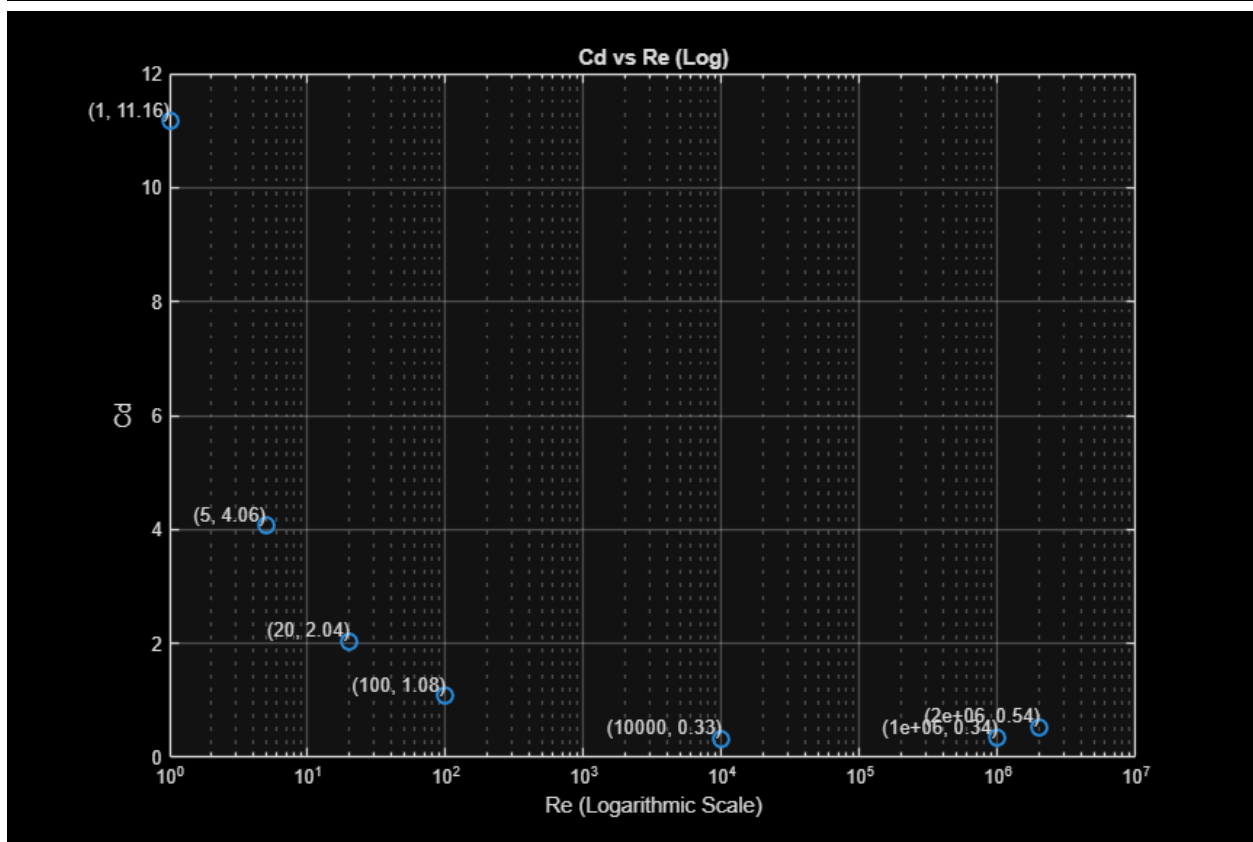
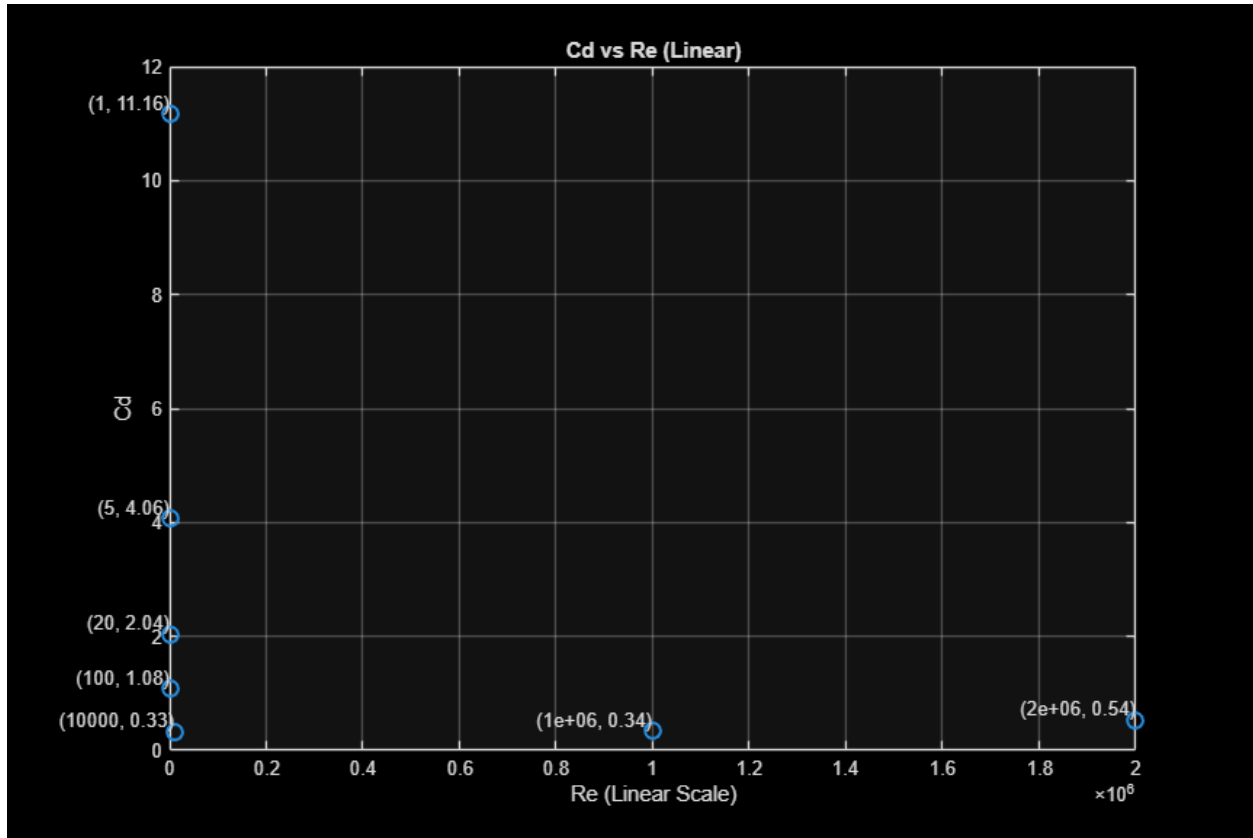
HW Calcs

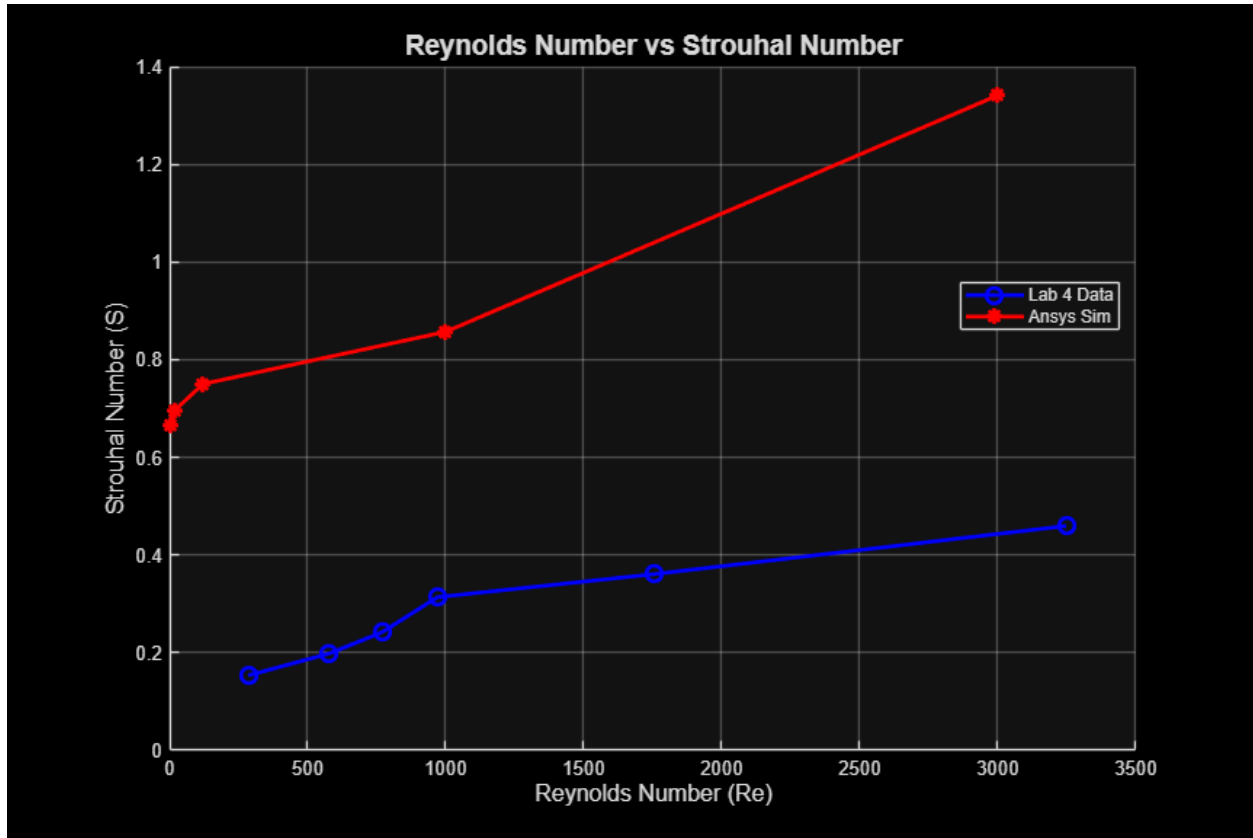
```
Re2 = [5,20,120,1000,3000]; %Calculated form # of vorticies per time in
animation
S2 = [0.666,0.697,0.75,0.857,1.341];
```

Plotting

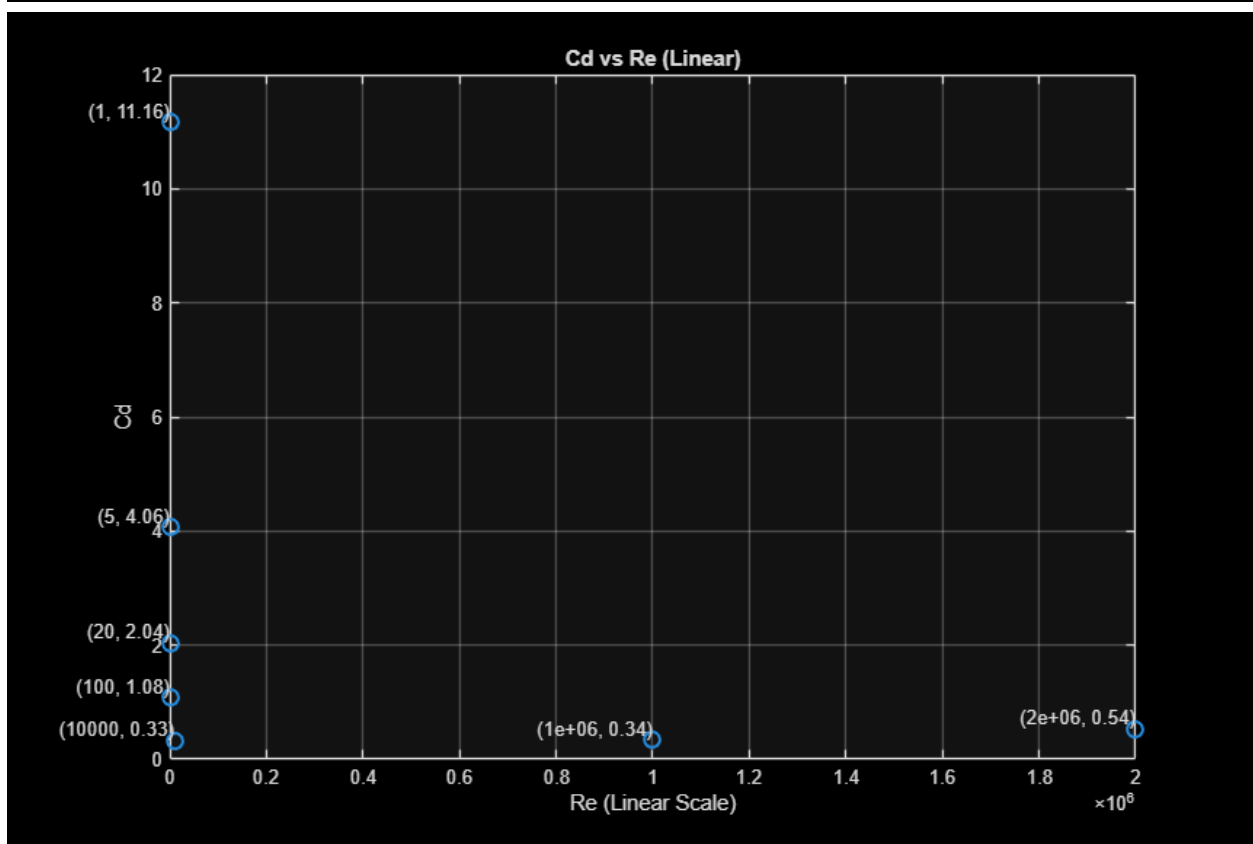
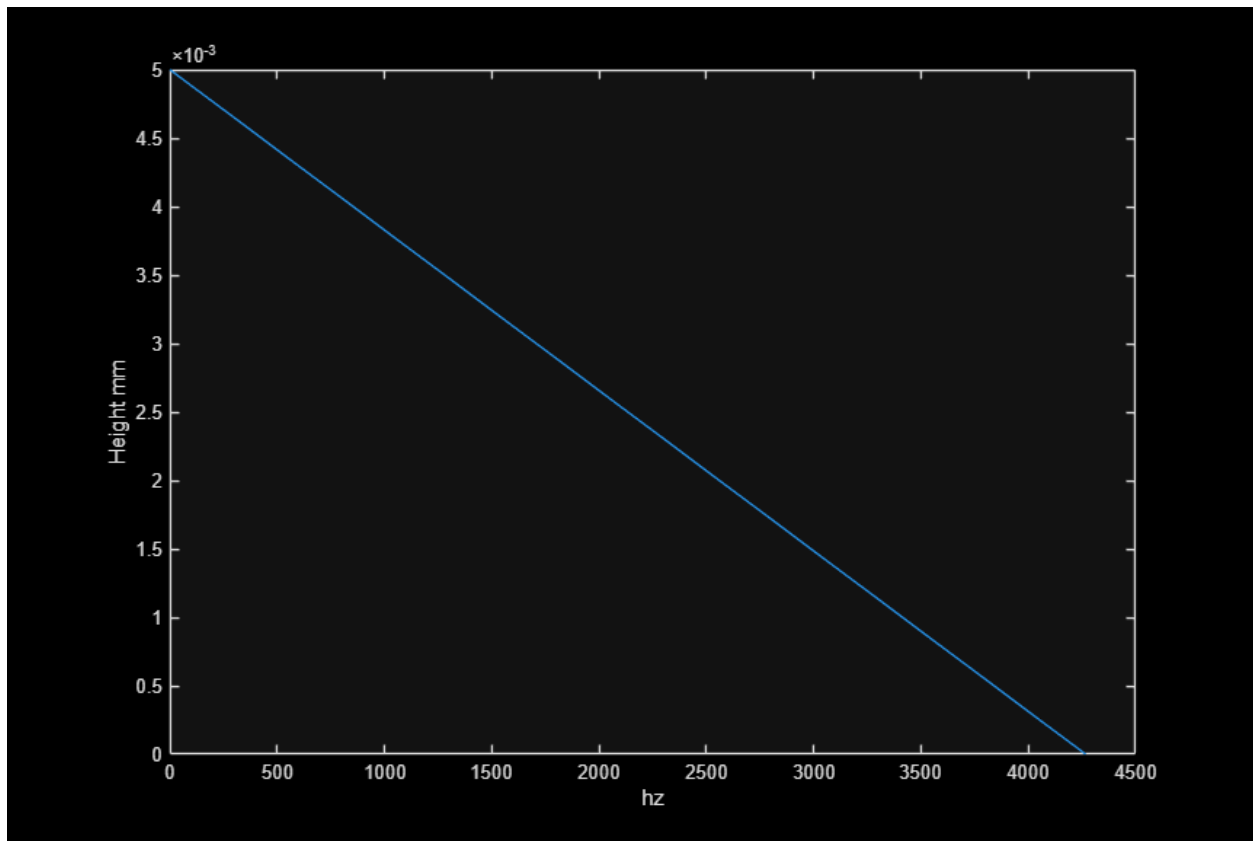
```
figure;  
hold on;  
grid on;  
  
% Plot S vs Re  
plot(Re, S, 'bo-', 'LineWidth', 2, 'MarkerSize', 8);  
  
% Plot S2 vs Re2  
plot(Re2, S2, 'r*- ', 'LineWidth', 2, 'MarkerSize', 8);  
  
% Add labels, title, and legend  
xlabel('Reynolds Number (Re)', 'FontSize', 12);  
ylabel('Strouhal Number (S)', 'FontSize', 12);  
title('Reynolds Number vs Strouhal Number', 'FontSize', 14);  
legend('Lab 4 Data', 'Ansys Sim', 'Location', 'Best');
```

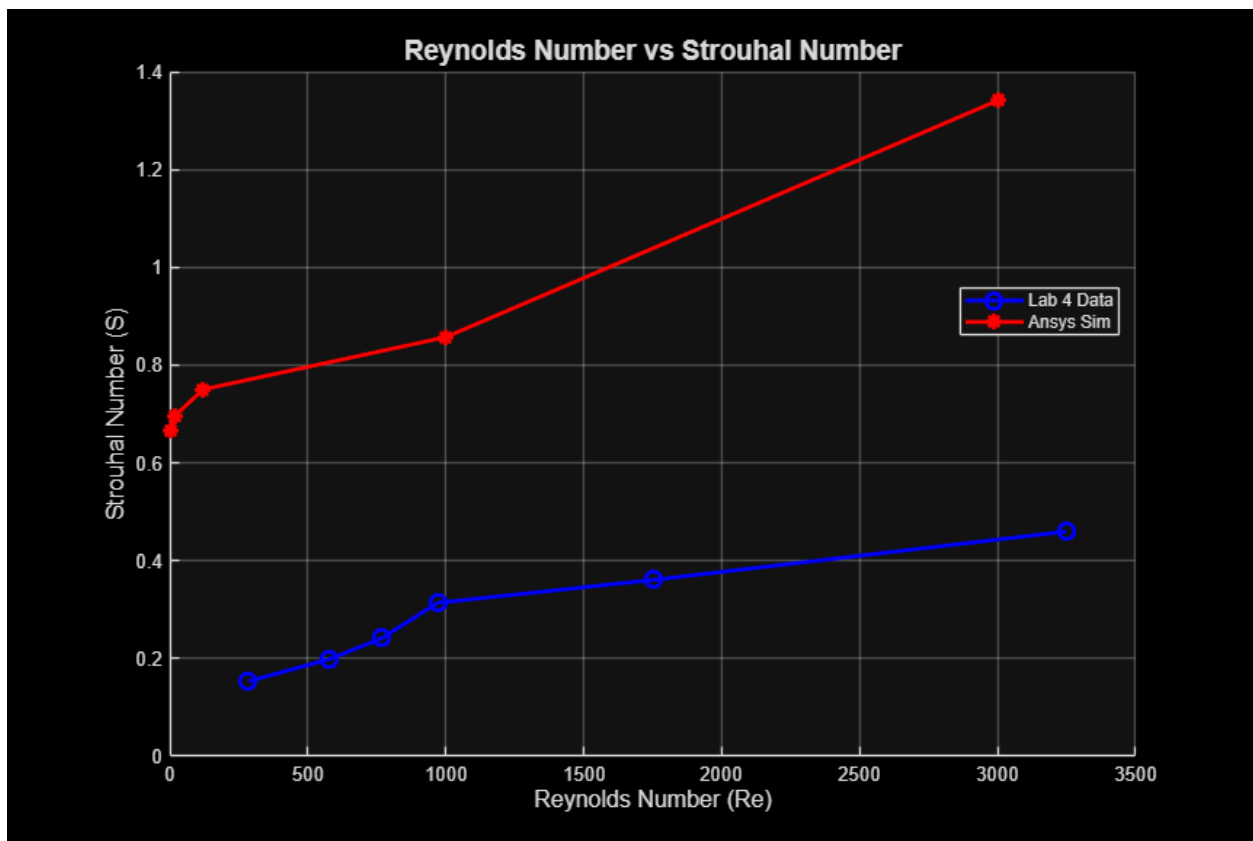
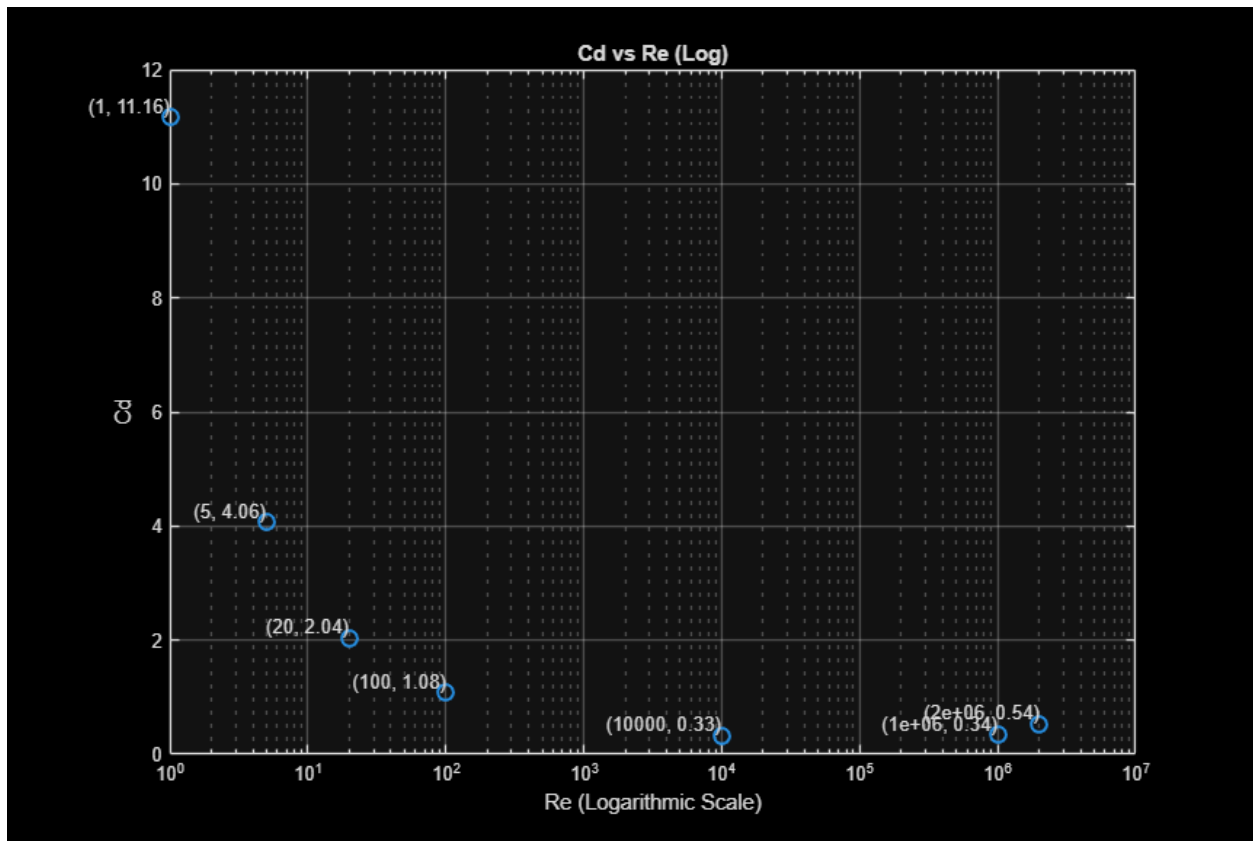


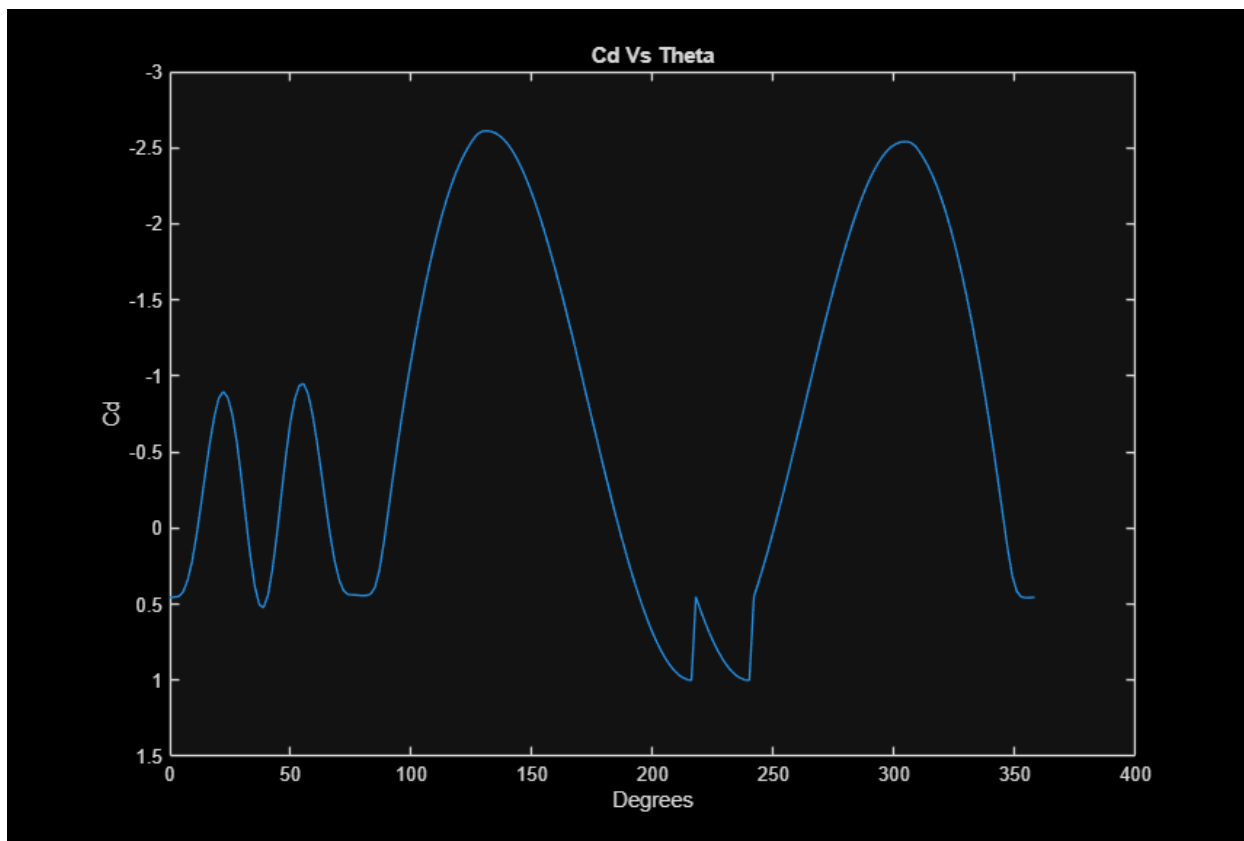




```
xy = readmatrix("CdPos");  
theta = linspace(0,360,196);  
  
figure  
plot(theta,xy(:,2))  
set(gca, 'YDir', 'reverse')  
xlabel("Degrees")  
ylabel('Cd')  
title('Cd Vs Theta')
```







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