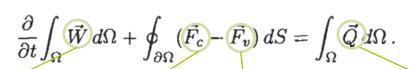


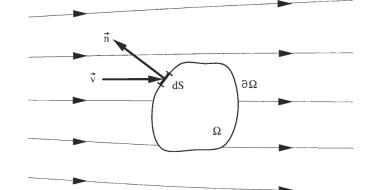
Part-II: Compressible FVM methods in OF

## **GEs for Compressible Flow: CFD**



# The Conservation Equations in **Integral Form**





$$\vec{W} = \begin{bmatrix} \rho \\ \rho u \\ \rho v \\ \rho w \\ \rho E \end{bmatrix}$$

$$\vec{F_c} = \begin{bmatrix} \rho V \\ \rho u V + n_x p \\ \rho v V + n_y p \\ \rho w V + n_z p \\ \rho H V \end{bmatrix}$$

$$V \equiv \vec{v} \cdot \vec{n} = n_x u + n_y v + n_z w$$

$$\vec{F_c} = \begin{bmatrix} \rho V \\ \rho uV + n_x p \\ \rho vV + n_y p \\ \rho wV + n_z p \\ \rho HV \end{bmatrix}, \quad \vec{F_v} = \begin{bmatrix} 0 \\ n_x \tau_{xx} + n_y \tau_{xy} + n_z \tau_{xz} \\ n_x \tau_{yx} + n_y \tau_{yy} + n_z \tau_{zz} \\ n_x \tau_{zx} + n_y \tau_{zy} + n_z \tau_{zz} \\ n_x \tau_{zx} + n_y \sigma_{y} + n_z \sigma_{z} \end{bmatrix}, \quad \vec{Q} = \begin{bmatrix} 0 \\ \rho f_{e,x} \\ \rho f_{e,y} \\ \rho f_{e,z} \\ \rho f_{e} \cdot \vec{v} + \dot{q}_h \end{bmatrix}.$$

$$\Theta_x = u\tau_{xx} + v\tau_{xy} + w\tau_{xz} + k\frac{\partial T}{\partial x}$$

$$\Theta_y = u\tau_{yx} + v\tau_{yy} + w\tau_{yz} + k\frac{\partial T}{\partial y}$$

$$\Theta_z = u\tau_{zx} + v\tau_{zy} + w\tau_{zz} + k\frac{\partial T}{\partial z}$$

$$ec{Q} = \left[ egin{array}{c} 
ho f_{e,x} \\ 
ho f_{e,y} \\ 
ho f_{e,z} \\ 
ho ec{f}_e \cdot ec{v} + \dot{q}_h \end{array} 
ight].$$



# Integration of time derivative

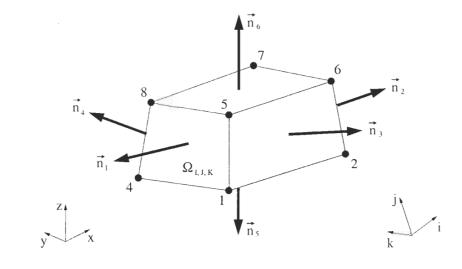
$$rac{\partial}{\partial t}\int_{\Omega}ec{W}\,d\Omega+\oint_{\partial\Omega}(ec{F}_{c}-ec{F}_{v})\,dS=\int_{\Omega}ec{Q}\,d\Omega\,.$$
 Step 2

$$rac{\partial}{\partial t}\int_{\Omega}ec{W}\,d\Omega=\Omega\,rac{\partialec{W}}{\partial t}$$
 . Step 7

$$\frac{\partial \vec{W}}{\partial t} = -\frac{1}{\Omega} \left[ \oint_{\partial \Omega} (\vec{F}_c - \vec{F}_v) \, dS - \int_{\Omega} \vec{Q} \, d\Omega \right] \, .$$

Step 3





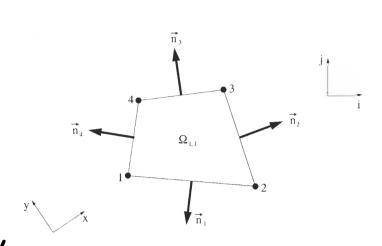
#### Step 4

$$\frac{d\vec{W}_{I,J,K}}{dt} = -\frac{1}{\Omega_{I,J,K}} \left[ \sum_{m=1}^{N_F} (\vec{F}_c - \vec{F}_v)_m \, \Delta S_m \, - \, (\vec{Q}\Omega)_{I,J,K} \right]$$

$$rac{d\, ec{W}_{I,J,K}}{dt} = -rac{1}{\Omega_{I,J,K}}\, ec{R}_{I,J,K}$$



## **Geometrical Quantities of a Control Volume**



#### Volume of cell

$$\Omega_{I,J} = \frac{b}{2} [(x_1 - x_3)(y_2 - y_4) + (x_4 - x_2)(y_1 - y_3)]$$

# Face area of cell

$$\vec{S}_{m} = \begin{bmatrix} S_{x,m} \\ S_{y,m} \end{bmatrix} = \vec{n}_{m} \Delta S_{m}$$

$$\vec{S}_{1} = \begin{bmatrix} S_{x,m} \\ S_{y,m} \end{bmatrix} = \vec{n}_{m} \Delta S_{m}$$

$$\vec{S}_{2} = b \begin{bmatrix} y_{3} - y_{2} \\ x_{2} - x_{3} \end{bmatrix} \quad \vec{n}_{m} = \frac{\vec{S}_{m}}{\Delta S_{m}}$$

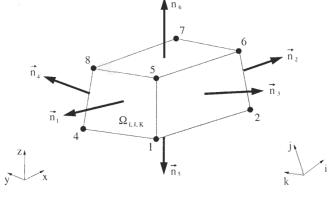
$$\vec{S}_{3} = b \begin{bmatrix} y_{4} - y_{3} \\ x_{3} - x_{4} \end{bmatrix} \quad \Delta S_{m} = |\vec{S}_{m}| = \sqrt{S_{x,m}^{2} + S_{y,m}^{2}}.$$

$$ec{S}_1 = b \left[ egin{array}{l} y_2 - y_1 \ x_1 - x_2 \end{array} 
ight]$$

$$\vec{S}_2 = b \begin{bmatrix} y_3 - y_2 \\ x_2 - x_3 \end{bmatrix} \qquad \vec{n}_m = \frac{\vec{S}_m}{\Delta S_m}$$

$$\vec{S}_3 = b \begin{bmatrix} y_4 - y_3 \\ x_3 - x_4 \end{bmatrix}$$

$$ec{S}_4 = b \left[ egin{array}{c} y_1 - y_4 \ x_4 - x_1 \end{array} 
ight].$$



#### face area of cell

#### Volume of cell

$$\Delta x_A = x_8 - x_1 \,, \quad \Delta x_B = x_5 - x_4 \,,$$

$$\Delta y_A=y_8-y_1\,,\quad \Delta y_B=y_5-y_4$$

$$\Delta z_A = z_8 - z_1 \,, \quad \Delta z_B = z_5 - z_4$$

$$ec{S}_1 = rac{1}{2} \left[ egin{array}{c} \Delta y_A \ \Delta z_B - \Delta z_A \ \Delta y_B \ \Delta z_A \ \Delta x_B - \Delta x_A \ \Delta z_B \ \Delta x_A \ \Delta y_B - \Delta y_A \ \Delta x_B \end{array} 
ight].$$

$$\Delta S_m = \sqrt{S_{x,m}^2 + S_{y,m}^2 + S_{z,m}^2}$$

$$\Delta y_A = y_8 - y_1 \,, \quad \Delta y_B = y_5 - y_4 \,, \quad \Omega_{I,J,K} = rac{1}{3} \sum_{m=1}^{m=6} (ec{r}_{
m mid} \cdot ec{S})_m$$

$$\vec{r}_{\text{mid,1}} = \frac{1}{4}(\vec{r}_1 + \vec{r}_5 + \vec{r}_8 + \vec{r}_4)$$

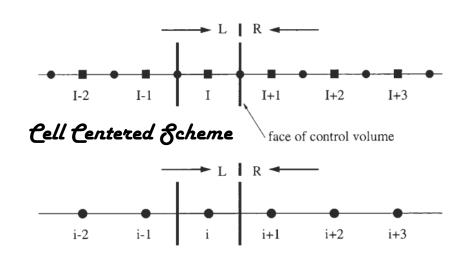


## **Discretization of Convective Terms**

- Various methods available for discretization are
- Central,
- Glux-Vector Splitting
- □ flux-difference Splitting
- □ Total Variation Diminishing (TVD) and
- Fluctuation splitting



# Left & Right States and Stencil



Cell Vertex Scheme

#### Central Scheme

- Vses same number of cells left and right of interface
- flux is "centered" by symmetric cell distribution across cell interface

#### **Vpwinding**

- Uses cells based on information propagation direction based on characteristics
- Asymmetric usage of cells across cell interface

$$U_{R} = U_{I+1} - \frac{\epsilon}{4} \left[ (1+\hat{\kappa})\Delta_{-} + (1-\hat{\kappa})\Delta_{+} \right] U_{I+1}$$

$$U_{L} = U_{I} + \frac{\epsilon}{4} \left[ (1+\hat{\kappa})\Delta_{+} + (1-\hat{\kappa})\Delta_{-} \right] U_{I}.$$

$$\Delta_{+}U_{I} = U_{I+1} - U_{I}$$

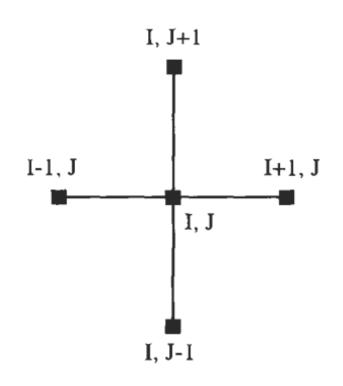
$$\Delta_{-}U_{I} = U_{I} - U_{I-1}.$$

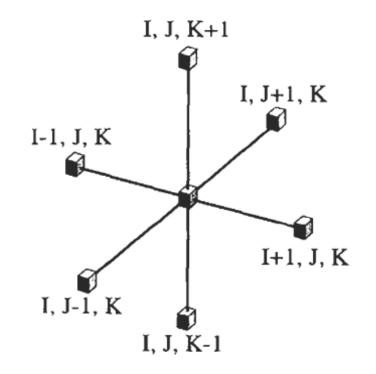
Based on values of  $\epsilon$  and  $\hat{\kappa}$  several upwind schemes can be defined such as

- first order upwind
- Second order upwind
- Vpwind biased linear interpolation
- · Second order central Scheme



Union of cells involved in computation of derived quantities is Stencil
(a)
(b)





2\_])

$$(I,J)$$
  $(I+1,J)$   $(I,J+1)$   $(I-1,J)$   $(I,J-1)$ 

3\_D

$$(I, J, K)$$
  $(I + 1, J, K)$   $(I, J + 1, K)$   $(I - 1, J, K)$   
 $(I, J - 1, K)$   $(I, J, K - 1)$   $(I, J, K + 1)$ .



## Flux Vector Splitting Scheme

1. Van Leer's Scheme

$$\vec{F}_c = \vec{F}_c^+ + \vec{F}_c^-,$$

$$(M_n)_{I+1/2} = \left(\frac{V}{c}\right)$$

$$(M_n)_{I+1/2} = M_L^+ + M_R^-$$

$$M_L^+ = \begin{cases} M_L & \text{if } M_L \ge +1 \\ \frac{1}{4}(M_L + 1)^2 & \text{if } |M_L| < 1 \\ 0 & \text{if } M_L \le -1 \end{cases} \qquad \begin{aligned} \vec{F}_c^\pm &= \begin{bmatrix} f_{\text{mass}}^\pm [n_x(-V \pm 2c)/\gamma + u] \\ f_{\text{mass}}^\pm [n_y(-V \pm 2c)/\gamma + v] \\ f_{\text{mass}}^\pm [n_z(-V \pm 2c)/\gamma + w] \\ f_{\text{energy}}^\pm \end{bmatrix}. \\ |M_n| &< 1 \\ f_{\text{mass}}^+ &= +\rho_L c_L \frac{(M_L + 1)^2}{4} \end{aligned}$$

$$(M_n)_{I+1/2} = \left(\frac{V}{c}\right)_{I+1/2}$$
,  $M_R^- = \begin{cases} 0 & \text{if } M_R \ge +1 \\ \frac{1}{4}(M_R - 1)^2 & \text{if } |M_R| < 1 \end{cases}$ .  $(M_n)_{I+1/2} = M_L^+ + M_R^-$ ,

$$M_L = rac{V_L}{c_L} \,, \quad M_R = rac{V_R}{c_R} \,.$$

$$\vec{F}_c^{\pm} = \begin{bmatrix} f_{\text{mass}}^{\pm} \\ f_{\text{mass}}^{\pm} \left[ n_x (-V \pm 2c)/\gamma + u \right] \\ f_{\text{mass}}^{\pm} \left[ n_y (-V \pm 2c)/\gamma + v \right] \\ f_{\text{mass}}^{\pm} \left[ n_z (-V \pm 2c)/\gamma + w \right] \\ f_{\text{energy}}^{\pm} \end{bmatrix}$$

$$f_{\text{mass}}^+ = +\rho_L c_L \frac{(M_L + 1)^2}{4}$$

$$f_{\text{mass}}^- = -\rho_R c_R \, \frac{(M_R - 1)^2}{4}$$

$$f_{\rm energy}^{\pm} = f_{\rm mass}^{\pm} \left\{ \frac{[(\gamma-1)V \pm 2c]^2}{2(\gamma^2-1)} + \frac{u^2+v^2+w^2-V^2}{2} \right\}_{L/R} \,. \label{eq:fenergy}$$

$$|M_n| \geq 1$$

$$\vec{F}_c^+ = \vec{F}_c \quad \vec{F}_c^- = 0 \quad \text{if } M_n \ge +1$$

$$\vec{F}_c^+ = 0$$
  $\vec{F}_c^- = \vec{F}_c$  if  $M_n \le -1$ .



### 2. Advection Vpstream Splitting Method (AVSM)

$$\vec{F_c} = V \begin{bmatrix} \rho \\ \rho u \\ \rho v \\ \rho w \\ \rho H \end{bmatrix} + \begin{bmatrix} 0 \\ n_x p \\ n_y p \\ n_z p \\ 0 \end{bmatrix}.$$

$$(\bullet)_{L/R} = \begin{cases} (\bullet)_L & \text{if } M_{I+1/2} \ge 0\\ \\ (\bullet)_R & \text{otherwise} \end{cases}$$

Convective flux spilitting same as Van Leer

$$p_{I+1/2} = p_L^+ + p_R^-$$

$$p_L^+ = \left\{ egin{array}{ll} p_L & ext{if } M_L \geq +1 \ \\ rac{p_L}{4} (M_L + 1)^2 (2 - M_L) & ext{if } |M_L| < 1 \ \\ 0 & ext{if } M_L \leq -1 \end{array} 
ight. ,$$

$$p_R^- = \begin{cases} 0 & \text{if } M_R \ge +1 \\ \frac{p_R}{4} (M_R - 1)^2 (2 + M_R) & \text{if } |M_R| < 1 \\ p_R & \text{if } M_R \le -1 \end{cases}$$



## Some other convective flux discretization schemes continued.....

Central Schemes	First Order Upwind Schemes	Second Order Upwind Schemes
1. Combined Space-Time Integration (a) Explicit Schemes  Lax-Friendrichs – First order (1954)  Lax-Wendroff – Second order (1960) (b) Two-Step Explicit Schemes Richtmyer and Morton (1967) MacCormack (1969) LeRat and Peyret (1974) (c) Implicit Schemes MacCormack (1981) Casier, Deconinck, Hirsch (1983) LeRat (1979, 1983) 2. Separate Space-Time Integration (a) Implicit Schemes Briley and McDonald (1975) Beam and Warming (1976) (b) Explicit Schemes (Multistage Runge-Kutta) Jameson, Schmidt, Turkel (1981)	1. Flux Vector Splitting Courant, Isaacson, and Reeves (1952) Moretti (1979) Steger and Warming (1981) VanLeer (1982) 2. Godunov Methods-Riemann Solvers (a) Exact Riemann Solvers Godunov (1959) – First order VanLeer (1979) – Second order Woodward and Colella (1984) Ben-Artzi and Falcovitz (1984) (b) Approximate Riemann Solvers Roe (1981) Enquist and Osher (1980) Osher (1982) Harten, Lax, Van Leer (1983)	1. Extrapolation (a) Variable Extrapolation (MUSCL) Van Leer (1979) (b) Flux Extrapolation Van Leer (1979) 2. Explicit TVD Upwind VanLeer (1974) Harten (1983) Osher (1984) Osher and Chakravarthy (1984) 3. Implicit TVD Upwind Yee (1986) 4. Central TVD Implicit or Explicit Davis (1984) Roe (1985) Yee (1985) 5. Essentially Nonoscillatory Scheme Harten and Osher (1987) 6. Flux Corrected Transport Boris and Book (1973)





# Implementation of Central Scheme in OpenFoam: rhoCentralFoam

Features of rhoCentralFoam

- Finite Volume, density based solver.
- Non-staggered/collocated field variables.
- Central/Central-upwind scheme.
- Applicable on polyhedral Mesh.
- Suitable for high speed viscous flows.



# Some of the Important Solution Methodology for High Speed Flows

- Notable methods for producing accurate non-oscillatory solutions are (convective terms discretization of governing equations)
- Monotone upstream-centred scheme for conservation laws
- Piece wise parabolic method (PPM)
- Essentially non-oscillatory scheme (ENO)
- Weighted ENO (WENO)

The above methods are complicated as they involve Riemann solvers, characteristic decomposition and Jacobian evaluation.

They are complex to implement!!





• To avoid the difficulty of implementation and to reduce cost of computation, Central schemes were devised which was first proposed by Nessyahu and Tadmor as second order accurate version of Lax-Friedrichs scheme.

• The more advanced versions of central scheme widely used to solve industrial problems are Kurganov-Tadmor (KT) and Kurganov-Noelle-Petrova (KNP) schemes

• These schemes are implemented in OpenFOAM package, with "rhoCentralFoam" as the solver name



## **Governing Equations: Differential Form**

Continuity fquation

$$\frac{\partial \rho}{\partial t} + \nabla \cdot [\boldsymbol{u} \rho] = 0$$

Momentum fquation

$$\frac{\partial(\rho \boldsymbol{u})}{\partial t} + \nabla \cdot [\boldsymbol{u}(\rho \boldsymbol{u})] + \nabla p + \nabla \cdot \boldsymbol{T} = 0$$

Conservation of Jotal Inergy

$$\frac{\partial(\rho E)}{\partial t} + \nabla \cdot [\mathbf{u}(\rho E)] + \nabla \cdot (\mathbf{u}p) + \nabla \cdot (\mathbf{T}\mathbf{u}) + \nabla \cdot \mathbf{j} = 0$$



• Here  $\rho$  is the mass density u is the fluid velocity, p is the pressure,

Total energy density  $E=e+0.5 |\mathbf{u}|^2$  with 'e' as specific internal energy j as the diffusion heat flux vector,  $\mathbf{T}$  is the viscous shear stress tensor (defined positive in compression)

 $T=-2\mu dev(D)$ 

μ is the dynamic viscosity (Sutherland's law or constant)

 $\mathbf{D} = \frac{1}{2} [\nabla \mathbf{u} + \nabla \mathbf{u}^T]$  (Deformation gradient tensor)

Deviatoric component  $dev(\mathbf{D}) = \mathbf{D} - \left(\frac{1}{3}\right) tr(\mathbf{D})\mathbf{I}$  *I* is the unit tensor

The diffusion heat flux vector defined by

 $j = -k\nabla T$  (Fourier's Law)

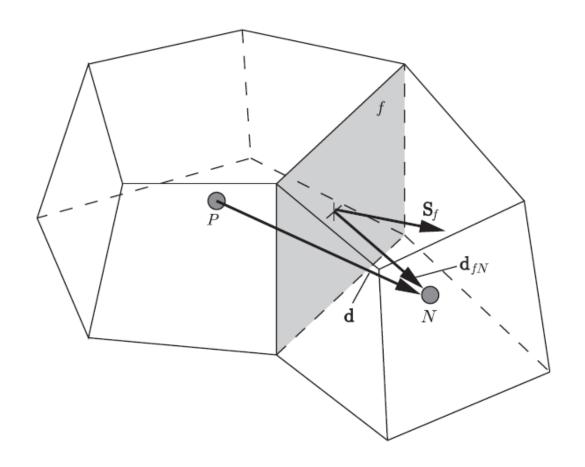
k= thermal conductivity

T= temperature

For calorically perfect gas,  $p=\rho RT$  and  $e=CvT=(\gamma-1)RT$   $\gamma=Cp/Cv$ , R is characteristic gas constant



## **Computational Method**



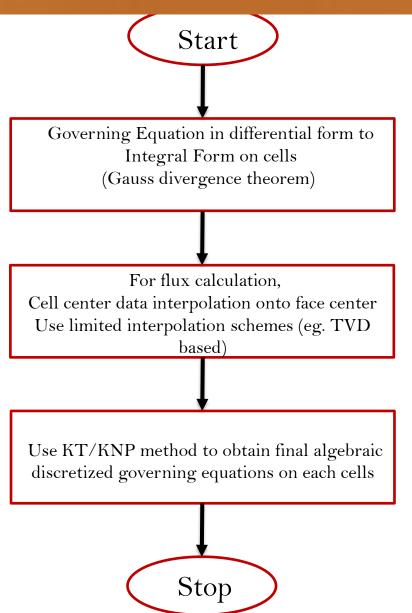
 $d_{fN}$  vector connecting face centre and cell centre of neighbouring cell d Vector connecting cell centre  $\mathbf{P}$  and cell centre  $\mathbf{N}$ 

 $S_f$  face area vector (outwards is positive)

All variables are stored at cell centres (**P,N**....)

(82)





The KT/KNP convective flux discretization method shall be explained in upcoming slides.....

Procedure to obtain discretized algebraic governing equation on collocated finite volume grid





# The Algebraic Discretized Equation

• The general variable  $\psi$  (tensor of any rank) can be convected in the flow field, the general term associated with convection in GE is:  $\nabla \cdot (u\psi)$ 

Application of Gauss divergence theorem

$$\iiint \nabla . (\boldsymbol{u}\boldsymbol{\psi}) dV = \iint d\boldsymbol{S}. [\boldsymbol{u}\boldsymbol{\psi}] = \sum_{f} S_{f}. [\boldsymbol{u}_{f}\boldsymbol{\psi}_{f}] = \sum_{f} \varphi_{f}\boldsymbol{\psi}_{f}$$

Here,  $\phi_f$  is the volumetric flux



## **Convective Terms**

• The general variable  $\psi$  (tensor of any rank) can be convected in the flow field, the general term associated with convection in GE is:

$$\nabla . (u\psi)$$

Application of Gauss divergence theorem

$$\iiint \nabla . (\boldsymbol{u}\boldsymbol{\psi}) dV = \iint d\boldsymbol{S}. [\boldsymbol{u}\boldsymbol{\psi}] = \sum_{f} S_{f}. [\boldsymbol{u}_{f}\boldsymbol{\psi}_{f}] = \sum_{f} \varphi_{f}\boldsymbol{\psi}_{f}$$

Here,  $\phi_f$  is the volumetric flux



$$\alpha = \begin{cases} \frac{1}{2} & for \ KT \ method \\ \frac{\lambda_{f+}}{\lambda_{f+}} & for \ KNP \ method \end{cases}$$

$$\lambda_{f+} = \max(c_{f+}|\mathbf{S}_{f}| + \phi_{f+}, c_{f-}|\mathbf{S}_{f}| + \phi_{f-}, 0)$$
  
$$\lambda_{f-} = \max(c_{f+}|\mathbf{S}_{f}| - \phi_{f+}, c_{f-}|\mathbf{S}_{f}| - \phi_{f-}, 0)$$

$$\omega_f = \begin{cases} \alpha \max(\lambda_{f+}, \lambda_{f-}) & for \ KT \ method \\ \alpha(1-\alpha)(\lambda_{f+}+\lambda_{f-}) & for \ KNP \ method \end{cases}$$



### **Gradient Terms**

$$\iiint \nabla(\boldsymbol{\psi})dV = \iint d\boldsymbol{S}\boldsymbol{\psi} = \sum_{f} \boldsymbol{S}_{f}\boldsymbol{\psi}_{f}$$

$$\sum_{f} \mathbf{S}_{f} \boldsymbol{\psi}_{f} = \sum_{f} [\alpha \mathbf{S}_{f} \boldsymbol{\psi}_{f^{+}} + (1 - \alpha) \mathbf{S}_{f} \boldsymbol{\psi}_{f^{-}}]$$



## **Laplacian Terms**

$$\iiint \nabla \cdot (\Gamma \nabla \boldsymbol{\psi}) dV = \iint d\boldsymbol{S} (\Gamma \nabla \boldsymbol{\psi}) = \sum_{f} \Gamma_{f} \boldsymbol{S}_{f} \cdot (\nabla \boldsymbol{\psi})_{f}$$

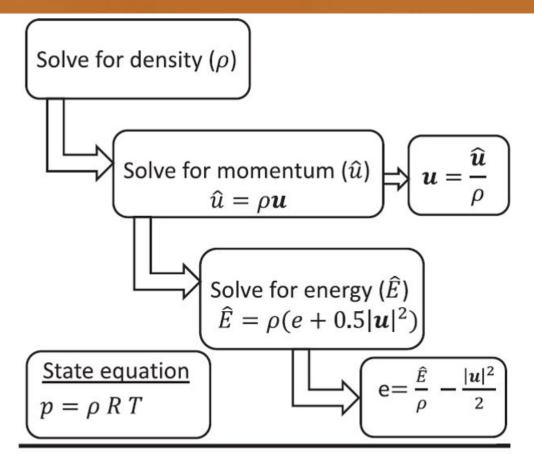
For Non-orthogonal Mesh,

$$S_f.(\nabla \psi)_f = A(\psi_N - \psi_P) + a.(\nabla \psi)_f$$

$$A = \frac{|S_f|^2}{S_f \cdot d}$$

$$a = S_f - Ad$$





Solve Viscous part to correct **u** and e

Solution Algorithm of rhoCentral foam





## **OpenFoam File: Implementation**

```
surfaceScalarField rho pos(interpolate(rho, pos));
surfaceScalarField rho neg(interpolate(rho, neg));
surfaceVectorField rhoU pos(interpolate(rhoU, pos, U.name()));
surfaceVectorField rhoU_neg(interpolate(rhoU, neg, U.name()));
volScalarField rPsi("rPsi", 1.0/psi);
surfaceScalarField rPsi pos(interpolate(rPsi, pos, T.name()));
surfaceScalarField rPsi neg(interpolate(rPsi, neg, T.name()));
surfaceScalarField e pos(interpolate(e, pos, T.name()));
surfaceScalarField e neg(interpolate(e, neg, T.name()));
surfaceVectorField U pos("U pos", rhoU pos/rho pos);
surfaceVectorField U_neg("U_neg", rhoU_neg/rho_neg);
surfaceScalarField p_pos("p_pos", rho_pos*rPsi_pos);
surfaceScalarField p neg("p neg", rho neg*rPsi neg);
surfaceScalarField phiv pos("phiv pos", U pos & mesh.Sf());
// Note: extracted out the orientation so becomes unoriented
phiv pos.setOriented(false);
surfaceScalarField phiv neg("phiv neg", U neg & mesh.Sf());
phiv neg.setOriented(false);
```

```
volScalarField c("c", sqrt(thermo.Cp()/thermo.Cv()*rPsi));
surfaceScalarField cSf_pos
(
    "cSf_pos",
    interpolate(c, pos, T.name())*mesh.magSf()
);
surfaceScalarField cSf_neg
(
    "cSf_neg",
    interpolate(c, neg, T.name())*mesh.magSf()
);
```

Interpolation of variables from left and right side of interface of control volume





```
surfaceScalarField ap
    "ap",
    max(max(phiv_pos + cSf_pos, phiv_neg + cSf_neg), v_zero)
);
surfaceScalarField am
    "am",
   min(min(phiv_pos - cSf_pos, phiv_neg - cSf_neg), v_zero)
);
surfaceScalarField a pos("a pos", ap/(ap - am));
surfaceScalarField amaxSf("amaxSf", max(mag(am), mag(ap)));
surfaceScalarField aSf("aSf", am*a pos);
if (fluxScheme == "Tadmor")
    aSf = -0.5*amaxSf;
    a pos = 0.5;
surfaceScalarField a neg("a neg", 1.0 - a pos);
phiv pos *= a pos;
phiv_neg *= a_neg;
surfaceScalarField aphiv_pos("aphiv_pos", phiv_pos - aSf);
surfaceScalarField aphiv neg("aphiv neg", phiv neg + aSf);
```

Calculations for scalar dissipation coefficient
for Ko or Ko scheme based on
user input flag (fluxScheme=="Tadmor")



```
phi = aphiv_pos*rho_pos + aphiv_neg*rho_neg;

surfaceVectorField phiU(aphiv_pos*rhoU_pos + aphiv_neg*rhoU_neg);
// Note: reassembled orientation from the pos and neg parts so becomes
// oriented
phiU.setOriented(true);

surfaceVectorField phiUp(phiU + (a_pos*p_pos + a_neg*p_neg)*mesh.Sf());

surfaceScalarField phiEp
(
    "phiEp",
    aphiv_pos*(rho_pos*(e_pos + 0.5*magSqr(U_pos)) + p_pos)
    + aphiv_neg*(rho_neg*(e_neg + 0.5*magSqr(U_neg)) + p_neg)
    + aSf*p_pos - aSf*p_neg
);
```

Calculation of Convective Fluxes of Governing *Equations* 



```
volScalarField muEff("muEff", turbulence->muEff());
volTensorField tauMC("tauMC", muEff*dev2(Foam::T(fvc::grad(U))));
Calculation of viscosity and shear stress tensor
// --- Solve density
solve(fvm::ddt(rho) + fvc::div(phi)); Solves density equation
// --- Solve momentum
solve(fvm::ddt(rhoU) + fvc::div(phiUp));
                             Predictor step of momentum equation
U.ref() =
    rhoU()
                          Update Boundary Condition on U
   /rho();
U.correctBoundaryConditions();
rhoU.boundaryFieldRef() == rho.boundaryField()*U.boundaryField();
if (!inviscid)
                          Viscous Corrector
    solve
                          step of momentum equation
        fvm::ddt(rho, U) - fvc::ddt(rho, U)
      - fvm::laplacian(muEff, U)
      - fvc::div(tauMC)
    rhoU = rho*U;
// --- Solve energy
surfaceScalarField sigmaDotU
                       Calculation of work done by viscous forces
    "sigmaDotU",
        fvc::interpolate(muEff)*mesh.magSf()*fvc::snGrad(U)
      + fvc::dotInterpolate(mesh.Sf(), tauMC)
  & (a_pos*U_pos + a_neg*U neg)
```

```
solve
    fvm::ddt(rhoE)
                         Predictor step of energy equation
  + fvc::div(phiEp)
  fvc::div(sigmaDotU)
);
e = rhoE/rho - 0.5*magSqr(U);
e.correctBoundaryConditions(); Update Boundary Condition on e
thermo.correct();
                               Extract temperature from e
rhoE.boundaryFieldRef() ==
    rho.boundaryField()*
                               Update boudanry field of rhoE
        e.boundaryField() + 0.5*magSqr(U.boundaryField())
    );
if (!inviscid)
                           Viscous Corrector
                           step of energy equation
    solve
       fvm::ddt(rho, e) - fvc::ddt(rho, e)
      - fvm::laplacian(turbulence->alphaEff(), e)
    thermo.correct();
    rhoE = rho*(e + 0.5*magSqr(U));
```



```
p.ref() =
    rho()
    /psi();
p.correctBoundaryConditions();
rho.boundaryFieldRef() == psi.boundaryField()*p.boundaryField();

turbulence->correct();

runTime.write();

runTime.printExecutionTime(Info);
```

Update value of pressure field and continue to the next time loop

## **Demo examples in OF: CFD**



#### • The Sod's Shock Tube Problem

**Initial Conditions** 

The state on the left side of the diaphragm is denoted by L

High Pressure

Low Pressure

$$\rho_L = 1.0 \text{ kg/m}^3$$
,  $p_L = 100000 \text{ Pa}$ ,  $T_L = 348.4 \text{ K}$ 

The state on the left side of the diaphragm is denoted by L

$$\rho_R = 0.125 \text{ kg/m}^3$$
,  $p_R = 10000 \text{ Pa}$ ,  $T_R = 278.7 \text{ K}$ 

## **Demo examples in OF: CFD**



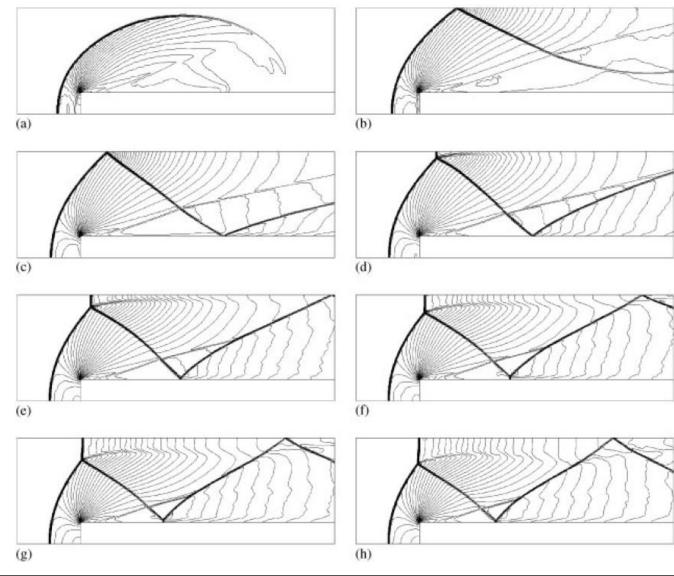
Forward Step (Woodward and Collela)



Unsteady flow over the forward step placed in supersonic stream of air

Mach 3 flow

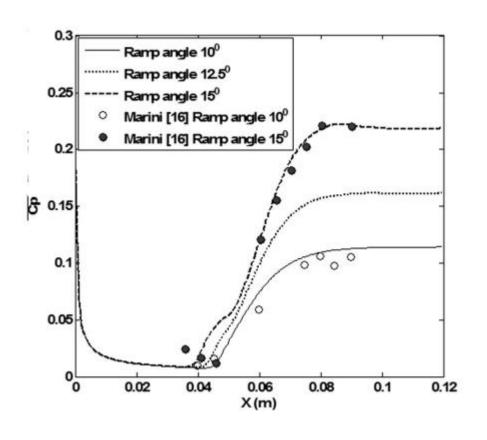
A standard benchmark test case to access the Performance of various numerical schemes



## **Demo examples in OF: CFD**



• Shock wave boundary layer interaction on compression corner



U=1380m/s P=191.4345 Pa T=131.7 Twall = 300 K

