

# PROJECT ASSIGNMENT #2: COMBUSTION THERMODYNAMICS



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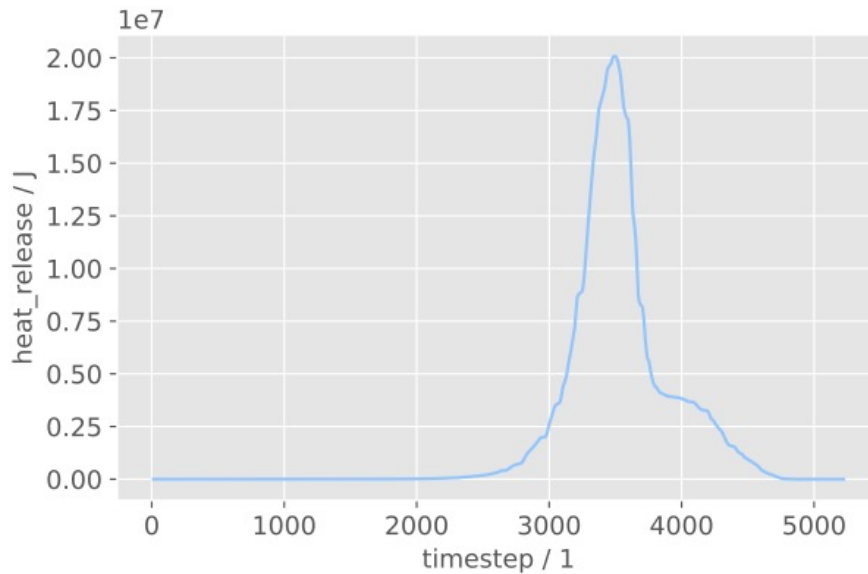
## Part II – Explosion theory

Note that all the figures regarding heat release, the unit should be in Watt instead of J, as displayed on the axis.

1. Calculate the volume and surface of this reactor

$$A = 4\pi r^2 = 4\pi * 0.037^2 = 0.017203 \text{ m}^2$$
$$V = \frac{4}{3} \pi r^3 = \frac{4}{3} \pi * (0.037)^3 = 2.12175 * 10^{-4} \text{ m}^3$$

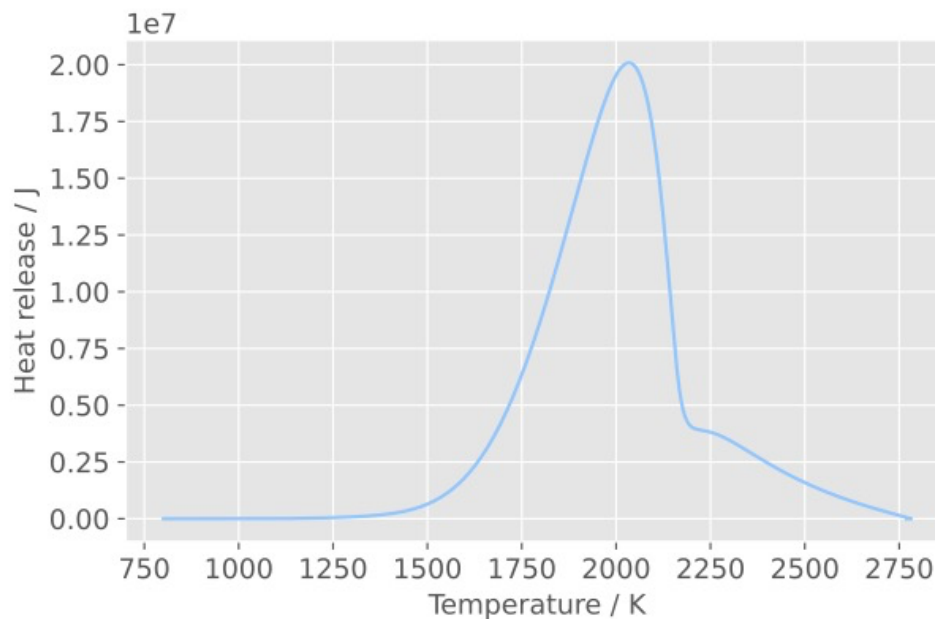
2. Execute the simulation and calculate the heat release per time step



3. Does the mixture ignite?

Yes, it auto ignites at  $t = 2.844500375606927\text{s}$

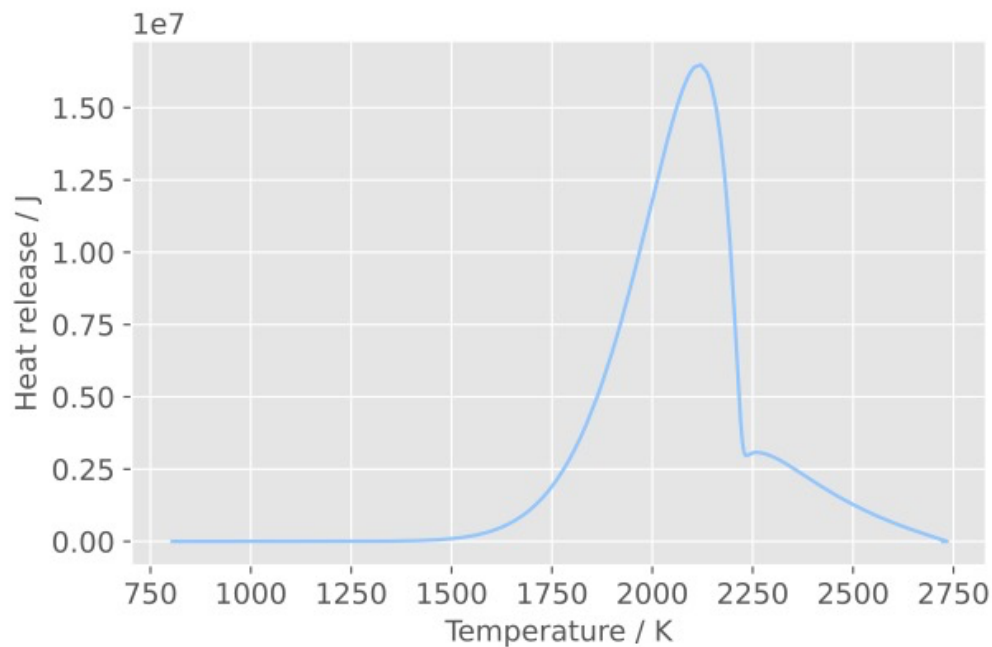
4. Plot the heat release of the reactor versus its temperature



### 5. Using a lighter gas methane

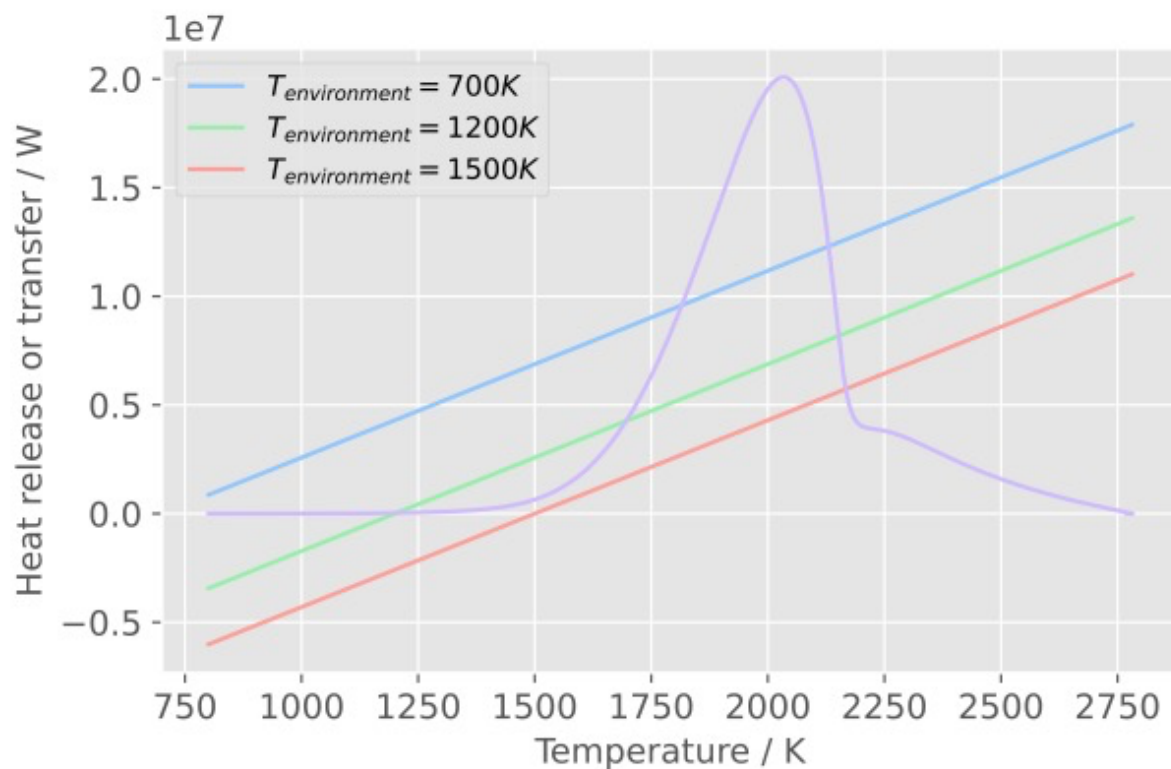
While a lighter gas methane is used, after researching about its ignition temperature at 1 atm, which is higher than that of the iso-octane, the estimated ignition delay time was pushed back to 200s to successfully auto-ignite the species.

The computed ignition delay is 143.24537259330438 s



The maximum heat release of methane is lower than that of the iso-octane, since methane is a more stable specie compared to isooctane hence a longer reaction time. IDT of such reaction should be longer compared to IDT of isooctane.

6. Compute the heat loss function
7. Plot



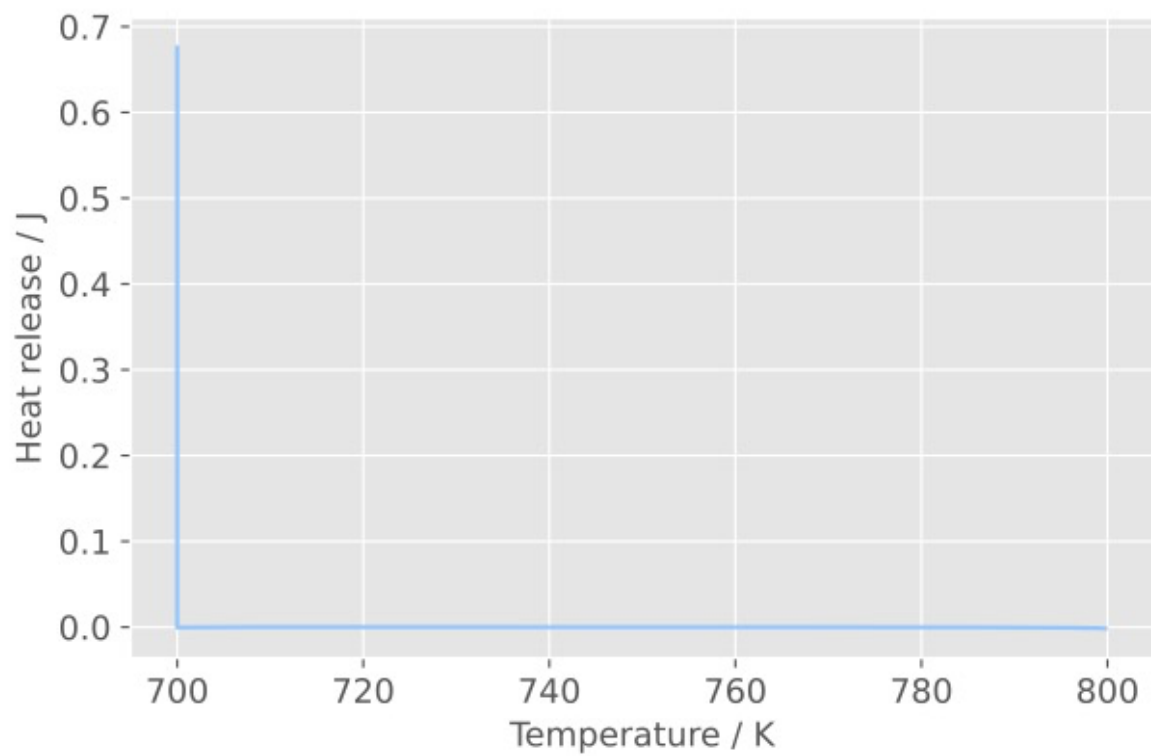
8. Determine if the mixture will ignite.

From the above plot, the mixture will only ignite when the environmental temperature is  $1500\text{K}$ . Two other environmental temperature will not lead to auto-ignition for the following reason:

- The slope is higher than the critical condition, hence the heat loss will be more than the heat generation in the combustor, causing the ignition to fail.
- For the case  $T_{\text{env}} = 1500\text{K}$ , the slope is lower than the point of criticality, and that means the heat generation in the combustor is higher than the heat loss to the surroundings, therefore the ignition could still be successful.

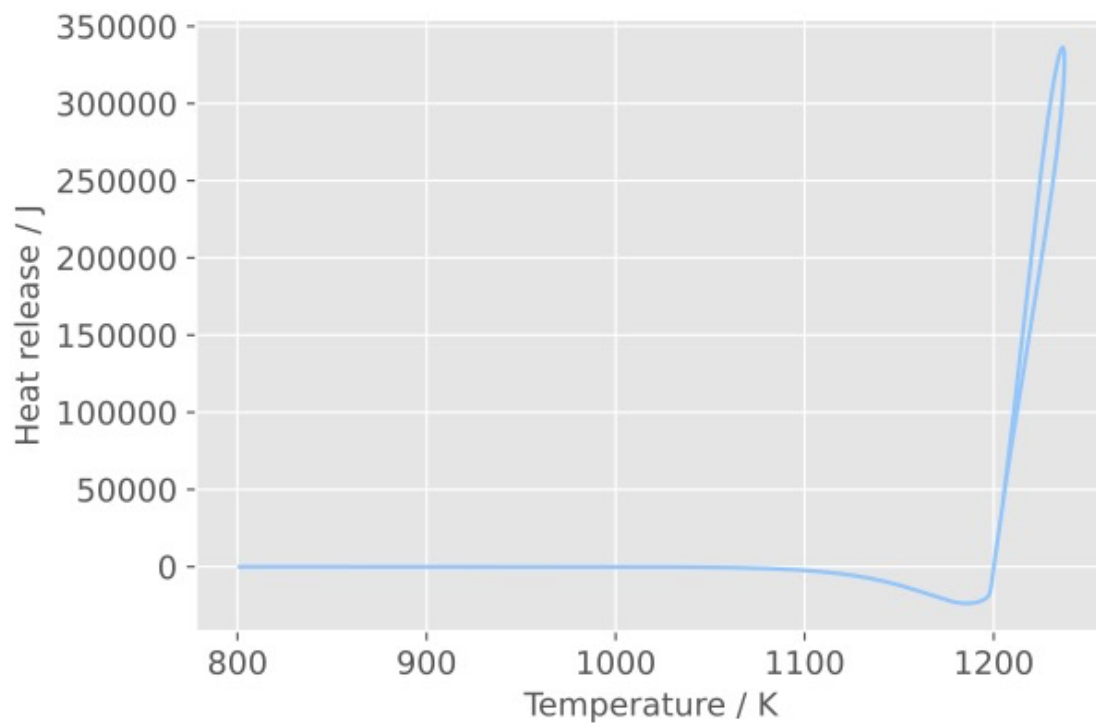
9. Confirm your theory by computing a reactor with the same heat loss functions than for Q6.

a.  $T_{\text{env}} = 700\text{K}$



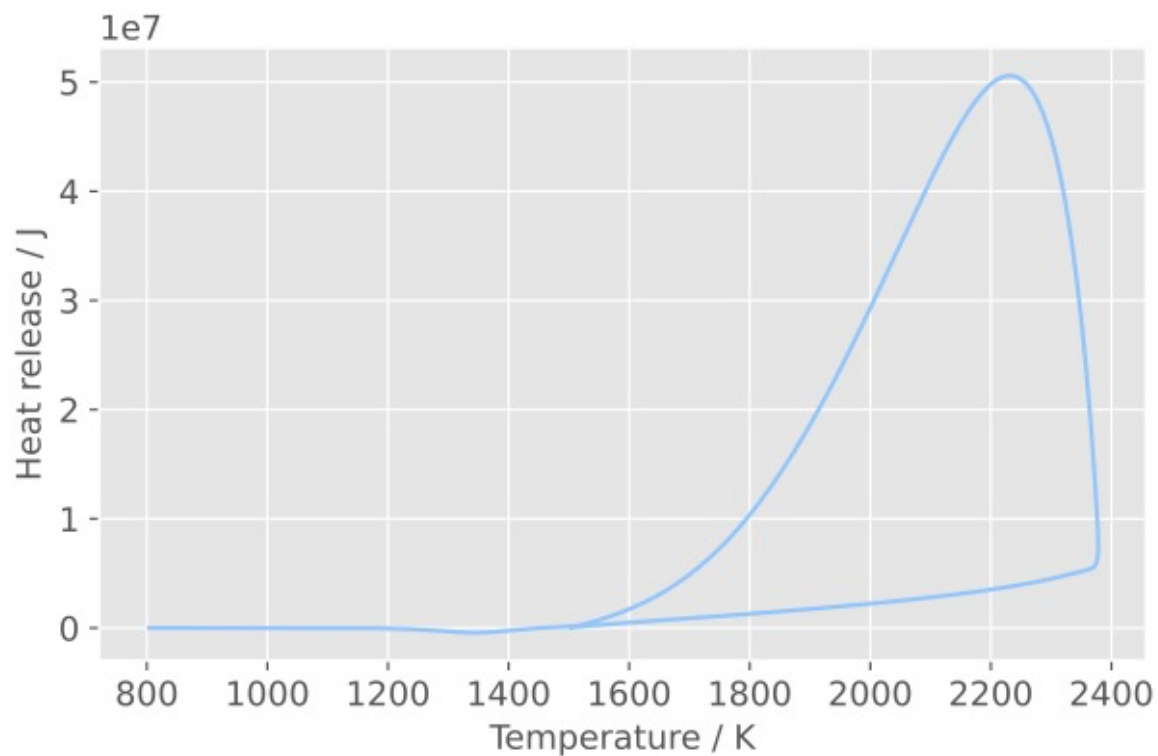
Heat release = 0, no auto ignition until  $t = 500\text{s}$ .

b.  $T_{\text{env}} = 1200\text{K}$



There exists heat release due to heat transfer to the surrounding, but it is still not high enough to conclude that there have been an auto ignition.

c.  $T_{env} = 1500K$



There exists enough heat release (around 50MW) to conclude that there have been an auto-ignition in the combustor, the temperature inside the combustor have also raised far above the environment due to the release of chemical potential energy inside the fuel.

#### 10. Ignition time calculation and comment

As stated above, auto-ignition will only take place for  $T_{env} = 1500 K$ , and the calculated ignition delay for such case is  $1.569007381918055e-05 s$ . Compared to the delay in the adiabatic case,  $t = 2.844500375606927s$ , the ignition delay for the non-adiabatic case was much shorter. The reason behind that is probably:

- The ignition delay was computed when the mixture reached a temperature of 1300K (800K initial combustor temp + 500K), hence at  $T_{env} = 1500K$ , there have been heat transfer into the combustor, causing the ignition delay to decrease

## Part III – Perfectly stirred reactor

### 1. Mass flow rate and equivalence ratio of iso-Octane

$$\eta = \frac{P_{out}}{\dot{Q}_{in}} = 42\%$$
$$\dot{Q}_{in} = P_{out}/0.42 = 120/0.42 = 285.714 \text{ MJ/s}$$
$$\dot{m}_{in} = \frac{\dot{Q}_{in}}{\text{Heating Value}} = 285.714/45 = 6.3492 \text{ kg/s}$$
$$\phi = \frac{6.3429/240}{144/1716} = \frac{0.03536173768}{0.04} = 0.3982$$

### 2. Equilibrium flame temperature, mole fractions of CO and NO

$$T_{equilibrium} = 1720K$$
$$X_{CO} = 0.0000023209 = 2.3209PPM$$
$$\text{e } X_{NO} = 0.0023688935$$

### 3. The concentration of PSR

$$X_{CO} = 0.0002324804 = 232.4804PPM$$
$$X_{CO} = 0.0000051471 = 5.1471PPM$$

### 4. The residence time of PSR

$$T_{res} = 9.9ms$$

### 5. How does the PSR concentration values for CO and NO compare with the equilibrium values

	Equilibrium	PSR
X_CO / PPM	2.32	232.48
X_NO / PPM	2368.89	5.1471

- The concentration of CO is higher in PSR due to the limited  $T_{res}$ , not enough CO is having time to be oxidized to CO<sub>2</sub> before exiting the reactor, also since in the equilibrium condition is assuming complete combustion, less CO concentration is formed.
- The concentration of NO is much lower than the equilibrium condition, also due to the short  $T_{res}$ . The formation of NO is highly dependent on reaction time. The reaction is not complete in the PSR reactor, and in the equilibrium case, more time could be taken to form the NO. As the formation of NO requires long time and high heat release.

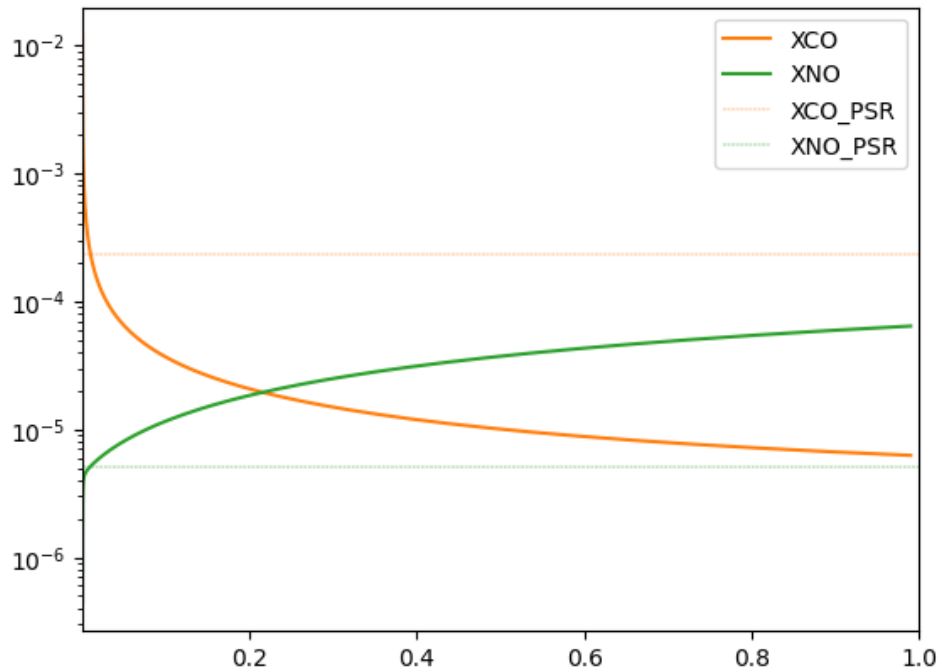
### 6. Temperature difference

	Equilibrium	PSR
Flame Temperature / K	1720	1723

- The temperature in the PSR is only slightly higher than that of the equilibrium case since the reaction time is long enough to consume all the chemical potential of the reactant. However, due to less NO is formed in the reactor, although more CO is formed in the PSR compared to equilibrium case, in total, more energy is used to form product, hence lower the temperature.



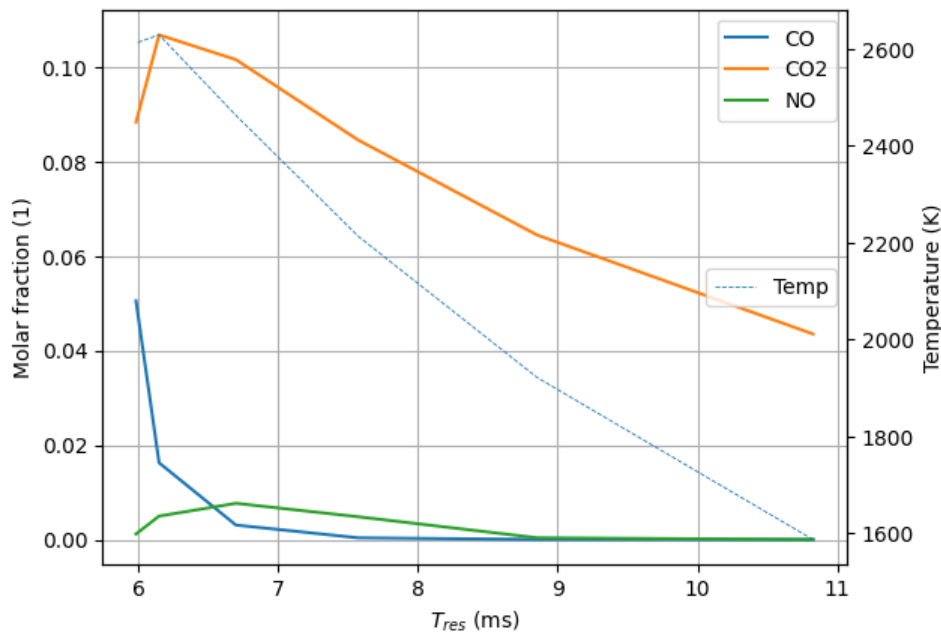
Bonus -



The x axis label will be  $T_{res} / s$  and y axis label is concentration, in log scale.

From the figure above, we could conclude that as the  $T_{res}$  increases, the concentration of CO decreases and that of the NO increases. The interception points between the dotted and solid line for both orange and green colour stands for the  $T_{res} = 9.9 \text{ ms}$ . Although both concentrations are not converging to the values in the equilibrium conditions, the trend could explain the drill here – more complete combustion, more NO formed and less CO formed at the given equivalence ratio, pressure. Since the formation of NO is endothermic and that of CO is exothermic, the temperature of the PSR is slightly higher than that of the equilibrium condition.

7. Looping through different power output, from 100MW to 350MW, in steps of 50MW

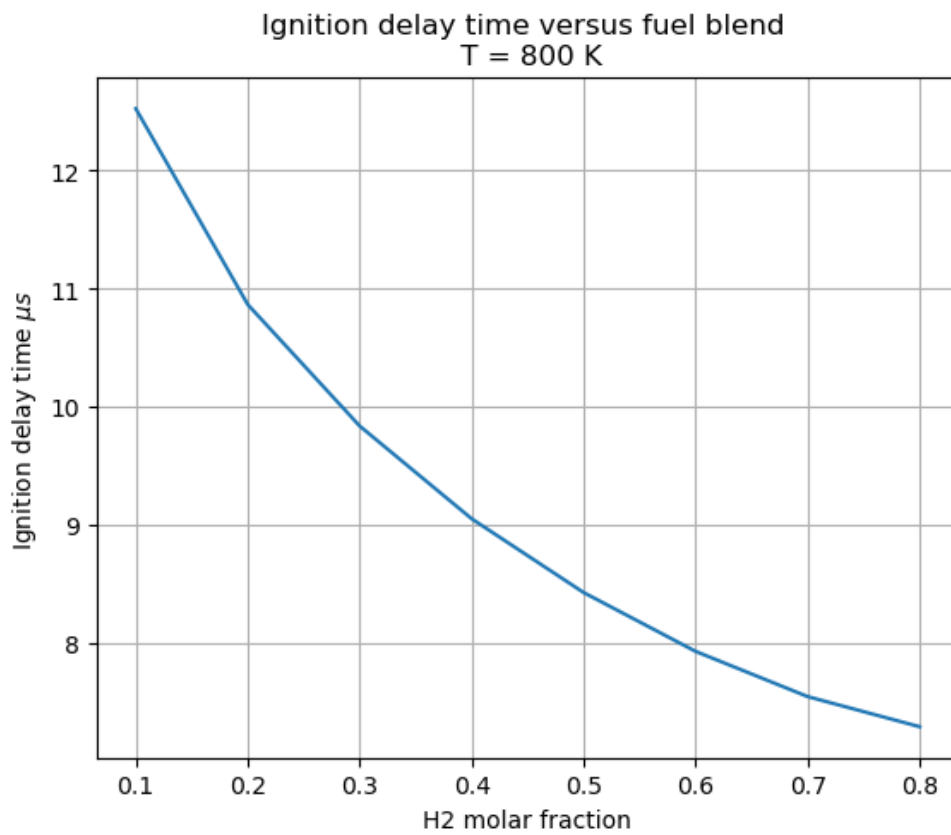
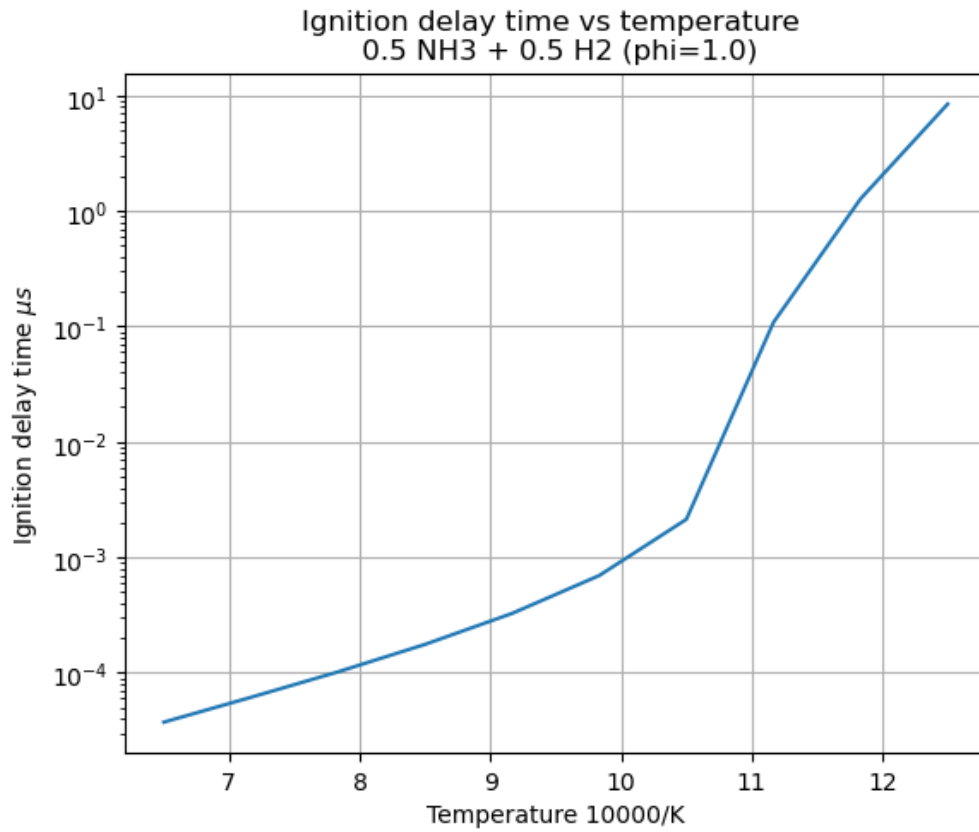


Power (MW)	M dot (kg/s)	phi	T res(ms)
100	5.291	0.33146	10.84062
150	7.937	0.49719	8.82521
200	10.582	0.66291	7.54112
250	13.228	0.82864	6.68887
300	15.873	0.99437	6.14994
350	18.519	1.16010	5.98743

- The optimal residence time is around 6.15ms, since the temperature is at its peak at such time.
- When the residence time is decreased from 6.15s, there is too much fuel going into the combustor, resulting in a incomplete combustion.
- When the residence temperature increases from 6.15s, there is too much air going in, resulting in a incomplete combustion, however the CO concentration decreases.
- At 6.15ms, the concentration of NO pollutant is high. The optimal selection for industrial setting is probably 8ms or 9ms depending on if a cleaner solution is desired or a higher output is desired. At such values, less pollutant is formed than the 6.15ms case.

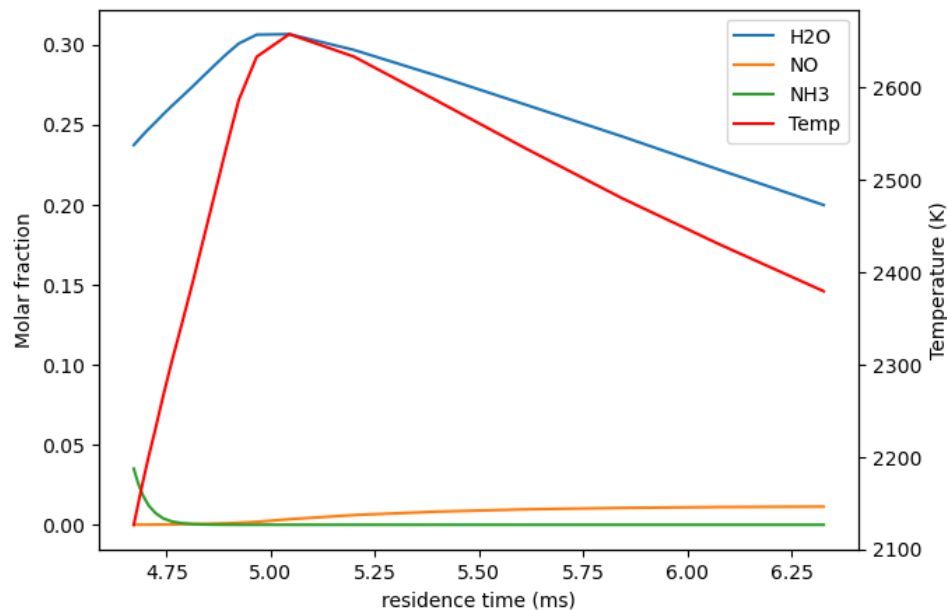
## Part VI: Relate this assignment to your design project

A good ignition delay time tracer for  $\text{NH}_3 + \text{H}_2$  combustion is the maximum gradient of the  $\text{OH}^*$  species (OH in an excited state). The  $\text{OH}^*$  formation sub-mechanism is included in the mechanism file.



- Reaction is faster when the initial state is hotter
- IDT is slower compared to C<sub>8</sub>H<sub>18</sub> (around 8.5 s versus 2.85 s) for the X(H<sub>2</sub>) = 0.5 blend

- When there is more hydrogen, the mixture ignites faster
- The range of IDT when modifying the hydrogen molar fraction suggests that a blend can be made to obtain specific combustion properties



- Lean combustion reduces the amount of NO produced but NH<sub>3</sub>, another harmful pollutant remains in important quantities
- At the stoichiometric residence time an important amount of NO is present in the exhaust
- For similar equivalence ratio, and the same air mass flow the temperature is much higher than for C<sub>8</sub>H<sub>18</sub>

Some improvements:

- Two points exist where  $X(\text{NO}) = X(\text{NH}_3)$  which could be used to react them together in an exhaust post treatment process
- Lean combustion cannot be used to reduce the pollution, thus inventive techniques should be used, such as a two-stage combustor
- Adding ammonia to hydrogen reduces the IDT and makes it safer.